

PROCESS AND EQUIPMENT FOR CONVERTING CARBON DIOXIDE IN FLUE GAS INTO NATURAL GAS BY USING DUMP POWER ENERGY

TECHNICAL FIELD

[0001] The invention relates to technology for energy conversion of industrial flue gas by dump energy arising from renewable energy generation, such as solar energy, hydroenergy, wind energy etc., and specifically relates to a method and a device for converting carbon dioxide in flue gas into natural gas by dump energy.

BACKGROUND OF THE INVENTION

[0002] At present, in the global total energy consumption of more than 16 billion t of standard coal every year, fossil fuels such as coal, oil and natural gas etc. account for more than 90%, no exception for China, thereby resulting in extremely huge amounts of carbon dioxide emission. Since 21st century, one of the biggest challenges facing the human is the greenhouse effect caused by the carbon dioxide emission, which results in global warming, climate change, as well as the global environmental problems having comprehensive impact on the ecology, economy and society. In 2010, the global carbon dioxide emission was enhanced to more than 30.6 billion tons, and China became the country with highest carbon dioxide emission, but the emission was still increasing. People are forced by the global energy shortage and increasingly serious environmental problems caused by carbon dioxide emission to find ways to solve these problems.

[0003] To solve the above problems, use of the renewable energy unprecedentedly expands. According to incomplete statistics of China, at present, the proportion of non-fossil energy, such as hydropower, nuclear power, wind power and solar energy etc. in the total primary energy consumption is increasing year by year, will be increased from the current 8.3% to 11.4% during the Twelfth Five-Year Plan, and will reach 15% by 2020. To achieve this goal, it is imperative to develop renewable energy.

[0004] However, according to the *Supervision Report of Wind Power Generation and Photovoltaic Power Generation* issued by the State Electricity Regulatory Commission in 2011, in the past half a year, as much as 2.776 billion kWh of the wind power cannot be used by people in China. The State Electricity Regulatory Commission indicated that because of lack of specific wind power delivery and wind power accommodation scheme, the contradiction between large-scale wind power delivery and accommodation is increasingly larger, and the grid connection obstacle has become one of the key problems restricting the development of wind power.

[0005] In terms of hydropower, China has built as many as 28 hydropower stations of more than 500,000 kW with the total installed capacity as much as 50.98 million kW. In 2010, the planned total installed capacity of 12 major hydropower bases (including existing) was 205.232 million kW, and annual power generation was 945.88 billion kW·h in China. In wet season of the hydropower project, there is enough generating capacity, but it is not possible to deliver much electric energy in the wet season, resulting in very low feed-in tariff, and losses of electric energy or equipment shutdown.

[0006] In terms of solar power generation, installed capacity of photovoltaic power generation market reached 400 mW in China in 2010, accounting for 3% of the total installed capacity of the world. According to the planning of the National Energy Administration, the installed capacity of solar power of China will reach more than 10 million kW by 2015, and more than 40 million kW by 2020. But some electric energy thereof will be bound to have grid connection bottleneck problems.

[0007] Those skilled in this art has always been trying to solve the problem of how to make full use of the above dump energy arising from renewable energy generation and further effectively realize the purpose of energy conservation, emission reduction, and reducing the greenhouse effect.

SUMMARY OF THE INVENTION

[0008] It is one objective of the invention to solve the defects of renewable energy generation such as grid connection obstacles or being difficult to store short-time dump energy, and the problem that fossil energy has environmental pollution caused by greenhouse gas, and provide a method and a device for converting carbon dioxide in flue gas into natural gas by dump energy.

[0009] To achieve the above purpose, the key concept of the method designed in the invention for converting carbon dioxide in flue gas into natural gas by dump energy is to first generate hydrogen through water electrolysis using pump energy, and then synthesize natural gas easy for storage or transportation through methanation reaction between hydrogen and carbon dioxide trapped from industrial flue gas, which also facilitates reasonable application of carbon dioxide discharged from industrial flue gas. The method comprises the following steps:

[0010] 1) performing voltage transformation and rectification on dump energy that is generated from renewable energy generation and is difficult for storage or grid connection, introducing the dump energy into an electrolyte solution to electrolyze water therein to H_2 and O_2 , and completely removing the water from H_2 ;

[0011] 2) purifying industrial flue gas to separate the CO_2 therein and purifying the CO_2 trapped therefrom;

[0012] 3) transporting H_2 generated from step 1) and CO_2 trapped from step 2) to a synthesis equipment comprising at least two fixed bed reactors, so that a high-temperature mixed gas with main ingredients of CH_4 and water vapor is generated through strong exothermic methanation reaction between H_2 and CO_2 ;

[0013] 4) employing the high-temperature mixed gas generated from step 3) to conduct indirect heat exchange with process water to yield superheated water vapor;

[0014] 5) delivering the superheated water vapor generated from step 4) to a turbine to generate electric energy, and returning the electric energy to step 1) for voltage transformation and rectification, and for water electrolysis; and

[0015] 6) condensing and drying the mixed gas in step 4) cooled through heat exchange, to obtain natural gas with CH₄ content up to the standard. The natural gas (SNG) can be sent to the existing natural gas pipe network through pressurized transport, or pressurized to liquefied natural gas (LNG) for transport.

[0016] Further, in step 1), the renewable energy is selected from solar energy, hydroenergy, wind energy, or a combination thereof. These renewable energies are the most environment-friendly, cheapest and safest. The electrolyte solution is preferably potassium hydroxide solution or other similar solutions with the density of 1.2-1.4 kg/m³. Reaction temperature of the electrolyte solution is controlled at 90 ± 2°C, and the reaction mechanism of water electrolysis is as follows: $2\text{H}_2\text{O} = 2\text{H}_2\uparrow + \text{O}_2\uparrow$. Compared with the pure water, the electrolyte solution can significantly lower the electrolytic reaction temperature, and save power consumption. After moisture removal and cooling of the resulting H₂ and O₂, H₂ may be used for the reaction in the next step, while O₂ may be as a by-product for other usage.

[0017] Further, various parameters of the fixed bed reactor at every stage in step 3) are as follows: inlet temperature: 250-300°C, reaction pressure: 3-4 mPa, outlet temperature: 350-700°C. Methanation reaction mechanism of H₂ and CO₂ is as follows: $4\text{H}_2 + \text{CO}_2 = \text{CH}_4 + 2\text{H}_2\text{O} + 4160 \text{ kJ/kg} \cdot \text{CO}_2$. In specific operation, generally their mixture at a volume ratio of H₂: CO₂ = 4: 1 is transferred to a fixed bed reactor for strong exothermic reaction in the presence of a nickel-based catalyst or a similar catalyst, whilst releasing a lot of heat, so that the temperature of the resulting mixed gas is greatly improved. At least two stage fixed bed reactors are provided to ensure complete reaction between H₂ and CO₂, and improve the utilization efficiency of H₂.

[0018] Further, in step 3), part of the high-temperature mixed gas from the primary fixed bed reactor is bypassed for cooling, water removal, pressurization and heating, and is then mixed with fresh H₂ and CO₂, so that the mixed gas is transported back to the primary fixed bed reactor after the volume content of CO₂ therein is 6-8%. In this way, on the one hand, fresh H₂ and CO₂ can be preheated with returning high-temperature gas to save energy consumption; on the other hand, the reaction heat can be controlled

through adjusting the volume content of CO₂, thereby controlling the highest outlet temperature of the fixed bed reactor, so that the catalyst is not deactivated at allowed temperature to ensure stable operation of the fixed bed reactor.

[0019] Further, in above step 4), firstly, the process water is heated to superheated water, which is then converted to water vapor, and finally the water vapor is converted to produce superheated water vapor. In this way, the process water is continuously, stably and reliably converted to yield superheated water vapor, so as to ensure that the turbine always uninterruptedly generates power. The electric energy generated thereby continues to be used for water electrolysis, so that the high heat generated from the methanation reaction is fully used to improve the conversion efficiency of the renewable energy.

[0020] Further, in step 5), the steam exhaust generated by the turbine after being driven for power generation is condensed to water, and then sent back to the process water line for recycling, so as to effectively improve the utilization efficiency of the process water, and save water resources.

[0021] Further, in step 6), condensed water from the mixed gas is sent back to the process water line for recycling, which can effectively improve the utilization efficiency of the process water, and save water resources.

[0022] To achieve the above objectives, the invention also provides a device for converting carbon dioxide in flue gas into natural gas using dump energy. The device comprises a transformer and rectifier device, an electrolytic cell, a turbine, a carbon dioxide heater, a primary fixed bed reactor, a secondary fixed bed reactor, a natural gas condenser, and a process water line. An outlet of the transformer and rectifier device is connected to a power interface of the electrolytic cell, a gas-liquid outlet of a cathode of the electrolytic cell is connected to a gas-liquid inlet of a hydrogen separator, a liquid outlet of the hydrogen separator is connected to a liquid reflux port of the cathode of the electrolytic cell, a H₂ outlet of the hydrogen separator is connected to an inlet of a hydrogen cooler, both the outlet of the hydrogen cooler and outlet of the carbon dioxide heater are connected to an inlet of the primary fixed bed reactor, an outlet of the primary

fixed bed reactor is connected to an inlet of the secondary fixed bed reactor successively through the superheater and mixed gas line of the primary heat exchanger, and the outlet of the secondary fixed bed reactor is connected to the inlet of the natural gas condenser successively through the secondary heat exchanger and the mixed gas line of the preheater. The process water line is connected to the aqueous medium inlet of the preheater, the aqueous medium outlet of the preheater is connected to the steam inlet of the superheater through a steam pocket, the steam outlet of the superheater is connected to the steam inlet of the turbine, and the electric outlet of the turbine is connected to the inlet of the transformer and rectifier device.

[0023] Preferably, the mixed gas outlet of the primary heat exchanger is still provided with a bypass connected to the heat medium inlet of a circulating heat exchanger, the heat medium outlet of the circulating heat exchanger is connected to the inlet of a circulating compressor through a circulating cooler, the outlet of the circulating compressor is connected to the heated medium inlet of the circulating heat exchanger, and the heated medium outlet of the circulating heat exchanger is connected to the inlet of the primary fixed bed reactor. In this way, a part of the high-temperature mixed gas generated from the reaction can reenter the primary fixed bed reactor by means of self-circulation, so as to realize preheating the fresh H_2 and CO_2 , reduce energy consumption and ensure continuous reaction.

[0024] Preferably, an intermediate fixed bed reactor is provided between the primary fixed bed reactor and the secondary fixed bed reactor. The inlet of the intermediate fixed bed reactor is connected to the mixed gas outlet of the primary heat exchanger, and the outlet of the intermediate fixed bed reactor is connected to the inlet of the secondary fixed bed reactor through an intermediate heat exchanger. In this way, in fact, three stage fixed bed reactors are provided, so as to distribute the methanation reaction rate of H_2 and CO_2 stage by stage, until complete reaction of the raw materials. At the same time, temperature of the fixed bed reactor can be reduced stage by stage, so as to obtain different quality of steam (temperature, pressure), and meet the needs of the turbine.

[0025] Further, the steam exhaust outlet of the turbine is connected to the process water line through the steam exhaust condenser, which can save the water resources, and improve the utilization rate of process water.

[0026] Further, the process water line is connected to the gas-liquid inlet of the hydrogen separator. In this way, water can be transported to the electrolytic cell by the hydrogen separator to supplement the water losses in the electrolytic reaction process and cool the heat generated from the water electrolysis process.

[0027] Further, the condensed water outlet of the above natural gas condenser is connected to the aqueous medium inlet of the preheater, so as to save the water resources, and improve the utilization rate of process water.

[0028] The invention has the following advantages:

[0029] First, carbon dioxide trapped from industrial flue gas is converted to methane fuel (i.e., the main ingredient of natural gas) convenient for storage and transport through methanation reaction with hydrogen generated from water electrolysis by dump energy arising from the renewable energy generation, such as solar energy, hydroenergy, and wind energy etc. In this way, methane fuel is easily introduced into the existing natural gas pipe network system, and may also be pressurized to liquefied natural gas (LNG) for transport by tank cars, thereby effectively solving the above grid connection obstacle of dump energy or problem of difficult storage of short-term dump energy.

[0030] Second, in the process of synthesizing methane using hydrogen and carbon dioxide, huge amounts of carbon dioxide in flue gas is utilized, thereby achieving the goal of reducing carbon dioxide emission, solving the problem of reducing huge amounts of carbon dioxide emission generated by fossil fuel, and bringing great economic benefits and social benefits.

[0031] Third, methanation reaction of hydrogen and carbon dioxide is a strong exothermic reaction, huge amounts of heat will be released in the process, the heat energy is used to produce high-temperature superheated steam to continue power generation, and

then the electric energy is used for circulation of water electrolysis, thereby greatly improving the conversion efficiency of renewable energy.

[0032] Fourthly, only methane and water vapor as the natural gas fuel are present in the end product of methanation reaction of hydrogen and carbon dioxide, and no other toxic by-products are available, which can not only ensure the quality of the natural gas, but also reduce environment pollution caused by greenhouse gas.

BRIEF DESCRIPTION OF THE DRAWINGS

[0033] FIG. 1 is a structural diagram of a device for converting carbon dioxide in flue gas into natural gas by dump energy; and

[0034] FIG. 2 is a structural diagram of another device for converting carbon dioxide in flue gas into natural gas by dump energy.

DETAILED DESCRIPTION OF THE EMBODIMENTS

[0035] The method and device in the invention are further illustrated in detail in the light of the drawings and specific embodiments as follows:

Example 1

[0036] A device for converting carbon dioxide into natural gas by dump energy, as shown in FIG. 1, comprises a transformer and rectifier device 1, an electrolytic cell 2, a turbine 4, a carbon dioxide heater 21, a primary fixed bed reactor 13, a secondary fixed bed reactor 11, a natural gas condenser 8 and a process water line 3. The outlet of the transformer and rectifier device 1 is connected to the power interface of the electrolytic cell 2. The gas-liquid outlet of the anode of the electrolytic cell 2 is connected to the gas-liquid inlet of the oxygen separator 20, liquid outlet of the oxygen separator 20 is connected to the liquid reflux port of the anode of the electrolytic cell 2, O₂ outlet of the

oxygen separator 20 is connected to the inlet of the oxygen cooler 19, and outlet of the oxygen cooler 19 is connected to a pressurized tank car or a filling device of O₂ (not shown in the figure) for other industrial use. The gas-liquid outlet of the cathode of the electrolytic cell 2 is connected to the gas-liquid inlet of the hydrogen separator 18, and the gas-liquid inlet of the hydrogen separator 18 is also connected to the process water line 3 to supplement water losses. The liquid outlet of the hydrogen separator 18 is connected to the liquid reflux port of the cathode of the electrolytic cell 2, H₂ outlet of the hydrogen separator 18 is connected to the inlet of the hydrogen cooler 17, outlet of the hydrogen cooler 17 is connected to the outlet of the carbon dioxide heater 21 and also connected to the inlet of the primary fixed bed reactor 13, so as to transport fresh H₂ and CO₂ to the primary fixed bed reactor 13.

[0037] Outlet of the primary fixed bed reactor 13 is connected to the inlet of the secondary fixed bed reactor 11 successively through a superheater 6 and mixed gas line of a primary heat exchanger 7, the mixed gas outlet of the primary heat exchanger 7 is still provided with a bypass connected to the heat medium inlet of a circulating heat exchanger 16, the heat medium outlet of the circulating heat exchanger 16 is connected to the inlet of a circulating compressor 14 through a circulating cooler 15, the outlet of the circulating compressor 14 is connected to the heated medium inlet of the circulating heat exchanger 16, and the heated medium outlet of the circulating heat exchanger 16 is connected to the inlet of the primary fixed bed reactor 13.

[0038] Outlet of the secondary fixed bed reactor 11 is successively connected to the inlet of a natural gas condenser 8 through a secondary heat exchanger 10 and mixed gas line of a preheater 9. The process water line 3 is connected to the aqueous medium inlet of the preheater 9, aqueous medium outlet of the preheater 9 is connected to the steam inlet of the superheater 6 through a steam pocket 12, the steam outlet of the superheater 6 is connected to the steam inlet of a turbine 4, and the steam exhaust outlet of the turbine 4 is connected to the process water line 3 through a steam exhaust condenser 5, and the electric outlet of the turbine 4 is connected to the inlet of the transformer and rectifier device 1 to provide electric energy for water electrolysis. In addition, the condensed

water outlet of the natural gas condenser 8 may also be connected to the aqueous medium inlet of the preheater 9 (not shown in the figure) to send the condensed water back to the system for recycling.

[0039] The process flow of the device for converting carbon dioxide in flue gas into natural gas by dump energy is as follows:

[0040] Dump energy arising from renewable energy generation, such as solar energy, hydroenergy or wind energy etc., is converted to required current through the transformer and rectifier device 1 to provide working power supply for the electrolytic cell 2.

Potassium hydroxide solution with the density of $1.2\text{--}1.4\text{ kg/m}^3$ is used as the electrolyte solution within the electrolytic cell 2, and the reaction temperature is controlled at $90 \pm 2^\circ\text{C}$. Here, anode and cathode of the electrolytic cell 2 respectively generate O_2 and H_2 carrying the electrolyte solution. The electrolyte solution is removed from O_2 generated therein with an oxygen separator 20, and is sent back to the electrolytic cell 2 to further participate in the reaction. Afterwards, O_2 is cooled in an oxygen cooler 19 to 45°C or so for water removal, and then delivered to a pressurized tank car or a filling device for industrial use. The electrolyte solution is removed from H_2 generated therein with a hydrogen separator 18, and is sent back to the electrolytic cell 2 to further participate in the reaction. Afterwards, H_2 is cooled in a hydrogen cooler 17 to 45°C or so for water removal, and then enters the reaction in the next step. Water losses in electrolysis is introduced into the hydrogen separator 18 through the process water line 3, is then supplemented to the electrolytic cell 2, and is also used to cool the heat generated in the water electrolysis process.

[0041] Meanwhile, CO_2 trapped from flue gas is purified, introduced into the carbon dioxide heater 21, heated, and mixed with H_2 purified through water removal at the volume ratio of $\text{H}_2 : \text{CO}_2 = 4:1$ to fresh gas, which is transported to the primary fixed bed reactor 13 for strong exothermic reaction (methanation). In order to control the reaction heat of methanation of H_2 and CO_2 , certain amount of CH_4 may be added into the CO_2 heater 21 generally at the volume ratio of $\text{H}_2 : \text{CO}_2 : \text{CH}_4 = 4:1:0.5$. Addition of CH_4 can be stopped after the reaction is stable. The primary fixed bed reactor 13 is kept at the inlet

temperature of 250-300°C, reaction pressure of 3-4 MPa, and outlet temperature of 600-700°C. In the presence of a nickel-based catalyst, most H₂ reacts with CO₂ to generate high-temperature mixed gas of CH₄ and water vapor. The high-temperature mixed gas is cooled to 250-300°C successively through the superheater 6 and primary heat exchanger 7, and then divided into two parts. Where, a part of high-temperature mixed gas enters a circulating cooler 15 through the heat medium line of the circulating heat exchanger 16, cooled to 30-40°C after heat exchange, pressurized to 3-4 MPa and heated to 180-200°C with a circulating compressor 14, finally further heated to 250-300°C through the heated medium line of the circulating heat exchanger 16, and mixed with fresh H₂ and CO₂ at such a ratio that the volume content of CO₂ in the mixed gas is 6-8%. The mixed gas is transported to the primary fixed bed reactor 13, and the cycle is repeated. Preheating fresh H₂ and CO₂ in above circulation can greatly reduce energy consumption and control the outlet temperature of the primary fixed bed reactor 13. Another part of high-temperature mixed gas is introduced into the secondary fixed bed reactor 11, which is kept at the inlet temperature of 250-300°C, reaction pressure of 3-4 MPa, and outlet temperature of 350-500°C, so that the unreacted H₂ and CO₂ therein continue to complete the strong exothermic reaction (methanation), until complete reaction of all raw materials.

[0042] The high-temperature mixed gas of CH₄ and water vapor from the secondary fixed bed reactor 11 is cooled successively through a secondary heat exchanger 10 and a preheater 9, further cooled through a natural gas condenser 8, where gas CH₄ is cooled to 45-50°C, and flows out from the gas output of the natural gas condenser 8. CH₄ with the purity of more than 94% is pressurized to SNG/LNG (natural gas/liquefied natural gas), and is transported through pipeline to the existing pipe network/tank car for storage and use; while the condensed water therein flows out from the condensed water output of the natural gas condenser 8, and is transported to the aqueous medium inlet of the preheater 9 for recycling.

[0043] In the above strong exothermic reaction process of methanation, the process water is introduced into the preheater 9 through the process water line 3, and is heated to

superheated water through heat exchange therein. Superheated water is transported to a steam pocket 12 through pipeline to evaporate into water vapor therein. Water vapor is transported to the superheater 6 through pipeline to convert to superheated water vapor under given pressure by further heating. The superheated vapor enters the turbine 4 through pipeline, the high-speed superheated water vapor drives the blades of the turbine 4 to rotate for power generation, the generated energy returns to the transformer and rectifier device 1 for voltage transformation, rectification, and further use for water electrolysis, so as to make full use of the waste heat in the strong exothermic reaction of methanation. The steam exhaust generated after the turbine is driven for power generation is transported to a steam exhaust condenser 5, and is condensed to water, which is sent back to the process water line 3 for recycling.

Example 2

[0044] Another device for converting carbon dioxide into natural gas by dump energy, as shown in FIG. 2, has the structure and process flow basically the same as that in Example 1, except that an intermediate fixed bed reactor 22 is provided between the primary fixed bed reactor 13 and the secondary fixed bed reactor 11. The inlet of the intermediate fixed bed reactor 22 is connected to the mixed gas outlet of the primary heat exchanger 7, and the outlet of the intermediate fixed bed reactor 22 is connected to the inlet of the secondary fixed bed reactor 11 through an intermediate heat exchanger 23. In this way, three stage fixed bed reactors are provided, so as to distribute the methanation reaction rate of H_2 and CO_2 in three stages, and ensure complete reaction of the raw materials. At the same time, inlet and outlet temperature of the three stage fixed bed reactors can be reduced successively, so as to obtain corresponding quality of steam (temperature, pressure), and meet the needs of the turbine 4.

CLAIMS

1. A method for converting carbon dioxide in flue gas into natural gas using dump energy, the method comprising:
 - 1) performing voltage transformation and rectification on dump energy that is generated from renewable energy generation, introducing the dump energy into an electrolyte solution to electrolyze water therein to H₂ and O₂, and removing the water from H₂;
 - 2) purifying industrial flue gas to separate CO₂ therein and purifying CO₂ trapped therefrom;
 - 3) transporting H₂ generated from step 1) and CO₂ trapped from step 2) to a synthesis equipment comprising at least two fixed bed reactors, so that a high-temperature mixed gas with main ingredients of CH₄ and water vapor is generated through exothermic methanation reaction between H₂ and CO₂;
 - 4) employing the high-temperature mixed gas generated from step 3) to conduct indirect heat exchange with process water to yield superheated water vapor;
 - 5) delivering the superheated water vapor generated from step 4) to a turbine to generate electric energy, and returning the electric energy to step 1) for voltage transformation and rectification and water electrolysis; and
 - 6) condensing and drying the mixed gas in step 4) cooled through heat exchange.
2. The method of claim 1, characterized in that the renewable energy is selected from solar energy, hydroenergy, wind energy, or a combination thereof.
3. The method of claim 1, characterized in that the electrolyte solution is potassium hydroxide solution with a density of 1.2-1.4 kg/m³, and a reaction temperature of the electrolyte solution is controlled at $90 \pm 2^{\circ}\text{C}$.

4. The method of claim 1, 2, or 3, characterized in that in step 3), the fixed bed reactors have an inlet temperature of 250-300°C, a reaction pressure of 3-4 mPa, and an outlet temperature of 350-700°C.
5. The method of claim 1, 2, or 3, characterized in that in step 3), part of the high-temperature mixed gas from a primary fixed bed reactor is bypassed for cooling, water removal, pressurization and heating, and is then mixed with fresh H₂ and CO₂, so that the mixed gas is transported back to the primary fixed bed reactor after a volume content of CO₂ therein is 6-8%.
6. The method of claim 1, 2, or 3, characterized in that in step 4), the process water is first heated to produce superheated water, which is then converted to water vapor, and finally the water vapor is converted to the superheated water vapor.
7. The method of claim 1, 2, or 3, characterized in that in step 5), steam exhaust generated by a turbine after being driven for power generation is condensed to water, and then sent back to the process water line for recycling.
8. The method of claim 1, 2, or 3, characterized in that in step 6), condensed water from the mixed gas is sent back to the process water line for recycling.
9. A device for converting carbon dioxide in flue gas into natural gas using dump energy, comprising a transformer and rectifier device (1), an electrolytic cell (2), a turbine (4), a carbon dioxide heater (21), a primary fixed bed reactor (13), a secondary fixed bed reactor (11), a natural gas condenser (8), and a process water line (3), wherein

an outlet of the transformer and rectifier device (1) is connected to a power interface of the electrolytic cell, a gas-liquid outlet of a cathode of the electrolytic cell (2) is connected to a gas-liquid inlet of a hydrogen separator (18),

a liquid outlet of the hydrogen separator (18) is connected to a liquid reflux port of the cathode of the electrolytic cell (2), a H₂ outlet of the hydrogen separator (18) is connected to an inlet of a hydrogen cooler (17), both an outlet of the hydrogen cooler (17) and an outlet of the carbon dioxide heater (21) are connected to an inlet of the primary fixed bed reactor (13);

an outlet of the primary fixed bed reactor (13) is connected to an inlet of the secondary fixed bed reactor successively through a superheater (6) and mixed gas line of a primary heat exchanger (7), and an outlet of the secondary fixed bed reactor (11) is connected to an inlet of the natural gas condenser (8) successively through a secondary heat exchanger (10) and a mixed gas line of the preheater (9); and

the process water line (3) is connected to an aqueous medium inlet of the preheater (9), an aqueous medium outlet of the preheater (9) is connected to a steam inlet of the superheater (6) through a steam pocket, a steam outlet of the superheater (6) is connected to a steam inlet of the turbine (4), and an electric outlet of the turbine (4) is connected to an inlet of the transformer and rectifier device (4).

10. The device of claim 9, characterized in that the mixed gas outlet of the primary heat exchanger is provided with a bypass connected to a heat medium inlet of a circulating heat exchanger (16), a heat medium outlet of the circulating heat exchanger (16) is connected to an inlet of a circulating compressor (14) through a circulating cooler (15), an outlet of the circulating compressor (14) is connected to a heated medium inlet of the circulating heat exchanger (16), and a heated medium outlet of the circulating heat exchanger (16) is connected to the inlet of the primary fixed bed reactor (13).
11. The device of claim 9 or 10, characterized in that an intermediate fixed bed reactor (22) is provided between the primary fixed bed reactor (13) and the

secondary fixed bed reactor (11); an inlet of the intermediate fixed bed reactor (22) is connected to a mixed gas outlet of the primary heat exchanger (7), and an outlet of the intermediate fixed bed reactor (22) is connected to the inlet of the secondary fixed bed reactor (11) through an intermediate heat exchanger (23).

12. The device of claim 9 or 10, characterized in that a steam exhaust outlet of the turbine (4) is connected to the process water line (3) through a steam exhaust condenser (5).
13. The device of claim 9 or 10, characterized in that the process water line (3) is connected to a gas-liquid inlet of the hydrogen separator (18).
14. The device of claim 9 or 10, characterized in that a condensed water outlet of the natural gas condenser (8) is connected to an aqueous medium inlet of the preheater (9).