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(21) International Application Number: PCT/US97/14416 (22) International Filing Date: 15 August 1997 (15.08.97) (30) Priority Data: 60/027,859 15 August 1996 (15.08.96) US 60/034,612 31 December 1996 (31.12.96) US 08/848,438 8 May 1997 (08.05.97) US (71) Applicant (for all designated States except US): EXXON CHEMICAL PATENTS INC. [US/US]; 5200 Bayway Drive, Baytown, TX 77520-5200 (US). (72) Inventors; and (75) Inventors/Applicants (for US only): BRADOW, Carl, W. [-/US]; 4115 North Webber Drive, Pearland, TX 77584 (US). GRENOBLE, Dane, C. [-/US]; 18201 Sandy Cove, Nassau Bay, TX 77058 (US). MILAM, Stanley, N. [-/US]; 710 Teetshorn, Houston, TX 77009 (US). WINQUIST, Bruce, H. [-/US]; 11202 Cold Spring Drive, Houston, TX 77043 (US). MURRAY, Brendan, D. [-/US]; 1118 Stoney Hill Drive, Houston, TX 77077 (US). FOLEY, Richard [-/US]; 5000 Montrose Boulevard #12H, Houston, TX 77006 (US).		(74) Agents: RUSSELL, Linda, K.; Exxon Chemical Company, P.O. Box 2149, Baytown, TX 77522-2149 (US) et al. (81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, GH, HU, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ARIPO patent (GH, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG). Published <i>With international search report.</i>
(54) Title: HYDROCARBON CONVERSION PROCESS (57) Abstract This invention provides an integrated process for converting a hydrocarbon feedstock having components boiling above about 100 °C into steam cracked products, which process comprises passing said feedstock to a hydrotreating zone to effect substantially complete decomposition of organic sulfur and/or nitrogen compounds, passing the product from said hydrotreating zone to an aromatics saturation zone, and subsequently passing the product from said aromatics saturation zone to a steam cracking zone, and recovering therefrom hydrogen and C ₁ -C ₄ hydrocarbons, steam cracked naphtha, steam cracked gas oils and steam cracked tar therefrom, wherein the amount of steam cracked gas oil produced is reduced by at least 30 percent, and the amount of steam cracked tar produced is reduced by at least about 40 percent, basis the starting hydrocarbon feedstock which has not been subjected to hydrotreating and aromatics saturation.		