CLAIMS

1. A process for producing a renewable hydrocarbon fuel product, the process comprising the steps of:

hydrotreating a renewable feed stock to produce a renewable paraffinic intermediate comprising at least 95% C8-C20 hydrocarbons; and

reacting said renewable paraffinic intermediate in a Fluid Catalytic Cracking (FCC) reaction zone under conditions sufficient to crack at least a portion of said renewable paraffinic intermediate to produce a renewable hydrocarbon fuel product;

wherein the renewable paraffinic intermediate is not isomerized.

2. The process of claim 1, further comprising the step of pre-treating said renewable feed stock.

3. The process of claim 1, wherein said reacting step comprises fluid catalytic cracking.

4. The process of claim 1, wherein conditions sufficient to crack at least a portion of said renewable paraffinic intermediate comprise a reaction temperature ranging from 400 °C to 800 °C.

5. The process of claim 1, wherein conditions sufficient to crack at least a portion of said renewable paraffinic intermediate comprise a reactor pressure ranging from greater than 0 to 80 psig.

6. The process of claim 1, further comprising the step of separating said renewable hydrocarbon fuel product into two or more constituent streams.

7. The process of claim 6, wherein said two or more constituent streams comprise at least two of a fuel gas stream, an ethylene stream, a propylene stream, a butylene stream, an LPG stream, a naphtha stream, an olefin stream, a diesel stream, a gasoline stream, a light cycle oil stream, a jet fuel stream, and a cat unit bottoms (slurry/decant oil) stream.

8. The process of claim 7, wherein at least one constituent stream is an olefin stream, and further comprising the step of feeding said olefin stream to an alkylation unit and/or a dimersol unit.

9. The process of claim 1, wherein said renewable paraffinic intermediate comprises propane.

10. The process of claim 9, further comprising the step of separating said propane from said renewable paraffinic intermediate and feeding said separated propane to a cracking unit.

11. The process of claim 1, wherein said renewable paraffinic intermediate comprises n-butane.

12. The process of claim 11, further comprising the step of separating said n-butane from said renewable paraffinic intermediate, and isomerizing said n-butane into isobutane.

13. The process of claim 1, wherein said reacting step is performed in the absence of a sulfur removal pre-treatment step of said renewable paraffinic intermediate.