

Acrylate-olefin copolymers as high viscosity base fluids

TECHNICAL FIELD OF THE INVENTION

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The invention relates to acrylate-olefin copolymers and to a method for the preparation of these polymers. The present invention is also directed to lubricant compositions comprising these copolymers, as well as to the use of these copolymers as a lubricant additive or a synthetic base fluid in a lubricating oil composition, preferably in a gear oil composition, a transmission oil composition, a hydraulic oil composition, an engine oil composition, a marine oil composition, an industrial lubricating oil composition or in grease.

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BACKGROUND OF THE INVENTION

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The present invention relates to the field of lubrication. Lubricants are compositions that reduce friction between surfaces. In addition to allowing freedom of motion between two surfaces and reducing mechanical wear of the surfaces, a lubricant also may inhibit corrosion of the surfaces and/or may inhibit damage to the surfaces due to heat or oxidation. Examples of lubricant compositions include, but are not limited to, engine oils, transmission fluids, gear oils, industrial lubricating oils, greases and metalworking oils.

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Lubricants typically contain a base fluid and variable amounts of additives. Conventional base fluids are hydrocarbons, such as mineral oils. The terminology base oil or base fluid is commonly used interchangeably. Here, base fluid is used as a general term.

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A wide variety of additives may be combined with the base fluid, depending on the intended use of the lubricant. Examples of lubricant additives include, but are not limited to, viscosity index improvers, thickeners, oxidation inhibitors, corrosion inhibitors, dispersing agents, high pressure additives, anti-foaming agents and metal deactivators.

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Typical non-polymeric base fluids are less effective as lubricants, because of their low viscosity and further decreased viscosity at higher operating temperatures. Therefore, polymeric additives are used to thicken the base oil and reduce the change in viscosity with change in temperature. The term Viscosity Index (VI) is used to describe this change in viscosity with temperature. The lower the VI, the greater the change in viscosity with temperature, and vice versa. Thus, a high VI is desired for lubricant formulations. In order to improve VI, polymeric additives or Viscosity Index Improvers (VII) may be added to a lubricant formulation.

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It is well-known in the art that alkyl acrylates are not recommended in VI improver application, and

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commercial VI improvers are based on methacrylates. While literature (Rashad et al. J. of Petr. Sci. and Engineering 2012, 173-177; Evin et al. J. of Sol. Chem 1994, 325-338) and patents (WO 96/17517) exist, it is generally known that the performance of polyacrylates as VI improver is inferior to the ones of polymethacrylates. Especially in WO 96/17517 it is mentioned that it was unexpectedly found that poly(alkyl acrylate) esters typically fail to adequately reduce the effect of temperature on viscosity when used in the hydraulic fluids.

The drawback of adding polymeric additives to a lubricant formulation is that they will undergo shear stress and will mechanically degrade over time. Higher molecular weight polymers are better thickeners but will be more prone to shear stress leading to polymer degradation. In order to decrease the amount of polymer degradation, the molecular weight of a polymer can be decreased, thereby obtaining a more shear stable polymer. These shear stable low molecular weight polymers are no longer very effective thickeners and must be used in larger concentrations in the lubricant in order to reach a desired viscosity. These low molecular weight polymers typically have molecular weights below 20,000 g/mol and are also called synthetic high viscosity base fluids. High viscosity base fluids are used to lift the VI and to thicken lubricant formulations with demanding shear stability requirements. A typical application are gear oils which have very demanding requirements due high mechanical stress and a broad temperature range in operation.

Typical products in this market are high viscosity polyalphaolefins (PAOs) and metallocene polyalphaolefins (mPAOs), typically sold in viscosity ranges from 40 to 300 cSt at 100°C (Choudary et al. Lubr. Sci. 2012, 23-44), whose key feature is good handling properties in term of viscosity since these base fluids are polymeric in nature and provide for an improved viscosity index. However, their weakness is the low polarity. Due to the apolar nature of PAO base oils DI packages and ageing products are poorly dissolved in the oil causing various problems.

It has been already described that higher polarity is provided by copolymers of alpha-olefins with maleates (DE3223694), copolymers of alpha-olefins and acrylates (DE2243064), copolymers of alpha-olefins and methacrylates (EP0471266) or terpolymers based on the aforementioned monomers (WO2020078770). Alternatively, oil compatible polyesters (WO0146350), poly alkyl(meth)acrylates (DE102010028195) or polyvinylethers (US20130165360) can be applied. A big advantage when polar high viscosity base fluids are used is that no polar low viscous fluids, such as esters, must be used as compatibilizers for the polar lubricant additives. Polar low viscous fluids are known to cause problems with coatings and seals which is less of an issue for high viscosity fluids.

Existing products, such as polyalphaolefins (PAOs), do not have the necessary performance level for some applications. There is also a need to provide alternative solutions in the area of industrial gear oils and not only for industrial lubricants. In particular, it would be desirable to replace existing high viscosity polyalphaolefins, as these products are expensive, and do not provide sufficient solubility for crucial formulation components.

It was therefore an object of the present invention to provide highly shear stable synthetic base fluids or lubricating oil additives, which, in lubricant oil compositions, have a positive influence on oil solubility and component solubility, as well as on low temperature performance. Furthermore, these new polymers should be able to thicken an oil to a desired viscosity. These highly shear stable polymers should also have a high viscosity index, high flash point, and good thermo-oxidative stability.

BRIEF SUMMARY OF THE INVENTION

The inventors of the present invention have surprisingly found that acrylate-olefin copolymers as defined in claim 1 are useful as highly shear stable lubricating oil additives or synthetic base fluids, depending on their treatment rate in the lubricating composition. The acrylate-olefin copolymers according to the invention have a higher viscosity index than their methacrylate counterparts as exemplified in the experimental part of the present invention, which was unexpected. The inventors of the present invention have found that the side chains of the resulting polymer which are derived from the acrylate monomer, but also from the α -olefin are crucial to achieve a combination of high VI and good low temperature properties.

A first aspect of the invention is an acrylate-olefin copolymer as defined in claim 1.

A second aspect of the invention is a method for preparing these copolymers as defined in claim 13.

A third aspect of the invention is a lubricant composition comprising at least one base oil and at least one copolymer according to the invention as defined in claim 14.

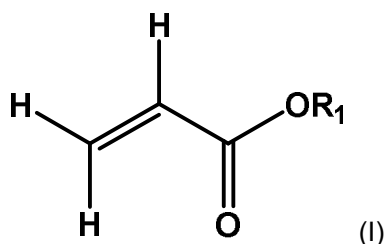
A fourth aspect of the invention is the use of these copolymers as lubricant additive or synthetic base fluid in a lubricating oil composition, preferably in a gear oil composition, a transmission oil composition, a hydraulic oil composition, an engine oil composition, a marine oil composition, an industrial lubricating oil composition or in grease.

DETAILED DESCRIPTION OF THE INVENTION

Copolymer according to the invention

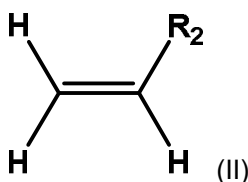
5 The present invention relates to a copolymer comprising:

a) 65 to 90 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one acrylate of Formula (I),



10 wherein R₁ means a linear or branched alkyl group having from 6 to 12 carbon atoms,

b) 10 to 35 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one non-functionalized alpha-olefin of Formula (II),



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wherein R₂ means a linear alkyl group having from 6 to 16 carbon atoms,

20 c) 0 to 10 % by weight of monomer units derived from at least one monomer selected from the list consisting of methacrylamides, fumarates, maleates or a mixture thereof, based on the total weight of the copolymer, and

wherein the copolymer has a kinematic viscosity at 100°C from 80 to 600 cSt according to ASTM D 445, and

25 wherein the copolymer comprises from 0 to 22 % by weight of monomer units derived from monomers with linear alkyl group having more than 8 carbon atoms, based on the total weight of the copolymer.

30 According to one aspect of the invention, it is preferred that the copolymer comprises 0 to 20 % by weight, more preferably 0 to 18 % by weight, of monomer units derived from monomers with linear alkyl group having more than 8 carbon atoms, based on the total weight of the copolymer.

According to another aspect of the invention, it is preferred that the copolymer has a kinematic viscosity at 100°C from 100 to 500 cSt according to ASTM D 445, more preferably from 150 to 400 cSt according to ASTM D 445, more preferably from 150 to 350 cSt according to ASTM D 445.

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According to another preferred aspect of the invention, the total content of monomer units derived from monomers a) and b) in the copolymer of the invention sums up to 90 % by weight, more preferably sums up to 95% by weight, even more preferably sums up to 98 % by weight, most preferably sums up to 100 % by weight, based on the total weight of the copolymer.

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According to another preferred aspect of the invention, the total content of monomer units derived from monomers a), b) and c) in the copolymer of the invention sums up to 90% by weight, more preferably sums up to 95% by weight, even more preferably sums up to 98 % by weight, most preferably sums up to 100 % by weight, based on the total weight of the copolymer.

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The acrylate a) of Formula (I) refers to esters of acrylic acid with straight chain or branched alcohols having 6 to 12 carbon atoms, preferably 6 to 10 carbon atoms, more preferably 8 to 10 carbons. The term encompasses individual acrylic esters with an alcohol of a particular length, and likewise mixtures of acrylic esters with alcohols of different lengths.

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According to one aspect of the invention, it is preferred that R¹ in the acrylate monomer of Formula (I) is a linear or branched alkyl group having from 6 to 10 carbon atoms, more preferably linear or branched alkyl group having 8 to 10 carbon atoms. Particularly preferred acrylates a) of Formula (I) are 2-ethylhexyl acrylate, 2-propylheptyl acrylate, n-octylacrylate or a mixture thereof.

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According to the present invention, it is preferred that the copolymer of the invention comprises 70 to 90 % by weight, more preferably 75 to 90 % by weight, of monomer units derived from the acrylate monomer a) of Formula (I), based on the total weight of the copolymer.

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According to the present invention, it is preferred that the copolymer of the invention comprises 10 to 30 % by weight, more preferably 10 to 25% by weight, of monomer units derived from the non-functionalized alpha-olefin b) of Formula (II), based on the total weight of the copolymer. Particularly preferred non-functionalized alpha-olefins b) of Formula (II) are selected from the group consisting of decene, dodecene, tetradecene, hexadecene or a mixture thereof.

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According to a preferred aspect of the present invention, the copolymer has a weight-average molecular weight from 5,000 to 30,000 g/mol, preferably from 7,000 to 25,000 g/mol, even more preferably from 8,000 to 20,000 g/mol according to DIN 55672-1.

In the present invention, the weight-average molecular weights (M_w) or number-average molecular weights (M_n) of the copolymers were determined by gel permeation chromatography (GPC) using PMMA calibration standards according to DIN 55672-1 using the following measurement conditions:

5 Eluent: tetrahydrofuran (THF)

Operation temperature: 35 °C

Columns: the column set consists of four columns: two columns SDV 106 Å, one column SDV 104 Å and one column SDV 103 Å (PSS Standards Service GmbH, Mainz, Germany), all with the size of 300 x 8 mm and an average particle size of 10 µm

10 Flow rate: 1mL/min

Injected volume: 100 µL

Instrument: Agilent 1100 series consisting of an autosampler, pump and column oven

Detection device: a refractive index detector from Agilent 1100 series.

15 Preferably, the copolymers of the invention have a very low degree of cross-linking and a narrow molecular weight distribution, which further contribute to their shear resistance. The low degree of crosslinking and the narrow molecular weight are reflected in the polydispersity index of the copolymers. Preferably, the polydispersity index (PDI) of the copolymers according to the invention is in the range of 1.0 to 4.0, more preferably 1.5 to 3.5. A polydispersity index in the
20 range of 1.0 to 3.5 is considered optimal for most industrial applications with regard to the shear resistance of the copolymers. The polydispersity index is defined as the ratio of weight-average molecular weight to number-average molecular weight (M_w/M_n).

25 According to a preferred aspect of the present invention, the copolymer of the invention has a COC flashpoint above 250°C according to ASTM D92.

The copolymers of the invention optionally comprise monomer units derived from monomer c), which is selected from the list consisting of methacrylamides, fumarates, maleates or a mixture thereof. Preferably, the amount of monomer units derived from monomer c) in the resulting
30 copolymer of the invention is from 0 to 10 % by weight, preferably from 0 to 7 % by weight, more preferably from 0 to 5 % by weight, even more preferably from 0 to 3 % by weight, based on the total weight of the copolymer. Particularly preferred monomers c) are di-2-ethylhexyl maleate, N-3-dimethylamino propyl methacrylamide di-2-ethylhexyl fumarate, or a mixture thereof.

35 It has been surprisingly observed that the incorporation of monomer units c) in the copolymer allows a full conversion of the non-functionalized alpha-olefins b) and thus no final distillation step is needed at the end of the copolymerization.

40 According to a preferred aspect of the present invention, on top of monomer units derived from monomers a), b) and optionally c), the acrylate-olefin copolymer of the invention further comprises

0 to 10 % by weight, more preferably 0 to 6 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one monomer d) selected from alkyl (meth)acrylates, vinyl esters or a mixture thereof. Particularly preferred monomers d) are lauryl methacrylate (LMA), stearyl methacrylate (SMA) or vinyl laurate (VLA).

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According to another preferred aspect of the present invention, the total content of monomer units of monomers a), b) c) and d) sums up to 95% by weight, more preferably 98% by weight, even more preferably 100 % by weight,

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According to another preferred aspect of the invention, when the copolymer consists of monomer units derived from monomers a), b), optionally c) and optionally d), the copolymer comprises 0 to 22 % by weight, more preferably 0 to 20 % by weight, even more preferably 0 to 18 % by weight, of monomer units derived from monomers a), b), c) and d) with linear alkyl group having more than 8 carbon atoms, based on the total weight of the copolymer.

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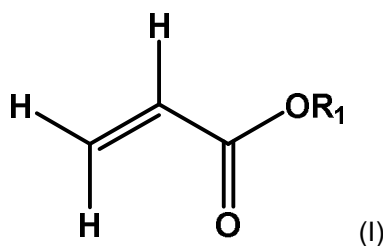
According to the invention, the copolymer is a statistical copolymer, with a sequential distribution of the monomer units derived from monomers a) and b) and optionally monomers c) and d).

Preferable copolymers of the invention

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According to a preferred aspect of the invention, the copolymer comprises:

a) 65 to 90 % by weight, more preferably 70 to 90 % by weight, even more preferably 75 to 90 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one acrylate of Formula (I),

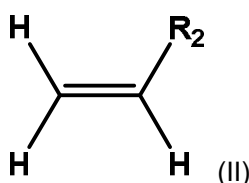


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wherein R₁ means a linear or branched alkyl group having from 8 to 10 carbon atoms,

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b) 10 to 35 % by weight, more preferably 10 to 30 % by weight, even more preferably 10 to 25 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one non-functionalized alpha-olefin of Formula (II),



wherein R₂ means a linear alkyl group having from 8 to 12 carbon atoms,

5 c) 0 to 10 % by weight, more preferably 0 to 5 % by weight, even more preferably 0 to 3 % by weight, of monomer units derived from at least one monomer selected from the list consisting of methacrylamides, fumarates, maleates or a mixture thereof, based on the total weight of the copolymer, and

10 wherein the copolymer has a kinematic viscosity at 100°C from 80 to 600 cSt according to ASTM D 445, and

wherein the copolymer comprises from 0 to 22 % by weight, preferably 0 to 18 % by weight, of monomer units derived from monomers with linear alkyl group having more than 8 carbon atoms, based on the total weight of the copolymer.

15 According to a preferred embodiment, the total content of monomer units of monomers a), b) and c) sums up to 95% by weight, more preferably 98% by weight, even more preferably 100 % by weight, based on the total weight of the copolymer.

20 According to a preferred embodiment, the copolymer further comprises 0 to 10 % by weight, more preferably 0 to 6 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one monomer d) selected from alkyl (meth)acrylates, vinyl ester or a mixture thereof. Particularly preferred monomers d) are lauryl methacrylate (LMA), stearyl methacrylate (SMA) or vinyl laurate (VLA).

25 According to a preferred embodiment, the total content of monomer units of monomers a), b), c) and d) sums up to 95% by weight, more preferably 98% by weight, even more preferably 100 % by weight,

30 **Method for preparing the copolymer according to the invention**

According to the present invention, the above-mentioned polymers are prepared following the method comprising the steps of:

- 35 i) providing a monomer composition as described above; and
ii) initiating radical polymerization in the monomer composition.

Standard free-radical polymerization is detailed, inter alia, in Ullmann's Encyclopedia of Industrial Chemistry, Sixth Edition. In general, a polymerization initiator and optionally a chain transfer agent are used for this purpose.

5 The polymerization can be conducted under standard pressure, reduced pressure or elevated pressure.

For the radical copolymerization of olefins with acrylates, the polymerization temperature is critical. In general, the copolymerization temperature is in the range from 140 to 180°C, preferably
10 from 150 to 170°C.

The polymerization step ii) may be performed with or without dilution in oil. Preferably, the polymerization step (ii) is made without dilution oil or any solvent.

15 Preferably, step (ii) comprises the addition of a radical initiator. Preferably, the radical initiator is selected from di-tert-butyl peroxide or dicumyl peroxide. Preferably, the total amount of radical initiator relative to the total weight of the monomer mixture is 0.01 to 5 % by weight, more preferably 0.1 to 1 % by weight. Preferably, the total amount of radical initiator is added continuously over the course of the copolymerization reaction (ii).

20 Preferably, the copolymerization step (ii) is made by feeding the acrylate monomers a), and optionally the monomers c) or any other comonomers, together with the initiator to the non-functionalized alpha-olefin monomers b). Preferably, the total reaction time of the radical polymerization is 2 to 5 hours, more preferably 3 hours.

25 In another preferred aspect of the invention, a third step iii) is optionally performed, corresponding to a distillation step to remove the unreacted alpha-olefin monomer b). Preferably, residual unreacted alpha-olefin monomer b) is removed by distillation at 150°C and pressures as low as 5 mbar using a rotary evaporator. Advantageously, no distillation step iii) is needed when the
30 copolymer of the invention comprises monomer units derived from monomer c). It has been surprisingly observed that small amounts of monomers c) (below 10% by weight, more preferably below 5% by weight, based on the total weight of the copolymer) enhance the conversion of the olefins during copolymerization (lower than 1 % by weight residual unreacted alpha-olefin b)), so that no distillation step iii) is needed.

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Lubricating oil compositions

As indicated above, the present invention also relates to a lubricating oil composition comprising at least one base oil and at least one copolymer as defined in the present invention.

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The base oils correspond to lubricant base oils, mineral, synthetic or natural, animal or vegetable oils suited to their use/chosen depending on the intended use.

5 The base oils used in formulating the lubricating oil compositions according to the present invention include, for example, conventional base stocks selected from API (American Petroleum Institute) base stock categories known as Group I, Group II, Group III, Group IV and Group V. The Group I and II base stocks are mineral oil materials (such as paraffinic and naphthenic oils) having a viscosity index (or VI) of less than 120. Group I is further differentiated from Group II in that the latter contains greater than 90% saturated materials and the former contains less than 10 90% saturated material (that is more than 10% unsaturated material). Group III is considered the highest level of mineral base oil with a VI of greater than or equal to 120 and a saturates level greater than or equal to 90%. Preferably the base oil included in the lubricating oil composition of the present invention is selected from the group consisting of API Group II and III base oils. Most preferably, the lubricant composition comprises an API Group III base oil. Group IV base oils are 15 polyalphaolefins (PAO). Group V base oils are esters and any other base oils not included in Group I to IV base oils. These base oils can be used individually or as a mixture.

In a preferred embodiment of the invention, the lubricating oil composition comprises from 0.1 to 99.9 % by weight, preferably from 1 to 95% by weight, of at least one base oil and from 0.1 to 20 99.9 % by weight, preferably from 5 % to 99 % by weight, of at least one copolymer according to the present invention, based on the total weight of the lubricating composition.

The lubricating oil compositions according to the present invention may also comprise any other additional additives suitable for use in the formulations. These additives include additional 25 viscosity index improvers, pour point depressants, dispersants, demulsifiers, defoamers, lubricity additives, friction modifiers, antioxidants, detergents, dyes, corrosion inhibitors and/or odorants.

Applications for the copolymer of the invention

30 The invention also relates to the use of the copolymer according to the present invention as a lubricant additive or a synthetic base fluid in a lubricating oil composition, preferably in a gear oil composition, a transmission oil composition, a hydraulic oil composition, an engine oil composition, a marine oil composition, an industrial lubricating oil composition or in grease.

35 EXPERIMENTAL PART

The invention is further illustrated in detail hereinafter with reference to examples and comparative examples, without any intention to limit the scope of the present invention. All percentages in relation to monomers or base fluids given in the tables below are weight percentages (wt%).

Abbreviations

	BF-26	Brookfield viscosity measured at -26°C
	BF-30	Brookfield viscosity measured at -26°C
	BV	bulk viscosity
5	BV40	bulk viscosity @40°C in accordance with ASTM D445
	BV100	bulk viscosity @100°C in accordance with ASTM D445
	cSt	centistokes
	cP	centipoise
	DBPO	di-tert-butyl peroxide
10	DCP	dicumyl peroxide
	Dec	decene
	DEHF	di-2-ethylhexyl fumarate
	DEHM	di-2-ethylhexyl maleate
	DMAPMAM	N-3-dimethylamino propyl methacrylamide
15	DoDec	dodecene
	EHA	2-ethylhexyl acrylate
	EHMA	2-ethylhexyl methacrylate
	HA	hexyl acrylate
	HexDec	hexadecene
20	Hitec® 2030	defoamer commercially available from Afton
	Hitec® 307	DI Package commercially available from Afton
	Hitec® 3250	DI Package commercially available from Afton
	IDA	iso-decyl acrylate
	IDMA	iso-decyl methacrylate
25	Ini	initiator
	ITDA	iso-tridecyl acrylate, commercially available from Aldrich
	KV	kinematic viscosity measured according to ASTM D445
	KV ₄₀	kinematic viscosity measured @40°C to ASTM D445
	KV ₁₀₀	kinematic viscosity measured @100°C to ASTM D445
30	LA	lauryl acrylate, dodecylacrylate
	LMA	lauryl methacrylate, 73% C12, 27% C14, all linear
	Mn	number-average molecular weight
	MO	methyloleate
	Mw	weight-average molecular weight
35	n.m.	not measured
	nOA	n-octylacrylate
	NB3080	Nexbase® 3080; Group III base oil from Neste with a KV100 of 7.9 cSt
	PAO100	polyalphaolefin base oil with a KV100 of 100 cSt from Chevron Phillips
	PAO4	polyalphaolefin base oil with a KV100 of 4 cSt
40	PAO6	polyalphaolefin base oil with a KV100 of 6 cSt

	PAO8	INEOS Durasyn 168 polyalphaolefin base oil with a KV ₁₀₀ of 7.8 cSt
	PAO8 I	INEOS Durasyn 128polyalphaolefin base oil with a KV ₁₀₀ of 7.8 cSt
	PDI	polydispersity index
	PHA	2-propylheptyl acrylate
5	PP	pour point
	Priolube 3970	ester base fluid available from Croda
	RC9420	DI package commercially available from Rheinchemie
	ReMo	Residual Monomer content
	SMA	stearyl methacrylate, 35% C16, 65% C18, all linear
10	SL KRL20	shear loss after 20 hours KRL measurement determined at 100°C
	SL KRL100	shear loss after 100 hours KRL measurement determined at 100°C
	TetDec	tetradecene
	VI	viscosity index
	VLA	vinyl laurate
15	VPL 1-180	Evonik VISCOPLEX® 1-180, pour point depressant
	VPL 1-300	Evonik VISCOPLEX® 1-300, pour point depressant
	Yubase 4	Group III base oil from SK Lubricants with a KV ₁₀₀ of 4 cSt

Test methods

20	KV	ASTM D445
	VI	ASTM D2270
	PP	ASTM D5950
	Copper Corrosion	ASTM D130
	Steel Corrosion	DIN ISO 7120
25	TOST	ASTM D2893
	RPVOT	ASTM D2272
	Foam	ASTM D892
	KRL	CEC L-45-A-99
	BF	ASTM D2983
30	COC	ASTM D92

In the present invention, the bulk viscosity (BV) of the product (product obtained from polymerization reaction) corresponds to the kinematic viscosity (KV) of the resulting product of the polymerization measured in accordance with ASTM D 445. Thus, the bulk viscosity of the polymers, BV40 and BV100 as shown in Tables 1, 2, 3 and 4 below, were measured as kinematic viscosity at 40°C and 100°C, respectively, in accordance with ASTM D445.

Examples

Synthesis 1: Pure acrylate (Ex.39*)

5 1.62 g of DBPO (0.6 wt% relative to the amount of acrylate) dissolved in 270.0 g EHA was slowly fed to 30.0 g of PAO8 under nitrogen at 160°C for 3 hours. After stirring for another hour, the resulting clear and colorless polymer solution was cooled down and used in the further experiments without further purification.

Synthesis 2: (Meth)acrylate/olefin copolymer with distillation step (Ex.8)

10 3.6 g of DBPO (0.3 wt% relative to the monomer in the feed) dissolved in 1200 g EHA was slowly fed to 300 g (0.33 molar equivalents relative to the (meth)acrylate) of 1-Decene under nitrogen at 160°C for 3 hours. After stirring for another hour, the resulting clear and colorless polymer was cooled down. Subsequently, the residual decene was removed by distillation at 150°C and pressures as low as 5 mbar using a rotary evaporator.

Synthesis 3: Acrylate/olefin copolymer without distillation step (Ex.54)

15 0.77 g of DBPO (0.3 wt% relative to the monomer in the feed) dissolved in 249.3 g EHA and 5.7 g DEHF was slowly fed to 45.0 g of 1-Tetradecene under nitrogen at 160°C for 3 hours. After stirring for another hour, the resulting clear and colorless polymer was cooled down and used without further purification.

20 Examples 1 to 28 were prepared in the same way as Synthesis 2, except that the amounts of reactants or other reaction conditions were changed as listed in Table 1. The alpha-olefin monomers are always first charged to the reactor and the (meth)acrylate monomers and the initiator are fed over a set period of time.

Examples 38 to 43 were prepared in the same way as Synthesis 1, except that the amounts of reactants or other reaction conditions were changed as listed in Table 3.

30 Examples 44 to 61 were prepared in the same way as Synthesis 3, except that the amounts of reactants or other reaction conditions were changed as listed in Table 4.

35 As the molar ratio in the reaction is not representative for the final composition, the final ratio of olefin in the polymer after distillation is given in weight % (olefin inc.). This ratio was determined gravimetrically under the assumption that the conversion of the (meth)acrylate is either complete or its boiling point is too high to be removed by the distillation. For example, Example 8 has a residual content of EHA of less than 0.01 wt% before the distillation step.

40 For some examples up to 3 polymers with similar viscosities were blended. For the blending process, the products were stirred together at 80°C for an hour. The blends are listed in Table 2

(see examples 29 to 37). The amount of incorporated olefin was calculated from the values determined for the separate components. The other values such as molecular weight or viscosity were measured on the blend.

5 A good high viscosity base fluid needs to combine several properties. An important criterion for high-performance gear oils is the low temperature performance. Aside from a low dependency of the viscosity on the temperature, which is also reflected in the VI, it is important that the polymers do not show strong intermolecular interactions, leading to bad low temperature performance.

10 The polymers according to this invention have a favorable combination of viscosity, viscosity index and shear stability as exemplified with Example 5, 6 or 8. In contrast, it can be observed that the acrylate-olefin copolymer comparative example 7*, which comprises 22.6% by weight of linear side chains with more than 8 carbon atoms, has a good VI (236) but as shown in the lubricant formulation thereof (example F-21*), does not perform well at low temperature (BF -26 = 192,000
15 cP). In contrast, the acrylate-olefin copolymer inventive example 50 with only 15 % by weight linear side chain with more than 8 carbon atoms combines both high VI (220) and as shown in the lubricant formulation thereof (example F-28) performs very well under even more severe low temperature conditions (BF -30 = 102,000 cP) (BF-30 instead of BF-26 for comparative example F-21*).

20 Surprisingly even longer side chains such as in inventive examples 48 (C12 side chain) or 51 (C14 side chain) perform on the same level as example 50 (C10 side chain) because the total amount of monomer units derived from monomers with linear alkyl group having more than 8 carbon atoms in total in the copolymer, is lower than 22 % by weight, based on the total weight
25 of the copolymer. The long linear side chains (more than 8 carbon atoms) can be any monomer units of the copolymer (any monomers a), b), c), d) or other comonomers) as shown in comparative example 13* which has 81% by weight of linear side chains of more than 8 carbon atoms due to a high content of laurylacrylate. As shown in comparative formulation F-38*, the high content of long linear side chains having more than 8 carbon atoms in the acrylate monomer
30 units results in extremely poor low temperature performance (PP of -18°C) despite a high VI (195), thus no good combination of high VI and good low temperature performance is achieved. The quantity of these sidechains is provided as ">C8 SC" in Tables 1 to 4.

While polymethacrylates are known as excellent VI improvers, they are surprisingly outperformed
35 in the lower molecular weight range by their acrylate counterparts. This is exemplified in Table 5, where F-2 and F-3* are based on very similar polymers (based on EHA for inventive example 29 and EHMA for comparative example 20*), but a much higher VI of the EHA based polymer (inventive example 29) results in a higher VI of the final formulation and a better low temperature viscosity.

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5 F-2 performs on a similar level as the PAO100 base formulation F-1*. Compared to pure polyolefins, the polar ester functions in the acrylate-olefin copolymer of the invention are beneficial for the overall compatibility of different formulation components (to allow the direct comparison with PAO100 the formulations in Table 4 were prepared without further additives). Different to PAOs, which have to be prepared by cationic or coordination polymerization methods, the radical polymerization process used for the preparation of the acrylate-olefin copolymers of the invention provides easy access to higher viscous products with good shear stability level in a commercially attractive way.

Table 1 Methacrylate-olefin copolymers or acrylate-olefin copolymers

Ex#	(M)A	Olefin	Ini [wt%]	T[°C]	Olefin [eq]	Olefin inc [wt%]	Mw [g/mol]	Mn [g/mol]	PDI	BV100 [cSt]	BV40 [cSt]	VI	>C8 SC [wt%]
Ex.1	EHA	Dec	0.10	150	2.00	34.7	6,410	3,450	1.9	87.9	n.m.	n.m.	0.0
Ex.2	EHA	Dec	0.04	150	2.00	30.5	7,680	3,860	2.0	117.2	n.m.	n.m.	0.0
Ex.3	EHA	Dec	0.05	150	2.00	29.7	8,090	4,020	2.0	128.1	n.m.	n.m.	0.0
Ex.4	EHA	Dec	0.07	150	1.00	25.4	10,500	4,750	2.2	188.7	2479	196	0.0
Ex.5	EHA	Dec	0.07	150	0.60	20.7	14,900	5,770	2.6	306.3	4372	214	0.0
Ex.6	EHA	Dec	0.07	150	0.40	18.6	19,500	6,390	3.1	445.8	6573	233	0.0
Ex.7*	EHA	DoDec	0.07	150	0.42	22.6	18,500	5,650	3.3	304.8	3551	236	22.6
Ex.8	EHA	Dec	0.30	160	0.33	18.2	15,600	5,980	2.6	299.7	4148	216	0.0
Ex.9	HexA	Dec	0.09	160	0.54	26.7	14,400	5,750	2.5	145.5	1425	214	0.0
Ex.10	HexA	Dec	0.08	160	0.54	26.2	14,300	6,260	2.3	160.1	1672	212	0.0
Ex.11	HexA	Dec	0.08	160	0.54	26.1	15,800	6,430	2.5	175.4	1809	218	0.0
Ex.12*	iTDA	Dec	0.05	150	0.54	19.4	15,100	6,440	2.3	258.6	4107	194	0.0
Ex.13*	LA	Dec	0.14	150	0.46	18.6	15,100	7,100	2.1	99.08	783,7	222	81.4
Ex.14	PHA	Dec	0.07	150	0.43	18.1	16,000	6,660	2.4	269.7	3221	226	0.0
Ex.15	PHA	Dec	0.08	150	0.43	17.9	15,400	6,580	2.3	259.8	3145	222	0.0
Ex.16	nOA	Dec	0.10	160	0.71	22.8	14,000	6,450	2.2	132.8	1294	210	0.0
Ex.17	nOA	Dec	0.10	160	0.61	23.4	14,700	6,570	2.2	138.3	1336	213	0.0
Ex.18*	EHMA	Dec	0.10	155	2.00	25.8	11,200	3,570	3.2	452.6	12200	178	0.0
Ex.19*	EHMA	Dec	0.30	155	2.00	31.3	6,210	2,720	2.3	143.8	2640	150	0.0
Ex.20*	EHMA	Dec	0.50	155	2.00	32.7	5,430	2,550	2.1	110.9	1899	143	0.0
Ex.21*	IDMA	Dec	0.80	150	2.00	31.2	6,550	2,920	2.2	129.5	n.m.	n.m.	0.0
Ex.22*	IDMA	Dec	0.65	150	2.00	29.0	7,750	3,250	2.4	184.6	n.m.	n.m.	0.0
Ex.23*	IDMA	Dec	0.10	155	2.00	21.5	12,200	3,790	3.2	n.m.	n.m.	n.m.	0.0
Ex.24*	IDMA	Dec	0.07	155	2.00	n.m.	13,500	4,050	3.3	n.m.	n.m.	n.m.	0.0
Ex.25*	LMA	Dec	0.12	150	1.50	18.2	n.m.	n.m.	n.m.	490.2	n.m.	n.m.	81.8
Ex.26*	LMA	Dec	0.13	150	1.50	17.6	n.m.	n.m.	n.m.	442.0	n.m.	n.m.	82.4
Ex.27*	LMA	Dec	0.20	155	2.00	23.7	10,700	4,000	2.7	131.7	n.m.	n.m.	85.3
Ex.28*	LMA	Dec	0.12	155	2.00	n.m.	13,700	4,260	3.2	182.3	n.m.	n.m.	85

(*) means comparative examples

Table 2 Blends of copolymers from Table 1

Ex#	Comp. 1 [wt%]	Comp. 2 [wt%]	Comp. 3 [wt%]	Olefin inc [wt%]	Mw [g/mol]	Mn [g/mol]	PDI	BV100 [cSt]	BV40 [cSt]	VI	>C8 SC [wt%]
Ex.29	50% Ex.1	50% Ex.2	n.m.	32.6	n.m.	n.m.	n.m.	99.9	1,137	178	0.0
Ex.30	64% Ex.3	36% Ex.4	n.m.	28.3	8,940	4,260	2.1	146.9	1,800	190	0.0
Ex.31	34% Ex.9	32% Ex.10	34% Ex.11	26.3	15,000	6,470	2.3	160.6	1,653	214	0.0
Ex.32	50% Ex.14	50% Ex.15	n.m.	18.0	n.m.	n.m.	n.m.	263.3	3,176	224	0.0
Ex.33	38% Ex.16	62% Ex.17	n.m.	23.2	n.m.	n.m.	n.m.	135.4	1,315	212	0.0
Ex.34*	51% Ex.21	49% Ex.22	n.m.	30.1	n.m.	n.m.	n.m.	147.0	2,753	150	0.0
Ex.35*	36% Ex.23	64% Ex.24	n.m.	n.m.	n.m.	n.m.	n.m.	450.7	11,740	181	0.0
Ex.36*	50% Ex.25	50% Ex.26	n.m.	17.9	23,900	5,940	4.0	468.1	8,699	213	82.1
Ex.37*	64% Ex.27	36% Ex.28	n.m.	n.m.	n.m.	n.m.	n.m.	146.8	1,979	180	85

(*) means comparative examples

Table 3 Pure polyacrylates

Ex#	(M)A	Solvent	Solvent [wt%]	Ini	Ini [wt%]	T [°C]	ReMo [wt%]	Mw [g/mol]	Mn [g/mol]	PDI	BV100 [cSt]	BV40 [cSt]	VI	>C10 SC [wt%]
Ex.38*	EHA	Yubase 4	20	DBPO	0.5	160	0.04	9590	5020	1.9	67.4	712	168	0.0
Ex.39*	EHA	PAO8	10	DBPO	0.6	160	0.02	16400	6970	2.4	210.3	2942	195	0.0
Ex.40*	PHA	PAO8	85	DCP	0.5	150	0.01	14100	7270	1.9	145.8	1671	197	0.0
Ex.41*	IDA	Nexbase 3080	75	DCP	0.5	150	n.m.	15400	7490	2.1	83.0	975	166	0.0
Ex.42*	LA	Nexbase 3080	70	DCP	0.5	150	n.m.	15600	8530	1.8	43.0	314	192	100.0
Ex.43*	ITDA	Nexbase 3080	75	DCP	0.5	150	n.m.	14700	7270	2.0	95.9	1320	157	0.0

(*) means comparative examples

Table 4 Acrylate-olefin copolymers comprising monomer units of monomer c)

Ex#	EHA [wt%]	PHA [wt%]	Olefin	Olefin [wt%]	DEHF [wt%]	Comonomer	Comonomer [wt%]	Ini [%]	Mw [g/mol]	Mn [g/mol]	PDI	BV100 [cSt]	BV40 [cSt]	VI	>C8 SC [wt%]
Ex.44	83.1		TetDec	15		DMPMAM	1.9	0.3	18,200	6,130	3.0	299.7	4,148	216	15.0
Ex.45	80		TetDec	15		DMPMAM	5	0.3	16,600	5,380	3.1	273.0	3,988	206	15.0
Ex.46	83.1		TetDec	15		DEHM	1.9	0.3	19,800	6,310	3.1	300.5	4,043	219	15.0
Ex.47	80		TetDec	15	5			0.3	16,200	5,820	2.8	283.9	3,823	216	15.0
Ex.48	80		TetDec	15	5			0.3	17,100	6,030	2.8	301.8	4,125	218	15.0
Ex.49	80		Dec	15	5			0.3	15,400	5,880	2.6	301.1	4,138	217	0.0
Ex.50	80		DoDec	15	5			0.3	16,600	6,000	2.8	303.6	4,103	220	15.0
Ex.51	80		HexDec	15	5			0.3	18,300	6,130	3.0	301.9	3,986	222	15.0
Ex.52		83.1	TetDec	15	1,9			0.3	14,600	5,890	2.5	203.8	2,538	206	15.0
Ex.53	79.5		Dec	15	5	DMPMAM	0.5	0.15	15,300	5,880	2.6	280.5	3,878	213	15.0
Ex.54	83.1		Tetdec	15	1,9			0.3	19,000	6,030	3.2	317.5	3,098	211	0.0
Ex.55	70	10	Tetdec	15	5			0.3	17,600	6,110	2.9	284.9	3,806	217	15.0
Ex.56	40	40	Tetdec	15	5			0.3	16,100	5,940	2.7	239.8	4,498	217	15.0
Ex.57	80		Dec	15		VLA	5	0.3	19,800	6,530	3.0	339.0	n.m.	n.m.	5.0
Ex.58	80		Dec	15		SMA	5	0.3	18,400	6,330	2.9	307.8	n.m.	n.m.	5.0
Ex.59	80		Dec	15		LMA	5	0.3	18,400	6,180	3.0	321.6	n.m.	n.m.	5.0
Ex.60	85		Dec	14		MO	1	0.7	18,600	6,190	3.0	330.9	n.m.	n.m.	0.0
Ex.61	80		TetDec	15	5			0.3	17,800	6,160	2.9	322.9	4,295	225	15.0

Table 5 Lubricant formulations with 100cSt high viscosity base fluids

Form. Ex.	F-1*	F-2	F-3*
PAO100 [wt%]	22.3		
Ex.29 [wt%]		31.5	
Ex.20* [wt%]			29.8
PAO4 [wt%]	77.7	68.5	70.2
KV40 [cSt]	46.0	46.1	45.9
KV100 [cSt]	8.4	8.5	8.1
VI	162	164	151
BF-40 [cP]	11,000	12,200	14,000
PP [°C]	-66	-66	-66

(*) means comparative examples

Examples of formulations with EHA homopolymers can be found in Tables 6 and 7. For process reasons the pure acrylates shown in Table 3 were prepared as solutions in oil, so that no bulk properties are available for these polymers. In order not to influence the comparison of the copolymers, the oil used for the polymerization was the same which was later used in the formulations. As can be seen the mentioned EHA homopolymers (comparative examples 38* and 39*) provide lower VIs in the formulation and show poorer low temperature performance. As shown in Table 8, the comparative polyacrylate examples with longer side chains as the EHA homopolymers also do not perform as good as the inventive acrylate-olefin copolymers of the invention.

Table 6 Lubricant formulations with 150 cSt high viscosity base fluids

Form. Ex.	F-4*	F-5	F-6*	F-7*	F-8*
Ex.38* [wt %]	35.2				
Ex.30 [wt %]		28.5			
Ex.19* [wt %]			28.2		
Ex.34* [wt %]				25.2	
Ex.37* [wt %]					23.1
VPL 1-300 [wt %]	0.3	0.3	0.3	0.3	0.3
Yubase 4 [%]	64.5	71.2	71.5	74.5	76.6
KV40 [cSt]	49.7	48.6	49.2	46.2	46.7
KV100 [cSt]	8.9	8.9	8.6	8.2	8.8
VI	161	166	152	153	172
BF-40 [cP]	90,000	55,000	83,000	77,000	solid
PP [°C]	-42	-39	-42	-39	-39

(*) means comparative examples

Table 7 Lubricant formulations with 450 cSt high viscosity base fluids

Form. Ex.	F-9*	F-10	F-11*	F-12*	F-13*	F-14	F-15*	F-16*
Ex.39* [wt %]	55.0				55.1			
Ex.6 [wt %]		47.0				47.4		
Ex.18* [wt %]			45.0				43.6	
Ex.35* [wt %]				43.0				42.1
RC9420 [wt%]	2.0	2.0	2.0	2.0				
Hitec 307 [wt%]					2.7	2.7	2.7	2.7
VPL 1-180 [wt %]					0.7	0.7	0.7	0.7
NB3080 [wt %]					41.6	43.4	53.1	54.6
PAO8 [wt%]	43.0	51.0	53.0	55.0				
KV40 [cSt]	312.9	320.3	325.3	318.9	314.9	326.5	312.6	312.7
KV100 [cSt]	36.4	39.5	34.5	34.5	36.3	39.6	33.4	33.8
VI	164	176	150	153	163	174	149	152
BF-26 [cP]	74,000	49,000	74,000	77,000	n.m.	n.m.	n.m.	n.m.
PP [°C]	-39	-45	-42	-45	-36	-39	n.m.	-39

(*) means comparative examples

Table 8 Lubricant formulations with pure polyacrylate high viscosity base fluids

Form. Ex.	F-17*	F-18*	F-190*	F-20*
Ex.40* [wt %]	62.4			
Ex.41* [wt %]		67.5		
Ex.42* [wt %]			96.6	
Ex.43* [wt %]				62.0
Viscoplex 1-180 [wt%]	0.7	0.7	0.7	0.7
Hitec 307 [wt%]	2.7	2.7	2.7	2.7
Nexbase 3080 [wt%]		29.1		34.6
PAO8 [wt%]	34.9			
KV40 [cSt]	328.1	314.5	315.5	313.6
KV100 [cSt]	38.1	35.2	42.9	33.1
VI	166	158	193	147
BF-26 [cP]	81,000	220,000	solid	212,000
PP [°C]	-45	-39	-6	-36

(*) means comparative examples

Table 9 Residual monomers of the polymers (all amounts in wt%) described in Table 4

	Residual monomers				
Ex#	EHA	PHA	Olefin	DEHF	Comonomer
Ex.44	0.12%		0.87%		0.01%
Ex.45	0.26%		1.09%		0.03%
Ex.46	0.07%		0.32%		0.57%
Ex.47	0.13%		0.33%	0.16%	
Ex.48	0.08%		0.35%	0.11%	
Ex.49	0.06%		0.58%	0.07%	
Ex.50	0.05%		0.40%	0.05%	
Ex.51	0.04%		0.25%	0.10%	
Ex.52		0.14%	0.47%	0.04%	
Ex.53	0.11%		0.72%	0.12%	0.00%
Ex.54	0.07%		0.37%	0.05%	
Ex.55	0.07%	0.07%	0.38%	0.0%	
Ex.56	0.03%	0.10%	0.36%	0.08%	
Ex.57	0.02%		0.57%		n.m.
Ex.58	0.04%		0.75%		n.m.
Ex.59	0.04%		0.71%		n.m.
Ex.60	0.02%		0.48%		0.53%
Ex.61	0.06%		0.03%	0.08%	

High-performance lubricants also need to fulfill many requirements. Especially excellent low temperature properties, high flashpoints and good ageing behavior are directly influenced by the choice of high viscosity base fluids.

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In Table 10 below, it is shown that the inventive acrylate-olefin copolymers of the invention have high flashpoints, which fulfills the requirements for gear oil applications.

The effect of different PAO viscosity grades is shown in Table 11 below (PAO4, PAO 6, PAO8). Lower grades such as PAO4 allow the use of higher amount of acrylate-olefin copolymer of the invention, which improves VI and low temperature performance of the resulting formulations even further. For inventive formulation F-23, further performance parameters are provided which are important for industrial gear oil formulations. The strong performance in the TOST and RPVOT test shows the good stability towards severe thermo-oxidative stress. The low foaming tendency and low corrosiveness of the formulation underline the suitability of the acrylate-olefin copolymers of the invention in gear oil formulations.

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Table 10: Flashpoint of some high viscosity base fluids

Example	COC [°C]
Ex.53	256
Ex.61	271
Ex.5	260

Table 11 320 cSt lubricant formulations with base oils of different viscosity

Form. Ex.	F-21	F-22	F-23	F-24	F-25
Ex. 7* [wt%]	51.2				
Ex. 5 [wt%]		51.6	63.3	57.5	51.9
Hitec 3250 [wt%]	2.0	2.0	2.0	2.0	2.0
PAO4 [wt%]			34,7		
PAO6 [wt%]				40.5	
PAO8 [wt%]	46.8	46.4			43.6
Priolube 3970 [wt%]					2.5
Hitec 3250 [wt%]	2.0	2.0	2.0	2.0	2.0
Hitec 2030 [wt%] (**)			0,02	0,02	0,02
KV40 [cSt]	321.9	319.8	326.1	318.4	316.7
KV100 [cSt]	40.3	38.9	41.83	39.87	38.66
VI	179	173	184	178	173
BF-26 [cP]	192,000	50,000	50,000	n.m.	n.m.
BF-30 [cP]	n.m.	n.m.	81,000	82,000	88,000
Copper Corrosion	n.m.	n.m.	1b	n.m.	n.m.
Steel Corrosion	n.m.	n.m.	free of rust	n.m.	n.m.
TOST KV100 increase [%]	n.m.	n.m.	6	n.m.	n.m.
RPVOT [min]	n.m.	n.m.	292	n.m.	n.m.
Foam after Sequence I [mL]	n.m.	n.m.	20	n.m.	n.m.
Foam after Sequence II [mL]	n.m.	n.m.	10	n.m.	n.m.
Foam after Sequence III [mL]	n.m.	n.m.	20	n.m.	n.m.
PP [°C]	-51	-48	-48	-48	-51
SL KRL20 100°C [%]	1.5	0.6	n.m.	n.m.	n.m.
SL KRL100 100°C [%]	n.m.	n.m.	3.6	2.5	n.m.

5 (*) means comparative example

(**) added on top

Performance of the polymers without the distillation step is shown in Tables 12 and 13 below and is on a similar level as the distilled samples (Table 1). Care needs to be taken with regard to the comparison of different formulations in PAO8 as two different samples were used. While “PAO8” has excellent low temperature properties, “PAO8 I” shows slightly inferior low temperature properties at an improved VI level.

Table 12: 320 cSt lubricant formulations with different high viscosity base fluids

Form. Ex	F-26	F-27	F-28	F-29	F-30	F-31	F-32	F-33	F-34	F-35
Ex.5 [wt%]	53.2									
Ex.49 [wt%]		54.2								
Ex.50 [wt%]			54.0							
Ex.51 [wt%]				53.0						
Ex.54 [wt%]					52.4					
Ex.46 [wt%]						52.6				
Ex.44 [wt%]							52.6			
Ex.45 [wt%]								53.6		
Ex.47 [wt%]									54.4	
Ex.48 [wt%]										53.4
Hitec 3250 [wt%]	2.0	2.0	2.0	2.0	2.0	2.0	2.0	2.0	2.0	2.0
PAO8 I [wt%]	44.8	43.8	44.0	45.0	45.6	45.4	45.5	44.4	43.4	44.4
KV40 [cSt]	318.8	320.2	322.1	317.7	317.7	316.6	321.1	323.9	322.5	323.3
KV100 [cSt]	39.3	38.6	39.1	39.1	39.2	39.2	38.9	37.7	39.3	39.6
VI	175	172	173	175	176	176	173	178	174	175
BF-30 [cP]	89k	116k	102k	102k	96k	97k	114k	124k	102k	93k
PP [°C]	-39	-39	-39	-39	-39	-39	-39	-36	-39	-39
SL KRL100 100°C [%]	6.3	2.4	3.1	4.7	5.0	5.7	4.8	2.8	3.4	4.3

"k" means thousands (10^3) e.g. BF -30 [cP] 89k cP= 89,000 cP

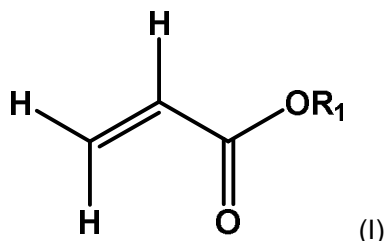
Table 13 320 cSt lubricant formulations with different high viscosity base fluids

Form. Ex.	F-36	F-37*	F-38*	F-39	F-40	F-41	F-42
Ex.31 [wt%]	60.0						
Ex12* [wt%]		50.0					
Ex13* [wt%]			71.8				
Ex.32 [wt%]				53.8			
Ex.33 [wt%]					63.5		
Ex.52 [wt%]						57.7	
Ex.8 [wt%]							52.1
Hitec 3250 [wt%]	2.0	2.0	2.0	2.0	2.0	2.0	2.0
PAO8 [wt%]	38.0	48.0	26.2	44.2	34.5	40.3	45.9
KV40 [cSt]	323.0	322.0	323.2	323.6	322.8	322.8	319.6
KV100 [cSt]	41.1	36.6	44.2	39.5	41.7	38.7	38.1
VI	182	162	195	174	185	171	170
BF-30 [cP]	95,000	140,000	solid	96,000	84,000	104,000	104,000
PP [°C]	-48	-42	-18	-45	-48	-48	-45
SL KRL20 100°C [%]	2.7	n.m.	1.6	5.2	2.2	3.6	3.5

CLAIMS

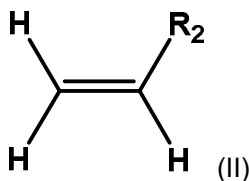
1. A copolymer comprising:

a) 65 to 90 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one acrylate of Formula (I),



wherein R₁ means a linear or branched alkyl group having from 6 to 12 carbon atoms,

b) 10 to 35 % by weight, based on the total weight of the copolymer, of monomer units derived from at least one non-functionalized alpha-olefin of formula (II),



wherein R₂ means a linear alkyl group having from 6 to 16 carbon atoms,

and

c) 0 to 10 % by weight of monomer units derived from at least one monomer selected from the list consisting of methacrylamides, fumarates, maleates or a mixture thereof, based on the total weight of the copolymer, and

wherein the copolymer has a kinematic viscosity from 80 to 600 cSt at 100 °C according to ASTM D 445, and

wherein the copolymer comprises from 0 to 22 % by weight of monomer units derived from monomers with linear alkyl group having more than 8 carbon atoms, based on the total weight of the copolymer.

2. The copolymer according to claim 1, wherein the copolymer comprises from 0 to 20 % by weight, preferably from 0 to 18 % by weight, of monomer units derived from monomers with linear alkyl group having more than 8 carbon atoms, based on the total weight of the copolymer.

3. The copolymer according to claim 1 or 2, wherein the copolymer has a kinematic viscosity from 100 to 500 cSt at 100°C according to ASTM D 445, preferably from 150 to 400 cSt according to ASTM D 445, more preferably from 150 to 350 cSt according to ASTM D 445.
- 5 4. The copolymer according to any one of claims 1 to 3, wherein the copolymer comprises 10 to 30 % by weight, preferably from 10 to 25 % by weight, of monomer units b) derived from the non-functionalized alpha-olefin of Formula (II), based on the total weight of the copolymer.
- 10 5. The copolymer according to any one of claims 1 to 4, wherein the non-functionalized alpha-olefin b) of Formula (II) is selected from the group consisting of decene, dodecene, tetradecene, hexadecene or a mixture thereof.
- 15 6. The copolymer according to any one of claims 1 to 5, wherein R₁ in the acrylate of Formula (I) is a linear or branched alkyl group having from 6 to 10 carbon atoms, preferably 8 to 10 carbon atoms, even more preferably the acrylate of Formula (I) is selected from 2-ethylhexyl acrylate, 2-propylheptyl acrylate, n-octylacrylate or a mixture thereof.
- 20 7. The copolymer according to any one of claims 1 to 6, wherein the copolymer comprises 0 to 7 % by weight, preferably from 0 to 5 % by weight, more preferably from 0 to 3 % by weight, of monomer units derived from monomer c), based on the total weight of the copolymer.
- 25 8. The copolymer according to any one of claims 1 to 7, wherein the total amount of monomer units derived from monomers a) and b) in the copolymer sums up to 90 % by weight, preferably sums up to 95 % by weight, even more preferably sums up to 98 % by weight, based on the total weight of the copolymer.
- 30 9. The copolymer according to any one of claims 1 to 8, wherein the total amount of monomer units derived from monomers a), b) and c) in the copolymer sums up to 90 % by weight, preferably sums up to 95 % by weight, more preferably sums up to 98 % by weight, most preferably sums up to 100 % by weight, based on the total weight of the copolymer.
- 35 10. The copolymer according to any one of claims 1 to 9, wherein the copolymer has a weight average molecular weight from 5,000 to 30,000 g/mol, preferably from 7,000 to 25,000 g/mol, even more preferably from 8,000 to 20,000 g/mol according to DIN 55672-1.
11. The copolymer according to any one of claims 1 to 10, wherein the copolymer has a PDI from 1 to 4, preferably from 1.5 to 3.5.

12. The copolymer according to any one of claims 1 to 11, wherein the copolymer has a COC flashpoint above 250°C according to ASTM D92.
- 5 13. A method for the preparation of a copolymer as defined in any one of claims 1 to 12, wherein the method comprises the steps of:
- i) providing a monomer composition,
 - ii) initiating radical polymerization in the monomer composition to obtain the copolymer.
- 10 14. A lubricant composition comprising one or more base oil and at least one copolymer according to any one of claims 1 to 12.
- 15 15. Use of a copolymer as defined in any one of claims 1 to 12 as a lubricant additive or a synthetic base fluid in a lubricating oil composition, preferably in a gear oil composition, a transmission oil composition, a hydraulic oil composition, an engine oil composition, a marine oil composition, an industrial lubricating oil composition or in grease.