$F / (\pi D \times N) \leq 1500$ kg/(h·m) (F1) .

3. The manufacturing method of the hydrogenated petroleum resin according to claim 1 or 2, wherein

the hydrogenated petroleum resin obtained by the volatile-component removal step has a softening point in a range from 90 degrees C to 160 degrees C.

4. The manufacturing method of the hydrogenated petroleum resin according to claim 2, wherein

the average diameter (D) of the flow path is in a range from 0.001 m (1 mm) to 0.02 m (20 mm).

5. The manufacturing method of the hydrogenated petroleum resin according to claim 2, wherein

the number (N) of the flow path is in a range from 1 to 100000.

6. The manufacturing method of the hydrogenated petroleum resin according to any one of claims 1 to 5, wherein

the reaction mixture has a viscosity in a range from 0.01 Pa·s to 1.0 Pa·s at a temperature in the volatile-component removal step, the viscosity being measured by a method according to JIS Z8803.

7. The manufacturing method of the hydrogenated petroleum resin according to any one of claims 1 to 6, wherein

the heater is configured to heat the reaction mixture to a range from 100 degrees C to 350 degrees C.

8. The manufacturing method of the hydrogenated petroleum resin according to any one of claims 1 to 7, wherein

the pressuring device is configured to pressurize the reaction mixture to 0.1 MPaG or more.

9. The manufacturing method of the hydrogenated petroleum