

DESCRIPTION

PROCESS FOR PRODUCTION OF WATER-ABSORBENT RESIN

5 Technical Field

[0001]

The present invention relates to a process for production of a water-absorbent resin, and a water-absorbent resin prepared thereby. More particularly, the present invention relates to a method for obtaining a water-absorbent resin with reduced odor in a process for production of a water-absorbent resin by reversed-phase suspension polymerization, and the water-absorbent resin prepared thereby.

15

Background Art

[0002]

Water-absorbent resins are widely used for hygienic materials such as disposable diapers and sanitary napkins, daily commodities such as pet sheets, and industrial materials such as water blocking materials for cables.

20

The hygienic materials such as disposable diapers and sanitary napkins generally comprise a top sheet, a back sheet, a hot melt adhesive, an elastic material, a water-absorbent resin, pulp fiber, and the like, and a number of synthetic resins and reforming agents are used therein.

25

Thus the hygienic materials have some odor originating from the raw material components. Since these hygienic materials are worn on a human body, the odor makes those who wear them uncomfortable even if it is subtle, and
5 therefore it is desired to develop an odor-free material.

Among the constituents of the hygienic materials, the water-absorbent resin has a subtle odor originating from the substances used in the production process, and since the odor tends to diffuse upon absorbing water, it is
10 considered to be desirable to reduce the odor.

[0003]

Known water-absorbent resins used for the hygienic materials include, for example, a partially-neutralized product of polyacrylic acid, a neutralized product of a
15 starch-acrylic acid graft polymer, a hydrolysate of a starch-acrylonitrile graft copolymer, a saponified product of a vinyl acetate-acrylic acid ester copolymer, and the like.

[0004]

20 As the process for production of such the water-absorbent resin, an aqueous polymerization method, a reversed-phase suspension polymerization method, and the like are known, but in the case of the water-absorbent resin prepared by the reversed-phase suspension
25 polymerization method, in which polymerization is performed by suspending a water-soluble monomer in a dispersion

medium, a major cause of the odor is considered to originate from the dispersion medium.

[0005]

Known conventional arts for producing the water-
5 absorbent resin by the reversed-phase suspension
polymerization method include a method of polymerizing an
 α,β -unsaturated carboxylic acid and the aqueous alkali
metal salt solution thereof in a petroleum hydrocarbon
solvent using a radical polymerization initiator in the
10 presence/non-presence of a crosslinking agent, in which a
sucrose fatty acid ester is used as a protective colloid
agent (see Patent Document 1), and a method of polymerizing
an α,β -unsaturated carboxylic acid and a 25% by weight or
higher aqueous alkali metal salt solution thereof in a
15 petroleum hydrocarbon solvent using a radical
polymerization initiator in the presence/non-presence of a
crosslinking agent, in which a polyglycerol fatty acid
ester with an HLB of 2-16 is used as a surfactant (see
Patent Document 2), but these production technologies did
20 not focus on reduction of odor, and thus the resultant
water-absorbent resins were not those with low enough odor.
Patent Document 1:

Japanese Unexamined Patent Publication (Kokai) No. 61-
87702

25 Patent Document 2:

Japanese Unexamined Patent Publication (Kokai) No. 62-

172006

Disclosure of the Invention

[0006]

5 An object of the present invention is to provide a process for production of a water-absorbent resin in which odor upon absorbing water is reduced, and the water-absorbent resin prepared thereby.

[0007]

10 Conventional reversed-phase suspension polymerization is performed by adding an aqueous monomer solution to a dispersion medium in which a surfactant is dissolved, followed by dispersing droplets of the aqueous monomer solution under stirring. However, the water-absorbent
15 resin prepared by such the polymerization method had odor originating from the dispersion medium when it absorbed water.

[0008]

20 Since a petroleum hydrocarbon with a boiling point of 80 to 130°C is generally used as the dispersion medium in the production of the water-absorbent resin by a reversed-phase suspension polymerization method, it was considered that odor could be reduced by drying the resin at a high temperature higher than the boiling point of the dispersion
25 medium. However, it was found that odor could not be reduced enough by a heat treatment.

[0009]

The present inventors have studied the cause why the water-absorbent resin prepared by the reversed-phase suspension polymerization method failed in reducing odor by heating, and have found that a small amount of the dispersion medium is confined in the particles of the water-absorbent resin.

The present inventors have intensively studied how to prevent the dispersion medium from being confined in the particles of the water-absorbent resin, and have found that a water-absorbent resin with extremely low odor originating from the dispersion medium, when it absorbs water, is obtained by a reversed-phase suspension polymerization method comprising dispersing an aqueous monomer solution in a dispersion medium to which no surfactant has been added, adding a surfactant to the resultant emulsion to disperse the monomer further, and polymerizing, which led to the completion of the present invention.

[0010]

That is, in one aspect, there is provided a process for production of a water-absorbent resin by subjecting a water-soluble ethylenically unsaturated monomer to reversed-phase suspension polymerization, comprising the following steps of:

(A) adding an aqueous solution of water-soluble ethylenically unsaturated monomer to a petroleum

hydrocarbon dispersion medium to disperse the aqueous solution in the dispersion medium,

(B) adding a surfactant to the emulsion to further disperse the monomer in the emulsion, and

(C) performing the reversed-phase suspension polymerization using a water-soluble radical polymerization initiator, optionally in the presence of an internal-crosslinking agent.

[0011]

The process for production of present invention enables the production of a water-absorbent resin with extremely low odor when it absorbs water.

[0011a]

Accordingly, in another aspect, there is provided a water-absorbent resin prepared by the production process as defined above.

Best Mode for Carrying Out the Invention

[0012]

In the process for production of the present invention, the first step is to add an aqueous solution of water-soluble ethylenically unsaturated monomer to a petroleum hydrocarbon dispersion medium to disperse the aqueous solution in the dispersion medium (step (A)).

Examples of the water-soluble ethylenically unsaturated monomer used in the present invention include monomers having an acid group, such as (meth)acrylic acid ["(meth)acrylic" denotes both "acrylic" and "methacrylic", and the same applies hereinafter], 2-(meth)acrylamide-2-methylpropanesulfonic acid and maleic acid and the salts

PCT/JP2007/059066

thereof; nonionic unsaturated monomers such as (meth)acrylamide, *N,N*-dimethyl (meth)acrylamide, 2-hydroxyethyl (meth)acrylate and *N*-methylol (meth)acrylamide; and amino group-containing unsaturated monomers such as diethylaminoethyl (meth)acrylate and diethylaminopropyl (meth)acrylate, and the quaternarized compounds thereof. These compounds can be used alone or in combination by mixing 2 or more thereof.

[0013]

10 Examples of the alkaline compound to be used at the time when the monomer having an acid group is neutralized to form a salt include lithium, sodium, potassium, ammonium compounds, and the like.

[0014]

15 Preferred water-soluble ethylenically unsaturated monomers include (meth)acrylic acid and the salts thereof, and (meth)acrylamide, in view of industrial availability.

 The monomer concentration of an aqueous solution of water-soluble ethylenically unsaturated monomer is from 20% by mass to the saturation concentration.

[0015]

 When the monomer having an acid group is neutralized, the preferred neutralization degree is from 30 to 90% by mol of the acid group in the water-soluble ethylenically unsaturated monomer. It is not preferred that the neutralization degree is lower than 30% by mol, because the

acid group tends not to be ionized under the neutralization degree, and thus the water-absorption capacity becomes low. It is not preferred that the neutralization degree exceeds 90% by mol, because when the monomer is used for hygienic materials, there is a possibility that problems may occur in its safety and the like.

The aqueous solution of a water-soluble ethylenically unsaturated monomer may contain a chain transfer agent, thickener and the like, if it is needed.

10 [0016]

Examples of the chain transfer agent include compounds such as thiols, thiol acids, secondary alcohols, hypophosphorous acid, phosphorous acid, and the like. These compounds can be used alone, or in combination of 2 or more thereof.

15 [0017]

Examples of the thickener include carboxymethyl cellulose, hydroxyethyl cellulose, hydroxypropyl cellulose, methylcellulose, polyethylene glycol, polyacrylic acid, a neutralized product of polyacrylic acid, polyacrylamide, and the like.

20 [0018]

Examples of the petroleum hydrocarbon used in the present invention as the dispersion medium for reversed-phase suspension polymerization include aliphatic hydrocarbons having 6 to 8 carbon atoms, such as *n*-hexane,

n-heptane, 2-methylhexane, 3-methylhexane and *n*-octane;
alicyclic hydrocarbons having 6 to 8 carbon atoms, such as
cyclohexane, methyl cyclopentane and methyl cyclohexane;
and aromatic hydrocarbons such as benzene, toluene and
5 xylene.

[0019]

Among these, it is preferred to use a dispersion
medium selected from at least one of the aliphatic
hydrocarbons or alicyclic hydrocarbons having 6 or 7 carbon
10 atoms, or a mixture thereof, in view of industrial
availability and cost.

[0020]

The amount of the dispersion medium to be used is
preferably from 50 to 600 parts by mass, more preferably
15 from 50 to 400 parts by mass, and further preferably from
50 to 200 parts by mass, based on 100 parts by mass of the
aqueous solution of water-soluble ethylenically unsaturated
monomer, since the amount enables uniform dispersion of the
the aqueous solution of water-soluble ethylenically
20 unsaturated monomer, and facilitates control of the
polymerization temperature.

[0021]

In the process for production of the present invention,
a further preferred result is obtained when the aqueous
25 solution of water-soluble ethylenically unsaturated monomer
is added to and dispersed in the petroleum hydrocarbon

dispersion medium in the presence of a polymeric dispersion agent.

[0022]

It is preferred to select a polymeric dispersion agent
5 which can be dissolved or dispersed in the above petroleum hydrocarbon dispersion medium as the polymeric dispersion agent used in the present invention, and that with an average molecular weight of 20,000 or less, preferably 10,000 or less, and more preferably 5,000 or less, is
10 exemplified. Specific examples of the polymeric dispersion agent include maleic anhydride modified polyethylene, maleic anhydride modified polypropylene, maleic anhydride modified ethylene-propylene copolymer, maleic anhydride-ethylene copolymer, maleic anhydride-propylene copolymer,
15 maleic anhydride-ethylene-propylene copolymer, polyethylene, polypropylene, ethylene-propylene copolymer, oxidized polyethylene, oxidized polypropylene, ethylene-acrylic acid copolymer, ethyl cellulose, ethylhydroxyethyl cellulose, anhydrous maleinated polybutadiene, anhydrous maleinated
20 EPDM (ethylene/propylene/diene terpolymer), and the like.

[0023]

Among these, it is preferred to use at least one selected from the group consisting of maleic anhydride modified polyethylene, maleic anhydride modified
25 polypropylene, maleic anhydride modified ethylene-propylene copolymer, maleic anhydride-ethylene copolymer, maleic

anhydride-propylene copolymer, maleic anhydride-ethylene-propylene copolymer, polyethylene, polypropylene, ethylene-propylene copolymer, oxidized polyethylene and oxidized polypropylene.

5 [0024]

The amount of the polymeric dispersion agent to be used is preferably from 0 to 5 parts by mass, more preferably from 0.01 to 3 parts by mass, and further preferably from 0.05 to 2 parts by mass, based on 100 parts
10 by mass of the aqueous solution of water-soluble ethylenically unsaturated monomer. It is not preferred that the amount of the polymeric dispersion agent to be added exceeds 5 parts by mass, since it is less economical.
[0025]

15 In the process for production of the present invention, a surfactant is added to the emulsion prepared in the above step (A) to further disperse the aqueous solution of water-soluble ethylenically unsaturated monomer in the petroleum hydrocarbon dispersion medium (step (B)).

20 Examples of the surfactant used in the step (B) include nonionic surfactants such as sorbitan fatty acid ester, polyoxyethylene sorbitan fatty acid ester, polyglycerin fatty acid ester, polyoxyethylene glycerin fatty acid ester, sucrose fatty acid ester, sorbitol fatty
25 acid ester, polyoxyethylene sorbitol fatty acid ester, polyoxyethylene alkyl ether, polyoxyethylene alkylphenyl

ether, polyoxyethylene castor oil, polyoxyethylene hardened
castor oil, alkylallyl formaldehyde condensed
polyoxyethylene ether, polyoxyethylene polyoxypropylene
alkyl ether, polyethylene glycol fatty acid ester, alkyl
5 glucoside, N-alkyl gluconamide, polyoxyethylene fatty acid
amide and polyoxyethylene alkylamine; and anionic
surfactants such as fatty acid salts, alkylbenzene
sulfonate, alkylmethyl taurate, polyoxyethylene alkylphenyl
ether sulfate, polyoxyethylene alkyl ether sulfate,
10 polyoxyethylene alkyl ether sulfonic acid and the salts
thereof, polyoxyethylene alkylphenyl ether phosphoric acid
and the salts thereof, and polyoxyethylene alkyl ether
phosphoric acid and the salts thereof. The surfactants can
be used alone or in combination of two or more thereof.

15 [0026]

Among these surfactants, at least one selected from
the group consisting of polyglycerin fatty acid ester,
sucrose fatty acid ester and sorbitan fatty acid ester is
preferred, in view of a dispersion stability of the aqueous
20 solution of water-soluble ethylenically unsaturated monomer.

The amount of the surfactant to be used in the step
(B) is preferably from 0.01 to 5 parts by mass, and more
preferably from 0.05 to 3 parts by mass, based on 100 parts
by mass of the aqueous solution of water-soluble
25 ethylenically unsaturated monomer. It is not preferred
that the amount of the surfactant to be added is less than

0.01 parts by mass, since the dispersion stability of the aqueous monomer solution becomes low, while it is not preferred that the amount exceeds 5 parts by mass since it is less economical.

5 [0027]

The form of the surfactant to be added in the step (B) is not particularly limited, but it is preferred to use after diluting or dissolving the surfactant in a small amount of the dispersion medium thereby bringing about the dispersion stability in a short time.

Also, the above-mentioned polymeric dispersion agent may be added in the step (B), in addition to the surfactant.
[0028]

When the polymeric dispersion agent is added together with the surfactant, the amount to be added thereof is preferably from 0 to 5 parts by mass, more preferably from 0.01 to 3 parts by mass, and further preferably from 0.05 to 2 parts by mass, based on 100 parts by mass of the aqueous solution of water-soluble ethylenically unsaturated monomer. It is not preferred that the amount of the polymeric dispersion agent to be added exceeds 5 parts by mass because it is less economical. It is also preferred to use the polymeric dispersion agent in a state that the dispersion agent has been dissolved or dispersed in a small amount of the dispersion medium under heat in advance thereby bringing about dispersion stability in a short time.

[0029]

In the process for production of the present invention, the reversed-phase suspension polymerization is performed on the emulsion prepared in the above step (B) optionally in the presence of an internal-crosslinking agent, using a water-soluble radical polymerization initiator to obtain a water-absorbent resin (step (C)).

Examples of the water-soluble radical polymerization initiator include persulfates such as potassium persulfate, ammonium persulfate and sodium persulfate; peroxides such as hydrogen peroxide; and azo compounds such as 2,2'-azobis(2-amidinopropane) dihydrochloride, 2,2'-azobis[N-(2-carboxyethyl)-2-methylpropionedi-amine] tetrahydrate, 2,2'-azobis(1-imino-1-pyrrolidino-2-methylpropane) dihydrochloride and 2,2'-azobis[2-methyl-N-(2-hydroxyethyl)-propionamide].

[0030]

Among these, potassium persulfate, ammonium persulfate, sodium persulfate and 2,2'-azobis(2-amidinopropane) dihydrochloride are preferred, in view of availability and handling.

The water-soluble radical polymerization initiator may be used as a redox polymerization initiator together with a reducing agent such as sulfite and ascorbic acid.

[0031]

The amount of the water-soluble radical polymerization

initiator to be used is generally from 0.01 parts to 1 part by mass, based on 100 parts by mass of the water-soluble ethylenically unsaturated monomer. It is not preferred that the amount is less than 0.01 parts by mass, since the polymerization degree becomes low, while it is not preferred that it exceeds 1 part by mass, since an abrupt polymerization reaction occurs.

[0032]

The timing when the water-soluble radical polymerization initiator is added is not particularly limited, but it is preferred to add the initiator in advance to the aqueous solution of water-soluble ethylenically unsaturated monomer.

[0033]

Examples of the internal-crosslinking agent to be used, if it is needed, include polyols such as (poly)ethylene glycol [(poly) denotes both cases with and without the prefix of "poly", and the same applies hereinafter], 1,4-butanediol, glycerin and trimethylol propane; poly-unsaturated esters having 2 or more vinyl groups, prepared by reaction of polyols with unsaturated acids such as acrylic acid and methacrylic acid; bisacrylamides such as *N,N'*-methylenebisacrylamide; polyglycidyl compounds having 2 or more glycidyl groups such as (poly)ethylene glycol diglycidyl ether, (poly)ethylene glycol triglycidyl ether, (poly)glycerin diglycidyl ether, (poly)glycerin triglycidyl

ether, (poly)propylene glycol polyglycidyl ether and (poly)glycerol polyglycidyl ether, and the like. These internal-crosslinking agents can be used alone or in combination of two or more thereof.

5 [0034]

The amount of the internal-crosslinking agent to be added is preferably from 0 to 3 parts by mass, more preferably from 0 to 1 part by mass, and further preferably from 0.001 to 0.1 parts by mass, based on 100 parts by mass
10 of the water-soluble ethylenically unsaturated monomer. It is not preferred that the amount to be added exceeds 3 parts by mass, since the crosslinkage is formed excessively and the water-absorption capacity declines too much.

It is preferred to use the internal-crosslinking agent
15 in a way that it has been added to the aqueous solution of water-soluble ethylenically unsaturated monomer in advance.
[0035]

The reaction temperature for performing the reversed-phase suspension polymerization cannot be determined
20 generally in the present invention, since it varies depending on the kind and amount of the polymerization initiator to be used, but the temperature is preferably from 20 to 100°C, and more preferably from 40 to 90°C. It is not preferred that the reaction temperature is lower
25 than 20°C, since the polymerization degree may decline, while it is not preferred that it exceeds 100°C, since an

abrupt polymerization reaction occurs.

[0036]

In the present invention, the reversed-phase suspension polymerization may be performed at the second stage, after adding the water-soluble ethylenically unsaturated monomer to the polymerization reaction suspension that completed the step (C). In the case where the reversed-phase suspension polymerization is performed in 2 stages, the polymerization reaction suspension is cooled until the surfactant reaches a precipitation state after completion of the first stage, and then the water-soluble ethylenically unsaturated monomer is added in the second stage to obtain particles in a form that the polymerized particles at the first stage are agglomerated. This is preferred because this method allows particles in a size suitable for an application to hygienic materials to be obtained.

The amount of the water-soluble ethylenically unsaturated monomer to be added at the second stage is preferably from 50 to 300 parts by mass, and more preferably from 100 to 200 parts by mass, based on 100 parts by mass of the water-soluble ethylenically unsaturated monomer at the first stage, in view of obtaining proper agglomerated particles.

Incidentally, when the reversed-phase suspension polymerization is performed in 2 stages, the above

mentioned step (A) and step (B) are performed during the polymerization at the first stage.

[0037]

In the present invention, a post-crosslinking reaction
5 on a surface layer of the particles of the water-absorbent resin may be performed out by adding a post-crosslinking agent having 2 or more functional groups, which has reactivity to the functional groups originating from the water-soluble ethylenically unsaturated monomer, to the
10 water-absorbent resin prepared in the steps (A) through (C) by the aforementioned method. The post-crosslinking on the particle surface layer of the water-absorbent resin enhances various performances such as water-absorption capacity under pressure, water-absorption rate and gel
15 strength, and provides performances suitable for application to hygienic materials.

[0038]

The post-crosslinking agent used for the post-crosslinking reaction is not particularly limited, as long
20 as it is able to react with the functional groups originating from the water-soluble ethylenically unsaturated monomer used for the polymerization.

Examples of the post-crosslinking agent to be used include polyols such as ethylene glycol, propylene glycol,
25 1,4-butanediol, trimethylol propane, glycerin, polyoxyethylene glycol, polyoxypropylene glycol and

polyglycerin; polyglycidyl compounds such as (poly)ethylene glycol diglycidyl ether, (poly)ethylene glycol triglycidyl ether, (poly)glycerin diglycidyl ether, (poly)glycerin triglycidyl ether, (poly)propylene glycol polyglycidyl ether and (poly)glycerol polyglycidyl ether; haloepoxy compounds such as epichlorohydrin, epibromohydrin and α -methylepichlorohydrin; compounds having 2 or more reactive functional groups such as isocyanate compounds including 2,4-tolylene diisocyanate and hexamethylene diisocyanate; oxetane compounds such as 3-methyl-3-oxetane methanol, 3-ethyl-3-oxetane methanol, 3-butyl-3-oxetane methanol, 3-methyl-3-oxetane ethanol, 3-ethyl-3-oxetane ethanol and 3-butyl-3-oxetane ethanol; oxazoline compounds such as 1,2-ethylenebisoxazoline; carbonate compounds such as ethylene carbonate. These post-crosslinking agents may be used alone or in combination of 2 or more thereof.

Among these, polyglycidyl compounds such as (poly)ethylene glycol diglycidyl ether, (poly)ethylene glycol triglycidyl ether, (poly)glycerin diglycidyl ether, (poly)glycerin triglycidyl ether, (poly)propylene glycol polyglycidyl ether and (poly)glycerol polyglycidyl ether are preferred, in view of excellent reactivity.

[0039]

The amount of the post-crosslinking agent to be added is preferably from 0.01 to 5 parts by mass, and more preferably from 0.02 to 3 parts by mass, based on 100 parts

by mass a total amount of the water-soluble ethylenically unsaturated monomer used for the polymerization.

[0040]

It is not preferred that the amount of the post-crosslinking agent to be added is less than 0.01 parts by mass, since it fails to enhance various capacity such as the water-absorption capacity under pressure, water-absorption rate and gel strength of the resultant resin, while it is not preferred to exceed 5 parts by mass, since it results in excessively low water-absorption capacity.

[0041]

When the post-crosslinking agent is added, it may be added as it is or in the form of an aqueous solution, or in the form of a solution dissolved in a hydrophilic organic solvent, if it is needed. Examples of the hydrophilic organic solvent include lower alcohols such as methyl alcohol, ethyl alcohol, *n*-propyl alcohol, isopropyl alcohol and propylene glycol; ketones such as acetone and methyl ethyl ketone; ethers such as diethyl ether, dioxane and tetrahydrofuran; amides such as *N,N*-dimethylformamide; sulfoxides such as dimethyl sulfoxide, and the like. These hydrophilic organic solvents may be used alone or in combination of 2 or more thereof.

[0042]

The timing of adding the post-crosslinking agent is not particularly limited as long as it is added after

completion of the polymerization. It is preferred that the post-crosslinking reaction is performed in a drying process after polymerization in the presence of water in a range of 1 part to 200 parts by mass, more preferably of 5 to 100 parts by mass, and most preferably of 10 to 50 parts by mass, based on 100 parts by mass of the water-absorbent resin. Thus, by adjusting the water content at the time of adding the post-crosslinking agent, post-crosslinkage is formed more properly on the particle surface layer of the water-absorbent resin, and excellent water-absorption capacity can be attained.

[0043]

The temperature in the post-crosslinking reaction is preferably from 50 to 250°C, more preferably from 60 to 180°C, further preferably from 60 to 140°C, and most preferably from 70 to 120°C.

In the present invention, the drying process may be performed under ambient pressure or reduced pressure, or even under nitrogen atmosphere in order to enhance the drying procedure efficiency. When the drying process is performed under ambient pressure, the drying temperature is preferably from 70 to 250°C, more preferably from 80 to 180°C, further preferably from 80 to 140°C, and most preferably from 90 to 130°C. In the case of reduced pressure, the drying temperature is preferably from 60 to 100°C, and more preferably from 70 to 90°C.

The water content of the water-absorbent resin after drying is 20% or less, in view of providing fluidity, and preferably 10% or less in general.

[0044]

5 The median particle size of the water-absorbent resin thus prepared is preferably from 10 to 300 μm , more preferably from 30 to 200 μm , and further preferably from 50 to 150 μm , when the reversed-phase suspension polymerization is performed in one stage. It is not
10 preferred that the median particle size of the water-absorbent resin is 10 μm or less, since dust is generated when the water-absorbent resin is handled, while the median particle size of 300 μm or more is not preferred, since the suspension stability in the polymerization reaction may
15 become low.

[0045]

 The shape of the water-absorbent resin thus prepared varies depending on the kind of surfactant or dispersion medium to be used, but generally is spherical or amorphous
20 with lots of irregularities. It is preferred to apply the method described in the present application to the spherical particles, since it reduces odor originating from the dispersion medium effectively.

25 Examples

[0046]

Next, the present invention will be described in detail below by way of Examples, but the present invention is not limited to the following Examples.

[0047]

5 Example 1

92.0 g of 80% by weight acrylic acid was placed in a 500 mL Erlenmeyer flask, and 102.2 g of 30% by weight sodium hydroxide was added dropwise into the flask while externally cooling the flask thereby performing
10 neutralization. 0.11 g of potassium persulfate, 8.3 mg of ethylene glycol diglycidyl ether and 43.6 g of ion-exchanged water were added thereto to prepare an aqueous solution of water-soluble ethylenically unsaturated monomer.

334 g of *n*-heptane as a petroleum hydrocarbon
15 dispersion medium was placed in a 2 L five-neck cylindrical round bottom flask equipped with a stirrer, reflux condenser and nitrogen gas inlet tube and heated, to which all of the aqueous solution of water-soluble ethylenically unsaturated monomer was added using a funnel, and the
20 mixture was stirred at an internal temperature of 40°C for 10 minutes (step (A)).

[0048]

Next, 0.92 g of sucrose fatty acid ester (Mitsubishi-Kagaku Foods Corp., trade name: S-370) as a surfactant was
25 dissolved in 8.28 g of *n*-heptane under heat, which was placed in the above round bottom flask using a funnel

thereby dispersing the aqueous solution of water-soluble ethylenically unsaturated monomer (step (B)).

[0049]

Then, after the atmosphere inside the system was fully replaced with nitrogen gas while the internal temperature of the round bottom flask containing the above emulsion was retained at 40°C, the round bottom flask was then heated in a water bath at 70°C for 1 hour thereby performing a polymerization reaction (step (C)).

After the polymerization reaction, the reaction product was heated in an oil bath at 120°C, and subjected to azeotropic distillation thereby removing 114 g of water off the system while refluxing *n*-heptane to obtain a dehydrated polymer.

Then, the polymer was heated in the oil bath at 120°C to remove *n*-heptane and water off the system by distillation, and dried under a nitrogen atmosphere to obtain 93 g of a water-absorbent resin. The median particle size was 127 µm, the absorption capacity of physiological saline was 60 g/g, and the water content was 2% in the resultant water-absorbent resin.

[0050]

Example 2

An aqueous solution of water-soluble ethylenically unsaturated monomer was prepared in the same manner as in Example 1.

334 g of *n*-heptane as a petroleum hydrocarbon dispersion medium was placed in a 2 L five-neck cylindrical round bottom flask equipped with a stirrer, reflux condenser and nitrogen gas inlet tube and heated, to which
5 all of above the aqueous solution of water-soluble ethylenically unsaturated monomer was added using a funnel, and the mixture was stirred at an internal temperature of 40°C for 10 minutes (step (A)).

[0051]

10 Next, 0.92 g of sucrose fatty acid ester (Mitsubishi-Kagaku Foods Corp., trade name: S-370) as a surfactant was dissolved in 8.28 g of *n*-heptane under heat, 0.92 g of maleic anhydride modified polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 1105A) as a polymeric dispersion
15 agent was dissolved in 8.28 g of *n*-heptane under heat, and both solutions were added to the above round bottom flask using a funnel thereby dispersing the aqueous solution of water-soluble ethylenically unsaturated monomer (step (B)).

[0052]

20 Then, after the atmosphere inside the system was fully replaced with nitrogen gas while the internal temperature of the round bottom flask containing the above emulsion was retained at 40°C, the round bottom flask was then heated in a water bath at 70°C for 1 hour thereby performing a
25 polymerization reaction (step (C)).

After the polymerization reaction, the reaction

product was heated in an oil bath at 120°C, and subjected to azeotropic distillation thereby removing 114 g of water off the system while refluxing *n*-heptane to obtain a dehydrated polymer. 4.6 g of a 2% aqueous solution of ethylene glycol diglycidyl ether was added to the resultant dehydrated polymer as a post-crosslinking agent, and a post-crosslinking reaction was performed at 80°C for 2 hours.

[0053]

Then, the polymer was heated in the oil bath at 120°C to remove *n*-heptane and water off the system by distillation, and dried under nitrogen atmosphere to obtain 94 g of a water-absorbent resin. The median particle size was 96 µm, the absorption capacity of physiological saline was 54 g/g, and the water content was 3% in the resultant water-absorbent resin.

[0054]

Example 3

92.0 g of 80% by weight acrylic acid was placed in a 500mL Erlenmeyer flask, and 102.2 g of 30% by weight sodium hydroxide was added dropwise into the flask with stirring while externally cooling the flask thereby performing neutralization. 0.11 g of potassium persulfate, 8.3 mg of ethylene glycol diglycidyl ether and 43.6 g of ion-exchanged water were added thereto to prepare an aqueous solution of water-soluble ethylenically unsaturated monomer.

[0055]

334 g of *n*-heptane as a petroleum hydrocarbon dispersion medium, was placed in a 2 L five-neck cylindrical round bottom flask equipped with a stirrer, reflux condenser and nitrogen gas inlet tube, to which 0.92 g of maleic anhydride modified polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 1105A) as a polymeric dispersion agent was added and dissolved under heat, followed by adding all of the aqueous solution of water-soluble ethylenically unsaturated monomer using a funnel, and the mixture was stirred at an internal temperature of 40°C for 10 minutes (step (A)).

[0056]

Next, 0.92 g of sucrose fatty acid ester (Mitsubishi-Kagaku Foods Corp., trade name: S-370) as a surfactant was dissolved in 8.28 g of *n*-heptane under heat, which was added to the above round bottom flask using a funnel thereby dispersing the aqueous solution of water-soluble ethylenically unsaturated monomer (step (B)).

Then, after the atmosphere inside the system was fully replaced with nitrogen gas while the internal temperature of the round bottom flask containing the above emulsion was retained at 40°C, the round bottom flask was then heated in a water bath at 70°C for 1 hour thereby performing a polymerization reaction (step (C)).

[0057]

After the polymerization reaction, 95 g of a water-absorbent resin was obtained in the same manner as in Example 2. The median particle size was 56 μm , the absorption capacity of physiological saline was 55 g/g, and the water content was 3% in the resultant water-absorbent resin.

[0058]

Example 4

94 g of a water-absorbent resin was obtained in the same manner as in Example 3, except for using 0.92 g of oxidized polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 4052E) instead of 0.92 g of maleic anhydride modified polyethylene as a polymeric dispersion agent. The median particle size was 60 μm , the absorption capacity of physiological saline was 56 g/g, and the water content was 2% in the resultant water-absorbent resin.

[0059]

Example 5

96 g of a water-absorbent resin was obtained in the same manner as in Example 3, except for using 0.92 g of oxidized polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 4052E) instead of 0.92 g of maleic anhydride modified polyethylene as a polymeric dispersion agent in the step (A), and adding a solution of 0.92 g of maleic anhydride modified polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 1105A) dissolved in 8.28 g of *n*-heptane under heat,

together with the surfactant, as the polymeric dispersion agent in the step (B). The median particle size was 63 μm , the absorption capacity of physiological saline was 56 g/g, and the water content was 2% in the resultant water-absorbent resin.

[0060]

Example 6

95 g of a water-absorbent resin was obtained in the same manner as in Example 2, except for using a solution of 1.84 g of decaglyceryl pentastearate (Nikko Chemical Co. Ltd., trade name: Decaglyn 5-S) dissolved in 8.28 g of n-heptane under heat as a surfactant instead of 0.92 g of sucrose fatty acid ester in Example 3. The median particle size was 86 μm , the absorption capacity of physiological saline was 55 g/g, and the water content was 2% in the resultant water-absorbent resin.

[0061]

Example 7

92.0 g of 80% by weight acrylic acid was placed in a 500 mL Erlenmeyer flask, and 102.2 g of 30% by weight sodium hydroxide was added dropwise into the flask with stirring while externally cooling the flask thereby performing neutralization. 0.11 g of potassium persulfate, 8.3 mg of N,N'-methylenebisacrylamide and 43.6 g of ion-exchanged water were added thereto to prepare an aqueous solution of water-soluble ethylenically unsaturated monomer.

352 g of cyclohexane as a petroleum hydrocarbon dispersion medium was placed in a 2 L five-neck cylindrical round bottom flask equipped with a stirrer, reflux condenser and nitrogen gas inlet tube, to which 0.92 g of maleic anhydride modified polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 1105A) as a polymeric dispersion agent was added and dissolved under heat, following by adding all of the aqueous solution of water-soluble ethylenically unsaturated monomer using a funnel, and the mixture was stirred at an internal temperature of 40°C for 10 minutes (step (A)).

[0062]

Next, 0.92 g of sucrose fatty acid ester (Mitsubishi-Kagaku Foods Corp., trade name: S-370) as a surfactant was dissolved in 8.28 g of cyclohexane under heat, which was added to the above round bottom flask using a funnel thereby dispersing the aqueous solution of water-soluble ethylenically unsaturated monomer (step (B)).

[0063]

Then, after the atmosphere inside the system was fully replaced with nitrogen gas while the internal temperature of the round bottom flask containing the above emulsion was retained at 40°C, the round bottom flask was then heated in a water bath at 70°C for 1 hour thereby performing a polymerization reaction (step (C)).

[0064]

After the polymerization reaction, the reaction product was heated in an oil bath at 120°C, and subjected to azeotropic distillation thereby removing 114 g of water off the system while refluxing cyclohexane to obtain a
5 dehydrated polymer. 4.6 g of a 2% aqueous solution of ethylene glycol diglycidyl ether as a crosslinking agent was added to the resultant dehydrated polymer, and a crosslinking reaction was performed at 75°C for 2 hours.
[0065]

10 Then, the polymer was heated in the oil bath at 120°C to remove cyclohexane and water off the system by distillation, and dried under nitrogen atmosphere to obtain 97 g of a water-absorbent resin. The median particle size was 103 μm , the absorption capacity of physiological saline
15 was 49 g/g, and the water content was 6% in the resultant water-absorbent resin.
[0066]

Example 8

A polymerization reaction suspension that completed
20 the polymerization reaction up to the step (C) in the same manner as in Example 3 was defined as the polymerization reaction suspension at the first stage, and the temperature was cooled at 25°C.

Separately, 128.8 g of 80% by weight acrylic acid was
25 placed in a 500 mL Erlenmeyer flask, and 142.9 g of 30% by weight sodium hydroxide was added dropwise into the flask

with stirring while externally cooling the flask thereby performing neutralization. 0.15 g of potassium persulfate, 11.6 mg of ethylene glycol diglycidyl ether and 16.7 g of distilled water were added thereto to prepare an aqueous solution of water-soluble ethylenically unsaturated monomer at the second stage.

[0067]

After the aqueous monomer solution at the second stage was added to the above polymerization reaction suspension at the first stage and the atmosphere inside the system was replaced with nitrogen gas, the system was heated in a water bath at 70°C for 1 hour thereby performing the reversed-phase suspension polymerization at the second stage.

After the polymerization reaction, the reaction product was heated in an oil bath at 120°C, and subjected to azeotropic distillation thereby removing 255 g of water off the system while refluxing *n*-heptane in the round bottom flask to obtain a dehydrated polymer. 8.2 g of a 2% aqueous solution of ethylene glycol diglycidyl ether as a crosslinking agent was added to the resultant dehydrated polymer, and the crosslinking reaction was performed at 80°C for 2 hours.

[0068]

Then, the reaction mixture was heated in the oil bath at 120°C to remove *n*-heptane and water off the system by

distillation, and dried under nitrogen atmosphere to obtain 232 g of a water-absorbent resin in a form of agglomerated spherical particles. The median particle size was 335 μm , the absorption capacity of physiological saline was 53 g/g, and the water content was 3% in the resultant water-absorbent resin.

[0069]

Comparative Example 1

92.0 g of 80% by weight acrylic acid was placed in a 500 mL Erlenmeyer flask, and 102.2 g of 30% by weight sodium hydroxide was added dropwise into the flask with stirring while externally cooling the flask thereby performing neutralization. 0.11 g of potassium persulfate, 8.3 mg of ethylene glycol diglycidyl ether and 43.6 g of ion-exchanged water were added thereto to prepare an aqueous solution of water-soluble ethylenically unsaturated monomer.

[0070]

342 g of *n*-heptane as a petroleum hydrocarbon dispersion medium was placed in a 2 L five-neck cylindrical round bottom flask equipped with a stirrer, reflux condenser and nitrogen gas inlet tube, to which 0.92 g of sucrose fatty acid ester (Mitsubishi-Kagaku Foods Corp., trade name: S-370) as a surfactant and 0.92 g of maleic anhydride modified polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 1105A) as a polymeric dispersion agent

were added and dissolved under heat at internal temperature of 80°C, and then all of the above aqueous solution of water-soluble ethylenically unsaturated monomer was added to the dispersion medium in the presence of the surfactant using a funnel, the atmosphere in the system was fully replaced with nitrogen gas while retaining the internal temperature of the round bottom flask containing the above emulsion at 40°C, and the emulsion was heated in a water bath at 70°C for 1 hour to perform a polymerization reaction.

[0071]

After the polymerization reaction, 95 g of a water-absorbent resin was obtained in the same manner as in Example 2. The median particle size was 59 μm , the absorption capacity of physiological saline was 52 g/g, and the water content was 2% in the resultant water-absorbent resin.

[0072]

Comparative Example 2

97 g of a water-absorbent resin was obtained in the same manner as in Comparative Example 1, except for using 1.84 g of decaglyceryl pentastearate (Nikko Chemical Co. Ltd., trade name: Decaglyn 5-S) as a surfactant instead of 0.92 g of sucrose fatty acid ester. The median particle size was 90 μm , the absorption capacity of physiological saline was 52 g/g, and the water content was 3% in the

resultant water-absorbent resin.

[0073]

Comparative Example 3

The water-absorbent resin prepared in the same manner
5 as in Comparative Example 2 was uniformly spread in a
stainless plate, and heated by a hot air drier at 180°C for
3 hours. The median particle size was 89 μm , the
absorption capacity of physiological saline was 55 g/g, and
the water content was 0% in the resultant water-absorbent
10 resin.

[0074]

Comparative Example 4

92.0 g of 80% by weight acrylic acid was placed in a
500 mL Erlenmeyer flask, and 102.2 g of 30% by weight
15 sodium hydroxide was added dropwise into the flask with
stirring while externally cooling the flask thereby
performing neutralization. 0.11 g of potassium persulfate,
8.3 mg of N,N'-methylenebisacrylamide and 43.6 g of ion-
exchanged water were added thereto to prepare an aqueous
20 solution of water-soluble ethylenically unsaturated monomer.

[0075]

360 g of cyclohexane as a petroleum hydrocarbon
dispersion medium was placed in a 2 L five-neck cylindrical
round bottom flask equipped with a stirrer, reflux
25 condenser and nitrogen gas inlet tube, to which 0.92 g of
sucrose fatty acid ester (Mitsubishi-Kagaku Foods Corp.,

trade name: S-370) as a surfactant and 0.92 g of maleic anhydride modified polyethylene (Mitsui Chemicals Inc., trade name: Hiwax 1105A) as a polymeric dispersion agent were added and dissolved under heat, and then all of the above aqueous solution of water-soluble ethylenically unsaturated monomer was added to the dispersion medium in the presence of the surfactant using a funnel, the atmosphere in the system was fully replaced with nitrogen gas while retaining the internal temperature at 40°C, and then the emulsion was heated in a water bath at 70°C for 1 hour thereby performing a polymerization reaction.

[0076]

After the polymerization reaction, 96 g of a water-absorbent resin was obtained in the same manner as in Example 7. The median particle size was 110 μm , the absorption capacity of physiological saline was 48 g/g, and the water content was 7% in the resultant water-absorbent resin.

[0077]

The median particle size, water content and odor sensory test of the water-absorbent resins prepared in the respective Examples and Comparative Examples were evaluated by the methods illustrated below.

[0078]

(Median particle size)

50 g of the water-absorbent resin was sieved with a

JIS standard sieve with a sieve opening of 250 μm . The median particle size was measured using a combination of sieves (A) when 50% by weight or more of the resin passed through the sieve opening, while using a combination of
5 sieves (B) when 50% by weight or more of the resin remained on the sieve.

(A) JIS standard sieves were stacked downward as follows; beginning with a sieve with a sieve opening of 425 μm at the top, followed by a sieve with a sieve opening of
10 250 μm , a sieve with a sieve opening of 180 μm , a sieve with a sieve opening of 150 μm , a sieve with a sieve opening of 106 μm , a sieve with a sieve opening of 75 μm , a sieve with a sieve opening of 45 μm and a tray in order.

(B) JIS standard sieves were stacked downward as
15 follows; beginning with a sieve with a sieve opening of 850 μm at the top, followed by a sieve with a sieve opening of 600 μm , a sieve with a sieve opening of 500 μm , a sieve with a sieve opening of 425 μm , a sieve with a sieve opening of 300 μm , a sieve with a sieve opening of 250 μm ,
20 a sieve with a sieve opening of 150 μm and a tray in order.

About 50 g of the water-absorbent resin was placed on the sieve at the top, and classified for 20 minutes using a low tap-type shaking machine.

[0079]

25 After the sieve classification, the weight of the water-absorbent resin remaining on the respective sieves

was calculated in terms of weight percent based on the total weight of resin, the values were integrated in order from the resins with a smaller particle size, and thereby the relations between the sieve openings and integration values of the weight percentage of the water-absorbent resin remaining on the sieve were plotted on a logarithmic-probability paper. The plots on the probability paper were connected with a straight line, and the particle size corresponding to integrated weight percent of 50% by weight was defined as the median particle size.

[0080]

(Water content)

About 2.5 g of the water-absorbent resin was weighed accurately (Xg), and after drying at 105°C with a hot air drier for 2 hours, the weight of the dried water-absorbent resin was measured (Yg), and then the water content was calculated by the following equation.

$$\text{Water content (\%)} = [(X - Y)/X] \times 100$$

[0081]

(Absorption capacity of physiological saline)

500 g of a 0.9% aqueous solution of sodium chloride was placed in a 500 mL beaker with a 3 cm-long bar and while stirring with a magnetic stirrer, 2.0 g of the water-absorbent resin was weighed accurately (Ag) and added to the beaker such that no unswollen lump is left, and then the mixture was stirred at a rate of 600 rpm for 1 hour.

Gel was filtered out by a JIS standard sieve which is 20 cm in diameter with a sieve opening of 38 μm , excessive water contained in the gel remaining on the sieve was roughly drained with a fluorine resin board, and then the sieve was tilted and left for 30 minutes for further draining. The weight of the gel remaining on the sieve (Bg) was weighed, and the absorption capacity of physiological saline was calculated by the following equation.

Absorption capacity of physiological saline (g/g) = B/A
[0082]
(Odor sensory test)

Odor of the water-absorbent resin originating from the dispersion medium upon swelling was compared by the following method. 20.0 g of 0.9% by mass saline at 25°C was placed in a 140 mL glass bottle with a lid (mayonnaise bottle), and stirred with a 3 cm-long bar. 4.0 g of the water-absorbent resin was added to the glass bottle and tightly sealed. The odor originating from the dispersion medium in the glass bottle was determined by five panelists in accordance with the six-level odor intensity indication method shown below, and evaluated by the mean value.

[0083]

Table 1

Six-level evaluation	Evaluation criteria
5	Very strong odor
4	Strong odor
3	Easily recognized odor
2	Slight odor, odor of what is recognized
1	Very slight odor which is detected with difficulty
0	No odor

[0084]

The odor sensory test results of the water-absorbent resin prepared in Examples 1 to 8 and Comparative Examples 1 to 4 are shown in Table 2.

5 [0085]

Table 2

Sample	Dispersion medium	Median particle size [μm]	Absorption capacity of physiological saline [g/g]	Odor sensory test (Evaluation by panelists)					
				A	B	C	D	E	Average
Example 1	Heptane	127	60	2	2	2	2	1	1.8
Example 2	Heptane	96	54	1	1	1	1	1	1.0
Example 3	Heptane	56	55	1	1	0	0	0	0.4
Example 4	Heptane	60	56	1	0	0	0	0	0.2
Example 5	Heptane	63	56	1	0	0	0	0	0.2
Example 6	Heptane	86	55	1	1	1	1	0	0.8
Example 7	Cyclohexane	103	49	2	2	2	2	1	1.8
Example 8	Heptane	335	53	0	0	0	0	0	0.0
Comparative Example 1	Heptane	59	52	3	3	3	3	3	3.0
Comparative Example 2	Heptane	90	52	3	3	3	3	3	3.0
Comparative Example 3	Heptane	89	55	3	3	3	3	3	3.0
Comparative Example 4	Cyclohexane	110	48	4	4	4	4	4	4.0

As is shown in Table 2, it is obvious that odor originating from the dispersion medium of the water-absorbent resin prepared by the production process of the present invention is lower, in the comparisons among the same kind of dispersion media.

10

CLAIMS

1. A process for production of a water-absorbent resin by
subjecting a water-soluble ethylenically unsaturated
5 monomer to reversed-phase suspension polymerization,
comprising the following steps of:

(A) adding an aqueous solution of water-soluble
ethylenically unsaturated monomer to a petroleum
hydrocarbon dispersion medium to disperse the aqueous
10 solution in the dispersion medium,

(B) adding a surfactant to the emulsion to further disperse
the monomer in the emulsion, and

(C) performing the reversed-phase suspension polymerization
using a water-soluble radical polymerization initiator

15 optionally in the presence of an internal-crosslinking
agent.

2. The process for production of a water-absorbent resin
according to claim 1, wherein the aqueous solution of
20 ethylenically unsaturated monomer is added to and dispersed
in the petroleum hydrocarbon dispersion medium in the
presence of a polymeric dispersion agent in the step (A).

3. The process for production of a water-absorbent resin
25 according to claim 1 or 2, wherein a polymeric dispersion
agent is further added together with the surfactant in the

step (B).

4. The process for production of a water-absorbent resin according to any one of claims 1 to 3, wherein the water-absorbent resin prepared by the steps (A) through (C) is subjected to post-crosslinking using a post-crosslinking agent.

5. The process for production of a water-absorbent resin according to any one of claims 1 to 4, wherein the surfactant is at least one selected from the group consisting of polyglycerin fatty acid ester, sucrose fatty acid ester and sorbitan fatty acid ester.

6. The process for production of a water-absorbent resin according to any one of claims 2 to 5, wherein the polymeric dispersion agent is at least one selected from the group consisting of maleic anhydride modified polyethylene, maleic anhydride modified polypropylene, maleic anhydride modified ethylene-propylene copolymer, maleic anhydride-ethylene copolymer, maleic anhydride-propylene copolymer, maleic anhydride-ethylene-propylene copolymer, polyethylene, polypropylene, ethylene-propylene copolymer, oxidized polyethylene and oxidized polypropylene.

7. The process for production of a water-absorbent resin

according to any one of claims 1 to 6, wherein the water-soluble ethylenically unsaturated monomer is at least one selected from the group consisting of acrylic acid and salts thereof, methacrylic acid and salts thereof, and
5 acrylamide.

8. The process for production of a water-absorbent resin according to any one of claims 1 to 7, wherein the petroleum hydrocarbon dispersion medium is at least one
10 selected from the group consisting of aliphatic hydrocarbons and alicyclic hydrocarbons having 6 to 7 carbon atoms.

9. A water-absorbent resin prepared by the production
15 process according to any one of claims 1 to 8.

PROCESS FOR PRODUCTION OF WATER-ABSORBENT RESIN

ABSTRACT

5 A purpose of the present invention is to reduce
odor of a water-absorbent resin during absorption of
water. Such the invention is attained by a process for
production of a water-absorbent resin by subjecting a
water-soluble ethylenically unsaturated monomer to
10 reversed-phase suspension polymerization. The process
comprises the following steps (A) to (C): (A) adding an
aqueous solution of water-soluble ethylenically
unsaturated monomer to a petroleum hydrocarbon
dispersion medium to disperse the aqueous solution in
15 the dispersion medium; (B) adding a surfactant to the
emulsion to further disperse the emulsion; and (C)
performing the reversed-phase suspension polymerization
using a water-soluble radical polymerization initiator,
optionally in the presence of an internal-crosslinking
20 agent.

(No suitable figure)