CLAIMS:

1. A method for making lubricant base stock, comprising:

a) performing solvent deasphalting using a C_{4+} solvent under effective solvent deasphalting conditions on a feedstock having a T5 boiling point of at least about 370°C (or at least about 400ºC, or at least about 450ºC, or at least about 500ºC), the effective solvent deasphalting conditions producing a yield of deasphalted oil of at least about 50 wt% of the feedstock;

b) hydroprocessing at least a portion of the deasphalted oil under first effective hydroprocessing conditions comprising first hydrocracking conditions to form a hydroprocessed effluent, the at least a portion of the deasphalted oil having an aromatics content of at least about 50 wt%;

c) separating the hydroprocessed effluent to form at least a fuels boiling range fraction, a first fraction having a T_5 distillation point of at least 370°C, and a second fraction having a T_5 distillation point of at least 370°C, the second fraction having a higher kinematic viscosity at 100°C than the first fraction;

d) hydroprocessing at least a portion of the first fraction under second effective hydroprocessing conditions, the second effective hydroprocessing conditions comprising exposing the first fraction to a medium pore dewaxing catalyst to form a first catalytically dewaxed effluent comprising a 370°C+ portion having a first kinematic viscosity at 100°C; and

e) hydroprocessing at least a portion of the second fraction under third effective hydroprocessing conditions, the third effective hydroprocessing conditions comprising exposing the second fraction to the medium pore dewaxing catalyst to form a second catalytically dewaxed effluent comprising a 370°C+ portion having a second kinematic viscosity at 100°C that is greater than the first kinematic viscosity at 100°C,

wherein the first hydroprocessing conditions further comprise first aromatic saturation conditions, the first aromatic saturation conditions comprising exposing the at least a portion of the deasphalted oil to a demetallization catalyst, the at least a portion of the deasphalted oil being exposed to the demetallization catalyst after exposing the at least a portion of the deasphalted oil to the hydrocracking catalyst; and

wherein the second effective hydroprocessing conditions are different from the third effective hydroprocessing conditions.

2. The method of claim 1, wherein the medium pore dewaxing catalyst comprises ZSM-5; wherein the medium pore dewaxing catalyst comprises 0.05 wt% or less of Group VIII metals; wherein the at least a portion of the deasphalted oil comprises a sulfur content of 300 wppm or more, or a combination thereof.

3. The method of claim 1, wherein:

during step b), the hydroprocessed effluent comprises a sulfur content of 300 wppm or less, a nitrogen content of 100 wppm or less, or a combination thereof;

during step d), the at least a portion of the first fraction is exposed to the second aromatic saturation conditions prior to the second catalytic dewaxing conditions, and the second aromatic saturation conditions optionally comprises exposing the at least a portion of the first fraction to an amorphous aromatic saturation catalyst; and

during step e), the at least a portion of the second fraction is exposed to the third aromatic saturation conditions prior to the third catalyst dewaxing conditions.

4. The method of any of claims 1 to 3, wherein the second effective hydroprocessing conditions and third effective hydroprocessing conditions are different based on a difference in at least one of a hydrocracking pressure, a hydrocracking temperature, a dewaxing pressure, and a dewaxing temperature.

5. The method of any of claims 1 to 4, wherein at least a portion of the first fraction, at least a portion of the second fraction, at least a portion of the first catalytically dewaxed effluent, at least a portion of the second catalytically dewaxed effluent, or a combination thereof is used as a feed for a steam cracker; or wherein at least a portion of the second catalytically dewaxed effluent is used as an asphalt blend component; or a combination thereof.

6. The method of any of claims 1 to 5, wherein separating the hydroprocessed effluent further comprises forming an additional fraction having a T_5 distillation point of at least 370°C, the method further comprising:

hydroprocessing at least a portion of the additional fraction under third effective hydroprocessing conditions, the third effective hydroprocessing conditions comprising catalytic dewaxing conditions, to form a third catalytically dewaxed effluent comprising a 370°C+ portion having a kinematic viscosity at 100°C of 3.5 cSt or more.

7. The method of any of claims 1 to 6, wherein the hydroprocessing at least a portion of the first fraction and the hydroprocessing at least a portion of the second fraction comprise block operation of a processing system.

8. The method of any of claims 1 to 7, further comprising recycling at least a portion of the second catalytically dewaxed effluent as part of the at least a portion of the deasphalted oil, as part of the at least a portion of the fist fraction, or a combination thereof.