

Description

This invention relates to a method of separating dinitrogen pentoxide (N_2O_5) from its solution in nitric acid.

It is well known that dinitrogen pentoxide (N_2O_5) can be prepared at relatively low cost by the electrochemical oxidation of dinitrogen tetroxide (N_2O_4) dissolved in concentrated nitric acid. Typically, the solution of N_2O_4 in nitric acid is situated in the anode compartment of an electrochemical cell with a second solution of N_2O_4 in nitric acid present in the cathode compartment. An acid-resistant ion-exchange membrane separates the two compartments. When current is passed through the cell, N_2O_5 is formed in the anode compartment and water in the cathode compartment.

It is also known from published USSR Inventor's Certificate SU-1089047A that solid N_2O_5 can be separated from strong, 35-40wt% solutions of N_2O_5 in nitric acid produced electrochemically, by the subsequent addition to the solution of moderate amounts of liquid N_2O_4 at a temperature of -5°C to 0°C . A 1:1 by weight solvate of N_2O_5 with nitric acid precipitates from the solution, from which pure N_2O_5 can be recovered by low pressure sublimation.

One of the disadvantages of this method of N_2O_5 separation is that it requires a starting solution of N_2O_5 in nitric acid which is inefficient and costly to produce electrochemically. SU-1089047A teaches that at the temperature (typically 10°C to 15°C) of electrochemical preparation of the 35-40wt% N_2O_5 starting solution, the total ($N_2O_4 + N_2O_5$) concentration in the solution must not exceed 38-40wt% in order to suppress the unwanted formation of precipitate in the electrochemical cell itself. By simple subtraction, it can be seen that the solution from which the N_2O_5 is to be separated must contain less than 5wt% N_2O_4 . However, in practice the electrical efficiency of electrochemical N_2O_5 production decreases sharply with increasing N_2O_5 concentration and decreasing N_2O_4 concentration (especially at N_2O_4 concentrations at or below 5wt%) in the anolyte. This is due in part to leakage of N_2O_4 and water through the cell membrane from the catholyte to the anolyte and also in part to the reduced electrical conductivity of the anolyte at low N_2O_4 concentrations which decreases electrical efficiency. Such leakage can (in the case of N_2O_4 leakage) be suppressed by employing a low N_2O_4 concentration in the catholyte, but this reduces catholyte conductivity. Water leakage can be reduced but at the expense of removing it at frequent intervals from the catholyte in order to keep its concentration low.

It has now been discovered that provided the anolyte is maintained at a temperature of at least 10°C , the anolyte can contain a much higher dissolved nitrogen oxide content than has hitherto been realised so enabling more efficient electrochemical methods of N_2O_5 generation to be utilised by virtue of the anolytes' higher N_2O_4 content.

Accordingly, the present invention provides a method of separating N_2O_5 from its solution in nitric acid which comprises the steps of:

(a) preparing, by the electrochemical oxidation of N_2O_4 in nitric acid, a nitric acid solution at a temperature of at least 10°C containing at least 45wt% of dissolved ($N_2O_4 + N_2O_5$) and having a dissolved N_2O_5 :nitric acid ratio by weight of at least 1:3.

(b) cooling the acid solution to less than 8°C until an N_2O_5 solvate precipitates from solution.

The method preferably further comprises the subsequent step of

(c) recovering the N_2O_5 solvate from the acid solution, most preferably by filtration.

In order to enhance the yield of solid precipitated, the acid solution prepared in step (a) preferably contains at least 50wt% of dissolved ($N_2O_4 + N_2O_5$). A maximum dissolved ($N_2O_4 + N_2O_5$) concentration of up to about 60wt% in step (a) is achievable without the formation of a separate liquid N_2O_4 phase. In practice, a maximum ($N_2O_4 + N_2O_5$) concentration in solution of about 55wt% is recommended.

In order to ensure that premature precipitation of N_2O_5 is prevented during the electrochemical oxidation of N_2O_4 , the solution is preferably prepared in step (a) at a temperature of at least 12°C more preferably at a temperature of from 15°C to 30°C and most preferably at a temperature of from 20°C to 25°C . The solubility of N_2O_5 advantageously increases with temperature especially at high N_2O_4 concentrations in solution, although above about 25°C thermal decomposition of N_2O_5 can become a problem.

At precipitation temperatures at or above about 5°C , the concentration of both N_2O_5 and N_2O_4 in the acid must approach saturation in order to produce any N_2O_5 precipitation and even then the yield of precipitate tends to be very low. The minimum precipitation temperature is preferably at least -25°C , more preferably at least -20°C , most preferably at least -15°C . Although the amount of N_2O_5 -rich solute increases with decreasing precipitation temperature, the cost of cooling the solution also increases and at temperatures below -15°C , contamination of the precipitate with solid N_2O_4 becomes an increasing problem. For these reasons, the precipitation temperature is most preferably within the range -15°C to 0°C .

The acid solution is preferably cooled to below -5°C , more preferably below -10°C , especially where the solution contains at least 50wt% ($N_2O_4 + N_2O_5$). This is because the combined effect of cooling and solvate precipitation on such solutions is a tendency for the N_2O_4 to reach its saturation limit and form a separate liquid

phase into which the N_2O_5 will migrate so reducing solute yield. However, at temperatures below about 0 to -5°C, it has been found that the reduction in N_2O_4 solubility with decreasing temperature during solvate precipitation becomes much less pronounced and may even increase slightly, whereas the corresponding reduction in N_2O_5 solubility with decreasing temperature tends to become more pronounced. Therefore, the amount of phase-separated N_2O_4 produced with decreasing acid temperature remains relatively small, and this factor, together with the steadily decreasing solubility of N_2O_5 in N_2O_4 with decreasing temperature, minimises N_2O_5 losses into that N_2O_4 phase.

The amount of N_2O_5 precipitated also advantageously increases with increasing N_2O_5 concentration in the solution prepared in step (a). It has been discovered that the acid solution prepared in step (a) may contain an approximate N_2O_5 :nitric acid ratio by weight of up to at least 1:1.8 at temperatures at or above 10°C without the formation of an N_2O_5 precipitate in solution. The overall upper limit for dissolved N_2O_5 concentration in solution is about 40 parts of weight of N_2O_5 to 60 parts by weight of nitric acid, preferably 35 parts by weight of N_2O_5 per 65 parts by weight of nitric acid.

The minimum concentration of N_2O_5 which must be present in solution in order to effect its precipitation during step (b) is found to vary according to the temperature of and N_2O_4 concentration within the acid solution, and is generally found to increase with decreasing N_2O_4 concentration and increasing temperature. For example, at a solution temperature of -15°C, the ratio by weight of N_2O_5 to nitric acid required to effect N_2O_5 precipitation must be at least about 1:3 even if the dissolved N_2O_4 concentration within the solution approaches saturation, whereas at a solution temperature of +5 to +8°C, the required minimum ratio rises considerably and must be greater than about 3:7. Since the amount of solid precipitated increases with increasing N_2O_5 concentration in solution, the ratio by weight of N_2O_5 to pure nitric acid in the solution prepared in step (a) is preferably at least 1:2.8 more preferably at least 3:7, in order to produce a reasonable yield of precipitate.

For any given precipitation temperature, the amount of N_2O_5 precipitated during step (b) generally increases with increasing concentration of dissolved N_2O_4 present in solution. For this reason, the solution prepared in step (a) preferably contains at least 15wt%, more preferably at least 20wt%, most preferably at least 25wt%, of N_2O_5 . The ratio by weight of N_2O_4 to nitric acid in the solution prepared in step (a) is preferably at least 1:4, more preferably at least 1:3. A high N_2O_4 concentration has the added advantage that during step (a) it increases the electrical conductivity of the anolyte and enables a higher N_2O_4 concentration to be used in the catholyte, and so improves the electrical efficiency of the electrochemical process for producing N_2O_5 . The preferred maximum concentration of N_2O_4 in the acid solution produced in step (a) is a single phase saturated N_2O_4 solution, although N_2O_4 concentration is conveniently not greater than 30wt% since cooling the solution with an N_2O_4 concentration at or below this level produces little or no separate liquid N_2O_4 into which appreciable amounts of N_2O_5 can migrate to reduce the yield of solute especially if a precipitation temperature of about -5°C or higher is used in step (b).

The present method preferably forms part of a process for the continuous or semi-continuous electrochemical generation of N_2O_5 in nitric acid, in which N_2O_4 in nitric acid is preferably recirculated through the anode compartment of an electrochemical cell. N_2O_5 solute is preferably recovered by the present method from at least part of the recirculated product stream from the anode compartment. Cooling of at least part of the acid solution stream to effect N_2O_5 solute precipitation at least partly removes the heat absorbed by the stream during anodic oxidation. Thereafter, before the acid solution stream is returned to the cell to effect further N_2O_5 generation therein, the precipitated N_2O_5 solute is preferably recovered from this stream, most preferably by filtration. Since the product stream must be recharged with N_2O_4 before being returned to the cell, then it is preferred that this step should be performed after recovery of the N_2O_5 solute previously precipitated by cooling.

In order to purify the N_2O_5 solute removed from the acid solution, it is conveniently washed with liquid N_2O_4 to remove nitric acid from its surface. Thereafter, it may be dried in a gas stream of, for example, air, N_2 or O_2 to drive off residual N_2O_4 . The gas stream may contain small amounts of ozone to convert at least some of the remaining residual N_2O_4 to solid N_2O_5 . Alternatively, in order to effect N_2O_5 purification the solute may be sublimed at a temperature of 5°C to 10°C and at a reduced pressure of 30-100mm Hg, and the sublimed N_2O_5 vapour resolidified on a cold surface at about -20°C. The solute so cleansed or the solid N_2O_5 so purified may then be dissolved in organic solvents for use as a nitrating agent in, for example, the process of converting hydroxyalkyloxetanes to nitroalkyloxetanes as described in US Patent No 3058994.

The present method may alternatively be used as a means of producing further solutions of N_2O_5 in nitric acid which are either more concentrated than and/or have lower N_2O_4 concentrations than the acid solution from which the N_2O_5 solute is initially recovered. In this case, the solute cleansing and purification steps described above are largely unnecessary. Instead, since the solute essentially consists of a mixture of N_2O_5 and nitric acid it may be dissolved in nitric acid to produce solutions of N_2O_5 in nitric acid to the required concentration which contain very little N_2O_4 in sharp contrast to the high levels of N_2O_4 to be found in the solution

produced in step (a). Redissolving the solute in nitric acid is especially advantageous for producing nitric acid solutions containing more than 25wt% N_2O_5 and/or less than 3% N_2O_4 since such solutions are difficult to produce efficiently and at relatively low cost by purely electrochemical means.

Mixtures of solute in nitric acid may also be prepared which contain N_2O_5 above its saturation limit in nitric acid. The resulting slurries provide more concentrated forms of N_2O_5 which are relatively stable and more easily stored and transported than solid solute.

The present invention will now be described by way of example only with reference to the accompanying drawings in which

Figure 1 is an outline phase diagram of acid solution components illustrating the conditions under which N_2O_5 precipitation occurs; and

Figure 2 is a schematic process flow diagram of the method of the invention used in conjunction with a continuous process for the electrochemical generation of N_2O_5 in nitric acid.

A series of experiments were conducted to establish the phase diagram illustrated in Figure 1.

Experiments 1 to 4

Four solutions of N_2O_5 in 100g nitric acid were prepared at known N_2O_5 concentrations, and were cooled to -15°C . In four separate experiments liquid N_2O_4 also at -15°C was slowly added with mixing to each of these solutions. The rate of addition was sufficiently slow to ensure complete dissolution of N_2O_4 into the acid solution, so preventing a build-up of a separate N_2O_4 phase before the N_2O_4 concentration in the acid had reached saturation.

N_2O_4 addition was continued until the formation of a white precipitate in solution was observed, and the amount of N_2O_4 added up to this point was recorded. Thereafter, N_2O_4 addition was continued further until the solution had virtually reached its saturation limit, the formation of further precipitate being observed during this time.

The precipitate was recovered by filtration on a Buchner funnel, washed with liquid N_2O_4 at -15°C to remove excess acid, and dried on the funnel in a stream of cold dry air. The recovered precipitate was identified by RAMAN spectroscopy as an N_2O_5 /nitric acid solvate.

The amount of added N_2O_4 required to initiate precipitation of N_2O_5 was found to be dependent on the initial concentration of N_2O_5 in the acid solution. This can be seen from Table 1 below which summarises the result of each experiment at the point of initial precipitation.

TABLE 1

Expt	Amount of N_2O_5 Present in 100g Nitric Acid (g)	wt% N_2O_5 in Solution	Amount of N_2O_4 Added to Initiate N_2O_5 Precipitation (g)	wt% Composition of Acid Solution at Initial N_2O_5 Precipitation		
				HNO_3	N_2O_5	N_2O_4
1	46.2	31.6	15.8	61.73	28.52	9.75
2	43.1	30.12	21.1	60.90	26.25	12.85
3	35.4	26.14	51.1	53.62	18.98	27.40
4	29.1	23.07	68.7*	50.8*	14.6*	34.6*

*A second, liquid N_2O_4 phase began to appear at this point and the experiment was stopped. No N_2O_5 precipitation was observed.

A similar precipitation effect is observed by first adding liquid N_2O_4 and then cooling the solution to -15°C .

For example, by adding at least 15.8g of N_2O_4 to the N_2O_5 solution used in Experiment 1, precipitation of N_2O_5 is observed at or before the solution has cooled to -15°C .

Experiments 5 to 7

An almost saturated solution of N_2O_5 in nitric acid was obtained by dissolving solid N_2O_5 (11.5g) in nitric acid (20.3g) at 20°C to produce a 36.2wt% solution of N_2O_5 in nitric acid. The solution was cooled and liquid N_2O_4 slowly added with mixing to raise its concentration in solution in an attempt to precipitate N_2O_5 in a similar manner to that described in Experiments 1 to 4. The experiment was conducted three times over at different temperatures. The upper temperature limit and minimum addition of N_2O_4 necessary to initiate precipitation were noted. The results of these experiments are given in Table 2 below.

TABLE 2

Expt	Temperature ($^\circ\text{C}$)	Amount of N_2O_4 Added to Initiate Precipitation (g)	Wt% Composition of Acid Solution at N_2O_4 Precipitation		
			HNO_3	N_2O_5	N_2O_4
5	10	*14.6	*44.7	*25.3	*30.0
6	8	3.45	57.59	32.62	9.79
7	5	3.45	57.59	32.62	9.79

*A second, liquid N_2O_4 phase began to appear at this point and the experiment was stopped. No N_2O_5 precipitation was observed.

This series of three experiments shows that a solution temperature of 8°C or less is required to effect N_2O_5 precipitation. At 10°C , no precipitate forms regardless of N_2O_4 concentration in solution.

Experiment 8

Solid N_2O_5 was added to a known weight of a 1:1 ratio by weight mixture of 100% nitric acid and N_2O_4 maintained at 25°C , until no more N_2O_5 would dissolve. It was observed that N_2O_4 started to form a separate liquid phase at the end of N_2O_5 addition.

Initial weight of N_2O_4/HNO_3 mixture : 11.7g
Amount of N_2O_4 added : 4.1g

The composition of a 1:1 N_2O_4/HNO_3 solution saturated with N_2O_5 is therefore:

37.0wt% HNO_3
37.0wt% N_2O_4
25.9wt% N_2O_5

Summary

The results of Experiments 1 to 8 are shown plotted on the phase diagram illustrated in Figure 1.

Key to Table 1

A = Experiment No 1

B = Experiment No 2

C = Experiment No 3

D = Experiment No 4

E = Experiment No 5

F = Experiment Nos 6 and 7

G = Experiment No 8

H = Point estimated from published sources

I = Point estimated from published sources

J = Point estimated from published sources

Line X_1Y_1 = line of constant weight ratio of $\text{HNO}_3:\text{N}_2\text{O}_5$ for Experiment No 4.

It will be seen from the phase diagram of Figure 1 that the broken curved line taken through points A, B, C, D and H represents the concentration of the three components HNO_3 , N_2O_4 and N_2O_5 in the nitric solution at a constant temperature of -15°C . Similar curves are also shown for nitric acid solutions at $5-8^\circ\text{C}$, 10°C and 25°C .

The solid line which passes through the cusps in each curve (line X_2Y_2) represents a boundary to the left of which the solution is saturated in N_2O_4 .

The phase diagram may be used to determine the appropriate amount of N_2O_5 solute which will precipitate from any given single-phase acid solution of N_2O_5 and N_2O_4 in nitric acid. For example, if an acid solution of composition Z is cooled to -15°C , the solution will lose both N_2O_5 and nitric acid and will assume a composition on the ABCDH curve. This composition will depend also upon the ratio of N_2O_5 to HNO_3 in the solute. If this solute composition is represented by point P (50% N_2O_5 , 50% HNO_3), then the eventual composition of the acid solution will be approximately at the point of intersection between the straight line passing through points P and Z, and the curve passing through points A, B and C. By comparing the composition Z with the predicted composition of the solution after cooling, the amount of N_2O_5 which will precipitate from solution into the solute can be calculated.

Example 1

Figure 2 is a schematic process flow diagram illustrating the use of the present method in conjunction with a continuous process for the electrochemical production of N_2O_5 in nitric acid. The temperatures shown are typical of those which may be employed.

The N_2O_5 production process outlined in Figure 2 employs a temperature-controlled reservoir 2, a recirculation pump 4, an electrochemical cell 6, and a flow divider 8 all connected together in a production loop to allow at least partial recirculation of the product acid. For any given rate of N_2O_5 production, recirculation increases the turbulent regime hence conductivity of the cell and reduces the concentration gradient of solution components through the cell. The cell 6 has an anode compartment 10, a cathode compartment 12, and an ion exchange membrane 14 separating the two compartments. The membrane 14 is preferably an anionic or semi-permeable (non-ionic) membrane.

A solution of N_2O_4 and N_2O_5 in nitric acid at 10°C is fed continuously by the pump 4 from the reservoir 2 through the anode compartment 10 where some of the N_2O_4 is electrochemically oxidised to N_2O_5 . The solution pumped from the reservoir 2 is saturated with N_2O_4 and contains N_2O_5 in the weight ratio of N_2O_5 :nitric acid of about 1:3. At the same time, a nitric acid solution containing 20wt% N_2O_4 and 8wt% water is fed continuously through the cathode compartment 12. Electrical current is passed through the cell 6 at 4.5 volts and a current density of $0.15-0.2$ amps cm^{-2} , and the flow rate of anolyte adjusted such that the N_2O_5 content of the acid solution leaving the anode compartment 10 is increased to an N_2O_5 -to- HNO_3 ratio of about 8:17 by weight.

The electrochemical reactions within the cell 6 cause the temperature of the acid solutions within the anode and cathode compartments 10 and 12 to increase. The heated product acid solution from the anode compartment 10, which at this point has a temperature of typically $15-25^\circ\text{C}$, is then fed to the flow divider 8 which divides the acid solution into two streams (A) and (B).

Stream (A) is recycled directly to the reservoir 2. Stream (B) is recycled to the reservoir 2 through a chiller/crystalliser 16 and a solids separator 18. The chiller/crystalliser 16 cools the stream (B) to a temperature (typically -15°C) at which a proportion of the N_2O_5 dissolved in solution is caused to precipitate out as an N_2O_5 solute, and a proportion of the N_2O_4 dissolved in solution is caused to form a separate liquid phase. The solute is recovered from the stream (B) in the solids separator 18 which may comprise, for example, a filter or a hydrocyclone. The cold, N_2O_5 -depleted stream (B) is then returned to the reservoir 2 where its entrained liquid

N_2O_4 phase rapidly redissolves in the acid solution due to the warmer conditions which prevail there.

Nitric acid and liquid N_2O_4 are added to the reservoir 2 to make up for process losses. The relative flow rates of streams (A) and (B) and the actual temperature of precipitation are adjusted to return the N_2O_5 -to-nitric acid ratio in the reservoir to 1:3 so that the whole process exists in a state of equilibrium. The rate of N_2O_4 addition is sufficiently high to form a separate, liquid N_2O_4 layer (D) in the reservoir above the acid layer (E). This ensures that at the controlled temperature within the reservoir (2) of typically 10°C , the acid layer is effectively saturated with dissolved N_2O_4 which promotes both high rates of N_2O_5 production in the cell 2 at which current efficiencies, and high rates of N_2O_5 precipitation in the chiller/crystalliser 16. A heating/cooling coil 20 is used to control the temperature of the reservoir 2. The addition of fresh nitric acid to the reservoir 2, and the use of an operating temperature in the reservoir which is generally much higher than that of the solids separator 18, help to ensure that any N_2O_5 precipitate carried over from the separator is rapidly redissolved in the reservoir before the acid solution is pumped back to the cell 6.

Example 2

The method and method conditions of Example 1 were repeated except that the acid solution was passed in series through three electrochemical cells 10 with their anode compartments 16 connected in series. In order to suppress the formation of a separate N_2O_4 phase during cooling/precipitation, the concentration of N_2O_4 in the acid solution within the reservoir was maintained at about 30wt% by carefully controlling its rate of addition. At 10°C , the acid solution within the reservoir was not therefore saturated with N_2O_4 and a separate N_2O_4 layer did not form. The flow rate through the cells 10 was adjusted to produce an acid solution leaving the last anode compartment having a N_2O_5 -to- HNO_3 ratio of about 3:5 at about 25°C , which is appropriately at the saturation limit of N_2O_5 in solutions of nitric acid and N_2O_4 at that temperature.

Example 3

The wet solvate product from Example 1 was washed at 5°C with a portion of the N_2O_4 layer taken from the reservoir 20 to remove nitric acid from the surface of the solvate crystals. The N_2O_4 was then returned to the reservoir to prevent loss of N_2O_5 from the system. The washed solvate was then dried in a stream of dry ozonised air at 10°C , and dissolved in dichloromethane in the proportion of 10g dried solvate to 90g dichloromethane.

Example 4

The wet solvate product of Example 1 or Example 2 was washed with a small amount of 99% nitric acid at 0°C to remove its surface contamination of residual N_2O_4 -rich nitric acid resulting from the solvates method of preparation. System losses were minimised by feeding the spent nitric acid washings to the reservoir 2. The washed solvate was then added to 99% nitric acid in the ratio of 35 parts by weight of solvate to 65 parts by weight of nitric acid to produce a clear concentrated solution of N_2O_5 in nitric acid containing low levels of N_2O_4 .

Example 5

The method of Example 4 was repeated except that the washed solvate was added to 99% nitric acid in the ratio of 85 parts by weight of solvate to 15 parts by weight of nitric acid, to produce a slurry of N_2O_5 in nitric acid.

Examples 6 and 7

The methods of Examples 4 and 5 were repeated except that the nitric acid washing steps were omitted, resulting in products containing slightly higher levels of N_2O_4 .

Claims

1. A method of separating N_2O_5 from its solution in nitric acid comprising the steps
 - (a) preparing, by the electrochemical oxidation of N_2O_4 in nitric acid, a nitric acid solution at a temperature of at least 10°C containing at least 45wt% of dissolved ($N_2O_4 + N_2O_5$) and having a dissolved N_2O_5 :nitric acid ratio by weight of at least 1:3, and



N_2O_4 phase rapidly redissolves in the acid solution due to the warmer conditions which prevail there.

Nitric acid and liquid N_2O_4 are added to the reservoir 2 to make up for process losses. The relative flow rates of streams (A) and (B) and the actual temperature of precipitation are adjusted to return the N_2O_5 -to-nitric acid ratio in the reservoir to 1:3 so that the whole process exists in a state of equilibrium. The rate of N_2O_4 addition is sufficiently high to form a separate, liquid N_2O_4 layer (D) in the reservoir above the acid layer (E). This ensures that at the controlled temperature within the reservoir (2) of typically 10°C , the acid layer is effectively saturated with dissolved N_2O_4 which promotes both high rates of N_2O_5 production in the cell 2 at which current efficiencies, and high rates of N_2O_5 precipitation in the chiller/crystalliser 16. A heating/cooling coil 20 is used to control the temperature of the reservoir 2. The addition of fresh nitric acid to the reservoir 2, and the use of an operating temperature in the reservoir which is generally much higher than that of the solids separator 18, help to ensure that any N_2O_5 precipitate carried over from the separator is rapidly redissolved in the reservoir before the acid solution is pumped back to the cell 6.

Example 2

The method and method conditions of Example 1 were repeated except that the acid solution was passed in series through three electrochemical cells 10 with their anode compartments 16 connected in series. In order to suppress the formation of a separate N_2O_4 phase during cooling/precipitation, the concentration of N_2O_4 in the acid solution within the reservoir was maintained at about 30wt% by carefully controlling its rate of addition. At 10°C , the acid solution within the reservoir was not therefore saturated with N_2O_4 and a separate N_2O_4 layer did not form. The flow rate through the cells 10 was adjusted to produce an acid solution leaving the last anode compartment having a N_2O_5 -to- HNO_3 ratio of about 3:5 at about 25°C , which is appropriately at the saturation limit of N_2O_5 in solutions of nitric acid and N_2O_4 at that temperature.

Example 3

The wet solvate product from Example 1 was washed at 5°C with a portion of the N_2O_4 layer taken from the reservoir 20 to remove nitric acid from the surface of the solvate crystals. The N_2O_4 was then returned to the reservoir to prevent loss of N_2O_5 from the system. The washed solvate was then dried in a stream of dry ozonised air at 10°C , and dissolved in dichloromethane in the proportion of 10g dried solvate to 90g dichloromethane.

Example 4

The wet solvate product of Example 1 or Example 2 was washed with a small amount of 99% nitric acid at 0°C to remove its surface contamination of residual N_2O_4 -rich nitric acid resulting from the solvates method of preparation. System losses were minimised by feeding the spent nitric acid washings to the reservoir 2. The washed solvate was then added to 99% nitric acid in the ratio of 35 parts by weight of solvate to 65 parts by weight of nitric acid to produce a clear concentrated solution of N_2O_5 in nitric acid containing low levels of N_2O_4 .

Example 5

The method of Example 4 was repeated except that the washed solvate was added to 99% nitric acid in the ratio of 85 parts by weight of solvate to 15 parts by weight of nitric acid, to produce a slurry of N_2O_5 in nitric acid.

Examples 6 and 7

The methods of Examples 4 and 5 were repeated except that the nitric acid washing steps were omitted, resulting in products containing slightly higher levels of N_2O_4 .

Claims

1. A method of separating N_2O_5 from its solution in nitric acid comprising the steps
(a) preparing, by the electrochemical oxidation of N_2O_4 in nitric acid, a nitric acid solution at a temperature of at least 10°C containing at least 45wt% of dissolved ($N_2O_4 + N_2O_5$) and having a dissolved N_2O_5 :nitric acid ratio by weight of at least 1:3, and



(b) cooling the acid solution to less than 8°C until an N_2O_5 solvate precipitates from solution.

2. A method according to claim 1 characterised in that the acid solution in step (a) contains at least 50wt% of dissolved ($N_2O_4 + N_2O_5$).
3. A method according to claim 1 characterised in that the ratio by weight of N_2O_4 to nitric acid in the acid solution prepared in step (a) is from 1:4 to saturation.
4. A method according to claim 1 characterised in that the acid solution prepared in step (a) contains at least 15wt% N_2O_4 .
5. A method according to claim 1 characterised in that the nitric acid solution is cooled in step (b) to a temperature of from -25°C to 0°C.
6. A method according to claim 2 characterised in that the acid solution is cooled in step (b) to a temperature of less than -5°C.
7. A method according to claim 1 characterised by the subsequent step of (c) recovering the N_2O_5 solvate from the acid solution.
8. A method according to claim 7 characterised in that the acid solution comprises a product stream taken continuously from the anode compartment of an electrochemical cell employed for said electrochemical oxidation.
9. A method according to claim 8 characterised in that at least part of the N_2O_5 -depleted product stream from step (c) is recirculated back through the anode compartment of the cell.
10. A method according to claim 9 characterised in that part of the recirculated product stream bypasses steps (b) and (c).
11. A method according to claim 9 characterised in that N_2O_4 is added to the product stream after step (c) but before the steam re-enters the anode compartment of the cell.
12. A method according to claim 11 characterised in that the N_2O_4 is added to the product stream in a reservoir containing the product acid as a first liquid phase and N_2O_4 as a second liquid phase.
13. A method according to claim 7 characterised in that after step (c), the recovered N_2O_5 solvate is at least partly dissolved in an organic solvent.
14. A method according to claim 7 characterised in that after step (c), the recovered N_2O_5 solvate is at least partly dissolved in nitric acid.

Patentansprüche

1. Verfahren zur Abscheidung von N_2O_5 aus seiner Lösung in Salpetersäure, das die Schritte
 (a) Herstellen einer Salpetersäurelösung, durch die elektrochemische Oxidation von N_2O_4 in Salpetersäure, bei einer Temperatur von wenigstens 10 °C, die wenigstens 45 Gew.% von gelöstem ($N_2O_4 + N_2O_5$) enthält und ein Gewichtsverhältnis von gelöstem N_2O_5 : Salpetersäure von wenigstens 1 : 3 hat, und
 (b) Abkühlen der sauren Lösung auf unter 8 °C, bis sich ein N_2O_5 Solvat aus der Lösung abscheidet, aufweist.
2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß die Säurelösung im Schritt (a) wenigstens 50 Gew.% gelöstes ($N_2O_4 + N_2O_5$) enthält.
3. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß das Gewichtsverhältnis von N_2O_4 zu Salpetersäure in der im Schritt (a) hergestellten Säurelösung von



1:4 bis Sättigung ist.

4. Verfahren nach Anspruch 1,
dadurch gekennzeichnet, daß
die im Schritt (a) hergestellte Säurelösung wenigstens 15 Gew.% N_2O_4 enthält.
5. Verfahren nach Anspruch 1,
dadurch gekennzeichnet, daß
die Salpetersäurelösung im Schritt (b) auf eine Temperatur von $-25\text{ }^{\circ}\text{C}$ bis $0\text{ }^{\circ}\text{C}$ abgekühlt wird.
6. Verfahren nach Anspruch 2,
dadurch gekennzeichnet, daß
die Säurelösung im Schritt (b) auf eine Temperatur von unter $-5\text{ }^{\circ}\text{C}$ abgekühlt wird.
7. Verfahren nach Anspruch 1,
gekennzeichnet durch
den nachfolgenden Schritt (c) der Erfassung des N_2O_5 -Solvats aus der Säurelösung.
8. Verfahren nach Anspruch 7,
dadurch gekennzeichnet, daß
die Säurelösung einen Produktstrom aufweist, der kontinuierlich aus dem Anodenabteil einer für die elektrochemische Oxidation verwendeten elektrochemischen Zelle entnommen wird.
9. Verfahren nach Anspruch 8,
dadurch gekennzeichnet, daß
wenigstens ein Teil des N_2O_5 -verarmten Produktstroms von Schritt (c) durch das Anodenabteil rückzirkuliert wird.
10. Verfahren nach Anspruch 9,
dadurch gekennzeichnet, daß
ein Teil des rückzirkulierten Produktstroms die Schritte (b) und (c) überbrückt.
11. Verfahren nach Anspruch 9,
dadurch gekennzeichnet, daß
 N_2O_4 dem Produktstrom nach dem Schritt (c), jedoch vor Wiedereintritt des Stromes in das Anodenabteil der Zelle zugesetzt wird.
12. Verfahren nach Anspruch 11,
dadurch gekennzeichnet, daß
das N_2O_4 dem Produktstrom in einem Speicher zugesetzt wird, der die Produktsäure als eine erste flüssige Phase und N_2O_4 als eine zweite flüssige Phase enthält.
13. Verfahren nach Anspruch 7,
dadurch gekennzeichnet, daß
nach dem Schritt (c) das erfaßte N_2O_5 -Solvat wenigstens teilweise in einem organischen Lösungsmittel gelöst wird.
14. Verfahren nach Anspruch 7,
dadurch gekennzeichnet, daß
nach dem Schritt (c) das erfaßte N_2O_5 -Solvat wenigstens teilweise in Salpetersäure gelöst wird.

Revendications

1. Procédé de séparation de N_2O_5 de sa solution dans de l'acide nitrique, comprenant les étapes consistant à :
(a) préparer, par l'oxydation électrochimique de N_2O_4 dans de l'acide nitrique, une solution dans de l'acide nitrique à une température d'au moins $10\text{ }^{\circ}\text{C}$ contenant au moins 45 % en poids de ($N_2O_4 + N_2O_5$) dissous et présentant un rapport pondéral N_2O_5 dissous:acide nitrique valant au moins 1:3, et



(b) refroidir la solution acide jusqu'à une température inférieure à 8 °C, jusqu'à ce qu'un produit de solvation de N_2O_5 précipite de la solution.

- 5 2. Procédé selon la revendication 1, caractérisé en ce que à l'étape (a), la solution acide contient au moins 50 % en poids de ($N_2O_4 + N_2O_5$) dissous.
3. Procédé selon la revendication 1, caractérisé en ce que le rapport pondéral de N_2O_4 à l'acide nitrique dans la solution acide préparée à l'étape (a) va de 1:4 à la saturation.
- 10 4. Procédé selon la revendication 1, caractérisé en ce que la solution acide préparée à l'étape (a), contient au moins 15 % en poids de N_2O_4 .
5. Procédé selon la revendication 1, caractérisé en ce que la solution d'acide nitrique est refroidie à l'étape (b) jusqu'à une température comprise entre -25 °C et 0 °C.
- 15 6. Procédé selon la revendication 2, caractérisé en ce que la solution acide est refroidie à l'étape (b) jusqu'à une température inférieure à -5 °C.
- 20 7. Procédé selon la revendication 1, caractérisé par l'étape subséquente (c) consistant à récupérer de la solution acide le produit de solvation de N_2O_5 .
8. Procédé selon la revendication 7, caractérisé en ce que la solution acide comprend un courant de produit prélevé en continu du compartiment anodique d'une cellule électrochimique servant à ladite oxydation électrochimique.
- 25 9. Procédé selon la revendication 8, caractérisé en ce qu'au moins une partie du courant de produit appauvri en N_2O_5 , provenant de l'étape (c), est remise en circulation et renvoyée dans le compartiment anodique de la cellule.
- 30 10. Procédé selon la revendication 9, caractérisé en ce qu'une partie du courant de produit remis en recirculation contourne les étapes (b) et (c).
11. Procédé selon la revendication 9, caractérisé en ce que du N_2O_4 est ajouté au courant de produit après l'étape (c), mais avant que le courant n'entre à nouveau dans le compartiment anodique de la cellule.
- 35 12. Procédé selon la revendication 11, caractérisé en ce que le N_2O_4 est ajouté au courant de produit dans un réservoir contenant de l'acide produit à titre de première phase liquide et N_2O_4 à titre de seconde phase liquide.
- 40 13. Procédé selon la revendication 7, caractérisé en ce qu'après l'étape (c), le produit de solvation de N_2O_5 , récupéré, est au moins partiellement dissous dans un solvant organique.
14. Procédé selon la revendication 7, caractérisé en ce qu'après l'étape (c), le produit de solvation de N_2O_5 , récupéré, est au moins partiellement dissous dans de l'acide nitrique.