

REACTOR COMPRISING A COIL FOR COOLANT CIRCULATION,
METHOD FOR MAKING SAME AND USE OF SUCH A REACTOR

The invention concerns a reactor for the treatment of a viscous medium
5 or for carrying out chemical reactions in a viscous medium, such as a
polymerization, such a reactor comprising such a coil for circulation of coolant
fluid. Finally, the invention relates to a method for making such a reactor and to
the use of such a reactor.

EP-A-0 659 476 discloses an apparatus used for the polymerization of
10 vinyl chloride in which coolant fluid circulation coils are used.

It is known to effect polymerization of polyamide continuously or
discontinuously. In the so-called discontinuous methods, one proceeds by
batches with reactors of autoclave type. In that case, it is known to evaporate the
water of an aqueous solution of two monomers and the water produced by their
15 polymerization, thanks to an outside heat supply.

Such heat supply must be sufficient for the reaction of polymerization to
take place in a period of time compatible with the criteria of productivity in
force in the industrial world. The heat supply must not be too great in order to
avoid, as far as possible, entraining one of the monomers with the vapour phase.
20 If a quantity of monomers is entrained with the vapour phase, this quantity must
be constant in order that the characteristics of the polyamide obtained be
reproducible. Furthermore, the supply of heat makes it possible

to monitor the reaction of polymerization insofar as it allows the evaporation of the water to be controlled.

To supply heat to the reaction medium, coils in which a coolant fluid circulates have been used in low-capacity autoclaves, i.e. ones with a volume less than 3 m³.

For reactors of greater capacity, in particular of the order of 5 to 6 m³, it has been possible to envisage using a coil and an agitator, the latter aiming at improving the homogeneity of the reaction medium and at increasing the coefficient of heat transfer.

However, this solution cannot be applied to high-capacity reactors, in particular ones with a capacity greater than 8 m³, as it is impossible to sufficiently increase the exchange surfaces constituted by the walls of the coil. In effect, if the overall diameter of the coil is increased, it is in that case no longer possible to house an efficient agitator in the vessel of the reactor. If the diameter of the tubes constituting the coil is decreased, the pressure drops associated with the circulation of coolant fluid in these tubes increase significantly. If a coil of very elaborate shape is created, the axial re-circulation of the reaction medium is hindered and the so-called "pumping" effect at the centre of the agitator is cancelled. Finally, a coil of elaborate shape with tubes of small diameter would not satisfy the criteria of mechanical strength allowing it to withstand prolonged use and/or incidents in manufacture.

It is a more particular object of example embodiments of the present invention to overcome these drawbacks by proposing a novel reactor provided with a coil which allows an efficient heat supply to a reaction medium of large volume,

while being compatible with the dimensions of the reactor vessel and with an agitator.

To that end, embodiments of the present invention relates to a reactor for the treatment of a viscous medium or for carrying out chemical reactions in viscous medium, this reactor comprising a vessel and a coil for circulation of a coolant fluid, this coil comprising at least one segment of tube wound along a helical generatrix, characterized in that the coil comprises at least a second segment of tube wound along a helical generatrix extending in parallel to the first segment between a distributor and a manifold, these first and second segments being centred on the same geometrical axis, with substantially the same bending radius and nested so that they together form a substantially cylindrical bundle.

Thanks to the use of two nested helical tube segments, it is possible that these segments each have a relatively short length, with the result that the pressure drop that they generate is relatively slight, even if the cross-section of the tube used may also be small. In addition, the fact that the helical tube segments have a relatively short length induces a relatively considerable slope thereof, i.e. greater than in the case of a single circular segment extending over the whole height of the coil. In this way, in the case of the coolant fluid being supplied in vapour phase able to condense in the tubes, the flow of the condensed fluid in these segments is more rapid, hence less risk of accumulation of condensates and less space requirement for liquid. The fact that these segments form a cylindrical bundle avoids their significantly disturbing

the flow or re-circulation of the reaction medium in the central part of a reactor.

In accordance with an aspect of the present invention, there is provided a reactor for treating a viscous medium or implementing chemical reactions in a viscous medium, said reactor comprising a vessel and a coil for circulation of a heat exchanging fluid, said coil comprising at least one first tube segment which is coiled according to a helicoidal generator and at least one second tube segment which is coiled according to a helicoidal generator and extends in parallel to said first segment between a distributor and a collector, characterised in that said first and second segments are centred on the same geometric axis, curved with substantially the same radius and interlaced, such that together they form a sheet of an overall cylindrical form.

In accordance with another aspect of the present invention, there is provided a method for producing a reactor for treating a viscous medium or implementing chemical reactions in a viscous medium, said reactor including a vessel and a coil for circulation of a heat exchanging fluid, said coil comprising at least one tube segment which is coiled according to a helicoidal generator, characterised in that it includes a stage comprising interlacing said segment with at least one second tube segment which is coiled according to a helicoidal generator curved with substantially the same radius as the first segment, so as to form a sheet of an overall cylindrical form.

The invention will be more readily understood and other advantages thereof will appear more clearly on reading the following description of a form of embodiment of a coil and a reactor according to the invention, of their respective manufacture and use, given solely by way of example and made with reference to the accompanying drawings, in which:

Figure 1 is a longitudinal section through a reactor according to the invention equipped with a coil according to the invention.

Figure 2 is a half-section of the coil shown in Figure 1.

Figure 3 schematically shows a step of manufacture of the coil of Figure 2.

Figure 4 is a view similar to Figure 3 for another step of manufacture of the coil.

Figure 5 is a plan view of the coil of Figure 2.

Figure 6 is a view from underneath of the coil of Figure 2, and

Figure 7 is a view in perspective of the coil of Figures 2 to 6.

The reactor 1 shown in Figure 1 is used for the polymerization of polyamide. It has a volume V of the order of 11 m^3 . This reactor 1 comprises a vessel 2 of substantially cylindrical shape with a substantially truncated bottom 21. A cover (not shown) is provided to be mounted on the vessel 2 in order to constitute the ceiling thereof and to ensure seal of the interior volume V of the reactor 1 with respect to the ambient medium.

An agitator 4 is provided in the volume V . It is driven by a shaft 41 aligned on a central axis $X-X'$ of the reactor and passing through the cover. The agitator 4 comprises

substantially helical blades mounted on a cage which surrounds a coil 5. In order to render the drawing clearer, the agitator 4 is silhouetted in dashed and dotted lines solely in Figure 1.

Other forms of agitators may be envisaged, as long as they are compatible
5 with the space available in the volume V.

The vessel 2 is of double envelope type in order to allow the circulation of a coolant fluid, this allowing the volume V to be heated.

A coil 5 is installed inside the vessel 2 and is supplied with coolant fluid from a vaporizer 6 which may be of any known type. Two partition passages 59
10 connect the coil 5 to tubes 61 and 62 respectively allowing supply of the coil 5 with hot coolant fluid and evacuation of comparatively less hot coolant fluid in the direction of the vaporizer 6.

In the present case, the coolant fluid is an oil in vapour phase at a temperature included between 300 and 350°C. Oil in vapour phase behaves like
15 a pure body and works in latent heat, with the result that it conserves its temperature, so that the reaction medium is subjected to a substantially homogeneous heat supply over the length of coil.

Arrows E_1 and E_2 represent the flow of the oil in the passages 59.

As is more particularly visible in Figures 2 to 7, the coil 5 is formed by
20 two bundles of tubes. More specifically, a first bundle 51 is formed by tubes with a substantially constant bending radius R_1 . A second bundle of tubes 52 is formed by tubes with a bending radius R_2 less than radius R_1 . The bundles 51 and 52 are substantially cylindrical and centred on a central axis X_5 .

of the coil 5, this axis merging with axis X-X' when the coil is installed in the reactor 1.

The bundle 51 is formed by three segments of tube 511, 512 and 513 each wound along a helical generatrix and nested in one another, i.e. together
5 forming the bundle 51.

In the same way, the bundle 52 is formed by two segments of tube 521 and 522 each wound along a helical generatrix and nested in each other.

As is visible in Figure 3, the bundle 51 is formed by "screwing" the segments 511, 512 and 513 about axis X_5 which is their common central axis.
10 The arrow F_1 represents the interleaving of the segment 512 in the segment 511, this interleaving being translated by an advance of the segment 512 parallel to axis X_5 , as represented by arrow F_2 . In the same way, the segment 513 may be interleaved between the segments 511 and 512.

As is visible in Figure 4, the bundle 52 is formed by the segment 522
15 interleaved in the segment 521 thanks to a movement of screwing represented by arrows F_1 and F_2 .

When the two bundles 51 and 52 are each formed with a substantially cylindrical shape and with a predefined radius R_1 or R_2 , it is possible to connect the segments of tube 511 to 513, 521 and 522 to a supply tank 53 forming
20 distributor and to an outlet manifold 54, said tank and manifold each being of substantially toric shape and centred on axis X_5 .

Elements 53 and 54 have a diameter greater than that of the segments of tube 511 to 513, 521 and 522, with the result that they make it possible to efficiently supply these segments with coolant fluid and to efficiently collect
25 the fluid coming from these segments, as is represented by arrows of flow E in Figures 5 and 6.

The radius R_3 of the torus formed by the tank 53 is chosen to be equal to radius R_2 , in the same way as radius R_4 of the outlet manifold 54. In this way, elements 53 and 54 are substantially aligned with the bundle 52, with the result that they do not disturb a flow in the central part of the coil 5, such flow being
5 represented by arrow E' in Figure 1.

The tank 53 is provided with two lifting ears 531 and 532 for supporting the coil 5 when it is placed in position in the vessel 2 or when it is extracted therefrom. Other lifting means may be envisaged, on the tank 53 or on other parts of the coil 5.

10 A tube 56, substantially parallel to axis X_5 , is housed between the bundles 51 and 52, this tube making it possible to supply the tank 53 from the passage 59 connected to the tube 61 of the vaporizer 6. This tube 56 has an internal cross-section substantially equal to that of the tank 53.

As is more particularly visible in Figure 5, the three segments of tube
15 511, 512 and 513 are connected to the tank 53 by connections 511a, 512a and 513a extending in an essentially radial direction with respect to the tank 53. Furthermore, the tubes 521 and 522 are connected to this tank 53 by connections 521a and 522a extending beneath the tank 53, i.e. in a direction substantially parallel to axis X_5 , while the connections 511a, 512a and 513a are
20 substantially perpendicular to this axis.

In the same way and as is visible in Figure 6, the tubes 511 to 513 are connected by essentially radial connections 511b, 512b and 513b to the manifold 54, while tubes 521 and 522 are connected to the manifold 54 by essentially axial connections 521b and 522b.

The radii R_1 and R_2 , the height h_5 of the coil 5 and the positioning of the elements 53 and 54 may be chosen so that the segments of tube 511 to 513, 521 and 522 present substantially the same length. These segments have the same internal cross-section. In that case they induce substantially the same pressure drop on the flow of coolant fluid.

With the foregoing in mind, it will be readily understood that the segments 511, 512, 513, 521 and 522 are mounted in parallel with respect to one another between the elements 53 and 54, which makes it possible to obtain relatively slight pressure drops, taking into account, in particular, the fact that the overall pressure drop of the three tubes 511, 512 and 513 is substantially less than that which would be generated by a single tube in helical configuration forming, alone, a bundle as dense as bundle 51.

In addition, the unitary slope of each of the tubes 511 to 513, which may be defined, as illustrated in Figures 1 and 3, by angle α_1 between a tube and a line Y_5 normal to axis 5, is substantially greater than the slope that a single tube, in helical configuration, would have in order to constitute the bundle 51 alone. This considerably reduces the risks of accumulation of condensates inside the segments 511 to 513 and minimizes the liquid retention in the lower part of these tubes.

The foregoing observations are also applicable to the tubes 521 and 522 of the second bundle 52.

As the tube 56 extends in a direction substantially parallel to axis $X-X'$ of the vessel 2, it does not disturb the flow E' of the reaction medium to a substantial degree.

In practice, the radius R_2 of the inner bundle 52 is chosen to have a value included between 20% and 40% of the radius R of the vessel 2. Under these conditions, the central well

P formed by the bundle 52 in the volume V of the reactor 1 is sufficiently wide for the re-circulation of reaction medium generated by the agitator 4 to be efficient.

It will also be noted that the construction of the coil 5 allows its geometry to be adapted to that of the bottom 21 of the vessel 2, with the result that the dead volume of the reactor 1, i.e. that part where little re-circulation is created, is limited to a maximum.

The invention has been shown with a coil 5 comprising an outer bundle 51 and an inner bundle 52. However, it is applicable with a coil comprising a single bundle composed of at least two nested segments of tube with a helical configuration.

In the case of a coil comprising one sole bundle, the radius of this bundle may be chosen with a value included between 20 and 70% of the radius of the reactor vessel.

The invention has been shown with the outer bundle 51 comprising three segments of tube 511, 512 and 513. However, it is applicable with a bundle comprising two segments or, on the contrary, more than three segments.

The invention has been shown with an agitator 4 arranged around the coil 5. However, it is also applicable with an agitator which might penetrate in the central well of the coil 5. In that case, the radii R_1 and R_2 of the coil 5 might be increased and the agitator might take the form of an endless screw.

The invention is independent of the exact type of vaporizer 6 and of the nature of the coolant fluid employed.

In Figures 3, 4 and 7, different textures have been used solely in order to differentiate the different parts of the coil 5 visually.

Claims

1. Reactor for treating a viscous medium or implementing chemical reactions in a viscous medium, said reactor comprising a vessel and a coil for circulation of a heat exchanging fluid, said coil comprising at least one first tube segment which is coiled according to a helicoidal generator and at least one second tube segment which is coiled according to a helicoidal generator and extends in parallel to said first segment between a distributor and a collector, characterised in that said first and second segments are centred on the same geometric axis, curved with substantially the same radius and interlaced, such that together they form a sheet of an overall cylindrical form.
2. Reactor according to claim 1, characterised in that said coil comprises a second sheet which is formed by at least one tube segment which is coiled according to a helicoidal geometry, extends between said distributor and said collector and is centred on said axis, said second sheet being of an overall cylindrical form, with a radius less than the radius of the first sheet.
3. Reactor according to claim 2, characterised in that said second sheet is formed by at least two tube segments which are coiled according to helicoidal generators, are interlaced and extend in parallel between said distributor and said collector.
4. Reactor according to one of the preceding claims, characterised in that said first sheet is formed by three tube segments

which are coiled according to helicoidal generators, and are interlaced.

5. Reactor according to one of the preceding claims, characterised in that said segments have substantially the same length and/or cause substantially the same head loss in the flow of said heat exchanging fluid, between said distributor and said collector.
6. Reactor according to one of the preceding claims, characterised in that said coil comprises a tube which extends, according to a direction which is overall parallel to said axis, between said first and second sheets, said tube being connected either to said distributor or to said collector.
7. Reactor according to one of the preceding claims, characterised in that said distributor and/or said collector have the form of a toroid and are centred on said axis.
8. Reactor according to claim 7, characterised in that said distributor and/or said collector are curved with a radius which is substantially equal to the radius of said first sheet or, possibly, of said second sheet, such that they are substantially in the extension of said first sheet or, possibly, of said second sheet.
9. Reactor according to one of the preceding claims, characterised in that it includes an agitator which is disposed around or in the interior of said coil.

10. Reactor according to claim 9, characterised in that said agitator is suspended from the top of said reactor and forms a cage surrounding said coil, the supply and the discharge of the heat exchanging fluid towards or from said coil being effected through the base of said reactor.
11. Reactor according to claim 9, characterised in that said agitator is formed by an endless screw which is centred on the geometric axis of an interior sheet or of the single sheet of said coil.
12. Reactor according to one of the preceding claims, characterised in that the interior sheet or the single sheet of said coil forms a central well of a radius between 20 and 70% of the radius of said vessel, preferably between 20 and 40% of said radius in the case of an interior sheet.
13. Method for producing a reactor for treating a viscous medium or implementing chemical reactions in a viscous medium, said reactor including a vessel and a coil for circulation of a heat exchanging fluid, said coil comprising at least one tube segment which is coiled according to a helicoidal generator, characterised in that it includes a stage comprising interlacing said segment with at least one second tube segment which is coiled according to a helicoidal generator curved with substantially the same radius as the first segment, so as to form a sheet of an overall cylindrical form.
14. Method according to claim 13, characterised in that said segments are interlaced by a screwing movement about a geometric axis which is common to said segments.

15. Use of a reactor with a volume greater than approximately 8 m^3 according to one of the claims 1 to 12 for treating a viscous medium.
16. Use according to claim 15 for implementing a polymerization reaction in a viscous medium.