Claims

1. A process for continuously distilling acrylates by means of a rectification column, wherein the acrylate content in the feed to the rectification column is at least 80% by weight, the liquid in the bottom region of the rectification column is heated by means of an evaporator, and the parts of the evaporator that are in contact with product are made from stainless steel.

2. The process according to claim 1, wherein methyl acrylate, ethyl acrylate, n-butyl acrylate or 2-ethylhexyl acrylate is used as acrylate.

3. The process according to claim 1 or 2, wherein the acrylate content in the feed to the rectification column is at least 85% by weight.

4. The process according to claim 1 or 2, wherein the acrylate content in the feed to the rectification column is at least 90% by weight.

5. The process according to claim 1 or 2, wherein the acrylate content in the feed to the rectification column is at least 95% by weight.

6. The process according to any of claims 1 to 5, wherein the evaporator is a shell and tube heat exchanger.

7. The process according to any of claims 1 to 6, wherein the parts of the evaporator that are in contact with product are made from stainless steel having 10.5% to 30.0% by weight of chromium.

8. The process according to claim 7, wherein the parts of the evaporator that are in contact with product are made from stainless steel additionally having 2.0% to 35.0% by weight of nickel.

9. The process according to claim 7 or 8, wherein the parts of the evaporator that are in contact with product are made from stainless steel additionally having 0.1% to 8.0% by weight of molybdenum.

10. The process according to any of claims 7 to 9, wherein the feed to the rectification column has an acid number of less than 100 mg of potassium hydroxide per g of feed.

11. The process according to any of claims 1 to 10, wherein the feed to the rectification column has an acid number of less than 10 mg of potassium hydroxide per g of feed.

12. The process according to any of claims 1 to 10, wherein the feed to the rectification column has an acid number of less than 1 mg of potassium hydroxide per g of feed.