Claims:

1. A method for the storage or transport of pyrolysis oil, the method comprising:

(i) providing a holding vessel for the storage or transport of pyrolysis oil;

(ii) flushing the holding vessel with an inert gas and maintaining the vessel under an inert atmosphere;

(iii) providing a pyrolysis oil obtained from the pyrolysis of end-of-life plastics material;

(iv) contacting the pyrolysis oil with water in a wash column, wherein the water is present in amount of at least 50wt% relative to the amount of pyrolysis oil; and

(v) filling the pyrolysis oil into the holding vessel for storage or transport with a minimum time in the holding vessel of at least 24 hours;

wherein the method further comprises adding an alkylphenol derived antioxidant to the pyrolysis oil before step (v) in an amount of from 250 to 750 mg per litre of pyrolysis oil.

2. The method according to claim 1, wherein the water is present in amount of from 100wt% to 200wt%, relative to the amount of pyrolysis oil.

3. The method according to claim 1 or claim 2, wherein the pyrolysis oil is contacted with the water for an average contact time of at least 10 minutes.

4. The method according to any preceding claim, wherein the method further comprises a step of washing and drying the holding vessel before the step of flushing the holding vessel with an inert gas.

5. The method according to any preceding claim, wherein the alkylphenol derived antioxidant comprises one or more antioxidants selected from the group comprising butylated hydroxyanisole (BHA), butylated hydroxytoluene (BHT), t-butylhydroquinone (TBHQ), and propyl gallate.

6. The method according to any preceding claim, wherein the pyrolysis oil is obtained in a method comprising:

(I) providing end-of-life plastics material;

(II) melting the end-of-life plastics material to form a molten plastics material;

(III) pyrolysing the molten plastics material in an oxygen-free atmosphere to provide pyrolysis gases and a char material;

(IV) condensing the pyrolysis gases to provide the pyrolysis oil.

7. The method according to claim 6, wherein the end-of-life plastics material is melted in step (II) in a heated extruder at a temperature of from 250 to 350ºC.

8. The method according to claim 6 or 7, wherein the pyrolysis of step (III) is conducted in an optionally agitated pyrolysis reactor at a temperature of from 350 to 450ºC.

9. The method according to any of claims 6 to 8, wherein, before step (IV), the method further comprises:

passing the pyrolysis gases from step (III) into a contactor having a bank of condenser elements so that some long chain gas components condense on said elements to provide a condensed long chain material;

returning said condensed long chain material to step (III) to be further pyrolysed; and

allowing short chain gas components to exit from the contactor in gaseous form before condensing in step (IV).

10. The method according to any of claims 6 to 9, wherein step (IV) comprises distilling said pyrolysis gases from the contactor in a distillation column.