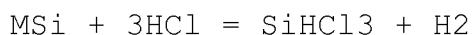


Silicon-based green bodies

The present invention relates to a sol-gel process for the inexpensive and in large quantities agglomeration of silicon particles in a green bodies which are more suitable for industrial uses of silicon than the particles itself.
5 The silicon particles come mostly from the recycling of silicon from semiconductors industry.

Nowadays there is a soaring demand in silicon for several applications but the area that is taking more and more silicon is the photovoltaic application which is growing in western countries at a steady pace. Unlike some high tech area of application the photovoltaic application does not need extremely high impurity meaning that some silicon that is not suitable for some areas of semiconductors industry can be taken by the photovoltaics. Recently the cost of polycrystalline silicon as a raw material has soared dramatically. To date, silicon is the primary photovoltaic material, with single crystal silicon, multi-crystal silicon and amorphous silicon comprising the majority of photovoltaic market. Currently, photovoltaic and electronics-grade silicon are widely produced from hydrogen reduction of trichlorosilane (Siemens process).
20 Trichlorosilane is generally obtained from metallurgical-grade silicon feedstock which has been mined from quartzite. The reaction for the preparation for trichlorosilane is the following:



Yield from this process is around 80-90%; the remaining is mainly made up of SiCl_4 which must be removed. As it is an exothermic procedure it must be cooled otherwise the yield becomes lower. The silicon produced with such process is then treated in order to obtain silicon ingots that are

then cut to produce the silicon panels. It has to be said that most of the times there is a step that concerns the addition of dopants such as boron or phosphorus to produce p-type or -type ingots respectively. With few exceptions, commercial solar cells produced today are based on p-type silicon ingot material. More in detail, the production of silicon ingots goes through a manufacturing step that is called directional solidification, in Norwegian patent application No. 20035830 filed December 29, 2003 it is disclosed a method for producing directionally solidified (Czochralski), float zone or multicrystalline silicon ingots or thin silicon sheets based on a silicon feedstock material produced from metallurgical grade silicon by means of metallurgical refining process, which is conducted by means of a heat-up cycle under vacuum until attaining a temperature greater or equal to 1400°C.

Only for the sake of a complete overview about the use of high purity silicon powder, it is interesting to mention the production of high grade SiO for the making of SiO films for electronic elements or heat reflecting thermal panels as well described in the patent filed by Tuemmler 1982-33176E. Also related to the use of silicon powder it is worth to mention the UK patent GB 2084979 filed by General Elctric it is described a process devised for producing chlorosilanes from silicon powder.

Very few literature has been published to finding reliable process that can allow to use also fine powder in the production of polycrystalline silicon. It is in fact known that the powder is difficult to melt and that can be leads to safety issues if the atmosphere is not completely Oxygen-free. That's why it is obvious for someone skilled in the art the benefits coming from a method that allows the compacting of silicon to be used for the melting to make silicon ingots. In fact, the ultra-fine silicon powder is actually a by-product of many process concerning the

manufacturing and the post-processing of silicon. Examples of processes that have ultra-fine silicon powder that cannot be directly recycled or used in melting applications are: fluid bed process for the making of electronic grade silicon, sawing of silicon bulls or chunks, rework of solar cells, or cutting of silicon wafers or ingots slicing. Interesting also to mention the method reported in the patent WO2008/041261 which is about the manufacturing of high grade silicon powder starting from multiple precursors by means of a transformer coupled plasma reactor. Also worth to report is the patent filed by Elkem A/S in which is described the melting of silicon in a big crucible and the molten silicon becomes the feed for an atomiser using inert gases. The size of the particles can be tailored from 0,1 to 1000 microns.

Most of these processes produce a very fine silicon powder which has to be purified as already described in the patent WO2006/137098. Most of the time these powders are mixed with abrasive dispersions which contains metals and/or silicon carbide particles and suspending agents such as polyethylene glycol. Normally these dispersion are reworked in order to be reused for the same application as described in the following patents: EP-A-786317, ep 0791385, WO01/43933 or US6,010,010. It is almost obvious that would be much more profitable to split the dispersion in its components with a major focus on the silicon part which would be sold to the photovoltaic industry after melting. As already said the fine powder cannot be molten and needs to be converted in a body that can be afterward molten. The universal method of treating fine powder is by addition of organic and inorganic binders to convert the powder to granules and pellets, as they are practised in the ceramic manufacturing as described in the US patent 2006/0040064. In the Japanese patent JP2007022914 is proposed a very original method of compressing e very fine powder (0,1 micron) made of SiC, the method comprises the

pressing of such powder with carbon powder in a predetermined shape; heating the compact to a temperature just beyond the melting point of silicon; and impregnating the compact heated at the temperature beyond the melting point of silicon with molten silicon. Worth also to mention the patent the method proposed in the US patent 7,175,685 where the authors describes the making of silicon ingots starting form silicon pellets and tablets made by tableting agglomerate-free high purity silicon powder without any additives and/or binders. The tableting is performed at room temperature and the density of the pellets is in the range 1.2-1,4 ml/g, the size in within the range of 1-3 grams

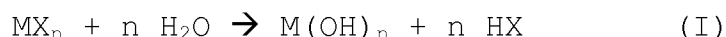
The present invention recognizes that it is possible to recover and recycle silicon powder. The invention proposes a method to compact the powder into "green bodies" that can be used by the smelter for the production of silicon ingots. The method is based on the so called sol-gel technology in fact it concerns the preparation of a solution with silanes in water solution and then the hydrolysis is initiated by setting the more suitable conditions. The hydrolysed solution is then added to the silicon powder that could be dried or dispersed in an organic solvent such as acetone or ethanol. The mixture so prepared is left under stirring till it is homogeneous and at this point it is poured into the molds for the preparation of the "green body". The said molds can be a crucible made of silica as those supplied by Cerandyne corp. or Vesuvium as mold can also be used any hollow objects suitable for the briquetting. The mixture in the molds is then left for consolidation of the matrix for at least 6 hours.

Without wishing to be bound to theory the authors think that in said period the so-called syneresis occurs which allows the formation of a network that is needed for

providing to the said green body the needed stiffness and prevent any formation of fines.

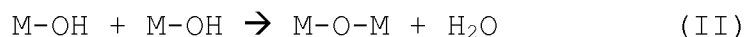
Before to go into the details of the invention the inventors would like to give some insights on the sol-gel technology. By the name "sol-gel" it is meant a broad range of techniques for the production of dry gels and green bodies. Contrary to traditional techniques, sol-gel processes start from solutions of precursors of the desired materials and avoid passing through melting operations or any briquetting or tableting technique. Although the technique allows for a broad range of modifications, all sol-gel processes have in common the following phases:

- production of a aqueous or hydro-alcoholic solution or, more frequently, of a suspension, of at least a compound MX_n , generally defined as precursor, containing a cation M at least three-valent and preferably tetra-valent, whose glassy oxide formation is desired;
- hydrolysis, that might be catalysed by acids or bases, of the precursor (or precursors) in the solution or suspension, with formation of M-OH groups, as shown in the reaction:



The thus obtained mixture, that may be a solution or a colloidal suspension, is defined as sol;

- polycondensation of M-OH groups according to the reaction:



with formation of an oxydic polymer, defined gel, that takes the whole volume originally occupied by the solution.

This phase is defined gelation;

- drying of the gel obtaining a dry gel formed of a porous monolithic body, having apparent density (weight divided by the geometric volume of the monolithic body) comprised between about 1/20 and 1/3 of the theoretical density of the corresponding non-porous oxide; drying
5 may be realized by controlled evaporation of the solvent, obtaining a body defined in the field as "xerogel", or by supercritical extraction of the solvent, obtaining a so-called "aerogel"; as given
10 above, the dry gel may find industrial applications as such, or it can be submitted to densification by thermal treatment, obtaining a glassy body of theoretical density.

The invention will be further illustrated by the following
15 examples. These non-limitative examples illustrate some embodiments meant to teach to the experts in the field how to practice the invention and to represent the best mode contemplated for realization of the invention.

20 **EXAMPLE 1**

0.7 g of tetramethoxysilane are mixed with 5 g ethanol and 1 g water and the solution so obtained is kept under stirring until complete hydrolysis of tetramethoxysilane occurs (solution becomes completely transparent). Then 14
25 g of silicon powder are added to the silane-based premix (weight ratio 1:0,49) and kept under stirring. The sludge so obtained is then poured in the mold. The whole process is conducted under nitrogen. Before the start of the drying phase the sample is kept in a sealed container at room
30 temperature for the consolidation of the green body. Silicon body is then dried under ventilated hood for 3 days. The product has been characterized by means of XRD spectroscopy that has shown that the content of SiO₂ in the

silicon product raised only of 0.5wt% because of the described treatment.

EXAMPLE 2

5 1,4 g of silica (Aerosil ox 50 supplied by Evonik industries) are mixed with 2 g water and the solution so obtained is kept under stirring until for one hour. Then 14 g of silicon powder are added to the silane-based premix (weight ratio 1:0,49) and kept under stirring. The sludge
10 so obtained is then poured in the mold. The whole process is conducted under nitrogen. Before the start of the drying phase the sample is kept in a sealed container at room temperature for the consolidation of the green body. Silicon body is then dried under ventilated hood for 3
15 days. The product has been characterized by means of XRD spectroscopy that has shown that the content of SiO₂ in the silicon product raised only of 0.9wt% because of the described treatment

As already said as feedstock could be used silicon recovered
20 from cutting, slicing and sawing of silicon wafer (among the others). Herewith is reported a non-limitative example which illustrates some embodiments meant to teach to the experts in the field how to practice the invention and to represent the best mode contemplated for realization of the
25 invention.

EXAMPLE 3

Silicon powder is could be either as cake from filtration or sludges from centrifugal treatment or as dry powder; the first step is the re-slurry operation which is made by
30 addition of deionised water and hydrochloric acid; the ratios among the chemicals. Water is added in such a quantity to adjust the density of the slurry
The slurry is then added in a reactor with hydrofluoric acid. After the treatment the slurry is sent to filtration

and the resulting silicon cake is washed with water, re-slurried with water adjusting the density.

The slurry is then mixed with hydrochloric acid and with hydrogen peroxide; water is adjusted to control the density
5 of the slurry. After the treatment the slurry is filtrated and the filtration cake is washed with water; liquids from filtration and washing containing HCl and H₂O₂, are sent to a neutralization tank the final step is the hydrofluoric acid and with hydrogen peroxide in such a quantity to
10 obtain the following ratios by weight. After the treatment the slurry is filtrated and washed with water. After filtration the product is washed again with HF and then with ethanol.

CLAIMS

1. Sol-gel process for the agglomeration of silicon powder.
- 5 2. The process is based on the following steps:
 - preparing a solution of alkoxide precursor and /or silica, water and solvent
 - mixing the solution to silicon particles
 - keep the said dispersion under stirring
 - 10 - drying of the dispersion till the formation of a dried green body.
3. Process according to claim 1 wherein the alkoxide precursor has the formula $X-ME(OR)_{n-1}$ in which Me is a metal belonging to the 3rd, 4th and 5th groups; more
15 preferably to the 4th group, especially is silicon, n is integer and represents the valence of Me; X is either OR or R where -OR is an alkoxide group and -R is an organic radical linear or branched with a number of carbon atoms up to 10.
- 20 4. Process according to claim 1 wherein the alkoxide precursor where the alkoxide precursor could be tetramethoxysilane and/or tetraethoxysilane and/or Methyltriethoxysilane.
5. Process according to claim 1 wherein the silica is
25 fumed silica
6. process according to claim 1 wherein the silica is colloidal silica
7. Process according to claim 2 wherein said solution is a solution containing from 1% to 50% by weight of

alkoxide precursor and more preferably from 2% to 18%, especially from 3% to 10%, more especially from 7% to 11%.

- 5 8. Process according to claim 2 wherein said solution is a solution containing from 1% to 50% by weight of silica and more preferably from 2% to 18%, especially from 3% to 10%, more especially from 7% to 11%.
- 10 9. Process according to claim 1 wherein the solvent is an alcohol and/or a ether and/or a ketone or a mixture of thereof.
- 10 10. Process according to claim 9 wherein the organic solvent could contain water
- 15 11. Process according to claim 1 wherein the molar ration silicon/alkoxide precursor is in the range from 10 to 150 and more preferably from 80 to 120.
12. Process according to claim 1 wherein the molar ration silicon/alkoxide precursor is in the range from 1 to 150 and more preferably from 20 to 120.
- 20 13. Process according to claim 1 wherein the silicon particles can be dried
14. Process according to claim 1 wherein the silicon particles can be wet with organic solvent
- 25 15. Process according to claim 10 wherein the water content is between 0.1% wt and 20%, more preferably from 1% to 10%, especially from 1% to 6%, more especially from 3% to 5.5%.
16. process according to claim 1 wherein before the drying the mixture is kept in the consolidation phase without solvent evaporation

17. process according to claim 1 wherein the drying is carried out at a temperature that is in the range 20 to 230°C.
18. Process according to claim 1 wherein the mixture is
5 poured in a mold.
19. A process according to any one of the claims 1-19 wherein the green bodies produced with said process are for use in photovoltaic application.