

Description

This invention is in the detergent field and relates to phase transfer assisted processes for condensing N-alkylglucamines with fatty esters to produce laundry detergent surfactants.

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BACKGROUND OF THE INVENTION

The present invention is set against a background of change in society's attitudes to how natural resources are used. Petroleum feedstocks are nonrenewable and increasingly costly, even impacting significantly on national balances of payment, and supply can be uncertain. There is a perception, increasingly commonly held, that it may be for the general good of society, as well as of the environment, to reduce the reliance of consumer disposable goods manufacturing on such feedstocks. However, a serious response to such notions requires efficient processes for converting locally or regionally available renewable resource feedstocks into desirable consumer goods such as laundry detergents.

The United States produces very considerable tonnages of sugars, such as glucose or corn syrup, as well as of fatty substances. There is a downward trend in traditional patterns of consumption of these particular renewable resources: people are tending to eat less sugars, and also less fatty foods, especially saturated fats, for health-related reasons. This makes their development for other uses, such as laundry detergents, all the more attractive.

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BACKGROUND ART

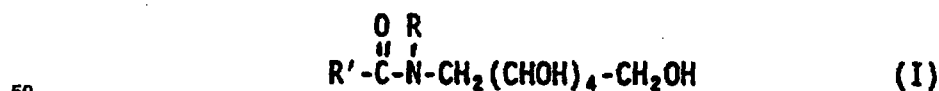
A number of years ago, processes were explored for making textile assistants or detergents from fatty acids or their derivatives in combination with N-alkylglucamines, the latter made by reductive amination of glucose. Glucose reductive amination processes are more fully disclosed in U.S. Patent 2,016,962, Flint et al, issued October 8, 1935.

U.S. Patent 1,985,424, Piggott, issued December 25, 1934 discloses manufacturing "textile assistants" by reacting (a) the product of heating glucose and aqueous methylamine in presence of hydrogen and a hydrogenating catalyst under pressure with (b) an organic carboxylic acid such as stearic acid or oleic acid. The condensation product, prepared at about 160 °C, is said to be "predominantly, if not exclusively, an amide" and is assertedly of the formula $R-CO-NR_1-CH_2-(CHOH)_4-CH_2OH$ wherein R is an alkyl radical containing at least 3 carbon atoms, while R_1 is hydrogen or an alkyl radical.

U.S. Patent 2,703,798, Schwartz, issued March 8, 1955 asserts that compositions produced by reacting fatty acids or acid anhydrides with N-alkylglucamines (presumably such as the process as taught by Piggott) have poor color and poor detergency properties. It is indeed chemically reasonable that more than one compound can be formed by the Piggott process. Piggott makes no attempt to quantitatively prove the structures of the compounds or mixtures he prepared.

Schwartz ('798) goes on to report an improvement as a result of reacting fatty ester (as distinct from fatty acid or anhydride) with N-alkylglucamines. Although this process may overcome one or another deficiency of the art, such as of Piggott, it now transpires that the Schwartz process still has difficulties, in particular, in that complex mixtures of compounds can be formed even by the Schwartz process. The reaction may take several hours and the process can fail to give high quality product. Neither the process of Piggott nor the process of Schwartz is known to have ever borne fruit in commercial practice.

In more detail, Schwartz notes that only one of several possible chemical reactions takes place when N-monoalkylglucamines are condensed with fatty esters or oils. The reaction is said to give compounds formulated as amides, e.g.,



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where R' is fatty alkyl and R is a short-chain alkyl, typically methyl. This structure is apparently the same as the structure proposed by Piggott. Schwartz contrasts the single-product outcome he believes he secures with compounds he asserts are actually produced when acids are reacted with N-alkylglucamines, namely mixtures of the amide (I) with one or more by-products, to which he assigns esteramide and esteramine structures and which assertedly include compounds which are "inert and waxy, impairing the surface activity of" the structure (I) amide.

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According to Schwartz, approximately equimolar proportions of N-monoalkylglucamines can be reacted with fatty alkyl esters by heating at 140°C-230°C, preferably 160°C-180°C at normal, reduced or superatmospheric pressures for a period "somewhat in excess of one hour" during which time two initially immiscible phases merge to form a product said to be a useful detergent.

5 Suitable N-monoalkylglucamines are illustrated by N-methylglucamine, N-ethylglucamine, N-isopropylglucamine and N-butylglucamine. Suitable fatty alkyl esters are illustrated by the product of reacting a C6-C30 fatty acid with an aliphatic alcohol e.g., methyl ester of lauric acid. Mixed glycerides of Manila oil or mixed glycerides of cochin coconut oil can apparently also be used as the fatty ester. When the glucamine is N-methylglucamine, the corresponding products with these fatty esters are characterized as the "fatty acid amides of N-methylglucamine", which are useful detergent surfactants. Another specific composition reported is assertedly "N-isopropylglucamine coconut fatty acid amide".

10 U.S. Patent 2,993,887, Zech, issued July 25, 1961 reveals there is even more complexity to the reactions of fatty substances with N-methylglucamine. In particular, Zech asserts that the products of high-temperature reaction (180°C-200°C) within the range disclosed by Schwartz have cyclic structures. No fewer than four possible structures are given. See '887 at column 1, line 63 - column 2, line 31.

What is now believed actually to be provided by the fatty ester- N-alkylglucamine process of Schwartz are compositions comprising mixtures of formula (I) compounds together with appreciable proportions (e.g., about 25%, often much more) of several other components, especially cyclic glucamide by-products (including but not limited to the structures proposed by Zech) or related derivatives such as esteramides wherein as compared with formula (I) at least one -OH moiety is esterified.

20 Moreover, a reinvestigation of Schwartz suggests that there are other significant unsolved problems in the process, including a tendency to form trace materials imparting very unsatisfactory color and/or odor to the product.

More recently, the work of Schwartz notwithstanding, Hildreth has asserted that compounds of formula (I) are new. See Biochem. J., 1982, Vol. 207, pages 363-366. In any event, these compositions are given a new name: "N-D-gluco-N-methylalkanamide detergents", and the acronym "MEGA". Hildreth provides a solvent-assisted process for making the compounds differing seminally from Schwartz in that it returns to the use of a fatty acid reactant, instead of fatty ester. Moreover, Hildreth relies on pyridine/ethyl chloroformate as the solvent/activator. This process is specifically illustrated for octanoyl-N-methylglucamide ("OMEGA"), nonanoyl-N-methylglucamide ("MEGA-9") and decanoyl-N-methylglucamide ("MEGA-10"). The process is said to be cheap and high-yield. One must of course assume that "cheap" is relative and is meant in the sense of specialized biochemical applications of interest to the author: in terms of large-scale detergent manufacture, the use of pyridine and ethyl chloroformate would hardly be viewed as consistent with an economic or environmentally attractive process. Therefore, the Hildreth process is not further considered herein.

Hildreth and other workers have purified certain formula (I) compounds, e.g., by recrystallization, and have described the properties of some of the structure (I) compounds. Recrystallization is, of course, a costly and potentially hazardous (flammable solvents) step in itself, and large-scale detergent manufacture would be more economical and safer without it.

40 According to Schwartz *supra*, the products of the Schwartz process can be used for cleaning hard surfaces. According to Thomas Hedley & Co. Ltd. (now Procter & Gamble), British Patent 809,060 published February 18, 1959, formula (I) compounds are useful as a surfactant for laundry detergents such as those having granular form. Hildreth (*supra*) mentions use of compounds of formula (I) in the biochemistry field as a detergent agent for solubilizing plasma membranes and EP-A 285,768, published December 10, 1988 describes application of formula (I) compounds as a thickener. Thus, these compounds, or compositions containing them, can be highly desirable surfactants.

Yet another process for making compositions comprising formula (I) compounds is included in the above-identified disclosure of improved thickeners. See EP-A 285,768. See also H. Kelkenberg, Tenside Surfactants Detergents 25 (1988) 8-13, *inter alia* for additional disclosures of processes for making N-alkylglucamines which, along with the above-identified art-disclosed N-alkylglucamine processes can be combined with the instant process for an overall conversion of glucose and fatty materials to useful surfactant compositions.

55 The relevant disclosures of EP-A 285,768 include a brief statement to the effect that "it is known that the preparation of chemical compounds of formula (I) is done by reacting fatty acids or fatty acid esters in a melt with polyhydroxy alkylamines which can be N-substituted, optionally in the presence of alkaline catalysts". The above-referenced art strongly suggests that this statement is a gross simplification or is inaccurate. EP-A 285,768 does not cite any references in support of the quoted statement, nor has any reference other than EP-A 285,768 been found which actually does disclose any catalytic condensation of

N-alkylglucamines with fatty esters or fatty triglycerides.

The European Patent Application contains the following Example entitled "Preparation of N-methyl-coconut fatty acid glucamide" in which "Na methylate" is understood to be synonymous with "sodium methoxide" and which has been translated from the German:

5 In a stirred flask 669 g (3.0 mol) of coconut fatty acid methyl ester and 585 g (3.0 mol) of N-methyl glucamine with the addition of 3.3 g Na methylate were gradually heated to 135°C. The methanol formed during the reaction was condensed under increasing vacuum at 100 to 15 mbar in a cooled collector. After the methanol evolution ended the reaction mixture was dissolved in 1.5 l of warm isopropanol, filtered and crystallized. After filtration and drying 882 g (=76% of theoretical) of waxy N-methyl coconut fatty acid
10 glucamide was obtained. Softening point = 80 to 84°C; Base number: 4 mg. KOH /g.

EP-A 285,768 continues with the following:

"In a similar manner the following fatty acid glucamides were
15 prepared:

	Yield	Softening Point	Base No.
	%	(°C)	(mg. KOH/g)
N-methyl lauric acid glucamide	76	94-96	6
20 N-methyl myristic acid glucamide	75	98-100	3
N-methyl palmitic acid glucamide	75	103-105	5
N-methyl stearic acid glucamide	84	96-98	6"

25 To summarize some important points of what can be gleaned from the art, the aforementioned Schwartz patent teaches that the problem of making formula (I) compounds from fatty esters or triglycerides and an N-alkylglucamine is solved by selecting fatty ester (instead of fatty acid) as the fatty reactant, and by doing simple uncatalyzed condensations. Later literature, such as Hildreth, changes direction back to a fatty acid-type synthesis, but does not document either that the teaching of the Schwartz patent is in error or how,
30 short of making highly pure formula (I) compounds, to make such surfactants to detergent formulators' specifications. On the other hand, there has been one disclosure, in a totally different technical field, of sodium methoxide-catalyzed formula (I) compound synthesis. As noted, the procedure involves gradual temperature staging up to 135°C and recrystallizing the product.

35 In view of the foregoing observations, it would be very desirable to further improve processes for making surfactant compositions comprising formula (I) compounds. Such processes should be useful on a large scale and should result directly in compositions meeting laundry detergent formulators' specifications without need for recrystallization.

Accordingly, it is an object of the instant invention to provide an improved process for manufacturing
40 surfactant compositions by reacting fatty esters and N-alkylglucamines in the presence of phase transfer agents.

This and other objects are secured, as will be seen from the following disclosure.

SUMMARY

45 The present invention relates to an improved process for preparing detergent surfactants, more specifically, surfactant compositions having a high proportion of compounds of formula (I) wherein R' is fatty alkyl and R is a short-chain hydrocarbyl, typically methyl, ethyl or the like. Products of the invention include the detergent surfactant, as well as detergent compositions consisting essentially of mixtures of the
50 surfactant with one or more additional laundry-useful components, especially alkaline laundry detergent builders.

In general, the process involves reacting fatty esters and N-alkylglucamines in the presence of particular phase transfer agents.

Suitable phase transfer agents for use in the present invention are members selected from the group
55 consisting of nonionic surfactants. Nonionic surfactants are generally disclosed in "Nonionic Surfactants", Ed. M. J. Schick, Marcel Dekker, NY, 1966 and numerous other texts in the detergent arts.

Preferred phase transfer agents for use herein consist essentially of a member selected from the group consisting of saturated fatty alcohol polyethoxylates, alkylpolyglycosides, linear glucamide surfactant and

mixtures thereof.

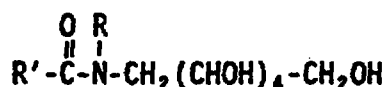
In general, the amount of phase transfer agent is from about 0.5% to about 95% of the total weight of the reactants.

The phase transfer agent is especially effective when the N-alkylglucamine and fatty ester are very difficult to mix. The problem is especially severe when the fatty ester is very hydrophobic, as in coconut or higher chain-length oils, oleyl methyl ester, stearyl methyl ester and the like. The invention confers its greatest benefits in such a circumstance.

Preferably, the present process is catalyzed and numerous suitable catalysts are identified hereinafter. Especially preferred catalysts include sodium carbonate and potassium carbonate.

The process efficiently converts the N-alkylglucamine, e.g., N-methyl-D-glucamine, to linear glucamide surfactant of quality suitable for the laundry detergent formulator, without need for recrystallization.

In a preferred embodiment, the invention encompasses a batch (noncontinuous) process wherein the amount of phase transfer agent is from about 1 weight % to about 10 weight %, the amount of catalyst is from about 0.5 mole % to about 50 mole % on N-alkylglucamine, conversion of N-alkylglucamine to compounds having linear structure of formula



wherein R is the alkyl residue of the glucamine and R' is the residue of the fatty ester is about 70 mole % or higher on N-alkylglucamine, and conversion of N-alkylglucamine to cyclic glucamide or esteramide by-products is about 15 mole % or lower.

Continuous process embodiments are also encompassed: in such embodiments, the proportion of phase transfer agent can vary widely within the above-identified general ranges.

The preferred catalysts, as they operate in the process, have the advantage of not catalytically increasing the formation of by-product such as esteramide or cyclized glucamide at the same time as catalyzing the desired amidation. This is surprising since esteramide by-product formation is an esterification reaction, and catalysts such as sodium carbonate or potassium carbonate have heretofore been used for catalyzing esterification reactions. See, for example, U.S. Patent 2,999,858, Curtis, issued September 12, 1961 which discloses a conversion of sucrose to sucrose fatty esters. See also U.S. Patent 3,558,597, von Brachel et al, issued January 26, 1971.

In short, the present invention is surprising in its ability to catalytically form surfactant compositions rich in formula (I) compounds selectively, without at the same time catalytically increasing by-product formation, especially by esterification.

In general, the present process takes N-alkylglucamines to linear glucamides of formula (I) with a conversion of about 70 mole % or higher, more preferably 80 mole % or higher based on N-alkylglucamine, whereas the conversion of N-alkylglucamine to by-product having cyclic glucamide or esteramide structure is generally about 15 mole % or lower.

The N-alkylglucamine starting-material can be prepared by any of the above-referenced literature methods and is illustrated by N-methylglucamine, N-ethylglucamine, N-propylglucamine and N-butylglucamine.

Highly preferred fatty ester is selected from saturated fatty methyl esters and fatty triglycerides.

The N-alkylglucamine and fatty ester are preferably used in approximately equimolar proportions in terms of the number of moles of fatty carbonyl moieties of the fatty ester per mole of N-alkylglucamine. Excellent results can also be achieved when there is a slight excess of fatty ester, e.g., about 1.05 moles per mole of N-alkylglucamine.

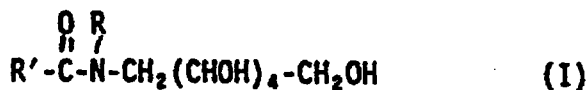
The present invention has many advantages, including a generally rapid and efficient process achieving a product which is useful without further purification for formulation in laundry detergents. The product of the process generally has good color and only low levels of nonvolatile by-product (notably cyclic by-product but also esteramides and the like). In certain embodiments of the invention, novel and useful compositions such as surfactant/builder intermediates for the formulator of granular laundry detergents are also secured.

Percentages and proportions herein are normally designated on a mole percentage basis unless otherwise indicated.

DETAILED DESCRIPTION OF THE INVENTION

The present invention relates to a phase transfer-assisted process for manufacturing linear glucamide surfactants from fatty esters and N-alkylglucamines. In the preferred product compositions, a high proportion (typically 70 mole % or higher, preferably 80 mole % or higher) of the N-alkylglucamine is converted to formula (I) compounds wherein R' is fatty alkyl and R is a short-chain hydrocarbyl, typically methyl, ethyl or the like.

When referring to "conversion" percentages herein, such conversion percentages are expressed on a mole percentage basis.



Although it is recognized that substantially pure compounds of formula (I) or, at the other extreme, highly impure compositions comprising (I) are not new, the term "linear glucamide surfactant" will be used herein to refer to the characteristic product of the process which is directly useful as a surfactant for large-scale laundry detergent formulation.

In general, "linear glucamide surfactant" as produced herein has a major proportion of the N-alkylglucamine starting-material converted to formula (I) compounds, while only minor proportions, e.g., 15 mole % or less (desirably, even as low as 2% or 0.5%, by weight), are converted to cyclic glucamide and/or esteramide.

By comparison, art-taught products such as those of Schwartz are believed to involve important conversion of the starting-material (e.g., 25 mole % or higher) to compounds departing from formula (I) by virtue of cyclization of the polyhydroxy moiety (cyclic glucamide) or esterification of the hydroxy moieties (esteramide).

In outline, the instant process comprises reacting a mixture of an N-alkylglucamine and a fatty ester in the presence of a phase transfer agent, preferably with a catalyst.

Phase Transfer Agent

The N-alkylglucamine and fatty ester mix with difficulty in the present process, and it is to this difficulty that the invention is particularly directed. The problem is especially severe when the fatty esters are relatively hydrophobic, e.g., coconut triglycerides or the ethyl esters of C₁₆ saturated fatty acids. To solve this problem, it has been discovered that nonionic surfactants such as a preformed formula (I) compound wherein R' is C₁₁H₂₃ and R is methyl may be used as a phase transfer agent or emulsifier. Phase transfer agent as used in the instant process is generally at a level of from about 0.5% to about 95% by weight of the reaction mixture. High levels such as 50% or more are best reserved for continuous mode embodiments where reaction times can be kept very short. In a batch (i.e., noncontinuous) process, a preferred level is from about 0.5 weight % to about 20 weight %, even more preferably from about 1 weight % to about 10 weight %. Such levels are also suitable for use in continuous mode embodiments. Continuous mode embodiments will, of course, concurrently recycle some catalyst, if it is present.

More generally, suitable phase transfer agents for use in the present invention are members selected from the group consisting of nonionic surfactants. Nonionic surfactants are generally disclosed in "Nonionic Surfactants", Ed. M. J. Schick, Marcel Dekker, NY, 1966 and numerous other texts in the detergent arts.

Preferred phase transfer agents for use herein consist essentially of a member selected from the group consisting of saturated fatty alcohol polyethoxylates, alkylpolyglycosides, linear glucamide surfactant and mixtures thereof.

In more detail, suitable nonionic surfactants useful as phase transfer agent are generally disclosed in U.S. Patent 3,929,678, Laughlin et al, issued December 30, 1975, at column 13, line 14 through column 16, line 6, incorporated herein by reference. Exemplary, nonlimiting classes of useful nonionic surfactants are listed below.

1. The polyethylene oxide condensates of alkylphenols. These compounds include the condensation products of alkylphenols having an alkyl group containing from about 6 to about 12 carbon atoms in either a straight-chain or branched-chain configuration with ethylene oxide, the ethylene oxide being present in an amount equal to from about 5 moles to about 25 moles of ethylene oxide per mole of alkylphenol. Examples of compounds of this type include nonylphenol condensed with about 9.5 moles

of ethylene oxide per mole of the nonylphenol; dodecylphenol condensed with about 12 moles of ethylene oxide per mole of the dodecylphenol; dinonylphenol condensed with about 15 moles of ethylene oxide per mole of the dinonylphenol; and diisooctylphenol condensed with about 15 moles of ethylene oxide per mole of the diisooctylphenol. Commercially available nonionic surfactants of this type include IGEPAL CO-630, marketed by the GAF Corporation; and TRITON X-45, X-114, X-100, and X-102, all marketed by the Rohm & Haas Company.

2. The condensation products of aliphatic alcohols with from about 1 mole to about 25 moles of ethylene oxide. The alkyl chain of the aliphatic alcohol can either be straight or branched, primary or secondary, and generally contains from about 8 carbon atoms to about 22 carbon atoms. Particularly preferred are the condensation products of alcohols having an alkyl group containing from about 10 to about 20 carbon atoms with from about 4 moles to about 10 moles of ethylene oxide per mole of alcohol. Examples of such ethoxylated alcohols include the condensation product of myristyl alcohol with about 10 moles of ethylene oxide per mole of alcohol; and the condensation product of coconut alcohol (a mixture of fatty alcohols with alkyl chains varying in length from 10 to 14 carbon atoms) with about 9 moles of ethylene oxide. Examples of commercially available nonionic surfactants of this type include TERGITOL 15-S-9 (the condensation product of C₁₁-C₁₅ linear alcohol with 9 moles ethylene oxide), TERGITOL 24-L-6 NMW (the condensation product of C₁₂-C₁₄ primary alcohol with 6 moles ethylene oxide with a narrow molecular weight distribution), both marketed by Union Carbide Corporation; NEODOL 45-9 (the condensation product of C₁₄-C₁₅ linear alcohol with 9 moles of ethylene oxide), NEODOL 23-6.5 (the condensation product of C₁₂-C₁₃ linear alcohol with 6.5 moles of ethylene oxide), NEODOL 45-7 (the condensation product of C₁₄-C₁₅ linear alcohol with 7 moles of ethylene oxide), NEODOL 45-4 (the condensation product of C₁₄-C₁₅ linear alcohol with 4 moles of ethylene oxide), marketed by Shell Chemical Company, and KYRO EOB (the condensation product of C₁₃-C₁₅ alcohol with 9 moles ethylene oxide), marketed by The Procter & Gamble Company.

3. The condensation products of ethylene oxide with a hydrophobic base formed by the condensation of propylene oxide with propylene glycol. The hydrophobic portion of these compounds preferably has a molecular weight of from about 1500 to about 1800 and exhibits water insolubility. The addition of polyoxyethylene moieties to this hydrophobic portion tends to increase the water solubility of the molecule as a whole, and the liquid character of the product is retained up to the point where the polyoxyethylene content is about 50% of the total weight of the condensation product, which corresponds to condensation with up to about 40 moles of ethylene oxide. Examples of compounds of this type include certain of the commercially-available PLURONIC surfactants, marketed by Wyandotte Chemical Corporation.

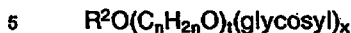
4. The condensation products of ethylene oxide with the product resulting from the reaction of propylene oxide and ethylenediamine. The hydrophobic moiety of these products consists of the reaction product of ethylenediamine and excess propylene oxide, and generally has a molecular weight of from about 2500 to about 3000. This hydrophobic moiety is condensed with ethylene oxide to the extent that the condensation product contains from about 40% to about 80% by weight of polyoxyethylene and has a molecular weight of from about 5,000 to about 11,000. Examples of this type of nonionic surfactant include certain of the commercially available TETRONIC compounds, marketed by Wyandotte Chemical Corporation.

5. Alkylpolysaccharides disclosed in U.S. Patent 4,565,647, Llenado, issued January 21, 1986, having a hydrophobic group containing from about 6 to about 30 carbon atoms, preferably from about 10 to about 16 carbon atoms and a polysaccharide, e.g., an alkylpolyglycoside, hydrophilic group containing from about 1.5 to about 10, preferably from about 1.5 to about 3, most preferably from about 1.6 to about 2.7 saccharide units. Any reducing saccharide containing 5 or 6 carbon atoms can be used, e.g., glucose, galactose and galactosyl moieties can be substituted for the glucosyl moieties. (Optionally the hydrophobic group is attached at the 2-, 3-, 4-, etc. positions thus giving a glucose or galactose as opposed to a glucoside or galactoside.) The intersaccharide bonds can be, e.g., between the one position of the additional saccharide units and the 2-, 3-, 4-, and/or 6-positions on the preceding saccharide units.

Optionally, and less desirably, there can be a polyalkyleneoxide chain joining the hydrophobic moiety and the polysaccharide moiety. The preferred alkylene oxide is ethylene oxide. Typical hydrophobic groups include alkyl groups, either saturated or unsaturated, branched or unbranched containing from about 8 to about 18, preferably from about 10 to about 16, carbon atoms. Preferably, the alkyl group is a straight chain saturated alkyl group. The alkyl group can contain up to about 3 hydroxy groups and/or the polyalkyleneoxide chain can contain up to about 10, preferably less than 5, alkyleneoxide moieties. Suitable alkyl polysaccharides are octyl, nonyldecyl, undecyldodecyl, tridecyl, tetradecyl, pentadecyl, hexadecyl, heptadecyl, and octadecyl, di-, tri-, tetra-, penta-, and hexagluco-sides, galactosides, lac-

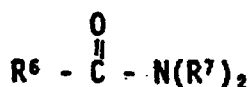
tosides, glucoses, fructosides, fructoses and/or galactoses. Suitable mixtures include coconut alkyl, di-, tri-, tetra-, and pentagluco-sides and tallow alkyl tetra-, penta-, and hexagluco-sides.

The preferred alkylpolyglycosides have the formula



wherein R^2 is selected from the group consisting of alkyl, alkylphenyl, hydroxyalkyl, hydroxyalkylphenyl, and mixtures thereof in which the alkyl groups contain from about 10 to about 18, preferably from about 12 to about 14, carbon atoms; n is 2 or 3, preferably 2; t is from 0 to about 10, preferably 0; and x is from about 1.3 to about 10, preferably from about 1.3 to about 3, most preferably from about 1.3 to about 2.7. The glycosyl is preferably derived from glucose. To prepare these compounds, the alcohol or alkylpolyethoxy alcohol is formed first and then reacted with glucose, or a source of glucose, to form the glucoside (attachment at the 1-position). The additional glycosyl units can then be attached between their 1-position and the preceding glycosyl units 2-, 3-, 4- and/or 6-position, preferably predominately the 2-position.

6. Fatty acid amide surfactants having the formula:



wherein R^6 is an alkyl group containing from about 7 to about 21 (preferably from about 9 to about 17) carbon atoms and each R^7 is selected from the group consisting of hydrogen, C_1 - C_4 alkyl, C_1 - C_4 hydroxyalkyl, and $-(C_2H_4O)_xH$ where x varies from about 1 to about 3.

Preferred amides are C_8 - C_{20} ammonia amides, monoethanolamides, diethanolamides, and isopropanolamides.

Catalyst

As noted, the present process is preferably catalyzed. Preferred catalysts suitable for use herein are selected from the group consisting of trillithium phosphate, trisodium phosphate, tripotassium phosphate, tetrasodium pyrophosphate, tetrapotassium pyrophosphate, pentasodium tripolyphosphate, pentapotassium tripolyphosphate, lithium hydroxide, sodium hydroxide, potassium hydroxide, calcium hydroxide, lithium carbonate, sodium carbonate, potassium carbonate, disodium tartrate, dipotassium tartrate, sodium potassium tartrate, trisodium citrate, tripotassium citrate, sodium basic silicates, potassium basic silicates, sodium basic aluminosilicates, potassium basic aluminosilicates, sodium methoxide, sodium ethoxide, sodium *n*-propoxide, sodium isopropoxide, sodium *t*-butoxide, potassium methoxide, potassium ethoxide, potassium *n*-propoxide, potassium isopropoxide, potassium *t*-butoxide, and mixtures thereof.

Highly preferred catalysts suitable for this invention can be selected from the group consisting of trisodium phosphate, tripotassium phosphate, sodium hydroxide, potassium hydroxide, calcium hydroxide, sodium carbonate, potassium carbonate and mixtures thereof. The most highly preferred catalysts from this group are selected from the group consisting of sodium carbonate, potassium carbonate, sodium hydroxide, potassium hydroxide, and mixtures thereof.

Suitable aluminosilicates are better illustrated by the zeolites, especially Zeolite Na-A. Such siliceous catalysts are all preferably small size, such as from about 1-10 micron.

More generally, "catalyst" in the context of the present invention refers to a compound or mixture which significantly enhances the rate of formation of formula (I) compounds from N-alkylglucamine and fatty ester. This is a unique amidation reaction, since there are also present potentially reactive esterifiable or cyclizable hydroxyl groups in the N-alkylglucamine. More specifically still, the enhancement achieved by the catalyst includes at the lower end of the preferred temperatures of the process, forming the desired formula (I) compounds more rapidly than would otherwise be possible, and at the higher end of the preferred temperatures of the process, forming (I) extremely quickly, e.g., within a matter of a few minutes. Catalysts herein assist amidation without concurrently catalyzing unwanted side-reactions, such as cyclization and esteramide formation, to any appreciable extent under the reaction conditions: that is to say, the catalysts are selective.

The catalysts differ from any impurity compounds, such as water, soap or fatty acid, which might be inherent in the process when it is carried out using industrial grades of the primary reactants. Thus

"catalyst" always refers to essential materials for the present process, which need to be added to the N-alkylglucamine and fatty ester for the invention to operate.

"Catalyst" is defined in a practical manner as referring to complete, stable chemical substances or mixtures thereof. The individual catalyst compounds or mixtures are available in commerce or can be made by literature methods. They can be weighed out and added to the other reactants in the instant process. Thus, catalysts herein are not defined as "active species" in the style of mechanistic discussions by chemists. Such species might or might not actually be generated *in-situ* in the reaction mixtures of the instant process. The invention is not to be considered limited by any such theory of catalyst operation.

Catalysts herein are generally compatible with the process. They do not contain highly reactive, grossly unsatisfactory functional groups such as peroxy, chloro, iodo, ketene, and so forth of the sort which ordinarily skilled chemists will generally recognize as not desirable for any elevated temperature amidation reactions of the present kind.

Catalysts herein preferably have particulate form: typically, they take the form of powders, as are generally available in commerce. Finely divided powders are generally preferred. Small particle sizes, such as a size of less than 50 micron or 1-10 micron can be very useful.

Catalysts herein preferably have substantially anhydrous form: hydrated salts may be usable but are significantly less preferred than anhydrous catalyst; aqueous catalyst solutions are excluded unless water is removed as further illustrated in the context of hydroxide catalysts hereinafter. Admission of water would lead to formation of fatty acids which are preferably minimized herein.

Highly preferred catalysts herein generally are water-soluble catalysts having monovalent cations: such preferred catalysts are more particularly illustrated by lithium carbonate, sodium carbonate and potassium carbonate.

Although alkali metal hydroxide catalysts are quite usable, they are not as preferred, at least on grounds of relatively difficult handling, as compared with the carbonates. A preferred sequence of steps when handling hydroxide catalyst comprises impregnating the N-alkylglucamine with an aqueous solution or methanolic solution, preferably an aqueous solution, of the hydroxide catalyst. In more detail, one such method for using sodium hydroxide or potassium hydroxide as catalysts in the instant process comprises adding the hydroxide as an aqueous solution to the N-alkylglucamine, typically at room temperature; drying the resulting intimate mixture of N-alkylglucamine and hydroxide catalyst under mild conditions, e.g., at 60°C-130°C under vacuum, then reacting the dried intimate mixture with the fatty ester.

In general, the levels of catalyst used in the instant process are of about 0.5 mole % or higher, e.g., from about 0.5 mole % to about 50 mole % based on N-alkylglucamine. Preferred levels are from about 1 mole % to about 20 mole %, even more preferably from about 2 mole % to about 10 mole %.

In one highly preferred embodiment of the instant process, the catalyst is anhydrous potassium carbonate powder, at a level of from about 2 mole % to about 5 mole % on N-alkylglucamine.

Mixed catalysts are also useful herein, as illustrated by mixtures of sodium carbonate and potassium carbonate in varying proportions.

Particularly useful as catalyst herein is porous granular anhydrous potassium carbonate, though porosity is not essential when the catalyst takes the form of a fine powder.

It will immediately be apparent that the instant process is remarkable in identifying much milder and more convenient catalysts than sodium methoxide for improved linear glucamide surfactant formation.

N-alkylglucamine

Various N-alkylglucamines are useful in the practice of this invention. Such N-alkylglucamines are more specifically illustrated by N-methylglucamine, N-ethylglucamine, N-propylglucamine and N-butylglucamine. The preferred N-alkylglucamines are derived from D-glucose, e.g., N-methyl-D-glucamine.

The N-alkylglucamine can be pure or can be industrial grade provided that certain specifications are adhered to. Thus, industrial grade N-alkylglucamine may contain sugars such as glucose, sorbitol or other relatively inert by-products from N-alkylglucamine manufacture (typically 0-5 weight %). However, industrial grade N-alkylglucamines for this process should have low or negligibly small contents, in parts per million, (e.g., 0-20 ppm, preferably 0-2 ppm) of transition metals such as nickel if the formation of color bodies or other adverse effects are to be minimized. It has been found that industrial grade N-alkylglucamines commonly contain such transition metals as a result of their manufacture by transition metal-catalyzed reductive amination of glucose or corn syrup.

The N-alkylglucamines used herein are generally of good color, preferably pure white with no trace of colored impurities. Also, the N-alkylglucamine is preferably substantially anhydrous.

One convenient check for N-alkylglucamine quality involves simply heating a sample to the temperature of the present process, e.g., 140°C. Industrial grade N-alkylglucamines which quickly darken at such a temperature are very likely to contain unacceptable levels of impurity.

It is usually possible to clean up industrial grade N-alkylglucamines which fail initial quality checks, either by washing them with methanol/water or by recrystallizing them. A useful method for lowering the level of nickel is to filter a solution of the N-alkylglucamine through basic silica gel or bleaching earth.

Fatty Ester

The fatty ester used herein is preferably a fatty (e.g., C₁₂-C₂₀) methyl ester or triglyceride which is highly saturated, although other esters, such as saturated and mixed saturated/unsaturated fatty ethyl esters, fatty monoglycerides or fatty diglycerides can also be used. Suitable fatty esters include those illustrated by Schwartz, *supra*. Preferred fatty esters are better illustrated by lauric methyl ester, palmitic methyl ester or, if a mixture of chain lengths is used, coconut methyl ester. When industrial grade fatty esters are used, excellent results are achieved with the following:

Procter & Gamble CE-1270 Methyl Ester:	
Acid Value:	0.2
Iodine Value:	0
Moisture (% K.F)	0.03
Color (% transmittance at 460 nm)	97
Chain Length (GC, Wt%)	
C 10	0.4
C 12	73.0
C 14	25.9
C 16	0.2

Procter & Gamble CE-1218 Methyl Ester:	
Acid Value:	0.6
Saponification Value	242
Iodine Value:	9.4
Moisture (% K.F)	0.04
Color (% transmittance at 460 nm)	97
Chain Length (GC, Wt%)	
C 10	0.5
C 12	57.4
C 14	20.7
C 16	10.0
C 18	1.9
C 18 1-unsaturated	7.3
C 18 2-unsaturated	1.5
C 20	0

Substantially pure lauric methyl ester and palmitic methyl ester can of course also be used. Preferred industrial grade fatty ester for use in the present process typically contains 10 ppm or lower, better 0 ppm of heavy metals, and a free fatty acid content of 5 weight % or lower, preferably 1 weight % or lower.

Reaction Conditions

In general, the temperatures, pressures, times and proportions of the two principal reactants can be as follows. Temperatures in the present process are normally from about 120°C to about 200°C, more preferably about 138°C or higher. Reaction periods in the process are normally from about 0.5 minutes to

about 5 hours.

The invention does, however, identify preferred temperatures and reaction periods depending on whether the process is carried out in a continuous mode or a noncontinuous mode. Thus, in a noncontinuous mode a preferred temperature is from about 138°C to about 170°C and the corresponding period is from about 20 minutes to about 90 minutes. In a continuous mode, a preferred temperature is from about 160°C to about 200°C and a corresponding period is from about 0.5 minutes to about 10 minutes. Generally, higher temperatures are accompanied by the shorter times. Moreover, higher catalyst levels speed up the process so that shortest times are associated with the higher catalyst levels.

Referring to the art, Schwartz favors high temperatures such as those of the order of 170°C, one must assume because he did not have suitable catalysts: such temperatures, especially with relatively long reaction times, e.g., an hour or more, can significantly increase by-product formation, especially cyclization.

EP-A 285,768 has slow heating to relatively low temperatures, specifically 135°C: this may be due to the need to avoid charring with the sodium methoxide catalyst, and is relatively uneconomic.

It is preferred to conduct the present process in the absence of air or oxygen. This is conveniently accomplished by maintaining an inert atmosphere of nitrogen or argon over the reaction mixtures, or by applying vacuum, the latter especially in the later stages of the process.

When operating uncatalyzed processes, e.g., using the Schwartz process, at such moderate temperatures, very long reaction times (typically several hours) are required, rendering the uncatalyzed process at such temperatures rather unattractive due to long reactor hold-ups. For example, at about 150°C, the Schwartz process typically requires about 7-8 hours.

In contrast, when operating according to the present catalyzed, phase-transfer assisted process in the above-indicated preferred temperature ranges, e.g., at about 150°C in a batch mode at a typical catalyst level of about 2 mole %, reaction times need be no more than 90 minutes. Continuous processing with much shorter reaction times is of course possible.

According to the present invention, it is highly preferred that the reaction should be checked for completion by any suitable technique, e.g., by watching for the end of methanol evolution, by thin layer chromatography (see hereinafter), or by gas chromatography, so that it can be stopped by cooling just as soon as it is complete.

The present process is generally carried out using stirring to mix the reactants properly. It should be appreciated that at the outset of the instant process, the reaction mixtures are three-phase, the phases comprising a liquid fatty ester phase, a molten N-alkylglucamine phase and a solid catalyst phase. Therefore it can be appreciated how important it is to properly mix the reactants. Best results are generally achieved in reactors designed for effective heat and mass transfer. The use of baffles in the reactor can be advantageous.

Relative proportions of N-alkylglucamine and fatty ester are generally as disclosed by Schwartz, U.S. Patent 2,703,798, incorporated by reference. Typical proportions are approximately equimolar for best results.

Processes herein generally do not need, and are preferably conducted without, added solvents and therefore generally differ from the art-disclosed process of Hildreth *supra*. The instant process is however tolerant of, and can even benefit from, the presence of varying amounts of methanol, ethanol, and glycerin, which are actually process by-products. Glycols such as ethylene glycol, 1,2-propylene glycol and glycerin can be added early in the process, typically in relatively small, nonsolvent amounts, as activators.

Vacuum is optionally applied during the present process, particularly as the process goes toward completion, for efficient removal of volatiles (especially methanol) when generated in the process. Use of vacuum can also improve product odor. When the fatty ester is a triglyceride, glycerin is formed during the process instead of methanol. The glycerin does not have to be removed from product of the process in all cases, since it can be useful in the final product or derivative thereof (a typical example being a bar soap stamped out from product of the invention).

It is possible to use the catalyst both for its catalytic function and for other desirable functions, to have it as an integral part of the final product. Thus the process has advantages of manufacturing simplicity and is especially valuable when the catalyst is known to be useful for its laundry detergent function. What has not hitherto been appreciated is to use as catalysts for linear glucamide formation materials which can later function in the product to modify its desirable properties, such as the water-dispersability of linear glucamide-containing particles. Water-dispersibility can be modified, especially upwardly, when the catalyst or phase transfer agent is highly water-soluble or capable of lowering the Krafft boundary of the glucamide. This is highly desirable for manufacture of low-temperature or all-temperature detergents.

Accordingly the new approach of the present invention results in an economically attractive option for making unique granular detergent intermediates, such as particles containing intimate mixtures of linear

glucamide surfactants with the catalytically active or phase transfer-active materials. Such particles are easily dispersed in water and offer increased manufacturing convenience to detergent formulators since they can be directly dry-mixed with other detergent ingredients rather than requiring additional premix process steps.

5 The simplicity of the present process makes it widely useful both nationally and abroad, e.g., in less sophisticated industrial economies.

The process of the invention has many alternate embodiments. Thus a number of addition sequences can be used. In one such sequence, a process is encompassed comprising the following ordered sequence of steps: (a) preheating the fatty ester to the above-identified temperatures; (b) adding the N-alkylglucamine
10 at said temperature and mixing to the extent needed to form a two-phase liquid/liquid mixture; (c) adding preformed reaction product with stirring; (d) mixing in the catalyst; and (e) stirring at said temperature until the end of the above-identified reaction period.

In yet another sequence, the following steps are carried out:

(a) preheating a solid/liquid mixture of N-alkylglucamine and fatty ester to the above-identified temperatures
15 with mixing, thereby melting the N-alkylglucamine and concurrently mixing it with the fatty ester in the shortest practical time; (b) at said temperatures, adding preformed product with stirring, said preformed product providing linear glucamide surfactant for phase transfer and concurrently providing a portion of the catalyst; the total amount of said preformed product added as combined phase transfer agent and catalyst being from about 2% to about 20% by weight of the reactants; (c) at said temperature, adding additional
20 catalyst in an amount sufficient to attain the above-identified catalyst levels; and (d) continuing to react with stirring until the end of the reaction period. To such a sequence can be added a step (e): mixing the product of step (d) in molten form with a large excess of said catalyst, thereby forming a linear glucamide surfactant/alkaline detergency builder mixture.

25 EXAMPLE I

Although a skilled chemist can vary apparatus configuration, one suitable apparatus for use herein comprises a three-liter four-necked flask fitted with a motor-driven paddle stirrer and a thermometer of length sufficient to contact the reaction medium. The other two necks of the flask are fitted with a nitrogen
30 sweep and a wide-bore side-arm (caution: a wide-bore side-arm is important in case of very rapid methanol evolution) to which is connected an efficient collecting condenser and vacuum outlet. The latter is connected to a nitrogen bleed and vacuum gauge, then to an aspirator and a trap. A 500 watt heating mantle with a variable transformer temperature controller ("Variac") used to heat the reaction is so placed on a lab-jack that it may be readily raised or lowered to further control temperature of the reaction.

35 N-methylglucamine (195 g., 1.0 mole, Aldrich, M4700-0) and methyl laurate (Procter & Gamble CE 1270, 220.9 g, 1.0 mole) are placed in the flask. The solid/liquid mixture is heated with stirring under a nitrogen sweep to form a melt (approximately 25 minutes). When the melt temperature reaches 145 °C, preformed product (40 g.) and catalyst (anhydrous powdered sodium carbonate, 10.5 g., 0.1 mole, J. T. Baker) are added. The nitrogen sweep is shut off and the aspirator and nitrogen bleed are adjusted to give
40 5 inches (5/31 atm.) Hg. vacuum. From this point on, the reaction temperature is held at 150 °C by adjusting the Variac and/or by raising or lowering the mantle.

Within 7 minutes, first methanol bubbles are sighted at the meniscus of the reaction mixture. A vigorous reaction soon follows. Methanol is distilled over until its rate subsides. Then adjust vacuum to give about 10 inches Hg. (10/31 atm.) vacuum. The vacuum is increased approximately as follows (in inches Hg at
45 minutes): 10 at 3, 20 at 7, 25 at 10. 11 minutes from the onset of methanol evolution, heating and stirring are discontinued co-incident with some foaming. Analysis by TLC (see after) shows that at this point, the process is complete. The product is cooled and solidifies.

EXAMPLE II

50

A baffled stainless steel jacketed reactor is provided. The reactor has a pressurizable steam-jacket and is equipped with a motor-driven stirrer, temperature measuring means, nitrogen/vacuum inlet/outlets similar to the arrangement in Example I, and a wide-bore side-arm connected to an efficient methanol collection condenser and trap. The reactor has a sight-glass closable port and a ball-valve closable port for reactant
55 addition and can be drained through a third port at the base. Steam can be passed through the jacket at controllable pressures of up to 150 psi or higher so that the reactor can quickly be heated to controlled temperatures up to 150 °C or higher.

Fatty methyl ester (41.5 lbs., 18.85 kg., 85.68 gram moles, Procter & Gamble CE-1270 Methyl Ester) is charged to the clean, nitrogen-purged reactor through the sight-glass port. The stirrer is set in motion and steam at 50 psi. is used to heat the stirred methyl ester to 100 °C (212 °F). Now N-methylglucamine (36.8 lbs., 16.71 kg., 85.68 gram moles, 99% + purity, heavy metal content < 2 ppm, Aldrich or Merck) is added through the sight glass port. The ports are closed and the reactor is heated at ambient pressure under nitrogen with stirring using 70 psi. steam so that the temperature reaches 130 °C (266 °F) and substantially all the N-methylglucamine has dissolved or melted.

A partial vacuum of 46 cm Hg. is now applied.

Substantially pure $\text{CH}_3(\text{CH}_2)_{10}\text{C}(\text{O})\text{N}(\text{CH}_3)\text{CH}_2(\text{CHOH})_4\text{CH}_2\text{OH}$, 7.8 lbs. (3548 g.) is added as phase transfer agent and catalyst (potassium carbonate anhydrous powder; 50 microns, 236 grams, 1.71 gram mole, LCP Chemicals) is added under nitrogen through the ball valve port when the reactor internal temperature is about 138 °C (280 °F).

The reaction is continued by stirring and holding the vacuum in the range 40 - 60 cm Hg. for about 90 minutes, the vacuum being adjusted as needed to control foaming.

The steam pressure is released and the contents of the reactor are drained as a melt onto a flat steel surface where solidification can occur. After holding at about 20 °C for a period sufficient to allow embrittlement, e.g., 18 hours, the product is broken into flakes and is ground to a powder.

EXAMPLE III

The procedure of Example II is repeated, with the exception that the reaction time is about 30 minutes and the product is secured as a concentrated aqueous mixture by slow addition of water to the rapidly stirred product in the reactor, starting at temperatures just above the melting-point.

EXAMPLE IV

The procedure of Example II is repeated except that an equimolar amount of Procter & Gamble Methyl Ester CE-1295 is substituted for the CE-1270 Ester.

EXAMPLE V

The procedure of Example I is repeated except that the fatty methyl ester is substituted by an equimolar amount of coconut oil.

EXAMPLE VI

The procedure of Example I is repeated except that the molten product is poured onto 1000 grams of sodium carbonate anhydrous powder preheated to 150 °C and thoroughly mixed with a cake-beater while slowly cooling to about 25 °C. The product is a granule which is useful as an intermediate for formulating granular laundry detergents. It can also be used directly for washing fabrics in an aqueous laundry bath, with excellent results.

Thin Layer Chromatography (TLC) Analysis

Processes herein can be monitored by TLC using Silica Gel GF plates (Analtech) and a solvent system consisting of CHCl_3 : MeOH: NH_4OH at a volume ratio of 80:23:3. Plates are preconditioned in 2:1 v/v CHCl_3 :MeOH prior to use to eliminate discoloration at the solvent front.

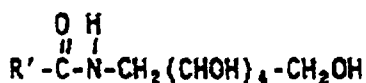
A typical procedure for analysis involves preparing in methanol a 5-10 wt.% solution of a sample from the process. The plates are spotted with the solution, dried, and processed in the 80:23:3 solvent solution for about 10-15 minutes. Plates are removed from the processing chamber and heat-dried. Upon cooling, the plates are dipped in a 10 wt.% solution of phosphomolybdic acid and allowed to dry. The plates are then placed on hot-plate at moderate heat for 5-10 minutes until the spots are pronounced. Overheating can cause discoloration of plate and fading of spots. An iodine chamber treatment can be used instead of the phosphomolybdic acid dip but staining is less permanent. Typical RF factors are:

COMPOUND	RF
Unreacted N-methyl-D-glucamine	0.0
Fatty acid impurity	0.2
Formula (I) compound	0.3
Cyclic by-product from dehydration of formula (I) compound	0.5
Esteramide by-product	0.7
Unreacted fatty ester	0.9

While the foregoing disclosure generally relates to a solventless method for preparing glucamine-derived surfactants, it is to be understood that variations are available which do not depart from the spirit and scope of this invention. Thus, sugars, especially reducing sugars such as fructose, galactose, mannose, maltose and lactose, as well as sugar sources such as high dextrose corn syrup, high fructose corn syrup and high maltose corn syrup, and the like, can be used to prepare the polyhydroxyamine component (i.e., to replace glucamine) of the reaction. Likewise, a wide variety of fats and oils (triglycerides) can be used herein in addition to the coconut oil exemplified above. For example, fats and oils such as soybean oil, cottonseed oil, sunflower oil, tallow, lard, safflower oil, corn oil, canola oil, peanut oil, fish oil, rapeseed oil, and the like, or hardened (hydrogenated) forms thereof, can be used as the source of triglycerides for use in the present process.

Claims

1. A process for manufacturing a linear glucamide surfactant characterized in that it comprises reacting an N-alkylglucamine with a fatty ester in the presence of a phase transfer agent.
2. A process according to Claim 1 wherein said phase transfer agent comprises a member selected from the group consisting of nonionic surfactants, preferably comprising one or more nonionic surfactants selected from saturated fatty alcohol polyethoxylates, alkylpolyglycosides, linear glucamide surfactants and mixtures thereof.
3. A process according to Claim 2 wherein there is additionally present a catalyst, and wherein said N-alkylglucamine is selected from N-methylglucamine, N-ethylglucamine, N-propylglucamine and N-butylglucamine and wherein said fatty ester is selected from fatty methyl esters, fatty ethyl esters and fatty triglycerides.
4. A process according to Claim 3 wherein said catalyst is selected from the group consisting of sodium carbonate, potassium carbonate and mixtures thereof, the amount of said catalyst is from 0.5 mole percent to 50 mole percent on N-alkylglucamine, conversion of N-alkylglucamine to compounds having linear structure of formula



wherein R is the alkyl residue of the glucamine and R' is the residue of the fatty ester is 70, preferably 80, mole percent or higher on N-alkylglucamine, and conversion of N-alkylglucamine to cyclic glucamide or esteramide by-products is 15, preferably 10, mole percent or lower.

5. A process according to Claim 4 wherein said N-alkylglucamine is N-methyl-D-glucamine, said fatty ester is selected from saturated fatty methyl esters and fatty triglycerides, the N-alkylglucamine and fatty ester are in approximately equimolar proportions as determined by the number of moles of fatty carbonyl moieties of the fatty ester per mole of N-alkylglucamine, and said catalyst is sodium carbonate.
6. A process according to Claim 5 wherein said N-alkylglucamine is industrial grade N-alkylglucamine having a heavy metal content of 20 ppm or lower and a free sugar content of 5 weight percent or lower.

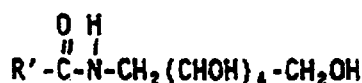


COMPOUND	RF
Unreacted N-methyl-D-glucamine	0.0
Fatty acid impurity	0.2
Formula (I) compound	0.3
Cyclic by-product from dehydration of formula (I) compound	0.5
Esteramide by-product	0.7
Unreacted fatty ester	0.9

While the foregoing disclosure generally relates to a solventless method for preparing glucamine-derived surfactants, it is to be understood that variations are available which do not depart from the spirit and scope of this invention. Thus, sugars, especially reducing sugars such as fructose, galactose, mannose, maltose and lactose, as well as sugar sources such as high dextrose corn syrup, high fructose corn syrup and high maltose corn syrup, and the like, can be used to prepare the polyhydroxyamine component (i.e., to replace glucamine) of the reaction. Likewise, a wide variety of fats and oils (triglycerides) can be used herein in addition to the coconut oil exemplified above. For example, fats and oils such as soybean oil, cottonseed oil, sunflower oil, tallow, lard, safflower oil, corn oil, canola oil, peanut oil, fish oil, rapeseed oil, and the like, or hardened (hydrogenated) forms thereof, can be used as the source of triglycerides for use in the present process.

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3. A process according to Claim 2 wherein there is additionally present a catalyst, and wherein said N-alkylglucamine is selected from N-methylglucamine, N-ethylglucamine, N-propylglucamine and N-butylglucamine and wherein said fatty ester is selected from fatty methyl esters, fatty ethyl esters and fatty triglycerides.
4. A process according to Claim 3 wherein said catalyst is selected from the group consisting of sodium carbonate, potassium carbonate and mixtures thereof, the amount of said catalyst is from 0.5 mole percent to 50 mole percent on N-alkylglucamine, conversion of N-alkylglucamine to compounds having linear structure of formula



wherein R is the alkyl residue of the glucamine and R' is the residue of the fatty ester is 70, preferably 80, mole percent or higher on N-alkylglucamine, and conversion of N-alkylglucamine to cyclic glucamide or esteramide by-products is 15, preferably 10, mole percent or lower.

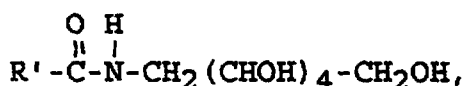
5. A process according to Claim 4 wherein said N-alkylglucamine is N-methyl-D-glucamine, said fatty ester is selected from saturated fatty methyl esters and fatty triglycerides, the N-alkylglucamine and fatty ester are in approximately equimolar proportions as determined by the number of moles of fatty carbonyl moieties of the fatty ester per mole of N-alkylglucamine, and said catalyst is sodium carbonate.
6. A process according to Claim 5 wherein said N-alkylglucamine is industrial grade N-alkylglucamine having a heavy metal content of 20 ppm or lower and a free sugar content of 5 weight percent or lower.



7. A process according to Claim 6 wherein said fatty ester is industrial grade fatty ester having a heavy metal content of 10 ppm or lower and a free fatty acid content of 5 weight percent or lower.
8. A process according to Claim 7 wherein said N-alkylglucamine, fatty ester and catalyst are reacted in a noncontinuous mode as a mixture at a temperature of from 138°C to 170°C for a period of from 20 minutes to 90 minutes.
9. A process according to Claim 8 wherein the amount of said phase transfer agent is from 0.5% to 20% of the total weight of the reactants including catalyst.
10. A process according to Claim 9 comprising the following ordered sequence of steps:
 - (a) preheating a solid/liquid mixture of said N-alkylglucamine and fatty ester to said temperature with mixing, thereby melting said N-alkylglucamine and concurrently mixing it with said fatty ester in the shortest practical time;
 - (b) at said temperature, adding preformed linear alkylglucamide product with stirring, said preformed product providing said linear glucamide surfactant as the phase transfer agent and concurrently providing a portion of said catalyst; the total amount of said preformed product being from 2% to 20% by weight of the reactants;
 - (c) at said temperature, adding additional catalyst in an amount sufficient to attain said catalyst level;
 - (d) continuing to react with stirring until the end of said reaction period, preferably at a temperature of 160°C to 180°C for a period of from 0.5 minutes to 10 minutes.

Patentansprüche

1. Verfahren zur Herstellung eines grenzflächenaktiven Mittels auf Basis von linearem Glucamid, dadurch gekennzeichnet, daß es das Umsetzen eines N-Alkylglucamins mit einem Fettester in Gegenwart eines Phasentransfer-Mittels umfaßt.
2. Verfahren nach Anspruch 1, worin das genannte Phasentransfer-Mittel ein von der aus nichtionischen grenzflächenaktiven Mitteln bestehenden Gruppe ausgewähltes Mitglied umfaßt, welches vorzugsweise eines oder mehrere nichtionische grenzflächenaktive Mittel umfaßt, die unter gesättigten Fettalkoholpolyethoxylaten, Alkylpolyglycosiden, grenzflächenaktiven Mitteln auf Basis von linearem Glucamid und Gemischen hiervon ausgewählt sind.
3. Verfahren nach Anspruch 2, worin zusätzlich ein Katalysator vorliegt, und worin das genannte N-Alkylglucamin unter N-Methylglucamin, N-Ethylglucamin, N-Propylglucamin und N-Butylglucamin ausgewählt ist und worin der genannte Fettester unter Fettmethylestern, Fettethylestern und Fetttriglyceriden ausgewählt ist.
4. Verfahren nach Anspruch 3, worin der genannte Katalysator von der aus Natriumcarbonat, Kaliumcarbonat und Gemischen hiervon bestehenden Gruppe ausgewählt ist, die Menge an dem genannten Katalysator von 0,5 Mol-% bis 50 Mol-% an N-Alkylglucamin beträgt, die Umwandlung von N-Alkylglucamin zu Verbindungen mit der linearen Struktur der Formel



- worin R den Alkylrest des Glucamins darstellt und R' der Rest des Fettesters ist, worin R den Alkylrest des Glucamins darstellt und R' der Rest des Fettesters ist, 70 Mol-%, vorzugsweise 80 Mol-% oder mehr, an N-Alkylglucamin beträgt und die Umwandlung von N-Alkylglucamin zu cyclischen Glucamid- oder Esteramid-Nebenprodukten 15 Mol-%, vorzugsweise 10 Mol-% oder weniger, beträgt.
5. Verfahren nach Anspruch 4, worin das genannte N-Alkylglucamin N-Methyl-D-glucamin ist, der genannte Fettester unter gesättigten Fettmethylestern und Fetttriglyceriden ausgewählt ist, das N-Alkylglucamin und der Fettester in ungefähr äquimolaren Verhältnissen, bestimmt durch die Anzahl der Mol an Fettcarbonylresten des Fettesters pro Mol N-Alkylglucamin, vorliegen und der genannte Katalysator

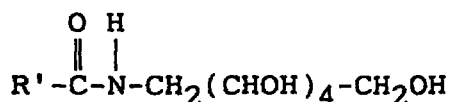


Natriumcarbonat ist.

6. Verfahren nach Anspruch 5, worin das genannte N-Alkylglucamin N-Alkylglucamin technischer Qualität mit einem Schwermetallgehalt von 20 ppm oder weniger und einem Gehalt an freiem Zucker von 5 Gew.-% oder weniger ist.
7. Verfahren nach Anspruch 6, worin der genannte Fettester ein Fettester technischer Qualität mit einem Schwermetallgehalt von 10 ppm oder weniger und einem Gehalt an freier Fettsäure von 5 Gew.-% oder weniger ist.
8. Verfahren nach Anspruch 7, worin das genannte N-Alkylglucamin der Fettester und der Katalysator in einer diskontinuierlichen Weise als ein Gemisch bei einer Temperatur von 138°C bis 170°C während einer Dauer von 20 Minuten bis 90 Minuten umgesetzt werden.
9. Verfahren nach Anspruch 8, worin die Menge des genannten Phasentransfer-Mittels von 0,5% bis 20% des Gesamtgewichtes der Reaktanten einschließlich des Katalysators beträgt.
10. Verfahren nach Anspruch 9, welches die folgende geordnete Anfolge von Schritten umfaßt:
 - (a) vorheriges Erhitzen eines Feststoff/Flüssigkeits-Gemisches aus dem genannten N-Alkylglucamin und Fettester auf die genannte Temperatur unter Vermischen, wodurch das genannte N-Alkylglucamin geschmolzen und gleichzeitig mit dem genannten Fettester in der kürzesten tatsächlichen Zeitdauer vermischt wird;
 - (b) Zusetzen des zuvor geformten linearen Alkylglucamidproduktes bei der genannten Temperatur unter Rühren, welches genannte zuvor geformte Produkt das genannte grenzflächenaktive Mittel auf Basis von linearem Glucamid als Phasentransfer-Mittel liefert, und gleichzeitiges Bereitstellen eines Teils des genannten Katalysators; wobei die Gesamtmenge des genannten zuvor geformten Produktes von 2 Gew.-% bis 20 Gew.-% der Reaktanten beträgt;
 - (c) Zusetzen von zusätzlichem Katalysator bei der genannten Temperatur in einer Menge, welche ausreicht, um die genannte Katalysatormenge zu erzielen;
 - (d) Fortsetzen der Umsetzung unter Rühren bis zum Ende der genannten Reaktionsdauer, vorzugsweise bei einer Temperatur von 160°C bis 180°C während einer Dauer von 0,5 Minuten bis 10 Minuten.

Revendications

1. Procédé de fabrication d'un tensio-actif à base de glucamide linéaire caractérisé en ce qu'il consiste à faire réagir une N-alkylglucamine avec un ester gras en présence d'un agent de transfert de phase.
2. Procédé selon la revendication 1, dans lequel ledit agent de transfert de phase comprend un élément choisi dans le groupe formé par les tensio-actifs non ioniques, comprenant de préférence un ou plusieurs tensio-actifs non ioniques choisis parmi les polyéthoxylates d'alcool gras saturés, les alkylpolyglycosides, les tensio-actifs à base de glucamide linéaire et leurs mélanges.
3. Procédé selon la revendication 2, dans lequel un catalyseur est de plus présent, et dans lequel ladite N-alkylglucamine est choisie parmi la N-méthylglucamine, la N-éthylglucamine, la N-propylglucamine et la N-butylglucamine et dans lequel ledit ester gras est choisi parmi les esters méthyliques gras, les esters éthyliques gras et les triglycérides gras.
4. Procédé selon la revendication 3, dans lequel ledit catalyseur est choisi dans le groupe formé par le carbonate de sodium, le carbonate de potassium et leurs mélanges, la quantité dudit catalyseur est de 0,5 pourcent en moles à 50 pourcent en moles par rapport à la N-alkylglucamine, le taux de conversion de la N-alkylglucamine en composés ayant une structure linéaire de formule





dans laquelle R est le résidu alkyle de la glucamine et R' est le résidu de l'ester gras, est de 70, de préférence 80 pourcent en moles ou plus par rapport à la N-alkylglucamine, et le taux de conversion de la N-alkylglucamine en sous-produits de glucamide ou d'estéramide cyclique, est de 15, de préférence 10 pourcent en moles ou moins.

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5. Procédé selon la revendication 4, dans lequel ladite N-alkylglucamine est la N-méthyl-D-glucamine, ledit ester gras est choisi parmi les esters méthyliques gras saturés et les triglycérides gras, la N-alkylglucamine et l'ester gras sont dans des proportions approximativement équimolaires, déterminées par le nombre de moles de fractions de type carbonyle gras de l'ester gras par mole de N-alkylglucamine, et ledit catalyseur est le carbonate de sodium.

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6. Procédé selon la revendication 5, dans lequel ladite N-alkylglucamine est une N-alkylglucamine de qualité industrielle ayant une teneur en métal lourd de 20 ppm ou moins et une teneur en sucre libre de 5 pourcent en poids ou moins.

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7. Procédé selon la revendication 6, dans lequel ledit ester gras est un ester gras de qualité industrielle ayant une teneur en métal lourd de 10 ppm ou moins et une teneur en acide gras libre de 5 pourcent en poids ou moins.

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8. Procédé selon la revendication 7, dans lequel ladite N-alkylglucamine, l'ester gras et le catalyseur sont mis à réagir dans un mode discontinu sous forme de mélange à une température comprise entre 138°C et 170°C pendant une durée comprise entre 20 minutes et 90 minutes.

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9. Procédé selon la revendication 8, dans lequel la quantité dudit agent de transfert de phase est de 0,5% à 20% du poids total des réactifs incluant le catalyseur.

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10. Procédé selon la revendication 9, comprenant dans l'ordre la séquence suivante des étapes consistant:
(a) à préchauffer un mélange solide/liquide de ladite N-alkylglucamine et de l'ester gras à ladite température tout en mélangeant, fondant ainsi ladite N-alkylglucamine et la mélangeant simultanément avec ledit ester gras dans la durée de mise en oeuvre la plus courte;

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(b) à ladite température, à ajouter le produit de type alkylglucamide linéaire préformé tout en mélangeant, ledit produit préformé fournissant ledit tensio-actif à base de glucamide linéaire sous forme d'agent de transfert de phase et fournissant simultanément une partie dudit catalyseur; la quantité totale dudit produit préformé étant comprise entre 2% et 20% en poids des réactifs;

(c) à ladite température, à ajouter un catalyseur supplémentaire en une quantité suffisante pour atteindre ledit niveau catalytique;

(d) à continuer la réaction tout en agitant jusqu'à la fin de ladite durée réactionnelle, de préférence à une température comprise entre 160°C et 180°C pendant une durée comprise entre 0,5 minutes et 10 minutes.

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