

Method for the preparation of cyclohexanone

The present invention relates to a method for preparing cyclohexanone from cyclohexane.

It relates more particularly to a method for preparing cyclohexanone having an impurity content that allows the use of the cyclohexanone as a raw material for producing ϵ -caprolactam.

The method of the invention comprises in particular a treatment of the cyclohexanol/cyclohexanone mixture produced by the oxidation by oxygen of the cyclohexane in a dehydrogenation step to convert the cyclohexanol to cyclohexanone and the impurities present such as cyclopentenol. The method of the invention is suitable for obtaining cyclohexanone with a high degree of purity, compatible with its use as a raw material for synthesizing ϵ -caprolactam.



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In fact, nylon-6 (polyamide-6) or polycaprolactam is a major thermoplastic material for producing wires, fibres and miscellaneous moulded parts. This polymer is obtained by the polymerization of ϵ -caprolactam.

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This compound can be obtained by various methods. One of the most widely used methods consists in producing cyclohexanone oxime from cyclohexanone.

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In this method, the cyclohexanone must have a high degree of purity to avoid introducing impurities that could be disturbing, particularly in the caprolactam polymerization step, and which could also alter the properties of the polyamide obtained, particularly the coloration of the polyamide and its ageing resistance.

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Cyclohexanone is generally obtained by the oxidation of liquid cyclohexane by a gas containing oxygen to produce a cyclohexanol/cyclohexanone mixture, followed, after purification and separation of the cyclohexanol from the cyclohexanone, by dehydrogenation of the cyclohexanol to cyclohexanone.

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This oxidation of cyclohexane to cyclohexanone/cyclohexanol can be carried out in a single step, in the presence of an oxidation catalyst, or in a first step of oxidation of cyclohexane to cyclohexyl hydroperoxide, without catalyst, followed by

catalytic decomposition of this hydroperoxide to cyclohexanol and cyclohexanone.

During these oxidation steps, many impurities are produced, such as aldehydes, acids, alcohols and ketones. It is generally impossible subsequently to convert these impurities to upgradeable products such as adipic acid and ϵ -caprolactam. These impurities must therefore be removed and separated from the cyclohexanone and/or cyclohexanol, particularly for producing cyclohexanone.

Methods for oxidizing cyclohexane in the presence of a catalyst comprise a step of purification of the cyclohexanone/cyclohexanol mixture by a basic treatment or distillation in basic medium. Such a basic treatment removes the impurities.

However, such a method requires supplementary treatment with the use of a new reagent, a basic compound such as a metal hydroxide. It is therefore also necessary to provide for the separation and recovery of this basic compound in the form of effluents that generally need treatment (incineration or other treatment). In the case of oxidation of cyclohexane to cyclohexyl hydroperoxide, it is also possible to implement a treatment with a basic compound, with the same advantages and drawbacks as those described above.

One of the goals of the present invention is to remedy these drawbacks by proposing a method for preparing cyclohexanone by the oxidation of cyclohexane without the need for a purification treatment using a basic compound.

For this purpose, the invention proposes a method for producing cyclohexanone characterized in that it comprises the following steps:

- oxidation of cyclohexane to cyclohexyl hydroperoxide by oxygen or an oxygen-containing gas in the absence of catalyst
- purification of the reaction mixture by washing with water
- decomposition of the cyclohexyl hydroperoxide to cyclohexanol and cyclohexanone in the presence of a catalyst
- recovery of the cyclohexanol/cyclohexanone mixture by the separation of unreacted cyclohexane and the separation of products with higher boiling points than cyclohexanol/cyclohexanone
- dehydrogenation of the cyclohexanol present in the cyclohexanol/cyclohexanone mixture in the presence of a dehydrogenation catalyst
- distillation of the mixture obtained in a first distillation step in order to obtain a top fraction (F_1) comprising the compounds with lower boiling points than cyclohexanone, and a bottom fraction (Q_1)
- distillation of the bottom fraction (Q_1) in a second distillation step to obtain a top fraction (F_2) consisting of cyclohexanone, and a bottom fraction (Q_2)

The preparation of the cyclohexanol/cyclohexanone mixture as described in the first steps does not permit the removal of all the undesirable impurities, and particularly the α,β -cyclopentene-cyclopentane-1-carboxaldehyde (cyclopentenal) that is also found in the cyclohexanol/cyclohexanone mixture. This compound, which has a boiling point close to that of cyclohexanone, is very difficult to separate from it by distillation. In fact, this compound responds to certain qualification tests commonly performed to qualify cyclohexanone, particularly for synthesizing caprolactam, like the UV test carried out with a light ray at a certain wavelength or an oxidation test. In

the method of the invention, this compound, cyclopentenol, is chemically converted during the dehydrogenation step to products separable from cyclohexanone by, for example, a conventional
5 distillation operation like the one mentioned in the sequence of operations described above.

The step of dehydrogenation of the cyclohexanol present in the cyclohexanol/cyclohexanone mixture is carried
10 out in the presence of a dehydrogenation catalyst and under the usual temperature and pressure conditions described in the literature, such as, for example, a temperature of between 200°C and 450°C and an absolute pressure of between 1 and 3 bar. Patent US 4 918 239
15 offers a descriptive example of this dehydrogenation step.

In one embodiment of the invention, this dehydrogenation step is carried out in the presence of
20 a catalyst based on copper, magnesium, zinc oxides and/or mixtures thereof.

Thus, the method of the invention is suitable for producing cyclohexanone meeting the purity
25 requirements, particularly for producing ϵ -caprolactam, particularly the UV test for determining the transmission of a light ray with a wavelength of 230 nm through a volume of cyclohexanone. This transmission must be higher than 86%.

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According to another feature of the invention, the bottom fraction Q_2 is distilled in a third distillation step to obtain a top fraction (F_3) consisting of cyclohexanol/cyclohexanone and a bottom fraction (Q_3)
35 consisting of high boiling point compounds.

The top fraction (F_3) is advantageously recycled into the stream of cyclohexanol/cyclohexanone mixture introduced in the cyclohexanol dehydrogenation step.

5 According to another feature of the method of the invention, the top fraction (F_1) is distilled in order to obtain a new top fraction (F_4) consisting of low boiling point compounds, and a new bottom fraction (Q_4) essentially consisting of cyclohexanone. This bottom
10 fraction (Q_4) is advantageously recycled into the cyclohexanol/cyclohexanone mixture introduced in the hydrogenation step.

The method of the invention is suitable for recovering
15 a cyclohexanone, as top fraction (F_2), having high purity criteria and particularly a UV test (% transmission at $\lambda = 230$ nm higher than the required specification). The cyclohexanone produced by the method of the invention is therefore advantageously
20 used for manufacturing ϵ -caprolactam by oximation.

Other advantages and details of the invention will appear more clearly from the examples given below exclusively for information, and from the description
25 of an embodiment of the method of the invention made with reference to the single figure appended hereto, which represents a block diagram of this embodiment.

Example 1:

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A mixture of cyclohexanol containing 600 ppm of cyclopentenal was fed at 1 into a column reactor 2.

A catalyst was placed in a fixed bed in the column 2.
35 The catalyst was based on copper oxide. The temperature in the column 2 was 230°C. The degree of conversion of cyclohexanol to cyclohexanone was 30%. The cyclopentenal concentration in the reaction mixture

issuing from the reactor 2 was below the limit detectable by known measurement methods, that is, less than 30 ppm.

5 Example 2:

A mixture containing 59% by weight of cyclohexanone, 39% by weight of cyclohexanol, 0.5% by weight of water and 1.5% by weight of heavy or light products such as
10 impurities to be removed, is fed into the reactor 2. Particular impurities included cyclopentenol that was present in a concentration of 2950 ppm.

The feed rate of this mixture into the reactor 2 was
15 215 g/h. The reactor temperature was 310°C. The reaction mixture issuing from the reactor contained 80.6% by weight of cyclohexanone, 16.5% by weight of cyclohexanol, and heavy or light impurities. The cyclopentenol concentration in this medium was lower
20 than the detection threshold, that is to say less than 30 ppm. The degree of conversion of cyclohexanol to cyclohexanone was 55%.

The reaction mixture issuing from the reactor 2 was fed
25 into a heat exchanger 3, then via the line 4 into a first distillation column 5. This column comprised 22 theoretical stages and operated under the usual temperature and pressure conditions known to a person skilled in the art in the field of cyclohexanone
30 distillation. The bottom fraction Q_1 was introduced into a second distillation column 6 also comprising 22 theoretical trays. The fraction F_2 recovered at the top was cyclohexanone with a degree of purity higher than 99.8% and having a transmission of 88.5% in the UV test
35 at a wavelength of 230 nm.

In the embodiment shown, the bottom fraction Q_2 can be fed into a third distillation column 7 for separating

the heavy products (with higher boiling point than that of cyclohexanone) in the form of a fraction Q_3 . The top fraction F_3 containing cyclohexanone and cyclohexanol can be recycled into the dehydrogenation reactor 2.

5 According to the embodiment shown in the appended figure, the top fraction F_1 collected from the distillation column 5 can be fed into a settler 8 in order to separate the aqueous phase and then to a distillation column 9. The bottom fraction Q_4
10 collected, containing cyclohexanone, can be recycled into the reactor 2. The top fraction F_4 containing light products, that is to say those of low boiling points, was treated as an effluent.

15 Example 3:

Example 2 was repeated but by feeding into the reactor a mixture containing 59% by weight of cyclohexanone, 39% by weight of cyclohexanol, 0.5% by weight of water
20 and 1.5% of heavy and light impurities including 360 ppm of cyclopentenol.

The feed rate of this mixture into the reactor 2 was 135 g/h. The reactor temperature was 270°C. The
25 composition of the reaction mixture issuing from the reactor 2 was:

75.2% by weight of cyclohexanone, 22.3% by weight of cyclohexanol, and heavy or light impurities. The cyclopentenol concentration in this medium was lower
30 than the detection threshold, that is, lower than 30 ppm. The degree of conversion of cyclohexanol to cyclohexanone was 44%. The cyclohexanone recovered as fraction F_2 had a cyclopentenol content of less than 30 mg/kg and a transmission of 89.5% in the UV test at
35 230 nm.

Claims

1. Method for producing cyclohexanone characterized in that it comprises the following steps:
 - 5 • oxidation of cyclohexane to cyclohexyl hydroperoxide by oxygen in the absence of catalyst
 - purification of the reaction mixture by washing with water
 - decomposition of the cyclohexyl hydroperoxide to
10 cyclohexanol and cyclohexanone in the presence of a catalyst
 - recovery of the cyclohexanol/cyclohexanone mixture by the separation of unreacted cyclohexane and the separation of products with higher boiling points
15 than cyclohexanol/cyclohexanone
 - dehydrogenation of the cyclohexanol present in the cyclohexanol/cyclohexanone mixture in the presence of a dehydrogenation catalyst
 - distillation of the mixture obtained in a first
20 distillation step in order to obtain a top fraction (F_1) comprising the compounds with lower boiling points than cyclohexanone, and a bottom fraction (Q_1)
 - distillation of the bottom fraction (Q_1) in a
25 second distillation step to obtain a top fraction (F_2) consisting of cyclohexanone, and a bottom fraction (Q_2)
2. Method according to Claim 1, characterized in that
30 the bottom fraction Q_2 is distilled in a third distillation step to obtain a top fraction (F_3) consisting of cyclohexanol/cyclohexanone and a bottom fraction (Q_3) consisting of high boiling point compounds.
- 35 3. Method according to Claim 2, characterized in that the top fraction (F_3) is mixed with the

cyclohexanol/cyclohexanone mixture introduced in the dehydrogenation step.

4. Method according to one of the preceding claims,
5 characterized in that the top fraction (F_1) is distilled, in a fourth distillation step, in order to obtain a top fraction (F_4) consisting of low boiling point compounds, and a bottom fraction (Q_4) consisting of cyclohexanone.
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5. Method according to Claim 4, characterized in that the bottom fraction (Q_4) is added to the cyclohexanol/cyclohexanone mixture introduced in the dehydrogenation step.
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6. Method according to one of the preceding claims, characterized in that the dehydrogenation step is carried out in the presence of a catalyst selected from the group comprising copper, magnesium and zinc
20 oxides and mixtures thereof.
7. Method according to one of the preceding claims, characterized in that the cyclohexanone obtained in the top fraction (F_2) is used as a raw material for
25 producing ϵ -caprolactam.