

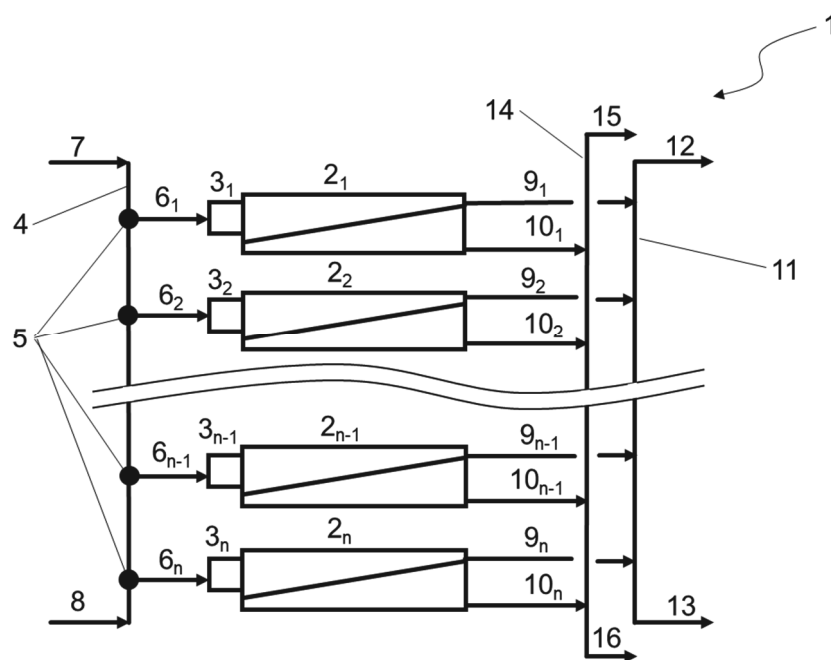


Figure 1: Membrane block according to the invention with a gas distribution via a distributor conduit and supply conduits, and discharging of permeate gas and of retentate gas by means of collection pipes

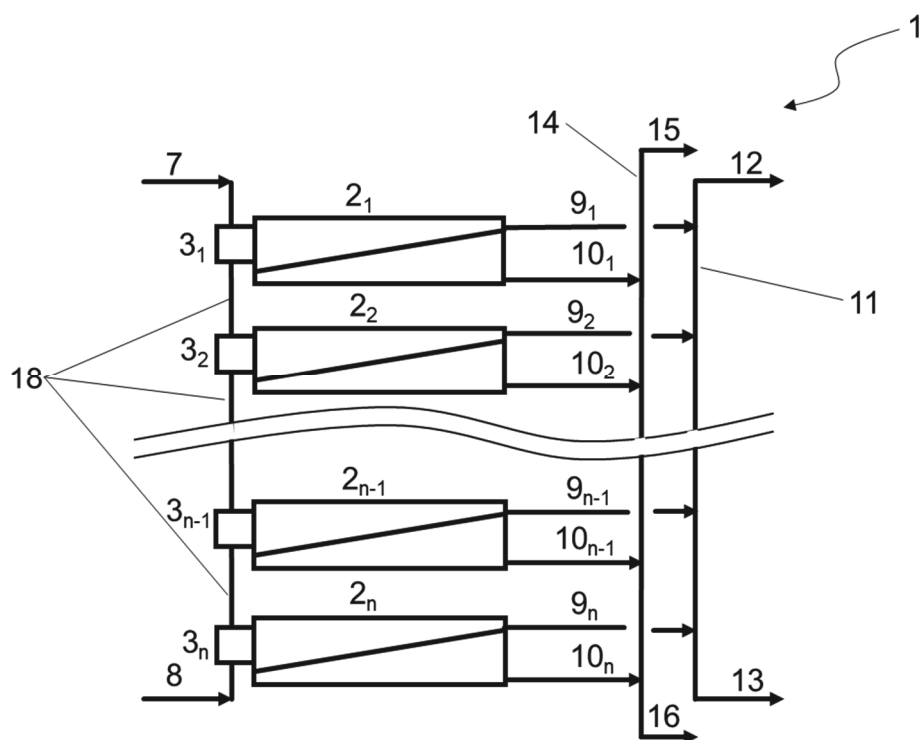


Figure 2: Membrane block according to the invention with gas distribution via connection conduits, and discharging of permeate gas and of retentate gas by means of collection pipes

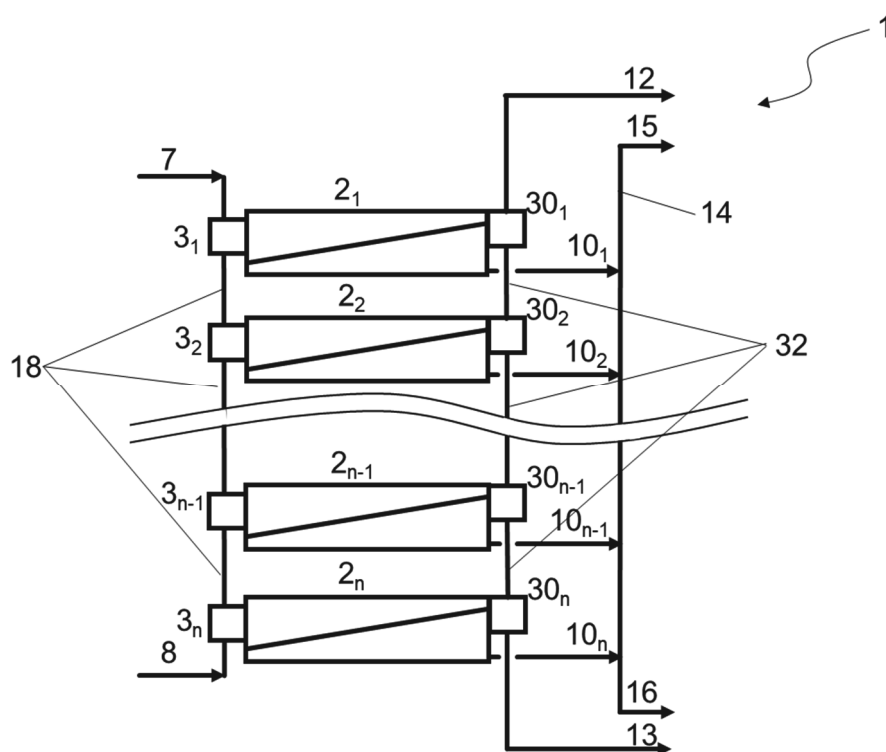


Figure 3: Membrane block according to the invention with a gas distribution by means of distributor conduit and discharging of permeate gas by means of collection pipes and discharging of retentate gas by means of retentate connection conduit

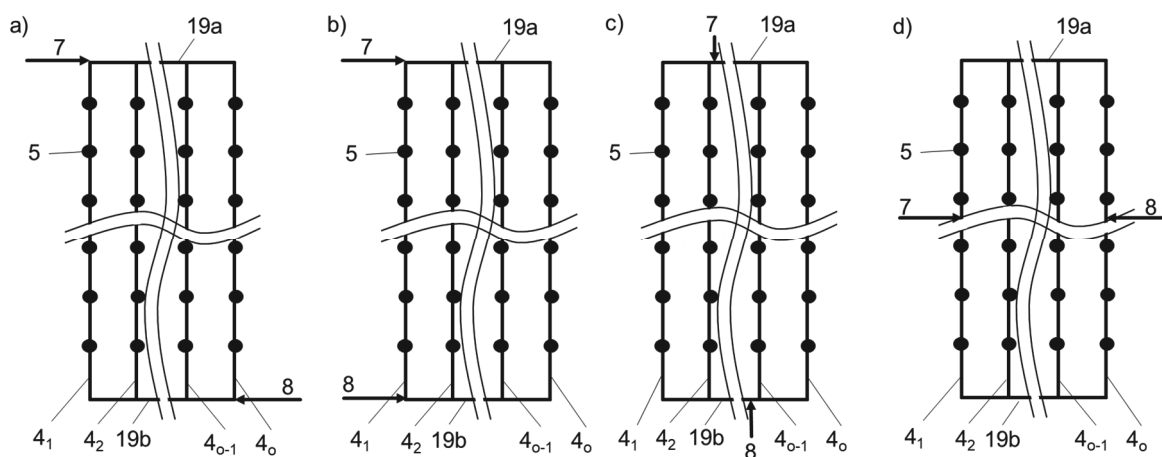


Figure 4: Linear semilattice of membrane blocks with distributor conduits and two gas sources

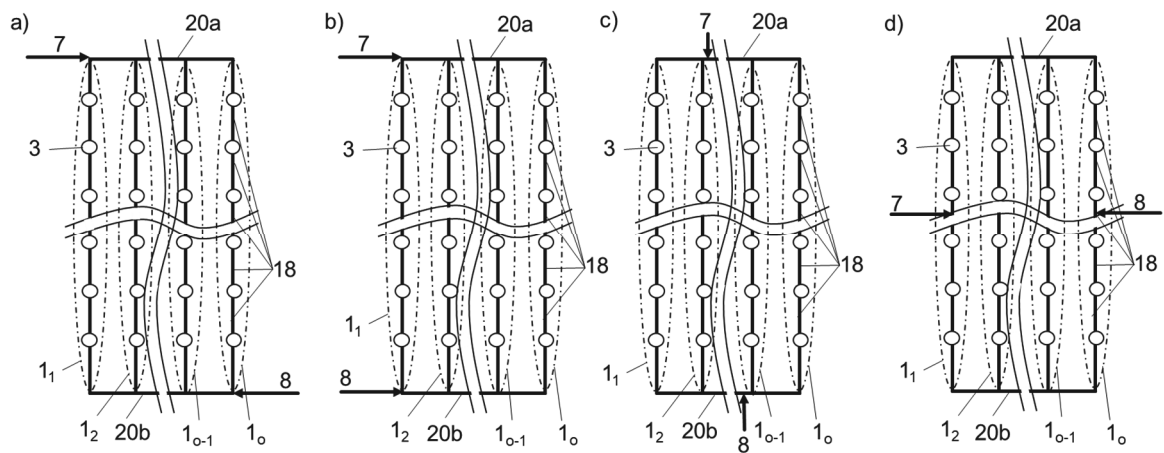


Figure 5: Linear semilattice of membrane blocks with connection conduits and two gas sources

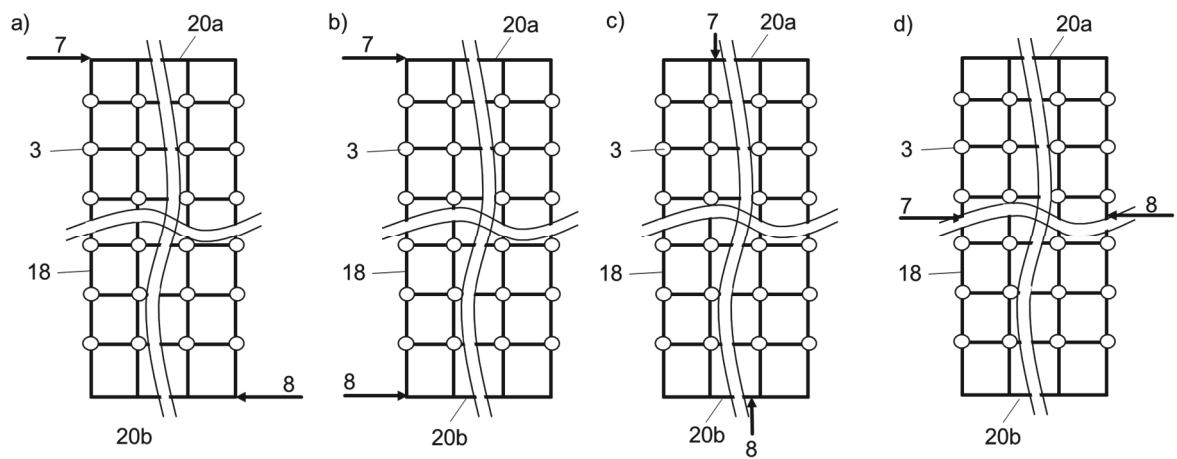


Figure 6: Linear complete lattice of membrane blocks with connection conduits and cross-distributor conduits and two gas sources

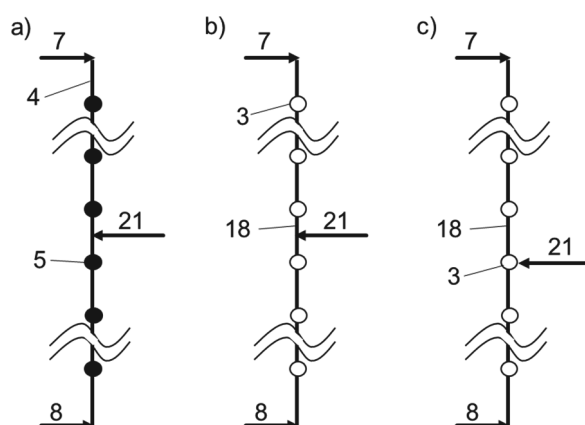


Figure 7: Membrane block according to the invention with distributor respectively connection conduit(s) and three gas sources

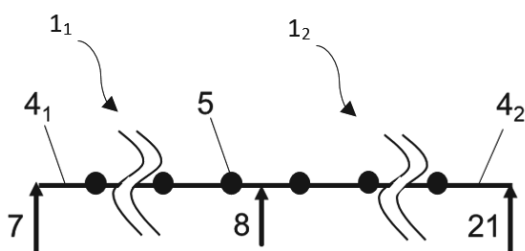


Figure 8: Two membrane blocks according to the invention, each with distributor conduit, and three gas sources

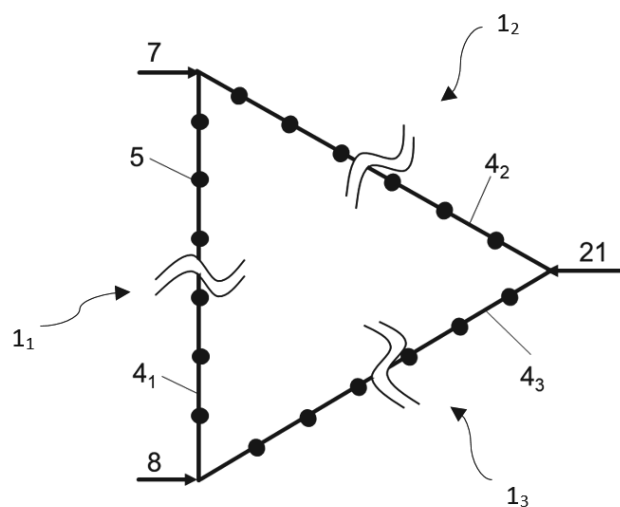


Figure 9: Three membrane blocks according to the invention, each with distributor conduit, and three gas sources in a ring circuit

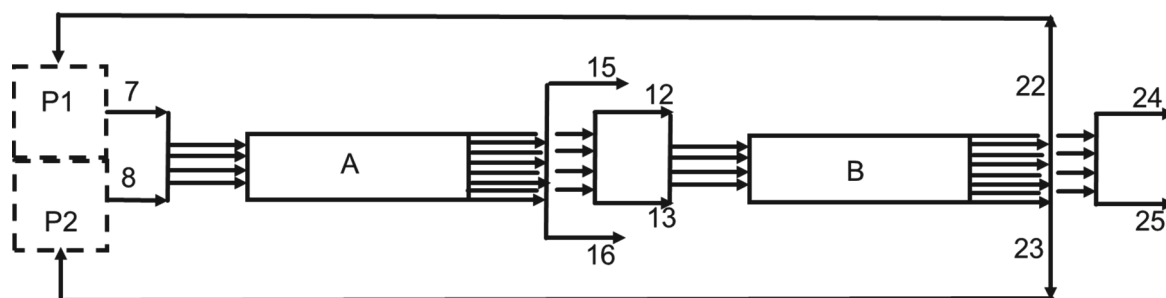


Figure 10: 2-stage interconnection of membrane separation stages according to the invention

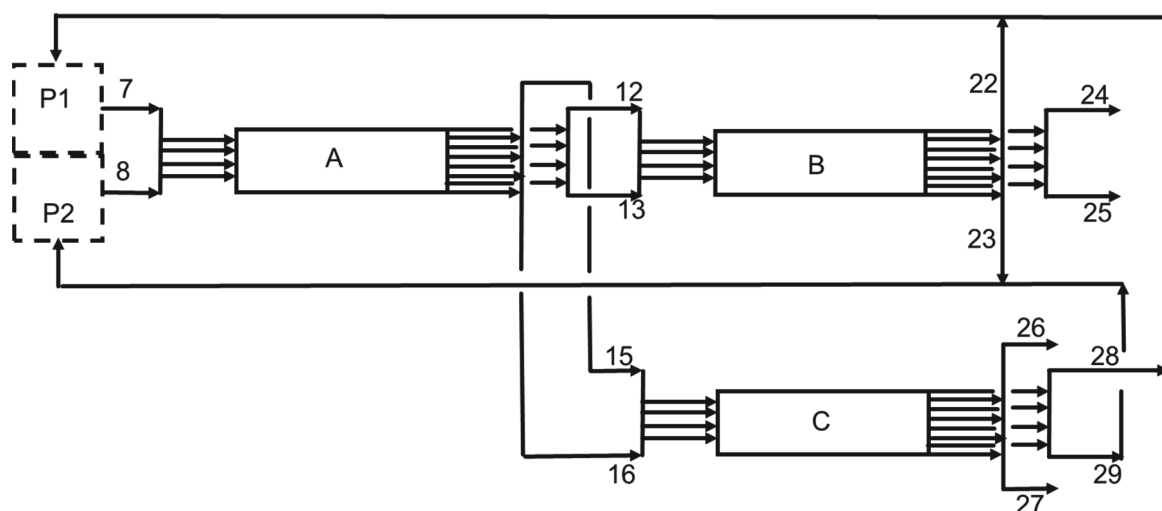


Figure 11: 3-stage interconnection of membrane separation stages according to the invention

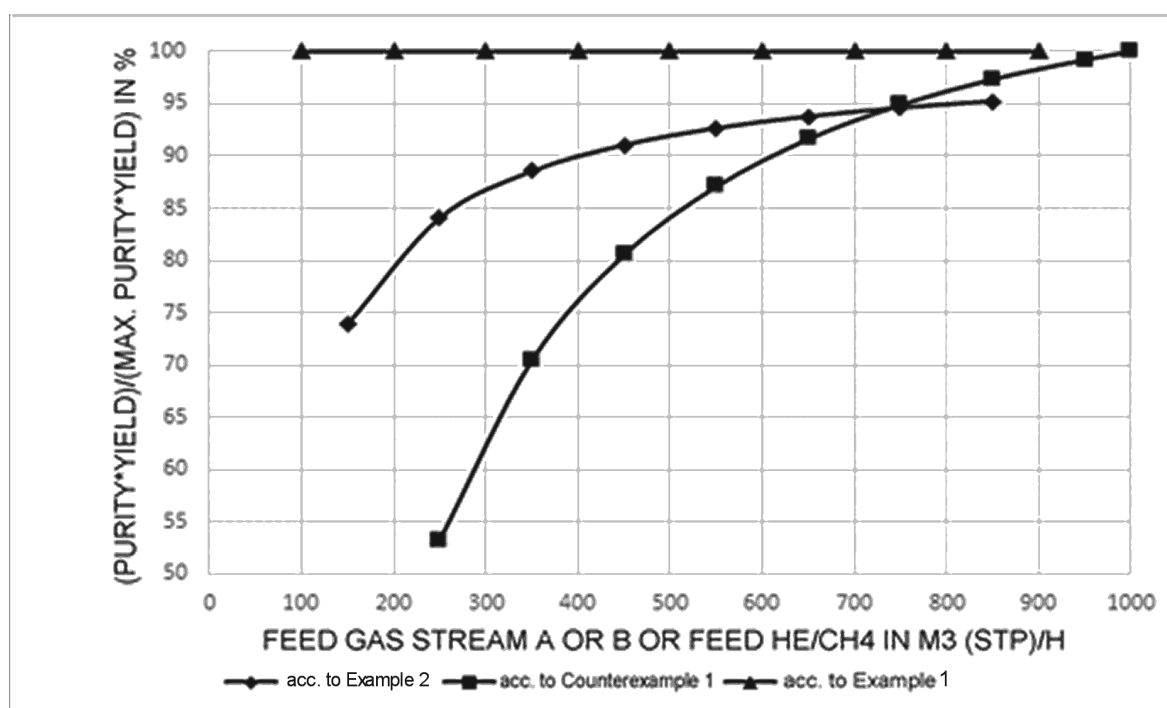


Figure 12: Comparison of the products of yield and purity of methane in the retentate (retentate gas conduit (12) or retentate from the He/CH₄ separation unit) based on the maximum achievable value from Examples 1 and 2 with Comparative Example 1