

Description

The present invention relates to a method for melting glass, in particular, to the first stage of melting, i.e. rendering batch materials to a liquefied state. The invention is applicable to all types of glass melting, including flat glass, container glass, fiber glass and sodium silicate glass.

Continuous glass melting processes conventionally entail depositing pulverulent batch materials onto a pool of molten glass maintained within a tank type melting furnace and applying thermal energy until the pulverulent materials are melted into the pool of molten glass.

The conventional tank type glass melting furnace possesses a number of deficiencies. A basic deficiency is that several operations, not all of which are compatible with one another, are carried out simultaneously within the same chamber. Thus, the melter chamber of a conventional furnace is expected to liquefy the glass batch, to dissolve grains of the batch, to homogenize the melt, and to refine the glass by freeing it of gaseous inclusions. Because these various operations are taking place simultaneously within the melter, and because different components of the glass batch possess different melting temperatures, it is not surprising that inhomogeneities exist from point to point within the melter.

In order to combat these inhomogeneities, a melting tank conventionally contains a relatively large volume of molten glass so as to provide sufficient residence time for currents in the molten glass to effect some degree of homogenization before the glass is discharged to a forming operation. These recirculating flows in a tank type melter result in inefficient use of thermal energy and maintaining the large volume of molten glass itself presents difficulties, including the need to heat such a large chamber and the need to construct and maintain such a large chamber made of costly and, in some cases, difficult to obtain refractory materials. Moreover, corrosion of the refractories introduces contaminants into the glass and requires rebuilding of the melter in a matter of a few years. Additionally, it is known that some components of the batch such as limestone, tend to melt out earlier than the sand and sink into the melt as globules, whereas higher melting temperature components, such as silica, tend to form a residual unmelted scum on the surface of the melt. This segregation of batch components further aggravates the problem of inhomogeneities.

Recent findings have indicated that a major rate limiting step of the melting process is the rate at which partly melted liquefied batch runs off the batch pile to expose underlying portions of the batch to the heat of the furnace. The conventional practice of floating a layer of batch on a pool of molten glass is not particularly conducive to aiding the runoff rate, due in part to the fact that the batch is partially immersed in the molten

glass. It has also been found that radiant energy is considerably more effective at inducing runoff than is convective heat from the pool of molten glass, but in a conventional melter, only one side of the batch is exposed to overhead radiant heat sources. Similarly, conventional overhead radiant heating is inefficient in that only a portion of its radiant energy is directed downwardly towards the material being melted. Not only is considerable energy wasted through the superstructure of the furnace, but the resulting thermal degradation of the refractory roof components constitutes a major constraint on the operation of many glass melting furnaces. Furthermore, attempting to heat a relatively deep recirculating mass of glass from above inherently produces thermal inhomogeneities which can carry over into the forming process and affect the quality of the glass products being produced.

Many proposals have been made for overcoming some of the problems of the conventional tank type glass melting furnace, but none has found significant acceptance since each proposal has major difficulties in its implementation. It has been proposed, for example, that glass batch be liquefied on a ramp-like structure down which the glass liquid would flow into a melting tank (e.g., US-A-296,227; 708,309; 2,593,197; 4,062,667; and 4,110,097). The intense heat and severely corrosive conditions to which such a ramp would be subjected has rendered such an approach impractical since available materials have an unreasonably short life in such an application. In some cases, it is suggested that such a ramp be cooled in order to extend its life, but cooling would extract a substantial amount of heat from the melting process and would diminish the thermal efficiency of the process. Also, the relatively large area of contact between the ramp and each unit volume of glass throughput would be a concern with regard to the amount of contaminants that may be picked up by glass. Furthermore, in the ramp approach, a transfer from a radiant source to the melting batch materials is in one direction only.

A variation on a ramp type melter is shown in US-A-2,451,582 where glass batch materials are dispersed in a flame and land on an inclined ramp. As in other such arrangements, the ramp in the patented arrangement would suffer from severe erosion and glass contamination.

The prior art has also suggested melting glass in rotating vessels where the melting material would be spread in a thin layer on the interior surface of the vessel and would, more or less, surround the heat source (e.g., US-A-1,889,509; 1,889,511; 2,006,947; 2,007,755; 4,061,487; and 4,185,984). As in the ramp proposals, the prior art rotary melters possess a severe materials durability problem and an undesirably large surface contact area per unit volume of glass throughput. In those embodiments where the rotating vessel is insulated, the severe conditions at the glass contact surface would indicate a short life for even the most

costly refractory materials and a substantial contamination of the glass throughput. In those embodiments where the vessel is cooled on the exterior surface, heat transfer through the vessel would subtract substantial amounts of thermal energy from the melting process, which would adversely affect the efficiency of the process. In a rotary melter arrangement shown in US—A—2,834,157 coolers are interposed between the melting material and the refractory vessel in order to preserve the refractories, and it is apparent that great thermal losses would be experienced in such an arrangement. In cyclone type melters, as shown in US—A—3,077,094 and 3,510,289, rotary motion is imparted to the glass batch materials by gaseous means as the vessel remains stationary, but the cyclone arrangements possess all the disadvantages of the rotary melters noted above.

Some prior art processes conserve thermal energy and avoid refractory contact by melting from the interior of a mass of glass batch outwardly, including US—A—1,082,195; 1,621,446; 3,109,045; 3,151,964; 3,328,149; and 3,689,679. Each of these proposals requires the use of electric heating and the initial liquefaction of the batch materials depends upon convective or conductive heating through the mass of previously melted glass. This is disadvantageous because radiant heating has been found to be more effective for the initial liquefaction step. Additionally, only the last two patents listed disclose continuous melting processes. In a similar arrangement disclosed in US—A—3,637,365, one embodiment is disclosed wherein a combustion heat source may be employed to melt a preformed mass of glass batch from the center outwardly, but it, too, is a batchwise process and requires the melting be terminated before the mass of glass batch is melted through.

US—A—3,526,492 refers to a glass pre-melter comprising a furnace constructed primarily of refractory material defining a combustion chamber to which glass ingredients are supplied onto an island within this chamber supporting the batch. On this island a pile of glass formula particles is provided and the surface of the pile will be continually swept by a flame and the material composing the pile melt primarily from its external surface.

US—A—3,917,479 shows a melting apparatus comprising a rotating vessel having an outlet opening for the molten product at its lower end. The material is heated within a cavity encircled by the side walls of the lined vessel. The centrifugal force of the rotating vessel is sufficiently high to maintain a film of the melted material on the surface of the lining. The liquid material will be completely melted when leaving the exit orifice. Since the molten material is retained as film in the vessel, its temperature continues to increase after it has become liquefied by exposure to the thermal energy within the vessel and therefore external cooling means must be provided to prevent the lining from being eroded.

It is the object of the invention to provide an

improved method of liquefying glass batches avoiding the disadvantages of the known methods described before.

This object is attained by a method of liquefying glass batch material by feeding the fusible material to an upper inlet portion of a heating vessel having side walls encircling a heated cavity, providing a lining on the interior of the side walls, heating the cavity to liquefy a layer of the material which flows on the lining to an outlet at the lower portion of the vessel and feeding the material onto the lining at a rate corresponding to the rate of drainage, characterized by providing as a substantial portion of the lining a layer of substantially the same glass batch material and maintaining at least a portion of the thickness of the layer unliquefied substantially by permitting liquefied material to drain freely from the vessel while the liquefied material contains incompletely melted portions of the batch.

A preferred embodiment of said method of liquefying is characterized in that the liquefied batch flows out of the liquefaction zone before its temperature exceeds 1260°C (2300°F).

In the present invention the initial process of liquefying batch material is isolated from the remainder of the melting process and is carried out in a manner uniquely suited to the needs of the particular step, thereby permitting the liquefaction step to be carried out with considerable economies in energy consumption and equipment size and cost. Central to the invention is the concept of employing glass batch itself as the support surface upon which liquefaction of glass batch takes place. It has been found that a steady state condition may be maintained in a liquefaction chamber by distributing fresh batch onto a previously deposited batch surface at essentially the same rate at which the batch is melting, whereby a substantially stable batch layer will be maintained beneath a transient batch layer, and liquefaction is essentially confined to the transient layer. Thus, the partially melted batch of the transient zone runs off the surface while contacting substantially only a batch surface, thus avoiding contaminating contact with refractories. Because glass batch is a good heat insulator, providing the stable batch layer with sufficient thickness protects any underlying support structure from thermal deterioration. Because the exterior of a furnace can thus be protected thermally, as well as from contact with corrosive molten materials, the materials requirements can be greatly relaxed, even permitting the use of mild steel as a furnace housing. The economies thus achieved in furnace construction can be substantial. Furthermore, because the furnace housing is protected by the insulating effect of the stable batch layer, no cooling of the support surface is required, thereby avoiding extraction of useful heat from the melting process.

In a preferred embodiment of the method a stable mass of glass batch is provided resting on a rigid support with a surface sloping downwardly toward an edge thereof, and providing a

transient layer on said surface of the stable glass batch and feeding additional glass batch to the transient layer. The stable mass of glass batch has a thickness of at least 3 cm.

The slope may be the natural angle of repose of the glass batch, or the angle may be increased by providing a preformed batch layer or by centrifugal force in a rotating furnace vessel. The runoff surface is preferably free from obstacles to flow so as to permit free drainage of the liquid out of the liquefaction zone into a subsequent zone where additional melting operations may be performed on the liquid. The liquid leaving the liquefaction zone is by no means a completely melted glass, but is a foamy, opaque fluid including unmelted sand grains and the like. However, it has been found that the additional energy required to complete the dissolution and refining of this runoff liquid constitutes a very small portion of the total energy required to melt glass in a conventional tank type melting operation. Thus, the relatively efficient liquefaction process of the present invention replaces a major energy consuming portion of the conventional melting process. Additionally, it has been found that the runoff liquid is surprisingly uniform in temperature and composition, and therefore each increment of the liquid has essentially identical needs for subsequent processing. This minimizes the need for subsequent homogenization and permits precisely tailoring the subsequent process steps to the specific needs for converting the runoff liquid to molten glass finished to the degree required for the product being produced.

Liquefaction of the batch is brought on by melting of the lowest-temperature-melting components of the batch. Thus, the liquid begins to flow out of the liquefaction zone at a temperature considerably below the temperature required for complete melting of glass, thereby advantageously limiting the function of the liquefaction zone to the unit operation of liquefying the batch. Essentially no increment of the liquefied batch is heated in the zone to a temperature substantially above that corresponding to the onset of flowability. As a result, the fluid leaves the zone at a relatively low, uniform temperature, and the cavity temperature within the liquefaction zone also remains relatively low. This has advantages for the construction of the liquefaction chamber and for reducing heat losses therefrom. The ability to accomplish a major step in the melting process without wastefully overheating some increments of the melt also has positive implications for energy conservation and for suppressing volatilization of some relatively volatile components that are sometimes included in the batch (e.g., sulfur and selenium).

In the embodiments of the invention, the thermal efficiency of the liquefaction process is further increased by providing a stable batch layer that substantially encircles a radiant heat source. Typically the batch surface may constitute a surface of revolution (e.g., a cylinder or

frustum). In this manner, radiant energy being emitted by the source will impinge directly upon batch being melted over a wide range of angles. Such an arrangement also permits an efficient use of high temperature heat sources, such as oxygen enriched flames, since much of the enhanced heat flux from such a source will productively impinge upon the surrounding batch surface. In the most preferred embodiments, the concept of encircling the heat source is combined with rotating the batch surface so as to increase the angle of repose.

The present invention may also be employed to improve the emissions of a glass melting furnace. Sulfates included in many glass batch formulas are known to contribute significantly to undesirable emissions from glass furnaces. A major purpose for including sulfates in a glass batch is to aid the initial liquefaction process in a conventional tank melter. But since the present invention is specifically adapted to liquefying glass batch, it has been found that efficient liquefaction can be achieved without the presence of sulfates in the batch. Thus, the present invention permits omitting sulfates from the batch, thereby eliminating the resultant emissions.

It has also been found that wetting the batch with water as is conventionally done in order to control dusting is not necessary with the present invention. Since vaporizing the water consumes energy in a melter, elimination of the water improves the energy efficiency. Even more significantly, the ability to use dry batch means that preheated batch may be fed to the process. If the batch is preheated by heat recovery from the exhaust gas stream, substantial energy savings can be attained. It is an advantage of the present invention that the process can accommodate preheated, dry, particulate batch, whereas prior art proposals to recover waste heat by preheating batch have usually been tied to the use of agglomerated batch. It has been found generally that the cost of agglomerating batch on a commercial scale virtually negates the potential energy savings.

The method of the invention is practiced in an apparatus which is characterized in that the support for the stable glass batch mass is a metallic vessel thermally protected from the heat within the liquefaction zone by the stable glass batch mass. The metallic vessel is a rotatable drum and the axis of said drum is substantially vertical.

Liquefying batch in accordance with the present invention can be carried out in a relatively compact vessel rather than the conventional tank type melter which contains a pool of molten glass. Reducing the size saves substantial construction costs. Also, by eliminating the need for a large residual pool of glass, product changeovers are facilitated by the present invention.

The invention will be more fully understood in view of the detailed description of several specific embodiments which follows.

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The drawings

Fig. 1 is a vertical cross-section through an embodiment of the present invention featuring a frusto-conical batch surface encircling a heat source.

Fig. 2 is a vertical cross-section of another embodiment of the present invention wherein an inclined rotary kiln provides a cylindrical batch surface.

Fig. 3 is a vertical cross-section of a preferred embodiment of the present invention wherein a drum rotating about a vertical axis of rotation provides a batch surface which is a paraboloid surface of rotation about a heat source.

Fig. 4 is a vertical cross-section of a schematic representation of a combustion melting furnace adapted to cooperate with the batch liquefier of the embodiment of Fig. 3.

Fig. 5 is a vertical cross-section of a schematic representation of an electric melting furnace adapted to cooperate with the batch liquefier of the embodiment of Fig. 3.

Detailed description of the embodiments

Since the invention relates to the initial step of liquefying glass batch, the descriptions of the embodiments will be limited to what would be only the initial portion of most glass melting operations. It should be understood that where the product requires, the inventive liquefaction step may be employed in combination with conventional means for further melting, refining, conditioning and forming the glass.

The embodiment of Fig. 1 has the feature wherein the batch layer encircles the radiant heat source. Such an arrangement advantageously results in a greater portion of the radiant energy productively impinging upon the batch material and permits greater utilization of the insulative effect of the batch layer. Because the heat source is encircled by the insulating batch layer, refractory materials need not be employed for the sidewalls of the housing in the Fig. 1 embodiment. Thus, the housing may comprise a steel vessel 50 which may be provided with a frusto-conical shape as illustrated, which may be generally parallel to the interior surface of the batch layer. However, the sloped surface of the batch layer need not correspond to the shape of the housing, and the housing may take any form such as a cylindrical or box shape. A cover 51 of ceramic refractory material may be provided to enclose the upper end of the liquefaction vessel. Batch 52 may be fed from a ring-type vibratory feeder 53 through an annular opening 54 in the cover 51 so that the batch enters the upper end of the vessel substantially evenly distributed around its upper periphery. A sloping, stable batch layer 55 lines the sides of the interior of the liquefaction vessel and may be comprised of loose batch or a preformed, molded lining. As shown in the drawing, the surface of the batch layer facing the heat source is preferably a surface of rotation, in this case a frusto-conical shape parallel to the shape of the housing 50. Paraboloid and cylindrical

surfaces may also be employed. However, it should be understood that while surfaces of revolution are preferred for the shape of the batch layer for the sake of receiving uniform heat from a central heat source, other non-revolutionary shapes may be employed, such as inverted pyramidal or tetrahedral shapes. It may be also noted that the batch layer need not be of uniform thickness as long as the minimum thickness is sufficient to provide the desired degree of insulation. Because of the excellent insulating properties of glass batch, a stable batch layer whose minimum thickness is on the order of about 3 centimeters to 5 centimeters, has been found more than adequate to protect a steel housing from undue thermal deterioration. A refractory ceramic bushing 56 at the bottom of the liquefaction chamber helps to retain the batch layer 55 in place, and a central opening 57 in the bushing defines an exit opening from the liquefaction chamber. A source of radiant energy, such as a burner 58 provides heat within the liquefaction zone for melting the batch being fed into the chamber which forms the transient layer 59. The transient layer 59 becomes fluid and flows downwardly through the exit opening 57. The liquefied batch may be captured in a pool 60 contained by a chamber 61 for subsequent processing. Combustion gases from the liquefaction zone may also pass through the opening 57, whereupon they may be discharged from the chamber 61 through a flue 62. Alternatively, an exhaust opening may be provided through the cover 51. Fig. 1 shows a single heat source 58 centrally located on the axis of the liquefaction zone but it should be understood that a plurality of heat sources could be provided with oblique orientations.

Referring now to Fig. 2, there is shown an embodiment featuring a rotary liquefaction zone. High thermal efficiency is provided by encircling the heat source with the batch material being melted, and the transient batch layer being melted is distributed within the vessel by means of its rotation. The rotating vessel comprises an inclined steel cylinder 65 which may be rotated by way of a motor 66. Loose glass batch may be fed to the upper open end of the cylinder by means of a screw feeder 67. Before the vessel is heated, an insulating layer of batch 68 is built up within the vessel. During operating, the rate of feeding the batch and the rate of heating are balanced against one another so that the layer 68 remains stable and serves as the surface upon which newly fed batch is melted and runs toward the lower end of the cylinder. A radiant heat source such as a combustion burner 69 may be oriented along the axis of the cylinder from either end of the cylinder. As shown in Fig. 2, the burner 69 is mounted in a refractory housing 70 which closes the lower end of the cylinder 65. The combustion gases pass axially through the cylinder and escape through the upper end into an exhaust box 71 which encompasses the upper end of the cylinder. Exhaust gases may be passed from the box 71 to a stack 72. The lower end of the rotating

cylinder may be provided with a refractory ceramic bushing 73 suitable for molten glass contact. A gap 74 between the burner housing 70 and the bottom inside edge of the cylinder is provided for escape of the liquefied batch 75 which may fall into a collecting pool 76 contained by a chamber 77 where the molten material may be subjected to subsequent processing. The angle of incline of the rotating cylinder will be determined by the rate at which it is desired for the liquefied batch to run out of the cylinder. The cylinder should rotate at a speed at which loose batch is held against the inside walls by centrifugal force. The minimum speed will depend upon the effective diameter of the cylinder. The following are calculated estimates:

Diameter	Revolutions per minute
0.5 Meters	60
1.0 Meters	43
2.0 Meters	37

The preferred embodiment is shown in Fig. 3 and is characterized by a liquefaction chamber rotating about the vertical axis, with glass batch encircling a central heat source. The rotary melter 80 of this embodiment includes a housing comprising a steel cylinder 81 and a steel floor 82. The housing is provided with vertical support by a plurality of rollers 83 which are affixed to a frame 84. A plurality of side rollers 85 maintain alignment of the housing. Rotation of the housing may be provided, for example, by driving one of the rollers 83 or 85 by motor means (not shown). A central opening in the floor 82 is provided with a refractory ceramic bushing 86 suitable for molten glass contact and having a central opening 87. Any suitable structure may be provided for supporting frame 84 but for purposes to be described hereinafter, it is preferred to make the entire liquefaction structure 80 relatively portable. Therefore, overhead hoist means may engage attachment means 88 affixed to upper portions of the frame 84. The upper end of the vessel may be closed by a refractory lid 90 which may be stationary and supported by the frame. The lid 90 is provided with a central bore 91 through which a burner 92 or other radiant heating means may be inserted. Alternatively, a plurality of heat sources may be employed. The lid is also provided with a feed opening 93 whereby batch may be fed from a screw feeder 94 or the like to the interior of the vessel. Before the vessel is heated, a stable layer of batch 95 is provided in the vessel by feeding loose batch while the housing is rotated. The loose batch assumes a generally paraboloid contour as shown in Fig. 3. The shape assumed by loose, dry batch is related to the speed of rotation as follows:

$$H = \mu R + (2\pi^2 \omega^2 R^2) / g$$

Where:

H=the elevation of a point on the batch surface in the direction parallel to the axis of rotation;
R=the radial distance of that point from the axis of rotation;

μ =a friction factor;

ω =angular velocity; and

g=the acceleration of gravity.

The friction factor may be taken as the tangent of the angle of repose, which for dry glass batch is typically about 35°. The above equation may be employed to select suitable dimensions for the rotary vessel at a selected speed of rotation or, conversely, for determining a suitable speed of rotation for a given vessel. The relationship shows that steeper slopes, which are generally preferred, require faster rotational speeds, and that at zero velocity, the slope is determined solely by the angle of repose as in the Fig. 1 embodiment (assuming no preforming of the batch layer).

During heating, continuous feeding of batch to the vessel of Fig. 3 results in a falling stream of batch 96 that becomes distributed over the surface of the stable batch layer, and by the action of the heat becomes liquefied in a transient layer 97 that runs to the bottom of the vessel and passes through opening 87. The liquefied batch falls as globules 98 from the exit opening and may be collected in a pool 99 within a vessel 100 for further processing. Exhaust gases from the combustion within the liquefaction vessel may also pass through the opening 87 and may be exhausted through a flue 101. Alternatively, an exhaust opening may be provided through the lid 90.

In Figs. 4 and 5, there are depicted combinations of the rotary melter 80 of the Fig. 3 embodiments combined with conventional means for completing the melting of the liquefied batch. In order to melt residual sand grains and to refine the liquefied batch emanating from the rotary melter 80, an overhead fired furnace 110 of conventional construction may be provided as shown in Fig. 4. The furnace contains a pool of the melt 111 and may be provided with one or more side ports 112 or an end port, as are well known in the art, from which flames may be directed above the melt for providing heat thereto. The furnace may include a conventional inlet extension portion 113, but rather than feeding batch at such a location, the output from one or more batch liquefiers may be fed to the furnace through an opening 114. Melted and refined glass may pass from the furnace to a forming operation by way of a conditioner or forehearth 115. The function of the furnace 110 is primarily to raise the temperature of the melt and to provide sufficient residence time for any residual sand grains to dissolve and for gaseous inclusions to evolve from the melt. These functions represent a minor portion of those carried out in a conventional melting furnace, and therefore the furnace 110 may be only a fraction of the size of a conventional furnace having the same throughput. In

other words, it is estimated that the batch liquefaction means of the present invention may replace one-half to two-thirds of a conventional flat glass melting furnace with commensurate savings in construction costs and with more efficient energy usage. A single liquefaction vessel may be used to provide liquefied batch to the furnace of a large scale, commercial glass-making operation, but it is generally more economical to provide a plurality of smaller units. Thus, to supply a throughput on the order of several hundred tons per day, it may be preferred to employ about three or four liquefaction units. It is preferred that each liquefaction unit be made portable so that a unit in need of maintenance may be removed and a reserve unit inserted in its place, thereby minimizing disruption of the glass-making operation. The use of a plurality of liquefaction units also provides an economical means for varying the throughput of the glass-making operation by increasing or decreasing the number of units in operation.

Fig. 5 illustrates another arrangement for completing the melting and refining of the output from one or more rotary liquefaction units 80, employing electric heat rather than overhead combustion firing. The electric melter 120 may be comprised of a refractory vessel 121 into which are inserted a plurality of electrodes 122 by which thermal energy is imparted to the melt by means of Joule resistance heating. The liquefied batch from a liquefaction unit or units may enter the electric melter through an opening 123. Following elevation of the melt temperature by the electric heating, a stream of the melt may pass through a submerged throat 124 to a refining zone 125 where gaseous inclusions are permitted to escape from the melt. It should be understood that in the arrangements shown in Figs. 4 and 5, the rotary liquefaction unit 80 is illustrated as the preferred embodiment, but that the other liquefaction units disclosed herein may be used in place thereof.

In a typical glass batch formula consisting primarily of sand, soda ash and limestone, the soda ash begins to melt first, followed by the limestone, and finally the sand. Physical melting is accompanied by chemical interactions, in particular, the molten alkalis attack the sand grains to effect their dissolution at a temperature below the melting point of silica. At some intermediate point in this process, the liquid phase of the heterogeneous mixture of reacting and melting materials begins to predominate and the material becomes flowable as a fluid. The temperature at which the batch becomes flowable will depend upon the particular batch formula, especially the amount and melting temperature of its lowest melting temperature ingredients. The most common low temperature melting ingredient is soda ash, which melts at 851°C (1564°F). Theoretically, a batch having a sufficient amount of soda ash may become liquefied at the soda ash melting temperature, but experience with commercial batch formulas indicates that the

temperature is somewhat higher 1090° to 1150°C (2000° to 2100°F) for a typical flat glass batch. This may be explained by the fact that batch melting is a complex series of interactions among the various ingredients, whereby the physical properties of the individual ingredients are not exhibited. It may also be that insufficient soda ash is present when melted to entrain by itself the remainder of the unmelted materials. Moreover, even though the present invention eliminates much of the overheating of conventional melters, the runoff temperatures observed with the present invention may not truly represent the initiation of liquefaction, but may include a small amount of heating after liquefaction. Other low temperature melting ingredients sometimes employed in glass batches, such as caustic soda and boric acid, have even lower melting temperatures than soda ash and may behave differently as runoff initiators. On the other hand, some types of glass other than flat glass require higher temperatures to melt. It is preferred to use the present invention with batch formulas that liquefy below 1650°C (3000°F). For many types of glasses made on a large scale commercially, the present invention would be expected to operate satisfactorily with liquefied batch draining from the liquefaction chamber at about 870° to 1260°C (1600° to 2300°F).

In the present invention, the liquefied batch drains from the liquefaction zone as soon as it reaches the fluid state, and therefore the fluid draining from the liquefaction zone has a nearly uniform temperature close to the liquefying temperature of the particular batch formula, typically about 1150°C (2100°F) in the case of conventional flat glass. Because heat is transported out of the liquefaction zone at the liquefying temperature, which is considerably lower than the temperatures attained in a conventional glass melter, the temperature of the liquefaction vessel may be maintained relatively low regardless of the temperature of the heat source. As a result, materials requirements may be reduced relative to a conventional melter, and use of high temperature heat sources is made possible. The greater heat flux afforded by high temperature heat sources advantageously increases the rate of throughput. An example of a high temperature heat source is a combustion burner supplied with oxygen as a partial or total replacement for combustion air. The use of oxygen is also advantageous in the present invention for the sake of reducing the volume of combustion gases, thereby decreasing any tendency of the fine batch materials to become entrained in the exhaust gas stream. This is particularly significant in the preferred practice of feeding the batch dry to the liquefaction vessel as opposed to the conventional practice of wetting the batch with water to inhibit dusting. Furthermore, the use of oxygen instead of air is believed to reduce the potentiality for creating nitrogen containing bubbles in the glass.

An example of a batch formula employed in the

commercial manufacture of flat glass is the following:

	Parts by weight
Sand	1000
Soda ash	313.5
Limestone	84
Dolomite	242
Rouge	0.75

The above batch formula yields approximately the following glass:

	By weight
SiO ₂	73.10%
Na ₂ O	13.75%
CaO	8.85%
MgO	3.85%
Al ₂ O ₃	0.10%
Fe ₂ O ₃	0.10%

The liquefied batch running out of the liquefaction zone of the present invention, when using the batch formula set forth above, is predominantly liquid (weight basis) and includes about 15% by weight or less of crystalline silica (i.e., undissolved sand grains). The liquid phase is predominantly sodium disilicate and includes almost the entire soda ash portion of the batch and most of the limestone and dolomite. The fluid, however, is quite foamy, having a density typically on the order of about 1.9 grams per cubic centimeter, as opposed to a density of about 2.5 grams per cubic centimeter for molten glass.

Although additional energy must be imparted to the liquid to convert it to a completely melted glass, it is estimated that a major portion of the overall energy consumption is spent in the batch liquefaction process, and that that portion of the process is carried out substantially more efficiently by the liquefaction methods of the present invention compared to a conventional tank-type melter. A theoretically derived value for the total energy required to completely melt glass is $2.929 \cdot 10^6$ kJ/metric ton (2.5 million BTU's per ton or 0.7 million kcal/metric ton) of glass produced. In order to complete the melting of the material leaving the liquefaction zone of the present invention, it is calculated that theoretically $0.418 \cdot 10^6$ kJ/metric ton (0.36 million BTU's per ton or 0.1 million kcal/metric ton) would be required, or about 14% of the total theoretical energy requirement. In a conventional overhead

fired tank melting furnace operating at state-of-the-art efficiency, total energy consumption has been found to be typically about $7.322 \cdot 10^6$ kJ/metric ton (6.25 million BTU's per ton or 1.75 million kcal/metric ton) of glass produced. The liquefaction process of the present invention, on the other hand, has been found to consume, typically, about $5.272 \cdot 10^6$ kJ/metric ton (4.5 million BTU's per ton or 1.26 million kcal/metric ton). Accordingly, it can be seen that the liquefaction step performed in accordance with the present invention accomplishes about 86% of the melting while consuming about 72% of the energy required by a conventional melter. The total energy efficiency of the present invention will depend upon the efficiency of the particular process employed to complete the melting of the liquefied batch, but if the efficiency of the subsequent stage is no better than the efficiency of a conventional tank-type melter, it can be estimated that the overall energy consumption for melting glass in accordance with the present invention would be about (5.4 million BTU's per ton) 1.5 million kcal/metric ton, or about 86% of the amount of energy used in the conventional melting process. In fact, it is contemplated that the energy efficiency of subsequent processing steps employed in conjunction with the batch liquefaction of the present invention would be better than that of the conventional melting process, since conditions may be provided that are particularly adapted to the specific tasks of melting residual sand grains and removing gaseous inclusions from the melt. Furthermore, the energy consumption figures employed above for the conventional melting process include heat recovery from the exhaust gases, whereas the figures for the liquefaction process of the present invention do not. Therefore, employing conventional heat recovery means with the process of the present invention may be expected to lower its energy requirements further.

A pilot scale trial of the embodiment of Fig. 6 employed a steel cylindrical drum (18 inches) 46 centimeters high and having an inside diameter of (25.25 inches) 64 centimeters. Optimum rotation of the drum was found to be in the range of 42 to 48 revolutions per minute in order to form a stable layer of loose batch covering the inside wall of the drum. The bottom exit opening had an (8 inch) 20 centimeter diameter. The burner was fired with natural gas and oxygen in stoichiometric ratio and expended $5.021 \cdot 10^6$ kJ/metric ton (4.3 million BTU's per ton or 1.2 million kcal/metric ton) of liquefied batch produced. The maximum production rate attained was 2.8 tons per day of liquefied batch.

Other modifications and variations as would be obvious to those of skill in the art may be resorted to without departing from the scope of the claims which follow.

Claims

1. A method of liquefying glass batch material

commercial manufacture of flat glass is the following:

	Parts by weight
Sand	1000
Soda ash	313.5
Limestone	84
Dolomite	242
Rouge	0.75

The above batch formula yields approximately the following glass:

	By weight
SiO ₂	73.10%
Na ₂ O	13.75%
CaO	8.85%
MgO	3.85%
Al ₂ O ₃	0.10%
Fe ₂ O ₃	0.10%

The liquefied batch running out of the liquefaction zone of the present invention, when using the batch formula set forth above, is predominantly liquid (weight basis) and includes about 15% by weight or less of crystalline silica (i.e., undissolved sand grains). The liquid phase is predominantly sodium disilicate and includes almost the entire soda ash portion of the batch and most of the limestone and dolomite. The fluid, however, is quite foamy, having a density typically on the order of about 1.9 grams per cubic centimeter, as opposed to a density of about 2.5 grams per cubic centimeter for molten glass.

Although additional energy must be imparted to the liquid to convert it to a completely melted glass, it is estimated that a major portion of the overall energy consumption is spent in the batch liquefaction process, and that that portion of the process is carried out substantially more efficiently by the liquefaction methods of the present invention compared to a conventional tank-type melter. A theoretically derived value for the total energy required to completely melt glass is $2.929 \cdot 10^6$ kJ/metric ton (2.5 million BTU's per ton or 0.7 million kcal/metric ton) of glass produced. In order to complete the melting of the material leaving the liquefaction zone of the present invention, it is calculated that theoretically $0.418 \cdot 10^6$ kJ/metric ton (0.36 million BTU's per ton or 0.1 million kcal/metric ton) would be required, or about 14% of the total theoretical energy requirement. In a conventional overhead

fired tank melting furnace operating at state-of-the-art efficiency, total energy consumption has been found to be typically about $7.322 \cdot 10^6$ kJ/metric ton (6.25 million BTU's per ton or 1.75 million kcal/metric ton) of glass produced. The liquefaction process of the present invention, on the other hand, has been found to consume, typically, about $5.272 \cdot 10^6$ kJ/metric ton (4.5 million BTU's per ton or 1.26 million kcal/metric ton). Accordingly, it can be seen that the liquefaction step performed in accordance with the present invention accomplishes about 86% of the melting while consuming about 72% of the energy required by a conventional melter. The total energy efficiency of the present invention will depend upon the efficiency of the particular process employed to complete the melting of the liquefied batch, but if the efficiency of the subsequent stage is no better than the efficiency of a conventional tank-type melter, it can be estimated that the overall energy consumption for melting glass in accordance with the present invention would be about (5.4 million BTU's per ton) 1.5 million kcal/metric ton, or about 86% of the amount of energy used in the conventional melting process. In fact, it is contemplated that the energy efficiency of subsequent processing steps employed in conjunction with the batch liquefaction of the present invention would be better than that of the conventional melting process, since conditions may be provided that are particularly adapted to the specific tasks of melting residual sand grains and removing gaseous inclusions from the melt. Furthermore, the energy consumption figures employed above for the conventional melting process include heat recovery from the exhaust gases, whereas the figures for the liquefaction process of the present invention do not. Therefore, employing conventional heat recovery means with the process of the present invention may be expected to lower its energy requirements further.

A pilot scale trial of the embodiment of Fig. 6 employed a steel cylindrical drum (18 inches) 46 centimeters high and having an inside diameter of (25.25 inches) 64 centimeters. Optimum rotation of the drum was found to be in the range of 42 to 48 revolutions per minute in order to form a stable layer of loose batch covering the inside wall of the drum. The bottom exit opening had an (8 inch) 20 centimeter diameter. The burner was fired with natural gas and oxygen in stoichiometric ratio and expended $5.021 \cdot 10^6$ kJ/metric ton (4.3 million BTU's per ton or 1.2 million kcal/metric ton) of liquefied batch produced. The maximum production rate attained was 2.8 tons per day of liquefied batch.

Other modifications and variations as would be obvious to those of skill in the art may be resorted to without departing from the scope of the claims which follow.

Claims

1. A method of liquefying glass batch material



by feeding the fusible material (52, 96) to an upper inlet portion of a heating vessel (50, 65, 81) having side walls encircling a heated cavity, providing a lining (55, 68, 95) on the interior of the side walls, heating the cavity to liquefy a layer (59, 68, 97) of the material which flows on the lining (55, 68, 95) to an outlet (57, 74, 87) at the lower portion of the vessel (50, 65, 89) and feeding the material (52, 96) onto the lining (55, 68, 95) at a rate corresponding to the rate of drainage, characterized by providing as a substantial portion of the lining (55, 68, 95) a layer (59, 68, 97) of substantially the same glass batch material and maintaining at least a portion of the thickness of the layer (59, 68, 97) unliquefied substantially by permitting liquefied material to drain freely from the vessel (50, 65, 81) while the liquefied material contains incompletely melted portions of the batch.

2. The method of Claim 1 characterized in that the liquefied batch flows out of the vessel (50, 65, 81) before its temperature exceeds 1260°C.

3. The method of Claims 1—2 characterized by providing the lining (55, 68, 95) of non-liquefied glass batch sloping at an angle greater than the natural angle of repose of the batch.

4. The method of Claims 1—3 characterized by providing a stable mass of glass batch with a thickness of at least 3 centimeters.

5. The method of Claims 1—4 characterized by rotating the vessel (65, 81) about its axis.

6. The method of Claim 5 characterized by rotating the vessel (81) about a vertical axis.

7. The method of Claims 1—6 characterized by feeding the batch as a dry mixture.

8. The method of Claims 1—7 characterized by using a batch essentially free of sulfur.

9. The method of Claims 1—8 characterized by depositing a stream of batch (52, 96) onto the upper portion of the sloped transient batch layer (59, 68, 97) and letting portions of the batch tumble onto the lower portions of the transient batch layer (59, 68, 97).

10. The method of Claims 1—9 characterized in that the liquefied batch is drained from the vessel (50, 65, 81) before the constituency of the batch has become fully melted.

11. The method of Claims 1—10 characterized in that the liquefied batch drained from the vessel (50, 65, 81) is received in a down-stream chamber where its temperature is raised to complete the melting process.

12. The method of Claim 2 characterized in that the melted ingredients of the liquefied batch flowing out of the vessel (50, 65, 81) include soda ash, caustic soda, or boric acid, and the unmelted particles include sand grains.

13. The method of Claims 1—12 characterized by subsequently imparting additional thermal energy to the molten fluid flowed out of the liquefaction zone so as to complete melting of the batch material.

Patentansprüche

1. Verfahren zum Verflüssigen von Glasgemen-

gematerial durch Zuführen von schmelzbarem Material (52, 96) zu einem oberen Einlaßteil eines Erwärmungsgefäßes (50, 65, 31), dessen Seitenwände einen aufgeheizten Raum umschließen, Ausbilden einer Auskleidung (55, 68, 95) auf der Innenseite der Seitenwände, Erwärmen des Raumes um eine Schicht (59, 68, 97) des auf der Auskleidung (55, 68, 95) zu einem im unteren Teil des Gefäßes (50, 65, 89) angeordneten Auslaß (57, 74, 87) fließenden Materials zu verflüssigen und Zuführen von Material (92, 96) auf die Auskleidung (55, 68, 95) mit einer der Abzugsgeschwindigkeit entsprechenden Geschwindigkeit, gekennzeichnet durch Ausbilden einer Schicht (59, 68, 97) aus im wesentlichen mit dem Glasgemengematerial übereinstimmenden Material als ein wesentlicher Teil der Auskleidung (55, 68, 95) und Aufrechterhalten mindestens eines unverflüssigten Teils der Schichtdicke der Schicht (59, 68, 97) im wesentlichen durch freies Abfließenlassen des verflüssigten Materials aus dem Gefäß (50, 65, 81), während das verflüssigte Material unvollständig geschmolzene Teile des Gemenges enthält.

2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß das verflüssigte Gemenge aus dem Gefäß (50, 65, 81) ausfließt, ehe seine Temperatur 1260°C überschreitet.

3. Verfahren nach Ansprüchen 1 bis 2, gekennzeichnet durch Ausbilden der Auskleidung (55, 68, 95) aus nicht-verflüssigtem Glasgemenge unter einem Winkel, der größer ist als der natürliche Schüttwinkel des Gemenges.

4. Verfahren nach Ansprüchen 1 bis 3, gekennzeichnet durch Ausbilden einer stabilen Masse von Glasgemenge mit einer Dicke von mindestens 3 cm.

5. Verfahren nach Ansprüchen 1 bis 4, gekennzeichnet durch Drehen des Gefäßes (65, 81) um seine Achse.

6. Verfahren nach Anspruch 5, gekennzeichnet durch Drehen des Gefäßes (81) um eine senkrechte Achse.

7. Verfahren nach Ansprüchen 1 bis 6, gekennzeichnet durch Zuführen des Gemenges als trockene Mischung.

8. Verfahren nach Ansprüchen 1 bis 7, gekennzeichnet durch Verwendung eines im wesentlichen schwefelfreien Gemenges.

9. Verfahren nach Ansprüchen 1 bis 8, gekennzeichnet durch Ablagern eines Stromes von Gemenge (52, 96) auf dem oberen Teil der gewölbten vorübergehenden Gemengeschicht (59, 68, 97) und Herabfallenlassen von Teilen des Gemenges auf darunterliegende Teile der vorübergehenden Gemengeschicht (59, 68, 97).

10. Verfahren nach Ansprüchen 1 bis 9, dadurch gekennzeichnet, daß das verflüssigte Gemenge ehe es vollständig geschmolzen ist aus dem Gefäß (50, 65, 81) abgezogen wird.

11. Verfahren nach Ansprüchen 1 bis 10, dadurch gekennzeichnet, daß das aus dem Gefäß (50, 65, 81) abgezogene verflüssigte Gemenge in einer darunter angeordneten Kammer aufge-



nommen und seine Temperatur zum Vervollständigen des Schmelzprozesses erhöht wird.

12. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die aus dem Gefäß (50, 65, 81) ausfließenden geschmolzenen Bestandteile des verflüssigten Gemenges Rohsoda, kausstisches Soda oder Borsäure und die nicht-geschmolzenen Teile Sandkörner enthalten.

13. Verfahren nach Ansprüchen 1 bis 12, gekennzeichnet durch anschließendes Aufbringen von zusätzlicher thermischer Energie auf den aus der Verflüssigungszone auslaufenden geschmolzenen Strom, um das Schmelzen des Gesamtmaterials zu vervollständigen.

Revendications

1. Procédé de liquéfaction de matières premières du verre, par introduction des matières fusibles (52, 96) dans une partie supérieure d'entrée d'un récipient de chauffage (50, 65, 81) dont les parois latérales entourent une cavité chauffée, formation d'un revêtement (55, 68, 95) sur la face intérieure des parois latérales, chauffage de la cavité pour liquéfier une couche (59, 68, 97) des matières qui s'écoule sur le revêtement (55, 68, 95) vers un orifice de sortie (57, 74, 87) à la partie inférieure du récipient (50, 65, 89) et apport des matières (52, 96) sur le revêtement (55, 68, 95) avec un débit qui correspond au débit d'évacuation, caractérisé en ce qu'il est formé, en tant que partie essentielle du revêtement (55, 68, 95), une couche (59, 68, 97) des mêmes matières premières du verre constituant la charge, et en ce qu'une fraction au moins de l'épaisseur de cette couche (59, 68, 97) est maintenue pratiquement non liquéfiée en permettant aux matières liquéfiées de s'écouler librement du récipient (50, 65, 81) alors que ces matières liquéfiées contiennent des fractions incomplètement fondues de la charge.

2. Procédé selon la revendication 1, caractérisé en ce que la charge liquéfiée s'écoule du récipient (50, 65, 81) avant que sa température ne dépasse 1260°C.

3. Procédé selon la revendication 1 ou 2, caractérisé en ce que le revêtement (55, 68, 95) de charge de verre non liquéfiée est formé avec une pente dont l'angle est plus grand que l'angle naturel de repos de la charge.

4. Procédé selon l'une quelconque des revendications 1 à 3, caractérisé en ce qu'il est formé une masse stable de charge de verre d'une épaisseur d'au moins 3 cm.

5. Procédé selon l'une quelconque des revendications 1 à 4, caractérisé en ce que le récipient (65, 81) est mis en rotation autour de son axe.

6. Procédé selon la revendication 5, caractérisé en ce que le récipient (81) est mis en rotation autour d'un axe vertical.

7. Procédé selon l'une quelconque des revendications 1 à 6, caractérisé en ce que la charge est introduite sous forme de mélange sec.

8. Procédé selon l'une quelconque des revendications 1 à 7, caractérisé en ce que la charge utilisée est essentiellement exempte de soufre.

9. Procédé selon l'une quelconque des revendications 1 à 8, caractérisé en ce qu'un courant de charge (52, 96) est déposé sur la partie supérieure de la couche transitoire de charge en pente (59, 68, 97) et en ce qu'on laisse des parties de la charge dégringoler sur les parties inférieures de la couche transitoire de charge (59, 68, 97).

10. Procédé selon l'une quelconque des revendications 1 à 9, caractérisé en ce que la charge liquéfiée est évacuée du récipient (50, 65, 81) avant que sa consistance ne soit devenue celle d'une fusion complète.

11. Procédé selon l'une quelconque des revendications 1 à 10, caractérisé en ce que la charge liquéfiée évacuée du récipient (50, 65, 81) est reçue dans une chambre aval, dans laquelle sa température est élevée afin d'achever le processus de fusion.

12. Procédé selon la revendication 2, caractérisé en ce que les ingrédients fondus de la charge liquéfiée qui s'écoule du récipient (50, 65, 81) comprennent de la soude calcinée, de la soude caustique ou de l'acide borique et les particules non fondues comprennent des grains de sable.

13. Procédé selon l'une quelconque des revendications 1 à 12, caractérisé en ce qu'il est fourni subséquentement une quantité supplémentaire d'énergie thermique au fluide fondu qui s'écoule de la zone de liquéfaction, de façon à achever la fusion des matières premières de la charge.

