What is claimed is:

1. A two stage hydrocracking process comprising:

a) hydrocracking a hydrocarbon feed in a first hydrocracking stage under hydrocracking conditions; and

b) passing an effluent from the first hydrocracking stage to a second hydrocracking stage wherein the effluent is hydrocracked under hydrocracking conditions, with the catalyst in the second hydrocracking stage comprising a base comprised of alumina, an amorphous silica-alumina (ASA) material, and a USY zeolite, impregnated with at least one Group 6 and at least one Group 8-10 metal, and an organic acid.

2. The process of claim 1, wherein the base comprises 0.1 to 40 wt. % alumina, 0.1 to 40 wt. % ASA, and 20 to 85 wt. % USY zeolite.

3. The process of claim 2, wherein the amount of alumina ranges from 20 to 30 wt. %.

4. The process of claim 2, wherein the amount of ASA ranges from 15 to 30 wt. %.

5. The process of claim 2, wherein the amount of USY zeolite ranges from 30 to 60 wt. %.

6. The process of claim 1, wherein the selectivity from the hydrocracking process of naphtha products having a boiling point in the range of 180-347° F (82-175° C) is at least 50 wt. %.

7. The process of claim 6, wherein the selectivity is at least 60 wt. %.

8. The process of claim 6, wherein at RCP=347° F (175° C), C_9 yield is at least 12 wt. % and C_{10} yield is at least 4 wt. %.

9. The process of claim 1, wherein effluent from the second hydrocracking stage comprises unconverted oil which is recycled back to the second hydrocracking stage, as recycled bottom oil (RBO).

10. The process of claim 9, wherein the paraffin content measured by mass spectrometry is at least 30 vol. % in the RBO.

11. The process of claim 9, wherein the H content measured by H NMR is at least 13.5 wt. % in the RBO.

12. The process of claim 1, wherein the first hydrocracking stage employs a conventional hydrocracking catalyst.

13. The process of claim 1, wherein the catalyst in the second hydrocracking stage comprises the metals nickel (Ni) and tungsten (W) impregnated into the base, and the organic acid comprises citric acid.

14. The process of claim 13, wherein the catalyst in the second hydrocracking stage comprises from 2 to 10 wt. % of nickel salt and from 8 to 40 wt. % of tungsten salt based on the bulk dry weight of the hydrocracking catalyst.

15. The process of claim 1, wherein the organic acid comprises citric acid.

16. The process of claim 1, wherein the catalyst in the second hydrocracking stage is prepared by a method comprising the steps of:

(a) forming an extrudable mass containing the catalyst support base,

(b) extruding the mass to form a shaped extrudate,

(c) calcining the mass to form a calcined extrudate,

(d) preparing an impregnation solution containing at least one metal nitrate or metal carbonate, an organic acid and an ammonium containing component, and adjusting the pH of the impregnation solution to between 1 and 5.5 with a hydroxide base, inclusive,

(e) contacting the shaped extrudate with the impregnation solution, and

(f) drying the impregnated extrudate at a temperature sufficient to remove the impregnation solution solvent, and to form a dried impregnated extrudate.

17. The process of claim 16, wherein the impregnation solution comprises nickel carbonate and citric acid.

18. The process of claim 17, wherein the organic acid comprises citric acid.

19. A hydrocracking catalyst comprising a base of alumina, an amorphous silicia-alumina, and a USY zeolite, with the base impregnated with at least one Group 6 metal and at least one Group 8-10 metal, and an organic acid, wherein the amount of alumina ranges from 20 to 30 wt.%.

20. The hydrocracking catalyst of claim 19, wherein the base comprises 0.1 to 40 wt. % ASA, and 20 to 85 wt. % USY zeolite.

21. The hydrocracking catalyst of claim 19, wherein the amount of ASA ranges from 15 to 30 wt. %.

22. The hydrocracking catalyst of claim 19, wherein the amount of USY zeolite ranges from 30 to 60 wt. %.

23. The hydrocracking catalyst of claim 19, wherein the catalyst comprises the metals nickel (Ni) and tungsten (W) impregnated into the base.

24. The hydrocracking catalyst of claim 23, wherein the catalyst comprises from 2 to 10 wt. % of nickel salt and from 8 to 40 wt. % of tungsten salt based on the bulk dry weight of the hydrocracking catalyst.

25. The catalyst of claim 19, wherein the catalyst comprises citric acid as the organic acid.