CLAIMS

1. A process for the rejuvenation of an at least partially spent catalyst resulting from a hydrotreating and/or hydrocracking process, said at least partially spent catalyst resulting from a fresh catalyst comprising at least one metal from group VIII, at least one metal from group VIb, an oxide support, and optionally phosphorus, said process comprises the following stages:
   a) the at least partially spent catalyst is regenerated in an oxygen-containing gas stream at a temperature of between 300°C and 550°C, so as to obtain a regenerated catalyst,
   b) then said regenerated catalyst is brought into contact with phosphoric acid and an organic acid chosen from gluconic acid, γ-ketovaleric acid, lactic acid, ascorbic acid or succinic acid,
   c) a drying stage is carried out at a temperature of less than 200°C, without subsequently calcining it, so as to obtain a rejuvenated catalyst.

2. The process as claimed in claim 1, in which the organic acid added per metal/metals from group VIb present in the regenerated catalyst molar ratio is between 0.01 and 5 mol/mol.

3. The process as claimed in one of the preceding claims, in which the phosphorus added per metal from group VIb already present in the regenerated catalyst molar ratio is between 0.01 and 5 mol/mol.

4. The process as claimed in one of the preceding claims, in which the fresh catalyst has a content of metal from group VIb of between 1% and 40% by weight of oxide of said metal from group VIb, with respect to the weight of the catalyst, and a total content of metal from group VIII of between 1% and 10% by weight of oxide of said metal from group VIII, with respect to the weight of the catalyst.

5. The process as claimed in one of the preceding claims, in which the fresh catalyst contains phosphorus, the total content of phosphorus being between 0.1% and 20% by weight, expressed as P_2O_5, with respect to the total weight of the catalyst.

6. The process as claimed in one of the preceding claims, in which the oxide support of the rejuvenated catalyst is chosen from aluminas, silica, silica-aluminas or also titanium or magnesium oxides, used alone or as a mixture with alumina or silica-alumina.

7. The process as claimed in one of the preceding claims, in which stage b) additionally comprises bringing the regenerated catalyst into contact with at least one compound comprising a metal from group VIb and at least one compound comprising a metal from group VIII.

8. The process as claimed in the preceding claim, in which the molar ratio of the metal from group VIb added per metal from group VIb already present in the regenerated catalyst is between 0.05 and 2.5 mol/mol, and the molar ratio of the metal from group VIII added per metal from group VIII already present in the regenerated catalyst is between 0.01 and 2.5 mol/mol.

9. The process as claimed in one of the preceding claims, in which the regeneration stage is preceded by a deoiling stage which comprises bringing an at least partially spent catalyst resulting from a hydrotreating and/or hydrocracking process into contact with a stream of inert gas at a temperature of between 300°C and 400°C.

10. The process as claimed in one of the preceding claims, in which the rejuvenated catalyst is subjected to a sulfidation stage after stage c).

11. The use of the catalyst obtained according to the process as claimed in one of claims 1 to 10 in a process for the hydrotreating and/or hydrocracking of hydrocarbon cuts.