CLAIMS:

1. A ~~supported~~ catalyst comprising a zeolite having a silica to alumina molar ratio of 500 or less, a first metal oxide binder having a crystallite size greater than 200 Å and a second metal oxide binder having a crystallite size less than 100 Å, wherein the second metal oxide binder is present in an amount less than 15 wt% of the total weight of the catalyst, wherein said zeolite is selected from ZSM-5, EU-1, ZSM-35, ZSM-11, ZSM-23, ZSM-57, NU-87, ZSM-22, EU-2, EU-11, ZBM-30, ZSM-48, ZSM-50, MCM-22, MCM-49, MCM-56 and combinations thereof.

2. The catalyst of claim 1, wherein the second metal oxide binder is present in an amount from 2 wt% to 10 wt% of the total weight of the catalyst.

3. The catalyst of claim 1, wherein the second metal oxide binder has a crystallite size less than 80 Å.

4. The catalyst of claim 1, wherein the first metal oxide binder is present in an amount from 10 wt% to 60 wt% of the total weight of the catalyst.

5. The catalyst of claim 1, wherein the metal oxide of each of the first and second metal oxide binders is selected from silica, alumina, titania, zirconia, and silica-alumina.

6. The catalyst of claim 1, wherein the zeolite has a silica to alumina molar ratio of 200 or less.

7. The catalyst of claim 1, wherein the zeolite has a silica to alumina molar ratio of 100 or less.

8. The catalyst of claim 1, wherein said zeolite has 10-membered ring pores.

9. The catalyst of claim 1, wherein said zeolite has unidirectional 10-membered ring pores.

~~10. The catalyst of claim 1, wherein said zeolite is selected from ZSM-5, EU-1, ZSM-35, ZSM-11, ZSM-23, ZSM-57, NU-87, ZSM-22, EU-2, EU-11, ZBM-30, ZSM-48, ZSM-50, MCM-22, MCM-49, MCM-56 and combinations thereof.~~

~~11.~~10. The catalyst of claim 1, wherein said zeolite comprises ZSM-48 and/or ZSM-23.

~~12.~~11. The catalyst of claim 1 and further comprising a metal hydrogenation component supported on the catalyst.

~~13.~~12. The catalyst of claim ~~11~~ 10, wherein the metal hydrogenation component is selected from platinum, palladium and mixtures thereof.

~~14.~~13. A process for dewaxing a wax-containing hydrocarbon feed, the process comprising contacting the feed under dewaxing conditions with a ~~supported~~ catalyst comprising a zeolite having a silica to alumina molar ratio of 500 or less, a first metal oxide binder having a crystallite size greater than 200 Å and a second metal oxide binder having a crystallite size less than 100 Å, wherein the second metal oxide binder is present in an amount less than 15 wt% of the total weight of the catalyst, wherein said zeolite is selected from ZSM-5, EU-1, ZSM-35, ZSM-11, ZSM-23, ZSM-57, NU-87, ZSM-22, EU-2, EU-11, ZBM-30, ZSM-48, ZSM-50, MCM-22, MCM-49, MCM-56 and combinations thereof.

~~15.~~14. The process of claim ~~14~~ 13, wherein the second metal oxide binder is present in an amount from 2 wt% to 10 wt% of the total weight of the catalyst.

~~16.~~15. The process of claim ~~14~~ 13, wherein the second metal oxide binder has a crystallite size less than 80 Å.

~~17.~~16. The process of claim ~~14~~ 13, wherein the first metal oxide binder is present in an amount from 10 wt% to 60 wt% of the total weight of the catalyst.

~~18.~~17. The process of claim ~~14~~ 13, wherein the metal oxide of each of the first and second metal oxide binders is selected from silica, alumina, titania, zirconia, and silica-alumina.

~~19.~~18. The process of claim ~~14~~ 13, wherein the zeolite has a silica to alumina molar ratio of 200 or less.

~~20.~~19. The process of claim ~~14~~ 13, wherein the zeolite has a silica to alumina molar ratio of 100 or less.

~~21.~~20. The process of claim ~~14~~ 13, wherein the said zeolite has 10-membered ring pores.

~~22.~~21. The process of claim ~~14~~ 13, wherein the said zeolite has unidirectional 10-membered ring pores.

~~23. The process of claim 14, wherein said zeolite is selected from ZSM-5, EU-1, ZSM-35, ZSM-11, ZSM-23, ZSM-57, NU-87, ZSM-22, EU-2, EU-11, ZBM-30, ZSM-48, ZSM-50, MCM-22, MCM-49, MCM-56 and combinations thereof.~~

~~24.~~22. The process of claim ~~14~~ 13, wherein said zeolite comprises ZSM-48 and/or ZSM-23.

~~25.~~23. The process of claim ~~14~~ 13, wherein the catalyst further comprises a metal hydrogenation component supported on the catalyst.

~~26.~~24. The process of claim ~~25~~ 23, wherein the metal hydrogenation component is selected from platinum, palladium and mixtures thereof.

~~27.~~25. The process of claim ~~14~~ 13, wherein the dewaxing conditions include a temperature of from 200 to 500°C, a pressure of from 790 to 20786 kPa (100 to 3000 psig), a liquid hourly space velocity of from 0.1 to 10 hr^{-1}, and a hydrogen treat gas rate from 45 to 1780 m^3/m^3 (250 to 10000 scf/B).

~~28.~~26. The process of claim ~~14~~ 13, wherein the dewaxing conditions include a temperature of from 250 to 400°C~~.~~, a pressure of from 1480 to 17339 kPa (200 to 2500 psig), a liquid hourly space velocity of from 0.1 to 5 hr^{-1} and a hydrogen treat gas rate from 89 to 890 m^3/m^3 (500 to 5000 scf/B).