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1 compartment comprising a number of blades shaped helicoidally around the axis; a
2 bottom compartment for the separation of the liquid and/or solids and a coaxial gas
3 discharge pipe projecting upwards from the bottom compartment through the middle and
4 top compartments, around which the helicoidal blades are fixed, in which bottom
5 compartment at least one plate with a circular outer rim is provided perpendicularly to the
6 axis of the vessel and under the gas discharge pipe, at least one diametrical baffle being
7 provided beneath the bottom plate, the overall height of each baffle being at least 1.0
8 times the internal diameter of the vessel.

9
10 However EP0436973A2, does not disclose the following different features of the
11 different claims disclosed herein:

12
13 1) a separator is configured to separate at a rate of up to 20 l/h for fluid flow
14 rate or 2000 NI/h for gas flow rate;

15 2) a separator assembly comprising a first separator and a second
16 separator wherein the separators are configured to separate particles in a condensing
17 mist of up to 10 microns in size;

18 3) a process wherein the separator is configured to separate particles of up
19 to 10 microns in size;

20 4) a separator characterized in that said at least one separator element
21 comprises a first conical fin, and a second conical fin (4) disposed adjacent to
22 said first conical fin (3) wherein said housing has an inner wall (20) and wherein
23 said first conical fin and said second conical fin is spaced from said inner wall of

said housing by .5 mm to 2 mm.

5) a separator system having two different separators coupled together via a conduit.

Therefore for each of the above independent reasons, the claimed inventions are patentable in view of EP0436973A2.

For example, cyclone/ centrifugal separators are used in high flow rate applications and not low flow rate applications. When this is used in conjunction with a coalescing filter, the filter element is choked up very quickly and requires very high maintenance. Therefore, there is a need for a centrifugal cyclone separator which does not have a coalescing filter element.

SUMMARY OF THE INVENTION

At least one embodiment of the invention relates to a centrifugal/ cyclone separator which separates particles, liquid droplets and or condensing mists (water based and or hydrocarbon based nature) from gases without using a filter element. With at least one embodiment of the present invention, the centrifugal/ cyclone separator can separate particles and or liquid droplets and condensing mists (water and or hydrocarbon) from gases without using a filter element and can operate optimally on low gas flow rate from 30 l/h up to 150 NI/h (Normal L/h). This embodiment is also able to separate fine particles and condensing mists up to 5 to 10 micron size which is attributed

1 to the combined effect of the use of an inlet spiral tube, a first conical fin and a second
2 conical fin. In addition, it is also attributable to the cylindrical body and the extension of
3 the vortex finder below the second conical fin.

4
5 The separator is specially designed to work optimally on low pressure and low gas
6 flow rate from 30 l/h up to 150 NI/h and is able to separate fine particles/mists between 5
7 to 10 micron size. It is also designed to separate up to a maximum of 20 l/h of liquid flow
8 or 2000 NI/h gas flow or a maximum of 40l/h of liquid flow or 1000 NI/h of gas flow. The
9 separator can work at low pressure close to atmospheric pressure or up to 100 barg
10
11 (barg= pressure in bars above ambient or atmospheric pressure) pressure.

12
13 The present invention is an innovative break-through for applying cyclonic/
14 centrifugal separator under low gas flow rate from 30 NI/h to 500 NI/h. It does not require
15 a filter element and can separate particles droplets condensing mists between 5-10
16 micron or less than 1 micron with cooler or liquid injection. It provides a robust and
17 maintenance-free solution as compared to that of coalescing filter and membrane filters
18 which provides service interval of a few days to two (2) weeks due to chokage of the fine
19 pores. Many critical process gas analyzers which are used for quality and safety control
20 in the process plants are often destroyed or make unavailable due to carry-over or
21 chokage of the traditional coalescing filter and membrane filter.

22
23 One reason why the centrifugal/ cyclone separator of the present invention can

1 separate particles and or liquid droplets and condensing mists (water and or
2 hydrocarbon) from gases without using a filter element, and can operate optimally on low
3 gas flow rate from 30 l/h up to 150 NI/h and is able to separate fine particles and
4 condensing mists up to 5 to 10 micron size is attributed to the combined effect of one or
5 more of the components of the separator. These components can include one or more
6 of an inlet spiral tube, at least one conical fin, a step in the cylindrical body, and the
7 extension of the vortex finder below the conical fin.

8 9 **BRIEF DESCRIPTION OF THE DRAWINGS**

10 Other objects and features of the present invention will become apparent from the
11 following detailed description considered in connection with the accompanying drawings
12 which disclose at least one embodiment of the present invention. It should be
13 understood, however, that the drawings are designed for the purpose of illustration only
14 and not as a definition of the limits of the invention.

15
16 In the drawings, wherein similar reference characters denote similar elements
17 throughout the several views:

18
19 FIG. 1 is an open side view of a first embodiment of the invention;

20 FIG. 2 is a side view of the stopper plate for use in both the first and second
21 embodiments of the invention; and

22 FIG. 3 is an open side view of a second embodiment of the invention;

23 FIG. 4 is a view of two separators in series; and

FIG. 5 is a side view of a cooler which can be optionally coupled to either an inlet of a first separator and/or an inlet of a second separator.

DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS

Turning in detail to the drawings, FIG. 1 shows a first embodiment of a separator 10 which includes an inlet tube 1. Cyclonic/ centrifugal separators have been used widely for separation of particles, liquid droplets and or condensing mists from gases under high gas flow rate involving at least Nm^3/h gas flow rate in order to generate sufficient high centrifugal/ cyclone forces. The dirty/ wet gas enters the separator from the top via the inlet tube 1. This inlet tube 1 is coiled spirally downwards to create centrifugal/cyclone forces to separate the particles, liquid droplets and or condensing mists from the gas. This tube stops above the conical fin 3 which is located above the second conical fin 4.

Separator 10 has an inlet spiral tube 1 which has a small inner bore to generate high gas flow velocity leading to high centrifugal/ cyclonic forces inside the top cylindrical housing 2 for effective separation. The tube 1 also guides the gas, liquid droplets, and or condensing mists smoothly from the outside of the separator spirally downwards. This is an excellent key feature which meets the requirement of cyclone inlet geometry to provide a smooth flow with minimum turbulent and minimum erosion. It is vital that the cyclone separator inlet geometry separation minimizes turbulence in the gas flow which can create new liquid mists splashing or particles turbulent flow resulting in carry over to

1 the clean and dry exist gas.

2
3 The other embodiment, that of separator 12 has an insert 1A having a threaded
4 area forming a flow path which functions like a spiral tube. This insert can comprise a
5 cylindrical block of material having a spiral path.

6
7 First and second conical fins 3 and 4 function to push the gas particles, liquid
8 droplets, and or condensing mists close to the cylindrical wall of the top housing 2. Upon
9 exiting the second conical fin 4 there is a step, ridge or protrusion 9 where the particles
10 liquid droplets and or mists enters cylindrical body 5 which is of bigger inner diameter
11 (see line d2) from that of the top cylindrical housing. The gas, particles, liquid droplets
12 and or mists continue to flow spirally downwards tangentially in the cylindrical body. The
13 tail end of the cyclonic gas flow rests on top of the vortex breaker 7 where the clean and
14 dry gas spirals axially upwards towards the vortex finder 6 and exit from the top right side
15 of the separator through gas outlet tube 15. The particles, liquid droplets and or
16 condensing mists continue to spiral beyond the vortex breaker and then their swirling
17 movement is stopped by the swirl stopper plates 8. The particles, liquid droplets mists
18 and or some gas then exit the separator from the bottom side 11.

19
20 First and second conical fins 3 and 4 force the gases, liquids droplets and mists
21 to coalesce/collide together to form larger size liquid droplets and larger size particles for
22 effective subsequent cyclonic/ centrifugal separation. The gaps between the first and
23 second conical fins 3 and 4 and the inner wall of 2 the top cylindrical housing can be

made relatively small. For example, this dimension can be any suitable dimension, wherein different examples can include a range from 0.5 mm to 1 mm (millimeters) or even up to 2 mm to enhance the compression and coalescing/collision effect. The edges of the first and second conical fins 3 and 4 are sharp or substantially sharp or at least sufficiently sharp to ensure clean dislodge of the gas, liquids and particles mixture and also to ensure minimum restriction to gas flow.

Step, ridge or protrusion 9 is disposed at the joint between the top cylindrical housing 2 and the cylindrical body 5. Step 9 ensures that liquid droplets, particles and or condensing mists dislodge cleanly and outwardly from the second conical fin 4 to avoid re-entrainment or creep flow around to the vortex finder 6 resulting in carry over with the existing clean and dry gas. The vortex finder 6 also extends below second conical fin 4 for the same purpose.

Lastly, two separators can be used in series to provide coarse and fine separation to avoid overloading the first separator. With this design, the gaps between first conical fin 3 and second conical fin 4 and the inner wall of the top cylindrical housing 2 of the first separator is usually bigger than that of the second separator. This configuration is shown in FIG. 4 which shows two separators 10a and 10b shown aligned in series with each other so that the material can make a pass through two different separators. With this design, the first separator 10a in the series would have the larger gap between the first conical fin 3, the second conical fin 4 and the inner wall shown here as 20 in separator 10a than the gap 21 between conical fin 3, and second conical fin 4 and wall

2b in separator 10b. As shown in this diagram, the processed gasses exit from exit port 15 and enter into port 16 on separator 10b. In this way, the gasses are processed twice so that there is sufficient separation of particles from the gasses.

To enhance separation efficiency, two separators can be used in series to guarantee separation performance where the first separator can be used for coarse separation while the second separator for fine separation without overloading the first separator. For separation of very fine mists or particles of less than 5 or smaller micron size in a very dry gas, a cooler shall be used in conjunction with the separator to create small amount of liquid condensate which forms liquid droplets or liquid film which can allow fine particles, mists to stick onto due to adhesion.

For separation of very fine mists or particles of less than 1 micron, the device can include a cooler 30 made up of a tube coil where fine mists can be adhered onto the liquid film due to centrifugal forces inside the tube coil and allows other mists/particles to adhere to. As shown in FIG. 5, the cooler 30 has an inlet 31 and an outlet 32 that can be connected to inlet spiral tube 14 of first separator or inlet spiral tube 16 of the 2nd separator. The cooler 30 serves to form liquid condensation which will create a liquid film for fine mists/fine particles to adhere onto before the separator. In at least one embodiment, the cooler is separate from the separator because the flow velocity in the separator is too fast and the residence time is too short to create the desired results.

The reason why the centrifugal/ cyclone separator can separate particles liquid

1 droplets condensing mists (water based and or hydrocarbon based nature} from gases
2 without using a filter element, and can operate optimally at low gas flow rate from 30 l/h
3 up to 150 NI/h, and is able to separate fine particles condensing mists up to 5 to 10
4 micron size is attributed to the combined effect of the components listed above. For
5 example, with the first embodiment, the design relies on the use of the inlet spiral tube 1,
6 the first conical fin 3 and the second conical fin 4, and the step 9 on the cylindrical body
7 and the extension of the vortex finder below second conical fin 4. With the second
8 embodiment, the design differs in that it relies on the insert 1A with threaded area
9 forming a flow path like spiral tube, while relying on the same or similar components as
10 with the first embodiment listed above.

11
12 The combined effect of these key components is an excellent separator geometry
13 which ensures very smooth non-turbulent, high velocity flow rate which generates high
14
15 centrifugal/ cyclonic action for separation. There is also low restriction to low gas flow.
16 excellent compression and collision/ coalescing of fine condensing mists and particles
17 with liquid droplets and large particles to create larger size droplets/ particles for effective
18 separation by the first and second conical fins 3 and 4. Finally, the sharp edges of the
19 first and second conical fins 3 and 4, the step 9 at the joint between the top cylindrical
20 housing and the cylindrical body and the extension of the vortex finder below the second
21 conical fin 4 all ensure clean dislodge and outwardly separation of particles liquid
22 droplets and condensing mists and gas to prevent carry-over to the existing clean and
23 dry gas.

1
2 The length of cylindrical body 5 can be shortened to improve residence time
3 inside the separator without affecting the separation efficiency.
4

5 The gaps between the conical fins 3 and 4 and the inner diameter of top
6 cylindrical housing 2 can be increased up to 2 mm if the size of the largest particle is
7 expected to be around 1 + mm for coarse separation such as shown in the embodiment
8 10A in FIG. 4. The overall diameter and dimension of the separator can be increased
9 proportionally to maintain steps and thickness of the top cylindrical housing and the
10 cylindrical body. The thickness of the top cylindrical housing 2 and cylindrical body can
11 be increased to cope with higher pressure and temperature as required for mechanical
12 strength. However, the internal dimensions of the mentioned key features shall not be
13 reduced. The length of the spiral coil can be increased or decreased slightly without
14 affecting the separation efficiency.
15

16 The first embodiment of the separator comprises an inlet spiral tube 1 which has a
17 small inner bore to generate high gas flow velocity leading to high centrifugal/ cyclonic
18 forces inside the top cylindrical housing 2 for effective separation. It is also designed to
19 separate up to a maximum of 20 l/h of liquid flow from 2000 NI/h gas flow or maximum of
20 40l/h from 1000 NI/h gas flow.
21

22 At least one embodiment uses a step 9 positioned at the joint between the top
23 cylindrical housing 2 or first section or first body to the second portion of the housing or

second cylindrical body 5 to ensure that liquid droplets, particles and or mists dislodge cleanly and outwardly from the second conical fin 4 to avoid re-entrainment or surface flow around to the vortex finder 6 resulting in carry over with the existing clean and dry gas. The vortex finder 6 also extends 5mm below the second conical fin 4 for the same purpose.

Lastly, small amount of water or hydrocarbon liquid spray can also be added with the inlet dry and dirty gas to create liquid droplets or films for the fine mist and fine particles to adhere onto.

The materials listed above, particularly the first body section 2, and the second body section 5 of the housing, the spiral tube 1, the insert 1A, the conical fin 3, the conical fin 4, the vortex finder 6, the vortex breaker 7, the swirl stopper plate 8, and the step 9, can be made from any suitable material such as but not limited to Stainless Steel, corrosion resistant metal or alloys, PTFE, Polycarbonate or other hard plastic that is mechanically strong to withstand the operating pressure and chemically resistant.

In all, the design allows for a filterless separator or a separator having no coalescing filter using the geometry of the components listed above. This creates a device that does not need to be serviced as much and does not need numerous filter replacements as well. Thus, the components as described above create a cyclone in the gas using a spiral feed mechanism or spiral mechanism such as tube 1 or component 1A to create a separating cyclonic effect in the gas. The more dense

1 particles (and mists) are pushed towards the edge of the housing where they (collide
2 and) condense. The separator elements or fins 3 and 4 are configured to push these
3 components towards the wall of the housing where they will coalesce or condense.
4 These condensed particles then drop towards the outlet 11 while the remaining
5 uncondensed portion of the gas is driven against the vortex breaker 7 and sent up into
6 the vortex finder 6 wherein the remaining gas is passed up and out of the separator out
7 from outlet port 15. In this way gasses are separated from liquid or solid material without
8 the need for a filter that would otherwise need to be replaced.

9
10 Accordingly, while at least one embodiment of the present invention have been
11 shown and described, it is to be understood that many changes and modifications may
12 be made thereunto without departing from the spirit and scope of the invention as
13 defined in the appended claims.

CLEAN CLAIMS

WHAT IS CLAIMED IS:

1. A separator (10) for use with a gas or a liquid comprising at least one housing (2) comprising at least one inlet and at least one outlet (11), at least one spiral mechanism (1) configured to cause the gas or the liquid to spiral within said housing, characterized in that:
 - at least one separator element (3, 4) disposed adjacent to said at least one spiral mechanism (1) is configured to further separate particles from the gas or the liquid wherein said separator (10) is configured to separate at a rate of up to 20 l/h for fluid flow rate or 2000 NI/h for gas flow rate.
2. The separator as in claim 1, wherein said housing (2) comprises a cylinder having a substantially hollow inner region.
3. The separator as in claim 1, wherein said spiral mechanism (1) comprises at least one spiral tube.
4. The separator as in claim 1, wherein said spiral mechanism (1A) comprises at least one insert having a threaded area forming a flow path.
5. The separator as in claim 1, wherein said spiral mechanism (1A) comprises an insert comprising a substantially cylindrical block of material having a spiral

1 path.

2

3 6. The separator as in claim 1, wherein said at least one separator (3, 4) element
4 comprises a substantially conical fin.

5

6 7. The separator as in claim 1, wherein said at least one separator element (3,
7 4) comprises a first conical fin, and a second conical fin disposed adjacent to
8 said first conical fin.

9

10 8. The separator as in claim 1, wherein said housing (2) comprises a first body
11 section and a second body section, said inlet being coupled to said first body
12 section, and said outlet (11) being coupled to said second body section.

13

14 9. The separator as in claim 8, wherein said first body section is narrower than
15 said second body section (5).

16

17 10. The separator as in claim 9, further comprising a step (9), coupled to said
18 housing (2), said step formed in a region where said second body section
19 meets said first body section.

20

21

22 11. The separator as in claim 9, wherein said step (9) is positioned adjacent to
23 said first body section and adjacent to said at least one separator element (3,
24 4).

25

1 12. The separator as in claim 8, further comprising a vortex finder (6) extending
2 from said first body section to said second body section.

3
4 13. The separator as in claim 12, further comprising a vortex breaker (6)
5 positioned downstream from said vortex finder (6), in said second body section
6 (5).

7
8 14. The separator as in claim 13, further comprising a swirl stopper plate (8)
9 configured to interrupt a swirling flow of fluid and/or gasses inside the housing
10 (2).

11
12
13 15. The separator as in claim 14, wherein said swirl stopper plate (8) is positioned
14 adjacent to said outlet in said second body section (5).

15
16 16. The separator as in claim 7, wherein said housing has an inner wall (20,21)
17 and wherein said first conical fin (3) and said second conical fin (4) is spaced
18 from said inner wall (20) of said housing by .5 mm to 2 mm.

19
20
21 17. The separator as in claim 1, wherein said spiral mechanism (1) is disposed
22 adjacent to said inlet and said vortex breaker (7) is disposed adjacent to said
23 outlet (11).

24
25 18. The separator as in claim 1, wherein said separator is configured to separate

1 particles in a condensing mist of up to 10 microns in size.

2
3 19. The separator as in claim 1, further comprising a cooler (30) having an outlet
4 coupled to said inlet of said separator and configured to cool the input of
5 gasses or liquid into the separator.

6
7 20. A separator assembly comprising: a first separator (10a) as claimed in claim
8 1 and a second separator (10b) as claimed in claim 1, wherein said second
9 separator is in fluid communication with said first separator.

10
11 21. A process for separating material comprising a gas and at least one of a solid
12 and/or a liquid comprising introducing the material to be separated into a
13 separator (3, 4), passing the material to be separated into at least one spiral
14 mechanism (1, 1A) to create a cyclonic effect, passing said material to be
15 separated through a separator element (3, 4) comprising a plurality of fins
16 which are configured to create a collision effect to condense particles of the
17 material to be separated into at non-gaseous form, passing said material past
18 a step (9) inside of said housing so that said material to be separated in non
19 gaseous form separate from said separator element, removing at least some
20 of said material to be separated in non gaseous form from at least some of a
21 remaining gas, expelling at least some of said non gaseous material to be
22 separated from the separator from a first outlet port; and characterized in that:
23 the step of expelling at least some of said gaseous material to be separated

1 from a second outlet port (11) results in said separator being configured to
2 separate particles in a condensing mist of up to 10 microns in size.
3

4 22. The process as in claim 21, wherein said separator is configured to separate
5 at a rate of up to 20 l/h for fluid flow rate or 2000 NI/h for gas flow rate.
6

7 23. The process as in claim 21, wherein said separator comprises a housing
8 wherein said housing has an inner wall (20, 21) and wherein said step of
9 passing said material through a separator element comprises passing the
10 material through a separator element that has a first conical fin (3) and a
11 second conical fin (4) which are spaced from said inner wall (20) of said
12 housing by 0.5 mm to 2 mm.
13