

Method and Apparatus for Measuring The Calorific Value Of A Gas

This invention relates to a method and apparatus for measuring the calorific value of a gas.

The gas may be a fuel gas, for example natural gas. The natural gas may be methane and may further comprise nitrogen and/or carbon dioxide. In addition to methane the natural gas may comprise at least one other hydrocarbon gas, for example ethane, propane, butane, pentane or hexane.

According to one aspect of the invention, a method of measuring the calorific value of a gas comprises making a measure of the speed of sound in the gas and using the speed of sound in an operation producing the calorific value corresponding to said speed of sound.

According to another aspect of the invention a method of measuring the calorific value of a gas comprises making a measure of the speed of sound in the gas, making a measure of a first thermal conductivity of the gas at a first temperature, making a measure of a second thermal conductivity of the gas at a second temperature which differs from the first temperature, and using the speed of sound and the first and second thermal conductivities in an operation producing the calorific value of the gas corresponding to said speed of sound and said first and second thermal conductivities.



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According to a further aspect of the invention an apparatus to measure the calorific value of a gas comprises means to measure the speed of sound in the gas and means to use the speed of sound in an operation producing the calorific value of the gas corresponding to said speed of sound.

According to a still further aspect of the invention an apparatus to measure the calorific value of a gas comprises means to measure a first thermal conductivity of the gas at a first temperature; means to measure a second thermal conductivity of the gas at a second temperature which differs from the first temperature, and means using the speed of sound and the first and second thermal conductivities in an operation producing the calorific value of the gas corresponding to said speed of sound and said first and second thermal conductivities.

The invention will now be further described, by way of example, with reference to the accompanying drawings in which:

Figure 1 diagrammatically shows an apparatus in which the invention can be performed; and

Figure 2 shows a diagrammatic example of a feed forward air/fuel gas control system utilising the present invention.

With reference to Figure 1 an apparatus 2 to measure the calorific value of a gas has a chamber 4 into which the gas is supplied through an inlet conduit 6 and leaves through an outlet

conduit 8. The inlet conduit 6 includes heat exchange means 6A, for example a copper coil by which the temperature of the incoming gas can be adjusted to a value substantially the same as that of the ambient temperature of the external atmosphere whereby the gas in the chamber 4 is of substantially uniform temperature throughout. The chamber 4 includes an ultra-sound emitter transducer 10 and an ultra sound receiver transducer 12. An electronic control means 14 including computer means is connected to a signal generator 16 so that under the control of the control means 14 the signal generator causes the transducer 10 to emit ultra-sound signals 18 as desired. The ultra-sound signals 18 are received by the transducer 12 and their reception signalled to the control means 14 via line 20. The time of flight of the ultra-sonic signals between transducers 10 and 12 is measured by the control means 14 which is arranged to calculate SOS which is the speed of sound in metres/second (m/s).

If desired some other means of measuring the speed of sound in the gas may be used, such as that disclosed in US4938066. However, the most preferable method is that disclosed in UK patent application Nos. GB 9813509.8, GB 9813513.0 and GB 9813514.8. These applications disclose the use of a resonator to measure the speed of sound of a gas within the resonator. A driving electronic circuit which may include or be in the form of a microprocessor is arranged to produce a sinusoidal signal over a suitable range of frequencies to drive a loudspeaker. The loudspeaker is arranged to apply an acoustic signal to the interior of a resonator. A microphone is arranged to detect the

magnitude of the acoustic signal within the resonator. The signal from the microphone is filtered and amplified by an appropriate electronic circuit and a processing means determines the resonant frequency relating to the gas within the resonator to determine its speed of sound.

A temperature sensor 22 in the chamber 4 provides the control means 14 with data on line 24 representing the value of the ambient temperature.

The ambient temperature sensor 22 may be part of a thermal conductivity sensor 28 comprising thermal conductivity observation means 30. The thermal conductivity sensor 28 may be a miniature thermal conductivity microsensor model type TCS208 available from Hartmann & Braun AG of Frankfurt am Main, Germany.

The thermal conductivity observation means 30 to observe the thermal conductivity of the gas has heater means which in response to signals on line 32 from the control means 14 can operate at more than one selected desired temperature above the ambient temperature observed by the sensor 22, and a signal representative of the thermal conductivity of the gas at the desired temperature is sent to the control means on line 34.

The control means 14 is arranged to cause the thermal conductivity sensor 28 to measure the thermal conductivity of the gas at two different desired temperatures t_H and t_L in which t_H is a pre-determined desired number of temperature degrees t_L

above the ambient temperature observed by the sensor 22 and t_L is a predetermined desired number of temperature degrees t_1 above ambient temperature; the number t_1 being greater than the number t_2 .

Using the observed or measured values of the speed of sound in the gas, the thermal conductivity of the gas at temperature t_H and t_L and the observed value of the ambient temperature of the gas by sensor 22, the control means 14 calculates the calorific value of the gas using the formula

$$CV = a.ThC_H + b.ThC_L + c.SoS + d.T_a + e.T_a^2 + f \quad - I$$

in which

CV is the calorific value;

ThC_H is the thermal conductivity of the gas at temperature t_H ;

ThC_L is the thermal conductivity of the gas at temperature t_L ;

SoS is the speed of sound in the gas at the ambient temperature;

T_a is the ambient temperature of the gas observed by the sensor 22, and a, b, c, d, e and f are respective constants.

The gas in question may be a mixture of two or more gases in which the composition of the mixture may be of variable proportions. For example the gas in question may be a fuel gas. Such a fuel gas may be natural gas. The natural gas may comprise methane and at least one of ethane, propane, butane, pentane or hexane, and may further comprise nitrogen and/or carbon dioxide.

In order to derive the constants a, b, c, d, e, and f in equation I, the mathematical technique known as regression analysis may

be used in respect of data collected in connection with the gas in question. The proportions of gases in the mixture may be varied to form a number of different samples. Using chromatographic methods the calorific value CV of a sample is obtained, the ambient temperature T_a of the sample is measured and the thermal activities ThC_H and ThC_L of the sample are measured. This is done for each sample in turn to obtain a set of measured values corresponding to each sample. The sets of values are inserted in equation I and the "best-fit" values for constants a, b, c, d, e and f are derived. In the case of natural gas coming ashore at a number of locations in the United Kingdom regression analysis was performed on samples from the different locations and also on gas equivalence groups which are artificial replications in the laboratory of mixtures of methane and ethane, methane and butane, methane and pentane, and methane and hexane in which, in the laboratory, those mixtures are represented by different mixtures of methane and propane.

When equation I was applied to natural gas and to gas equivalence groups and regression analysis used, the following values for the constants were derived, namely:-

a = 36.25649,

b = -45.5768,

c = 0.047029

d = 0.091067,

e = 0.00074, and

f = 24.18731, when

CV is the calorific value of gas in $\text{MJ/m}^3_{\text{st}}$ (Megajoules/standard cubic metres);

ThC_H is the thermal conductivity of the gas in W/m.K (where K is degrees Kelvin) at a temperature of substantially 70 degrees Celsius above ambient temperature T_a ;

ThC_L is the thermal conductivity of the gas in W/m.K at a temperature t_L which is substantially 50 degrees Celsius above ambient temperature T_a ;

SoS is the speed of sound in the gas in m/s , and

T_a is the ambient temperature of the gas in degrees Celsius.

In the above application of equation I to natural gas the value of t_L is substantially 70°C and the value of t_H is substantially 50°C . Thus the difference between the temperatures t_H and t_L at which the thermal conductivities ThC_H and ThC_L are measured differ by substantially 20°C [$(T_a + 70) - (T_a + 50) = 20$].

The value of the calorific value CV of the gas calculated by the control means 14 may be visually displayed and/or printed or otherwise recorded by recording means 36 in response to signals from the control means.

By any suitable technique know per se the control means 16 may be provided with information representing the relative density of the gas or the control means may be provided with information enabling it to calculate the relative density RD of the gas. The

control means 14 may calculate or otherwise obtain the value of the Wobble Index WI of the gas using the formula $WI = \frac{CV}{\sqrt{RD}}$

A method of measuring relative density is described in our co-pending British patent application No. GB9715448.8 filed on 22nd July 1997.

When fuel gas is combusted in a process (e.g. furnace, kiln, compressor, engine, etc.) some form of control system is used to set the oxygen (in this case in the form of air) / fuel gas ratio to ensure optimum combustion. An allowance is made in the amount of excess air to account in part, for variations in fuel gas composition changes. This allowance means that the process is running less efficiently than it could do because extra air is being heated and vented.

However, a measure of the calorific value or Wobbe Index, which is indicative of the fuel gas quality and which may be found according to the present invention, may be used in a feed forward control strategy to improve the accuracy of control available and achieve better efficiency.

An apparatus to perform such control is shown in Fig. 2. Fuel gas is supplied via a conduit 40, such as a pipe, to a gas fired process 41 such as a furnace, kiln, a compressor or an engine and oxygen in the form of air is supplied to the process 41 via another conduit 42. Any suitable device 43 which may be in the form of one or more probes temporarily insertable into the

conduit 40 or as one or more permanent fixtures is arranged to measure the speed of sound of the fuel gas passing through the conduit 40, the thermal conductivities of the gas ThC_H , ThC_L at two temperatures t_H and t_L and the ambient temperature of the gas T_a . The speed of sound of the fuel gas SOS , the thermal conductivities ThC_H and ThC_L and the ambient temperature of the gas T_a are measured by device 43 and passed via a connection 44 to a control means 45, which may be a microprocessor or a computer for example. Control means 45 determines the calorific value of the fuel gas from the received measurements from device 43 as explained earlier. Having determined a measure of the gas quality, the control means is able to adjust the air/fuel gas ratio setpoint using an oxygen/fuel gas ratio control system 46, 47 to achieve better efficiency. In this case the oxygen/fuel gas control system comprises two variable opening valves 46, 47 one in each of the fuel gas and air conduits 40, 42 respectively and both controlled by the control means 45 via connections 48, 49. Alternatively the oxygen/fuel gas control system could comprise a variable opening valve on just one of conduits 40, 42.

CLAIMS

1. A method of measuring the calorific value of a gas comprising making a measure of the speed of sound in the gas and using the speed of sound in an operation producing the calorific value of the gas corresponding to said speed of sound.
2. A method of measuring the calorific value of a gas comprising making a measure of a first thermal conductivity of the gas at a first temperature, making a measure of a second thermal conductivity of the gas at a second temperature which differs from the first temperature, and using the speed of sound and the first and second thermal conductivities in an operation producing the calorific value of the gas corresponding to said speed of sound and said first and second thermal conductivities.
3. A method as claimed in Claim 2, in which the calorific value is obtained by a procedure involving use of the formula:-

$$CV = a.ThC_H + b.ThC_L + c.SoS + d.T_a + e.T_a^2 + f,$$

where CV is the calorific value of the gas,

where ThC_H is the first thermal conductivity of the gas at said first temperature,

where ThC_L is the second thermal conductivity of the gas at said second temperature which is lower than said first temperature,

where SoS is the speed of sound in gas at ambient temperature and

where T_1 is the ambient temperature of said gas whereof said thermal conductivities are measured, the first and second temperatures being greater than said ambient temperature, and a, b, c, d, e and f are constants.

4. A method as claimed in Claim 3, in which SoS is the speed of sound in m/s, the thermal conductivities are in units of Watts/metre x degrees Kelvin (W/m.k), the temperature T_1 and the first and second temperatures are in degrees Celsius, and the calorific value is in megajoules/standard cubic metre ($\text{MJ/m}^3_{\text{st}}$).
5. A method as claimed in Claim 3 or Claim 4 in which the gas is fuel gas.
6. A method as claimed in Claim 5 in which the fuel gas is natural gas,
7. A method as claimed in Claim 4, in which the gas is natural gas comprising at least one hydrocarbon gas which is methane, and said natural gas further comprises nitrogen and/or carbon dioxide.

8. A method as claimed in any one of Claims 3 to 7, in which the first temperature is substantially 70°C above ambient temperature.
9. A method as claimed in any one of claims 3 to 8, in which the second temperature is substantially 50°C above the ambient temperature.
10. A method as claimed in Claim 7, or in Claim 8 or Claim 9 when either is dependant from Claim 7, in which:-
 - a is substantially 36.25649,
 - b is substantially -45.5768,
 - c is substantially 0.047029,
 - d is substantially 0.091067,
 - e is substantially 0.00074, and
 - f is substantially 24,18731.
11. A method of measuring the calorific value of a gas, substantially as hereinbefore described with reference to the accompanying drawing.
12. A method of measuring the Wobbe index of gas using the formula $WI = \frac{CV}{\sqrt{RD}}$ in which WI is the Wobbe index, RD is the relative density of the gas, and CV is the calorific value obtained by the method as claimed in any one of Claims 1 to 11.

13. An apparatus to measure the calorific value of a gas comprising means to measure the speed of sound in the gas and means to use the speed of sound in an operation producing the calorific value of the gas corresponding to said speed of sound.
14. An apparatus to measure the calorific value of a gas comprising means to measure a first thermal conductivity of the gas at a first temperature; means to measure a second thermal conductivity of the gas at a second temperature which differs from the first temperature, and means using the speed of sound and the first and second thermal conductivities in an operation producing the calorific value of the gas corresponding to said speed of sound and said first and second thermal conductivities.
15. An apparatus as claimed in Claim 14, in which the calorific value is obtained by a procedure involving use of the formula:-
- $$CV = a.ThC_H + b.ThC_L + c.SoS + d.T_a + e.T_a^2 + f,$$
- where CV is the calorific value of the gas,
- where ThC_H is the first thermal conductivity of the gas at said first temperature,
- where ThC_L is the second thermal conductivity of the gas at said second temperature which is lower than said first temperature,
- where SoS is the speed of sound in gas at ambient temperature and

where T_1 is the ambient temperature of said gas whereof said thermal conductivities are measured, the first and second temperatures being greater than said ambient temperature, and a, b, c, d, e and f are constants.

16. An apparatus as claimed in Claim 15, in which SoS is the speed of sound in m/s, the thermal conductivities are in units of Watts/metre x degrees Kelvin ($W/m.k$), the temperature T_1 and the first and second temperatures are in degrees Celsius, and the calorific value is in megajoules/standard cubic metre (MJ/m^3_{st}).
17. An apparatus as claimed in Claim 15 or Claim 16 in which the gas is fuel gas.
18. An apparatus as claimed in Claim 17 in which the fuel gas is natural gas,
19. An apparatus as claimed in Claim 16, in which the gas is natural gas comprising at least one hydrocarbon gas which is methane, and said natural gas further comprises nitrogen and/or carbon dioxide.
20. An apparatus as claimed in any one of Claims 15 to 19, in which the first temperature is substantially $70^\circ C$ above ambient temperature.

21. An apparatus as claimed in any one of claims 15 to 20, in which the second temperature is substantially 50°C above the ambient temperature.
22. An apparatus as claimed in Claim 19, or in Claim 20 or Claim 21 when either is dependant from Claim 19, in which:-
- a is substantially 36.25649,
 - b is substantially -45.5768,
 - c is substantially 0.047029,
 - d is substantially 0.091067,
 - e is substantially 0.00074, and
 - f is substantially 24,18731.
23. An apparatus to measure the calorific value of a gas, substantially as hereinbefore described with reference to the accompanying drawing.
24. A control means for adjusting the oxygen/fuel gas ratio of a gas fired process comprising an apparatus for measuring the calorific value of a fuel gas for the gas fired process according to any of Claims 13 to 23, and means for adjusting an oxygen/fuel gas ratio control system for the gas fired process in accordance with the determined calorific value.
25. A furnace comprising means for receiving a supply of oxygen; means for receiving a supply of fuel gas; an

oxygen/fuel gas ratio control system; and a control means according to Claim 24.

26. A kiln comprising means for receiving a supply of oxygen; means for receiving a supply of fuel gas; an oxygen/fuel gas ratio control system; and a control means according to Claim 24.
27. A compressor comprising means for receiving a supply of oxygen; means for receiving a supply of fuel gas; an oxygen/fuel gas ratio control system; and a control means according to Claim 24.
28. An engine comprising means for receiving a supply of oxygen; means for receiving a supply of fuel gas; an oxygen/fuel gas ratio control system; and a control means according to Claim 24.
29. An apparatus to measure the Wobbe index of gas using the formula $WI = \frac{CV}{\sqrt{RD}}$ in which WI is the Wobbe index, RD is the relative density of the gas, and CV is the calorific value obtained using an apparatus as claimed in any one of Claims 13 to 23.