WHAT IS CLAIMED IS:

1. A reforming process for producing aromatic hydrocarbons comprising providing a hydrocarbonaceous feed predominantly comprising a naphtha fraction; separating the hydrocarbonaceous feed into a first feedstream predominantly comprising C_{8+} hydrocarbons and a second feedstream predominantly comprising C_{7-} hydrocarbons;

contacting the first feedstream, or a fraction thereof, with a first reforming catalyst in a first reformer comprising the first reforming catalyst under first reforming conditions effective to form a first reformate comprising aromatic hydrocarbons, wherein the first catalyst is primarily selective for reforming C_{8+} hydrocarbons to aromatic hydrocarbons;

contacting the second feedstream, or a fraction thereof, with a second reforming catalyst in a second reformer comprising a second catalyst under second reforming conditions effective to form a second reformate, wherein the second catalyst is primarily selective for reforming C_{7-} hydrocarbons to aromatic hydrocarbons and the second reformer is in parallel flow configuration with the first reformer; and optionally, combining the first reformate, or a fraction thereof, with the second reformate, or a fraction thereof; and

wherein the catalyst selective for reforming C_{7-} hydrocarbons is selected from ZSM-5, ZSM-11, ZSM-12, ZSM-22, ZSM-23, ZSM-35, ZSM-38, ZSM-48, MCM- 22, SSZ-20, SSZ-25, SSZ-26, SSZ-32, SSZ-33, SSZ-35, SSZ-37, SSZ-42, SSZ-43, SSZ-44, SSZ-45, SSZ-47, SSZ-58, SSZ-74, SUZ-4, EU-1, NU-85, NU-87, NU-88, IM-5, TNU-9, ESR-10, TNU-10, or a combination thereof.

2. A method for modifying a catalytic reforming process, wherein, the catalytic reforming process comprises a first reformer comprising a first reforming catalyst primarily selective for reforming C_{8+} hydrocarbons to aromatic hydrocarbons;

the method comprising,

separating a hydrocarbonaceous feed to the first reformer predominantly comprising a naphtha fraction into a first feedstream predominantly comprising C_{8+} hydrocarbons and a second feedstream predominantly comprising C_{7-} hydrocarbons;

adding a second reformer to the catalytic reforming process, in parallel flow configuration with the first reformer, the second reformer comprising a second reforming catalyst primarily selective for reforming C_{7-} hydrocarbons to aromatic hydrocarbons;

wherein the modified catalytic reforming process comprises:

providing a hydrocarbonaceous feed predominantly comprising a naphtha fraction;

separating the hydrocarbonaceous feed into a first feedstream predominantly comprising C_{8+} hydrocarbons and a second feedstream predominantly comprising C_{7-} hydrocarbons;

contacting the first feedstream, or a fraction thereof, with a first reforming catalyst in a first reformer comprising the first reforming catalyst under first reforming conditions effective to form a first reformate, wherein the first catalyst is primarily selective for reforming C_{8+} hydrocarbons to aromatic hydrocarbons;

contacting the second feedstream, or a fraction thereof, in a second reformer comprising the second catalyst under second reforming conditions effective to form a second reformate, wherein the second catalyst is primarily selective for reforming C_{7-} hydrocarbons to aromatic hydrocarbons, wherein the catalyst selective for reforming C_{7-} hydrocarbons is selected from ZSM-5, ZSM-11, ZSM-12, ZSM-22, ZSM-23, ZSM-35, ZSM-38, ZSM-48, MCM- 22, SSZ-20, SSZ-25, SSZ-26, SSZ-32, SSZ-33, SSZ-35, SSZ-37, SSZ-42, SSZ-43, SSZ-44, SSZ-45, SSZ-47, SSZ-58, SSZ-74, SUZ-4, EU-1, NU-85, NU-87, NU-88, IM-5, TNU-9, ESR-10, TNU-10, or a combination thereof; and

optionally, combining the first reformate, or a fraction thereof, with the second reformate, or a fraction thereof.

3. The process of claim 1 or the method of claim 2, wherein the first and second catalysts are not the same.

4. The process of claim 1 or the method of claim 2, wherein the C_{7-} hydrocarbon fraction is directly or indirectly fed to the catalyst selective for reforming C_{7-} hydrocarbons to aromatic hydrocarbons.

5. The process of claim 1 or the method of claim 2, wherein the C_{8+} hydrocarbon fraction is directly or indirectly fed to the catalyst selective for reforming C_{8+} hydrocarbons to aromatic hydrocarbons.

6. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{7-} hydrocarbons comprises a zeolite having a silica to alumina molar ratio of at least 200, or at least 400, or at least 500, or at least 1000, or at least 1500, or at least 2000, a

crystallite size of less than 10 microns.

~~7. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{7-} hydrocarbons is selected from ZSM-5, ZSM-11, ZSM-12, ZSM-22, ZSM-23, ZSM-35, ZSM-38, ZSM-48, MCM- 22, SSZ-20, SSZ-25, SSZ-26, SSZ-32, SSZ-33, SSZ-35, SSZ-37, SSZ-42, SSZ-43, SSZ-44, SSZ-45, SSZ-47, SSZ-58, SSZ-74, SUZ-4, EU-1, NU-85, NU-87, NU-88, IM-5, TNU-9, ESR-10, TNU-10, or a combination thereof.~~

~~8.~~7. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{7-} hydrocarbons is selected from ZSM-5, ZSM-11, ZSM-12, ZSM-22, ZSM-23, ZSM-35, ZSM-38, ZSM-48, or a combination thereof.

~~9.~~8. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{7-} hydrocarbons comprises ZSM-5.

~~10.~~9. The process or the method of claim ~~9~~8, wherein the ZSM-5 has a silica to alumina molar ratio of at least 200, or at least 400, or at least 500, or at least 1000, or at least 1500, or at least 2000.

~~11.~~10. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{7-} hydrocarbons comprises in the range of between 0.1 wt.% and 5 wt.%, or between 0.1 wt.% and 2 wt.%, or between 0.1 wt.% and 1 wt.%, or between 0.2 wt.% and 0.6 wt.%, of a Group VIIIB metal, or a Group VIIIB metal selected from nickel, ruthenium, rhodium, palladium, iridium, platinum, or a combination thereof, or a Group VIIIB metal selected from iridium, palladium, platinum, or a combination thereof, or a Group VIIIB metal comprising platinum.

~~12.~~11. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{7-} hydrocarbons comprises in the range of between 0.1 wt.% and 5 wt.%, or between 0.1 wt.% and 2 wt.%, or between 0.1 wt.% and 1 wt.%, or between 0.2 wt.% and 0.6 wt.%, of a Group VIIIB metal other than platinum, or a metal selected from rhenium, germanium, tin, lead, gallium, indium, or a combination thereof, or a metal comprising rhenium.

~~13.~~12. The process of claim 1 or the method of claim 2, wherein the catalyst selective for reforming C_{8+} hydrocarbons comprises a non-zeolitic naphtha reforming catalyst, or an alumina supported non-zeolitic catalyst comprising a Group VIIIB metal.

~~14.~~13. The process of claim 1 or the method of claim 2, wherein the reforming of the C_{7-} hydrocarbons to aromatic hydrocarbons includes conditions of: a pressure in the range of 50 to 300 psi, preferably 60 to 200 psi, more preferably, 70 to 150 psi; a temperature in the range of

800°F to 1100°F, preferably 850°F to 980°F; an LHSV of 0.1 to 3.0 hr^{-1}, preferably 0.5 to 2.5 hr^{-1}, more preferably 1.0 to 2.0 hr^{-1}; and a H_2 : HC hydrogen to hydrocarbon molar ratio in the range of 1:1 to 6:1, preferably 1.5:1 to 3:1.

~~15.~~14. The process of claim 1 or the method of claim 2, wherein the reforming of the C_{8+} hydrocarbons to aromatic hydrocarbons includes conditions of: a pressure in the range of 100 to 500 psi, preferably 150 to 450 psi, more preferably, 200 to 440 psi; a temperature in the range of 800°F to 1100°F, preferably 850°F to 980°F; an LHSV of 0.1 to 3.0 hr^{-1}, preferably 0.5 to 2.5 hr^{-1}, more preferably 1.0 to 2.0 hr^{-1}; and a H_2 : HC hydrogen to hydrocarbon molar ratio in the range of 1:1 to 7:1, preferably 3:1 to 6:1.