CLAIMS

1. A method for purifying lipid material, said method comprising the steps of
   i) providing a lipid material feed (a),

   ii) preparing a mixture (b) by mixing feed (a) with an alkali,

   iii) heat-treating the mixture (b) at a temperature of at least 200 °C, such as from 200 to 300 °C,

   iv) phase-separating a heat-treated mixture from step (iii) to obtain a heat-treated purified lipid material (c) and a reject containing inorganic chlorine,

   v) optionally subjecting the heat-treated purified lipid material (c) to a treatment at acidic conditions to obtain a further purified lipid material (d),

   vi) recovering the heat-treated purified lipid material (c) from treatment of step iv) and/or the further purified lipid material (d) from treatment of step v).

2. The method according to claim 1, wherein said alkali in step (ii) is selected from NaOH, KOH, LiOH or a combination thereof.

3. The method according to any one of the preceding claims, wherein the alkali in step (ii) is provided as an aqueous solution.

4. The method according to any one of the preceding claims, wherein the heat-treating step iii) is carried out at a pressure of 100 - 5100 kPa(a), 150 - 5100 kPa(a), 200 - 600 kPa(a), or 300 - 500 kPa(a), and/or wherein the step iii) has a residence time at said conditions from 5 to 120 minutes.

5. The method according to any one of the preceding claims, wherein the phase-separation of the heat-treated mixture in step iv) is preceded by evaporation under conditions capable of removing water from said heat-treated mixture, wherein said evaporation conditions preferably comprise at least one of temperature from 80-130 °C and pressure from 1-100 kPa(a).

6. The method according to any one of the preceding claims, wherein the lipid material feed (a) contains no more than about 2 wt-% water, generally no more than about 1 wt-% water, such as from 0.1 to 1 wt-% water.

7. The method according to any one of the preceding claims, wherein the lipid material feed (a) is subjected to removal of solid impurities prior to step ii).

8. The method according to any one of the preceding claims, wherein the treatment at acidic conditions in step v) is selected from bleaching and degumming.

9. The method according to any one of the preceding claims, wherein the feed comprises at least one feed selected from used cooking oil (UCO), brown grease (BG), and combinations thereof.

10. The method according to any of the preceding claims, wherein the phase-separating means in step iv) comprises filtration, centrifugation, settling or any combination thereof.

11. The method according to any of the preceding claims, wherein the heat-treated purified lipid material (c) and/or the further purified lipid material (d) contains at least about 10 wt-%, preferably at least about 20 wt-%, more preferably at least about 25 wt-%, most preferably at least about 60 wt-%, less chlorine calculated as elemental chlorine than the lipid feed material (a).

12. The method according to any of the preceding claims, wherein the heat-treated purified lipid material (c) and/or the further purified lipid material (d) is further subjected to a post-treatment comprising hydroprocessing.

13. Use of the heat-treated purified lipid material (c) or the further purified lipid material (d) obtained from the method according to any of the claims 1-12 as a feed to at least one hydroprocessing, preferably to catalytic hydroprocessing to obtain renewable hydrocarbons.

14. The use according to claim 13 wherein a co-feed of fossil origin is fed to the hydroprocessing, preferably to catalytic hydroprocessing.

15. The use according to claim 14, wherein the catalytic hydroprocessing comprises one or more of hydrodeoxygenation, hydroisomerisation, hydrocracking, hydrodenitrogenation, hydrodesulfurisation, hydrodehalogenation, hydrodearomatisation or hydrogenation of double bonds.