

- 1 -

INTERFACIAL METHOD FOR
PREPARING
COPOLYESTERCARBONATES

BACKGROUND OF THE INVENTION

5 This invention relates to the preparation of
copolyestercarbonates, and more particularly to an improved method
for their preparation by interfacial methods.

 The preparation of copolyestercarbonates by the
interfacially conducted condensation of dihydroxyaromatic compounds
10 with dicarboxylic acids and phosgene in an immiscible
aqueous-organic medium is known. It ordinarily takes place in the
presence of a tertiary amine, a phase transfer catalyst or both. The
product copolyestercarbonates have properties similar to those of
polycarbonates but are generally more ductile, especially when the
15 ester units are derived from aliphatic acids.

 Among the uses presently under study for
copolyestercarbonates is in optical disk fabrication. For this purpose,
it is frequently advantageous to incorporate structural units which have
very low or even negative intrinsic birefringence, such as those
20 derived from spiro(bis)indane bisphenols and especially
6,6'-dihydroxy-3,3,3',3'-tetramethyl-1,1'-spiro(bis)indane (CAS #1568-
80-5), hereinafter designated "SBI". When SBI units are present in
polycarbonates, however, they are very brittle, processing is difficult
and it is almost essential to improve ductility and processability by
25 incorporation of ester units.

 The interfacial preparation of copolyestercarbonates is
also known. In this method of preparation, reaction is conducted
between phosgene and a mixture of a dihydroxyaromatic compound
and a dicarboxylic acid (or corresponding acid chloride) in an
30 immiscible aqueous-organic mixture. The reaction takes place under

alkaline conditions and in the presence of a catalyst, typically a tertiary amine, phase transfer catalyst or combination of the two.

5 The polymer ideally produced by this method contains ester and polycarbonate units. It is often found, however, that said polymer also contains moieties incorporating anhydride linkages, which are thermally and hydrolytically unstable.

10 It is frequently found that anhydride linkages are produced in substantial proportions under normal interfacial reaction conditions. The presence of such linkages can often be minimized by careful control of the pH of the reaction mixture. This has not been found to be true, however, when a large proportion of acid-derived groups, for example 10 mole percent or higher, is desired in the polymer.

15 US Patents 5,510,449 and 5,519,105 describe procedures for the preparation of polycarbonates, including copolyestercarbonates, in which a mixture of phase transfer catalyst and tertiary amine is employed. There is no suggestion, however, of a method for decreasing the proportion of anhydride linkages in a copolyestercarbonate.

20 Therefore, it is of interest to adjust the reaction conditions in interfacial copolyestercarbonate preparation to suppress the formation of anhydride linkages, particularly when large percentages of ester groups are desired in the polymer.

SUMMARY OF THE INVENTION

25 The present invention provides a method for producing copolyestercarbonates interfacially which minimizes the formation of anhydride linkages. This is done easily by a suitable choice of catalytic species and phosgenation conditions, and is effective even for the incorporation of ester groups in large proportions.

The invention is a method for preparing a copolyestercarbonate which comprises:

5 passing phosgene, under reactive conditions including a pH in the range of about 4.5-9.5, into a mixture comprising at least one dihydroxyaromatic compound, at least one dicarboxylic acid, water and a water-immiscible organic solvent, in the presence of both at least one phase transfer catalyst and at least one aliphatic or alicyclic tertiary amine, the proportion of said phase transfer catalyst being in the range of about 1-12 mole percent based on total dihydroxyaromatic
10 compound and dicarboxylic acid and the proportion of phosgene being at least about 50% by weight of stoichiometric; and

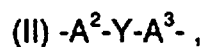
raising the pH to at least about 10 and continuing phosgene passage until a stoichiometric excess of at least 5% phosgene by weight has been introduced.

15 DETAILED DESCRIPTION; PREFERRED EMBODIMENTS

The dihydroxyaromatic compounds employed in the method of this invention typically have the formula



wherein A^1 is an aromatic organic radical. At least a portion of total
20 dihydroxyaromatic compounds employed are generally those in which A^1 has the formula



wherein each of A^2 and A^3 is a monocyclic divalent aryl radical and Y is a bridging radical in which one or two carbonate atoms separate A^2
25 and A^3 .

The A^2 and A^3 radicals are most often unsubstituted phenylene, especially p-phenylene which is preferred, or substituted derivatives thereof. The bridging radical Y is most often a hydrocarbon group and particularly a saturated group such as

methylene, cyclohexylidene, or isopropylidene which is preferred. Thus, the most preferred bisphenol is 2,2-bis(4-hydroxyphenyl)propane, also known as "bisphenol A".

5 It is also frequently preferred to employ a mixture of dihydroxyaromatic compounds, at least one of which is a spiro(bis)indane bisphenol as illustrated by SBI and its 5,5'-dihydroxy isomer. SBI is usually preferred by reason of its particular effectiveness and relative ease of preparation.

10 The term "bisphenol" will frequently be used hereinafter to designate the preferred dihydroxyaromatic compounds which are usually spiro(bis)indane bisphenols and those having formula I. However, it should be understood that other dihydroxyaromatic compounds can be substituted therefor when appropriate.

The dicarboxylic acid may be aliphatic or aromatic.
15 Illustrative aromatic acids are terephthalic and isophthalic acid. Typical aliphatic acids include those containing 4-25 carbon atoms, including adipic acid, azelaic acid, suberic acid and 1,12-dodecane - dicarboxylic acid. The aliphatic dicarboxylic acids are generally preferred by reason of their excellent ductility improving properties,
20 with the C₆₋₂₀ acids being more preferred and sebacic and 1,12-dodecanedioic acid being most preferred.

Materials suitable for use as phase transfer catalysts are well known in the art. They include onium salts and crown ethers, with onium salts generally being preferred.

25 As used herein, the term "onium salt" with reference to phase transfer catalysts designates salts formally having at least one positively charged nitrogen, phosphorus or sulfur atom which in turn has all valences satisfied by organic radicals. The preferred onium salts are tetraalkylammonium, tetraalkylphosphonium and
30 hexaalkylguanidinium salts, especially the halides and more especially the chlorides and bromides. Illustrative onium salts are

tetramethylammonium chloride, tetramethylammonium bromide,
methyltri-n-butylammonium chloride, tetraethylphosphonium chloride,,
tetraethylphosphonium bromide,
bis(tri-n-butyl)-1,4-hexylenediammonium dibromide,
5 bis(tri-n-butyl)-1,6-butylenediammonium dibromide,
hexaethylguanidinium chloride, hexaethylguanidinium bromide and the
quaternary bisphenolates (e.g., compounds containing one
hexaalkylguanidinium cation, three protons and one divalent
bisphenolate anion) disclosed in copending, commonly owned
10 application Serial No. 08/768,871. The tetraalkylammonium salts are
often preferred because of their particular suitability and relatively low
cost.

Suitable aliphatic and alicyclic tertiary amines include
those having about 5-20 carbon atoms. Examples are triethylamine,
15 tri-n-butylamine, 4-methylmorpholine and 4-ethylmorpholine.
Triethylamine is often preferred.

Water-immiscible organic solvents which may be
employed in the method of the invention include chlorinated aliphatic
hydrocarbons, such as methylene chloride, chloroform,
20 dichloroethane, trichloroethane, tetrachloroethane, dichloropropane
and 1,2-dichloroethylene, and substituted aromatic hydrocarbons such
as chlorobenzene, o-dichlorobenzene and the various chloro toluenes.
The chlorinated aliphatic hydrocarbons are preferred, with methylene
chloride being most preferred.

25 Endcapping agents may also be present in the reaction
mixture. They are typically phenols as exemplified by phenol, p-cresol
and cumylphenol.

In the first step of the method of this invention, phosgene
is passed into a mixture of the bisphenol, dicarboxylic acid, phase
30 transfer catalyst, tertiary amine, water and organic solvent. The
proportions of water and organic solvent are not critical but are
typically reflected in a volume ratio of aqueous to organic phase in the

range of about 0.2-1.1:1. Reaction temperatures are generally in the range of about 15-50°C, preferably about 35-45°C.

The proportion of tertiary amine employed is not critical. Illustrative proportions are in the range of about 0.001-3.0 mole percent based on total bisphenol and dicarboxylic acid. It is, however, critical that the tertiary amine be present in combination with the phase transfer catalyst during the entire course of the first step. If the phase transfer catalyst alone is present when the reaction is initiated and the tertiary amine is added later, anhydride levels in the product increase significantly.

On the other hand, the proportion of phase transfer catalyst is critical from the standpoint of minimizing anhydride linkage formation. It is in the range of about 1-12, preferably about 3-12 and most preferably about 6.5-10.5 mole percent on the same basis.

The pH of the reaction mixture is maintained in the range of about 4.5-9.5 and preferably about 6.5-9.5 during the first step of phosgene addition, typically by the addition of aqueous alkali such as sodium hydroxide or potassium hydroxide to neutralize hydrochloric acid formed upon reaction of the phosgene. As used herein, pH designates that of the aqueous phase of the reaction mixture. Phosgene addition is continued in the first step until at least about 50% and preferably about 75-90% by weight of the stoichiometric amount has been added.

When the required amount of phosgene has been added in the first step, the pH of the reaction mixture is raised to at least about 10, preferably about 10-11, by the addition of further alkali. Phosgene addition is then continued until the total amount of phosgene added is at least 5% and preferably about 10-25% by weight in excess of the stoichiometric amount.

When the reaction is complete, the copolyestercarbonate may be isolated by conventional means. These typically include

separation of the organic and aqueous phases, washing of the organic phase with aqueous acid and/or water and precipitation of the polymer by pouring into boiling water, by steam precipitation or by combination with a non-solvent such as methanol.

5 The copolyestercarbonates prepared by the method of this invention have been found to contain much lower proportions of anhydride linkages than those prepared by other methods. This decrease in the level of anhydride linkages appears to be the result of at least three process features: the presence of both tertiary amine
10 and phase transfer catalyst at the beginning of the phosgenation, the presence of phase transfer catalyst in the prescribed amount, and the maintenance of the pH during the first phosgenation step at the prescribed level.

 The level of anhydride linkages in the product may be
15 determined by carbon-13 nuclear magnetic resonance spectroscopy. It may also be determined by proton nuclear magnet resonance spectroscopy except when SBI units are present, since the shifts of some of the protons in said units cause interference with the shifts of the protons characteristic of anhydride linkages.

20 The invention is illustrated by the following examples. All percentages are by weight unless otherwise indicated.

EXAMPLE 1

 A number of 500-ml Morton flasks were charged with 9.6 g (31.3 mmol) of SBI, 5.0 g (21.9 mmol) of bisphenol A, 2.2 g (9.4
25 mmol) of 1,12-dodecanedioic acid, 250 mg (1.17 mmol) of p-cumylphenol, 100 ml of methylene chloride, 50 ml of distilled water, 125 μ l of triethylamine and 0.5 ml of a 75% aqueous solution of methyl-tri-n-butylammonium chloride (3.5 mole percent based on bisphenols and dicarboxylic acid). Phosgene was passed into the
30 mixtures, with stirring, at 0.25 g/min, with maintenance of the pH at the desired level by addition of 25% aqueous sodium hydroxide solution. When 85 mole percent of the stoichiometric amount of phosgene had

been added, the pH was raised to 10.5 and phosgene addition was continued until a 20 mole percent excess had been introduced.

5 The organic and aqueous phases were separated and the organic phase was washed with aqueous hydrochloric acid solution and 4 times with distilled water. The copolyestercarbonates were precipitated by pouring the methylene chloride solution into boiling water in a blender, and were separated by filtration, washed with water and dried at 120° under vacuum.

10 The results are given in Table I. pH values are those maintained in the first phosgenation step.

TABLE I

Run	pH	Phase Transfer cat., mole %	Anhydride linkages, %
1	5	3.5	6.8
2	6	3.5	6.8
3	7	0	21
4	7	1.7	10
5	7	3.5	6.8
6	7	7.0	2
7	7	10.0	1
8	8	3.5	4.0
9	9	3.5	1.7
10	10	3.5	9.5

15 It is apparent that the level of anhydride linkages was significantly lower in Runs 1, 2 and 5-9, in which the pH and the level of phase transfer catalyst were maintained within the prescribed range, than in Runs 3 and 4, in which no phase transfer catalyst or only a very small proportion thereof was employed, and Run 10, in which the pH was at a higher value than prescribed. It is also apparent from
20 Runs 5-7 that within the prescribed range of phase transfer catalyst, high levels are preferred.

EXAMPLE 2

The procedure of Example 1 was repeated, using a mixture of 11.4 g (50 mmol) of bisphenol A and 2.9 g (12.5 mmol) of 1,12-dodecanedioic acid. The pH in the first step was maintained at 8, and the various runs differed in presence or absence of phase transfer catalyst and in time of introduction of the triethylamine. The results are given in Table II.

TABLE II

Run	Phase transfer cat., mole %	Triethylamine addition time	Anhydride linkages, %
1	0	Beginning of first step	21
2	3.5	Beginning of first step	0
3	3.5	Just before pH increase	22
4	3.5	Just after pH increase	19
5	3.5	End of phosgenation	20

The improvement produced by the employment of the phase transfer catalyst and the simultaneous employment throughout the reaction of the triethylamine is apparent.

EXAMPLE 3

The procedure of Example 2 was repeated, substituting SBI on an equimolar basis for the bisphenol A. The product contained no detectable level of anhydride linkages. In a control in which the phase transfer catalyst was omitted, the product contained 21% anhydride linkages.



What is claimed is:

1. A method for preparing a copolyestercarbonate which comprises:

5 passing phosgene, under reactive conditions including a pH in the range of about 4.5-9.5, into a mixture comprising at least one dihydroxyaromatic compound, at least one dicarboxylic acid, water and a water-immiscible organic solvent, in the presence of both at least one phase transfer catalyst and at least one aliphatic or alicyclic tertiary amine, the proportion of said phase transfer catalyst being in the range of about 1-12 mole percent based on total dihydroxyaromatic compound and dicarboxylic acid and the proportion of phosgene being
10 at least about 50% by weight of stoichiometric; and

raising the pH to at least about 10 and continuing phosgene passage until a stoichiometric excess of at least 5% phosgene by weight has been introduced.

2. A method according to claim 1 wherein the dihydroxyaromatic compound is bisphenol A.

3. A method according to claim 1 wherein the dihydroxyaromatic compound is a mixture of bisphenol A and 6,6'-dihydroxy-3,3,3',3'-tetramethyl-1,1'-spiro(bis)indane.

4. A method according to claim 1 wherein the dicarboxylic acid is an aliphatic dicarboxylic acid.

5. A method according to claim 4 wherein the dicarboxylic acid is sebacic acid or 1,12-dodecanedioic acid.

6. A method according to claim 1 wherein the organic solvent is a chlorinated aliphatic hydrocarbon.

7. A method according to claim 6 wherein the organic solvent is methylene chloride.



8. A method according to claim 1, wherein the tertiary amine is triethylamine.

9. A method according to claim 1 wherein the phase transfer catalyst is an onium salt.

10. A method according to claim 9 wherein the phase transfer catalyst is a tetraalkylammonium, tetraalkylphosphonium or hexaalkylguanidinium halide.

11. A method according to claim 10 wherein the phase transfer catalyst is a tetraalkylammonium chloride or bromide.

12. A method according to claim 11 wherein the phase transfer catalyst is methyltri-n-butylammonium chloride.

13. A method according to claim 1 wherein the proportion of phase transfer catalyst is in the range of about 6.5-10.5 mole percent.

14. A method according to claim 1 wherein the pH is maintained in the range of about 6.5-9.5 during the first step.

15. A method according to claim 1 wherein phosgene addition in the first step is continued until about 75-90% by weight of the stoichiometric amount has been added.

16. A method according to claim 1 in which the pH in the second step is in the range of about 10-11.

17. A method according to claim 1 wherein the total amount of phosgene added is about 10-25% by weight in excess of the stoichiometric amount.

18. A method for preparing a copolyestercarbonate which comprises:



- 12 -

passing phosgene, under reactive conditions including a pH in the range of about 6.5-9.5, into a mixture comprising:

- 5 at least one dihydroxyaromatic compound selected from the group consisting of bisphenol A and a mixture of bisphenol A and 6,6'-dihydroxy-3,3,3',3'-tetramethyl-1,1'-spiro(bis)indane,
- at least one C₆₋₂₀ aliphatic dicarboxylic acid,
- water, and
- 10 methylene chloride,
- in the presence of both
- at least one onium salt as a phase transfer catalyst and
- at least one aliphatic tertiary amine having about 5-20 carbon atoms,
- 15 the proportion of said onium salt being in the range of about 3-12 mole percent based on total dihydroxyaromatic compound and dicarboxylic acid and the proportion of phosgene being at least about 50% by weight of stoichiometric; and
- raising the pH to at least about 10 and continuing
- 20 phosgene passage until a stoichiometric excess of at least 5% phosgene by weight has been introduced.