

SPECIFICATION

ISOCYANATE PRODUCTION PROCESS

5 Technical Field

[0001]

The present invention relates to an isocyanate production process.

Background Art

10 [0002]

Isocyanates are widely used as raw materials of such products as polyurethane foam, paints, adhesives and the like. The main industrial production process of isocyanates involves reacting amine compounds with phosgene (phosgene method), and nearly the entire amount of isocyanates produced throughout the world are
15 produced according to the phosgene method. However, the phosgene method has numerous problems.

[0003]

Firstly, this method requires the use of a large amount of phosgene as the raw material. Phosgene is extremely toxic and requires special handling precautions to
20 prevent exposure of handlers thereof, and also requires special apparatuses to detoxify waste.

Secondly, since highly corrosive hydrogen chloride is produced in large amounts as a by-product of the phosgene method, in addition to requiring a process for detoxifying the hydrogen chloride, in many cases hydrolytic chlorine is contained
25 in the isocyanates produced. Consequently, in the case of using isocyanates produced by the phosgene method, the isocyanates may have a detrimental effect on

the weather resistance and heat resistance of polyurethane products.

[0004]

On the basis of this background, a process for producing isocyanate compounds has been sought that does not use phosgene. One example of a method for producing isocyanate compounds without using phosgene that has been proposed involves thermal decomposition of carbamic acid esters. Isocyanates and hydroxy compounds have long been known to be obtained by thermal decomposition of carbamic acid esters (see, for example, Non-Patent document 1). The basic reaction is illustrated by the following formula:

[0005]



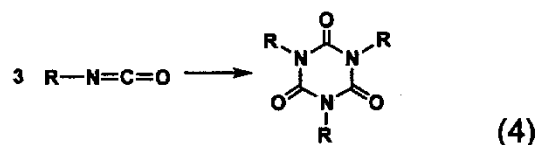
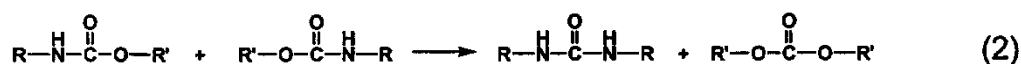
[0006]

(wherein R represents an organic residue having a valence of a, R' represents a monovalent organic residue, and a represents an integer of 1 or more).

[0007]

On the other hand, thermal decomposition of carbamic acid esters is susceptible to the simultaneous occurrence of various irreversible side reactions such as thermal denaturation reactions undesirable for carbamic acid esters or condensation of isocyanates formed by the thermal decomposition. Examples of these side reactions may include a reaction in which urea bonds are formed as represented by the following formula (2), a reaction in which carbodiimides are formed as represented by the following formula (3), and a reaction in which isocyanurates are formed as represented by the following formula (4) (see Non-Patent documents 1 and 2).

[0008]



[0009]

- 5 Note that in the above formulas, R and R' represent groups such as aliphatic alkyl groups or aromatic alkyl groups.

In addition to these side reactions leading to a decrease in yield and selectivity of the target isocyanate, in the production of polyisocyanates in particular, these reactions may make long-term operation difficult as a result of, for example, causing
10 the precipitation of polymeric solids that clog the reaction vessel.

[0010]

Various processes have been proposed thus far for the production of isocyanates without using phosgene.

[0011]

- 15 According to the description of Patent document 1, aliphatic diurethane and / or alicyclic diurethane and / or aliphatic polyurethane and / or alicyclic polyurethane are obtained by reacting aliphatic primary diamine and / or alicyclic primary diamine and / or aliphatic primary polyamine and / or alicyclic primary polyamine in the presence of an O-alkyl carbamate and alcohol, in the presence or absence of a catalyst at a
20 temperature of from 160 to 300°C such that the ratio of amine NH₂ groups to carbamate to alcohol is 1:0.8 to 10:0.25 to 50, and by removing the ammonia formed as necessary. The resulting diurethane and / or polyurethane can be converted to the corresponding diisocyanate and / or highly functional polyisocyanate as necessary. Details of the reaction conditions of the thermal decomposition are not

described in the applicable patent document.

[0012]

According to Patent document 2, aromatic diisocyanates and / or polyisocyanates are produced by going through the following two steps. More specifically, in the first step, an aromatic primary amine and / or aromatic primary polyamine are reacted with an O-alkyl carbamate in the presence or absence of a catalyst and in the presence or absence of urea and alcohol to form an aryl diurethane and / or aryl polyurethane followed by removal of the ammonia formed as necessary. In the second step, an aromatic isocyanate and / or aromatic polyisocyanate are obtained by thermal decomposition of the aryl diurethane and / or aryl polyurethane.

[0013]

Other publications contain descriptions relating to the partial substitution of urea and / or diamine a carbonyl-containing compound such as N-substituted carbamate and / or dialkyl carbonate, or by mono-substituted urea, di-substituted urea, mono-substituted polyurea or di-substituted polyurea (see Patent document 3, Patent document 4, Patent document 5, Patent document 6 and Patent document 7). Patent document 8 describes a process for producing aliphatic O-aryl urethane by reacting (cyclic) aliphatic polyamines with urea and aromatic hydroxy compounds.

[0014]

Several processes are known for forming the corresponding isocyanate and alcohol by thermal decomposition of the (cyclic) aliphatic, and particularly the aromatic monourethanes and diurethanes, examples of which may include a process carried out at a high temperature in a gaseous phase, and a process carried out under comparatively low temperature conditions in a liquid phase. In these processes, however, since there are cases in which, for example, the reaction

mixture forms precipitates, polymeric substances and closed compounds in the reaction vessel and recovery apparatus due to the occurrence of side reactions as previously described, or these substances form substances that adhere to the walls of the reaction vessel, economic efficiency is poor in the case of producing isocyanates over a long period of time.

[0015]

Thus, chemical methods, such as the use of a special catalyst (see Patent document 9 and Patent document 10) or a catalyst combined with an insert solvent (see Patent document 11) are disclosed for improving yield during thermal decomposition of urethane.

[0016]

For example, Patent document 12 describes a process for producing hexamethylene diisocyanate involving thermal decomposition of hexamethylene diethyl urethane in the presence of dibenzyl toluene used as a solvent and in the presence of a catalyst mixture containing methyl toluene sulfonate and diphenyl tin dichloride. However, since there is no detailed description of production of the starting components, isolation or purification and arbitrary recovery of the solvent and catalyst mixture, the economic effects of this process were unable to be assessed.

[0017]

According to the process described in Patent document 13, urethane can be easily decomposed to isocyanate and alcohol in a carbon-containing fluidized bed without using a catalyst. In addition, according to the description of Patent document 14, hexamethylene dialkyl urethane can be decomposed in a gaseous phase at a temperature exceeding 300°C in the presence or absence of a gas-permeable packaging material composed of, for example, carbon, copper, bronze, steel, zinc, aluminum, titanium, chromium, cobalt or quartz, resulting in the

formation of hexamethylene diisocyanate.

[0018]

According to the description of Patent document 14, the process is carried out in the presence of a hydrogen halide and / or hydrogen halide donor. However, this process is unable to achieve a yield of hexamethylene diisocyanate of 90% or more. This is because the decomposition product partially rebonds resulting in the formation of urethane bonds. Thus, purification of the hexamethylene diisocyanate by distillation is still required, and there are numerous cases in which yield loss increases.

[0019]

Moreover, Patent document 15 discloses that monocarbamates can be advantageously decomposed at high yield without using a solvent under reduced pressure and / or in the presence or absence of a stabilizer and at a comparatively low temperature. The decomposition products (monoisocyanates and alcohol) are removed by distillation from a boiling reaction mixture and captured separately by fractional condensation. A method for partially removing the reaction mixture is generically described in order to remove by-products formed during thermal decomposition. Thus, although it is possible to remove by-products from the bottom of the reaction vessel, the problem of the case of substances adhering to the walls of the reaction vessel as previously described remains, and problems regarding long-term operation are unresolved. In addition, there is no description regarding the industrial use of the removed residual substances (containing large amounts of useful components).

[0020]

According to the description of Patent document 16, thermal decomposition of aliphatic, alicyclic or aromatic polycarbamates is carried out at from 150 to 350°C and

from 0.001 to 20 bar, in the presence of an inert solvent, and in the presence or absence of a catalyst and assistant in the form of hydrogen chloride, organic acid chloride, alkylation agent or organic tin compound. By-products formed can be removed continuously from the reaction vessel together with the reaction solution, for example, and corresponding amounts of fresh solvent or recovered solvent are added simultaneously. Examples of disadvantages of this process may include a decrease in the space time yield of polyisocyanate due to the use of a circulating solvent, and a large energy requirement, including recovery of the solvent. Moreover, since the assistant used is volatile under the reaction conditions, contamination of the decomposition products can occur. In addition, since there is a large amount of residual substances formed relative to the polyisocyanate formed, there is some doubt regarding economic efficiency and reliability as an industrial process.

[0021]

Patent document 17 describes a process for continuous thermal decomposition of a carbamate supplied along the inner walls of a tubular reaction vessel in the form of a liquid in the presence of a high boiling point solvent, an example of which may include an alicyclic diurethane in the form of 5-(ethoxycarbonylamino)-1-(ethoxycarbonylaminomethyl)-1,3,3-trimethylcyclohexane. This process has the shortcomings of low yield and low selectivity during production of (cyclic) aliphatic diisocyanates. In addition, there is no description of a continuous method accompanying recovery of rebonded or partially decomposed carbamates, nor is there any mention of post-treatment of solvent containing by-products and catalyst.

[0022]

According to the description of Patent document 18, a circulating process is disclosed for producing (cyclic) aliphatic diisocyanates by conversion of the

corresponding diamine to diurethane followed by thermal decomposition of the urethane. This process minimizes decreases in yield by recirculating the product of the urethane decomposition step following reaction with alcohol to an urethanation step. By-products that are unable to be recirculated are removed by separating the
5 by-products by distilling a mixture of the urethanation products, and in this case, residues of no value are formed in the form of bottom products, and all components having a comparatively low boiling point, including diurethane, are removed from the top of the column. However, this process has the shortcoming of using a large amount of energy. This is because, in addition to requiring all diurethanes to be
10 evaporated in the presence of a catalyst, the diurethanes must be evaporated at a temperature level within a range of the decomposition temperature of urethane. Isocyanate groups formed in useful products react with residual urethane, frequently resulting in the formation of comparatively high molecular weight by-products that decrease yield.

15 [0023]

According to the description of Patent document 19, a process is disclosed whereby worthless by-products are partially removed outside the system prior to carrying out thermal decomposition of polyurethane. The shortcoming of this process is a decrease in the yield of isocyanate since polyurethane ends up being
20 contained in the by-products partially removed outside the system. In addition, although components that do not undergo thermal decomposition present in a reaction mixture obtained in the thermal decomposition step of polyurethane and containing unreacted polyurethane, high boiling point oligomers, and other worthless by-products that are able to be reused are separated and continuously removed from
25 the thermal decomposition apparatus and recirculated to the urethanation step following reaction with alcohol either directly or as necessary in an attempt to

increase the yield of isocyanates, recirculated high boiling point oligomers present in the system during the urethanation step may precipitate in the urethanation reaction vessel and gradually accumulate on the walls of the reaction vessel, thereby impairing operation over a long period of time.

5 [0024]

In addition, according to the description of Patent document 20, isocyanates are produced by continuous thermal cleavage decomposition of carbamic acid ester using a process in which a reaction medium containing carbamic acid ester is heated so that a biphasic mixture is formed having a gas volume of greater than 50%, the
10 gaseous phase is continuously discharged from the reaction vessel, and the liquid phase is continuously discharged from the reaction vessel. In this process as well, although components that do not undergo thermal decomposition present in a reaction mixture containing unreacted polyurethane, high boiling point oligomers, and other worthless by-products that are able to be reused are separated and
15 continuously removed from the thermal decomposition apparatus and recirculated to the urethanation step following reaction with alcohol either directly or as necessary in an attempt to increase the yield of isocyanates, similar to the process described above, recirculated high boiling point oligomers present in the system during the urethanation step may precipitate in the urethanation reaction vessel and gradually
20 accumulate on the walls of the reaction vessel, thereby impairing operation over a long period of time.

[0025]

Patent document 21 discloses a process for carrying out thermal decomposition by evaporating methyl urethane, obtained by reacting dimethyl carbonate and amine
25 in the presence of a basic catalyst followed by introducing into a thermal decomposition reaction vessel. Although unevaporated components are removed

from the bottom of the evaporator during evaporation of methyl urethane, since methyl urethane ends up being contained in the removed components, this process has the shortcoming of causing a decrease in the yield of isocyanate. In addition, thermal denaturation of methyl urethane also tends to occur easily since methyl urethane vapor is transferred at a high temperature.

Patent document 1 : U.S. Patent No. 4497963

Patent document 2 : U.S. Patent No. 4290970

Patent document 3 : U.S. Patent No. 4388238

10 Patent document 4 : U.S. Patent No. 4430505

Patent document 5 : U.S. Patent No. 4480110

Patent document 6 : U.S. Patent No. 4596678

Patent document 7 : U.S. Patent No. 4596679

Patent document 8 : European Patent Publication No. 0320235

15 Patent document 9 : U.S. Patent No. 2692275

Patent document 10 : U.S. Patent No. 3734941

Patent document 11 : U.S. Patent No. 4081472

Patent document 12 : U.S. Patent No. 4388426

Patent document 13 : U.S. Patent No. 4482499

20 Patent document 14 : U.S. Patent No. 4613466

Patent document 15 : U.S. Patent No. 4386033

Patent document 16 : U.S. Patent No. 4388246

Patent document 17 : U.S. Patent No. 4692550

Patent document 18 : European Patent No. 0355443

25 Patent document 19 : U.S. Patent No. 5386053

Patent document 20 : Japanese Patent No. 3238201

Patent document 21 : U.S. Patent No. 5315034

Non-Patent document 1 : Berchte der Deutechen Chemischen Gesellschaft, Vol. 3, p. 653, 1870

Non-Patent documents 2 : Journal of American Chemical Society, Vol. 81, p. 2138, 1959

Disclosure of the Invention

Problems to be Solved by the Invention

[0026]

10 As has been described above, various studies have been conducted on processes for producing isocyanates without using toxic phosgene. However, due to the problem of long-term, continuous operation being difficult due to the formation of high boiling point by-products and the adhesion of these high boiling point by-products to the reaction vessel, hardly any of these processes have been carried
15 out industrially.

An object of the present invention is to provide a process that allows stable production of isocyanates over a long period without using phosgene that is free of the various problems found in the prior art.

Means for Solving the Problems

20 [0027]

As a result of conducting extensive studies to solve the above problems, the inventors of the present invention unexpectedly found that, in a process for producing isocyanates by subjecting carbamic acid ester to a thermal decomposition reaction, operation can be carried out continuously for a long period of time without causing
25 clogging of the reaction vessel due to adhesion of by-products thereto by supplying a liquid phase component recovered from a bottom of the thermal decomposition

reaction vessel to an upper portion of the thermal decomposition reaction vessel, thereby leading to completion of the present invention.

[0028]

Namely, the present invention provides the following:

- 5 [1] a process for producing an isocyanate by subjecting a carbamic acid ester to a thermal decomposition reaction, comprising the steps of:

recovering a low boiling point component in a form of a gaseous phase component from a thermal decomposition reaction vessel in which the thermal decomposition reaction is carried out;

- 10 recovering a liquid phase component containing the carbamic acid ester from a bottom of the thermal decomposition reaction vessel; and

supplying all or a portion of the liquid phase component to an upper portion of the thermal decomposition reaction vessel.

- [2] the process according to item [1], wherein the carbamic acid ester is supplied to
15 the thermal decomposition reaction vessel within a temperature range of from 50 to 180°C.

[3] the process according to item [1] or [2], wherein the carbamic acid ester is supplied to the thermal decomposition reaction vessel in a form of a liquid.

- [4] the process according to any one of items [1] to [3], wherein the carbamic acid
20 ester is a carbamic acid ester produced by reacting a carbonic acid ester with an amine compound.

- [5] the process according to item [4], wherein the reaction vessel for producing the carbamic acid ester and the thermal decomposition reaction vessel may be the same or different, and the reaction vessel for producing the carbamic acid ester and the
25 thermal decomposition reaction vessel are at least one reaction vessel selected from the group consisting of a column-type reaction vessel and a tank-type reaction

vessel.

[6] the process according to any one of items [1] to [5], wherein the thermal decomposition reaction vessel is composed of at least one reaction vessel selected from the group consisting of an evaporator, a continuous multistage distillation column, a packed column, a thin film evaporator and a falling film evaporator.

[7] the process according to any one of items [1] to [6], wherein the thermal decomposition reaction is carried out in a liquid phase.

[8] the process according to any one items [4] to [7], wherein a mixture, in which all or a portion of a hydroxy compound and / or all or a portion of the carbonic acid ester has been separated from a mixture containing the carbamic acid ester produced by reacting a carbonic acid ester and an amine compound, is supplied to a thermal decomposition reaction apparatus.

[9] the process according to item [8], wherein the separation is carried out by distillative separation, and the distillative separation is carried out at 180°C or lower.

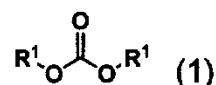
[10] the process according to any one of items [1] to [9], wherein all or a portion of the liquid phase component recovered from the bottom of the thermal decomposition reaction vessel is supplied to the upper portion of the thermal decomposition reaction vessel within a temperature range of from 50 to 180°C.

[11] the process according to any one of item [4] to [10], wherein the carbonic acid ester is used at a stoichiometric ratio of 1 time or more based on amino groups constituting the amine compound.

[12] the process according to any one of items [1] to [11], further comprising cleaning a high boiling point by-product adhered to the thermal decomposition reaction vessel, with an acid.

[13] the process according to item [12], wherein the acid is an aromatic hydroxy compound.

[14] the process according to any one of items [4] to [13], wherein the carbonic acid ester is a compound represented by the following formula (1):



(wherein R¹ represents an aliphatic group having 1 to 12 carbon atoms or an aromatic group having 6 to 12 carbon atoms).

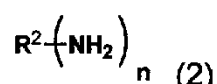
[15] the process according to item [14], wherein the carbonic acid ester contains a metal atom at from 0.001 ppm to 10%.

[16] the process according to item [15], wherein the metal atom is one type or a plurality of types of metal atoms selected from the group consisting of iron, nickel,

cobalt, zinc, tin, copper and titanium atoms.

[17] the process according to any one of items [14] to [16], wherein R¹ in the carbonic acid ester represents an aliphatic group having 5 to 7 carbon atoms or an aromatic group having 6 to 7 carbon atoms.

[18] the process according to any one of items [4] to [17], wherein the amine compound is a compound represented by the following formula (2):



(wherein R² represents a group selected from the group consisting of an aliphatic group having 1 to 20 carbon atoms and an aromatic group having 6 to 20 carbon atoms, the above group containing an atom selected from carbon and oxygen atoms, and having a valence equal to n, and

n represents an integer of from 2 to 10).

[19] the process according to item [18], wherein the amine compound is a diamine compound represented by formula (2) in which n is 2.

[20] the process according to any one of items [1] to [19], wherein a low boiling point component is supplied to a distillation column in a form of a gaseous

component from the low boiling point component formed by the thermal decomposition reaction and recovered in a form of a gaseous phase component, and a hydroxy compound originating from the carbamic acid ester and an isocyanate originating from the carbamic acid ester are separated in the distillation column.

5 [21] the process according to any one of items [1] to [20], wherein a hydroxy compound originating from the carbamic acid ester and an isocyanate originating from the carbamic acid ester are recovered separately from a low boiling point component formed by the thermal decomposition reaction and recovered in a form of a gaseous component by a thin film evaporator.

10 [22] the process according to any one of items [1] to [21], wherein the isocyanate is recovered from the liquid phase component by distillative separation.

[23] the process according to any one of items [14] to [22], wherein R^1 in the carbonic acid ester in formula (1) represents an aliphatic group having 1 to 12 carbon atoms, and the carbonic acid ester is produced according to a process which
15 comprises the following steps (1) and (2):

step (1): obtaining a reaction mixture containing a dialkyl carbonate by reacting an organic tin compound having a tin-oxygen-carbon bond and carbon dioxide; and

step (2): obtaining a dialkyl carbonate and a residue liquid by separating the reaction mixture.

20 [24] the process according to any one of items [14] to [22], wherein R^1 in the carbonic acid ester in formula (1) represents an aromatic group having 6 to 12 carbon atoms, and the carbonic acid ester is produced according to a process which comprises the following step (3) in addition to the steps (1) and (2):

step (3): obtaining a diaryl carbonate by reacting the dialkyl carbonate
25 separated in step (2) and an aromatic hydroxy compound A followed by recovering a by-product alcohol.

[25] the process according to item [23] or [24], wherein the carbonic acid ester is a carbonic acid ester produced by a process which comprises the following steps (4) and (5) in addition to the steps (1) and (2) or the steps (1) to (3):

step (4): forming an organic tin compound having a tin-oxygen-carbon bond and water by reacting the residue liquid obtained in step (2) with an alcohol followed by removing the water from a reaction system; and

step (5): reusing the organic tin compound having the tin-oxygen-carbon bond obtained in step (4) as the organic tin compound having the tin-oxygen-carbon bond of step (1).

[26] the process according to item [25], wherein the alcohol recovered in step (3) is reused as the alcohol of step (4).

[27] the process according to item [25], wherein in the case the hydroxy compound is an alcohol, it is used as the alcohol of step (4), while in the case the hydroxy compound is an aromatic hydroxy compound, it is used as the aromatic hydroxy compound A of step (3).

[28] the process according to any one of items [8] to [27], wherein the separated carbonic acid ester is reused as a carbonic acid ester.

[29] the process according to any one of items [1] to [28], wherein the thermal decomposition reaction of the carbamic acid ester is carried out in the absence of a solvent.

[30] the process according to any one of items [4] to [29], wherein supply of the amine compound to the reaction vessel in which the carbonic acid ester and the amine compound are reacted is carried out in a liquid state.

[31] the process according to any one of items [4] to [30], wherein supply of the amine compound to the reaction vessel in which the carbonic acid ester and the amine compound are reacted is carried out in a form of a mixture with alcohol, water

or carbonic acid ester.

Advantageous Effects of the Invention

[0029]

- 5 According to the present invention, isocyanates can be produced without using phosgene, and continuous operation is possible over a long period of time.

Brief Description of Drawings

[0030]

- 10 FIG. 1 is a conceptual drawing showing a continuous production apparatus for producing carbonic acid ester according to an embodiment of the present invention;

 FIG. 2 is a conceptual drawing showing a carbamic acid ester production apparatus according to an embodiment of the present invention;

- FIG. 3 is a conceptual drawing showing a low boiling point component
15 distillation apparatus according to an embodiment of the present invention;

 FIG. 4 is a conceptual drawing showing a low boiling point component distillation apparatus according to an embodiment of the present invention;

 FIG. 5 is a conceptual drawing showing an isocyanate production apparatus according to an embodiment of the present invention;

- 20 FIG. 6 is a conceptual drawing showing an isocyanate production apparatus according to an embodiment of the present invention;

 FIG. 7 is a conceptual drawing showing a carbamic acid ester production apparatus according to an embodiment of the present invention;

- FIG. 8 is a conceptual drawing showing an isocyanate production apparatus
25 according to an embodiment of the present invention;

 FIG. 9 is a conceptual drawing showing a carbamic acid ester production

apparatus according to an embodiment of the present invention;

FIG. 10 is a conceptual drawing showing a carbamic acid ester production apparatus according to an embodiment of the present invention; and

FIG. 11 is a conceptual drawing showing an isocyanate production apparatus
5 according to an embodiment of the present invention.

Description of Reference Numerals

[0031]

(in FIG. 1)

10 101, 107 : distillation column

102 : column-type reaction vessel

103, 106 : thin film evaporator

104 : autoclave

105 : decarbonization tank

15 111, 112, 117 : reboiler

121, 123, 126, 127 : condenser

1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, 15, 16, 17 : line

(in FIG. 2)

201, 202, 203, 206 : storage tank

20 204 : baffled reaction vessel

205 : column

21, 22, 23, 24, 25 : line

(in FIG. 3)

302 : continuous multistage distillation column

25 305, 306 : storage tank

301 : preheater

303 : condenser

304 : reboiler

31, 32, 33, 34, 35 : line

(in FIG. 4)

5 402 : continuous multistage distillation column

405, 406 : storage tank

401 : preheater

403 : condenser

404 : reboiler

10 41, 42, 43, 44, 45 : line

(in FIG. 5)

501 : thin film evaporator

502, 505 : continuous multistage distillation column

508, 509, 510 : storage tank

15 503, 506 : condenser

504, 507 : reboiler

50, 51, 52, 53, 54, 55, 56, 57, 58, 59, 60, 61, 62, 63, 64 : line

(in FIG. 6)

701 : thin film evaporator

20 702, 705, 708 : continuous multistage distillation column

703, 706, 709 : condenser

704, 707, 710 : reboiler

711 : storage tank

70, 71, 72, 73, 74, 75, 76, 77, 78, 79, 80, 81, 82, 83, 84, 85, 86, 87, 88, 89 : line

25 (in FIG. 7)

721, 722, 723, 725 : storage tank

724 : baffled reaction vessel

A1, A2, A3, A4 : line

(in FIG. 8)

801, 804, 807 : continuous multistage distillation column

5 802, 605, 808 : condenser

803, 806, 809 : reboiler

B1, B2, B3, B4, B5, B6, B7, B8, B9, B10, B11, B12, B13, B14, B15 : line

(in FIG. 9)

901, 902, 903, 906 : storage tank

10 904 : baffled reaction vessel

905 : column

C1, C2, C3, C4, C5, C6 : line

(in FIG. 10)

1001, 1002, 1003, 1006 : storage tank

15 1004 : baffled reaction vessel

1005 : column

1007 : condenser

D1, D2, D3, D4, D5, D6 : line

(in FIG. 11)

20 1102, 1409, 1411 : storage tank

1104 : baffled reaction vessel

1105, 1106 : continuous multistage distillation column

1107, 1110 : condenser

1108, 1112 : reboiler

25 E1, E2, E3, E4, E5, E6, E7, E8, E9, E10, E11, E12, E13 : line

Best Mode for Carrying Out the Invention

[0032]

The following provides a detailed explanation of the best mode for carrying out the present invention (hereinafter referred to as "present embodiment"). It should be noted that the present invention is not limited to the following present embodiment, but rather can be modified in various ways within the scope of the gist thereof.

[0033]

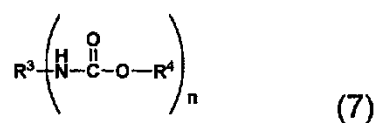
The isocyanate production process according to the present embodiment is a process for producing isocyanate by subjecting a carbamic acid ester, produced by reacting a carbonic acid ester and an amine compound, to a thermal decomposition reaction in the absence of a solvent, which comprises the steps of: recovering a low boiling point component from the thermal decomposition reaction vessel in which the thermal decomposition reaction is carried out in the form of a gaseous phase component; recovering a liquid phase component containing carbamic acid ester from a bottom of the thermal decomposition reaction vessel; and supplying all or a portion of the liquid phase component to an upper portion of the thermal decomposition reaction vessel.

[0034]

<Carbamic Acid Ester>

Although there are no particular limitations on the carbamic acid ester used in the isocyanate production process according to the present embodiment, a carbamic acid ester represented by the following formula (7) is used preferably:

[0035]



[0036]

(wherein R^3 represents a group selected from the group consisting of an aliphatic group having 1 to 20 carbon atoms and an aromatic group having 6 to 20 carbon atoms, the above group containing an atom selected from carbon and oxygen atoms, and having a valence equal to n ,

5 R^4 represents an aliphatic group having 1 to 20 carbon atoms or aromatic group having 6 to 20 carbon atoms, the aliphatic and aromatic group containing an atom selected from carbon and oxygen atoms, and

n represents an integer of from 1 to 10).

[0037]

10 In formula (7) above, the carbamic acid ester is preferably a polycarbamic acid ester in which n is a number selected from integers of 2 or more, and more preferably a polycarbamic acid ester in which n is 2.

[0038]

Examples of R^3 in formula (7) may include linear hydrocarbons such as
15 methylene, dimethylene, trimethylene, tetramethylene, pentamethylene, hexamethylene or octamethylene; unsubstituted alicyclic hydrocarbons such as cyclopentane, cyclohexane, cycloheptane, cyclooctane or bis(cyclohexyl)alkane; alkyl-substituted cyclohexanes such as methylcyclopentane, ethylcyclopentane, methylcyclohexane (including isomers), ethylcyclohexane (including isomers),
20 propylcyclohexane (including isomers), butylcyclohexane (including isomers), pentylcyclohexane (including isomers) or hexylcyclohexane (including isomers); dialkyl-substituted cyclohexanes such as dimethylcyclohexane (including isomers), diethylcyclohexane (including isomers) or dibutylcyclohexane (including isomers); trialkyl-substituted cyclohexanes such as 1,5,5-trimethylcyclohexane,
25 1,5,5-triethylcyclohexane, 1,5,5-tripropylcyclohexane (including isomers) or 1,5,5-tributylcyclohexane (including isomers); monoalkyl-substituted benzenes such

as toluene, ethylbenzene or propylbenzene; dialkyl-substituted benzenes such as xylene, diethylbenzene or dipropylbenzene; and aromatic hydrocarbons such as diphenylalkane or benzene. In particular, hexamethylene, phenylene, diphenylmethane, toluene, cyclohexane, xylenyl, methylcyclohexane, isophorone and
5 dicyclohexylmethane groups are used preferably.

[0039]

Examples of R^4 in formula (7) above may include alkyl groups such as a methyl group, an ethyl group, a propyl group (including isomers), a butyl group (including isomers), a pentyl group (including isomers), a hexyl group (including isomers), a
10 heptyl group (including isomers), an octyl group (including isomers), a nonyl group (including isomers), a decyl group (including isomers), an undecyl group (including isomers), a dodecyl group (including isomers), a tridecyl group (including isomers), a tetradecyl group (including isomers), a pentadecyl group (including isomers), a hexadecyl group (including isomers), a heptadecyl group (including isomers), an
15 octadecyl group (including isomers), a nonadecyl group (including isomers) or an eicosyl group (including isomers); cycloalkyl groups such as a cyclopentyl group, a cyclohexyl group, a cycloheptyl group, a cyclooctyl group, a cyclononyl group or a cyclodecyl group; alkoxyalkyl groups such as a methoxymethyl group, a methoxyethyl group (including isomers), a methoxypropyl group ((including isomers),
20 a methoxybutyl group (including isomers), a methoxypentyl group (including isomers), a methoxyhexyl group (including isomers), a methoxyheptyl group (including isomers), a methoxyoctyl group (including isomers), a methoxynonyl group (including isomers), a methoxydecyl group (including isomers), a methoxyundecyl group (including isomers), a methoxydodecyl group (including isomers), a methoxytridecyl group
25 (including isomers), a methoxytetradecyl group (including isomers), a methoxypentadecyl group (including isomers), a methoxyhexadecyl group (including

isomers), a methoxyheptadecyl group (including isomers), a methoxyoctadecyl group (including isomers), a methoxynonadecyl group (including isomers), an ethoxymethyl group, an ethoxyethyl group (including isomers), an ethoxypropyl group (including isomers), an ethoxybutyl group (including isomers), an ethoxypentyl group (including isomers), an ethoxyhexyl group (including isomers), an ethoxyheptyl group (including isomers), an ethoxyoctyl group (including isomers), an ethoxynonyl group (including isomers), an ethoxydecyl group (including isomers), an ethoxyundecyl group (including isomers), an ethoxydodecyl group (including isomers), an ethoxytridecyl group (including isomers), an ethoxytetradecyl group (including isomers), an ethoxypentadecyl group (including isomers), an ethoxyhexadecyl group (including isomers), an ethoxyheptadecyl group (including isomers), an ethoxyoctadecyl group (including isomers), a propyloxymethyl group (including isomers), a propyloxyethyl group (including isomers), a propyloxypropyl group (including isomers), a propyloxybutyl group (including isomers), a propyloxypentyl group (including isomers), a propyloxyhexyl group (including isomers), a propyloxyheptyl group (including isomers), a propyloxyoctyl group (including isomers), a propyloxynonyl group (including isomers), a propyloxydecyl group (including isomers), a propyloxyundecyl group (including isomers), a propyloxydodecyl group (including isomers), a propyloxytridecyl group (including isomers), a propyloxytetradecyl group (including isomers), a propyloxypentadecyl group (including isomers), a propyloxyhexadecyl group (including isomers), a propyloxyheptadecyl group (including isomers), a butyloxymethyl group (including isomers), a butyloxyethyl group (including isomers), a butyloxypropyl group (including isomers), a butyloxybutyl group (including isomers), a butyloxypentyl group (including isomers), a butyloxyhexyl group (including isomers), a butyloxyheptyl group (including isomers), a butyloxyoctyl group (including isomers), a butyloxynonyl group (including isomers), a butyloxydecyl group (including isomers),

isomers), a heptyloxydodecyl group (including isomers), a heptyloxytridecyl group (including isomers), an octyloxymethyl group, an octyloxyethyl group (including isomers), an octyloxypropyl group (including isomers), an octyloxybutyl group (including isomers), an octyloxypropyl group (including isomers), an octyloxyhexyl group (including isomers), an octyloxyheptyl group (including isomers), an octyloxyoctyl group (including isomers), an octyloxynonyl group (including isomers), an octyloxydecyl group (including isomers), an octyloxyundecyl group (including isomers), an octyloxydodecyl group (including isomers), a nonyloxymethyl group (including isomers), a nonyloxyethyl group (including isomers), a nonyloxypropyl group (including isomers), a nonyloxybutyl group (including isomers), a nonyloxypropyl group (including isomers), a nonyloxyhexyl group (including isomers), a nonyloxyheptyl group (including isomers), a nonyloxyoctyl group (including isomers), a nonyloxynonyl group (including isomers), a nonyloxydecyl group (including isomers), a nonyloxyundecyl group (including isomers), a decyloxymethyl group (including isomers), a decyloxyethyl group (including isomers), a decyloxypropyl group (including isomers), a decyloxybutyl group (including isomers), a decyloxypropyl group (including isomers), a decyloxyhexyl group (including isomers), a decyloxyheptyl group (including isomers), a decyloxyoctyl group (including isomers), a decyloxynonyl group (including isomers), a decyloxydecyl group (including isomers), an undecyloxymethyl group, an undecyloxyethyl group (including isomers), an undecyloxypropyl group (including isomers), an undecyloxybutyl group (including isomers), an undecyloxypropyl group (including isomers), an undecyloxyhexyl group (including isomers), an undecyloxyheptyl group (including isomers), an undecyloxyoctyl group (including isomers), an undecyloxynonyl group (including isomers), a dodecyloxymethyl group (including isomers), a dodecyloxyethyl group (including isomers), a dodecyloxypropyl group

(including isomers), a dodecyloxybutyl group (including isomers), a dodecyloxypentyl group (including isomers), a dodecyloxyhexyl group (including isomers), a dodecyloxyheptyl group (including isomers), a dodecyldecyloxyoctyl group (including isomers), a tridecyloxymethyl group (including isomers), a tridecyloxyethyl group (including isomers), a tridecyloxypropyl group (including isomers), a tridecyloxybutyl group (including isomers), a tridecyloxypentyl group (including isomers), a tridecyloxyhexyl group (including isomers), a tridecyloxyheptyl group (including isomers), a tetradecyloxymethyl group (including isomers), a tetradecyloxyethyl group (including isomers), a tetradecyloxypropyl group (including isomers), a tetradecyloxybutyl group (including isomers), a tetradecyloxypentyl group (including isomers), a tetradecyloxyhexyl group (including isomers), a pentadecyloxymethyl group, a pentadecyloxyethyl group (including isomers), a pentadecyloxypropyl group (including isomers), a pentadecyloxybutyl group (including isomers), a pentadecyloxypentyl group (including isomers), a hexadecyloxymethyl group (including isomers), a hexadecyloxyethyl group (including isomers), a hexadecyloxypropyl group (including isomers), a hexadecyloxybutyl group (including isomers), a heptadecyloxymethyl group, a heptadecyloxyethyl group (including isomers), a heptadecyloxypropyl group (including isomers), an octadecyloxymethyl group (including isomers) or an octadecyloxyethyl group (including isomers); and, aromatic groups such as a phenyl group, a methylphenyl group (including isomers), an ethylphenyl group (including isomers), a propylphenyl group (including isomers), a butylphenyl group (including isomers), a pentylphenyl group (including isomers), a hexylphenyl group (including isomers), a heptylphenyl group (including isomers), an octylphenyl group (including isomers), a nonylphenyl group (including isomers), a decylphenyl group (including isomers), a dodecylphenyl group (including isomers), a phenylphenyl group (including isomers), a phenoxyphenyl group (including isomers),

a cumylphenyl group (including isomers), a dimethylphenyl group (including isomers),
a diethylphenyl group (including isomers), a dipropylphenyl group (including isomers),
a dibutylphenyl group (including isomers), a dipentylphenyl group (including isomers),
a dihexylphenyl group (including isomers), a diheptylphenyl group (including isomers),
5 a diphenylphenyl group (including isomers), a diphenoxyphenyl group (including
isomers), a methylethylphenyl group (including isomers), a methylpropylphenyl group
(including isomers), a methylbutylphenyl group (including isomers), a
methylpentylphenyl group (including isomers), a methylhexylphenyl group (including
isomers), a methylheptylphenyl group (including isomers), a methyloctylphenyl group
10 (including isomers), a methylnonylphenyl group (including isomers), a
methyldecylphenyl group (including isomers), a methyldodecylphenyl group
(including isomers), a methylphenylphenyl group (including isomers), a
methylphenoxyphenyl group (including isomers), a methylcumylphenyl group
(including isomers), an ethylpropylphenyl group (including isomers), an
15 ethylbutylphenyl group (including isomers), an ethylpentylphenyl group (including
isomers), an ethylhexylphenyl group (including isomers), an ethylheptylphenyl group
(including isomers), an ethyloctylphenyl group (including isomers), an
ethylnonylphenyl group (including isomers), an ethyldecylphenyl group (including
isomers), an ethyldodecylphenyl group (including isomers), an ethylphenylphenyl
20 group (including isomers), an ethylphenoxyphenyl group (including isomers), an
ethylcumylphenyl group (including isomers), a propylbutylphenyl group (including
isomers), a propylpentylphenyl group (including isomers), a propylhexylphenyl group
(including isomers), a propylheptylphenyl group (including isomers), a
propyloctylphenyl group (including isomers), a propylnonylphenyl group (including
25 isomers), a propyldecylphenyl group (including isomers), a propylphenylphenyl group
(including isomers), a propylphenoxyphenyl group (including isomers), a

butylpentylphenyl group (including isomers), a butylhexylphenyl group (including isomers), a butylheptylphenyl group (including isomers), a butyloctylphenyl group (including isomers), a butylnonylphenyl group (including isomers), a butyldecylphenyl group (including isomers), a butylphenylphenyl group (including isomers), a
5 butylphenoxyphenyl group (including isomers), a pentylhexylphenyl group (including isomers), a pentylheptylphenyl group (including isomers), a pentyloctylphenyl group (including isomers), a pentylnonylphenyl group (including isomers), a pentylphenylphenyl group (including isomers), a pentylphenoxyphenyl group (including isomers), a hexylheptylphenyl group (including isomers), a
10 hexyloctylphenyl group (including isomers), a hexylphenylphenyl group (including isomers), a hexylphenoxyphenyl group (including isomers), a trimethylphenyl group (including isomers), a triethylphenyl group (including isomers), a tripropylphenyl group (including isomers), a tributylphenyl group (including isomers), a dimethylethylphenyl group (including isomers), a dimethylpropylphenyl group
15 (including isomers), a dimethylbutylphenyl group (including isomers), a dimethylpentylphenyl group (including isomers), a dimethylhexylphenyl group (including isomers), a dimethylheptylphenyl group (including isomers), a dimethyloctylphenyl group (including isomers), a dimethylnonylphenyl group (including isomers), a dimethyldecylphenyl group (including isomers), a
20 dimethyldodecylphenyl group (including isomers), a dimethylphenylphenyl group (including isomers), a dimethylphenoxyphenyl group (including isomers), a dimethylcumylphenyl group (including isomers), a diethylmethylphenyl group (including isomers), a diethylpropylphenyl group (including isomers), a diethylbutylphenyl group (including isomers), a diethylpentylphenyl group (including
25 isomers), a diethylhexylphenyl group (including isomers), a diethylheptylphenyl group (including isomers), a diethyloctylphenyl group (including isomers), a

diethylnonylphenyl group (including isomers), a diethyldecylphenyl group (including isomers), a diethylphenylphenyl group (including isomers), a diethylphenoxyphenyl group (including isomers), a diethylcumylphenyl group (including isomers), a dipropylmethylphenyl group (including isomers), a dipropylethylphenyl group (including isomers), a dipropylbutylphenyl group (including isomers), a dipropylpentylphenyl group (including isomers), a dipropylhexylphenyl group (including isomers), a dipropylheptylphenyl group (including isomers), a dipropylphenylphenyl group (including isomers), a dipropylphenoxyphenyl group (including isomers), a dibutylmethylphenyl group (including isomers), a dibutylethylphenyl group (including isomers), a dibutylpropylphenyl group (including isomers), a dibutylpentylphenyl group (including isomers), a dibutylhexylphenyl group (including isomers), a dibutylphenylphenyl group (including isomers), a dibutylphenoxyphenyl group (including isomers), a dipentylmethylphenyl group (including isomers), a dipentylethylphenyl group (including isomers), a dipentylpropylphenyl group (including isomers), a dipentylbutylphenyl group (including isomers), a dihexylmethylphenyl group (including isomers), a dihexylethylphenyl group (including isomers), a methylethylpropylphenyl group (including isomers), a methylethylbutylphenyl group (including isomers), a methylethylpentylphenyl group (including isomers), a methylethylhexylphenyl group (including isomers), a methylethylheptylphenyl group (including isomers), a methylethyl-octylphenyl group (including isomers), a methylethyl-nonylphenyl group (including isomers), a methylethyl-decylphenyl group (including isomers), a methylethylphenoxyphenyl group (including isomers), a methylethylcumylphenyl group (including isomers), a methylpropylbutylphenyl group (including isomers), a methylpropylpentylphenyl group (including isomers), a methylpropylhexylphenyl group (including isomers), a methylpropylheptylphenyl group (including isomers), a

methylpropyloctylphenyl group (including isomers), a methylpropylnonylphenyl group (including isomers), a methylpropyldecylphenyl group (including isomers), a methylpropylphenoxyphenyl group (including isomers), a methylpropylcumylphenyl group (including isomers), a methylbutylpentylphenyl group (including isomers), a methylbutylhexylphenyl group (including isomers), a methylbutylheptylphenyl group (including isomers), a methylbutyloctylphenyl group (including isomers), a methylbutylphenoxyphenyl group (including isomers), a methylbutylcumylphenyl group (including isomers), a methylpentylhexylphenyl group (including isomers), a methylpentylheptylphenyl group (including isomers), a methylpentyloctylphenyl group (including isomers), a methylpentylphenoxyphenyl group (including isomers), a methylhexylheptylphenyl group (including isomers), an ethylpropylbutylphenyl group (including isomers), an ethylpropylpentylphenyl group (including isomers), an ethylpropylhexylphenyl group (including isomers), an ethylpropylheptylphenyl group (including isomers), an ethylpropyloctylphenyl group (including isomers), an an ethylpropylnonylphenyl group (including isomers), an ethylpropylphenoxyphenyl group (including isomers), an ethylpropylcumylphenyl group (including isomers), an ethylbutylpentylphenyl group (including isomers), an ethylbutylhexylphenyl group (including isomers), an ethylbutylheptylphenyl group (including isomers), an ethylbutyloctylphenyl group (including isomers), an ethylbutylphenoxyphenyl group (including isomers), an ethylpentylhexylphenyl group (including isomers), an ethylpentylheptylphenyl group (including isomers), an ethylpentylphenoxyphenyl group (including isomers), a propylbutylphenyl group (including isomers), a propylbutylpentylphenyl group (including isomers), a propylbutylhexylphenyl group (including isomers), a propylbutylheptylphenyl group (including isomers), a propylbutylphenoxyphenyl group (including isomers), a propylpentylhexylphenyl group (including isomers) or a propylpentylphenoxyphenyl group.

[0040]

Among these groups, alkyl groups in which the number of carbon atoms constituting the group is a number selected from the group consisting of integers of from 5 to 12 or aryl groups in which the number of carbon atoms constituting the group is a number selected from the group consisting of integers of from 6 to 12 are preferable, and alkyl groups in the form of pentyl groups (including isomers), hexyl groups (including isomers), heptyl groups (including isomers) or octyl groups (including isomers), in which the number of carbon atoms constituting the group is a number selected from the group consisting of integers of from 5 to 7, and aryl groups in the form of phenyl groups or methylphenyl groups (including isomers), in which the number of carbon atoms constituting the group is a number selected from the group consisting of integers of from 5 to 7 are used more preferably. In the case of alkyl groups or aryl groups in which the number of carbon atoms is 4 or less, since the boiling point of the carbamic acid ester is not sufficiently high, under the conditions of thermal decomposition of carbamic acid esters to be described later, there are cases in which the carbamic acid ester is distilled off in the gaseous phase, thereby making it difficult to separate from isocyanates and the like. In addition, in the case of alkyl groups or aryl groups in which the number of carbon atoms is 8 or more, since the difference between the boiling point of the hydroxy compound formed in the thermal decomposition reaction and the boiling point of the isocyanate becomes small, difficulties may be encountered during separation.

[0041]

Examples of such alkyl polycarbamates may include alkyl carbamates such as N,N'-hexanediy-bis-carbamic acid dipentyl ester (including isomers), N,N'-hexanediy-bis-carbamic acid dihexyl ester (including isomers), N,N'-hexanediy-bis-carbamic acid diheptyl ester (including isomers),

dipentyl-4,4'-methylene-dicyclohexylcarbamate (including isomers),
 dihexyl-4,4'-methylene-dicyclohexylcarbamate (including isomers),
 diheptyl-4,4'-methylene-dicyclohexylcarbamate (including isomers),
 3-(pentyloxycarbonylaminomethyl)-3,5,5-trimethylcyclohexyl carbamic acid pentyl
 5 ester (including isomers), 3-(hexyloxycarbonylaminomethyl)-
 3,5,5-trimethylcyclohexyl carbamic acid hexyl ester (including isomers),
 3-(heptyloxycarbonylaminomethyl)-3,5,5-trimethylcyclohexyl carbamic acid heptyl
 ester (including isomers), toluene dicarbamic acid dipentyl ester (including isomers),
 toluene dicarbamic acid dihexyl ester (including isomers), toluene dicarbamic acid
 10 diheptyl ester (including isomers), N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic acid
 dipentyl ester, N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic acid dihexyl ester or
 N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic acid diheptyl ester; and, aryl
 carbamates such as N,N'-hexanediyl-bis-carbamic acid diphenyl ester,
 N,N'-hexanediyl-bis-carbamic acid di(methylphenyl) ester (including isomers),
 15 diphenyl-4,4'-methylene-dicyclohexylcarbamate,
 di(methylphenyl)-4,4'-methylene-dicyclohexylcarbamate (including isomers),
 3-(phenoxy carbonylaminomethyl)-3,5,5-trimethylcyclohexyl carbamic acid phenyl
 ester (including isomers), 3-((methylphenoxy)carbonylaminomethyl)-
 3,5,5-trimethylcyclohexyl carbamic acid (methylphenyl) ester (including isomers),
 20 toluene dicarbamic acid diphenyl ester (including isomers), toluene dicarbamic acid
 di(methylphenyl) ester (including isomers), N,N'-(4,4'-methanediyl-diphenyl)-
 biscarbamic acid diphenyl ester or N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic
 acid di(methylphenyl) ester.

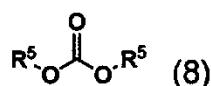
[0042]

25 These carbamic acid esters can be produced using a known process, and may
 be produced by, for example, reacting the amine compounds, carbon monoxide,

oxygen and aliphatic alcohols or aromatic hydroxy compounds. In addition, carbamic acid esters may also be produced by reacting the amine compounds, urea and the aliphatic alcohols or aromatic hydroxy compounds, or by reacting carbonic acid esters and the amine compounds. Carbamic acid esters are preferably
5 produced by reacting the carbonic acid esters and the amine compounds.

Carbonic acid esters represented by the following formula (8) can be used for the carbonic acid ester.

[0043]



10 [0044]

(wherein R^5 represents a linear or branched aliphatic group having 1 to 20 carbon atoms or an aromatic group having 6 to 20 carbon atoms).

[0045]

Examples of R^5 may include alkyl groups such as a methyl group, an ethyl
15 group, a propyl group (including isomers), a butyl group (including isomers), a pentyl group (including isomers), a hexyl group (including isomers), a heptyl group (including isomers), an octyl group (including isomers), a nonyl group (including isomers), a decyl group (including isomers), an undecyl group (including isomers), a dodecyl group (including isomers), a tridecyl group (including isomers), a tetradecyl
20 group (including isomers), a pentadecyl group (including isomers), a hexadecyl group (including isomers), a heptadecyl group (including isomers), an octadecyl group (including isomers), a nonadecyl group (including isomers) or an eicosyl group (including isomers); cycloalkyl groups such as a cyclopentyl group, a cyclohexyl group, a cycloheptyl group, a cyclooctyl group, a cyclononyl group or a cyclodecyl
25 group; alkoxyalkyl groups such as a methoxymethyl group, a methoxyethyl group

(including isomers), a methoxypropyl group ((including isomers), a methoxybutyl group (including isomers), a methoxypentyl group (including isomers), a methoxyhexyl group (including isomers), a methoxyheptyl group (including isomers), a methoxyoctyl group (including isomers), a methoxynonyl group (including isomers),
5 a methoxydecyl group (including isomers), a methoxyundecyl group (including isomers), a methoxydodecyl group (including isomers), a methoxytridecyl group (including isomers), a methoxytetradecyl group (including isomers), a methoxypentadecyl group (including isomers), a methoxyhexadecyl group (including isomers), a methoxyheptadecyl group (including isomers), a methoxyoctadecyl group
10 (including isomers), a methoxynonadecyl group (including isomers), an ethoxymethyl group, an ethoxyethyl group (including isomers), an ethoxypropyl group (including isomers), an ethoxybutyl group (including isomers), an ethoxypentyl group (including isomers), an ethoxyhexyl group (including isomers), an ethoxyheptyl group (including isomers), an ethoxyoctyl group (including isomers), an ethoxynonyl group (including isomers), an ethoxydecyl group (including isomers), an ethoxyundecyl group
15 (including isomers), an ethoxydodecyl group (including isomers), an ethoxytridecyl group (including isomers), an ethoxytetradecyl group (including isomers), an ethoxypentadecyl group (including isomers), an ethoxyhexadecyl group (including isomers), an ethoxyheptadecyl group (including isomers), an ethoxyoctadecyl group
20 (including isomers), a propyloxymethyl group (including isomers), a propyloxyethyl group (including isomers), a propyloxypropyl group (including isomers), a propyloxybutyl group (including isomers), a propyloxypentyl group (including isomers), a propyloxyhexyl group (including isomers), a propyloxyheptyl group (including isomers), a propyloxyoctyl group (including isomers), a propyloxynonyl group
25 (including isomers), a propyloxydecyl group (including isomers), a propyloxyundecyl group (including isomers), a propyloxydodecyl group (including isomers), a

(including isomers), a decyloxynonyl group (including isomers), a decyloxydecyl group (including isomers), an undecyloxymethyl group, an undecyloxyethyl group (including isomers), an undecyloxypropyl group (including isomers), an undecyloxybutyl group (including isomers), an undecyloxypentyl group (including isomers), an undecyloxyhexyl group (including isomers), an undecyloxyheptyl group (including isomers), an undecyloxyoctyl group (including isomers), an undecyloxynonyl group (including isomers), a dodecyloxymethyl group (including isomers), a dodecyloxyethyl group (including isomers), a dodecyloxypropyl group ((including isomers), a dodecyloxybutyl group (including isomers), a dodecyloxypentyl group (including isomers), a dodecyloxyhexyl group (including isomers), a dodecyloxyheptyl group (including isomers), a dodecyloxyoctyl group (including isomers), a tridecyloxymethyl group (including isomers), a tridecyloxyethyl group (including isomers), a tridecyloxypropyl group (including isomers), a tridecyloxybutyl group (including isomers), a tridecyloxypentyl group (including isomers), a tridecyloxyhexyl group (including isomers), a tridecyloxyheptyl group (including isomers), a tetradecyloxymethyl group (including isomers), a tetradecyloxyethyl group (including isomers), a tetradecyloxypropyl group (including isomers), a tetradecyloxybutyl group (including isomers), a tetradecyloxypentyl group (including isomers), a tetradecyloxyhexyl group (including isomers), a pentadecyloxymethyl group (including isomers), a pentadecyloxyethyl group (including isomers), a pentadecyloxypropyl group (including isomers), a pentadecyloxybutyl group (including isomers), a pentadecyloxypentyl group (including isomers), a hexadecyloxymethyl group (including isomers), a hexadecyloxyethyl group (including isomers), a hexadecyloxypropyl group (including isomers), a hexadecyloxybutyl group (including isomers), a heptadecyloxymethyl group (including isomers), a heptadecyloxyethyl group (including isomers), a heptadecyloxypropyl group

(including isomers), an octadecyloxymethyl group (including isomers) or an octadecyloxyethyl group (including isomers); and, aromatic groups such as a phenyl group, a methylphenyl group (including isomers), an ethylphenyl group (including isomers), a propylphenyl group (including isomers), a butylphenyl group (including isomers), a pentylphenyl group (including isomers), a hexylphenyl group (including isomers), a heptylphenyl group (including isomers), an octylphenyl group (including isomers), a nonylphenyl group (including isomers), a decylphenyl group (including isomers), a dodecylphenyl group (including isomers), a phenylphenyl group (including isomers), a phenoxyphenyl group (including isomers), a cumylphenyl group (including isomers), a dimethylphenyl group (including isomers), a diethylphenyl group (including isomers), a dipropylphenyl group (including isomers), a dibutylphenyl group (including isomers), a dipentylphenyl group (including isomers), a dihexylphenyl group (including isomers), a diheptylphenyl group (including isomers), a diphenylphenyl group (including isomers), a diphenoxyphenyl group (including isomers), a methylethylphenyl group (including isomers), a methylpropylphenyl group (including isomers), a methylbutylphenyl group (including isomers), a methylpentylphenyl group (including isomers), a methylhexylphenyl group (including isomers), a methylheptylphenyl group (including isomers), a methyloctylphenyl group (including isomers), a methylnonylphenyl group (including isomers), a methyldecylphenyl group (including isomers), a methyldodecylphenyl group (including isomers), a methylphenylphenyl group (including isomers), a methylphenoxyphenyl group (including isomers), a methylcumylphenyl group (including isomers), an ethylpropylphenyl group (including isomers), an ethylbutylphenyl group (including isomers), an ethylpentylphenyl group (including isomers), an ethylhexylphenyl group (including isomers), an ethylheptylphenyl group (including isomers), an ethyloctylphenyl group (including isomers), an

ethylnonylphenyl group (including isomers), an ethyldecylphenyl group (including isomers), an ethyldodecylphenyl group (including isomers), an ethylphenylphenyl group (including isomers), an ethylphenoxyphenyl group (including isomers), an ethylcumylphenyl group (including isomers), a propylbutylphenyl group (including isomers), a propylpentylphenyl group (including isomers), a propylhexylphenyl group (including isomers), a propylheptylphenyl group (including isomers), a propyloctylphenyl group (including isomers), a propylnonylphenyl group (including isomers), a propyldecylphenyl group (including isomers), a propylphenylphenyl group (including isomers), a propylphenoxyphenyl group (including isomers), a butylpentylphenyl group (including isomers), a butylhexylphenyl group (including isomers), a butylheptylphenyl group (including isomers), a butyloctylphenyl group (including isomers), a butylnonylphenyl group (including isomers), a butyldecylphenyl group (including isomers), a butylphenylphenyl group (including isomers), a butylphenoxyphenyl group (including isomers), a pentylhexylphenyl group (including isomers), a pentylheptylphenyl group (including isomers), a pentyloctylphenyl group (including isomers), a pentylnonylphenyl group (including isomers), a pentylphenylphenyl group (including isomers), a pentylphenoxyphenyl group (including isomers), a hexylheptylphenyl group (including isomers), a hexyloctylphenyl group (including isomers), a hexylphenylphenyl group (including isomers), a hexylphenoxyphenyl group (including isomers), a trimethylphenyl group (including isomers), a triethylphenyl group (including isomers), a tripropylphenyl group (including isomers), a tributylphenyl group (including isomers), a dimethylethylphenyl group (including isomers), a dimethylpropylphenyl group (including isomers), a dimethylbutylphenyl group (including isomers), a dimethylpentylphenyl group (including isomers), a dimethylhexylphenyl group (including isomers), a dimethylheptylphenyl group (including isomers), a

dimethyloctylphenyl group (including isomers), a dimethylnonylphenyl group (including isomers), a dimethyldecylphenyl group (including isomers), a dimethyldodecylphenyl group (including isomers), a dimethylphenylphenyl group (including isomers), a dimethylphenoxyphenyl group (including isomers), a dimethylcumylphenyl group (including isomers), a diethylmethylphenyl group (including isomers), a diethylpropylphenyl group (including isomers), a diethylbutylphenyl group (including isomers), a diethylpentylphenyl group (including isomers), a diethylhexylphenyl group (including isomers), a diethylheptylphenyl group (including isomers), a diethyloctylphenyl group (including isomers), a diethylnonylphenyl group (including isomers), a diethyldecylphenyl group (including isomers), a diethylphenylphenyl group (including isomers), a diethylphenoxyphenyl group (including isomers), a diethylcumylphenyl group (including isomers), a dipropylmethylphenyl group (including isomers), a dipropylethylphenyl group (including isomers), a dipropylbutylphenyl group (including isomers), a dipropylpentylphenyl group (including isomers), a dipropylhexylphenyl group (including isomers), a dipropylheptylphenyl group (including isomers), a dipropylphenylphenyl group (including isomers), a dipropylphenoxyphenyl group (including isomers), a dibutylmethylphenyl group (including isomers), a dibutylethylphenyl group (including isomers), a dibutylpropylphenyl group (including isomers), a dibutylpentylphenyl group (including isomers), a dibutylhexylphenyl group (including isomers), a dibutylphenylphenyl group (including isomers), a dibutylphenoxyphenyl group (including isomers), a dipentylmethylphenyl group (including isomers), a dipentylethylphenyl group (including isomers), a dipentylpropylphenyl group (including isomers), a dipentylbutylphenyl group (including isomers), a dihexylmethylphenyl group (including isomers), a dihexylethylphenyl group (including isomers), a methylethylpropylphenyl group

(including isomers), a methylethylbutylphenyl group (including isomers), a methylethylpentylphenyl group (including isomers), a methylethylhexylphenyl group (including isomers), a methylethylheptylphenyl group (including isomers), a methylethylloctylphenyl group (including isomers), a methylethylnonylphenyl group (including isomers), a methylethyldecylphenyl group (including isomers), a methylethylphenoxyphenyl group (including isomers), a methylethylcumylphenyl group (including isomers), a methylpropylbutylphenyl group (including isomers), a methylpropylpentylphenyl group (including isomers), a methylpropylhexylphenyl group (including isomers), a methylpropylheptylphenyl group (including isomers), a methylpropyloctylphenyl group (including isomers), a methylpropylnonylphenyl group (including isomers), a methylpropyldecylphenyl group (including isomers), a methylpropylphenoxyphenyl group (including isomers), a methylpropylcumylphenyl group (including isomers), a methylbutylpentylphenyl group (including isomers), a methylbutylhexylphenyl group (including isomers), a methylbutylheptylphenyl group (including isomers), a methylbutyloctylphenyl group (including isomers), a methylbutylphenoxyphenyl group (including isomers), a methylbutylcumylphenyl group (including isomers), a methylpentylhexylphenyl group (including isomers), a methylpentylheptylphenyl group (including isomers), a methylpentyloctylphenyl group (including isomers), a methylpentylphenoxyphenyl group (including isomers), a methylhexylheptylphenyl group (including isomers), an ethylpropylbutylphenyl group (including isomers), an ethylpropylpentylphenyl group (including isomers), an ethylpropylhexylphenyl group (including isomers), an ethylpropylheptylphenyl group (including isomers), an ethylpropyloctylphenyl group (including isomers), an ethylpropylnonylphenyl group (including isomers), an ethylpropylphenoxyphenyl group (including isomers), an ethylpropylcumylphenyl group (including isomers), an ethylbutylpentylphenyl group (including isomers), an ethylbutylhexylphenyl group

(including isomers), an ethylbutylheptylphenyl group (including isomers), an ethylbutyloctylphenyl group (including isomers), an ethylbutylphenoxyphenyl group (including isomers), an ethylpentylhexylphenyl group (including isomers), an ethylpentylheptylphenyl group (including isomers), an ethylpentylphenoxyphenyl group (including isomers), a propylbutylphenyl group (including isomers), a propylbutylpentylphenyl group (including isomers), a propylbutylhexylphenyl group (including isomers), a propylbutylheptylphenyl group (including isomers), a propylbutylphenoxyphenyl group (including isomers), a propylpentylhexylphenyl group (including isomers) or a propylpentylphenoxyphenyl group. Among these groups, alkyl groups in which the number of carbon atoms constituting the group is a number selected from the group of integers of from 1 to 20, such as a methyl group, an ethyl group, a propyl group (including isomers), a butyl group (including isomers), a pentyl group (including isomers), a hexyl group (including isomers), a heptyl group (including isomers) or an octyl group (including isomers), are preferable. Among these groups, alkyl groups having 1 to 12 carbon atoms or aromatic groups having 6 to 12 carbon atoms are preferable, while alkyl groups having 5 to 7 carbon atoms or aromatic groups having 5 to 7 carbon atoms are more preferable. Examples of such carbonic acid esters may include dipentyl carbonate (including isomers), dihexyl carbonate (including isomers), diheptyl carbonate (including isomers), diphenyl carbonate and di(methylphenyl) carbonate.

[0046]

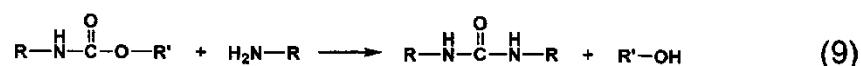
These carbonic acid esters contain metal atoms preferably within a range of from 0.001 ppm to 10%, more preferably within a range of from 0.001 ppm to 5%, and even more preferably within a range of from 0.002 ppm to 3%. In addition, the metal atoms may be present in the form of metal ions or in the form of individual metal atoms. The metal atoms are preferably metal atoms capable of having a

valence of from 2 to 4, and one type or a plurality of types of metals selected from the group consisting of iron, cobalt, nickel, zinc, tin, copper and titanium are preferable.

The inventors of the present invention unexpectedly found that when the carbonic acid esters containing metal atoms at a concentration within the above range are

5 used, an effect is demonstrated that inhibits a denaturation reaction of the carbamic acid esters formed in the reaction between the carbonic acid esters and the amine compounds. Although the mechanism by which this effect is demonstrated is not clear, the inventors of the present invention presumed that these metal atoms coordinate to urethane bonds (-NHCOO-) of carbamic acid esters formed in the
10 reaction, thereby stabilizing the urethane bonds and inhibiting side reactions as indicated in formula (2) above and formula (9) below, for example:

[0047]



[0048]

15 (wherein each of R and R' independently represents an alkyl group or aromatic group).

[0049]

In addition, although the effect of inhibiting denaturation of carbamic acid esters by metal atoms is also observed in the transport of a reaction liquid containing
20 carbamic acid esters to be described later, the mechanism of this effect is also presumed to be the same as that described above.

[0050]

Although similar effects are expected to be obtained even if a mixture is produced by mixing carbonic acid esters and the amine compounds and the
25 previously indicated examples of metal atoms are added to the mixture within the

above range, as a result of extensive studies conducted by the inventors of the present invention, it was determined that it is difficult to obtain the above effects simply by adding metal atoms to the mixture of the carbonic acid esters and the amine compounds. Although the reason for obtaining such a result is not clear, the
5 inventors of the present invention presumed that, in contrast to the carbonic acid esters coordinating to the metal atoms contained in the carbonic acid ester, since the interaction between the metal atoms and the amine compounds is greater than the interaction between the metal atoms and the carbonic acid esters, the metal atoms added to the mixture of the carbonic acid esters and the amine compounds strongly
10 coordinate to the amine compounds, thereby making it difficult to coordinate to the urethane bonds of the formed carbamic acid esters.

[0051]

Although the carbonic acid esters in the present embodiment are preferably produced by the process described below, in the case the previously indicated
15 examples of metal atoms are contained in the carbonic acid esters produced according to this process within the preferable range described above, that carbonic acid ester can be used as is. In the case the amount of the metal atoms contained in the carbonic acid esters is less than the previously described range, other metal atoms can be added in the form of an organic salt such as acetates or naphthenates,
20 chloride or acetyl acetone complex. In addition, in the case the amount of the metal atoms is greater than the previously described range, the carbonic acid esters can be used after reducing the amount of metal atoms to within the previously described range by removing by, for example, cleaning with solvent, distillative purification, crystallization or using an ion exchange resin.

25 [0052]

Note that since metal atoms contained within the above range in carbonic acid

esters are not recognized to have catalytic action in reactions between carbonic acid esters and amine compounds in nearly all cases, in this sense, they are clearly distinguished from catalysts used for the production of carbamic acid esters to be described later.

5 [0053]

Since the amount of metal components contained in the diaryl carbonate can be quantified by various known methods, such as atomic absorption analysis, inductively coupled plasma-atomic emission spectrometry, inductively coupled plasma mass spectrometry, fluorescent X-ray analysis, X-ray photoelectron spectroscopy, electron beam microanalysis or secondary ion mass spectrometry, the method can be selected in consideration of the form of the sample and the amount of metal components contained therein.

[0054]

The carbonic acid esters are preferably produced according to the following steps (1) and (2) in the case the carbonic acid ester is a dialkyl carbonate, or are produced according to the following steps (1) to (3) in the case the carbonic acid ester is a diaryl carbonate, namely:

step (1): (dialkyl carbonate formation step) obtaining a reaction mixture containing a dialkyl carbonate by reacting an organic tin compound having a tin-oxygen-carbon bond and carbon dioxide,

step (2): (dialkyl carbonate separation step) obtaining a residue liquid together with separating the dialkyl carbonate from the reaction mixture; and

step (3): (diaryl carbonate production step) obtaining a diaryl carbonate by reacting the dialkyl carbonate separated in step (2) and an aromatic hydroxy compound A followed by recovering a by-product alcohol.

[0055]

In addition, the following steps (4) and (5) can be carried out in addition to these steps (1) and (2) or steps (1) to (3), namely:

step (4): (organic tin compound regeneration step) forming an organic tin compound having a tin-oxygen-carbon bond and water by reacting the residue liquid
5 obtained in step (2) with an alcohol followed by removing the water from the reaction system; and

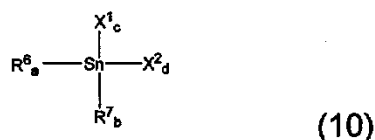
step (5): (recycling step) reusing the organic tin compound having the tin-oxygen-carbon bond obtained in step (4) as the organic tin compound having the tin-oxygen-carbon bond of step (1).

10 [0056]

Dialkyl tin compounds are preferably used for the organic tin compound used in step (1). Dialkyl tin compound refers to an organic tin compound in which two alkyl groups are bonded to a single tin atom.

Examples of these dialkyl tin compounds may include compounds selected
15 from at least one type of compound selected from the group consisting of dialkyl tin compounds represented by the following formula (10) and tetraalkyl distannoxane compounds represented by the following formula (11):

[0057]



20 [0058]

(wherein each of R^6 and R^7 independently represents a linear or branched alkyl group having 1 to 12 carbon atoms,

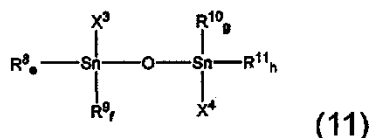
each of X^1 and X^2 independently represents at least one type of substituent selected from the group consisting of an alkoxy group, an acyloxy group and a

halogen atom,

a and b respectively represent integers of from 0 to 2, and $a + b = 2$, and

c and d respectively represent integers of from 0 to 2, and $c + d = 2$);

[0059]



[0060]

(wherein each of R^8 , R^9 , R^{10} and R^{11} independently represents a linear or branched alkyl group having 1 to 12 carbon atoms,

X^3 and X^4 represent at least one type of substituent selected from the group
10 consisting of an alkoxy group, an acyloxyl group and a halogen atom, and

e, f, g and h respectively represent integers of from 0 to 2, $e + f = 2$ and $g + h = 2$).

[0061]

Examples of R^6 and R^7 in the dialkyl tin catalyst represented by formula (10)
15 above as well as examples of R^8 , R^9 , R^{10} and R^{11} in the tetraalkyl distannoxane compound represented by formula (11) above may include alkyl groups in the form of aliphatic hydrocarbon groups in which the number of carbon atoms constituting the group is a number selected from the group consisting of integers of from 1 to 12, such as a methyl group, an ethyl group, a propyl group (including isomers), a butyl group (including isomers), a pentyl group (including isomers), a hexyl group (including isomers), a heptyl group (including isomers), an octyl group (including isomers), a nonyl group (including isomers), a decyl group (including isomers) or a dodecyl group (including isomers). More preferable examples may include linear or
20 branched alkyl groups in which the number of carbon atoms constituting the group is

a number selected from the group consisting of integers of from 1 to 8, and although dialkyl tin compounds can be used in which the alkyl group is an alkyl group in which the number of carbon atoms constituting the group is outside the range indicated above, there are cases in which fluidity may be poor or productivity may be impaired.

- 5 Moreover, an n-butyl group or n-octyl group is more preferable in consideration of ease of acquisition during industrial production.

[0062]

- X^1 and X^2 of the dialkyl tin compound represented by formula (10) above and X^3 and X^4 of the tetraalkyl distannoxane compound represented by formula (11)
- 10 above may include at least one type of substituent selected from the group consisting of an alkoxy group, an acyloxyl group and a halogen atom, and in the case the group is an alkoxy group and / or an acyloxy group, the number of carbon atoms constituting the group is preferably a number selected from the group consisting of integers of from 0 to 12. Examples of such groups may include alkoxy groups
- 15 composed of a linear or branched saturated alkyl group and an oxygen atom, such as a methoxy group, an ethoxy group, a propoxy group (including isomers), a butoxy group (including isomers), a pentyloxy group (including isomers), a hexyloxy group (including isomers), a heptyloxy group (including isomers), an octyloxy group (including isomers), a nonyloxy group (including isomers) or a decyloxy group
- 20 (including isomers); acyloxyl groups composed of a linear or branched saturated alkyl group, carbonyl group and oxygen atom, such as an acetoxy group, a propionyloxy group, a butyryloxy group, a valeryloxy group or a lauroyloxy group; and halogen atoms such as a chloro group or bromo group. More preferable examples may include alkoxy groups having 4 to 8 carbon atoms in consideration of fluidity and
- 25 solubility as well as use as a carbonic acid ester production catalyst.

[0063]

Examples of dialkyl tin compounds represented by formula (10) may include dialkyl-dialkoxy tins such as dimethyl-dimethoxy tin, dimethyl-diethoxy tin, dimethyl-dipropoxy tin (including isomers), dimethyl-dibutoxy tin (including isomers), dimethyl-dipentyloxy tin (including isomers), dimethyl-dihexyloxy tin (including isomers), dimethyl-diheptyloxy tin (including isomers), dimethyl-dioctyloxy tin (including isomers), dimethyl-dinonyloxy tin (including isomers), dimethyl-didecyloxy tin (including isomers), dibutyl-dimethoxy tin (including isomers), dibutyl-diethoxy tin (including isomers), dibutyl-dipropoxy tin (including isomers), dibutyl-dibutyloxy tin (including isomers), dibutyl-dipentyloxy tin (including isomers), dibutyl-dihexyloxy tin (including isomers), dibutyl-diheptyloxy tin (including isomers), dibutyl-dioctyloxy tin (including isomers), dibutyl-dinonyloxy tin (including isomers), dibutyl-didecyloxy tin (including isomers), dioctyl-dimethoxy tin (including isomers), dioctyl-diethoxy tin (including isomers), dioctyl-dipropoxy tin (including isomers), dioctyl-dibutyloxy tin (including isomers), dioctyl-dipentyloxy tin (including isomers), dioctyl-dihexyloxy tin (including isomers), dioctyl-diheptyloxy tin (including isomers), dioctyl-dioctyloxy tin (including isomers), dioctyl-dinonyloxy tin (including isomers) or dioctyl-didecyloxy tin (including isomers); dialkyl-diacyloxy tins such as dimethyl-diacetoxy tin, dimethyl-dipropionyloxy tin (including isomers), dimethyl-dibutyryloxy tin (including isomers), dimethyl-valeryloxy tin (including isomers), dimethyl-dilauroyloxy tin (including isomers), dibutyl-diacetoxy tin (including isomers), dibutyl-dipropionyloxy tin (including isomers), dibutyl-dibutyryloxy tin (including isomers), dibutyl-divaleryloxy tin (including isomers), dibutyl-dilauroyloxy tin (including isomers), dioctyl-diacetoxy tin (including isomers), dioctyl-dipropionyloxy tin (including isomers), dioctyl-dibutyryloxy tin (including isomers), dioctyl-valeryloxy tin (including isomers) or dioctyl-dilauroyloxy tin (including isomers); and, dialkyl-dihalide tins such as dimethyl-dichloro tin, dimethyl-dibromo tin, dibutyl-dichloro tin (including isomers),

dibutyl-dibromo tin (including isomers), dioctyl-dichloro tin (including isomers) or dioctyl-dibromo tin (including isomers).

Among these, dialkyl tin dialkoxides such as dimethyl-dimethoxy tin, dimethyl-diethoxy tin, dimethyl-dipropoxy tin (including isomers), dimethyl-dibutoxy tin (including isomers), dimethyl-dipentyloxy tin (including isomers), dimethyl-dihexyloxy tin (including isomers), dimethyl-diheptyloxy tin (including isomers), dimethyl-dioctyloxy tin (including isomers), dimethyl-dinonyloxy tin (including isomers), dimethyl-didecyloxy tin (including isomers), dibutyl-dimethoxy tin (including isomers), dibutyl-diethoxy tin (including isomers), dibutyl-dipropoxy tin (including isomers), dibutyl-dibutyloxy tin (including isomers), dibutyl-dipentyloxy tin (including isomers), dibutyl-dihexyloxy tin (including isomers), dibutyl-diheptyloxy tin (including isomers), dibutyl-dioctyloxy tin (including isomers), dibutyl-dinonyloxy tin (including isomers), dibutyl-didecyloxy tin (including isomers), dioctyl-dimethoxy tin (including isomers), dioctyl-diethoxy tin (including isomers), dioctyl-dipropoxy tin (including isomers), dioctyl-dibutyloxy tin (including isomers), dioctyl-dipentyloxy tin (including isomers), dioctyl-dihexyloxy tin (including isomers), dioctyl-diheptyloxy tin (including isomers), dioctyl-dioctyloxy tin (including isomers), dioctyl-dinonyloxy tin (including isomers) or dioctyl-didecyloxy tin (including isomers) are preferable, dialkyl-dialkoxy tins such as dibutyl-dipropoxy tin (including isomers), dibutyl-dibutyryloxy tin (including isomers), dibutyl-dipentyloxy tin (including isomers), dibutyl-dihexyloxy tin (including isomers), dibutyl-diheptyloxy tin (including isomers), dioctyl-dipropoxy tin (including isomers), dioctyl-dibutoxy tin (including isomers), dioctyl-dipentyloxy tin (including isomers), dioctyl-dihexyloxy tin (including isomers) or dioctyl-diheptyloxy tin (including isomers) are more preferable, and dibutyl-dibutyloxy tin (including isomers), dibutyl-dipentyloxy tin (including isomers), dibutyl-dihexyloxy tin (including isomers), dibutyl-diheptyloxy tin (including isomers), dibutyl-dioctyloxy tin (including isomers), dioctyl-dibutyloxy tin

(including isomers), dioctyl-dipentyloxy tin (including isomers), dioctyl-dihexyloxy tin (including isomers), dioctyl-diheptyloxy tin (including isomers) or dioctyl-dioctyloxy tin (including isomers) is even more preferable.

Although the monomer structure is shown for the dialkyl tin compounds
5 represented by the formula (10), this may be a polymer structure or an associate.

[0064]

Examples of tetraalkyl dialkoxy distannoxanes represented by the formula (11)
may include 1,1,3,3-tetraalkyl-1,3-dialkoxy distannoxanes such as
1,1,3,3-tetramethyl-1,3-dimethoxy distannoxane, 1,1,3,3-tetramethyl-1,3-diethoxy
10 distannoxane, 1,1,3,3-tetramethyl-1,3-dipropoxy distannoxane (including isomers),
1,1,3,3-tetramethyl-1,3-dibutoxy distannoxane (including isomers),
1,1,3,3-tetramethyl-1,3-dipentyloxy distannoxane (including isomers), 1,1,3,3-
tetramethyl-1,3-dihexyloxy distannoxane (including isomers), 1,1,3,3-tetramethyl-
1,3-diheptyloxy distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-dioctyloxy
15 distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-dinonyloxy distannoxane
(including isomers), 1,1,3,3-tetramethyl-1,3-didecyloxydistannoxane (including
isomers), 1,1,3,3-tetrabutyl-1,3-dimethoxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-diethoxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-dipropoxy distannoxane (including isomers),
20 1,1,3,3-tetrabutyl-1,3-dibutoxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-dipentyloxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-dihexyloxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-diheptyloxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-dioctyloxy distannoxane (including isomers),
25 1,1,3,3-tetrabutyl-1,3-dinonyloxy distannoxane (including isomers),
1,1,3,3-tetrabutyl-1,3-didecyloxy distannoxane (including isomers),

	1,1,3,3-tetraoctyl-1,3-dimethoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-diethoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dipropoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dibutoxy	distannoxane	(including isomers),
5	1,1,3,3-tetraoctyl-1,3-dipentyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dihexyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-diheptyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dioctyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dinonyloxy	distannoxane	(including isomers) or
10	1,1,3,3-tetraoctyl-1,3-didecyloxy	distannoxane	(including isomers);
	1,1,3,3-tetraalkyl-1,3-diacyloxy	distannoxanes	such as
	1,1,3,3-tetramethyl-1,3-diacetoxy		distannoxane,
	1,1,3,3-tetramethyl-1,3-dipropionyloxy	distannoxane	(including isomers),
	1,1,3,3-tetramethyl-1,3-dibutyryloxy	distannoxane	(including isomers),
15	1,1,3,3-tetramethyl-1,3-divaleryloxy	distannoxane	(including isomers),
	1,1,3,3-tetramethyl-1,3-dilauroyloxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-diacetoxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-dipropionyloxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-dibutyryloxy	distannoxane	(including isomers),
20	1,1,3,3-tetrabutyl-1,3-divaleryloxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-dilauroyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-diacetoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dipropionyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dibutyryloxy	distannoxane	(including isomers),
25	1,1,3,3-tetraoctyl-1,3-divaleryloxy	distannoxane	(including isomers) or
	1,1,3,3-tetraoctyl-1,3-dilauroyloxy	distannoxane	(including isomers); and,

1,1,3,3-tetraalkyl-1,3-dihalide distannoxanes such as 1,1,3,3-tetramethyl-1,3-dichloro distannoxane, 1,1,3,3-tetramethyl-1,3-dibromo distannoxane, 1,1,3,3-tetrabutyl-1,3-dichloro distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dibromo distannoxane (including isomers),
 5 1,1,3,3-tetraocyl-1,3-dichloro distannoxane (including isomers) or 1,1,3,3-tetraocyl-1,3-dibromo distannoxane (including isomers).

Among these, 1,1,3,3-tetraalkyl-1,3-dialkoxy distannoxanes such as 1,1,3,3-tetramethyl-1,3-dimethoxy distannoxane, 1,1,3,3-tetramethyl-1,3-diethoxy distannoxane, 1,1,3,3-tetramethyl-1,3-dipropoxy distannoxane (including isomers),
 10 1,1,3,3-tetramethyl-1,3-dibutoxy distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-dipentyloxy distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-dihexyloxy distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-diheptyloxy distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-dioctyloxy distannoxane (including isomers), 1,1,3,3-tetramethyl-1,3-dinonyloxy distannoxane
 15 (including isomers), 1,1,3,3-tetramethyl-1,3-didecyloxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dimethoxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-diethoxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dipropoxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dibutoxy distannoxane (including isomers),
 20 1,1,3,3-tetrabutyl-1,3-dipentyloxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dihexyloxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-diheptyloxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dioctyloxy distannoxane (including isomers), 1,1,3,3-tetrabutyl-1,3-dinonyloxy distannoxane (including isomers),
 25 1,1,3,3-tetrabutyl-1,3-didecyloxy distannoxane (including isomers), 1,1,3,3-tetraoctyl-1,3-dimethoxy distannoxane (including isomers),

	1,1,3,3-tetraoctyl-1,3-diethoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dipropoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dibutoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dipentyloxy	distannoxane	(including isomers),
5	1,1,3,3-tetraoctyl-1,3-dihexyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-diheptyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dioctyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dinonyloxy	distannoxane	(including isomers) or
	1,1,3,3-tetraoctyl-1,3-didecyloxy	distannoxane	(including isomers) are preferable, and
10	1,1,3,3-tetrabutyl-1,3-dibutoxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-dipentyloxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-dihexyloxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-diheptyloxy	distannoxane	(including isomers),
	1,1,3,3-tetrabutyl-1,3-dioctyloxy	distannoxane	(including isomers),
15	1,1,3,3-tetraoctyl-1,3-dibutoxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dipentyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-dihexyloxy	distannoxane	(including isomers),
	1,1,3,3-tetraoctyl-1,3-diheptyloxy	distannoxane	(including isomers) or
	1,1,3,3-tetraoctyl-1,3-dioctyloxy	distannoxane	(including isomers) is more preferable.

20 Although the monomer structure is shown for the tetraalkyl dialkoxy distannoxanes represented by formula (11) above, this may also be a polymer structure or an associate.

In general, organic tin compounds easily adopt an associated structure, and although, for example, dialkyl tin dialkoxy tin is known to form a dimer structure, and
25 tetraalkyl dialkoxy distannoxanes are known to be present by forming a ladder structure in which two or three molecules are associated, even in cases in which

there are changes in this associated state, the representation of a compound in the form of a monomer structure is common for a person with ordinary skill in the art.

In addition, the previously indicated dialkyl tin compound may be used alone or two or more types may be used as a mixture.

5 [0065]

A previously disclosed production process (such as that disclosed in WO 2005/111049) can preferably be used as the process for producing the dialkyl tin compounds. This process is a process for producing the dialkyl tin compounds from dialkyl tin oxides and alcohols

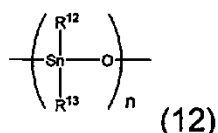
10 [0066]

Examples of alcohols used in the present embodiment may include alcohols such as methanol, ethanol, propanol (including isomers), butanol (including isomers), pentanol (including isomers), hexanol (including isomers), heptanol (including isomers), octanol (including isomers), nonanol (including isomers) or decanol (including isomers), and an alcohol is preferably used in which the number of carbon atoms constituting is a number selected from the group consisting of integers of from 1 to 12.

[0067]

Dialkyl tin oxides represented by the following formula (12) are used for the dialkyl tin oxides used in the alkyl tin alkoxide synthesis process:

[0068]



[0069]

(wherein each of R^{12} and R^{13} independently represents a linear or branched alkyl

group having 1 to 12 carbon atoms).

[0070]

Examples of R^{12} and R^{13} may include alkyl groups in the form of aliphatic hydrocarbon groups having 1 to 12 carbon atoms, such as a methyl group, an ethyl
5 group, a propyl group (including isomers), a butyl group (including isomers), a pentyl group (including isomers), a hexyl group (including isomers), a heptyl group (including isomers), an octyl group (including isomers), a nonyl group (including isomers), a decyl group (including isomers), an undecyl group (including isomers) or a dodecyl group (including isomers). More preferable examples may include linear
10 or branched saturated alkyl groups having 1 to 8 carbon atoms, while even more preferable examples may include an n-butyl group and an n-octyl group.

[0071]

Tetraalkyl dialkoxo distannoxanes and/or dialkyl tin dialkoxides are obtained by dehydration reaction of the alcohols and the dialkyl tin oxides while removing the
15 water formed from the system. The temperature at which the reaction is carried out is, for example, within a range of from 80 to 180°C, and in order to distill off the water formed from the system, although varying according to the reaction pressure, a temperature of from 100 to 180°C is preferable. Although a high temperature is preferable for the reaction temperature to accelerate the reaction rate, since
20 undesirable reactions such as decomposition may also occur at high temperatures thereby decreasing yield, the reaction temperature is more preferably within a range of from 100 to 160°C. The reaction pressure is a pressure that allows water formed to be removed from the system, and the reaction is carried out at a pressure of from 20 to 1×10^6 Pa, although varying according to the reaction temperature. There are
25 no particular limitations on the reaction time of the dehydration reaction, and is generally from 0.001 to 50 hours, preferably from 0.01 to 10 hours and more

preferably from 0.1 to 2 hours. The reaction may be terminated once the desired alkyl tin alkoxide composition has been obtained. Progression of the reaction is also determined by measuring the amount of water extracted outside the system, and can also be determined by a method using ^{119}Sn -NMR by sampling the reaction liquid.

5 In order to produce the mixture of the present embodiment in step (1), the reaction is terminated after confirming the obtaining of a composition in which the molar ratio of tetraalkyl dialkoxy distannoxane and dialkyl tin dialkoxide contained in the alkyl tin alkoxide composition obtained in the above reaction, when expressed as the combined molar percentage of both, is within a range of from 0:100 to 80:20 and
10 more preferably within a range of from 10:90 to 70:30. The alcohol used may be used while still present in the reaction system, and the alcohol may also be used by distilling off the alcohol depending on the case. Since there is the advantage of being able to reduce the size of the reaction vessels of the other steps, it is preferable to remove as much of the alcohol as possible. Removal by known
15 distillation is preferable for the removal method, and known distillation equipment can be used for the distiller used for distillation. A thin film distillation apparatus is preferably used for the distillation apparatus since the alcohol can be removed in a short period of time. There are no particular limitations on the type of reaction vessel of the dehydration reaction, and a known tank type or a column type reaction
20 vessel can be used. A low boiling point reaction mixture containing water is extracted in gaseous form from the reaction vessel by distillation, while a high boiling point reaction mixture containing a produced alkyl tin alkoxide or alkyl tin alkoxide mixture is extracted in the form of a liquid from a lower portion of the reaction vessel. Various known methods are used for such a reaction vessel, examples of which may
25 include types using reaction vessels containing a stirring tank, a multistage stirring tank, a distillation column, a multistage distillation column, a multitubular reactor, a

continuous multistage distillation column, a packed column, a thin film evaporator, a reactor provided with a support inside, a forced circulation reactor, a falling film evaporator, a falling drop evaporator, a trickle flow reactor or a bubble column, and types using combinations thereof. Methods using a column-type reactor are
5 preferable from the viewpoint of efficiently shifting the equilibrium to the products side, while a structure having a large gas-liquid contact area is preferable for being able to rapidly transfer the water formed to the gaseous phase. Although continuous methods using a multitubular reactor, a multistage distillation column or a packed column packed with a packing can also be used, since the dialkyl tin oxide used in
10 this step is generally a solid, it is preferable to employ a method in which the reaction is first carried out in a tank-type reaction vessel followed by increasing the content of dialkyl tin dialkoxide in a column-type reaction vessel. Although known materials may be used for the materials of the reaction vessel and lines provided they do not have a detrimental effect, materials such as SUS304, SUS316 or SUS316L are
15 inexpensive and can be used preferably. Known process apparatuses such as a flow meter, a thermometer and other measuring instruments or a reboiler, a pump or a condenser and the like may be added as necessary, a known method such as steam or a heater may be used for heating, and a known method such as air cooling, cooling water or brine can be used for cooling.

20 [0072]

Step (1) is a step for producing carbonic acid esters by reacting dialkyl tin compounds produced according to the process described above with gaseous carbon dioxide. A previously disclosed carbonic acid ester production process (such as that disclosed in WO 03/055840 or WO 04/014840) is preferably used in this step.

25 [0073]

The alkyl tin compounds supplied to this step may be supplied from an alkyl tin

alkoxide synthesis step at the start of production, or from a dialkyl tin compound production step of step (4) to be described later through step (5) during continuous production.

[0074]

5 In step (1), the above-mentioned dialkyl tin alkoxide and gaseous carbon dioxide are absorbed and undergo a chemical reaction to obtain a mixture containing a carbon dioxide-bonded form of the dialkyl tin alkoxide. During this chemical reaction, the dialkyl tin alkoxide is reacted in a liquid form. The dialkyl tin alkoxide is preferably put into liquid form by heating to obtain the dialkyl tin alkoxide in the liquid
10 form in the case the dialkyl tin alkoxide is in a solid form. In addition, it may also be put into liquid form by a solvent and the like. Although varying according to the reaction temperature, the reaction pressure is preferably within a range of from normal pressure to 1 MPa and more preferably within a range of from normal pressure to 0.6 MPa. Although varying according to the reaction pressure, the
15 reaction temperature is preferably within a range of from -40 to 80°C, and in consideration of fluidity during transfer, more preferably from 0 to 80°C and most preferably within a range of from normal temperature (e.g., 20°C) to 80°C. The reaction time may be within a range of from several seconds to 100 hours, and in consideration of productivity and the like, is preferably from several minutes to 10
20 hours. A known tank type reaction vessel or a column type reaction vessel can be used for the reaction vessel. In addition, a plurality of reaction vessels may be used in combination. Since the reaction is a reaction between carbon dioxide gas (gas) and an alkyl tin alkoxide composition (liquid), in order to carry out the reaction efficiently, it is preferable to increase the contact surface area between the gas and
25 liquid by increasing the gas-liquid interface. Known findings can be used for the method for reacting while increasing the gas-liquid interface in this manner, and

examples of preferable methods thereof may include increasing the stirring speed or generating bubbles in the liquid in the case of a tank type reaction vessel, and using a packed column or using a plate column in the case of a column type reaction vessel. Examples of such column type reaction vessels may include plate column
5 types using a tray such as a bubble tray, a porous plate tray, a valve tray or a counter-current tray, and packed column types packed with various types of packing materials such as a raschig ring, a lessing ring, a pole ring, a Berl saddle, an Interlock saddle, a Dixon packing, a McMahon packing, Helipak, a Sulzer packing or Mellapak. Although known materials may be used for the materials of the reaction
10 vessel and lines provided they do not have a detrimental effect, materials such as SUS304, SUS316 or SUS316L are inexpensive and can be used preferably. Known process apparatuses such as a flow meter, a thermometer and other measuring instruments or a reboiler, a pump or a condenser and the like may be added as necessary, a known method such as steam or a heater may be used for heating, and
15 a known method such as air cooling, cooling water or brine can be used for cooling. Since the reaction is normally an exothermic reaction, the reaction vessel may be cooled or it may be cooled by dissipation of heat there from. Alternatively, the reaction vessel may also be heated if the purpose is combining with a carbonic acid esterification reaction. A known method such as a method using a heat jacket or a
20 method using an internal coil can be used to heat and cool the reaction vessel. The carbon dioxide gas and alkyl tin alkoxide composition supplied to the reaction vessel may be supplied separately to the reaction vessel or they may be mixed prior to supplying to the reaction vessel. These components may also be supplied from a plurality of locations in the reaction vessel. Completion of the reaction can be
25 determined by, for example, ^{119}Sn -NMR analysis.

[0075]

Next, a reaction liquid containing carbonic acid ester is obtained from the carbon dioxide-bonded form of the dialkyl tin alkoxide obtained in the above manner according to the method described below.

Although the reaction temperature is within a range of from 110 to 200°C, and a high temperature is preferable for the reaction temperature in order to accelerate the reaction rate, since undesirable reactions such as decomposition also occur at high temperatures thereby decreasing yield, the reaction temperature is more preferably within a range of from 120 to 180°C, the reaction time is preferably within a range of from 0.1 to 10 hours, and the reaction pressure is within a range of from 1.5 to 20 MPa and preferably from 2.0 to 10 MPa. The reaction is terminated after the desired carbonic acid ester has formed in the reaction vessel. Progression of the reaction can be confirmed by, for example, sampling the reaction liquid in the reaction vessel, and analyzing the carbonic acid ester formed by a method such as ¹H-NMR or gas chromatography. For example, the reaction may be terminated after the carbonic acid ester has been formed at a molar ratio of 10% or more of the dialkyl tin alkoxide and / or carbon dioxide-bonded form of the dialkyl tin alkoxide contained in the dialkyl tin alkoxide and / or carbon dioxide-bonded form of the dialkyl tin alkoxide, and in the case of desiring to increase the yield of the carbonic acid ester, the reaction may be terminated after allowing to continue until the value reaches 90% or more. A known reaction vessel can be used for the reaction vessel, and a column type reaction vessel or a tank type reaction vessel can be used preferably. Although known materials may be used for the materials of the reaction vessel and lines provided they do not have a detrimental effect, materials such as SUS304, SUS316 or SUS316L are inexpensive and can be used preferably. Known process apparatuses such as a flow meter, thermometer and other measuring instruments or a reboiler, a pump or a condenser and the like may be added as necessary, a known

method such as steam or a heater may be used for heating, and a known method such as air cooling, cooling water or brine can be used for cooling.

[0076]

Step (2) in the present embodiment is a step for obtaining a residue liquid from
5 the reaction liquid containing carbonic acid ester obtained in step (1) above together with separating and recovering the carbonic acid ester. A known method or apparatus can be preferably used for the separation method, and a preferable method is distillation.

Carbonic acid ester and the residue liquid are obtained by batch, semi-batch or
10 continuous distillation of the reaction liquid transferred from step (1) above. A preferable example of a distillation method may include supplying the reaction liquid to a distiller, separating the carbonic acid ester in the form of a gaseous phase component from a top of the distiller outside the system, and extracting the residue liquid in the form of a liquid component from a bottom of the distiller. Although
15 varying according to the boiling point of the carbonic acid ester and pressure, the temperature in this step is within a range of from normal temperature (e.g., 20°C) to 200°C, and since there are cases in which denaturation of tin compounds in the residue liquid may occur or the amount of carbonic acid ester may decrease due to a reverse reaction at high temperatures, the reaction temperature is preferably within a
20 range of from normal temperature (e.g. 20°C) to 150°C. Although varying according to the type of carbonic acid ester and temperature at which the reaction is carried out, the reaction is generally carried out at normal pressure to reduced pressure conditions, and in consideration of productivity, the pressure is more preferably within a range of from 100 Pa to 80 KPa and most preferably within a range of from 100 Pa
25 to 50 KPa. The reaction can be carried out a reaction time within a range of from 0.01 to 10 hours, and since there are cases in which tin compounds contained in the

reaction liquid are denatured and cases in which the amount of carbonic acid ester decreases due to a reverse reaction when the reaction is carried out for a long period of time at high temperatures, the reaction time is preferably within a range of from 0.01 to 0.5 hours and most preferably within a range of from 0.01 to 0.3 hours. A known distiller can be used for the distiller, a column type distiller or a tank type distiller can be used preferably, or a plurality of types can be used in combination. More preferable examples of the distillers may include a thin film evaporator and a thin film distiller, and a thin film evaporator provided with a distillation column or a thin film distiller is most preferable. Although known materials may be used for the materials of the reaction vessel and lines provided they do not have a detrimental effect, materials such as SUS304, SUS316 or SUS316L are inexpensive and can be used preferably. Known process apparatuses such as a flow meter, a thermometer and other measuring instruments or a reboiler, a pump or a condenser and the like may be added as necessary, a known method such as steam or a heater may be used for heating, and a known method such as air cooling, cooling water or brine can be used for cooling.

[0077]

Step (3) is a step for obtaining a diaryl carbonate by reacting the dialkyl carbonate separated in step (2) and an aromatic hydroxy compound A followed by recovering a by-product alcohol. Aromatic hydroxy compound as mentioned here refers to a compound corresponding to a compound R^1OH in which a hydrogen atom is added to a group R^1O (wherein R^1 represents an aromatic group as previously defined, and O represents an oxygen atom) constituting the diaryl carbonate represented by formula (8) above. Specific examples of preferably used aromatic hydroxy compound A may include phenol, mono-substituted phenols such as methylphenol (including isomers), ethylphenol (including isomers), propylphenol

(including isomers), butylphenol (including isomers), pentylphenol (including isomers) or hexylphenol (including isomers); di-substituted phenols such as dimethylphenol (including isomers), diethylphenol (including isomers), dipropylphenol (including isomers), methylethylphenol (including isomers), methylpropylphenol (including isomers), methylbutylphenol (including isomers), methylpentylphenol (including isomers), ethylpropylphenol (including isomers) or ethylbutylphenol (including isomers); tri-substituted phenols such as trimethylphenol (including isomers), triethylphenol (including isomers), dimethylethylphenol (including isomers), dimethylpropylphenol (including isomers) or dimethylbutylphenol (including isomers); and naphthol (including isomers).

[0078]

Step (3) in the present embodiment is a step for obtaining diaryl carbonate by reacting a component mainly containing carbonic acid ester separated in step (2) and the aromatic hydroxy compound A. Numerous processes for obtaining alkyl aryl carbonates and diaryl carbonates from dialkyl carbonates and aromatic hydroxy compounds have been previously proposed, and these technologies can be preferably applied in the present embodiment as well.

[0079]

The reaction of step (3) comprises a transesterification reaction between the carbonic acid ester and the aromatic hydroxy compound, and a disproportionation reaction of the dialkyl aryl carbonate obtained in the transesterification reaction.

The transesterification reaction is an equilibrium reaction and in order to allow the reaction to proceed advantageously, it is preferable to carry out the reaction while extracting the alcohol formed by elimination in the transesterification reaction, and in this case, the boiling point of the aromatic hydroxy compound used in step (3) is preferably higher than the boiling point of the alkyl alcohol constituting the alkyl

carbonate obtained in step (2). In particular, in the case of carrying out steps (1) to (3) continuously by repeating one or more times, the boiling point of the alkyl alcohol is preferably lower than the standard boiling point of the aromatic hydroxy compound, and the difference between the boiling points thereof is preferably 2°C and more preferably 10°C in consideration of ease of separation.

[0080]

Examples of dialkyl carbonates used in step (3) may include dimethyl carbonate, diethyl carbonate, dipropyl carbonate (including isomers), dibutyl carbonate (including isomers), dipentyl carbonate (including isomers), dihexyl carbonate (including isomers), diheptyl carbonate (including isomers), dioctyl carbonate (including isomers), dinonyl carbonate (including isomers), didecyl carbonate (including isomers), dicyclopentyl carbonate (including isomers), dicyclohexyl carbonate (including isomers), dicycloheptyl carbonate (including isomers), dibenzyl carbonate, diphenethyl carbonate (including isomers), di(phenylpropyl) carbonate (including isomers), di(phenylbutyl) carbonate (including isomers), di(chlorobenzyl) carbonate (including isomers), di(methoxybenzyl) carbonate (including isomers), di(methoxymethyl) carbonate (including isomers), di(methoxyethyl) carbonate (including isomers), di(chloroethyl) carbonate (including isomers), di(cyanoethyl) carbonate (including isomers), methylethyl carbonate, methylpropyl carbonate (including isomers), methylbutyl carbonate (including isomers), ethylpropyl carbonate (including isomers), ethylbutyl carbonate (including isomers), ethylene carbonate and propylene carbonate. The carbonic acid ester used may be one type or a mixture.

Among these dialkyl carbonates, those dialkyl carbonates that are used preferably in the present embodiment are alcohols in which the standard boiling point of the alcohol constituting the carbonic acid ester is higher than the standard boiling point of water in the form of alkyl alcohols having an alkyl group having 4 to 12

carbon atoms, alkenyl alcohols having a linear or branched alkenyl group having 4 to 12 carbon atoms, cycloalkyl alcohols and aralkyl alcohols. In order to allow the reaction carried out in step (3) to proceed advantageously, an alcohol having a standard boiling point lower than the standard boiling point of the aromatic hydroxy compound used in step (3) is more preferable in consideration of removing the alcohol formed in the reaction of step (3). Namely, a dialkyl carbonate is preferable that is composed of an alcohol having a standard boiling point higher than the standard boiling point of water but lower than the standard boiling point of the aromatic hydroxy compound.

The amount of the aromatic hydroxy compound used in step (3) can be within a range of a stoichiometric ratio of from 0.1 to 10000 times the amount of dialkyl carbonate separated in step (2) and used in step (3). Since the reaction of step (3) is mainly an equilibrium reaction, although a large amount of the aromatic hydroxy compound is advantageous, since an increase in the amount used results in the need for a larger reaction vessel as well as a large distillation column for subsequently separating the product, the amount of the aromatic hydroxy compound is preferably within a range of from 1 to 1000 times and more preferably within a range of from 1 to 100 times the amount of the dialkyl carbonate.

[0081]

Although the compounds supplied to step (3) mainly contains dialkyl carbonate, aromatic hydroxy compound and, as necessary, a catalyst, impurities may be present provided they do not have a particularly detrimental effect on the reaction.

Although products in the form of alcohol, alkyl aryl carbonate and diaryl carbonate and the like may be contained among these supplied raw materials, since the reaction is reversible, the reaction rate of the raw materials decreases in the case the concentrations of these products are excessively high, thereby making this

undesirable. Although able to be varied according to the type and amount of catalyst and the reaction conditions, the weight ratio of the supplied dialkyl carbonate and aromatic hydroxy compound is generally such that the aromatic hydroxy compound is preferably supplied at a molar ratio within a range of from 0.01 to 1000
5 times the dialkyl carbonate in the supplied raw materials.

Although varying according to the reaction conditions and type and internal structure of the reaction vessel, the reaction time of the transesterification reaction of step (3) is generally from 0.001 to 50 hours, preferably from 0.01 to 10 hours and more preferably from 0.05 to 5 hours. The reaction temperature refers to the
10 temperature within the reaction vessel, and although varying according to the types of raw materials used in the form of the dialkyl carbonate and the aromatic hydroxy compound, is generally within a range of from 50 to 350°C and preferably from 100 to 280°C. In addition, although varying according to the types of raw material compounds used, the reaction temperature and the like, the reaction pressure may
15 be decreased pressure, normal pressure or increased pressure, and the reaction is generally carried out within a range of from 10 Pa to 20 MPa.

[0082]

Although the use of a solvent is not necessarily required in the present embodiment, a suitable inert solvent can be used as a reaction solvent for the
20 purpose of, for example, facilitating the reaction procedure, examples of which may include ethers, aliphatic hydrocarbons, aromatic hydrocarbons, aliphatic hydrocarbon halides and aromatic hydrocarbon halides. In addition, an inert gas such as nitrogen, helium or argon may also be present in the reaction system as an inert substance in the reaction, and the above inert gases and low boiling point organic
25 compounds inactive in the reaction may be introduced in gaseous form from the lower portion of a continuous multistage distillation column for the purpose of

accelerating the removal of low boiling point by-products formed by distillation.

[0083]

A catalyst may be added when carrying out the transesterification reaction of step (3). Although alkyl aryl carbonate and diaryl carbonate are obtained from carbonic acid ester by transesterification as previously described, since the equilibrium of this transesterification reaction is biased towards the reactants and since the reaction rate is slow, when producing diaryl carbonate by this process, several proposals have been made to improve these, and a known process can be preferably used in the present embodiment.

Although varying according to the type of catalyst used, the type of reaction vessel, the types and weight ratio of the carbonic acid ester and aromatic hydroxy compound and reaction conditions such as the reaction temperature and reaction pressure, the amount of catalyst in the case of using a catalyst in the present embodiment is generally from 0.0001 to 50% by weight when expressed as the ratio to the total amount of supplied raw materials in the form of the carbonic acid ester and aromatic hydroxy compound. In addition, in the case of using a solid catalyst, the catalyst is preferably used at an amount of from 0.01 to 75% by volume based on the volume of the empty column of the reaction vessel.

Numerous metal-containing catalysts are known in proposals relating to catalysts for increasing reaction rate, and known transesterification reaction catalysts can be used in the present embodiment as well. In a process for producing alkyl aryl carbonate and / or a mixture of alkyl aryl carbonate and diaryl carbonate by reacting the carbonic acid esters and the aromatic hydroxy compounds, Lewis acids such as transition metal hydrides or compounds that purify Lewis acids, tin compounds such as organic tin alkoxides or organic tin oxides, salts and alkoxides of alkaline earth metals or alkaline metals, lead compounds, metal complexes such as

those of copper, iron or zirconium, titanate acid esters, mixtures of Lewis acids and protic acids, Sc, Mo, Mn, Bi or Te compounds, and ferric acetate have been proposed as examples of such catalysts. Although formation of diaryl carbonate can occur by the transesterification reaction only, it is also formed by a disproportionation reaction of the alkyl aryl carbonate formed in the transesterification reaction. Here, a disproportionation reaction refers to a reaction in which dialkyl carbonate and diaryl carbonate are formed from two molecules of alkyl aryl carbonate. Although the alkyl aryl carbonate further reacts with the aromatic hydroxy compound to become a diaryl carbonate, since the disproportionation reaction is faster, in the case of desiring to obtain a diaryl carbonate, diaryl carbonate is obtained by disproportionating the alkyl aryl carbonate. Both of these reactions are equilibrium reactions. It is advantageous to allow the reaction to proceed while extracting alkyl alcohol in the transesterification reaction for producing alkyl aryl carbonate, and advantageous to allow the reaction to proceed while extracting dialkyl carbonate in the disproportionation step. Thus, the preferable reaction conditions differ in each stage. Although it is necessary to carry out the reaction by dividing into two stages in the case of carrying out the reaction continuously, in the case of carrying out the reaction in batches, the reaction can also be carried out sequentially within the same reaction vessel.

Thus, a catalyst that catalyzes the disproportionation reaction may also be present with the previously described transesterification catalyst. Numerous examples of such catalysts have been proposed, examples of which may include Lewis acids and transition metal compounds capable of generating Lewis acids, polymeric tin compounds, compounds represented by the general formula $R-X(=O)OH$ (wherein X is selected from the group consisting of Sn and Ti, while R is selected from the group consisting of monovalent hydrocarbon groups), mixtures of

Lewis acids and protic acids, lead catalysts, titanium and zirconium compounds, tin compounds and Sc, Mo, Mn, Bi or Te compounds.

[0084]

The disproportionation step is a step in which dialkyl carbonate and diaryl
5 carbonate are obtained by disproportionating the alkyl aryl carbonate obtained in the
transesterification step. As was previously described, a disproportionation catalyst
may be added when carrying out the transesterification reaction to carry out the
transesterification reaction and disproportionation reaction simultaneously, or the
transesterification reaction and disproportionation reaction may be carried out
10 separately and continuously or in batches. In addition, although there are cases in
which diaryl carbonate is obtained simultaneous to alkyl aryl carbonate in the
transesterification reaction as well in the case of carrying out the transesterification
reaction and disproportionation reaction separately, in this case as well, the
disproportionation reaction can be carried out as is. As was previously indicated,
15 the disproportionation reaction is a step in which alkyl aryl carbonate is obtained by a
transesterification reaction between the dialkyl carbonate and the aromatic hydroxy
compound, and in order to allow this equilibrium reaction to proceed advantageously,
it is advantageous to employ a method that allows the reaction to proceed while
extracting alcohol. Since the disproportionation reaction is also subjected to the
20 restriction of equilibrium, if attempting to allow the reaction to proceed
advantageously, a method that allows the reaction to proceed while extracting either
the dialkyl carbonate or diaryl carbonate formed in the disproportionation reaction
outside the system is advantageous. In the present embodiment, it is preferable to
carry out the disproportionation reaction while extracting the dialkyl carbonate outside
25 the system by selecting the respective alkoxy groups and aryl groups so that the
dialkyl carbonate of the products boils at a lower temperature than the diaryl

carbonate. The extracted dialkyl carbonate may be used by returning to a step prior to the disproportionation reaction. If the amount of diaryl carbonate produced is to be increased, it is preferable to use the extracted dialkyl carbonate by returning to the transesterification step.

5 A catalyst of a disproportionation reaction may be used in the disproportionation reaction. Numerous examples of such catalysts have been proposed. Examples of such catalysts that have been proposed may include Lewis acids and transition metal compounds capable of generating Lewis acids, polymeric tin compounds, compounds represented by the general formula $R-X(=O)OH$ (wherein X is selected
10 from the group consisting of Sn and Ti, while R is selected from the group consisting of monovalent hydrocarbon groups), mixtures of Lewis acids and protic acids, lead catalysts, titanium and zirconium compounds, tin compounds and Sc, Mo, Mn, Bi or Te compounds.

[0085]

15 The same catalysts as the transesterification catalysts used in the transesterification step can be used for the disproportionation reaction catalyst in the present embodiment.

 The alkyl aryl carbonate used in the disproportionation step is an alkyl aryl carbonic acid ester. Examples of alkyl aryl carbonates may include methylphenyl
20 carbonate, ethylphenyl carbonate, propylphenyl carbonate (including isomers), butylphenyl carbonate (including isomers), allylphenyl carbonate (including isomers), pentylphenyl carbonate (including isomers), hexylphenyl carbonate (including isomers), heptylphenyl carbonate (including isomers), octyltolyl carbonate (including isomers), nonyl (ethylphenyl) carbonate (including isomers), decyl (butylphenyl)
25 carbonate (including isomers), methyltolyl carbonate (including isomers), ethyltolyl carbonate (including isomers), propyltolyl carbonate (including isomers), butyltolyl

carbonate (including isomers), allyltolyl carbonate (including isomers), methylxylyl carbonate (including isomers), methyl (trimethylphenyl) carbonate (including isomers), methyl (chlorophenyl) carbonate (including isomers), methyl (nitrophenyl) carbonate (including isomers), methyl (methoxyphenyl) carbonate (including isomers), methyl (pyridyl) carbonate (including isomers), ethylcumyl carbonate (including isomers), methyl (benzoylphenyl) carbonate (including isomers), ethylxylyl carbonate (including isomers) and benzylxylyl carbonate (including isomers). These alkyl aryl carbonates may be of one type or a mixture of two or more types.

Among these alkyl aryl carbonates, those which are preferably used in the present embodiment are those in which the alcohol constituting the alkyl aryl carbonate is an alcohol having a boiling point higher than that of water, the boiling point of the alcohol constituting the alkyl aryl carbonate is lower than the boiling point of the aromatic hydroxy compound constituting the alkyl aryl carbonate, is selected from, for example, alkyl alcohols having a linear or branched alkyl group having 4 to 12 carbon atoms, alkenyl alcohols having a linear or branched alkenyl group having 4 to 12 carbon atoms, cycloalkyl alcohols and aralkyl alcohols, and when considering the removal of dialkyl carbonate formed in the disproportionation reaction, is preferably a dialkyl carbonate having a boiling point lower than that of the diaryl carbonate obtained in the disproportionation reaction to enable the disproportionation reaction to proceed advantageously. As examples of such optimum combinations, the alcohol, the alcohol corresponding to the alkoxy group of a metal compound having a metal-carbon-oxygen bond represented by the previously mentioned formulas (9) and (10), and the alcohol constituting the dialkyl carbonate are alcohols selected from the group consisting of pentanol (including isomers), hexanol (including isomers) and heptanol (including isomers), while the aromatic hydroxy compound is an aromatic hydroxy compound selected from phenol and cresol.

[0086]

Although compounds supplied to the disproportionation reaction mainly contain alkyl aryl carbonate and a catalyst as necessary, impurities may also be present provided they do not have a particularly detrimental effect on the reaction.

5 Although varying according to the type of catalyst used, the type of reaction vessel, the type and amount of the alkyl aryl carbonate and reaction conditions such as the reaction temperature and reaction pressure, the amount of catalyst in the case of using a catalyst in the present embodiment is generally from 0.0001 to 50% by weight when expressed as the ratio to the total amount of supplied raw materials in
10 the form of the alkyl aryl carbonate. In addition, in the case of using a solid catalyst, the catalyst is preferably used at an amount of from 0.01 to 75% by volume based on the volume of the empty column of the reaction vessel.

[0087]

15 Although alcohol, aromatic hydroxy compound and diaryl carbonate and the like may be contained among these supplied raw materials, since the reaction is reversible, the reaction rate of the raw materials decreases in the case the concentrations of these components are excessively high, thereby making this undesirable.

20 Although varying according to the reaction conditions and type and internal structure of the reaction vessel, the reaction time of the disproportionation reaction is generally from 0.001 to 50 hours, preferably from 0.01 to 10 hours and more preferably from 0.05 to 5 hours. Although varying according to the type of alkyl aryl carbonate used, the reaction temperature is generally within a range of from 50 to 350°C and preferably from 100 to 280°C. In addition, although varying according to
25 the types of raw material compounds used, the reaction temperature and the like, the reaction pressure may be decreased pressure, normal pressure or increased

pressure, and the reaction is generally carried out within a range of from 10 Pa to 20 MPa.

Although the use of a solvent is not necessarily required in the disproportionation step of the present embodiment, a suitable inert solvent can be used as a reaction solvent for the purpose of, for example, facilitating the reaction procedure, examples of which may include ethers, aliphatic hydrocarbons, aromatic hydrocarbons, aliphatic hydrocarbon halides and aromatic hydrocarbon halides. In addition, an inert gas such as nitrogen, helium or argon may also be present in the reaction system as an inert substance in the reaction, and the above inert gases and low boiling point organic compounds inactive in the reaction may be introduced in gaseous form from the lower portion of a continuous multistage distillation column for the purpose of accelerating the distillation of low boiling point by-products formed.

[0088]

Following completion of the disproportionation reaction, diaryl carbonate is obtained by removing the catalyst, alkyl aryl carbonate, aromatic hydroxy compound and alcohol by known methods.

[0089]

There are no particular limitations on the type of reaction vessel used in the transesterification and disproportionation steps, and various known methods are used, examples of which may include types using a stirring tank, a multistage stirring tank or a multistage distillation column and combinations thereof. Batch type or continuous type reaction vessels can be used for these reaction vessels. Methods using a multistage distillation column are preferable from the viewpoint of efficiently shifting the equilibrium to the products side, and a continuous method using a multistage distillation column is particularly preferable. A multistage distillation column refers to a distillation column having multiple stages in which the number of

theoretical plates of distillation is 2 or more, and any multistage distillation column may be used provided it allows continuous distillation. Any multistage distillation column can be used for the multistage distillation column provided it is ordinarily used as a multistage distillation column, examples of which may include tray column types using a bubble tray, a porous plate tray, a valve tray or a counter-current tray, and packed column types packed with various types of packing materials such as a raschig ring, a lessing ring, a pole ring, a Berl saddle, an Interlock saddle, a Dixon packing, a McMahon packing, Helipak, a Sulzer packing or Mellapak. Moreover, a combination tray-packed column type is also used preferably that combines a tray portion with a portion packed with a packing material. In the case of carrying out a continuous method using a multistage distillation column, the starting substances and reactants are continuously supplied to a continuous multistage distillation column, and simultaneous to carrying out the transesterification reaction and / or disproportionation reaction between both substances in the liquid phase or gas-liquid phase in the presence of a metal-containing catalyst within the distillation column, a high boiling point reaction mixture containing the alkyl aryl carbonate and / or diaryl carbonate produced is extracted in liquid form from the lower portion of the distillation column, while a low boiling point reaction mixture containing by-products formed is continuously extracted in a gaseous state from the upper portion of the distillation column by distillation, thereby resulting in the production of diaryl carbonate.

0090]

Although the preceding description has indicated a production example of dialkyl carbonate and diaryl carbonate using a dialkyl tin compound, the following steps (4) and (5) can be carried out in addition to the above-mentioned steps (1) to (3), the steps (4) and (5) comprising the steps of:

step (4): forming an organic tin compound having a tin-oxygen-carbon bond

and water by reacting the residue liquid obtained in step (2) with an alcohol followed by removing the water from the reaction system; and

step (5): reusing the organic tin compound having the tin-oxygen-carbon bond obtained in step (4) as the organic tin compound having the tin-oxygen-carbon bond of step (1).

Step (4) is a step for regenerating a dialkyl tin compound by reacting the distillation residue obtained in step (2) with an alcohol.

[0091]

Examples of alcohols used in this step may include alcohols such as methanol, ethanol, propanol (including isomers), butanol (including isomers), pentanol (including isomers), hexanol (including isomers), heptanol (including isomers), octanol (including isomers), nonanol (including isomers) or decanol (including isomers), and although an alcohol is preferably used in which the number of carbon atoms constituting the alcohol is a number selected from the group consisting of integers of 1 to 12, more preferably an alcohol is used that is the same as the alcohol used in the previously described alkyl tin alkoxide synthesis step.

[0092]

The conditions of the dehydration reaction are preferably the same as the conditions of the above-mentioned alkyl tin alkoxide synthesis step. The reaction may be terminated once the desired alkyl tin alkoxide composition has been obtained. Progression of the reaction is also determined by measuring the amount of water extracted outside the system, and can also be determined by a method using ^{119}Sn -NMR by sampling the reaction liquid. In order to produce the mixture of the present embodiment in step (1), the reaction is terminated after confirming the obtaining of a composition in which the molar ratio of tetraalkyl dialkoxy distannoxane and dialkyl tin dialkoxide contained in the alkyl tin alkoxide composition obtained in

the above reaction, when expressed as the combined molar ratio of both, is within a range of from 0:100 to 80:20 and more preferably within a range of from 10:90 to 70:30. The alcohol used may be used while still present in the reaction system, and the alcohol may also be used by distilling off the alcohol depending on the case.

- 5 Since there is the advantage of being able to reduce the size of the reaction vessels of the other steps, it is preferable to remove as much of the alcohol as possible. Removal by known distillation is preferable for the removal method, and known distillation equipment can be used for the distiller used for distillation. A thin film distillation apparatus is preferably used for the distillation apparatus since the alcohol
- 10 can be removed in a short period of time. Differing from the alkyl tin alkoxide synthesis step, since dialkyl tin oxide normally in a solid state is not used in this step, there are few restrictions on the reaction vessel. Namely, there are no particular limitations on the type of reaction vessel of the dehydration reaction, and a known tank type or a column type reaction vessel can be used. A low boiling point reaction
- 15 mixture containing water is extracted in gaseous form from the reaction vessel by distillation, while a high boiling point reaction mixture containing a produced alkyl tin alkoxide or alkyl tin alkoxide mixture is extracted in the form of a liquid from the lower portion of the reaction vessel. Various known methods are used for such a reaction vessel, examples of which may include types using reaction vessels containing a
- 20 stirring tank, a multistage stirring tank, a distillation column, a multistage distillation column, a multitubular reactor, a continuous multistage distillation column, a packed column, a thin film evaporator, a reactor provided with a support inside, a forced circulation reactor, a falling film evaporator, a falling drop evaporator, a trickle flow reactor or a bubble column, and types using combinations thereof. Methods using a
- 25 columnar reactor are preferable from the viewpoint of efficiently shifting the equilibrium to the products side, while a structure having a large gas-liquid contact

area is preferable for being able to rapidly transfer the water formed to the gaseous phase. Continuous methods using a multitubular reactor, a multistage distillation column or a packed column packed with a packing are particularly preferable. Although known materials may be used for the materials of the reaction vessel and
5 lines provided they do not have a detrimental effect, materials such as SUS304, SUS316 or SUS316L are inexpensive and can be used preferably. Known process apparatuses such as a flow meter, a thermometer and other measuring instruments or a reboiler, a pump or a condenser and the like may be added as necessary, a known method such as steam or a heater may be used for heating, and a known
10 method such as air cooling, cooling water or brine can be used for cooling.

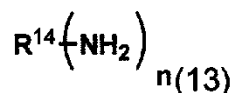
[0093]

The dialkyl tin compound produced in step (4) as described above is reused in the form of the dialkyl tin compound used in step (1) according to the next step (5) (recycling step) in which the organic tin compound having the tin-oxygen-carbon
15 bond obtained in step (4) is reused as the organic tin compound having a tin-oxygen-carbon bond of step (1).

[0094]

An amine compound represented by the following formula (13) is used for the amine compound used in the production process of the present embodiment:

20 [0095]



[0096]

(wherein R^{14} represents a group selected from the group consisting of an aliphatic group having 1 to 20 carbon atoms and an aromatic group having 6 to 20 carbon
25 atoms, the above group containing an atom selected from carbon and oxygen atoms,

and having a valence equal to n , and

n represents an integer of 1 to 10).

[0097]

In formula (13) above, a polyamine compound in which n is 1 to 3 is used preferably, while a polyamine compound in which n is 2 is used more preferably.

Examples of such polyamine compounds may include aliphatic diamines such as hexamethylene diamine, 4,4'-methylenebis(cyclohexylamine) (including isomers), cyclohexane diamine (including isomers) or 3-aminomethyl-3,5,5-trimethylcyclohexyl amine (including isomers); and aromatic diamines such as phenylene diamine (including isomers), toluene diamine (including isomers) or 4,4'-methylenedianiline. Among these, aliphatic diamines such as hexamethylene diamine, 4,4'-methylenebis(cyclohexylamine) (including isomers), cyclohexane diamine (including isomers) and 3-aminomethyl-3,5,5-trimethylcyclohexyl amine (including isomers) are used preferably, while hexamethylene diamine, 4,4'-methylenebis(cyclohexylamine) and 3-aminomethyl-3,5,5-trimethylcyclohexyl amine are used more preferably.

The amine compound is preferably supplied in a liquid state to the reaction vessel in which production of carbamic acid ester is carried out. In general, the amine compound as exemplified above is frequently a solid at normal temperature (e.g., 20°C), and in such cases, although the amine compound can be supplied in a liquid state by heating to a temperature equal to or higher than the melting point of the amine compound, if the amine compound is supplied at an excessively high temperature, since there are cases in which side-reactions such as thermal denaturation reactions caused by heating may occur, the amine compound is preferably supplied in a liquid state at a comparatively low temperature in the form of a mixture with an alcohol, water or carbonic acid ester.

[0098]

Although varying according to the reacted compounds, the reaction conditions under which the reaction between the carbonic acid ester and amine compound is carried out are such that the stoichiometric ratio of the carbonic acid ester to the amino groups of the amine compound is within a range of from 1.1 to 1000 times, and although the carbonic acid ester is preferably in excess with respect to the amino groups of the amine compound in order to complete the reaction quickly by increasing the reaction rate, in consideration of the size of the reaction vessel, the stoichiometric ratio is preferably within a range of from 2 to 100 times and more preferably within a range of from 2.5 to 30 times. The reaction temperature is generally within a range of from normal temperature (e.g., 20°C) to 200°C. Although a high temperature is preferable for increasing the reaction rate, on the other hand, since undesirable reactions also occur at high temperatures, the reaction temperature is preferably within a range of from 50 to 150°C. A known cooling apparatus or a heating apparatus may be installed in the reaction vessel to maintain a constant reaction temperature. In addition, although varying according to the types of compounds used and the reaction temperature, the reaction pressure may be decreased pressure, normal pressure or increased pressure, and the reaction is generally carried out within a range of from 20 to 1×10^6 Pa. There are no particular limitations on the reaction time (residence time in the case of a continuous process), and is generally from 0.001 to 50 hours, preferably from 0.01 to 10 hours and more preferably from 0.1 to 5 hours. In addition, the reaction can also be terminated by confirming that a desired amount of carbamic acid ester has been formed by, for example, liquid chromatography after sampling the reaction liquid. In the present embodiment, a catalyst can be used as necessary, and examples of catalysts that can be used may include organic metal compounds and inorganic metal compounds

of tin, lead, copper or titanium, and basic catalysts such as alcoholates of alkaline metals or alkaline earth metals in the form of methylates, ethylates and butyrates (including isomers) of lithium, sodium, potassium, calcium or barium. Although it is not necessarily required to use a reaction solvent in the present embodiment, a
5 suitable solvent is preferably used as a reaction solvent for the purpose of facilitating the reaction procedure, examples of which may include alkanes such as hexane (including isomers), heptane (including isomers), octane (including isomers), nonane (including isomers) or decane (including isomers); aromatic hydrocarbons and alkyl-substituted aromatic hydrocarbons such as benzene, toluene, xylene (including
10 isomers), ethyl benzene, diisopropyl benzene (including isomers), dibutyl benzene (including isomers) or naphthalene; alcohols such as methanol, ethanol, propanol (including isomers), butanol (including isomers), pentanol (including isomers), hexanol (including isomers), heptanol (including isomers), octanol (including isomers) or nonanol (including isomers); aromatic compounds substituted with a halogen or
15 nitro group such as chlorobenzene, dichlorobenzene (including isomers), bromobenzene, dibromobenzene (including isomers), chloronaphthalene, bromonaphthalene, nitrobenzene or nitronaphthalene; polycyclic hydrocarbon compounds such as diphenyl, substituted diphenyl, diphenyl methane, terphenyl, anthracene or dibenzyl toluene (including isomers); aromatic hydroxy compounds
20 such as phenol, methylphenol (including isomers), ethylphenol (including isomers), butylphenol (including isomers), pentylphenol (including isomers), dimethylphenol (including isomers), diethylphenol (including isomers), dibutylphenol (including isomers) or dipentylphenol (including isomers); aliphatic hydrocarbons such as cyclohexane, cyclopentane, cyclooctane or ethylcyclohexane; alicyclic alcohols such
25 as cyclohexanol, cyclopentanol or cyclooctanol; ketones such as methyl ethyl ketone or acetophenone; esters such as dibutyl phthalate, dihexyl phthalate, dioctyl

phthalate or benzylbutyl phthalate; ethers and thioethers such as diphenyl ether or diphenyl sulfide; and sulfoxides such as dimethylsulfoxide or diphenylsulfoxide. These solvents can be used alone or two or more types can be used as a mixture. In addition, carbonic acid ester used in excess with respect to amino groups of the amine compound is also preferably used as a solvent in the reaction.

[0099]

There are no particular limitations on the reaction apparatus used when carrying out this reaction, and a known reaction vessel can be used. For example, conventionally known reaction vessels can be suitably combined, such as a stirring tank, a pressurized stirring tank, a depressurized stirring tank, a column type reaction vessel, a distillation column, a packed column or a thin film distiller. There are no particular limitations on the material of the reaction vessel, and known materials can be used, examples of which may include glass, stainless steel, carbon steel, Hastelloy, glass-lined base materials and Teflon (registered trademark) coated materials.

[0100]

<Removal of Hydroxy Compound>

The reaction liquid containing carbamic acid ester produced by reacting with carbonic acid ester and amine compound as indicated above may be supplied directly to the reaction vessel in which thermal decomposition of carbamic acid ester is carried out (hereinafter referred to as "thermal decomposition reaction vessel"), or may be supplied to the thermal decomposition reaction vessel after having purified the carbamic acid ester from the reaction liquid. However, since isocyanate formed by thermal decomposition of the carbamic acid ester forms carbamic acid ester by reacting with a hydroxy compound (alcohol and / or aromatic hydroxy compound), in order to increase the reaction efficiency of the thermal decomposition reaction, it is

preferable to remove the hydroxy compound (alcohol and / or aromatic hydroxy compound) from the reaction liquid in advance prior to carrying out the thermal decomposition reaction.

[0101]

5 In the present embodiment, carbamic acid ester can be purified and supplied to the thermal decomposition reaction vessel by a known method such as a method in which a low boiling point component such as the reaction solvent is distilled from the reaction liquid by distillation in the case of using a hydroxy compound and / or carbonic acid ester and / or reaction solvent, a method in which the carbamic acid
10 ester is cleaned by a solvent that is inert and has low solubility in carbamic acid ester, or a method involving purification by crystallization. Among these methods, a method in which a low boiling point component such as the reaction solvent is distilled off by distillation in the case of using a hydroxy compound and / or carbonic acid ester and / or reaction solvent is preferably carried out in consideration of the
15 ease of the procedure and so forth.

[0102]

A known distillation apparatus can be used for the apparatus for separating the hydroxy compound and carbonic acid ester from the reaction liquid by distillation. For example, methods using an apparatus such as a distillation column, a multistage
20 distillation column, a multitubular reactor, a continuous multistage distillation column, a packed column, a thin film evaporator, a falling film evaporator or a falling drop evaporator, and methods using a combination thereof are used. Although varying according to the types of compounds contained in the reaction liquid, the conditions under which the distillative separation is carried out are such that the temperature is
25 preferably within a range of from normal temperature (e.g., 20°C) to 180°C, and since there are cases in which undesirable reactions occur at high temperatures, the

temperature is preferably within a range of from 50 to 150°C. A known cooling apparatus or a heating apparatus may be installed in the reaction vessel to maintain a constant temperature. In addition, although varying according to the types of compounds contained in the reaction liquid and the temperature, the pressure may be decreased pressure, normal pressure or increased pressure, and distillative separation is normally carried out within a range of from 20 to 1×10^6 Pa. In the case of carrying out the procedure for a long period of time at high temperatures, particularly in the case of distillative separation, since carbamic acid ester contained in the reaction liquid may undergo thermal denaturation resulting in a decrease in the yield of the carbamic acid ester, distillative separation is carried out under a reduced pressure at a pressure that is as close as possible to the degree of depressurization able to be achieved by the distillation apparatus, and a temperature is preferably selected that is within an adequate temperature range for distilling off the compound desired to be removed from the reaction liquid in the gaseous phase, and is as low as possible within the temperature range that allows the carbamic acid ester, or a mixture containing the carbamic acid ester following distillative separation, to be present as a liquid. Although the primary objective of distillative separation is to separate hydroxy compound (alcohol and / or aromatic hydroxy compound) from the reaction liquid, in the case of using carbonic acid ester and reaction solvent contained in the reaction liquid, it is preferable to also separate the reaction solvent. If the subsequently described thermal decomposition reaction is carried out while carbonic acid ester and / or reaction solvent are still contained in the reaction liquid, a step is required for separating the formed isocyanate or hydroxy compound, thereby resulting in a complex procedure.

[0103]

The hydroxy compound and / or carbonic acid ester separated and recovered in

the reaction, and a solvent in the case the reaction liquid contains a solvent, are each preferably reused. The hydroxy compound is reused as a hydroxy compound (alcohol and / or aromatic hydroxy compound) in the carbonic acid ester production step, the carbonic acid ester is reused as carbonic acid ester in the production of carbamic acid ester, and the solvent is reused as solvent in the production of carbamic acid ester.

[0104]

In the case a catalyst is used in the production of carbamic acid ester and a catalyst or catalyst residue is contained in the reaction liquid, the catalyst contained in the reaction liquid or carbamic acid ester can be used directly as a catalyst for the thermal decomposition reaction, or the catalyst may be removed from the reaction liquid or carbamic acid ester. In the case of using a basic catalyst in particular, since reactions attributable to the catalyst may occur during the thermal decomposition reaction causing a decrease in yield, it is preferable in such cases to carry out the thermal decomposition reaction after first removing the catalyst. Known methods can be used to remove the catalyst. An example of a preferable method for removing the catalyst may involve neutralization by treating with an organic acid or inorganic acid in a homogeneous phase or heterogeneous phase. A mono- or dicarboxylic acid, alkyl or aryl sulfonate or phosphate, ion exchange resin or activated charcoal and the like are used to remove the catalyst. The catalyst is removed within a range of from normal temperature (e.g., 20°C) to 180°C since carbamic acid ester may solidify at low temperatures, while thermal denaturation may occur at high temperatures. Preferably, removal of catalyst is carried out in continuation after having carried out the step for producing carbamic acid ester while maintaining the temperature at a temperature at which the formed carbamic acid ester does not precipitate from the reaction liquid of the carbamic acid ester

production step. In the case of separating solvent and / or hydroxy compound and / or carbonic acid ester from the reaction liquid of the carbamic acid ester production step, the previously described separation procedure is preferably carried out after having removed the catalyst from the reaction liquid.

5 [0105]

<Transfer of Carbamic Acid Ester>

The reactant containing carbamic acid ester produced according to the reaction between carbonic acid ester and amine compound (hereinafter referred to as "reactant"), or a mixture containing carbamic acid ester in which hydroxy compound
10 has been removed from the reaction liquid according to the method described above (hereinafter referred to as "residue liquid"), is supplied to a thermal decomposition reaction vessel.

Since carbamic acid esters easily form hydrogen bonds between molecules by ester groups constituting the carbamic acid ester, they frequently have a high melting
15 point. In the transfer of carbamic acid esters having a high melting point, the carbamic acid ester is transferred after having converted to a vehicle by, for example, crushing or forming into pellets, or the carbamic acid ester is heated to a temperature higher than the melting point thereof and transferred in a liquid state. However, in the case of transferring solid carbamic acid ester that has been converted to a
20 vehicle, there is a frequently the need for a complex apparatus to ensure stable transfer of a fixed amount of carbamic acid ester, or the need for a process for maintaining the form of the carbamic acid ester within a certain range in cases of the risk of clogging of the transfer line or frequent fluctuations in the form of the carbamic acid ester. Thus, the reactant or the residue liquid is preferably supplied to the
25 thermal decomposition reaction vessel in liquid form.

[0106]

In the case of transferring the reactant or the residue liquid in the liquid form, although it is preferable to heat to a high temperature in consideration of preventing solidification during transfer, if transferred at an excessively high temperature, since there are many case in which the carbamic acid ester contained in the reactant or the residue liquid undergoes thermal denaturation, the reactant or the residue liquid is preferably transferred within a temperature range of from 30 to 200°C, more preferably from 50 to 180°C and even more preferably from 80 to 150°C.

[0107]

<Carbamic Acid Ester Thermal Decomposition Reaction>

Next, an explanation is provided of the production of isocyanate by carrying out a thermal decomposition reaction on the carbamic acid ester.

The thermal decomposition reaction in the present embodiment is a reaction in which the corresponding isocyanate and hydroxy compound (alcohol or aromatic hydroxy compound) are formed from the carbamic acid ester.

[0108]

The reaction temperature is generally within a range of from 100 to 350°C, and although a high temperature is preferable for increasing the reaction rate, since side reactions as described above may be conversely caused by the carbamic acid ester and / or the reaction product in the form of the isocyanate at high temperatures, the reaction temperature is preferably within a range of from 150 to 300°C. A known cooling apparatus or a heating apparatus may be installed in the reaction vessel to maintain a constant reaction temperature. In addition, although varying according to the types of compounds used and reaction temperature, the reaction pressure may be decreased pressure, normal pressure or increased pressure, and the reaction is generally carried out at a pressure within a range of from 20 to 1×10^6 Pa. There are no particular limitations on the reaction time (residence time in the case of a

continuous method) and is generally from 0.001 to 100 hours, preferably from 0.005 to 50 hours and more preferably from 0.01 to 10 hours.

[0109]

There are cases in which side reactions as described above may occur in cases of holding the carbamic acid ester at high temperatures for an extended period of time. In addition, isocyanates formed by the thermal decomposition reaction may also cause such side reactions. Thus, the time during which the carbamic acid ester and the isocyanate are held at a high temperature is preferably as short as possible, and the thermal decomposition reaction is preferably carried out by a continuous process. A continuous process refers to a process in which a mixture containing the carbamic acid ester is continuously supplied to a reaction vessel and subjected to the thermal decomposition reaction followed by continuously extracting the isocyanate and hydroxy compound formed from the thermal decomposition reaction vessel. In this continuous process, a low boiling point component formed by thermal decomposition of the carbamic acid ester is preferably recovered from the upper portion of the thermal decomposition reaction vessel in the form of a gaseous phase component, while the remainder is recovered from the bottom of the thermal decomposition reaction vessel in the form of a liquid phase component. Although all compounds present in the thermal decomposition reaction vessel can be recovered in the form of gaseous phase components, by allowing liquid phase components to remain in the thermal decomposition reaction vessel, polymeric compounds formed by side reactions caused by the carbamic acid ester and / or isocyanate are dissolved, thereby demonstrating the effect of preventing the polymeric compounds from adhering to and accumulating in the thermal decomposition reaction vessel. Although isocyanate and hydroxy compound are formed by thermal decomposition of carbamic acid ester, at least one of these compounds is recovered in the form of a

gaseous phase component. Which of these compounds is recovered in the form of a gaseous phase component depends on the conditions of the thermal decomposition reaction.

[0110]

5 Here, although the term "low boiling point component formed by thermal decomposition of carbamic acid ester" used in the present embodiment corresponds to the hydroxy compound and / or isocyanate formed by thermal decomposition of the carbamic acid ester, it particularly refers to compounds able to exist as a gas under the conditions under which the thermal decomposition reaction is carried out.

10 [0111]

A method can be employed by which the isocyanate and hydroxy compound formed by the thermal decomposition reaction are recovered in the form of a gaseous phase component, while a liquid phase component is recovered containing the carbamic acid ester and / or carbonic acid ester. In this method, the isocyanate and
15 hydroxy compound may be recovered separately in the thermal decomposition reaction vessel. The recovered gaseous phase component containing isocyanate is preferably supplied in the gaseous phase to a distillation apparatus for separation and purification of the isocyanate. On the other hand, the liquid phase component containing the carbamic acid ester and / or carbonic acid ester is recovered from the
20 bottom of the thermal decomposition reaction vessel, all or a portion of the liquid phase component is supplied to the upper portion of the thermal decomposition reaction vessel, and the carbamic acid ester is again subjected to the thermal decomposition reaction. The upper portion of the thermal decomposition reaction vessel as referred to here refers to, for example, to the second plate and beyond
25 from the bottom in terms of the number of theoretical plates in the case the thermal decomposition reaction vessel is a distillation column, or refers to the portion higher

than the heated conductive surface in the case the thermal decomposition reaction vessel is a thin film distiller. When supplying all or a portion of the liquid phase component to the thermal decomposition reaction vessel, the liquid phase component is preferably transferred while holding at a temperature of from 50 to 180°C, more preferably from 70 to 170°C and even more preferably from 100 to 150°C. In the case the liquid phase component contains carbonic acid ester, the liquid phase component may be supplied to the thermal decomposition reaction vessel after having separated and recovered the carbonic acid ester from the liquid phase component. The separated and recovered carbonic acid ester is preferably reused.

[0112]

Although previously mentioned, in the thermal decomposition reaction, the liquid phase component is preferably recovered from the bottom of the thermal decomposition reaction vessel. This is because, as a result of having the liquid phase component present in the thermal decomposition reaction vessel, polymeric by-products formed by side reactions caused by carbamic acid ester and / or isocyanate are dissolved and are able to be discharged from the thermal decomposition reaction vessel in the form of a liquid phase component, thereby having the effect of reducing adhesion and accumulation of these polymeric compounds in the thermal decomposition reaction vessel.

[0113]

Although all or a portion of the liquid phase component is supplied to the upper portion of the thermal decomposition reaction vessel and the carbamic acid ester is re-subjected to the thermal decomposition reaction, there are cases in which polymeric by-products accumulate in the liquid phase component if this step is repeated. In such cases, all or a portion of the liquid phase component can be

removed from the reaction system to reduce the accumulation of polymeric by-products or maintain at a constant concentration.

[0114]

The hydroxy compound and / or carbonic acid ester contained in the gaseous phase component and / or liquid phase component obtained in the thermal decomposition reaction as described above can each be separated and recovered for reuse. More specifically, the hydroxy compound can be reused as the hydroxy compound of step (3) for production of carbonic acid ester, and the carbonic acid ester can be reused as a raw material for the production of carbamic acid ester.

10 [0115]

Although there are no particular limitations on the type of thermal decomposition reaction vessel, a known distillation apparatus is used preferably to efficiently recover the gaseous phase component. Various known methods are used, examples of which may include a distillation column, a multistage distillation column, a multitubular reactor, a continuous multistage distillation column, a packed column, a thin film evaporator, a reactor provided with a support inside, a forced circulation reactor, a falling film evaporator, a falling drop evaporator and types using combinations thereof. From the viewpoint of rapidly removing low boiling point components from the reaction system, a tubular reactor is preferable, while a reaction vessel such as a tubular thin film evaporator, a tubular falling film evaporator is used more preferably, and structures having a large gas-liquid contact area are preferable for being able to rapidly transfer low boiling point components formed to the gaseous phase.

[0116]

25 Although known materials may be used for the thermal decomposition reaction vessel and lines provided they do not have a detrimental effect on the carbamic acid

ester or products in the form of the hydroxy compound, isocyanate and the like, SUS304, SUS316 or SUS316L and the like can be used preferably since they are inexpensive.

[0117]

5 <Cleaning the Thermal Decomposition Reaction Vessel>

In the present embodiment, although polymeric by-products originating from side reactions as represented by the previously indicated formulas (2), (3) and (4) are formed accompanying thermal decomposition of carbamic acid ester, there are cases in which these thermal decomposition reaction by-products may adhere to the thermal decomposition reaction vessel when operating for an extended period of time even in case of carrying out the thermal decomposition reaction according to the method described above. If these compounds adhering to the thermal decomposition reaction vessel accumulate to a certain degree, operation of the thermal decomposition reaction vessel becomes impaired, and since there are frequently cases in which this makes long-term operation difficult, it was necessary to perform work consisting of disassembling and cleaning the thermal decomposition reaction vessel.

[0118]

The inventors of the present invention unexpectedly found that compounds adhered to the thermal decomposition reaction vessel easily dissolve in acids. On the basis of these findings, in the case high boiling point substances have become adhered to the thermal decomposition reaction vessel, the inventors of the present invention conceived and perfected a method for keeping the inside of the thermal decomposition reaction vessel (and particularly the walls thereof) clean by cleaning the walls of the thermal decomposition reaction vessel with the acids to dissolve these high boiling point substances and remove them from the thermal

decomposition reaction vessel. Since this method enables the walls of the thermal decomposition reaction vessel to be cleaned without having to disassemble and separately clean the thermal decomposition reaction vessel, the down time of the thermal decomposition reaction vessel can be shortened considerably, thereby
5 resulting in high isocyanate production efficiency.

[0119]

There are no particular limitations on the acids used for cleaning provided it is able to dissolve the polymeric by-products, and organic acids or inorganic acids may be used, although organic acids are used preferably. Although examples of organic
10 acids used may include carbonic acid, sulfonic acid, sulfinic acid, phenols, enols, thiophenols, imides, oximes and aromatic sulfonamides, carbonic acid and phenols are used preferably. Examples of such compounds may include saturated or unsaturated aliphatic monocarboxylic acid compounds such as formic acid, acetic acid, propionic acid, n-butyric acid, isobutyric acid, valeric acid, isovaleric acid,
15 2-methylbutanoic acid, pivalic acid, hexanoic acid, isocaproic acid, 2-ethylbutanoic acid, 2,2-dimethylbutanoic acid, heptanoic acid (including isomers), octanoic acid (including isomers), nonanoic acid (including isomers), decanoic acid (including isomers), undecanoic acid (including isomers), dodecanoic acid (including isomers), tetradecanoic acid (including isomers), hexadecanoic acid (including isomers), acrylic
20 acid, crotonic acid, isocrotonic acid, vinyl acetate, methacrylic acid, angelic acid, tiglic acid, allyl acetate or undecenoic acid (including isomers); saturated or unsaturated aliphatic dicarboxylic acids such as oxalic acid, malonic acid, succinic acid, glutaric acid, adipic acid, heptanedioic acid (including isomers), octanedioic acid (including isomers), nonanedioic acid (including isomers), decanedioic acid (including isomers),
25 maleic acid, fumaric acid, methylmaleic acid, methylfumaric acid, pentenedioic acid (including isomers), itaconic acid or allylmalonic acid; saturated or unsaturated

aliphatic tricarboxylic acid compounds such as 1,2,3-propanetricarboxylic acid, 1,2,3-propenetricarboxylic acid or 2,3-dimethylbutane-1,2,3-tricarboxylic acid; aromatic monocarboxylic acid compounds such as benzoic acid, methylbenzoic acid (including isomers), ethylbenzoic acid (including isomers), propylbenzoic acid (including isomers), dimethylbenzoic acid (including isomers) or trimethylbenzoic acid (including isomers); aromatic dicarboxylic acid compounds such as phthalic acid, isophthalic acid, terephthalic acid or methylisophthalic acid (including isomers); aromatic tricarboxylic acid compounds such as hemimellitic acid, trimellitic acid or trimesinic acid; mono-substituted phenols such as phenol, methylphenol (including isomers), ethylphenol (including isomers), propylphenol (including isomers), butylphenol (including isomers), pentylphenol (including isomers), hexylphenol (including isomers), heptylphenol (including isomers), octylphenol (including isomers), nonylphenol (including isomers), decylphenol (including isomers), dodecylphenol (including isomers), phenylphenol (including isomers), phenoxyphenol (including isomers) or cumylphenol (including isomers); di-substituted phenols such as dimethylphenol (including isomers), diethylphenol (including isomers), dipropylphenol (including isomers), dibutylphenol (including isomers), dipentylphenol (including isomers), dihexylphenol (including isomers), diheptylphenol (including isomers), dioctylphenol (including isomers), dinonylphenol (including isomers), didodecylphenol (including isomers), diphenylphenol (including isomers), diphenoxyphenol (including isomers), dicumylphenol (including isomers), methylethylphenol (including isomers), methylpropylphenol (including isomers), methylbutylphenol (including isomers), methylpentylphenol (including isomers), methylhexylphenol (including isomers), methylheptylphenol (including isomers), methyloctylphenol (including isomers), methylnonylphenol (including isomers), methyldecylphenol (including isomers), methyl dodecylphenol (including isomers),

methylphenylphenol (including isomers), methylphenoxyphenol (including isomers),
 methylcumylphenol (including isomers), ethylpropylphenol (including isomers),
 ethylbutylphenol (including isomers), ethylpentylphenol (including isomers),
 ethylhexylphenol (including isomers), ethylheptylphenol (including isomers),
 5 ethyloctylphenol (including isomers), ethylnonylphenol (including isomers),
 ethyldecylphenol (including isomers), ethyldodecylphenol (including isomers),
 ethylphenylphenol (including isomers), ethylphenoxyphenol (including isomers),
 ethylcumylphenol (including isomers), propylbutylphenol (including isomers),
 propylpentylphenol (including isomers), propylhexylphenol (including isomers),
 10 propylheptylphenol (including isomers), propyloctylphenol (including isomers),
 propylnonylphenol (including isomers), propyldecylphenol (including isomers),
 propyldodecylphenol (including isomers), propylphenylphenol (including isomers),
 propylphenoxyphenol (including isomers), propylcumylphenol (including isomers),
 butylpentylphenol (including isomers), butylhexylphenol (including isomers),
 15 butylheptylphenol (including isomers), butyloctylphenol (including isomers),
 butylnonylphenol (including isomers), butyldecylphenol (including isomers),
 butyldodecylphenol (including isomers), butylphenylphenol (including isomers),
 butylphenoxyphenol (including isomers), butylcumylphenol (including isomers),
 pentylhexylphenol (including isomers), pentylheptylphenol (including isomers),
 20 pentyloctylphenol (including isomers), pentylnonylphenol (including isomers),
 pentyldecylphenol (including isomers), pentyldodecylphenol (including isomers),
 pentylphenylphenol (including isomers), pentylphenoxyphenol (including isomers),
 pentylcumylphenol (including isomers), hexylheptylphenol (including isomers),
 hexyloctylphenol (including isomers), hexylnonylphenol (including isomers),
 25 hexyldecylphenol (including isomers), hexyldodecylphenol (including isomers),
 hexylphenylphenol (including isomers), hexylphenoxyphenol (including isomers),

hexylcumylphenol (including isomers), heptyloctylphenol (including isomers),
 heptylnonylphenol (including isomers), heptyldecylphenol (including isomers),
 heptyldodecylphenol (including isomers), heptylphenylphenol (including isomers),
 heptylphenoxyphenol (including isomers), heptylcumylphenol (including isomers),
 5 octylnonylphenol (including isomers), octyldecylphenol (including isomers),
 octyldodecylphenol (including isomers), octylphenylphenol (including isomers),
 octylphenoxyphenol (including isomers), octylcumylphenol (including isomers),
 nonyldecylphenol (including isomers), nonyldodecylphenol (including isomers),
 nonylphenylphenol (including isomers), nonylphenoxyphenol (including isomers),
 10 nonylcumylphenol (including isomers), dodecylphenylphenol (including isomers),
 dodecylphenoxyphenol (including isomers) or dodecylcumylphenol (including
 isomers); and, tri-substituted phenols such as trimethylphenol (including isomers),
 triethylphenol (including isomers), tripropylphenol (including isomers), tributylphenol
 (including isomers), tripentylphenol (including isomers), trihexylphenol (including
 15 isomers), triheptylphenol (including isomers), trioctylphenol (including isomers),
 trinonylphenol (including isomers), tridecylphenol (including isomers),
 tridodecylphenol (including isomers), triphenylphenol (including isomers),
 triphenoxyphenol (including isomers), tricumylphenol (including isomers),
 dimethylethylphenol (including isomers), dimethylpropylphenol (including isomers),
 20 dimethylbutylphenol (including isomers), dimethylpentylphenol (including isomers),
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 isomers), diethylphenylphenol (including
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 (including isomers), dipentyloctylphenol (including isomers), dipentylnonylphenol
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 (including isomers), dipentylphenylphenol (including isomers), dipentylphenoxyphenol
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 25 diphenoxynonylphenol (including isomers), diphenoxydecylphenol (including isomers),
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 5 methylpentylododecylphenol (including isomers), methylpentylphenylphenol (including
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 20 isomers), ethylbutylheptylphenol (including isomers), ethylbutylloctylphenol (including
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 isomers), ethylbutylododecylphenol (including isomers), ethylbutylphenylphenol
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 25 isomers), ethylpentylheptylphenol (including isomers), ethylpentylloctylphenol
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5 ethylhexylnonylphenol (including isomers), ethylhexyldecylphenol (including isomers), ethylhexyldodecylphenol (including isomers), ethylhexylphenylphenol (including isomers), ethylhexylphenoxyphenol (including isomers), ethylhexylcumylphenol (including isomers), ethylheptyloctylphenol (including isomers), ethylheptylnonylphenol (including isomers), ethylheptyldecylphenol (including isomers),
10 ethylheptyldodecylphenol (including isomers), ethylheptylphenylphenol (including isomers), ethylheptylphenoxyphenol (including isomers), ethylheptylcumylphenol (including isomers), ethyloctylphenol (including isomers), ethyloctylnonylphenol (including isomers), ethyloctyldecylphenol (including isomers), ethyloctyldodecylphenol (including isomers), ethyloctylphenylphenol (including isomers),
15 ethyloctylphenoxyphenol (including isomers), ethyloctylcumylphenol (including isomers), ethylnonyldecylphenol (including isomers), ethylnonyldodecylphenol (including isomers), ethylnonylphenylphenol (including isomers), ethylnonylphenoxyphenol (including isomers), ethylnonylcumylphenol (including isomers), ethyldecyldodecylphenol (including isomers),
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25 isomers), propylbutylpentylphenol (including isomers), propylbutylhexylphenol (including isomers), propylbutylheptylphenol (including isomers),

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nonyldecylphenylphenol (including isomers), nonyldecylphenoxyphenol (including isomers), nonyldecylcumylphenol (including isomers), nonyldodecylphenylphenol (including isomers), nonyldodecylphenoxyphenol (including isomers), nonyldodecylcumylphenol (including isomers), nonylphenylphenoxyphenol (including isomers), nonylphenylcumylphenol (including isomers), decyldodecylphenylphenol (including isomers), decyldodecylphenoxyphenol (including isomers), decyldodecylcumylphenol (including isomers), decylphenylphenoxyphenol (including isomers), decylphenylcumylphenol (including isomers), dodecylphenylphenoxyphenol (including isomers), dodecylphenylcumylphenol (including isomers) or phenylphenoxy cumylphenol (including isomers). Among these organic acids, in consideration of separation of isocyanate formed in the thermal decomposition reaction in the case of organic acid remaining in the thermal decomposition reaction vessel, an organic acid is preferably selected for which the difference between the boiling point thereof and the standard boiling point of the isocyanate is 10°C or more.

[0120]

Various methods can be used to clean the thermal decomposition reaction vessel using the above cleaning solvent, examples of which may include cleaning the thermal decomposition reaction vessel by introducing the cleaning solvent from the upper portion of the thermal decomposition reaction vessel, and cleaning the inside of the thermal decomposition reaction vessel by introducing the cleaning solvent from the bottom of the thermal decomposition reaction vessel and boiling it inside the thermal decomposition reaction vessel.

It is not necessary to carry out the cleaning procedure each time the thermal decomposition reaction is carried out, but rather the cleaning frequency can be arbitrarily determined according to the compounds used, operating rate and so forth, and the cleaning procedure is preferably carried out once every 1 to 20000 hours of

operation, more preferably once per one day to one year of operating time, and even more preferably once per one month to one year of operating time. The thermal decomposition reaction vessel may be provided with a line for introducing the cleaning solvent.

5 [0121]

In addition, when carrying out thermal decomposition of carbamic acid ester for the purpose of cleaning the thermal decomposition reaction vessel, the cleaning solvent can also be present in the conditions of the thermal decomposition reaction. This differs from the inert solvent as referred to in the prior art (see, for example, U.S. Patent No. 4081472). For example, according to this patent document, although an inert solvent refers to a compound that does not react with isocyanate formed by thermal decomposition of carbamic acid ester, in contrast thereto, as stated in the literature (Journal of the American Chemical Society, Vol. 64, p. 2229, 1942), for example, that urethane is formed by a reaction between an aromatic hydroxy compound and phenyl isocyanate, aromatic hydroxy compounds are able to react with isocyanates. The aromatic hydroxy compound may be supplied to the thermal decomposition reaction vessel after mixing with a reaction mixture or a distillation residue when transferring the reaction mixture obtained by reaction of carbonic acid ester and amine compound, or the distillation residue in which hydroxy compound and/or carbonic acid ester and / or reaction solvent has been separated from the reaction mixture, to the thermal decomposition reaction vessel, or the aromatic hydroxy compound may be supplied by providing a line for supplying the aromatic hydroxy compound separate from the line for supplying the reaction mixture.

[0122]

25 Isocyanates obtained by the production process of the present embodiment can be preferably used as production raw materials of polyurethane foam, paints,

adhesives and the like. In addition, since isocyanates can be produced according to the production process of the present embodiment in good yield without using toxic phosgene, the present invention is industrially extremely important.

5 EXAMPLES

[0123]

Although the following provides a detailed explanation of the present invention based on examples thereof, the scope of the present invention is not limited by these examples.

10 <Analytical Methods>

1) NMR Analysis

Apparatus: JNM-A400 FT-NMR system, JEOL Ltd., Japan

(1) Preparation of ^1H - and ^{13}C -NMR Analysis Samples

About 0.3 g of sample solution were weighed followed by the addition of about
15 0.7 g of heavy chloroform (99.8%, Aldrich Corp., USA) and about 0.05 g of internal standard in the form of tetramethyl tin (guaranteed reagent, Wako Pure Chemical Industries, Ltd., Japan) and mixing to uniformity to obtain solutions used as NMR analysis samples.

(2) Quantitative Analysis

20 Analyses were performed for each standard and quantitative analyses were performed on the analysis sample solutions based on the resulting calibration curve.

[0124]

2) Liquid Chromatography

Apparatus: LC-10AT system, Shimadzu Corp., Japan

25 Column: Silica-60 column, Tosoh Corp., Japan, two columns connected in series

Developing solvent: Mixed liquid of hexane/tetrahydrofuran (80/20) (v/v)

Solvent flow rate: 2 mL/min

Column temperature: 35°C

Detector: R.I. (refractometer)

5 (1) Liquid Chromatography Analysis Samples

About 0.1 g of sample were weighed followed by the addition of about 1 g of tetrahydrofuran (dehydrated, Wako Pure Chemical Industries, Ltd., Japan) and about 0.02 g of internal standard in the form of bisphenol A (guaranteed reagent, Wako Pure Chemical Industries, Ltd., Japan) and mixing to uniformity to obtain solutions

10 used as liquid chromatography analysis samples.

(2) Quantitative Analysis

Analyses were performed for each standard and quantitative analyses were performed on the analysis sample solutions based on the resulting calibration curve.

[0125]

15 3) Gas Chromatography

Apparatus: GC-2010, Shimadzu Corp., Japan

Column: DB-1 column, Agilent Technologies Corp., USA, length: 30 m, inner diameter: 0.250 mm, film thickness: 1.00 µm

20 Column temperature: Held at 50°C for 5 minutes followed by increasing at the rate of 10°C/min to 200°C; held at 200°C for 5 minutes followed by increasing at the rate of 10°C/min to 300°C

Detector: FID

(1) Gas Chromatography Analysis Samples

25 About 0.05 g of sample were weighed followed by the addition of about 1 g of acetone (dehydrated, Wako Pure Chemical Industries, Ltd., Japan) and about 0.02 g of internal standard in the form of toluene (dehydrated, Wako Pure Chemical

Industries, Ltd., Japan) and mixing to uniformity to obtain solutions used as gas chromatography analysis samples.

(2) Quantitative Analysis

Analyses were performed for each standard and quantitative analyses were performed on the analysis sample solutions based on the resulting calibration curve.

[0126]

4) Inductively Coupled Plasma Mass Spectrometry

Apparatus: SPQ-8000, Seiko Epson Corp., Japan

(1) Inductively Coupled Plasma Mass Spectrometry Analysis Samples

About 0.15 g of sample were ashed with dilute sulfuric acid followed by dissolving in dilute nitric acid.

(2) Quantitative Analysis

Analyses were performed for each standard and quantitative analyses were performed on the analysis sample solutions based on the resulting calibration curve.

[0127]

[Reference Example 1] Production of Bis(3-methylbutyl) Carbonate

Step (I-1): Production of Dialkyl Tin Catalyst

625 g (2.7 mol) of di-n-butyl tin oxide (Sankyo Organic Chemicals Co., Ltd., Japan) and 2020 g (22.7 mol) of 3-methyl-1-butanol (Wako Pure Chemical Industries, Ltd., Japan) were placed in a 5000 mL volumetric pear-shaped flask. The flask was connected to an evaporator (R-144, Shibata Co., Ltd., Japan) to which was connected an oil bath (OBH-24, Masuda Corp., Japan) equipped with a temperature controller, a vacuum pump (G-50A, Ulvac Inc., Japan) and a vacuum controller (VC-10S, Okano Seisakusho Co., Ltd.). The purge valve outlet of this evaporator was connected to a line containing nitrogen gas flowing at a normal pressure. After closing the purge valve of the evaporator to a reduce pressure inside the system, the

purge valve was opened gradually to allow nitrogen to flow into the system and return to the normal pressure. The oil bath temperature was set to be about 145°C, the flask was immersed in the oil bath and rotation of the evaporator was started. After heating for about 40 minutes in the presence of atmospheric pressure nitrogen with
5 the purge valve of the evaporator left open, distillation of 3-methyl-1-butanol containing water began. After maintaining in this state for 7 hours, the purge valve was closed, pressure inside the system was gradually reduced, and excess 3-methyl-1-butanol was distilled with the pressure inside the system at from 74 to 35 kPa. After the fraction no longer appeared, the flask was taken out of the oil bath.
10 After allowing the flask to cool to the vicinity of room temperature (25°C), the flask was taken out of the oil bath, the purge valve was opened gradually and the pressure inside the system was returned to atmospheric pressure. 886 g of reaction liquid were obtained in the flask. Based on the results of ^{119}Sn -, ^1H - and ^{13}C -NMR analyses, 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane was confirmed
15 to have been obtained at a yield of 99% based on di-n-butyl tin oxide. The same procedure was then repeated 12 times to obtain a total of 10635 g of 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane.

[0128]

Step (I-2): Production of Bis(3-methylbutyl) Carbonate

20 Bis(3-methylbutyl) carbonate was produced in a continuous production apparatus like that shown in FIG. 1. 1,1,3,3-Tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane produced in the manner described above was supplied at the rate of 4388 g/hr from a line 4 into column-type reaction vessel 102 packed with Metal Gauze CY Packing (Sulzer Chemtech Ltd., Switzerland) and having an inner
25 diameter of 151 mm and effective length of 5040 mm, and 3-methyl-1-butanol purified with continuous multistage distillation column 101 was supplied at the rate of 14953

g/hr from line 2. The liquid temperature inside reaction vessel 102 was controlled to 160°C by a heater and reboiler 112, and the pressure was adjusted to be about 120 kPa-G with a pressure control valve. The residence time in the reaction vessel was about 17 minutes. 3-methyl-1-butanol containing water at the rate of 15037 g/hr from a top of the reaction vessel via line 6, and 3-methyl-1-butanol at the rate of 825 g/hr via line 1, were pumped to distillation column 101 packed with Metal Gauze CY Packing and provided with reboiler 111 and condenser 121 to carry out distillative purification. In the top of distillation column 101, a fraction containing a high concentration of water was condensed by condenser 121 and recovered from line 3. Purified 3-methyl-1-butanol was pumped to column-type reaction vessel 102 via line 2 located in the lower portion of distillation column 101. An alkyl tin alkoxide catalyst composition containing di-n-butyl-bis(3-methylbutyloxy) tin and 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane was obtained from the lower portion of column-type reaction vessel 102, and supplied to thin film evaporator 103 (Kobelco Eco-Solutions Co., Ltd., Japan) via line 5. The 3-methyl-1-butanol was distilled off in thin film evaporator 103 and returned to column-type reaction vessel 102 via condenser 123, line 8 and line 4. The alkyl tin alkoxide catalyst composition was pumped from the lower portion of thin film evaporator 103 via line 7 and supplied to autoclave 104 while adjusting the flow rate of di-n-butyl-bis(3-methylbutyloxy) tin and 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane to about 5130 g/hr. Carbon dioxide was supplied to autoclave 104 by line 9 at the rate of 973 g/hr, and the pressure inside autoclave 104 was maintained at 4 MPa-G. The temperature inside autoclave 104 was set to be 120°C, the residence time was adjusted to about 4 hours, and a reaction between the carbon dioxide and the alkyl tin alkoxide catalyst composition was carried out to obtain a reaction liquid containing bis(3-methylbutyl) carbonate.

This reaction liquid was transferred to a decarbonization tank 105 via line 10 and a control valve to remove residual carbon dioxide, and the carbon dioxide was recovered from line 11. Subsequently, the reaction liquid was transferred to thin film evaporator 106 (Kobelco Eco-Solutions Co., Ltd., Japan) set to be about 142°C and about 0.5 kPa via line 12, and supplied while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane to about 4388 g/hr to obtain a fraction containing bis(3-methylbutyl) carbonate. On the other hand, the evaporation residue was circulated to column-type reaction vessel 102 via line 13 and line 4 while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane to about 4388 g/hr. The fraction containing bis(3-methylbutyl) carbonate was supplied to a distillation column 107 packed with Metal Gauze CY packing and equipped with reboiler 117 and condenser 127 via condenser 126 and transfer line 14 at the rate of 959 g/hr followed by distillative purification to obtain 99 wt% bis(3-methylbutyl) carbonate from recovery line 15 at the rate of 944 g/hr. When the alkyl tin alkoxide catalyst composition of transfer line 13 was analyzed by ^{119}Sn -, ^1H - and ^{13}C -NMR analysis, it was found to contain 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane but not contain di-n-butyl-bis(3-methylbutyloxy) tin. After carrying out the above-mentioned continuous operation for about 240 hours, alkyl tin alkoxide catalyst composition was extracted from extraction line 16 at the rate of 18 g/hr, while 1,1,3,3-tetra-n-butyl-1,3-bis(3-methylbutyloxy) distannoxane produced according to the above process was supplied from line 17 at the rate of 18 g/hr. The resulting bis(3-methylbutyl) carbonate contained 23 ppm of metal atoms in the form of iron.

[0129]

[Reference Example 2] Production of Dibutyl Carbonate

Step (II-1): Production of Dialkyl Tin Catalyst

692 g (2.78 mol) of di-n-butyl tin oxide and 2001 g (27 mol) of 1-butanol (Wako Pure Chemical Industries, Ltd., Japan) were placed in a 3000 mL volumetric pear-shaped flask. The flask containing a mixture in the form of a white slurry was connected to an evaporator to which was connected an oil bath equipped with a temperature controller, a vacuum pump and a vacuum controller. The purge valve outlet of the evaporator was connected to a line containing nitrogen gas flowing at normal pressure. After closing the purge valve of the evaporator to reduce pressure inside the system, the purge valve was opened gradually to allow nitrogen to flow into the system and return to normal pressure. The oil bath temperature was set to be 126°C, the flask was immersed in the oil bath and rotation of the evaporator was started. After heating for about 30 minutes at a normal pressure with the purge valve of the evaporator left open, the mixture boiled and distillation of a low boiling point component began. After maintaining in this state for 8 hours, the purge valve was closed, pressure inside the system was gradually reduced, and residual low boiling point component was distilled with the pressure inside the system at from 76 to 54 kPa. After the low boiling point component no longer appeared, the flask was taken out of the oil bath. The reaction liquid was in the form of a clear liquid. Subsequently, the flask was taken out of the oil bath, the purge valve was opened gradually and the pressure inside the system was returned to normal pressure. 847 g of reaction liquid were obtained in the flask. Based on the results of ^{119}Sn -, ^1H - and ^{13}C -NMR analyses, 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane was obtained at a yield of 99% based on di-n-butyl tin oxide. The same procedure was then repeated 12 times to obtain a total of 10180 g of 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane.

[0130]

Step (II-2): Production of Dibutyl Carbonate

Carbonic acid ester was produced in a continuous production apparatus like that shown in FIG. 1. 1,1,3,3-Tetra-n-butyl-1,3-di(n-butyloxy) distannoxane produced in Step (II-1) was supplied at the rate of 4201 g/hr from feed line 4 into a column-type reaction vessel packed with Mellapak 750Y packing (Sulzer Chemtech Ltd., Switzerland) and having an inner diameter of 151 mm and effective length of 5040 mm, and 1-butanol purified with continuous multistage distillation column 101 was supplied to column-type reaction vessel 102 at the rate of 24717 g/hr from line 2. The liquid temperature inside reaction vessel 102 was adjusted to 160°C by heater and reboiler 112, and the pressure was adjusted to be about 120 kPa-G with a pressure control valve. The residence time in the reaction vessel was about 10 minutes. 1-butanol containing water at the rate of 24715 g/hr from a top of the reaction vessel via line 6, and 1-butanol at the rate of 824 g/hr via feed line 1, were pumped to continuous multistage distillation column 101 packed with Metal Gauze CY Packing (Sulzer Chemtech Ltd., Switzerland) and provided with reboiler 111 and condenser 121 to carry out distillative purification. In the top of continuous multistage distillation column 101, a fraction containing a high concentration of water was condensed by condenser 121 and recovered from transfer line 3. Purified 1-butanol was pumped via line 2 located in the lower portion of continuous multistage distillation column 101. An alkyl tin alkoxide catalyst composition containing di-n-butyl tin-di-n-butyloxy and 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane was obtained from the lower portion of column-type reaction vessel 102, and supplied to thin film evaporator 103 (Kobelco Eco-Solutions Co., Ltd., Japan) via line 5. The 1-butanol was distilled off in thin film evaporator 103 and returned to column-type reaction vessel 102 via condenser 123, transfer line 8 and transfer line 4. The alkyl tin alkoxide catalyst composition was pumped from the lower portion of thin film evaporator 103 via line 7 and supplied to autoclave 104 while adjusting the flow rate

of the active components in the form of di-n-butyl tin-di-n-butyloxy and 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane to about 4812 g/hr. Carbon dioxide was supplied to autoclave 104 by feed line 9 at the rate of 973 g/hr, and the pressure inside autoclave 104 was maintained at 4 MPa-G. The temperature inside the autoclave was set to be 120°C, the residence time was adjusted to about 4 hours, and a reaction between the carbon dioxide and the alkyl tin alkoxide catalyst composition was carried out to obtain a reaction liquid containing dibutyl carbonate. This reaction liquid was transferred to decarbonization tank 105 via line 10 and a control valve to remove residual carbon dioxide, and the carbon dioxide was recovered from line 11. Subsequently, the reaction liquid was pumped to thin film evaporator 106 (Kobelco Eco-Solutions Co., Ltd., Japan) set to be 140°C and about 1.4 kPa via line 12, and supplied while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane to about 4201 g/hr to obtain a fraction containing dibutyl carbonate. On the other hand, the evaporation residue was circulated to column-type reaction vessel 102 via line 13 and line 4 while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane to about 4201 g/hr. The fraction containing dibutyl carbonate was supplied to distillation column 107 packed with Metal Gauze CY packing (Sulzer Chemtech Ltd., Switzerland) and equipped with reboiler 117 and condenser 127 via condenser 126 and line 14 at the rate of 830 g/hr followed by distillative purification to obtain 99 wt% dibutyl carbonate from transfer line 15 at the rate of 814 g/hr. When the alkyl tin alkoxide catalyst composition of transfer line 13 was analyzed by ^{119}Sn -, ^1H - and ^{13}C -NMR analysis, it was found to contain 1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane but not contain di-n-butyl tin-di-n-butyloxy. After carrying out the above-mentioned continuous operation for about 600 hours, alkyl tin alkoxide catalyst composition was extracted from extraction line 16 at the rate of 16 g/hr, while

1,1,3,3-tetra-n-butyl-1,3-di(n-butyloxy) distannoxane produced in step (II-1) was supplied from line 17 at the rate of 16 g/hr. The resulting dibutyl carbonate contained 0.3 ppm of metal atoms in the form of iron.

[0131]

5 [Reference Example 3] Production of Bis(2-ethylbutyl) Carbonate

Step (III-1): Production of Dialkyl Tin Catalyst

893 g (2.48 mol) of di-n-octyl tin oxide (Sankyo Organic Chemicals Co., Ltd., Japan) and 2403 g (23.6 mol) of 2-ethyl-1-butanol were placed in a 5000 mL volumetric pear-shaped flask. The flask was connected to an evaporator to which
10 was connected an oil bath equipped with a temperature controller, a vacuum pump and a vacuum controller. The purge valve outlet of the evaporator was connected to a line containing nitrogen gas flowing at a normal pressure. After closing the purge valve of the evaporator to reduce pressure inside the system, the purge valve was opened gradually to allow nitrogen to flow into the system and return to the normal
15 pressure. The oil bath temperature was set to be about 165°C, the flask was immersed in the oil bath and rotation of the evaporator was started. After heating for about 40 minutes in the presence of nitrogen at atmospheric pressure with the purge valve of the evaporator left open, distillation of 2-ethyl-1-butanol containing water began. After maintaining in this state for 7 hours, the purge valve was closed,
20 pressure inside the system was gradually reduced, and residual 2-ethyl-1-butanol was distilled with the pressure inside the system at from 74 to 25 kPa. After the fraction no longer appeared, the flask was taken out of the oil bath. After allowing the flask to cool to the vicinity of room temperature (25°C), the flask was taken out of the oil bath, the purge valve was opened gradually and the pressure inside the
25 system was returned to atmospheric pressure. 1125 g of reaction liquid were obtained in the flask. Based on the results of ^{119}Sn -, ^1H - and ^{13}C -NMR analyses,

1,1,3,3-tetra-n-octyl-1,3-bis(2-ethylbutyloxy) distannoxane was confirmed to have been obtained at a yield of 99% based on di-n-octyl tin oxide. The same procedure was then repeated 12 times to obtain a total of 13510 g of 1,1,3,3-tetra-n-octyl-1,3-bis(2-ethylbutyloxy) distannoxane.

5 [0132]

Step (III-2): Production of Carbonic Acid Ester and Recovery of Deactivated Composition of Dialkyl Tin Catalyst

Carbonic acid ester was produced in a continuous production apparatus like that shown in FIG. 1. 1,1,3,3-Tetra-n-octyl-1,3-bis(2-ethylbutyloxy) distannoxane
10 produced in the manner described above was supplied at the rate of 6074 g/hr from line 4 into column-type reaction vessel 102 packed with Metal Gauze CY packing and having an inner diameter of 151 mm and effective length of 5040 mm, and 2-ethyl-1-butanol purified with continuous multistage distillation column 101 was supplied at the rate of 12260 g/hr from line 2. The liquid temperature inside reaction
15 vessel 102 was adjusted to 160°C by a heater and reboiler 112, and the pressure was adjusted to about 120 kPa-G with a pressure control valve. The residence time in the reaction vessel was about 17 minutes. 2-ethyl-1-butanol containing water at the rate of 12344 g/hr from the top of the reaction vessel via line 6, and 2-ethyl-1-butanol at the rate of 958 g/hr via line 1, were pumped to continuous
20 multistage distillation column 101 packed with Metal Gauze CY Packing and provided with reboiler 111 and condenser 121 to carry out distillative purification. In the top of continuous multistage distillation column 101, a fraction containing a high concentration of water was condensed by condenser 121 and recovered from recovery line 3. Purified 2-ethyl-1-butanol was pumped column-type reaction vessel
25 102 via line 2 located in the lower portion of continuous multistage distillation column 101. An alkyl tin alkoxide catalyst composition containing

di-n-octyl-bis(2-ethylbutyloxy) tin and 1,1,3,3-tetra-n-octyl-1,3-bis(2-ethylbutyloxy) distannoxane was obtained from the lower portion of column-type reaction vessel 102, and supplied to thin film evaporator 103 via line 5. The 2-ethyl-1-butanol was distilled off in thin film evaporator 103 and returned to column-type reaction vessel 102 via condenser 123, line 8 and line 4. The alkyl tin alkoxide catalyst composition was pumped from the lower portion of thin film evaporator 103 via line 7 and supplied to autoclave 104 while adjusting the flow rate of di-n-octyl-bis(2-ethylbutyloxy) tin and 1,1,3,3-tetra-n-octyl-1,3-bis (2-ethylbutyloxy) distannoxane to about 6945 g/hr. Carbon dioxide was supplied to autoclave 104 by line 9 at the rate of 973 g/hr, and the pressure inside autoclave 104 was maintained at 4 MPa-G. The temperature inside the autoclave was set to be 120°C, the residence time was adjusted to about 4 hours, and a reaction between the carbon dioxide and the alkyl tin alkoxide catalyst composition was carried out to obtain a reaction liquid containing bis(2-ethylbutyl) carbonate. This reaction liquid was transferred to decarbonization tank 105 via line 10 and a control valve to remove residual carbon dioxide, and the carbon dioxide was recovered from line 11. Subsequently, the reaction liquid was transferred to thin film evaporator 106 set to about 142°C and about 0.5 kPa via line 12, and supplied while adjusting the flow rate of 1,1,3,3-tetra-n-octyl-1,3-bis(2-ethylbutyloxy) distannoxane to about 6074 g/hr to obtain a fraction containing bis(2-ethylbutyl) carbonate. On the other hand, the evaporation residue was circulated to column-type reaction vessel 102 via line 13 and line 4 while adjusting the flow rate of 1,1,3,3-tetra-n-octyl-1,3-bis(2-ethylbutyloxy) distannoxane to about 6704 g/hr. The fraction containing bis(2-ethylbutyl) carbonate was supplied to distillation column 107 packed with Metal Gauze CY packing and equipped with reboiler 117 and condenser 127 via condenser 126 and line 14 at the rate of 959 g/hr followed by distillative purification to obtain 99 wt% bis(2-ethylbutyl) carbonate from recovery line 15 at the

rate of 1075 g/hr. When the alkyl tin alkoxide catalyst composition of line 13 was analyzed by ^{119}Sn -, ^1H - and ^{13}C -NMR analysis, it was found to contain 1,1,3,3-tetra-*n*-octyl-1,3-bis(2-ethylbutyloxy) distannoxane but not contain di-*n*-octyl-bis(2-ethylbutyloxy) tin. After carrying out the above-mentioned
5 continuous operation for about 220 hours, alkyl tin alkoxide catalyst composition was supplied from extraction line 16 at the rate of 18 g/hr, 1,1,3,3-tetra-*n*-octyl-1,3-bis(2-ethylbutyloxy) distannoxane produced in the manner described above was supplied from line 17 at the rate of 18 g/hr, and 180 g of a deactivated catalyst composition of 1,1,3,3-tetra-*n*-octyl-1,3-bis(2-ethylbutyloxy)
10 distannoxane was extracted from extraction line 16. The resulting bis(2-ethylbutyl) carbonate contained 4.8 ppm of metal atoms in the form of iron.

[0133]

[Reference Example 4] Production of Diheptyl Carbonate

Step (IV-1): Production of Dialkyl Tin Catalyst

15 692 g (2.78 mol) of di-*n*-butyl tin oxide and 3137 g (27 mol) of 1-heptanol (Wako Pure Chemical Industries, Ltd., Japan) were placed in a 3000 mL volumetric pear-shaped flask. The flask containing a mixture in the form of a white slurry was attached to an evaporator to which was connected an oil bath equipped with a temperature controller, a vacuum pump and a vacuum controller. The purge valve
20 outlet of the evaporator was connected to a line containing nitrogen gas flowing at normal pressure. After closing the purge valve of the evaporator to reduce pressure inside the system, the purge valve was opened gradually to allow nitrogen to flow into the system and reach a pressure of 39 kPa. The oil bath temperature was set to be 150°C, the flask was immersed in the oil bath and rotation of the evaporator was
25 started. After heating for about 30 minutes at a normal pressure with the purge valve of the evaporator left open, the mixture boiled and distillation of a low boiling

point component began. After maintaining in this state for 8 hours, the purge valve was closed, pressure inside the system was gradually reduced, and residual low boiling point component was distilled with the pressure inside the system at from 39 to 10 kPa. After the low boiling point component no longer appeared, the flask was
5 taken out of the oil bath. The reaction liquid was in the form of a clear liquid. Subsequently, the flask was taken out of the oil bath, the purge valve was opened gradually and the pressure inside the system was returned to the normal pressure. 952 g of reaction liquid were obtained in the flask. Based on the results of ^{119}Sn -, ^1H - and ^{13}C -NMR analyses, 1,1,3,3-tetra-n-butyl-1,3-diheptyloxy distannoxane was
10 obtained at a yield of 99% based on di-n-butyl tin oxide. The same procedure was then repeated 12 times to obtain a total of 11431 g of 1,1,3,3-tetra-n-butyl-1,3-diheptyloxy distannoxane.

[0134]

Step (IV-2): Production of Diheptyl Carbonate

15 Carbonic acid ester was produced in a continuous production apparatus like that shown in FIG. 1. 1,1,3,3-Tetra-n-butyl-1,3-di-n-heptyloxy distannoxane produced in Step (IV-1) was supplied at the rate of 4757 g/hr from line 4 into a column-type reaction vessel packed with Mellapak 750Y packing (Sulzer Chemtech Ltd., Switzerland) and having an inner diameter of 151 mm and effective length of
20 5040 mm, and 1-heptanol purified with continuous multistage distillation column 101 was supplied to column-type reaction vessel 102 at the rate of 13967 g/hr from line 2. The liquid temperature inside the reaction vessel was adjusted to 170°C by a heater and reboiler 112, and the pressure was adjusted to be about 120 kPa-G with a pressure control valve. The residence time in the reaction vessel was about 10
25 minutes. 1-heptanol containing water at the rate of 14051 g/hr from the top of the reaction vessel via line 6, and 1-heptanol at the rate of 1086 g/hr via line 1, were

pumped to continuous multistage distillation column 101 packed with Metal Gauze CY Packing (Sulzer Chemtech Ltd., Switzerland) and provided with reboiler 111 and condenser 121 to carry out distillative purification. In the top of continuous multistage distillation column 101, a fraction containing a high concentration of water was condensed by condenser 121 and recovered from line 3. Purified 1-heptanol was pumped via transfer line 2 located in the lower portion of continuous multistage distillation column 101. An alkyl tin alkoxide catalyst composition containing di-n-butyl tin-di-n-heptyloxy and 1,1,3,3-tetra-n-butyl-1,3-di-n-heptyloxy distannoxane was obtained from the lower portion of column-type reaction vessel 102, and supplied to thin film evaporator 103 (Kobelco Eco-Solutions Co., Ltd., Japan) via line 5. The 1-heptanol was distilled off in thin film evaporator 103 and returned to column-type reaction vessel 102 via condenser 123, line 8 and line 4. The alkyl tin alkoxide catalyst composition was pumped from the lower portion of thin film evaporator 103 via line 7 and supplied to autoclave 104 while adjusting the flow rate of the active components in the form of di-n-butyl tin-di-n-heptyloxy and 1,1,3,3-tetra-n-butyl-1,3-di-n-heptyloxy distannoxane to about 5764 g/hr. Carbon dioxide was supplied to autoclave 104 by line 9 at the rate of 973 g/hr, and the pressure inside autoclave 104 was maintained at 4 MPa-G. The temperature inside the autoclave was set to be 120°C, the residence time was adjusted to about 4 hours, and a reaction between the carbon dioxide and the alkyl tin alkoxide catalyst composition was carried out to obtain a reaction liquid containing diheptyl carbonate. The reaction liquid was transferred to decarbonization tank 105 via line 10 and a control valve to remove residual carbon dioxide, and the carbon dioxide was recovered from line 11. Subsequently, the reaction liquid was pumped to thin film evaporator 106 (Kobelco Eco-Solutions Co., Ltd., Japan) set to be 140°C and about 1.4 kPa via line 12, and supplied while adjusting the flow rate of

1,1,3,3-tetra-n-butyl-1,3-di-n-heptyloxy distannoxane to about 4757 g/hr to obtain a fraction containing dibutyl carbonate. On the other hand, the evaporation residue was circulated to column-type reaction vessel 102 via line 13 and line 4 while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-di-n-heptyloxy distannoxane to be about 5764 g/hr. The fraction containing diheptyl carbonate was supplied to distillation column 107 packed with Metal Gauze CY packing (Sulzer Chemtech Ltd., Switzerland) and equipped with reboiler 117 and condenser 127 via condenser 126 and line 14 at the rate of 1223 g/hr followed by distillative purification to obtain 99 wt% diheptyl carbonate from line 15 at the rate of 1208 g/hr. When the alkyl tin alkoxide catalyst composition of line 13 was analyzed by ^{119}Sn -, ^1H - and ^{13}C -NMR analysis, it was found to contain 1,1,3,3-tetra-n-butyl-1,3-di-n-heptyloxy distannoxane but not contain di-n-butyl tin-di-n-heptyloxy. After carrying out the above-mentioned continuous operation for about 600 hours, alkyl tin alkoxide catalyst composition was extracted from extraction line 16 at the rate of 22 g/hr, while 1,1,3,3-tetra-n-butyl-1,3-di-n-heptyloxy distannoxane produced in step (IV-1) was supplied from feed line 17 at the rate of 22 g/hr. The resulting diheptyl carbonate contained 26 ppm of metal atoms in the form of iron.

[0135]

[Reference Example 5] Production of Bis(2-ethylhexyl) Carbonate

20 Step (V-1): Production Dialkyl Tin Catalyst

692 g (2.78 mol) of di-n-butyl tin oxide and 3516 g (27 mol) of 2-ethyl-1-hexanol (Wako Pure Chemical Industries, Ltd., Japan) were placed in a 3000 mL volumetric pear-shaped flask. The flask containing a mixture in the form of a white slurry was attached to an evaporator to which was connected an oil bath equipped with a temperature controller, a vacuum pump and a vacuum controller. The purge valve outlet of the evaporator was connected to a line containing nitrogen gas flowing at a

normal pressure. After closing the purge valve of the evaporator to reduce pressure inside the system, the purge valve was opened gradually to allow nitrogen to flow into the system and reach a pressure of about 26 kPa. The oil bath temperature was set to be 150°C, the flask was immersed in the oil bath and rotation of the evaporator was started. After heating for about 30 minutes at the normal pressure with the purge valve of the evaporator left open, the mixture boiled and distillation of a low boiling point component began. After maintaining in this state for 8 hours, the purge valve was closed, pressure inside the system was gradually reduced, and residual low boiling point component was distilled with the pressure inside the system at 26 to 10 kPa. After the low boiling point component no longer appeared, the flask was taken out of the oil bath. The reaction liquid was in the form of a clear liquid. Subsequently, the flask was taken out of the oil bath, the purge valve was opened gradually and the pressure inside the system was returned to the normal pressure. 990 g of reaction liquid were obtained in the flask. Based on the results of ^{119}Sn -, ^1H - and ^{13}C -NMR analyses, 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane was obtained at a yield of 99% based on di-n-butyl tin oxide. The same procedure was then repeated 12 times to obtain a total of 11880 g of 1,1,3,3-tetra-n-butyl- 1,3-bis(2-ethylhexyloxy) distannoxane.

[0136]

Step (V-2): Production of Bis(2-ethylhexyl) Carbonate

Carbonic acid ester was produced in a continuous production apparatus like that shown in FIG. 1. 1,1,3,3-Tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane produced in Step (V-1) was supplied at the rate of 4943 g/hr from line 4 into a column-type reaction vessel packed with Mellapak 750Y packing (Sulzer Chemtech Ltd., Switzerland) and having an inner diameter of 151 mm and effective length of 5040 mm, and 2-ethyl-1-hexanol purified with continuous multistage distillation

column 101 was supplied to column-type reaction vessel 102 at the rate of 15653 g/hr from line 2. The liquid temperature inside the reaction vessel was adjusted to be 170°C by a heater and reboiler 112, and the pressure was adjusted to be about 120 kPa-G with a pressure control valve. The residence time in the reaction vessel was about 10 minutes. 2-Ethyl-1-hexanol containing water at the rate of 15737 g/hr from the top of the reaction vessel via line 6, and 2-ethyl-1-hexanol at the rate of 1217 g/hr via line 1, were pumped to continuous multistage distillation column 101 packed with Metal Gauze CY Packing (Sulzer Chemtech Ltd., Switzerland) and provided with reboiler 111 and condenser 121 to carry out distillative purification. In the top of continuous multistage distillation column 101, a fraction containing a high concentration of water was condensed by condenser 121 and recovered from line 3. Purified 2-ethyl-1-hexanol was pumped via line 2 located in the lower portion of continuous multistage distillation column 101. An alkyl tin alkoxide catalyst composition containing di-n-butyl tin-bis(2-ethylhexyloxy) and 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane was obtained from the lower portion of column-type reaction vessel 102, and supplied to thin film evaporator 103 (Kobelco Eco-Solutions Co., Ltd., Japan) via line 5. The 2-ethyl-1-hexanol was distilled off in thin film evaporator 103 and returned to column-type reaction vessel 102 via condenser 123, line 8 and line 4. The alkyl tin alkoxide catalyst composition was pumped from the lower portion of thin film evaporator 103 via line 7 and supplied to autoclave 104 while adjusting the flow rate of the active components in the form of di-n-butyl tin-bis(2-ethylhexyloxy) and 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane to about 6083 g/hr. Carbon dioxide was supplied to the autoclave by line 9 at the rate of 973 g/hr, and the pressure inside the autoclave was maintained at 4 MPa-G. The temperature inside the autoclave was set to be 120°C, the residence time was adjusted to about 4 hours, and a reaction between the carbon dioxide and

the alkyl tin alkoxide catalyst composition was carried out to obtain a reaction liquid containing bis(2-ethylhexyl) carbonate. This reaction liquid was transferred to decarbonization tank 105 via line 10 and a control valve to remove residual carbon dioxide, and the carbon dioxide was recovered from line 11. Subsequently, the reaction liquid was pumped to thin film evaporator 106 (Kobelco Eco-Solutions Co., Ltd., Japan) set to 140°C and about 1.4 kPa via line 12, and supplied while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane to about 4943 g/hr to obtain a fraction containing dibutyl carbonate. On the other hand, the evaporation residue was circulated to column-type reaction vessel 102 via transfer line 13 and transfer line 4 while adjusting the flow rate of 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane to about 4943 g/hr. The fraction containing dibutyl carbonate was supplied to distillation column 107 packed with Metal Gauze CY packing (Sulzer Chemtech Ltd., Switzerland) and equipped with reboiler 117 and condenser 127 via condenser 126 and line 14 at the rate of 1354 g/hr followed by distillative purification to obtain 99 wt% bis(2-ethylhexyl) carbonate from transfer line 15 at the rate of 1339 g/hr. When the alkyl tin alkoxide catalyst composition of line 13 was analyzed by ^{119}Sn -, ^1H - and ^{13}C -NMR analysis, it was found to contain 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane but not contain di-n-butyl tin-bis(2-ethylhexyloxide). After carrying out the above-mentioned continuous operation for about 600 hours, alkyl tin alkoxide catalyst composition was extracted from extraction line 16 at the rate of 23 g/hr, while 1,1,3,3-tetra-n-butyl-1,3-bis(2-ethylhexyloxy) distannoxane produced in step (V-1) was supplied from feed line 17 at the rate of 23 g/hr. The resulting bis(2-ethylhexyl) carbonate contained 30 ppm of metal atoms in the form of iron.

[0137]

[Reference Example 6] Production of Diphenyl Carbonate

Diphenyl carbonate was produced using the dibutyl carbonate obtained in Reference Example 2.

Step (VI-1): Production of Aromatic Carbonic Acid Ester

[Preparation of Catalyst]

5 79 g of phenol and 32 g of lead monoxide were heated for 10 hours at 180°C after which the water formed was distilled off together with phenol. About 2.5 g of water were extracted in 10 hours. Subsequently, phenol was distilled off from an upper portion of the reaction vessel to prepare a catalyst.

[Production of Aromatic Carbonic Acid Ester]

10 An apparatus like that shown in FIG. 2 was used.

A mixture comprising the dibutyl carbonate obtained in step (I-2), phenol and the catalyst prepared above (adjusted so that the weight ratio of dibutyl carbonate and phenol in the mixture was about 65/35 and the lead concentration was about 1% by weight) was continuously fed in a liquid state through preheater 201 to the middle
15 stage of continuous multistage distillation column 202 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 21 at the rate of about 270 g/hr and allowed to react. The amount of heat required for the reaction and distillation was supplied by circulating the liquid in the bottom of the column through line 23 and reboiler 204. The liquid temperature in
20 the bottom of continuous multistage distillation column 202 was 238°C, the pressure at the top of the column was about 250 kPa, and the reflux ratio was set to be about 2. Gas distilled from the top of continuous multistage distillation column 202 was extracted from line 22, and continuously extracted into storage tank 205 through condenser 203 from line 24 at the rate of about 67 g/hr. Liquid was continuously
25 extracted from the bottom of the column through line 23 into storage tank 206 at the rate of about 204 g/hr.

The composition of the liquid extracted from line 24 consisted of about 33% by weight of 1-butanol, about 65% by weight of phenol and about 2% by weight of dibutyl carbonate. The composition of the liquid extracted to storage tank 206 consisted of about 11% by weight of phenol, about 60% by weight of dibutyl carbonate, about 26% by weight of butylphenyl carbonate, and about 1.6% by weight of diphenyl carbonate, and the lead concentration was about 1% by weight.

Next, an apparatus like that shown in FIG. 3 was used.

Liquid extracted into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m from line 31 at the rate of about 203 g/hr. The amount of heat required for the reaction and distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 240°C, the pressure at the top of the column was about 27 kPa, and the reflux ratio was set to about 2. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted from line 34 into storage tank 305 at the rate of about 165 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 39 g/hr.

The composition of the liquid extracted from line 34 consisted of about 500 ppm of 1-butanol, about 13% by weight of phenol, about 85% by weight of dibutyl carbonate and about 2% by weight of butylphenyl carbonate. The composition of the liquid extracted to storage tank 306 consisted of about 0.3% by weight of dibutyl carbonate, about 32% by weight of butylphenyl carbonate, and about 61% by weight of diphenyl carbonate, and the lead concentration was about 7% by weight.

[Recycling of Alcohol]

Alcohol was recycled using an apparatus like that shown in FIG. 4.

Liquid continuously extracted into storage tank 205 was continuously fed through a preheater 401 to a position of about 0.7 m from the bottom of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m from line 41 at the rate of about 201 g/hr to carry out distillative separation. The amount of heat required for the distillative separation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 145°C, the pressure at the top of the column was about 13 kPa, and the reflux ratio was set to be about 0.3. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and extracted from line 44 into storage tank 405 at the rate of about 68 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 133 g/hr.

The composition of the liquid extracted from line 44 contained about 99% by weight of 1-butanol and about 100 ppm of phenol. The composition of the liquid extracted to storage tank 406 consisted of about 2% by weight of dibutyl carbonate and about 98% by weight of phenol.

20 [Purification of Diaryl Carbonate]

Diaryl carbonate was purified using an apparatus like that shown in FIGS. 5 and 6.

Liquid extracted to storage tank 306 was continuously fed through preheater 501 to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 51 at the rate of about 195 g/hr. The amount of heat

required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 53 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 210°C, the pressure at the top of the column was about 1.5 kPa, and the reflux ratio was set to be about 1. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 52, and continuously extracted from line 54. Liquid was extracted from the bottom of the column through line 53 into storage tank 506 at the rate of about 14 g/hr.

The composition of the liquid extracted from line 54 contained about 0.3% by weight of dibutyl carbonate, about 34% by weight of butylphenyl carbonate and about 66% by weight of diphenyl carbonate.

Liquid extracted from line 54 was continuously fed through preheater 601 to the middle stage of continuous multistage distillation column 602 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m from line 61 at the rate of about 181 g/hr. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 63 and reboiler 604. The liquid temperature in the bottom of continuous multistage distillation column 602 was 232°C, the pressure at the top of the column was about 15 kPa, and the reflux ratio was set to be about 2. Gas distilled from the top of continuous multistage distillation column 602 was condensed in condenser 603 via line 62 and continuously extracted from line 64. Liquid was extracted from the bottom of the column through line 63 into storage tank 606 at the rate of about 119 g/hr.

The composition of the liquid extracted from line 64 contained about 0.6% by weight of dibutyl carbonate, about 99% by weight of butylphenyl carbonate and about 0.4% by weight of diphenyl carbonate. The composition of the liquid extracted to

storage tank 606 contained about 0.1% by weight of butylphenyl carbonate and about 99.9% by weight of diphenyl carbonate. The diphenyl carbonate contained 8.2 ppm of a metal component in the form of iron.

[0138]

5 [Example 1]

Step (1-1): Production of N,N'-hexanediyl-bis-carbamic Acid
Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 2.

3333 g (16.5 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1
10 were supplied to a baffled reaction vessel 204 made of SUS and having an inner
volume of 5 L from storage tank 201 via line 21 with line 24 closed, and 383.5 g (3.3
mol) of hexamethylene diamine (Aldrich Corp., USA) were supplied to the reaction
vessel 204 from storage tank 202 via line 22. The liquid temperature inside the
reaction vessel 204 was adjusted to be about 80°C, and 6.4 g of sodium methoxide
15 (28% methanol solution, Wako Pure Chemical Industries, Ltd., Japan) were supplied
to the SUS reaction vessel 204 from storage tank 203 via line 23 to carry out a
reaction.

As a result of analyzing the solution following the reaction by liquid
chromatography, N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester was
20 found to have been formed at a yield of 99.7%.

Line 24 was opened and the reaction liquid was supplied to column 205 which
was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and
Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C
by an external jacket so as to neutralize the sodium methoxide. The solution was
25 then transferred to storage tank 206 via line 25.

[0139]

Step (1-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of the continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 43 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 237 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 237 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 150 g/hr. Liquid was continuously extracted from the bottom of the column

through line 43 into storage tank 406 at the rate of about 87 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.2% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

5 [0140]

Step (1-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 (Kobelco Eco-Solutions Co., Ltd., Japan)
10 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to to about 13 kPa. The mixture recovered into storage tank 406 in step (1-2) was heated to 160°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr. In addition, dibutyl tin dilaurate (Wako Pure Chemical Industries, Ltd., Japan) was fed from line 51 at the
15 rate of about 25.2 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus
20 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through
25 line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 150°C, and the pressure at the top of the

column was about 50 kPa. Gas distilled from the top of the continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

5 The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the
10 bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in
15 the steady state was about 130 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 11 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine
20 was 96.7%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0141]

25 [Example 2]

Step (2-1): Production of 3-((3-methylbutyloxy)carbonylamino-methyl-

3,5,5-trimethylcyclohexylcarbamic Acid (3-methylbutyl) Ester

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3394 g (16.8 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1, 596 g (3.5 mol) of 3-aminomethyl-3,5,5-trimethylcyclohexylamine (Aldrich Corp., USA) instead of hexamethylene diamine, and 6.8 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, 3-((3-methylbutoxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic acid (3-methylbutyl) ester was found to have been formed at a yield of 99.5%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0142]

Step (2-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303

via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 43 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 237 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

5 The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 237 g/hr. The amount of heat required for distillation was supplied by circulating the
10 liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of
15 about 138 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 98 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 99.0% by weight of 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic acid
20 (3-methylbutyl) ester.

[0143]

Step (2-3): Production of Isocyanate by Thermal Decomposition of 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic Acid
(3-methylbutyl) Ester

25 A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1

m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (2-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 200 g/hr. In addition, dibutyl tin dilaurate (Wako Pure Chemical Industries, Ltd., Japan) was fed from line 51 at the rate of about 25.2 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 150°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the

bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 107 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 9 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of isophorone diisocyanate. The yield based on hexamethylene diamine was 96.5%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0144]

[Example 3]

Step (3-1): Production of N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic Acid Bis(3-methylbutyl) Ester

Ferrous acetylacetonate was added to the bis(3-methylbutyl) carbonate of Reference Example 1 to prepare bis(3-methylbutyl) carbonate containing 7.4% of metal atoms in the form of iron. A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 2917 g (14.4 mol) of the bis(3-methylbutyl) carbonate, 753 g (3.8 mol) of 4,4'-methylenedianiline (Aldrich Corp., USA) instead of hexamethylene diamine, and 7.3 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic acid bis(3-methylbutyl) ester was found to have been formed

at a yield of 99.1%. The reaction liquid was supplied to column 205 which packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then
5 transferred to storage tank 206 via line 25.

[0145]

Step (3-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid
10 state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 270 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid
15 temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of the continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 48 g/hr. Liquid was continuously extracted from the bottom of the
20 column through line 33 into storage tank 306 at the rate of about 222 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner
25 diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 237 g/hr. The amount of heat required for distillation was supplied by circulating the

liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403
5 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 102 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 120 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.5% by weight of
10 N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic acid bis(3-methylbutyl) ester.
[0146]

Step (3-3): Production of Isocyanate by Thermal Decomposition of
N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 6.

15 Thin film distillation apparatus 701 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 1.3 kPa. The mixture recovered into storage tank 406 in step (3-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 701 via line 70 at the rate of about 190 g/hr. In addition, dibutyl tin dilaurate was fed from line 71 at the rate of about 14
20 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 701 via line 73, and circulated to the top of thin film distillation apparatus 701 via line 74. A gaseous phase component was extracted from line 72.

The gaseous phase component extracted from thin film distillation apparatus 701 via line 72 was continuously fed to the middle stage of continuous multistage
25 distillation column 702 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of

the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 76 and reboiler 704. The liquid temperature in the bottom of continuous multistage distillation column 702 was 200°C, and the pressure at the top of the column was 60 kPa. Gas distilled from the top of continuous multistage distillation column 702 was condensed in condenser 703 via line 75 and continuously extracted from line 77. A liquid phase component was extracted from line 78.

The liquid phase component extracted from line 78 was continuously fed to the middle stage of a continuous multistage distillation column 705 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 81 and reboiler 707. The liquid temperature in the bottom of continuous multistage distillation column 705 was 210°C, and the pressure at the top of the column was about 2.5 kPa. Gas distilled from the top of continuous multistage distillation column 705 was condensed in condenser 706 via line 80 and continuously extracted via line 82. A liquid component was extracted from line 84.

The liquid phase component extracted from line 84 was continuously fed to the middle stage of continuous multistage distillation column 708 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 86 and reboiler 710. The liquid temperature in the bottom of continuous multistage distillation column 708 was 220°C, and the pressure at the top of the column was about 0.5 kPa. Gas distilled from the top of continuous multistage distillation column 708 was condensed in condenser 709 via line 85 and

continuously extracted via line 87 at the rate of about 105 g/hr. The liquid extracted from line 87 contained about 99.9% by weight of 4,4'- diphenylmethane diisocyanate. The yield based on 4,4'-methylenedianiline was 95.3%. Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of thin film distillation apparatus 701.

[0147]

[Example 4]

Step (4-1): Production of Bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl Carbamate

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3064 g (15.2 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1, 778 g (3.7 mol) of 4,4'-methylenebis(cyclohexylamine) (Aldrich Corp., USA) instead of hexamethylene diamine, and 7.1 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl carbamate was found to have been formed at a yield of 99.0%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0148]

Step (4-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation

column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 270 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 45 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 225 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 225 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 111 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 114 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 99.1% by weight of bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl carbamate.

[0149]

Step (4-3): Production of Isocyanate by Thermal Decomposition of
N,N'-(4,4'-methanediyl-diphenyl)-biscarbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 6.

5 Thin film distillation apparatus 701 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to about 1.3 kPa. The mixture recovered into storage tank 406 in step (4-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 701 via line 70 at the rate of about 200 g/hr. In addition, dibutyl tin dilaurate was fed from line 71 at the rate of about 14
10 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 701 via line 73, and circulated to the top of the thin film distillation apparatus 701 via line 74. A gaseous phase component was extracted from line 72.

The gaseous phase component extracted from thin film distillation apparatus 701 via line 72 was continuously fed to the middle stage of continuous multistage
15 distillation column 702 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 76 and reboiler 704. The liquid temperature in the bottom of continuous
20 multistage distillation column 702 was 200°C, and the pressure at the top of the column was 60 kPa. Gas distilled from the top of continuous multistage distillation column 702 was condensed in condenser 703 via line 75 and continuously extracted from line 77. A liquid phase component was extracted from line 78.

The liquid phase component extracted from line 78 was continuously fed to the
25 middle stage of continuous multistage distillation column 705 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of

2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 81 and reboiler 707. The liquid temperature in the bottom of continuous multistage distillation column 705 was 210°C, and the pressure at the top of the column was about 2.5 kPa. Gas distilled from the top of continuous multistage distillation column 705 was condensed in condenser 706 via line 80 and continuously extracted via line 82. A liquid component was extracted from line 84.

The liquid phase component extracted from line 84 was continuously fed to the middle stage of continuous multistage distillation column 708 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 86 and reboiler 710. The liquid temperature in the bottom of continuous multistage distillation column 708 was 220°C, and the pressure at the top of the column was about 0.5 kPa. Gas distilled from the top of continuous multistage distillation column 708 was condensed in condenser 709 via line 85 and continuously extracted via line 87 at the rate of about 105 g/hr. The liquid extracted from line 87 contained about 99.8% by weight of 4,4'-methylenebis(cyclohexylisocyanate). The yield based on 4,4'-methylenebis(cyclohexylamine) was 93.2%. Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of thin film distillation apparatus 701. When continuous operation was carried out for 30 days, accumulation of adhered substances was observed on the walls of thin film distillation apparatus 701.

[0150]

[Example 5]

Step (5-1): Production of Toluene-2,4-dicarbamic Acid Bis(2-ethylbutyl)

Ester

Bis(2-ethylbutyl) carbonate of Reference Example 3 was placed in pear-shaped flask having an internal volume of 10 L, a three-way valve, distillation column packed with Helipak No. 3, fractionating column equipped with a reflux condenser and coupled to a distillate collector, and thermometer were attached to the pear-shaped flask and the inside of the system was replaced with nitrogen in a vacuum to carry out distillative purification of the bis(2-ethylbutyl) carbonate. When ¹H-NMR measurement was carried out on the distillative purification product, it was found to contain about 99.9% by weight of bis(2-ethylbutyl) carbonate. In addition, it also contained 0.003 ppm of metal atoms in the form of iron.

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3589 g (15.6 mol) of the above bis(2-ethylbutyl) carbonate instead of bis(3-methylbutyl) carbonate, 464 g (3.8 mol) of 2,4-toluenediamine (Aldrich Corp., USA) instead of hexamethylene diamine, and 7.3 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, toluene-2,4-dicarbamic acid bis(2-ethylbutyl) ester was found to have been formed at a yield of 98.5%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0151]

25 Step (5-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 300 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 60 kPa. Gas distilled from the top of the continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 56 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 244 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 244 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of the continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 0.7 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 138 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 106 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid

chromatography, the mixture was found to contain about 98.9% by weight of toluene-2,4-dicarbamic acid bis(2-ethylbutyl) ester.

[0152]

Step (5-3): Production of Isocyanate by Thermal Decomposition of
5 Toluene-2,4-dicarbamic Acid Bis(2-ethylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (5-2) was heated to 170°C and
10 supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 190 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 15.7 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted
15 from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of
20 the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of the continuous multistage distillation column 502 was 160°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of the continuous multistage
25 distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of

continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of the continuous multistage distillation column 505 was 160°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 83 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 16 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of 2,4-tolylene diisocyanate. The yield based on 2,4-toluenediamine was 94.7%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0153]

[Example 6]

Step (6-1): Production of N,N'-hexanediyl-bis-carbamic Acid Bis(2-ethylbutyl) Ester

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3483 g (15.1 mol) of the

bis(2-ethylbutyl) carbonate of Reference Example 3 instead of bis(3-methylbutyl) carbonate, a mixture of 418 g (3.6 mol) of hexamethylene diamine and 368 g (3.8 mol) of 2-ethyl-1-butanol instead of hexamethylene diamine, and 6.9 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(2-ethylbutyl) ester was found to have been formed at a yield of 99.5%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0154]

Step (6-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 270 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 60 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 69 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 201 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner
5 diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 201 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 0.7 kPa. Gas distilled from the
10 top of the continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 115 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 86 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid
15 chromatography, the mixture was found to contain about 98.3% by weight of N,N'-hexanediyl-bis-carbamic acid bis(2-ethylbutyl) ester.

[0155]

Step (6-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(2-ethylbutyl) Ester

20 A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (6-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about
25 270 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 22.7 g/hr. A liquid phase component was extracted from the bottom of thin film

distillation apparatus 501 via line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of the continuous multistage distillation column 502 was 160°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of the continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of the continuous multistage distillation column 505 was 160°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 116 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 22 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine
5 was 95.5%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0156]

10 [Example 7]

Step (7-1): Production of 3-(phenoxycarbonylaminomethyl)-3,5,5-trimethylcyclohexylcarbamic Acid Phenyl Ester

A reaction was carried out using an apparatus like that shown in FIG. 7.

1992 g (9.3 mol) of the diphenyl carbonate of Reference Example 6 were
15 supplied to baffled reaction vessel 724 made of SUS and having an inner volume of 5 L from storage tank 721 via line A1 with line A4 closed, and 1311 g (14.0 mol) of phenol were supplied to the reaction vessel made of SUS from storage tank 722 via line A2. The liquid temperature inside reaction vessel 724 was adjusted to be about 50°C, and 528 g (3.1 mol) of 3-aminomethyl-3,5,5-trimethylcyclohexylamine were
20 supplied to reaction vessel 724 from storage tank 723 via line A3 at the rate of about 250 g/hr.

As a result of analyzing the solution following the reaction by liquid chromatography,
3-(phenoxycarbonylaminomethyl)-3,5,5-trimethylcyclohexylcarbamic acid phenyl ester was found to have been formed at a
25 yield of 99.3%.

Line A4 was opened and the reaction liquid was transferred to storage tank 725

via line A4.

[0157]

Step (7-2): Removal of Low Boiling Point Component

Phenol was removed using an apparatus like that shown in FIG. 3.

5 The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 300 g/hr. The amount of heat required for distillation was supplied by circulating the
10 liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 60 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of
15 about 155 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 145 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

 The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to middle stage of continuous multistage distillation
20 column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 145 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C,
25 and the pressure at the top of the column was about 0.4 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403

via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 55 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 90 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 99.1% by weight of 3-(phenoxy-carbonylaminomethyl)-3,5,5-trimethylcyclohexylcarbamic acid phenyl ester.

[0158]

Step (7-3): Production of Isocyanate by Thermal Decomposition of 3-(phenoxy-carbonylaminomethyl)-3,5,5-trimethylcyclohexylcarbamic Acid Phenyl Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 220°C and the pressure within was set to about 13 kPa. The mixture recovered into storage tank 406 in step (7-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 300 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through

line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 150°C, and the pressure at the top of the column was about 15 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously
5 extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of
10 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.3 kPa. Gas distilled from the top of continuous
15 multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62 at the rate of about 135 g/hr.

The liquid extracted from line 92 was a solution that contained about 99.8% by weight of isophorone diisocyanate. The yield based on 3-aminomethyl-3,5,5-trimethylcyclohexylamine was 95.3%. Although continuous operation was carried
20 out for 10 days, there was no accumulation of adhered substances observed on the walls of the film distillation apparatus 501.

[0159]

[Example 8]

Step (8-1): Production of N,N'-hexanediyl-bis-carbamic Acid Di(n-heptyl)
25 Ester

A process was carried out in the same manner as step (1-1) of Example 1 with

the exception of carrying out the reaction by supplying 3445 g (13.3 mol) of the diheptyl carbonate of Reference Example 4 instead of bis(3-methylbutyl) carbonate, 360 g (3.1 mol) of hexamethylene diamine and 6.0 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by

5 liquid chromatography, N,N'-hexanedyl-bis-carbamic acid di(n-heptyl) ester was found to have been formed at a yield of 98.9%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide.

10 The solution was then transferred to storage tank 206 via line 25.

[0160]

Step (8-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid

15 state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid

20 temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 13 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 52 g/hr. Liquid was continuously extracted from the bottom of the column

25 through line 33 into storage tank 306 at the rate of about 228 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 228 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 170°C, and the pressure at the top of the column was about 0.13 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 136 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 92 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.6% by weight of N,N'-hexanediyl-bis-carbamic acid di(n-heptyl) ester.

[0161]

Step (8-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Di(n-heptyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (8-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 270 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 19.6 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of the thin film

distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 160°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

A gaseous phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 160°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 107 g/hr.

After operating for 40 hours, the liquid phase component was extracted into

storage tank 510 from line 64 at the rate of about 21 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 94.9%.

5 Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0162]

[Example 9]

10 Step (9-1): Production of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 2687 g (13.3 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1, 407 g (3.5 mol) of
15 hexamethylene diamine and 6.8 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester was found to have been formed at a yield of 99.5%.

After opening line 24, the reaction liquid was supplied to column 205 which was
20 packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0163]

25 Step (9-2): Removal of Low Boiling Point Component

A process was carried out in the same manner as step (1-2) of Example 1 with

the exception of continuously feeding the mixture recovered into storage tank 206 in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 from line 31 at the rate of about 300 g/hr, continuously extracting a liquid phase component from the bottom of the column to storage tank 306 via line 33 at the rate of about 241 g/hr, and continuously feeding the mixture recovered into storage tank 306 in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 from line 41 at the rate of about 241 g/hr. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 123 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 118 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.5% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

[0164]

Step (9-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 (Kobelco Eco-Solutions Co., Ltd., Japan) having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. A process was carried out in the same manner as step (1-3) of Example 1 with the exception of heating the mixture recovered into storage tank 406 in step (9-2) to 200°C, supplying to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr, and feeding dibutyl tin dilaurate from line 51 at the rate of about 25.3 g/hr. A liquid was extracted

into storage tank 509 via line 62 at the rate of about 107 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 82 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 79.6%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of thin film distillation apparatus 501.

10 [0165]

[Example 10]

Step (10-1): Production of Bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl Carbamate

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3272 g (16.2 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1, 757 g (3.6 mol) of 4,4'-methylenebis(cyclohexylamine) instead of hexamethylene diamine, and 6.9 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl carbamate was found to have been formed at a yield of 98.9%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0166]

Step (10-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 44 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 236 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 236 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 127 g/hr. Liquid was continuously extracted from the bottom of the column

through line 43 into storage tank 406 at the rate of about 109 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 99.0% by weight of bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl carbamate.

5 [0167]

Step (10-3): Production of Isocyanate by Thermal Decomposition of Bis(3-methylbutyl)-4,4'-methylene-dicyclohexyl Carbamate

A reaction was carried out using an apparatus like that shown in FIG. 8.

The mixture recovered into storage tank 406 in step (10-2) was heated to
10 170°C and fed to the middle stage of continuous multistage distillation column 801
packed with Dickson packing (diameter: 6 mm) and having an inner diameter of
about 5 cm and column length of 2 m via line B0 at the rate of about 220 g/hr, while
at the same time dibutyl tin dilaurate was fed from line B1 at the rate of 15.7 g/hr to
carry out a thermal decomposition reaction. The amount of heat required for the
15 thermal decomposition reaction was supplied by circulating the liquid in the bottom of
the column through line B3 and reboiler 803. The liquid temperature in the bottom
of continuous multistage distillation column 801 was 280°C, and the pressure at the
top of the column was about 15 kPa. Gas distilled from the top of continuous
multistage distillation column 801 was condensed in condenser 802 via line B2 and
20 continuously extracted from line B4. A liquid phase component was recovered from
the bottom of continuous multistage distillation column 801 via line B3.

A liquid phase component extracted via line B6 was continuously fed to the
middle stage of continuous multistage distillation column 804 packed with Dickson
packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of
25 2 m to carry out distillative separation of the liquid phase component. The amount
of heat required for distillative separation was supplied by circulating the liquid in the

bottom of the column through line B8 and reboiler 806. The liquid temperature in the bottom of continuous multistage distillation column 804 was 220°C, and the pressure at the top of the column was about 5.2 kPa. Gas distilled from the top of continuous multistage distillation column 804 was condensed in condenser 805 via line B7 and continuously extracted from line B9. A liquid phase component was recovered from the bottom of continuous multistage distillation column 804 via line B8 and line B11.

The liquid phase component extracted from line B8 was continuously fed to the middle stage of continuous multistage distillation column 807 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line B14 and reboiler 809. The liquid temperature in the bottom of continuous multistage distillation column 807 was 220°C, and the pressure at the top of the column was about 0.40 kPa. Gas distilled from the top of continuous multistage distillation column 807 was condensed in condenser 808 via line B12 and continuously extracted via line B13. The extracted amount in the steady state was about 108 g/hr.

The liquid extracted from line B13 was a solution that contained about 99.8% by weight of 4,4'-methylene-bis(cyclohexylisocyanate). The yield based on 4,4'-methylenebis(cyclohexylamine) was 82.2%. When continuous operation was carried out for 10 days, accumulation of adhered substances was observed inside continuous multistage distillation column 801.

[0168]

[Example 11]

Step (11-1): Production of N,N'-hexanediyl-bis-carbamic Acid

Bis(2-ethylbutyl) Ester

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3547 g (15.4 mol) of the bis(2-ethylbutyl) carbonate of Reference Example 3 instead of bis(3-methylbutyl) carbonate, 407 g (3.5 mol) of hexamethylene diamine and 6.8 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(2-ethylbutyl) ester was found to have been formed at a yield of 99.1%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0169]

15 Step (11-2): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(2-ethylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 206 in step (11-1) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 790 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 21.9 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 160°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 160°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 112 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 182 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by

weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 88.2%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0170]

[Example 12]

Step (12-1): Production of 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic Acid (3-methylbutyl) Ester

10 A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3224 g (16.0 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1, 647 g (3.8 mol) of 3-aminomethyl-3,5,5-trimethylcyclohexylamine instead of hexamethylene diamine, and 7.3 g of sodium methoxide (28% methanol solution). As a result of analyzing
15 the solution following the reaction by liquid chromatography, 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic acid (3-methylbutyl) ester was found to have been formed at a yield of 98.8%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by
20 removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0171]

Step (12-2): Removal of Low Boiling Point Component

25 Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid

state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 48 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 232 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 237 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of the continuous multistage distillation column 402 was 200°C, and the pressure at the top of the column was about 7.9 kPa. Gas distilled from the top of the continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 123 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 109 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 84.0% by weight of

3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic acid
(3-methylbutyl) ester.

[0172]

Step (12-3): Production of Isocyanate by Thermal Decomposition of
5 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic Acid
(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1
m² was heated to 270°C and the pressure within was set to be about 13 kPa. The
10 mixture recovered into storage tank 406 in step (12-2) was heated to 170°C and
supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about
200 g/hr. In addition, dibutyl tin dilaurate (Wako Pure Chemical Industries, Ltd.,
Japan) was fed from line 51 at the rate of about 25.2 g/hr. A liquid phase
component was extracted from the bottom of thin film distillation apparatus 501 via
15 line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54.
A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus
501 via line 52 was continuously fed to the middle stage of continuous multistage
distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an
20 inner diameter of 5 cm and column length of 2 m to carry out distillative separation of
the gaseous phase component. The amount of heat required for distillative
separation was supplied by circulating the liquid in the bottom of the column through
line 56 and reboiler 504. The liquid temperature in the bottom of continuous
multistage distillation column 502 was 150°C, and the pressure at the top of the
25 column was about 50 kPa. Gas distilled from the top of continuous multistage
distillation column 502 was condensed in condenser 503 via line 55 and continuously

extracted from line 57. A gaseous phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The gaseous phase component extracted from line 59 was continuously fed to middle stage of continuous multistage distillation column 505 packed with Dickson
5 packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid
10 temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 90.0 g/hr.

After operating for 40 hours, a liquid phase component was extracted into
15 storage tank 510 from line 64 at the rate of about 44 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of isophorone diisocyanate. The yield based on hexamethylene diamine was 81.5%.

Although continuous operation was carried out for 10 days, there was no
20 accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0173]

[Example 13]

Step (13-1): Production of N,N'-hexanediyl-bis-carbamic Acid
25 Bis(2-ethylhexyl) Ester

A process was carried out in the same manner as step (1-1) of Example 1 with

the exception of carrying out the reaction by supplying 3609 g (12.6 mol) of the bis(2-ethylhexyl) carbonate of Reference Example 5 instead of bis(3-methylbutyl) carbonate, 349 g (3.0 mol) of hexamethylene diamine and 5.8 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanedyl-bis-carbamic acid bis(2-ethylhexyl) ester was found to have been formed at a yield of 98.5%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0174]

Step (13-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 300 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 13 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 58 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 242 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner
5 diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 219 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 210°C, and the pressure at the top of the column was about 0.13 kPa. Gas distilled from
10 the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 145 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 98 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid
15 chromatography, the mixture was found to contain about 73.9% by weight of N,N'-hexanediyl-bis-carbamic acid bis(2-ethylhexyl) ester.

[0175]

Step (13-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(2-ethylhexyl) Ester

20 A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (13-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about
25 270 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 22.7 g/hr. A liquid phase component was extracted from the bottom of thin film

distillation apparatus 501 via line 53, and circulated to the top of the thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of the continuous multistage distillation column 502 was 160°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of the continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of the continuous multistage distillation column 505 was 160°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 75.1 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 82 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 70.9%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of the thin film distillation apparatus 501.

[0176]

10 [Example 14]

Step (14-1): Production of N,N'-hexanediyl-bis-carbamic Acid Dibutyl Ester

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3293 g (18.9 mol) of the dibutyl carbonate of Reference Example 2 instead of bis(3-methylbutyl) carbonate, 523 g (4.5 mol) of hexamethylene diamine and 8.7 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid di(n-butyl) ester was found to have been formed at a yield of 98.8%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0177]

25 Step (14-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 290 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 150°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 50 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 240 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 240 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 150°C, and the pressure at the top of the column was about 1.3 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 132 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 108 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid

chromatography, the mixture was found to contain about 98.5% by weight of N,N'-hexanediyl-bis-carbamic acid di(n-butyl) ester.

[0178]

Step (14-3): Production of Isocyanate by Thermal Decomposition of

5 N,N'-hexanediyl-bis-carbamic Acid Di(n-butyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (14-2) was heated to 170°C and
10 supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 260 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 25.6 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

15 The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative
20 separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 160°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously
25 extracted from line 57. A gaseous phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The gaseous phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component.

5 The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 160°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506
10 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 75.1 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 104 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by
15 weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 75.1%.

When continuous operation was carried out for 48 hours, there was accumulation of adhered substances observed on the walls of the top and sides of thin film distillation apparatus 501.

20 [0179]

[Example 15]

Step (15-1): Production of N,N'-hexanediyl-bis-carbamic Acid
Bis(3-methylbutyl) Ester

An apparatus was used like that shown in FIG. 10.

25 A mixture of 639 g (5.5 mol) of hexamethylene diamine and 64 g of water was supplied to baffled reaction vessel 1004 made of SUS and having an inner volume of

5 L from storage tank 1001 via line D1 with line D4 closed. The liquid temperature inside reaction vessel 1004 was adjusted to be about 80°C, and the pressure inside reaction vessel 1004 was reduced to 30 kPa to distill off the water. The water was condensed in condenser 1007 and extracted via line D6.

5 3333 g (16.5 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1 were supplied from storage tank 1002 to reaction vessel 1004 via line D2, and the liquid temperature inside reaction vessel 1004 was adjusted to about 80°C. 6.4 g of sodium methoxide (28% methanol solution, Wako Pure Chemical Industries, Ltd., Japan) were supplied from storage tank 1003 to SUS reaction vessel 1004 via line
10 D3 to carry out a reaction.

As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester was found to have been formed at a yield of 99.7%.

After opening line D4, the reaction liquid was supplied to column 1005 which
15 was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 1006 via line D5.

[0180]

20 Step (15-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 1006 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner
25 diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the

liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 67 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 213 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 213 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of the continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 78 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 135 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.2% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

[0181]

Step (15-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 (Kobelco Eco-Solutions Co., Ltd., Japan) having a heat-conducting surface area of 0.1 m^2 was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (15-2) was heated to 160°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr. In addition, dibutyl tin dilaurate (Wako Pure Chemical Industries, Ltd., Japan) was fed from line 51 at the rate of about 25.2 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and circulated to the top of thin film distillation apparatus 501 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 150°C , and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of

2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 131 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 11 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 97.2%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of thin film distillation apparatus 501.

[0182]

[Example 16]

Step (16-1): Production of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

Bis(3-methylbutyl) carbonate of Reference Example 1 was placed in pear-shaped flask having an internal volume of 10 L, a three-way valve, distillation column packed with Helipak No. 3, fractionating column equipped with a reflux condenser and coupled to a distillate collector, and thermometer were attached to the pear-shaped flask and the inside of the system was replaced with nitrogen in a vacuum to carry out distillative purification of the bis(3-methylbutyl) carbonate. The

flask was cooled to terminate distillative purification when distillate equal to about two-thirds the charged amount was obtained. When $^1\text{H-NMR}$ measurement was carried out on the distillative purification product, it was found to contain about 99.9% by weight of bis(3-methylbutyl) carbonate. In addition, metal atoms in the form of iron, cobalt, nickel, zinc, tin, copper and titanium contained in the distillate were below the detection limit (0.001 ppm).

A process was carried out in the same manner as step (1-1) of Example 1 with the exception of carrying out the reaction by supplying 3535 g (17.5 mol) of the recovered distillate in the form of bis(3-methylbutyl) carbonate, 407 g (3.5 mol) of hexamethylene diamine, and 6.8 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis carbamic acid bis(3-methylbutyl) ester was found to have been formed at a yield of 94.0%.

Line 24 was opened and the reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0183]

* Step (16-2): Removal of Low Boiling Point Component

A process was carried out in the same manner as step (1-2) of Example 1 with the exception of continuously feeding the mixture recovered into storage tank 206 in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 from line 31 at the rate of about 280 g/hr, continuously extracting a liquid phase component from the bottom of the column to storage tank 306 via line 33 at the rate of about 239 g/hr, and continuously feeding the mixture

recovered into storage tank 306 in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 from line 41 at the rate of about 239 g/hr. Gas distilled from the top of the continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 157 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 82 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.4% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

[0184]

Step (16-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 (Kobelco Eco-Solutions Co., Ltd., Japan) having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. A process was carried out in the same manner as step (1-3) of Example 1 with the exception of heating the mixture recovered into storage tank 406 in step (16-2) to 200°C, supplying to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr, and feeding dibutyl tin dilaurate from line 51 at the rate of about 25.3 g/hr. A liquid was extracted into storage tank 509 via line 62 at the rate of about 131 g/hr.

After operating for 40 hours, the liquid phase component was extracted into storage tank 510 from line 64 at the rate of about 77 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine

was 91.7%.

Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of thin film distillation apparatus 501.

5 [0185]

[Example 17]

Step (17-1): Production of N,N'-hexanediyl-bis-carbamic Acid
Bis(3-methylbutyl) Ester

Ferrous acetylacetonate was added to the bis(3-methylbutyl) carbonate of
10 Reference Example 1 to prepare bis(3-methylbutyl) carbonate having a metal atom
content in the form of iron of 11%. The same process as that of step (1-1) of
Example 1 was carried out with the exception of supplying 3434 g (17.0 mol) of the
bis(3-methylbutyl) carbonate, 395 g (3.5 mol) of hexamethylene diamine and 6.6 g of
sodium methoxide (28% methanol solution). As a result of analyzing the solution
15 following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid
bis(3-methylbutyl) ester was found to have been formed at a yield of 92.0%.

Line 24 was opened and the reaction liquid was supplied to column 205 which
was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and
Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C
20 by an external jacket so as to neutralize the sodium methoxide. The solution was
then transferred to storage tank 206 via line 25.

[0186]

Step (17-2): Removal of Low Boiling Point Component

A process was carried out in the same manner as step (1-2) of Example 1 with
25 the exception of continuously feeding the mixture recovered into storage tank 206 in
a liquid state through preheater 301 to the middle stage of continuous multistage

distillation column 302 from line 31 at the rate of about 280 g/hr, continuously extracting a liquid phase component from the bottom of the column to storage tank 306 via line 33 at the rate of about 240 g/hr, and continuously feeding the mixture recovered into storage tank 306 in a liquid state through preheater 401 to the middle
5 stage of continuous multistage distillation column 402 from line 41 at the rate of about 240 g/hr. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 160 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the
10 rate of about 80 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.1% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

[0187]

15 Step (17-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 (Kobelco Eco-Solutions Co., Ltd., Japan) having a heat-conducting surface area of 0.1 m² was heated to 270°C and the
20 pressure within was set to be about 13 kPa. A process was carried out in the same manner as step (1-3) of Example 1 with the exception of heating the mixture recovered into storage tank 406 in step (17-2) to 200°C, supplying to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr, and feeding dibutyl tin dilaurate from line 51 at the rate of about 25.2 g/hr. A liquid was extracted
25 into storage tank 509 via line 62 at the rate of about 127 g/hr.

After operating for 40 hours, the liquid phase component was extracted into

storage tank 510 from line 64 at the rate of about 85 g/hr.

The liquid extracted from line 62 was a solution that contained about 99.8% by weight of hexamethylene diisocyanate. The yield based on hexamethylene diamine was 87.5%.

5 Although continuous operation was carried out for 10 days, there was no accumulation of adhered substances observed on the walls of thin film distillation apparatus 501.

[0188]

[Example 18]

10 Step (18-1): Production of N,N'-hexanediyl-bis-carbamic Acid Bis(3-methylbutyl) Ester

The same process as that of step (1-1) of Example 1 was carried out with the exception of supplying 2969 g (14.7 mol) of the bis(3-methylbutyl) carbonate of Reference Example 1, 488 g (4.2 mol) of hexamethylene diamine and 8.1 g of
15 sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester was found to have been formed at a yield of 99.1%.

Line 24 was opened and the reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and
20 Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0189]

Step (18-2): Removal of Low Boiling Point Component

25 A process was carried out in the same manner as step (1-2) of Example 1 with the exception of continuously feeding the mixture recovered into storage tank 206 in

a liquid state through preheater 301 to middle stage of continuous multistage distillation column 302 from line 31 at the rate of about 300 g/hr, continuously extracting a liquid phase component from the bottom of the column to storage tank 306 via line 33 at the rate of about 221 g/hr, and continuously feeding the mixture
5 recovered into storage tank 306 in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 from line 41 at the rate of about 221 g/hr. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 104 g/hr. Liquid was continuously
10 extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 117 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 98.7% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

15 [0190]

Step (18-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Diphenyl Ester

A reaction was carried out using an apparatus like that shown in FIG. 11.

Reaction vessel 1104 made of SUS and having the same shape as SUS
20 reaction vessel 202 of FIG. 2 was heated to 270°C and the pressure within was set to be about 13 kPa. The N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester extracted into storage tank 406 in step (18-2) was supplied to reaction vessel 1104 at the rate of 280 g/hr, and dibutyl tin dilaurate was simultaneously supplied from storage tank 1102 via line E2 to reaction vessel 1104 at the rate of 25.3 g/hr. A
25 gaseous phase component was extracted from line E4, and the gaseous phase component was continuously fed to the middle stage of continuous multistage

distillation column 1105 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through
5 line E6 and reboiler 1108. The liquid temperature in the bottom of continuous multistage distillation column 1105 was 150°C, and the pressure at the top of the column was about 15 kPa. Gas distilled from the top of continuous multistage distillation column 1102 was condensed in condenser 1107 via line E5 and continuously extracted from line E7. A liquid phase component was extracted from
10 line E9 of continuous multistage distillation column 1105 at a location lower than line E4.

The liquid phase component extracted from line E9 was continuously fed to the middle stage of continuous multistage distillation column 1106 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of
15 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line E11 and reboiler 1112. The liquid temperature in the bottom of continuous multistage distillation column 1106 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of
20 continuous multistage distillation column 1106 was condensed in condenser 1110 via line E10 and continuously extracted into storage tank 1111 via line E12 at the rate of about 88 g/hr. The liquid recovered into storage tank 1111 was a solution that contained about 99.8% by weight of hexanediyl diisocyanate. The yield based on hexamethylene diamine was 64.4%.

25 When continuous operation was carried out for 10 hours, there was accumulation of adhered substances observed on the walls of reaction vessel 1104.

[0191]

[Example 19] Cleaning of Reaction Vessel

A cleaning procedure was carried out on thin film distillation apparatus 701 in which accumulation of adhered substance was observed in Example 4. Thin film
5 distillation apparatus 701 was heated to 180°C and the inside of thin film distillation apparatus 701 was replaced with a nitrogen atmosphere at atmospheric pressure. Phenol was supplied from line 70 at the rate of about 1200 g/hr, extracted from line 83 and a liquid phase component was recovered from line 89 into storage tank 711. When this procedure was carried out for 1 hour, adhered substance was not
10 observed on the inside of thin film distillation apparatus 701.

[0192]

[Examples 20 to 27]

The procedure of Example 4 was carried out continuously and various cleaning solvents were used every 30 days to carry out the cleaning procedure using the
15 same method as Example 19. Those results are shown in Table 1.

[0193]

[Comparative Example 1]

Step (A-1): Production of N,N'-hexanediyl-bis-carbamic Acid
Bis(3-methylbutyl) Ester

20 A reaction was carried out using an apparatus like that shown in FIG. 9.

2909 g (14.4 mol) of bis(3-methylbutyl) carbonate of Reference Example 1 were supplied to baffled reaction vessel 904 made of SUS and having an inner volume of 5 L from storage tank 901 via line C1 with lines C4 and C6 closed, and 349 g (3.0 mol) of hexamethylene diamine were supplied to reaction vessel 904 from storage tank
25 902 via line C2. The liquid temperature inside reaction vessel 904 was adjusted to about 80°C, and 8.7 g of sodium methoxide (28% methanol solution) were supplied

to reaction vessel 904 made of SUS from storage tank 903 via line C3 to carry out a reaction.

As a result of analyzing the solution following the reaction by liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester was
5 found to have been formed at a yield of 99.0%.

Line C4 was opened and the reaction liquid was supplied to column 905 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was
10 then transferred to storage tank 906 via line C5.

[0194]

Step (A-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 906 was continuously fed in a liquid
15 state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for the reaction and distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304.
20 The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 44 g/hr. Liquid was continuously extracted from the
25 bottom of the column through line 33 into storage tank 306 at the rate of about 236 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 236 g/hr. The amount of heat required for the reaction and distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 146 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 90 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 97.6% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

[0195]

Step (A-3): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis (3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

After closing line 54, thin film distillation apparatus 501 (Kobelco Eco-Solutions Co., Ltd., Japan) having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (A-2) was heated to 160°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr. In

addition, dibutyl tin dilaurate (Wako Pure Chemical Industries, Ltd., Japan) was fed from line 51 at the rate of about 25.1 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and recovered in storage tank 510 via line 54. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 150°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of the continuous multistage distillation column 505 was condensed in condenser 506 via

line 60 and continuously extracted into storage tank 509 via line 62.

[0196]

Step (A-4): Continuous Production of Carbamic Acid Ester

Production of carbamic acid ester was continuously carried out using an
5 apparatus like that shown in FIG. 9.

About 220 g of the mixture extracted from storage tank 510 were supplied to
reaction vessel 904 via line C5 with line C4 closed, 2909 g (14.4 mol) of
bis(3-methylbutyl) carbonate were supplied to baffled reaction vessel 904 made of
SUS and having an inner volume of 5 L from storage tank 901 via line C1, and 349 g
10 (3.0 mol) of hexamethylene diamine were supplied to the reaction vessel 904 from
storage tank 902 via line C2. The liquid temperature inside the reaction vessel 904
was adjusted to about 80°C, and 8.7 g of sodium methoxide (28% methanol solution)
were supplied to reaction vessel 904 made of SUS from storage tank 903 via line C3
to carry out a reaction. As a result of analyzing the solution following the reaction by
15 liquid chromatography, N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester
was found to have been formed at a yield of 92.0% based on the supplied
hexamethylene diamine.

Line C4 was opened and the reaction liquid was supplied to column 905 which
was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and
20 Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C
by an external jacket so as to neutralize the sodium methoxide. The solution was
then transferred to storage tank 906 via line C5.

[0197]

Step (A-5): Removal of Low Boiling Point Component

25 Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid

state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for the reaction and distillation was supplied
5 by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from
10 line 34 at the rate of about 39 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 241 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid
15 state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 241 g/hr. The amount of heat required for the reaction and distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404.
20 The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 144 g/hr. Liquid was continuously extracted from the
25 bottom of the column through line 43 into storage tank 406 at the rate of about 97 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 94.3% by weight of N,N'-hexanediyl-bis-carbamic acid bis(3-methylbutyl) ester.

[0198]

5 Step (A-6): Production of Isocyanate by Thermal Decomposition of N,N'-hexanediyl-bis-carbamic Acid Bis (3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

After closing line 54, thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m^2 was heated to 270°C and the pressure within
10 was set to be about 13 kPa. The mixture recovered into storage tank 406 in step (A-5) was heated to 160°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 280 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about 24.2 g/hr. A liquid phase component was extracted from the bottom of thin film distillation apparatus 501 via line 53, and recovered in
15 storage tank 510 via line 64. A gaseous phase component was extracted from line 52.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an
20 inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of the continuous multistage distillation column 502 was 150°C , and the pressure at the top of the
25 column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously

extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The liquid phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson
5 packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the liquid phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure
10 at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. Liquid was recovered from line 62 at the rate of about 38.7 g/hr, and the liquid contained about 99.8% by weight of hexamethylene diisocyanate.

15 When operation was carried out continuously for 10 days by repeating steps (A-4) to (A-6) above, accumulation of adhered substances was observed on the walls of reaction vessel 904, column 905, storage tank 906, thin film distillation apparatus 501, storage tank 510 and lines connecting these components.

[0199]

20 [Comparative Example 2]

Step	(B-1):	Production	of
		3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic	Acid
		(3-methylbutyl) Ester	

A process was carried out in the same manner as step (1-1) of Example 1 with
25 the exception of carrying out the reaction by supplying 3394 g (16.8 mol) of bis(3-methylbutyl) carbonate of Reference Example 1, 596 g (3.5 mol) of

3-aminomethyl-3,5,5-trimethylcyclohexylamine instead of hexamethylene diamine and 6.8 g of sodium methoxide (28% methanol solution). As a result of analyzing the solution following the reaction by liquid chromatography, 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic acid (3-methylbutyl) ester was found to have been formed at a yield of 99.5%. The reaction liquid was supplied to column 205 which was packed with an acidic ion exchange resin (Amberlyst-15, spherical, Rohm and Haas Co., USA) adjusted by removing the moisture and which was warmed to 80°C by an external jacket so as to neutralize the sodium methoxide. The solution was then transferred to storage tank 206 via line 25.

[0200]

Step (B-2): Removal of Low Boiling Point Component

Alcohol was removed using an apparatus like that shown in FIG. 3.

The mixture recovered into storage tank 206 was continuously fed in a liquid state through preheater 301 to the middle stage of continuous multistage distillation column 302 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 31 at the rate of about 280 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 33 and reboiler 304. The liquid temperature in the bottom of continuous multistage distillation column 302 was 160°C, and the pressure at the top of the column was about 70 kPa. Gas distilled from the top of continuous multistage distillation column 302 was condensed in condenser 303 via line 32 and continuously extracted into storage tank 305 from line 34 at the rate of about 43 g/hr. Liquid was continuously extracted from the bottom of the column through line 33 into storage tank 306 at the rate of about 237 g/hr.

Carbonic acid ester was removed using an apparatus like that shown in FIG. 4.

The mixture recovered into storage tank 306 was continuously fed in a liquid state through preheater 401 to the middle stage of continuous multistage distillation column 402 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of about 5 cm and column length of 2 m from line 41 at the rate of about 237 g/hr. The amount of heat required for distillation was supplied by circulating the liquid in the bottom of the column through line 43 and reboiler 404. The liquid temperature in the bottom of continuous multistage distillation column 402 was 160°C, and the pressure at the top of the column was about 2.6 kPa. Gas distilled from the top of continuous multistage distillation column 402 was condensed in condenser 403 via line 42 and continuously extracted into storage tank 405 from line 44 at the rate of about 138 g/hr. Liquid was continuously extracted from the bottom of the column through line 43 into storage tank 406 at the rate of about 98 g/hr.

As a result of analyzing the mixture extracted into storage tank 406 by liquid chromatography, the mixture was found to contain about 99.0% by weight of 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic acid (3-methylbutyl) ester.

[0201]

Step (B-3): Production of Isocyanate by Thermal Decomposition of 3-((3-methylbutyloxy)carbonylamino-methyl-3,5,5-trimethylcyclohexylcarbamic Acid (3-methylbutyl) Ester

A reaction was carried out using an apparatus like that shown in FIG. 5.

Thin film distillation apparatus 501 having a heat-conducting surface area of 0.1 m² was heated to 270°C and the pressure within was set to be about 0.13 kPa. The mixture recovered into storage tank 406 in step (B-2) was heated to 170°C and supplied to the top of thin film distillation apparatus 501 via line 50 at the rate of about 200 g/hr. In addition, dibutyl tin dilaurate was fed from line 51 at the rate of about

25.2 g/hr, and a gaseous phase component was extracted from line 52. Hardly any liquid phase component was recovered from the bottom of thin film distillation apparatus 501.

The gaseous phase component extracted from thin film distillation apparatus 501 via line 52 was continuously fed to the middle stage of continuous multistage distillation column 502 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 56 and reboiler 504. The liquid temperature in the bottom of continuous multistage distillation column 502 was 150°C, and the pressure at the top of the column was about 50 kPa. Gas distilled from the top of continuous multistage distillation column 502 was condensed in condenser 503 via line 55 and continuously extracted from line 57. A liquid phase component was extracted from line 59 of continuous multistage distillation column 502 at a location lower than line 52.

The gaseous phase component extracted from line 59 was continuously fed to the middle stage of continuous multistage distillation column 505 packed with Dickson packing (diameter: 6 mm) and having an inner diameter of 5 cm and column length of 2 m to carry out distillative separation of the gaseous phase component. The amount of heat required for distillative separation was supplied by circulating the liquid in the bottom of the column through line 61 and reboiler 507. The liquid temperature in the bottom of continuous multistage distillation column 505 was 150°C, and the pressure at the top of the column was about 1.5 kPa. Gas distilled from the top of continuous multistage distillation column 505 was condensed in condenser 506 via line 60 and continuously extracted into storage tank 509 via line 62. The extracted amount in the steady state was about 101 g/hr.

The liquid extracted from line 62 was a solution containing about 99.8% by weight of isophorone diisocyanate. The yield based on hexamethylene diamine was 91.5%.

When continuous operation was carried out for 24 hours, accumulation of an adhered substance was observed on the walls of thin film distillation apparatus 501.

[0202]

[Comparative Examples 3 to 5]

The procedure of Example 4 was carried out continuously and various cleaning solvents were used every 30 days to carry out the cleaning procedure using the same method as Example 15. Those results are shown in Table 1.

[0203]

[Table 1]

Table 1 Results of Carrying Out Cleaning Procedure

	Temperature in thin film distillation apparatus	Cleaning solvent	Cleaning solvent supply rate	Cleaning time	Results
Example 20	200°C	2,6-dimethylphenol	1000 g/hr	2 hr	O
Example 21	210°C	2,4,6-trimethylphenol	800 g/hr	2 hr	O
Example 22	250°C	2-phenylphenol	1000 g/hr	3 hr	O
Example 23	280°C	2,4(α,α -dimethylbenzyl) phenol	1200 g/hr	1 hr	O
Example 24	200°C	4-ethoxyphenol	1100 g/hr	2 hr	O
Example 25	270°C	4-dodecylphenol	1300 g/hr	1 hr	O
Example 26	200°C	Salicylic acid	800 g/hr	2 hr	O
Example 27	220°C	Benzoic acid	800 g/hr	4 hr	O
Comp. Ex. 3	200°C	n-dodecane	1000 g/hr	4 hr	×
Comp. Ex. 4	200°C	Naphthalene	1000 g/hr	4 hr	×
Comp. Ex. 5	180°C	1-phenyl ethanol	1000 g/hr	4 hr	×

O: Adhered substances not observed after cleaning procedure

×: Adhered substances observed after cleaning procedure

Industrial Applicability

[0204]

Since the isocyanate production process according to the present invention enables isocyanate to be efficiently produced without using highly toxic phosgene, 5 the production process of the present invention is highly useful industrially and has high commercial value.

CLAIMS

I (We) claim:

1. A process for producing an isocyanate by subjecting a carbamic acid ester
5 to a thermal decomposition reaction, comprising the steps of:

recovering a low boiling point component in a form of a gaseous phase
component from a thermal decomposition reaction vessel in which the thermal
decomposition reaction is carried out;

recovering a liquid phase component containing the carbamic acid ester from a
10 bottom of the thermal decomposition reaction vessel; and

supplying all or a portion of the liquid phase component to an upper portion of
the thermal decomposition reaction vessel.

2. The process according to Claim 1, wherein the carbamic acid ester is
15 supplied to the thermal decomposition reaction vessel within a temperature range of
from 50 to 180°C.

3. The process according to Claim 1, wherein the carbamic acid ester is
supplied to the thermal decomposition reaction vessel in a form of a liquid.

20 4. The process according to Claim 1, wherein the carbamic acid ester is a
carbamic acid ester produced by reacting a carbonic acid ester with an amine
compound.

25 5. The process according to Claim 4, wherein the reaction vessel for
producing the carbamic acid ester and the thermal decomposition reaction vessel

may be the same or different, and the reaction vessel for producing the carbamic acid ester and the thermal decomposition reaction vessel are at least one reaction vessel selected from the group consisting of a column-type reaction vessel and a tank-type reaction vessel.

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6. The process according to Claim 1, wherein the thermal decomposition reaction vessel is composed of at least one reaction vessel selected from the group consisting of an evaporator, a continuous multistage distillation column, a packed column, a thin film evaporator and a falling film evaporator.

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7. The process according to Claim 1, wherein the thermal decomposition reaction is carried out in a liquid phase.

8. The process according to Claim 4, wherein a mixture, in which all or a
15 portion of a hydroxy compound and / or all or a portion of the carbonic acid ester has been separated from a mixture containing the carbamic acid ester produced by reacting a carbonic acid ester and an amine compound, is supplied to a thermal decomposition reaction apparatus.

20 9. The process according to Claim 8, wherein the separation is carried out by distillative separation, and the distillative separation is carried out at 180°C or lower.

10. The process according to Claim 1, wherein all or a portion of the liquid
phase component recovered from the bottom of the thermal decomposition reaction
25 vessel is supplied to the upper portion of the thermal decomposition reaction vessel within a temperature range of from 50 to 180°C.

11. The process according to Claim 4, wherein the carbonic acid ester is used at a stoichiometric ratio of 1 time or more based on amino groups constituting the amine compound.

5

12. The process according to Claim 1, further comprising cleaning a high boiling point by-product adhered to the thermal decomposition reaction vessel, with an acid.

10 13. The process according to Claim 12, wherein the acid is an aromatic hydroxy compound.

14. The process according to Claim 4, wherein the carbonic acid ester is a compound represented by the following formula (1):



(wherein R¹ represents an aliphatic group having 1 to 12 carbon atoms or an aromatic group having 6 to 12 carbon atoms).

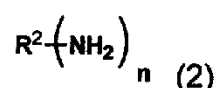
15. The process according to Claim 14, wherein the carbonic acid ester
20 contains a metal atom at from 0.001 ppm to 10%.

16. The process according to Claim 15, wherein the metal atom is one type or a plurality of types of metal atoms selected from the group consisting of iron, nickel, cobalt, zinc, tin, copper and titanium atoms.

25

17. The process according to Claim 14, wherein R¹ in the carbonic acid ester represents an aliphatic group having 5 to 7 carbon atoms or an aromatic group having 6 to 7 carbon atoms.

5 18. The process according to Claim 4, wherein the amine compound is a compound represented by the following formula (2):



(wherein R² represents a group selected from the group consisting of an aliphatic group having 1 to 20 carbon atoms and an aromatic group having 6 to 20 carbon
10 atoms, the above group containing an atom selected from carbon and oxygen atoms, and having a valence equal to n, and

n represents an integer of from 2 to 10).

19. The process according to Claim 18, wherein the amine compound is a
15 diamine compound represented by formula (2) in which n is 2.

20. The process according to Claim 1, wherein a low boiling point component is supplied to a distillation column in a form of a gaseous component from the low boiling point component formed by the thermal decomposition reaction and
20 recovered in a form of a gaseous phase component, and a hydroxy compound originating from the carbamic acid ester and an isocyanate originating from the carbamic acid ester are separated in the distillation column.

21. The process according to Claim 1, wherein a hydroxy compound
25 originating from the carbamic acid ester and an isocyanate originating from the

carbamic acid ester are recovered separately from a low boiling point component formed by the thermal decomposition reaction and recovered in a form of a gaseous component by a thin film evaporator.

5 22. The process according to Claim 1, wherein the isocyanate is recovered from the liquid phase component by distillative separation.

23. The process according to Claim 14, wherein R^1 in the carbonic acid ester in formula (1) represents an aliphatic group having 1 to 12 carbon atoms, and the
10 carbonic acid ester is produced according to a process which comprises the following steps (1) and (2):

step (1): obtaining a reaction mixture containing a dialkyl carbonate by reacting an organic tin compound having a tin-oxygen-carbon bond and carbon dioxide; and

step (2): obtaining a dialkyl carbonate and a residue liquid by separating the
15 reaction mixture.

24. The process according to Claim 14, wherein R^1 in the carbonic acid ester in formula (1) represents an aromatic group having 6 to 12 carbon atoms, and the carbonic acid ester is produced according to a process which comprises the following
20 step (3) in addition to the steps (1) and (2):

step (3): obtaining a diaryl carbonate by reacting the dialkyl carbonate separated in step (2) and an aromatic hydroxy compound A followed by recovering a by-product alcohol.

25 25. The process according to Claim 23 or 24, wherein the carbonic acid ester is a carbonic acid ester produced by a process which comprises the following steps

(4) and (5) in addition to the steps (1) and (2) or the steps (1) to (3):

step (4): forming an organic tin compound having a tin-oxygen-carbon bond and water by reacting the residue liquid obtained in step (2) with an alcohol followed by removing the water from a reaction system; and

5 step (5): reusing the organic tin compound having the tin-oxygen-carbon bond obtained in step (4) as the organic tin compound having the tin-oxygen-carbon bond of step (1).

26. The process according to Claim 25, wherein the alcohol recovered in step
10 (3) is reused as the alcohol of step (4).

27. The process according to Claim 25, wherein in the case the hydroxy
compound is an alcohol, it is used as the alcohol of step (4), while in the case the
hydroxy compound is an aromatic hydroxy compound, it is used as the aromatic
15 hydroxy compound A of step (3).

28. The process according to Claim 8, wherein the separated carbonic acid
ester is reused as a carbonic acid ester.

20 29. The process according to Claim 1, wherein the thermal decomposition
reaction of the carbamic acid ester is carried out in the absence of a solvent.

30. The process according to Claim 4, wherein supply of the amine compound
to the reaction vessel in which the carbonic acid ester and the amine compound are
25 reacted is carried out in a liquid state.

31. The process according to Claim 4, wherein supply of the amine compound to the reaction vessel in which the carbonic acid ester and the amine compound are reacted is carried out in a form of a mixture with alcohol, water or carbonic acid ester.