

Description

This invention relates to catalytic dewaxing.

Dewaxing processes of various kinds are widely used in the petroleum refining industry to improve the fluidity at low temperatures of various petroleum fractions, including fuels such as jet fuel, kerosene, home heating oil, diesel fuel as well as lubricants, where the necessity of procuring good low temperature performance is particularly pressing because the paraffinic nature of lubricants coupled with the high molecular weight of the lubricant fractions generally implies a relatively high wax content which will lead to poor low temperature performance unless adequate remedial measures are taken. Originally, dewaxing was carried out by physical techniques, especially solvent dewaxing using solvent mixtures such as MEK/toluene or by autorefrigerant processes such as propane dewaxing. More recently, however, catalytic dewaxing processes have established themselves commercially. Catalytic dewaxing processes are available both for fuels and for lubricants. The Mobil Distillate Dewaxing process (MDDW) is useful with fuels such as jet fuel and diesel fuel and the Mobil Lube Dewaxing process (MLDW) with lubricants, including distillate (neutral) and residual (bright stock) types. The MDDW and MLDW processes both employ shape-selective cracking to remove waxy components, mainly normal and slightly branched chain paraffins, from the feed to produce a dewaxed product having a reduced pour point which is dependent on the severity of the processing. The MLDW process employs a second reactor containing a hydrofinishing catalyst which ensures that the dewaxed lube product meets all applicable quality and engine performance criteria, as described in "Industrial Application of Shape-Selective Catalysis": Catal. Rev.-Sci. Eng. 28 (2-3) 185-264 (1986), especially page 244. See also Refining Process Handbook (Hydrocarbon Processings, September, 1986), pages 89,90 and, as an example of an early proposal in this field, Oil and Gas Journal, 6 January 1975, pages 69-73.

Catalytic dewaxing processes selectively remove the longer chain, waxy paraffins, mainly n-paraffins and mono-methyl paraffins from the feed. Most processes of this type operate by selectively cracking the waxy paraffins to produce lower molecular weight products which may then be removed by distillation from the higher boiling lube stock. The catalysts which have been proposed for this purpose have usually been zeolites which have a pore size which admits the straight chain, waxy n-paraffins either alone or with only slightly branched chain paraffins but which exclude the less waxy, more highly branched materials and cycloaliphatics. Zeolites such as ZSM-5, ZSM-11, ZSM-12, ZSM-22, ZSM-23, ZSM-35 and ZSM-38 have been proposed for this purpose in dewaxing processes, as described in U.S. Patent Nos. Re 28,398 (3,700,585); 3,852,189; 3,894,938; 4,176,050; 4,181,598; 4,222,855; 4,229,282; 4,287,388; 4,259,170; 4,283,271; 4,283,272; 4,357,232 and 4,428,819 to which reference is made for details of such processes. A dewaxing process employing synthetic offretite is described in U.S. Patent No. 4,259,174. A process using a mixture of zeolites of different pore sizes is disclosed in U.S. Patent No. 4,601,993. Reference is made to these patents for details of such processes.

The catalytic dewaxing processes using intermediate pore size zeolites such as ZSM-5 operate, as described above, by selectively cracking the waxy components of the feed. This results in a loss in yield since the components which are in the lube boiling range undergo a bulk conversion to lower boiling fractions which, although they may be useful in other products, must be removed from the lube stock. Another approach to processing of lube stocks is described in U.S. Patent Nos. 4,419,220 and 4,518,485, in which the waxy components of the feed, comprising straight chain and slightly branched chain paraffin, are removed by isomerization over a catalyst based on zeolite beta. During the isomerization, the waxy components are converted to relatively less waxy isoparaffins and at the same time, the slightly branched chain paraffins undergo isomerization to more highly branched aliphatics. A measure of paraffin cracking does take place during the operation so that not only is the pour point reduced by reason of the isomerization but, in addition, the heavy ends undergo some cracking or hydrocracking to form liquid range materials which contribute to a low viscosity product. The degree of cracking is, however, limited so as to maintain as much of the feedstock as possible in the desired boiling range.

The catalysts used in these processes have invariably included a binder in addition to the zeolite, at least when the process was to be operated on a commercial scale. There is a number of reasons for this. First, in a commercial scale unit, a considerable depth of catalyst is maintained in the conventional trickle-bed, downflow reactor so that the catalyst at the bottom of the bed requires significant crushing resistance to withstand the weight of catalyst above. It also requires considerable attrition resistance to withstand the stresses of handling during manufacture and loading into the unit. A further consideration is that it should be practicable to produce the catalyst in the desired particle size and shape using conventional equipment and this requirement generally implies that the catalyst should be capable of being produced by extrusion.

Extrusion is one way of obtaining a material which has a high degree of strength for various applications, both catalytic and noncatalytic. Some aluminosilicate zeolites have long been used as catalysts for a wide variety of organic conversion processes and, in general, crystalline aluminosilicate zeolites are incorporated with a matrix or binder material in order to impart strength to them. The most commonly used matrix materials have

included alumina and mixtures of alumina with clays because these materials were very easy to extrude and resulted in the production of an extrudate which had desirable physical strength.

Silica is known to be a desirable matrix and possesses advantages over alumina in certain catalytic reaction. For example U.S. Patent No. 4,013,732 discloses ZSM-5 with a silica matrix, see Column 7. U.S. Patent No. 3,843,741 and U.S. Patent No. 3,702,886 would broadly teach the use of ZSM-5 with a silica matrix. Thus, although it was considered desirable to composite ZSM-5 with a silica matrix, it was not possible to do this by an extrusion because silica and zeolites will not extrude in conventional extruding equipment to give reasonably strong products. The only way that composites of ZSM-5 and silica could be made was by a pilling or pelleting which involved mixing silica and the appropriate zeolite and squeezing it together to form a shaped structure having minimum physical strength.

Catalysts may be produced from silica gels. U.S. Patent No. 3,969,274 describes the advantages of having silica as a support for catalysts but utilizes a silica gel which has been subjected to steam treating in order to enhance its crush strength. A steaming step is stated to be required in order to make the process operable.

Silica-zeolite pellets or extrudates may be treated with various materials in order to increase their strength. For example, U.S. Patent No. 3,846,337 discloses silica-bound silicate particles of improved crush strength which can be prepared by admixing reactive silica sols with siliceous particles, and contacting the resulting combination with ammonium phosphate, an acid phosphate or both.

U.S. Patent No. 4,111,843 describes the preparation of porous silica particles by adding excess alkali to a water glass and then precipitating a hydrogel with acid. The excess alkali is stated to be responsible for increasing pore diameter. The patent discloses (Column 2, line 15), that the extrudability of microporous silica-alumina catalyst carriers of exceptional strength can be achieved by following the process of the patent. However, the patent does not disclose anything with regard to extrudates of silica particles, (see Column 6, line 66 and following).

U.S. Patent No. 4,582,815 and its corresponding European Publication No. 167324 disclose a method for making extrudates of exceptional strength, by mulling either pure silica, or a crystalline aluminosilicate zeolite, or more preferably, a mixture of silica with a crystalline aluminosilicate zeolite with water to a solids level of 25 to 75 percent in the presence of 0.25 to 10 weight percent of a basic material such as sodium hydroxide (calculated as solid sodium hydroxide and based on the total solids present).

It is theorized in U.S. Patent 4,582,815 that the successful extrusion or formation of shaped bodies by wetting and compressing powders requires that the particles be capable of being brought into close proximity with each other so that the van der Waals forces become operative in subsequently holding the particle together. Chemical binding by crosslinking may also occur for some binders but the initial requirement is still for close packing. Highly siliceous materials like silica and zeolites of high silica-to-alumina ratios are hydrophobic. It has been discovered that by substituting an alkali metal for hydrogen in the silanol groups on the outside surfaces of siliceous materials they can generally thereby be made more easily extrudable with crush strengths far exceeding those heretofore described for silica-bound materials.

It has now been found that in catalytic dewaxing processes, the aging rate of the catalyst may be reduced by almost an order of magnitude by forming the particles of the dewaxing catalyst entirely from the zeolite which effects the dewaxing, that is, the catalyst particles are formed from the zeolite without any added binder. The binder-free catalysts have a significant advantage over catalysts prepared by binding the zeolite with a matrix-forming oxide such as silica or alumina. The substantially reduced aging rates obtained with the binder-free catalysts enable cycle lengths to be increased with a greater stream factor and less down-time related to catalyst reactivation or regeneration. In addition, adverse side reactions catalysed by the binder are eliminated and the dewaxed products may be found to possess improved oxidation stability.

According to the present invention there is therefore provided a catalytic dewaxing process in which a waxy hydrocarbon feed is catalytically dewaxed by means of a dewaxing catalyst comprising a binder-free zeolite having dewaxing activity. In most cases, the zeolite will be an intermediate pore size zeolite having acidic functionality, preferably ZSM-5, ZSM-11 or ZSM-23 although other zeolites may also be employed. The catalyst will normally be employed in the form of an extrudate i.e. a solid particle produced by a process of extrusion.

Figures 1 and 2 are graphs showing aging comparisons for various dewaxing catalysts described below. The present process dewaxes a variety of waxy hydrocarbon feeds usually having an initial boiling point of at least 315°C (600°F) and more usually 343°C (65°F). Lubricants are a special class of hydrocarbon fractions which may be dewaxed by the present process since catalyst aging problems have been most severe with lube feeds.

Lubricant feeds boil in the lube boiling range, i.e. 315°C+ (600°F+) and usually 345°C+ (650°F+) and are of suitable lubricating characteristics. They are conventionally produced by the vacuum distillation of a fraction from a crude source of suitable type. Generally, the crude will be subjected to an atmospheric distillation and the atmospheric residuum (long resid) will be subjected to vacuum distillation to produce the initial lube stocks.

The vacuum distillate stocks of "neutral" stocks are generally highly paraffinic fractions of relatively low viscosity ranging typically from 20 cST (100 SUS) at 40°C for a light neutral to about 160 cST (750 SUS) at 40°C for a heavy neutral. The vacuum resid may be used as a source of more viscous lubes after deasphalting, usually by propane deasphalting (PDA) followed by solvent extraction to remove undesirable, high viscosity, low viscosity index (V.I.) aromatic components, using a solvent which is selective for aromatics such as furfural, phenol, or dimethylformamide. The raffinate is generally referred to as Bright Stock and typically has a viscosity of 1000 to 3000 SUS at 100°C (210 to 610 cST). The neutral fractions may also be subjected to solvent extraction to improve their V.I. and other qualities by selective removal of the aromatics.

Lube feeds may also be obtained by other procedures whose general objective is to produce an oil of suitable lubricating character from other sources, including marginal quality crudes, shale oil, tar sands and/or synthetic stocks from processes such as methanol or olefin conversion or Fischer-Tropsch synthesis. The lube hydrocracking process is especially adapted to use in a refinery for producing lubricants from asphaltic or other marginal crude sources because it employs conventional refinery equipment to convert the relatively aromatic (asphaltic) crude to a relatively paraffinic lube range produce by hydrocracking. Integrated all-catalytic lubricant production processes employing hydrocracking and dewaxing are described in U.S. Patents Nos. 4,414,097; 4,283,271; 4,283,272; 4,383,913; 4,347,121; 3,684,695 and 3,755,145. Processes for converting low molecular weight hydrocarbons and other starting materials to lubestocks are described, for example, in U.S. Patents Nos. 4,547,612; 4,547,613; 4,547,609; 4,517,399 and 4,520,221, to which reference is made for a description of these processes.

The present dewaxing process is of particular utility with lube feeds, by reason of their characteristics, have an extremely adverse effect on the catalyst aging rate. Feeds of this type typically include highly paraffinic, highly waxy feeds such as those derived from Libyan or Pacific Basin crude sources. Feeds of this type normally include at least 25 weight percent paraffins or more, for example, at least 35 or even at least 50 weight percent paraffins. The rapid catalyst aging associated with feeds of this type is believed to be caused by the rapid accumulation of coke during the cracking of the large quantity of waxy components in feeds of this type. A typical feed of this type is the Minas (Indonesian) gas oil whose composition is given in Table 1 (raw) and Table 2 (hydrotreated) below. A paraffinic North Sea feed has its composition shown in Table 3 below.

Table 1
Minas Gas Oil

Nominal boiling range, °C(°F)	345°-540° (650°-1000°)
API Gravity	33.0
Hydrogen, wt pct	13.6
Sulfur, wt pct	0.07
Nitrogen, ppmw	320
Basic Nitrogen, ppmw	160
CCR	0.04
Composition, wt pct	
Paraffins	60
Naphthenes	23
Aromatics	17
Bromine No.	0.8
KV, 100°C, cSt	4.18
Pour Point, °C(°F)	46 (115)
95% TBP, °C(°F)	510 (950)

Table 2
HDT Minas Feed

	Nominal boiling range, °C(°F)	345-510 (650-950)
5	API Gravity	38.1
	H, wt pct	14.65
	S, wt pct	0.02
	N, ppmw 16	
	Pour Point, °C(°F)	38 (100)
	KV at 100°C, cSt	3.324
10	P/N/A wt pct	
	Paraffins	66
	Naphthenes	20
	Aromatics	14

15 NOTE: Hydrotreated over Ni-Mo/Al₂O₃ hydrotreating catalyst, 800 psig H₂, 367° - 391°C (710° - 735°F), 1 LHSV, 712 l.l.⁻¹ hydrogen:feed ratio.

Table 3
HDT North Sea Gas Oil

	Nominal boiling range, °C	345-455 (650-850)
25	API Gravity	31.0
	H, wt pct	13.76
	S, wt pct	0.012
	N, ppmw	34
	Pour Point, °C(°F)	32 (90)
	KV at 100°C cSt	4.139
30	P/N/A wt pct.	
	Paraffins	30
	Naphthenes	42
	Aromatics	28

35 The waxy nature of a feed is indicated, of course, by poor fluidity properties such as pour point or freeze point. Pour point is a particularly good measure of waxiness. Feeds with pour points above about 40°C (about 100°F) e.g. about 43°C or higher (110°F or higher) are particularly apt for treatment in the present process because feeds of this type have typically given substantial aging problems with more conventional catalytic dewaxing processes. Highly waxy feeds of this type typically include feeds derived, as mentioned above, from Libyan and Pacific Basin crude sources including mainland Chinese sources but they may also have other origins, for example, Kirkuk lube feeds have high pour points, typically above about 43°C (110°F) e.g. 46°C (114°F) and they usually cause rapid aging in conventional alumina-bound dewaxing catalysts. The present binder-free dewaxing catalyst, on the other hand, enables feeds of this kind to be dewaxed with long effective cycle lengths.

45 Another class of lube range feeds with which the present process is particularly useful are the feeds which contain large quantities of contaminants, especially of heteroatoms such as nitrogen and sulfur. Feeds of this type generally cause rapid catalyst aging because the contaminants block the acidic sites on the catalyst and, for this reason, basic contaminants e.g. basic nitrogen are particularly troublesome, especially when coupled with high paraffin levels as with certain mainland Chinese feeds. Basic nitrogen levels of 100 ppm or higher e.g. 200 or 400 ppm are associated with rapid aging particularly at paraffin contents above 25 weight percent and feeds of this type are particularly apt to be treated by the present process.

50 The compositions of two mainland Chinese origin lube feeds of this type are set out in Tables 4 and 5 below. Table 4 gives the properties of a waxy heavy neutral of mainland Chinese origin, and Table 5 gives the properties of a propane deasphalted resid.

Table 4
Heavy Neutral Properties

5	SP.Gr., 15/4°C	0.8826
	Viscosity, cSt @100°C	11.4
	@150°C	4.49
	Pour Point, °C	57.5
	Color (ASTM)	D8.0
10	Flash Point (C.L.), °C	288
	Total Nitrogen, ppmw	1000
	Basic Nitrogen, ppmw	460
	Sulfur, ppmw	1100
	Carbon, wt pct	86.37
15	Hydrogen, wt pct	13.38
	RCR, wt pct	0.38
	R.I. @70°C	1.47
	Oil Content, wt pct	63.4
	Aniline Point, °C	115.6
20	Distillation (D8-1160), °C	
	IBP/5 vol pct	201/451
	10/20	467/486
	30/40	496/505
	50/60	513/522
25	70/80	532/542
	90/95	- / -
	Aromatic Fraction (fa)*	0.067

* Calculated by The Densimetric Method

Table 5
PDA Resid

5	SP.Gr., 15/4°C	0.8875
	Viscosity, cSt @100°C	24.3
	@150°C	8.41
	Pour Point, °C	50.0
	Color (ASTM)	D8.0
10	Flash Point (C.L.), °C	306
	Total Nitrogen, ppmw	1200
	Basic Nitrogen, ppmw	580
	Sulfur, ppmw	1000
	Carbon, wt pct	86.39
15	Hydrogen, wt pct	13.42
	RCR, wt pct	0.68
	R.I. @70°C	1.4719
	Oil Content, wt pct	52.8
	Aniline Point, °C	130.8
20	Distillation (D8-1160), °C	
	IBP/5 vol pct	309/486
	10/20	516/552
	30/40	- / -
25	Aromatic Fraction (fa)*	0.055

* Calculated by The Densimetric Method

30 The improvements in catalyst aging rate are noted most with the feedstocks which present the greatest difficulties in processing with conventional alumina-bound catalysts. Aging problems have been severe when operating with particular stocks and alumina-bound dewaxing catalysts and accordingly, the present self-bound catalysts afford a solution when these problems are encountered. The present dewaxing process is of significant utility with lube feeds which have an initial boiling point of at least about 399°C (750°F) and of especial utility with those having an initial boiling point of about 415°C (775°F) and a 50% point of at least about 455°C (850°F) or higher (ASTM method D-1160). Residual type feeds such as bright stocks which have presented processing difficulties will benefit from the use of the present catalysts. Feeds of this type have an IBP of at least about 399°C (750°F), usually at least about 415°C (775°F) with a 50% point of at least about 510°C (950°F), usually at least about 540°C (1000°F) by ASTM method D1160-1 133Pa (1mm Hg).

40 Prior to the catalytic dewaxing the feed may be subjected to hydrotreating under conventional conditions, if necessary, to remove heteroatoms and possibly to effect some aromatics saturation.

The dewaxing catalyst comprises particles of a zeolite having dewaxing capability, i.e., the capability of selectively removing waxy hydrocarbon components from the feed. The preferred zeolites for this purpose are the intermediate pore size zeolites which are characterized by a Constraint Index of 1 to 12, as described in J. Catalysis 67, 218-222 (1981). As described there, a Constraint Index of 1 to 12 is related to the structure of the zeolite and is associated with zeolites which have a channel system with windows of 10-membered rings although constrained, shape-selective cracking is also observed with other structures such as that of TMA offretite. In fact, TMA offretite may be more selective in its dewaxing than some of the true intermediate pore size (10-ring) zeolites such as ZSM-5, as noted in "TMA Offretite: Relationship Between Structure and Catalytic Properties", Chen et al, J. Catalysis 86, 24-31 (1984). The utility of a zeolite for shape selective dewaxing is therefore appropriately determined by the Constraint Index rather than structure since this is a measure of shape-selective properties. The method by which Constraint Index is to be determined is described in U.S. Patent No. 4,016,218, to which reference is made for a description of the method.

Constraint Index (C.I.) values for some typical materials are given in Table 6 below:

Table 6
Constraint Index

	<u>temperature)</u>	<u>CI (at test</u>
	ZSM-4	0.5 (316°C)
	ZSM-5	6-8.3 (371°C-316°C)
10	ZSM-11	5-8.7 (371°C-316°C)
	ZSM-12	2.3 (316°C)
	ZSM-20	0.5 (371°C)
	ZSM-22	7.3 (427°C)
	ZSM-23	9.1 (427°C)
15	ZSM-34	50 (371°C)
	ZSM-35	4.5 (454°C)
	ZSM-38	2 (510°C)
	ZSM-48	3.5 (538°C)
	ZSM-50	2.1 (427°C)
20	TMA Offretite	3.7 (316°C)
	TEA Mordenite	0.4 (316°C)
	Clinoptilolite	3.4 (510°C)
	Mordenite	0.5 (316°C)
	REY	0.4 (316°C)
25	Amorphous Silica-alumina	0.6 (538°C)
	Dealuminized Y	0.5 (510°C)
	Erionite	38 (316°C)
	Zeolite Beta	0.6-2.0 (316°C-399°C)

30 The nature of the Constraint Index parameter and the technique by which it is determined admit of the possibility that a given zeolite can be tested under different conditions to give different values of Constraint Index. Constraint Index seems to vary with severity of operation (conversion) and the presence or absence of binders. Likewise, other variables, such as crystal size of the zeolite, the presence of occluded contaminants, etc., may affect the Constraint Index. It is therefore possible so to select test conditions, e.g. temperature, as to establish
35 more than one value for the Constraint Index of a particular zeolite. This explains the range of Constraint Indices for some zeolites, such as ZSM-5, ZSM-11 and Beta.

The above CI values typically characterize the specified zeolites, but the specified values are the cumulative result of several variables in the determination and calculation of the index. Thus, for a given zeolite exhibiting a CI value within the range of 1 to 12, depending on the temperature employed during the test method
40 within the range of 290°C to about 538°C, with accompanying conversion between 10% and 60%, the CI may vary. Likewise, other variables such as the crystal size of the zeolite, the presence of possibly occluded contaminants and binders intimately combined with the zeolite may affect the CI. The determination of CI therefore affords a means for characterizing the zeolites of interest which is approximate, taking into consideration the manner of its determination, with the possibility, in some instances, of compounding variable extremes. However,
45 in all instances, at a temperature within the above-specified range of 290°C to about 538°C, the CI will have a value within the approximate range of 1 to 12 for the preferred class of zeolites which exhibit shape-selective dewaxing characteristics. The intermediate pore size zeolites perform the shape-selective dewaxing by selectively cracking the waxy components of the feed, as mentioned above and as described in greater detail in "Industrial Application of Shape-Selective Catalysis", Chen et al, *Catal. Rev.-Sci.Eng.* 28 (2 & 3), 185-264
50 (1986), especially 199-208, 241-247, to which reference is made for a description of these dewaxing processes. Intermediate pore size zeolites which may be used for catalytic dewaxing include ZSM-5, ZSM-11, ZSM-22, ZSM-23, ZSM-48 and synthetic ferrierites such as ZSM-35 and ZSM-38. Of these ZSM-5 and ZSM-11 are preferred, although ZSM-23 and synthetic ferrierites such as ZSM-35 and ZSM-38 provide highly shape-selective dewaxing properties by reason of the highly constrained access which they provide for paraffinic species.
55 Because the dewaxing proceeds by a shape-selective cracking mechanism, no metal component on the catalyst is needed but a metal component such as nickel or palladium, having hydrocarbon functionality may optionally be present because such components may improve removal of coke during catalyst reactivation. Up to about 5 wt.% metal is sufficient, typically about 1 wt.% being satisfactory for this purpose.

It has also been found that dewaxing may be effected by a process of isomerizing of the waxy paraffinic components, mainly normal and slightly branched chain paraffins, to less waxy iso-paraffinic components which also possess high viscosity indices. This process has the potential for improved yield since the undesired waxy components are not removed from the appropriate product boiling range by cracking but, rather, by isomerization to acceptable product components within the same boiling range. Zeolite beta is effective for dewaxing in this way. Catalytic dewaxing processes employing beta are described in U.S. Patents Nos. 4,419,220 and 4,518,485 to which reference is made for a description of such processes.

In general terms the catalytic dewaxing processes are operated under conditions of elevated temperature, usually ranging from about 205° to 427°C (400° to 800°F), but more commonly from 260° to 371°C (500° to 700°F), e.g. 315° to 371°C (600° to 700°F), depending on the dewaxing severity necessary to achieve the target pour point, with the temperature increasing in each dewaxing cycle to compensate for decreasing catalyst activity. Hydrogen is not required stoichiometrically but promotes extended catalyst life by reductive coke removal. The process is therefore carried out in the presence of hydrogen, usually at relatively low pressure below 1000 psig (7000 kPa) and typically at 400-800 psig (2860 to 562 kPa, abs.). Hydrogen circulation rate is typically 1000-4000 SCF/bbl, usually 2000 to 3000 SCF/bbl (about 180 to 710, usually 355 to 535 n.l.-1). Space velocity will vary according to the charge stock and the severity needed to achieve the target pour point but is typically in the range of 0.5 to 5 LHSV (hr⁻¹), usually 1 to 2 LHSV.

The dewaxing process is operated cyclically with the catalyst being subjected to restorative treatment from time to time to restore its dewaxing activity and selectivity. Catalyst deactivation occurs progressively during each dewaxing cycle between successive restorative treatments, mainly by the accumulation of coke and inhibitors on the catalyst. Restorative treatment may be either oxidative, by treatment with oxygen-containing gas at elevated temperature to remove coke and other inhibitors or, alternatively, by treatment with hydrogen at elevated temperature. Conditions for oxidative and reductive treatments as well established in such processes. Oxidative regeneration treatments are described, for example, in U.S. Patents Nos. 3,069,362 and 3,069,363 and G.B. Patent No. 1,148,545. Hydrogen reactivation treatments are described, for example, in U.S. Patents Nos. 4,358,395, 4,508,836 and 4,560,670.

The dewaxing may be carried out in conventional equipment, suitably in a fixed-bed, downflow, trickle reactor. Commercial reactors of this kind typically employ a catalyst bed 5m. deep with a diameter depending upon the capacity of the unit and the space velocity desired for the feed being used and the target pour point.

The present process employs a particular dewaxing catalyst which consists essentially of the zeolite. No binder is used. It has been found that when the zeolite is extruded without binder, unexpectedly low aging rates are achieved.

Although it would be expected that longer dewaxing runs could be achieved by eliminating the binder (because an increased amount of zeolite can be accommodated within a given reactor volume), the improvements which have been observed exceed the expected magnitudes by a significant amount. Current commercial dewaxing catalysts typically employ 35 wt% alumina binder and so, compared to such catalysts, the amount of zeolite which can be placed in an existing reactor is increased by about one half (100/65). A corresponding increase in cycle length would therefore be expected but it has been found that the extension in the duration of the dewaxing cycle between successive restorative treatments (typically hydrogen reactivation or oxidative regeneration) is greater than this and is largely to be attributed to the absence of the alumina binder. Although the alumina binder used for the catalysts has low acidity and therefore might not be expected to participate in non-shape-selective catalytic cracking reactions, it does nevertheless have a deleterious effect which is overcome by the use of the present unbound zeolite catalysts. The catalyst aging rates which have been observed with the present unbound catalysts are typically five to twelve times less than the rates achieved with otherwise comparable catalysts with an alumina binder, resulting in corresponding improvements in cycle duration.

The fact that the improvements in catalyst aging rate are real and substantial is demonstrated by comparison of the relative aging rates of the alumina-bound and unbound catalysts at comparable space velocities (LHSV) relative to the zeolite component. Reducing the space velocity on any dewaxing catalyst results in an improvement in aging but the improvements obtained with the present binder-free catalysts are better than would be expected on this basis of comparison.

A direct comparison between the alumina-bound and unbound catalysts with typical heavy neutral feeds indicates that the unbound catalyst achieves a reduction of 65 to 90 percent in the aging rate using the same zeolitic dewaxing component (on the same feedstock for the same product pour point and with otherwise identical process conditions e.g. space velocity). In practice, the space velocity (LHSV) will be from 0.1 to 3 hr.⁻¹, more usually 0.25 to 1.5 hr.⁻¹. Space velocities within this range are applicable even with charge stocks which are difficult to process with conventional alumina bound catalysts. The exact value of the space velocity should be selected according to the characteristics of the feed although, as a generalization, the space velocity should be towards the lower end of this range for the higher boiling feeds such as bright stock and at the higher end

for distillate feeds such as the neutral lubestocks and distillate fuels. In all cases where practical comparisons are mad at equal process rates over the same volume of catalyst (same LHSV), the binder-free catalyst gives substantially lower aging rates. With certain lubestocks which cannot be dewaxed successfully or economically with alumina-bound catalysts are quite amenable to treatment at practicable space velocities with the binder-free catalyst.

The improvements in aging rate obtained with the unbound catalysts are most marked at higher temperatures. Normally the temperature of the catalyst bed is raised progressively as the dewaxing cycle continues in order to compensate for the progressive deactivation of the catalyst. At higher temperatures, however, the oxidation stability of the dewaxed products decreases so that a limit is imposed on the extent to which cycle life can be extended by the expedient of increasing temperature. The present catalysts, however, produce products of superior oxidation stability especially at the higher temperatures characteristic of the end of the dewaxing cycle. In addition, the absence of the alumina binder is expected to improve dewaxing selectivity at higher temperatures so that it may be possible to extend the dewaxing cycle by continuing to raise the temperature beyond the point which would be acceptable with a conventional alumina-bound catalyst (with the same feed and product pour point), without excessive losses in yield or oxidation stability. During each dewaxing cycle the improvement in aging rate will become more apparent during the second half of the cycle as the higher temperatures are reached; for this reason, the progressive increase in temperature required to compensate for catalyst deactivation may be less in the second half of the cycle than in the first so that cycle duration may be extended by the reduced aging rate, especially during the second half of the cycle.

It is tentatively theorised that in the absence of a reactive binder, the aging mechanism is one which involves random plugging of the pores of the catalyst. With conventional alumina-bound dewaxing catalysts, it is the aging caused by the alumina that apparently causes loss of activity and selectivity even though the alumina is substantially inert. It is conceivable that the plugging which does take place is on the alumina itself and in the pores between the alumina and the zeolite so that, regardless of the continued viability of the zeolite, access to it by the feed is no longer possible. By eliminating the binder, the true aging rate of the zeolite becomes manifest and may be effectively exploited.

The unbound (or, alternatively, self-bound) dewaxing catalysts used in the present process are suitably produced by the extrusion method described in U.S. Patent No. 4,582,815, to which reference is made for a description of the method and of the extruded products obtained by its use. The method described there enables extrudates having high crush strength to be produced on conventional extrusion equipment and accordingly, the method is eminently suitable for producing the present catalysts which are silica-rich by reason of the silica content of the zeolite. The catalysts are produced by mulling the zeolite, as described in U.S. 4,582,815, with water to a solids level of 25 to 75 wt% in the presence of 0.25 to 10 wt% of basic material such as sodium hydroxide (calculated as solid basic material, based on total solids present). Further details are to be found in U.S. Patent 4,582,815.

The catalysts are used in the form of extruded shaped particles. The particles may be cylindrical, or polygonal e.g. square, rectangular, hexagonal, in cross section or any other shape which lends itself to formation by extrusion. Lobes shapes are particularly useful e.g. tri-lobe (cloverleaf) or quadrulobe. In any event, it is preferred to use extrudates which have a maximum diffusion distance of not more than 0.025 inch (0.63mm), preferably not more than 0.02 inch (0.51 mm) although larger size extrudates may be used in bigger reactors e.g. 0.03125 inch (0.8mm). Catalysts of this type are particularly useful for dewaxing residual feeds, for example, feeds with an IBP of at least 370°C (700°F) and a 50 vol. percent boiling point of at least 480°C (900°F). The use of shaped catalysts of this kind for dewaxing high boiling feeds is described in U.S. application Serial No. 938,214, filed 5 December 1986 and its counterpart EU 1,681,146, to which reference is made for details of such a process. The use of quadrulobe catalysts is described in U.S. Patent No. 4,016,067, of trilobed catalysts in U.S. Patent No. 3,674,680 and various other polylobular catalysts in U.S. Patents Nos. 4,118,310, 4,028,227, 3,764,565 and 3,966,644. The use of hollow catalyst particles is described in U.S. Patent No. 4,441,990. Reference is made to these disclosures for details of such shaped catalysts which may be used in the present process.

In order to improve the quality of the dewaxed lube products, a hydrotreating step may follow the catalytic dewaxing in order to saturate lube range olefins as well as to remove heteroatoms, color bodies and, if the hydrotreating pressure is high enough, to effect saturation of residual aromatics. Generally, however, the post-dewaxing hydrotreating is carried out in cascade with the dewaxing step so that the relatively low hydrogen pressure of the dewaxing step will prevail during the hydrotreating and this will generally preclude a significant degree of aromatics saturation. Generally, the hydrotreating will be carried out at temperatures from about 205° to 315°C (about 400° to 600°F), usually with higher temperatures for residual fractions (bright stock), for example, about 260° to 300°C (about 500° to 575°F) and lower temperatures for the neutral stocks, for example, about 220° to 260°C (about 425° to 500°F). System pressures will correspond to overall pressures typically

from 2860 to 7000 kPA, abs. (400 to 1000 psig) although lower and higher values may be employed. Space velocity in the hydrotreater is typically from 0.1 to 5 LHSV (hr^{-1}), and in most cases from 0.5 to 1 hr^{-1} .

Processes employing sequential lube catalytic dewaxing-hydrotreating are described in U.S. Patent Nos. 4,181,598; 4,137,148 and 3,894,938. A process employing a reactor with alternating dewaxing-hydrotreating beds is disclosed in U.S. Patent No. 4,597,854. Reference is made to these patents for details of such processes.

The hydrotreating catalysts which may be used before and after the dewaxing comprise a hydrogenation component on a porous support. Because the desired hydrogenation reactions require no acidic functionality and because no conversion to lower boiling products is desired in this step, the support is substantially non-acidic in character. Suitable supports include alumina, silica and silica-alumina. The hydrogenation component is typically a base metal of Groups VIA or VIIIA (IUPAC Table) such as nickel, cobalt, molybdenum or tungsten but may also be a noble metal such as palladium or platinum. Combinations of base metals such as cobalt-molybdenum, nickel-molybdenum are particularly favored. Hydrotreating catalysts of this type are commercially available.

Example 1

A 0.5 inch (12.5 mm.) diameter reactor was packed with 15 ml of 1/25 in. (1mm.) diameter cylindrical extrudate of ZSM-5 containing no added binder (packing density 0.62g./ml). The space above and below the catalyst was packed with quartz to improve the flow and the temperature profile. A bright stock raffinate of Arab Light crude origin was pumped over the catalyst at the rate of 15 ml/hour (1 LHSV) while the temperature was maintained at a value sufficient to produce a dewaxed oil of -7°C (20°F) pour point as measured by ASTM D-97. The run was arbitrarily stopped at 358°C (676°F) after 333 days on stream. The starting temperature, corrected for irregularities of pour point at start up was 279°C (535°F). The average aging rate was 0.24°C/day (0.43°F/day). The comparable aging rate for a comparable ZSM-5 dewaxing catalyst with 35% alumina binder catalyst, (65% zeolite) is 2.8°C/day (5°F/day) or 12 times faster.

An aging rate comparison was made for a heavy neutral lube stock (700 SUS) of North Sea origin. The properties of the feed are given in Table 7 below.

Table 7
North Sea HN

5	Pour Point, °C	60
	K.V. @ 100°C	11.38
	K.V. @ 300°F	4.39
	Bromine No.	0.80
	Refractive Index @ 70°C	1.461
	Gravity, API	30.90
10	Water-Azeo Distn, ppm	20.00
	Furfural, ,ppm	2.00
	Sulfur, wt%	0.17
	Basic Nitrogen, ppm	90.0
	Nitrogen, ppm	97.0
15	Hydrogen, wt%	13.52
	Ni, ppm	0.20
	V, ppm	0.00
	Fe, ppm	0.25
	Cu, ppm	0.26
20	Na, ppm	5.00
	Color ASTM Oil	0.75
	Aniline Point, °C	121.7
	Carbon Residue, %	0.10
25	Distillation	D1160-1
	(vol % Distilled)	IBP, °F
		5%
		10%
		30%
30		50%
		70%
		80%
		90%
		95%
35		End Point
		Pct. Recov

The heavy neutral feed was catalytically dewaxed over a ZSM-5 dewaxing catalyst comprising ZSM-5 bound with alumina (65% ZSM-5, 35% alumina) in the form of a 1/32 inch (0.8 mm) cylindrical extrudate. The feed was dewaxed to a constant product pour point of -7°F (20°C) by progressively raising the reactor temperature from a start-of-cycle temperature of about 260°C (500°F) to compensate for catalyst aging. Hydrogen pressure was 400 psig (2860 kPa abs.) and the hydrogen circulation rate 2500 SCF/bbl (445 n.l.-1. -1). Space velocity relative to the catalyst was 0.5 LHSV, equivalent to 1.2 WHSV relative to the zeolite component. The aging rate was determined to be 4.4°C/day (7.9°F/day), as shown in Fig. 1 (curve A).

A similar run using a 0.0625 inch (1.6 mm) dia. cylindrical extrudate of alumina-bound ZSM-5 (65% ZSM-5) produced similar results with an aging rate of 3.6°C/day (6.5°F/day), as shown in Fig. 1 (curve B).

When corrected to a WHSV of 0.6 relative to the zeolite component of the dewaxing catalyst, the aging rate is 1.1°C/day (2.0°F/day), as indicated by curve C.

A self-bound (100% zeolite) ZSM-5 dewaxing catalyst having the same alpha value as those used in the above comparisons was used for dewaxing the heavy neutral feed at a space velocity of 0.5 LHSV, 0.67 WHSV relative to the zeolite. The aging rate was found to be 0.4°C/day (0.7°F/day) as indicated by curve D in Fig. 1. Thus, the aging rate of the catalyst is improved to an extent which is greater than that attributable to the difference in space velocity between the bound catalyst and the unbound catalyst (compare curves C and D). Note that if the end-of-cycle (EOC) temperature is set at 360°C (675°F) to avoid excessive non-selective cracking, the alumina-bound catalyst will achieve a cycle length of only about 20 days at a space velocity of 0.5 on the catalyst (1.2 WHSV on the zeolite), whereas the alumina-free, self-bound catalyst reached the selected EOC temperature only after 235 days. At comparable space velocities (LHSV) on the catalyst, a cycle extension of about 12 times is obtained (curves A, B and D).

In a second dewaxing cycle after air regeneration, using the same feed and dewaxing conditions, the aging rate was approximately 0.3°C/day (0.5°F/day) at 0.5 LHSV and 0.7°C/day (1.3°F/day) at 0.85 LHSV. This higher value of the space velocity is approximately the same WHSV on zeolite corresponding to 0.5 LHSV for a 65/35 ZSM-5 Al₂O₃ catalyst which ages at 3.8°-4.4°C/day (7°-8°F/day) with the same feed at 0.5 LHSV.

The dewaxing operation was run for 180 days at 0.5 LHSV and for 30 days at 0.85 LHSV (equivalent in terms of oil processed to 51 days at 0.5 LHSV, to give an equivalent of 231 days total at 0.5 LHSV). The EOC temperature was only 343°C (650°F) as compared to 357°C (675°F) on the first cycle. After 30 days at 0.85 LHSV the rate was dropped again to 0.5 and a lighter feed was processed for 29 days at 1.0 LHSV to an EOC temperature of 356°C (673°F).

Fig. 1 clearly shows that the binder-free catalyst ages more slowly than the alumina-bound catalyst even when the process rate (LHSV) over the alumina-bound catalyst is reduced by 50 percent to make the ratio of oil to zeolite 10 percent less than it was with the unbound catalyst. These results were obtained regardless of the fact that the alumina-bound catalyst had been prepared in a manner known to be most suitable in other respects for the feedstock being processed.

Example 2

Aging studies similar to those reported in Example 1 were carried out with an Arab Light Bright Stock.

The feed was dewaxed to -7°C (20°F) pour point over ZSM-5 dewaxing catalysts at 2860 kPa abs. (400 psig) 2500 SCF/bbl (445 n.1.1.-1)H₂, using three extruded dewaxing catalysts with a zeolite component of comparable alpha value. The extrudates were 1/32 inch (0.8 mm) cylindrical extrudates of unsteamed, alumina-bound ZSM-5 (65% ZSM-5) and 1/16 inch (1.6 mm) cylindrical extrudates of the same catalyst. The self-bound catalyst of comparable initial activity was used in the form of 1/25 inch (1 mm) cylindrical extrudates.

The results are shown in Figure 2 which indicates the corrected dewaxing temperature to achieve a -7°C (20°F) pour point. The self-bound catalyst (curve B) has a significant cycle length advantage based on volume of catalyst (uncorrected LHSV). Upon correcting for zeolite content and based on LHSV a 10-33 percent improvement in initial aging rate (below 325°, about 600°F) is found for the self-bound catalyst. The aging rate comparison is 0.3°C/day (0.5°F/day) for the self-bound catalyst and 0.30-0.42°C/day (0.56°-0.75°F/day) for the bound catalyst. Although comparable projected cycle lengths would be achieved, no aging "tail" is noted with the self-bound catalyst.

Figure 2 shows that the self-bound catalyst ages slightly faster than the alumina-bound zeolite at temperatures up to about 293°C (560°F) at twice the space velocity but at higher temperatures the alumina bound catalyst ages significantly faster. In addition, the self-bound catalyst ages more slowly at temperatures above 332°C (630°F) and lasts longer. On a WHSV basis the alumina-bound catalyst was operated at 91 percent of that for the self-bound catalyst and its smaller particle diameter probably accounts for its apparently greater activity at temperatures up to 293°C (560°F). At the higher temperatures, however, the binder-free catalyst is clearly superior despite the conditions favoring the bound catalyst. This provides a further demonstration that the effect is not due to the relatively larger amount of zeolite in the binder-free or the low WHSV over the binder-free catalyst. The ability to use higher space velocities is a significant advantage to the refiner since it enables a given unit to have a greater throughput, thereby offering a potentially significant economic advantage.

Claims

1. A catalytic dewaxing process in which a lubricant boiling range hydrocarbon feed is catalytically dewaxed by contact with an extruded, particulate, binder-free intermediate pore size zeolite dewaxing catalyst in the presence of hydrogen at a temperature of 204° to 427°C, which is progressively increased during a dewaxing cycle to compensate for catalyst aging, the aging rate of the binder-free catalyst being less than that of a dewaxing catalyst comprising the same zeolite composited with an alumina binder.

2. A process according to claim 1 in which the binder-free dewaxing catalyst comprises extruded particles of an intermediate pore size zeolite selected from ZSM-5, ZSM-11 and ZSM-23.

3. A process according to any one of the preceding claims in which the aging rate of the binder-free dewaxing catalyst is less than 2.8°C/day.

4. A process according to any one of the preceding claims in which the feed has an initial boiling point of at least 399°C.

5. A process according to any one of the preceding claims in which the feed has an initial boiling point of at least 399°C and a 50% boiling point of at least 540°C at 1 mm Hg. (133 Pa) and the dewaxing catalyst comprises extruded particles of ZSM-5.



In a second dewaxing cycle after air regeneration, using the same feed and dewaxing conditions, the aging rate was approximately 0.3°C/day (0.5°F/day) at 0.5 LHSV and 0.7°C/day (1.3°F/day) at 0.85 LHSV. This higher value of the space velocity is approximately the same WHSV on zeolite corresponding to 0.5 LHSV for a 65/35 ZSM-5 Al₂O₃ catalyst which ages at 3.8°-4.4°C/day (7°-8°F/day) with the same feed at 0.5 LHSV.

The dewaxing operation was run for 180 days at 0.5 LHSV and for 30 days at 0.85 LHSV (equivalent in terms of oil processed to 51 days at 0.5 LHSV, to give an equivalent of 231 days total at 0.5 LHSV). The EOC temperature was only 343°C (650°F) as compared to 357°C (675°F) on the first cycle. After 30 days at 0.85 LHSV the rate was dropped again to 0.5 and a lighter feed was processed for 29 days at 1.0 LHSV to an EOC temperature of 356°C (673°F).

Fig. 1 clearly shows that the binder-free catalyst ages more slowly than the alumina-bound catalyst even when the process rate (LHSV) over the alumina-bound catalyst is reduced by 50 percent to make the ratio of oil to zeolite 10 percent less than it was with the unbound catalyst. These results were obtained regardless of the fact that the alumina-bound catalyst had been prepared in a manner known to be most suitable in other respects for the feedstock being processed.

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The results are shown in Figure 2 which indicates the corrected dewaxing temperature to achieve a -7°C (20°F) pour point. The self-bound catalyst (curve B) has a significant cycle length advantage based on volume of catalyst (uncorrected LHSV). Upon correcting for zeolite content and based on LHSV a 10-33 percent improvement in initial aging rate (below 325°, about 600°F) is found for the self-bound catalyst. The aging rate comparison is 0.3°C/day (0.5°F/day) for the self-bound catalyst and 0.30-0.42°C/day (0.56°-0.75°F/day) for the bound catalyst. Although comparable projected cycle lengths would be achieved, no aging "tail" is noted with the self-bound catalyst.

Figure 2 shows that the self-bound catalyst ages slightly faster than the alumina-bound zeolite at temperatures up to about 293°C (560°F) at twice the space velocity but at higher temperatures the alumina bound catalyst ages significantly faster. In addition, the self-bound catalyst ages more slowly at temperatures above 332°C (630°F) and lasts longer. On a WHSV basis the alumina-bound catalyst was operated at 91 percent of that for the self-bound catalyst and its smaller particle diameter probably accounts for its apparently greater activity at temperatures up to 293°C (560°F). At the higher temperatures, however, the binder-free catalyst is clearly superior despite the conditions favoring the bound catalyst. This provides a further demonstration that the effect is not due to the relatively larger amount of zeolite in the binder-free or the low WHSV over the binder-free catalyst. The ability to use higher space velocities is a significant advantage to the refiner since it enables a given unit to have a greater throughput, thereby offering a potentially significant economic advantage.

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2. A process according to claim 1 in which the binder-free dewaxing catalyst comprises extruded particles of an intermediate pore size zeolite selected from ZSM-5, ZSM-11 and ZSM-23.

3. A process according to any one of the preceding claims in which the aging rate of the binder-free dewaxing catalyst is less than 2.8°C/day.

4. A process according to any one of the preceding claims in which the feed has an initial boiling point of at least 399°C.

5. A process according to any one of the preceding claims in which the feed has an initial boiling point of at least 399°C and a 50% boiling point of at least 540°C at 1 mm Hg. (133 Pa) and the dewaxing catalyst comprises extruded particles of ZSM-5.



6. A process according to any one of the preceding claims in which the feed has an initial boiling point of at least 399°C.

7. A process according to any one of the preceding claims in which the feed has an initial boiling point of at least 399°C and a 50% point of at least 540°C at 1 mm Hg (133 Pa).

5 8. A process according to any one of the preceding claims in which the feed has a basic nitrogen content of at least 100 ppmw.

9. A process according to any one of the preceding claims in which the feed includes at least 35 weight percent paraffins.

10 10. A process according to any one of the preceding claims in which the intermediate pore size zeolite is ZSM-5.

11. A process according to any one of the preceding claims in which the dewaxing catalyst includes a metal component having hydrogenation activity.

12. A process according to claim 11 in which the dewaxing cycle is continued to an end-of-cycle temperature in excess of that obtainable with a dewaxing catalyst comprising the same zeolite composited with an alumina binder using the same feedstock and dewaxing conditions at the same product pour point.

13. A process according to claim 12 in which the end-of-cycle temperature is at least 28°C above the end-of-cycle temperature with the alumina-bound catalyst.

14. A process according to any one of the preceding claims in which the process operates at a predetermined LHSV and the LHSV is higher than that which would be attainable with a dewaxing catalyst comprising the same zeolite composited with an alumina binder using the same feedstock and dewaxing conditions at the same product pour point at the same aging rate.

Revendications

25 1. Un procédé de déparaffinage catalytique dans lequel une charge d'hydrocarbures de point d'ébullition du domaine de celui des lubrifiants est déparaffinée catalytiquement par contact avec un catalyseur de déparaffinage extrudé à base de zéolite particulaire exempt de liant à dimension de pores intermédiaire, en présence d'hydrogène à une température de 204 à 427°C, qui est progressivement augmentée pendant un cycle de déparaffinage pour compenser le vieillissement du catalyseur, la vitesse de vieillissement du catalyseur exempt de liant étant inférieure à celle d'un catalyseur de déparaffinage comprenant la même zéolite combinée à un liant à base d'alumine.

30 2. Un procédé selon la revendication 1, dans lequel le catalyseur de déparaffinage exempt de liant est formé de particules extrudées d'une zéolite à dimension de pores intermédiaire choisie parmi ZSM-5, ZSM-11 et ZSM-23.

35 3. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la vitesse de vieillissement du catalyseur de déparaffinage exempt de liant est inférieure à 2,8°C par jour.

4. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la charge a un point d'ébullition initial d'au moins 399°C.

40 5. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la charge a un point d'ébullition initial d'au moins 399°C et un point d'ébullition à 50% d'au moins 540°C sous 1 mm Hg (133 Pa), le catalyseur de déparaffinage comprenant des particules de ZSM-5 extrudées.

6. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la charge a un point d'ébullition initial d'au moins 399°C.

45 7. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la charge a un point d'ébullition initial d'au moins 399°C et un point d'ébullition à 50% d'au moins 540°C sous 1 mm Hg (133 Pa).

8. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la charge a une teneur en azote basique d'au moins 100 ppmw.

50 9. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la charge inclue au moins 35% en poids de paraffine.

10. Un procédé selon l'une quelconque des revendications précédentes, dans lequel la zéolite à dimension de pores intermédiaire est la ZSM-5.

11. Un procédé selon l'une quelconque des revendications précédentes, dans lequel le catalyseur de déparaffinage inclue un composant métallique ayant une activité d'hydrogénation.

55 12. Un procédé selon la revendication 11, dans lequel le cycle de déparaffinage est mis en oeuvre jusqu'à une température de fin de cycle supérieure à celle pouvant être obtenue avec un catalyseur de déparaffinage comprenant la même zéolite combinée à un liant à base d'alumine, en utilisant la même charge et les mêmes conditions de déparaffinage pour le même point de coulée de produit.



13. Un procédé selon la revendication 12, dans lequel la température de fin de cycle est au moins supérieure d'au moins 28°C à la température de fin de cycle dans le cas du catalyseur lié à l'alumine.

14. Un procédé selon l'une quelconque des revendications précédentes, dans lequel le procédé est mis en oeuvre à une VSHL prédéterminée et cette VSHL est supérieure à celle qui peut être obtenue avec un catalyseur de déparaffinage comprenant la même zéolite combinée avec un liant à base d'alumine, utilisant la même charge et les mêmes conditions de déparaffinage pour le même point de coulée de produit à la même vitesse de vieillissement.

10 Patentansprüche

1. Katalytisches Entparaffinierungsverfahren, bei dem eine Kohlenwasserstoffzufuhr im Siedebereich des Schmiermittels durch Kontakt mit einem extrudierten, partikelförmigen, bindemittelfreien Entparaffinierungskatalysator in Form eines Zeoliths mittlerer Porengröße in Gegenwart von Wasserstoff bei einer Temperatur von 204 bis 427°C katalytisch entparaffiniert wird, wobei diese Temperatur während des Entparaffinierungszyklus fortlaufend erhöht wird, um die Alterung des Katalysators zu kompensieren, wobei die Alterungsrate des bindemittelfreien Katalysators geringer als die des Entparaffinierungskatalysators ist, der den gleichen Zeolith umfaßt, der mit dem Aluminiumoxid-Bindemittel zusammengesetzt ist.

2. Verfahren nach Anspruch 1, worin der bindemittelfreie Entparaffinierungskatalysator extrudierte Partikel eines Zeoliths mit mittlerer Porengröße umfaßt, der aus ZSM-5, ZSM-11 und ZSM-23 ausgewählt ist.

3. Verfahren nach einem der vorstehenden Ansprüche, worin die Alterungsrate des bindemittelfreien Entparaffinierungskatalysators weniger als 2,8°C/Tag beträgt.

4. Verfahren nach einem der vorstehenden Ansprüche, worin die Zufuhr einen Anfangssiedepunkt von mindestens 399°C aufweist.

5. Verfahren nach einem der vorstehenden Ansprüche, worin die Zufuhr einen Anfangssiedepunkt von mindestens 399°C und 50%-Siedepunkt von mindestens 540°C bei 1mm Hg (133 Pa) aufweist und der Entparaffinierungskatalysator extrudierte Partikel von ZSM-5 umfaßt.

6. Verfahren nach einem der vorstehenden Ansprüche, worin die Zufuhr einen Anfangssiedepunkt von mindestens 399°C aufweist.

7. Verfahren nach einem der vorstehenden Ansprüche, worin die Zufuhr einen Anfangssiedepunkt von mindestens 399°C und 50%-Punkt von mindestens 540°C bei 1mm Hg (133 Pa) aufweist.

8. Verfahren nach einem der vorstehenden Ansprüche, worin die Zufuhr einen Gehalt an basischem Stickstoff von mindestens 100 ppmw aufweist.

9. Verfahren nach einem der vorstehenden Ansprüche, worin die Zufuhr mindestens 35 Gew.-% Paraffine beinhaltet.

10. Verfahren nach einem der vorstehenden Ansprüche, worin der Zeolith mit mittlerer Porengröße ZSM-5 ist.

11. Verfahren nach einem der vorstehenden Ansprüche, worin der Entparaffinierungskatalysator eine metallkomponente beinhaltet, die Hydrierungsaktivität aufweist.

12. Verfahren nach Anspruch 11, worin der Entparaffinierungszyklus bis zu einer Temperatur am Ende des Zyklus fortgeführt wird, die höher als die Temperatur ist, die mit einem Entparaffinierungskatalysator erhalten werden kann, der den gleichen Zeolith umfaßt, der mit einem Aluminiumoxid-Bindemittel zusammengesetzt ist, wobei das gleiche Ausgangsmaterial und die gleichen Entparaffinierungsbedingungen beim gleichen Pourpoint des Produktes angewendet werden.

13. Verfahren nach Anspruch 12, worin die Temperatur am Ende des Zyklus mindestens 28°C oberhalb der Temperatur am Ende des Zyklus beim mit Aluminiumoxid gebundenen Katalysator liegt.

14. Verfahren nach einem der vorstehenden Ansprüche, worin das Verfahren bei einer bestimmten LHSV arbeitet und diese LHSV höher als die ist, die mit einem Entparaffinierungskatalysator erreichbar wäre, der den gleichen Zeolith umfaßt, der mit einem Aluminiumoxid-Bindemittel zusammengesetzt ist, wobei das gleiche Ausgangsmaterial und die gleichen Entparaffinierungsbedingungen beim gleichen Pourpoint des Produktes und der gleichen Alterungsrate angewendet werden.