CLAIMS:

1. A method for making lubricant base stock, comprising:

performing solvent deasphalting using a C_4 or C_5 solvent under effective solvent deasphalting conditions on a feedstock having a T5 boiling point of at least 370°C, the effective solvent deasphalting conditions producing a yield of deasphalted oil of at least 50 wt% of the feedstock;

hydroprocessing at least a portion of the deasphalted oil under first effective hydroprocessing conditions to form a hydroprocessed effluent having a sulfur content of 100 wppm or less and a nitrogen content of 100 wppm or less, the at least a portion of the deasphalted oil having an aromatics content of at least 50 wt%;

separating the hydroprocessed effluent to form at least a fuels boiling range fraction and a bottoms fraction; and

hydroprocessing at least a portion of the hydroprocessed bottoms fraction under second effective hydroprocessing conditions, the second effective hydroprocessing conditions comprising catalytic dewaxing conditions, to form a catalytically dewaxed effluent; and

solvent extracting at least a portion of the catalytically dewaxed effluent to form a solvent processed effluent,

wherein the solvent processed effluent comprises a 950°F+ (510°C+) portion having a VI of at least 80, a pour point of -6°C or less, a cloud point of -2°C or less, and an aromatic content of less than 10 wt%.

2. The method of claim 1, wherein the solvent extracting comprises solvent extracting with n-methylpyrrolidone, furfural, or a combination thereof.

3. The method of any of the above claims, wherein hydroprocessing at least a portion of the hydroprocessed bottoms fraction under second effective hydroprocessing conditions comprises hydrocracking the at least a portion of the hydroprocessed bottoms fraction under hydrocracking conditions to form a hydrocracked effluent, and catalytically dewaxing at least a portion of the hydrocracked effluent under the catalytic dewaxing conditions to form a second hydroprocessing effluent comprising the catalytically dewaxed effluent.

4. The method of claim 3, wherein hydroprocessing at least a portion of the hydroprocessed bottoms fraction under second effective hydroprocessing conditions further comprises performing aromatic saturation on the catalytically dewaxed effluent prior to the at least one of solvent extracting and solvent dewaxing.

5. The method of any of the above claims, wherein at least a portion of the catalytically dewaxed effluent is solvent dewaxed, the first effective hydroprocessing conditions comprising conditions for conversion of 10 wt% to 40 wt% of the deasphalted oil relative to a conversion temperature of 510°C, the catalytically dewaxed effluent having a wax content of at least 6 wt%, the solvent processed effluent having a wax content of at least 4 wt%.

6. The method of any of the above claims, wherein the 950°F+ (510°C+) portion has a pour point of -10°C or less; or wherein the 950°F+ (510°C+) portion has a cloud point of -10°C or less; or a combination thereof.

7. The method of any of the above claims, wherein the solvent processed effluent or the solvent dewaxed effluent has a pour point of -10°C or less; or wherein the solvent processed effluent or the solvent dewaxed effluent has a cloud point of -5°C or less; or a combination thereof.

8. The method of any of the above claims, wherein the 950°F+ (510°C+) portion has a difference between a cloud point temperature and a pour point temperature of 15°C or less.

9. The method of any of the above claims, wherein the solvent processed effluent or the solvent dewaxed effluent has a VI of at least 90, or wherein the 950°F+ (510°C+) portion has a VI of at least 90, or a combination thereof.

10. The method of any of the above claims, wherein hydroprocessing at least a portion of the deasphalted oil comprises hydrotreating the at least a portion of the deasphalted oil, hydrocracking the at least a portion of the deasphalted oil, or a combination thereof.

11. The method of any of the above claims, wherein the yield of deasphalted oil is at least 55 wt%, or wherein the C_{4+} solvent comprises a mixture of two or more C_5 isomers, or wherein performing solvent deasphalting comprises a deasphalting temperature of less than 190°C, or a combination thereof.

12. The method of any of the above claims, further comprising adding 0.1 wt% to 2.5 wt% of an additive to solvent processed effluent, the additive comprising a Group I bright stock, an alkylated naphthalene, or a combination thereof.

13. The method of any of the above claims, wherein the deasphalted oil has an aromatics content of at least 55 wt% based on a weight of the deasphalted oil.

14. The method of any of the above claims, wherein in addition to solvent extracting the at least a potion of the catalytically dewaxed effluent, method comprises solvent dewaxing at least a portion of the catalytically dewaxed effluent to form a second solvent processed effluent, wherein the catalytically dewaxed effluent is underdewaxed.