CLAIMS

1. A method for producing a methacrylic polymer composition, which comprises

a first polymerization step wherein a raw material composition A comprising a raw material monomer A containing no less than 50% by weight of methyl methacrylate, a polymerization initiator A, and a chain transfer agent A is supplied into a first complete mixing type reactor through a supply port of the reactor, and the raw material composition A is subjected to a continuous bulk polymerization in the first complete mixing type reactor, and a resulting intermediate composition is withdrawn through an effluent port of the first complete mixing type reactor; and

a second polymerization step wherein a raw material composition B comprising a raw material monomer B containing no less than 50% by weight of methyl methacrylate, a polymerization initiator B, and a chain transfer agent B, and the intermediate composition withdrawn in the first polymerization step are supplied into a second complete mixing type reactor through a supply port of the reactor, and the raw material composition B and the intermediate composition are further subjected to a continuous bulk polymerization in the second complete

mixing type reactor, and a resulting methacrylic polymer composition is withdrawn through an effluent port of the second complete mixing type reactor;

wherein the following formulae (I), (II), (III), (IV) and (V) are satisfied:

$$120 \leq T1 \leq 160 \quad (I)$$

$$140 \leq T2 \leq 180 \quad (II)$$

$$20 \leq T2-T1 \leq 60 \quad (III)$$

$$1.7 \leq [S2]/[S1] \quad (IV)$$

$$1 \leq Q1/Q2 \leq 50 \quad (V)$$

wherein

T1 is a temperature (°C) in the first complete mixing type reactor in the first polymerization step,

T2 is a temperature (°C) in the second complete mixing type reactor in the second polymerization step,

[S1] is a concentration (% by weight) of the chain transfer agent A in the raw material composition A supplied into the first complete mixing type reactor,

[S2] is a concentration (% by weight) of the chain transfer agent B relative to the total amount of the raw material composition B and the intermediate composition, both of which are supplied into the second complete mixing type reactor,

Q1 is a flow rate (cm^3/min) of the intermediate composition supplied into the second complete mixing type reactor, and

Q2 is a flow rate (cm^3/min) of the raw material composition B supplied in the second complete mixing type reactor.

2. The method according to claim 1, wherein the following formulae (VI) and (VII) are further satisfied:

$$40 \leq x \leq 60 \qquad \text{(VI)}$$

$$\theta 1 + \theta 2 \leq 180 \qquad \text{(VII)}$$

wherein

x is a polymerization conversion (% by weight) of the methacrylic polymer composition withdrawn through the effluent port of the second complete mixing type reactor,

$\theta 1$ is an average residence time (min) in the first complete mixing type reactor in the first polymerization step, and

$\theta 2$ is an average residence time (min) in the second complete mixing type reactor in the second polymerization step.

3. The method according to claim 1, wherein each of the

effluent ports of the first and second complete mixing type reactors is located on a top of each of the reactors.

4. The method according to claim 1, wherein the continuous bulk polymerizations in the first polymerization step and the second polymerization step are conducted under adiabatic conditions.