

Catalyst and conversion of synthesis gas therewith

This invention is concerned with a catalyst and process for converting synthesis gas, i.e. mixtures of gaseous carbon oxides with hydrogen or hydrogen donors, to hydrocarbon mixtures.

Processes for the conversion of coal and other hydrocarbons, such as natural gas, to a gaseous mixture consisting essentially of hydrogen and carbon monoxide and/or dioxide are well known. Those of major importance depend either on the partial combustion of the fuel with an oxygen-containing gas or on the high temperature reaction of the fuel with steam, or on a combination of these two reactions. An excellent summary of the art of gas manufacture, including synthesis gas, from solid and liquid fuels is given in Encyclopedia of Chemical Technology, Edited by Kirk-Othmer, Second Edition, Volume 10, pages 353—433 (1966), Interscience Publishers, New York, New York.

It is also well known that synthesis gas will undergo conversion to reduction products of carbon monoxide, such as hydrocarbons, at from about 149°C (300°F) to about 454°C (850°F) under from about one to one thousand atmospheres pressure, over a fairly wide variety of catalysts. The Fischer-Tropsch process, for example, which has been most extensively studied, produces a range of liquid hydrocarbons, a portion of which have been used as low octane gasoline. Catalysts that have been studied for this and related processes include those based on iron, cobalt, nickel, ruthenium, thorium, rhodium and osmium, or their oxides.

Recently, it has been discovered that the conversion of synthesis gas into valuable products can be greatly enhanced by employing a special type of crystalline aluminosilicate zeolite exemplified by ZSM-5 in admixture with a carbon monoxide reduction catalyst.

Thus, for example, in United States Patent US—A—4,086,262, there is disclosed a process for the conversion of syngas by passing the same at elevated temperature over a catalyst which comprises an intimate mixture of a Fischer-Tropsch component and a special type of zeolite such as ZSM-5. Said patent points out that the products produced are hydrocarbon mixtures which are useful in the manufacture of heating oil, high octane gasoline, aromatic compounds, and chemical intermediates.

From U.S.—A—4,086,262 (particularly Examples 6 to 8) and FR—A—2,268,771 (particularly Example 9) it is known to prepare a catalyst for synthesis gas reactions which catalyst includes an iron compound, a zeolite having a $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratio greater than 12 and a constraint index between 1 and 12, and a matrix material. The iron compounds employed are ferric nitrate, ilmenite, magnetite and iron carbide.

As can well be appreciated, the patent and technical literature relating to the Fischer-Tropsch process, is, indeed, extensive and the various catalysts reported in the prior art have been used by themselves as well as in admixture with catalytically inactive supports such as kieselguhr. Although the reasons for using catalytically inactive supports have varied, nevertheless, it would appear that one reason for using the same is that it resulted in increased surface area of the Fischer-Tropsch component upon which it was deposited or admixed and that it also aided in controlling the heat requirements of the overall exothermic reactions.

It is also known in the art to admix a Fischer-Tropsch component with a material, such as silica-alumina which is known to be catalytically active for the conversion of hydrocarbons.

The process of this invention is directed towards an improvement in the process of converting syngas to a very specific product. The product with which the instant invention is concerned is a naphtha having a boiling range of less than 400°F at a 90% overhead which is defined as a C_5^+ naphtha wherein said fraction is at least 45 weight percent of the total hydrocarbons produced. The instant invention is also concerned with obtaining the above-defined product in good yields and good selectivities from the starting syngas material as well as towards the catalyst per se.

The process of this invention is carried out by contacting said synthesis gas with a catalyst which comprises at least three separate components which are present in a single particle as opposed to a mixture of three separate particles. The catalyst of this invention comprises iron, an acidic crystalline aluminosilicate zeolite having a pore size of about 5 Angstrom units, a silica alumina ratio of at least 12, and a constraint index of about 1—12 (preferably ZSM-5) and a matrix material. The crystalline aluminosilicates employed in the novel process of this invention are fully set forth in aforementioned United States Patent US—A—4,086,262 which is herein incorporated by reference. The preferred class of zeolites used is exemplified by ZSM-5, ZSM-11, ZSM-12, etc. As has heretofore been stated, the manner in which the iron is introduced into the catalyst is of prime importance.

The matrix portion of the single particle catalyst is not narrowly critical and suitable matrices include silica, alumina, silica-alumina, silica-zirconia, silica-magnesia, etc.

One surprising feature of the process of this invention is that the catalysts which are employed may be unpromoted and yet they still exhibit high activity with little evident aging, and, in fact, are capable of converting syngas to the olefinic or aromatic naphtha product previously described while producing no more than 30 weight percent of methane plus ethane, based on total hydrocarbons. In fact, the use of promoters, which the prior art found necessary in previous iron-containing catalysts, is definitely not preferred due to the fact that most promoters are alkaline in nature and they have a tendency to migrate to the acidic crystalline aluminosilicate zeolite component and to decrease the

activity of the same. Therefore, it would appear that the single particle catalyst of the instant invention represents a significant departure from the teachings of the prior art in that not only are alkaline promoters not necessary for sustained operation, but, in fact, are detrimental to the activity of the zeolitic component.

The single particle iron-containing catalyst of this invention can be prepared by adding the appropriate acidic crystalline aluminosilicate previously defined and a water insoluble iron derivative of an organic iron compound to a hydrogel before drying, homogenizing the same, and thereafter forming either fixed bed or fluidized bed catalysts by conventional techniques.

The water-insoluble derivatives of organic compounds include water-insoluble organic iron salts such as the oxalate, the formate, as well as mixtures thereof.

The amount of water-insoluble iron derivative of an organic compound which is added is not narrowly critical and an amount sufficient to produce 2.5 to 20 weight percent and more preferably 2.5 to 10 weight percent expressed as Fe, based on the finished catalyst, is used.

One embodiment of this invention resides in the in situ formation of the water insoluble organic iron derivative in the hydrogel. In this embodiment a water soluble iron salt such as iron sulfate is added to the hydrogel followed by treatment with oxalic or formic acid in order to form the organic salt in situ.

Following the addition of the water insoluble organic iron salt (either directly or prepared in situ), the catalyst can be formulated into a fixed bed or fluidized bed catalyst by conventional techniques.

It is to be understood that methods of making fluidized bed catalysts containing crystalline aluminosilicate zeolites and matrices are well known in the art and that no novelty is claimed in this step per se. Thus, for example, a composite of the crystalline aluminosilicate zeolite and a siliceous matrix can be made by admixing an aqueous alkali metal silicate with or without a particulate weighting agent, such as kaolin clay, desirably as a dispersion in water so as to intimately mix the clay particles with the alkali metal silicate. This admixing is conveniently done at room temperature, although, of course, higher or lower temperatures may be employed if desired. The mixture is then heated, generally to a temperature of from 38 to 71°C (100—160°F) and acid is added to adjust the pH to from about 8—10. The temperature is maintained for a time of about 1—6 hours or longer. At this point, if a silica-zirconia weighting agent (e.g. clay) matrix is desired, a zirconium salt is added, desirably as an aqueous solution thereof. Acid is then added to reduce the pH to about 4—7 and form a silica gel weighting agent or a silica gel-zirconia gel weighting agent slurry, which is then admixed with a slurry of the acidic crystalline aluminosilicate zeolite and the water insoluble organic iron salt previously described. The resulting composite is then homogenized and then treated with a source of ammonium ions or hydrogen ions in order to reduce the sodium content to a low level which is desirably less than about 0.1% weight sodium and then spray dried to produce particles of a size range appropriate for use in a fluidized-bed reactor.

As is generally known in fluidized bed catalysts for catalytic cracking, the catalyst additionally includes a weighting agent. The most preferred weighting agent is kaolin clay. Other weighting agents may be substituted in whole or in part for the kaolin clay so long as the weighting agents are not detrimental to the finished catalyst.

The matrices may also be based on alumina for fluidized bed catalysts, such formulations generally do not lead to the desired physical characteristics. However, an alumina matrix (or border) may be prepared for fixed bed catalysts.

The relative proportion of crystalline aluminosilicate zeolite is not narrowly critical and it can range from about 5—40 weight percent of the matrix material.

As has been indicated earlier, the crystalline aluminosilicate zeolite, the iron compound and the matrix are then thoroughly mixed in a form of an aqueous slurry in order to homogenize the same and thereafter subdivided and dried to form the desired particles. A particularly good method of making microspherical particles (e.g. of particle size of about 1—200 μm) especially suitable for use in the fluidized bed process is spray-drying.

The temperature of the air (or other gas) entering the spray drier is ordinarily within the range of 260—538°C (500—1000°F). The temperature used will depend on such factors as the quantity of material to be dried and the quality of air used in the drying. The evaporation rate will vary depending on the quantity of air used in the drying. The temperature of the particles which are being dried is generally within the range of 65 to 204°C (150—400°F) at the completion of the drying, but preferably 93—177°C (200—350°F).

The drying may be effected by a process in which the particles to be dried and a hot air stream are moving in the same direction for the entire drying period (concurrent drying) or where the hot stream flows in the opposite direction (countercurrent drying), or by semi-concurrent drying. It is to be understood that spray-drying to form fluidized bed catalysts is well known in the art and a representative procedure is described in United States Patent US—A—3,553,104, the entire contents of which are incorporated by reference.

The iron-containing catalysts are thereafter heated in order to decompose the organic iron compounds. The temperature utilized is not critical and it can range from 46°C (115°F) to 649°C (1200°F) for periods of time ranging from about 1 to 48 hours.

The iron-containing catalysts must be then pretreated prior to use for the conversion of syngas. In

this connection, it has been found that the nature of the pretreatment is critical. The catalyst must be pretreated with syngas or with CO prior to use. As opposed to prior art catalysts, the use of hydrogen alone has an adverse effect on catalytic properties. Treatment with syngas or carbon monoxide is conveniently carried out at atmospheric pressure and at temperatures of 288—343°C for periods of time ranging from 1/2 hour up to 24 hours.

Another embodiment of this invention resides in a modification involving the in situ formation of the water insoluble organic iron salt. In this embodiment, a water-soluble iron salt such as ferrous sulfate or iron gluconate is added to an alumina dispersion followed by addition of an appropriate organic acid such as oxalic acid in order to form an alumina-iron oxalate composition. This composition can be used as the source of iron by the addition of the same to the hydrogel-containing matrix and crystalline aluminosilicate zeolite followed by processing in the manner previously described.

A particularly desirable embodiment of this invention resides in the use of matrices made from mixtures of colloidal silica and colloidal alumina instead of conventional procedures in which sodium silicate and aluminum sulfate are employed. In this embodiment colloidal alumina is added to colloidal silica which usually contains a slurry of a weighting agent such as clay. Crystalline aluminosilicate zeolite and water-insoluble organic iron salt are added followed by homogenizing and drying in the manner previously described.

The acidic crystalline aluminosilicate component of the catalyst is characterized by a pore dimension greater than about 0.5 nm, i.e. it is capable of sorbing paraffins, and it has a silica-to-alumina ratio of at least 12 and a constraint index within the range of 1 to 12. Zeolite A, for example, with a silica-to-alumina ratio of 2.0 is not useful in this invention, and it has no pore dimension greater than about 0.5 nm.

The crystalline aluminosilicates herein referred to, also known as zeolites, constitute an unusual class of natural and synthetic minerals. They are characterized by having a rigid crystalline framework structure composed of an assembly of silicon and aluminum atoms, each surrounded by a tetrahedron of shared oxygen atoms, and a precisely defined pore structure. Exchangeable cations are present in the pores.

The acidic crystalline aluminosilicate component preferably is in the hydrogen form.

The catalysts referred to herein utilize members of a special class of zeolites exhibiting some unusual properties. They are very active even with silica-to-alumina ratios exceeding 30. This activity is surprising since catalytic activity of zeolites is generally attributed to framework aluminum atoms and cations associated with these aluminum atoms. These zeolites retain their crystallinity for long periods in spite of the presence of steam even at high temperatures which induce irreversible collapse of the crystal framework of other zeolites, e.g., of the X and A type. Furthermore, carbonaceous deposits, when formed, may be removed by burning at higher than usual temperatures to restore activity. In many environments the zeolites of this class exhibit very low coke forming capability, conducive to very long times on stream between burning regenerations.

An important characteristic of the crystal structure of this class of zeolites is that it provides constrained access to, and egress from, the intra-crystalline free space by virtue of having a pore dimension greater than about 0.5 nm and pore windows of about a size such as would be provided by 10-membered rings of oxygen atoms. It is to be understood, of course, that these rings are those formed by the regular disposition of the tetrahedra making up the anionic framework of the crystalline aluminosilicate, the oxygen atoms themselves being bonded to the silicon or aluminum atoms at the centers of the tetrahedra. Briefly, the preferred zeolites useful in this invention comprise, in combination; a silica-to-alumina ratio of at least about 12; and a structure providing constrained access to the crystalline free space.

The silica-to-alumina ratio referred to may be determined by conventional analysis. This ratio is meant to represent as closely as possible, the ratio in the rigid anionic framework of the zeolite crystal and to exclude aluminum in the binder or in cationic or other form within the channels. Although zeolites with a silica-to-alumina ratio of at least 12 are useful, it is preferred to use zeolites having higher ratios of at least about 30. Such zeolites, after activation, acquire an intracrystalline sorption capacity for normal hexane which is greater than that for water, i.e., they exhibit "hydrophobic" properties. It is believed that this hydrophobic character is advantageous in the present invention.

The zeolites useful as catalysts in this invention freely sorb normal hexane and have a pore dimension greater than about 5 Angstroms. In addition, their structure must provide constrained access to some larger molecules. It is sometimes possible to judge from a known crystal structure whether such constrained access exists. For example, if the only pore windows in a crystal are formed by 8-membered rings of oxygen atoms, then access by molecules of larger cross-section than normal hexane is substantially excluded and the zeolite is not of the desired type. Zeolites with windows of 10-membered rings are preferred, although excessive puckering or pore blockage may render these zeolites substantially ineffective. Zeolites with windows of 12-membered rings do not generally appear to offer sufficient constraint to produce the advantageous conversions desired in the instant invention, although structures can be conceived, due to pore blockage or other cause, that may be operative.

Rather than attempt to judge from crystal structure whether or not a zeolite possesses the necessary constrained access, a simple determination of the "constraint index" may be made by

continuously passing a mixture of equal weight of normal hexane and 3-methylpentane over a small sample, approximately 1 gram or less, of zeolite at atmospheric pressure according to the following procedure. A sample of the zeolite, in the form of pellets or extrudate, is crushed to a particle size about that of coarse sand and mounted in a glass tube. Prior to testing, the zeolite is treated with a stream of air at 538°C (1,000°F) for at least 15 minutes. The zeolite is then flushed with helium and the temperature adjusted between 288°C (550°F) and 510°C (950°F) to give an overall conversion between 10% and 60%. The mixture of hydrocarbons is passed at 1 liquid hourly space velocity (i.e. 1 volume of liquid hydrocarbon per volume of catalyst per hour) over the zeolite with a helium dilution to give a helium to total hydrocarbon mole ratio of 4:1. After 20 minutes on stream, a sample of the effluent is taken and analyzed, most conveniently by gas chromatography, to determine the fraction remaining unchanged for each of the two hydrocarbons.

The "constraint index" is calculated as follows:

$$\text{Constraint Index} = \frac{\log_{10} (\text{fraction of n-hexane remaining})}{\log_{10} (\text{fraction of 3-methylpentane remaining})}$$

The constraint index approximates the ratio of the cracking rate constants for the two hydrocarbons. Catalysts suitable for the present invention are those which employ a zeolite having a constraint index from 1.0 to 12.0. Constraint Index (CI) values for some typical zeolites including some not within the scope of this invention are:

	Zeolite	C.I.
25	Erionite	38
	ZSM-5	8.3
	ZSM-11	8.7
	ZSM-35	6.0
	TMA Offretite	3.7
30	ZSM-38	2.0
	ZSM-12	2
	Beta	0.6
	ZSM-4	0.5
	Acid Mordenite	0.5
35	REY	0.4
	Amorphous silica-alumina	0.6

The above-described Constraint Index is an important and even critical, definition of those zeolites which are useful to catalyze the instant process. The very nature of this parameter and the recited technique by which it is determined, however, admit of the possibility that a given zeolite can be tested under somewhat different conditions and thereby have different constraint indexes. Constraint index seems to vary somewhat with severity of operation (conversion). Therefore, it will be appreciated that it may be possible to so select test conditions to establish multiple constraint indexes for a particular given zeolite which may be both inside and outside the above-defined range of 1 to 12.

Thus, it should be understood that the parameter and property "Constraint Index" as such value is used herein as an inclusive rather than exclusive value. That is, a zeolite when tested by any combination of conditions within the testing definition set forth hereinabove to have a constraint index of 1 to 12 is intended to be included in the instant catalyst definition regardless that the same identical zeolite tested under other defined conditions may give a constraint index value outside of 1 to 12.

The class of zeolites defined herein is exemplified by ZSM-5, ZSM-11, ZSM-12, ZSM-35 and ZSM-38, respectively defined by the x-ray diffraction data furnished in U.S. Patent Specifications 3,702,886, 3,709,979, 3,832,449, 4,016,245 and 4,046,859.

The novel process of this invention is carried out at temperatures ranging from about 260—316°C (500—600°F) and more preferably from 288°C (550°F) to about 304°C (580°F). The novel process of this invention is carried out at gas hourly space velocities (GHSV), ranging from 400 to 20,000 and more desirably from 500 to 6,000, based on fresh feed and total catalyst volume. Hydrogen to carbon oxides ratios can vary from 0.5:1 to 2:1 and more preferably are about 1:1, pressures ranging from 446 to 6996 kPa (50 to 1,000 psig) and more preferably from 1135 to 2859 kPa (150 to 400 psig) are employed.

It is to be understood that although this invention has been described with reference to iron only, the catalyst can contain minor amounts of additional substances such as tin, phosphorus and tungsten, rare earth, vanadium, manganese, molybdenum, etc.

The following examples will illustrate the novel process of this invention. All percentages, unless otherwise specified, are by weight.

Example 1

The fluid catalyst matrix of this example was prepared in the following manner. Q-Brand silicate solution (7972.2 grams) was added to a water slurry containing 1861 grams WP kaolin clay in 38 kg (83.7 lbs) of water. After heating to 49°C (120°F) 752.4 grams of 97% H₂SO₄ was added and the resulting hydrogel heated to 60°C (140°F) for two hours. A solution containing 139.4 grams aluminum sulfate in 560 cc water was added, followed by 166.7 grams sodium zirconium silicate solution. The mixture was acidified with H₂SO₄ to a pH of 4.7 and left to stand overnight to form a gel.

Example 2

300 grams of the gel prepared in Example 1 was mixed with 14.1 grams of the ammonium form of ZSM-5 and 14.7 grams of ferrous oxalate dihydrate. After blending well, the mixture was dried in vacuo, exchanged two times with 69 grams (NH₄)₂SO₄ in 462 cc H₂O, washed to remove sodium and sulfate and oven dried. One half of the dried material was calcined in air for three hours at 538°C (1000°F). The finished catalyst contained 7.7% iron and 0.02% sodium.

Example 3

The other half of the catalyst prepared in Example 2 was treated in nitrogen for three hours at 538°C (1000°F). The iron content was 7.7%.

Example 4

One hundred grams of the gel prepared in Example 1 was mixed with 7.5 grams ferrous sulfate 7-hydrate in 30 cc of water, followed by the addition of 5.0 grams oxalic acid dihydrate dissolved in 40 cc of water. To this mixture was added 4.7 grams of ammonium ZSM-5 zeolite, and after homogenization and drying in vacuo, the catalyst was exchanged twice with 23 grams of ammonium sulfate in 155 cc H₂O, and washed until free of sulfate ion. After drying at ca. 46°C (115°F) the finished catalysts contained 7.8% iron.

Example 5

The procedure used in Example 4 was repeated with the exception that sufficient ferrous sulfate heptahydrate was used to give a finished catalyst containing 13.1% iron.

Example 6

The procedure of Example 4 was repeated with the exception that sufficient iron sulfate heptahydrate was used to give 16.1% iron in the finished catalyst.

Example 7 (Comparative)

Q-Brand silicate solution (7972.2 grams) was added to a water slurry containing 1861 grams WP kaolin clay in 38 kg (83.7 lbs) of water. After heating to 49°C (120°F) 752.4 grams of 97% H₂SO₄ was added and the resulting hydrogel heated to 60°C (140°F) for two hours. A solution containing 139.4 grams aluminum sulfate in 560 cc water was added, followed by 166.7 grams sodium zirconium silicate solution. The mixture was acidified with H₂SO₄ to a pH of 4.7 and left to stand overnight. After removal of 2000 grams of the gel for other studies, 2563 grams of the ammonium form of ZSM-5 slurried with 8000 cc H₂O was added to the remainder of the gel, and the mixture homogenized and spray-dried. The gel was exchanged twice with 2723.5 grams (6 lbs) of ammonium sulfate in 18.2 kg (40 lbs) H₂O and washed until free of sulfate, followed by drying at 121°C (250°F). The Na content was less than 0.01%. 10.0 grams of the above was impregnated with a solution containing 6.70 grams of ferric oxalate, Fe₂(C₂O₄)₃ · 6H₂O in 60 cc of water. After drying in vacuo and calcining in air for three hours at 538°C (1000°F) the finished catalyst contained 8.5% iron (Ex. 7a). (A portion of this catalyst was maintained in the uncalcined state, labeled 7b).

It is to be noted that ferric oxalate is water-soluble so that this example is outside the scope of the instant invention.

Example 8

A fluid catalyst matrix was prepared by adding 10,722 grams Q-Brand sodium silicate to a slurry of 930 grams kaolin clay in 51.1 kg (112.5 lbs) H₂O. After heating to 49°C (120°F) 1012 grams of 97% H₂SO₄ was added. At pH 10.51 the gel was heated to 60°C (140°F) for two hours and a solution of 186.6 grams aluminum sulfate in 746 cc H₂O was added, followed by 166.7 grams of sodium zirconium silicate in 1617 cc H₂O. The pH was adjusted to 4.58 by addition of H₂SO₄ and left to stand overnight.

Example 9

The catalyst of this example was prepared by filtering one-half of the gel matrix prepared in Example 8. The filter cake was slurried with 300 grams (NH₄)₂SO₄ in 6 liters of water, filtered again, and washed with water until the washings were free of sulfate. The gel was homogenized with the addition of 1132 grams of low sodium ZSM-5 zeolite (30.6% solid content) in 3400 cc H₂O and 1204 grams

ferrous oxalate dihydrate, and the mixture spray dried. An air calcination for 3 hours at 538°C (1000°F) gave the finished catalyst which contained 9.9% iron. Other properties are listed below:

Properties of iron/ZSM-5 fluid syn gas catalysts

Composition, Wt. %	
SiO ₂	73.8
Al ₂ O ₃	6.1
Fe ₂ O ₃ (fe)	14.2 (9.9)
ZrO ₂	1.5
HZSM-5	30
SiO ₂ /Al ₂ O ₃ (zeolite)	70/1
Surface area, m ² /g (BET)	
Particle density, g/cc	.575
Real density, g/cc	2.65
Packed density, g/cc	0.35
Pore volume, cc/g	0.91

Particle size distribution

μm	Calculated wt. %
0—20	2.2
0—30	4.3
0—40	9.1
0—60	28.8
0—80	56.4
0—100	79.3
Mean diameter	75.6 μm

Example 10

One hundred grams of the fluid matrix prepared in Example 9 was mixed with 8.65 grams ferrous sulfate · 7H₂O and 1.00 grams copper sulfate in 100 cc H₂O. Oxalic acid dihydrate (11.5 grams) in 100 cc of water was added followed by 4.7 grams of low sodium form ZSM-5 (11% dry solids). The mixture was homogenized, dried, and washed until sulfate-free. After drying and calcining at 538°C (1000°F) for 3 hours, the finished catalyst contained 8.6% iron and 2.7% copper.

Example 11

The procedure of Example 10 was followed with the exception that the CuSO₄ was replaced with 2.54 grams Cr₂(SO₄)₃. The finished catalyst contained 11.6% iron and 0.15% chromium after calcination.

Example 12

One hundred grams of the fluid gel matrix prepared in Example 9 was exchanged with ammonium sulfate and washed with water until sulfate-free. A solution containing 12.9 grams iron (II) gluconate in 200 cc was added, followed by 5.3 grams oxalic acid dihydrate in 40 cc H₂O and 9.79 grams low sodium ZSM-5. The mixture was homogenized, filtered, dried and calcined at 538°C (1000°F) for 3 hours giving a finished catalyst with 5.7% iron content.

Example 13

A fluid catalyst gel matrix for this example was prepared by adding 10,722 grams Q-Brand sodium silicate to a slurry containing 930 grams of WP kaolin clay in 51.1 kg (112.5 lbs) H₂O. The procedure of Example 8 was followed identically. The next day the gel was divided into three equal portions.

Example 14

A one-third portion of the gel prepared in Example 13 was filtered, and the filter cake was slurried with a solution containing 1364 grams FeSO₄ · 7H₂O in 5400 cc water, followed by the addition of 682 grams oxalic acid dihydrate in 6300 cc H₂O. After filtration, the gel was slurried with 300 ppm ammonium sulfate dissolved in 6 liters of water, refiltered and washed with water until the washings were sulfate-free. A slurry containing 755 grams of acid ZSM-5 (30.6% solids) in 3750 cc H₂O was added and the mixture was homogenized and spray-dried. The finished catalyst after calcination in air at 538°C (1000°F) for 3 hours contained 12.7% iron. Other properties are listed in the following table

TABLE

Zeolite/iron wt. ratio=0.92

Surface area (BET)	358 m ² /g
Density, real	2.55 g/cc
Density, particle	1.30 g/cc
Density, packed	0.37 g/cc
Powder pore volume	0.36 cc/g

Particle size, μm	Wt. %
0—20	1.7
0—30	8.9
0—40	20.3
0—60	43.6
0—80	60.8
0—100	72.3
Mean particle diameter	64.0 μm

Example 15

The catalyst of this example was prepared by contacting one-third of the gel prepared in Example 13 with a solution containing 300 grams ammonium sulfate in 6 liters H₂O for one hour. The gel was then filtered and washed with water until the washings appeared sulfate-free. A solution containing 2783 grams FeSO₄ · 7H₂O in 10.8 liters H₂O was slurried with the gel cake and the mixture heated to 49°C (120°F) after which a hot 65°C (150°F) solution containing 1391 grams H₂C₂O₄ · 2H₂O in 10 liters H₂O was added. After filtration and water washing to remove sulfate ions, the gel cake was mixed with 1270 grams acid ZSM-5 (30.6% solids) in 6780 cc H₂O, homogenized, and spray-dried. The finished catalyst was calcined in air at 538°C (1000°F) for three hours and contained 23.8% iron. Other properties are shown in the following table:

TABLE

Zeolite/iron wt. ratio=0.67

Surface area, m ² /g (BET)	267
Density, real, g/cc	2.90
Density, particle, g/cc	1.68
Density, packed, g/cc	0.36

Particle size, μm	Wt. %
0—20	17.6
0—30	26.9
0—40	37.1
0—60	56.6
0—80	72.0
0—100	82.6
Mean particle diameter	50.5 μm

Example 16

A pure silica-base catalyst was prepared by mixing 37.0 grams of an aqueous silica sol (sold as Ludox-LS® by E.I. du Pont de Nemours & Co.) with 7.0 grams ferrous oxalate dihydrate and 1.4 grams of ZSM-5 in the ammonium form. After homogenizing and drying, the finished catalyst contained 10.5% iron.

Example 17

A clay-free silica gel matrix with small amount of zirconia and alumina added to enhance physical properties was prepared by adding 205 cc of 97% H₂SO₄ to a warm 49°C (120°F) solution containing 3986 grams Q-Brand sodium silicate in 19 kg (41.85 lbs) of deionized water. The gel after heating to 60°C (140°F) for two hours and cooled was mixed with 70 grams aluminum sulfate in 280 cc H₂O, followed by 83 grams of sodium zirconium silicate in 805 cc H₂O, which was acidified with 55 cc of sulfuric acid. The pH was adjusted to 4.68 by addition of 20% H₂SO₄ solution and stirred gently over ca. 65 hours.

Example 18

This catalyst was prepared by adding a solution containing 11.5 grams of FeSO₄ · 7H₂O in 45 cc H₂O to 137.1 grams of the gel prepared in Example 17 which contained 8.97% solids on a dry basis. A solution of 7.7 grams oxalic acid dihydrate in 65 cc H₂O was then added to the gel, followed by 4.6

grams of ZSM-5 in the ammonium form. After homogenizing and drying, the catalyst was contacted twice with a solution containing 46 grams ammonium sulfate in 300 cc water and finally washed until sulfate-free. The dry, finished catalyst contained 11.1% iron.

5 Example 19

This catalyst was prepared in manner identical to that in Example 18 except one-half the amount of zeolite was used. The finished catalyst contained 11.9% iron.

Example 20

10 This example illustrates the use of pure alumina as a binder for the metal and zeolite components. The catalyst was prepared by blending together 7.0 grams $\text{FeC}_2\text{O}_4 \cdot 2\text{H}_2\text{O}$, 4.4 grams ammonium ZSM-5, and 11.7 grams α -alumina monohydrate. The catalyst contained 9.1% iron in finished form.

Example 21 (Comparative)

15 This catalyst was prepared by blending 4.4 grams ammonium ZSM-5 and 11.7 grams alpha-alumina monohydrate and impregnating the mixture with 15.72 grams $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ dissolved in 17 cc H_2O . After drying, the calcined catalyst (538°C for 3 hours) contained 7.5% iron.

This catalyst was prepared by impregnation and is outside the scope of this invention.

20 Example 22

Another pure alumina supported catalyst was prepared by adding 40.8 grams Q-Loid® A-30 alumina dispersion (24.77% solids) to a solution of 12.9 grams iron (II) gluconate in 75 cc H_2O at 60°C (140°F). A solution containing 5.3 grams oxalic acid dihydrate in 45 cc H_2O was then added, followed by 9.79 grams of low sodium ZSM-5 (30.6% solids). The finished catalyst, dried and calcined 25 at 538°C (1000°F) for three hours, contained 4.25% iron.

Example 23 is illustrative of catalysts prepared by combining highly dispersed silica and alumina fluid matrices. This example incorporates the metal and ZSM-5 class zeolite in a matrix prepared by mixing colloidal dispersions of silica and alumina and shows improved physical properties and higher activity and selectivity for the mixed sol matrix.

30

Example 23

The mixed silica-alumina sol catalyst was prepared by adding 2000 grams Ludox-LS® silica sol in 1535 cc of water to a clay dispersion containing 348.8 grams WP kaolin in 4667 cc H_2O . An alumina dispersion prepared by the addition of 666.7 grams Dispal-M® alumina to 40 grams of 70% nitric acid+6040 cc. water was then added to the above-prepared silica-clay mixture, followed by 3268 35 grams of the low sodium form of ZSM-5 in 2488 cc H_2O . Finally, a slurry containing 1049 grams ferrous oxalate dihydrate in 2489 cc H_2O was added and the mixture was then homogenized and spray-dried. The fluidized bed catalyst was heated in nitrogen at ca. 593°C (1100°F) for three hours followed by a final air calcination for three hours at 538°C (1000°F). The finished catalyst contained 9.1% iron. 40 Other properties are listed below:

TABLE

Composition, wt. %		
45	SiO_2	21
	Al_2O_3	21
	Clay	11
	HZSM-5	34
	Fe_2O_3	13
50	Real density, g/cc	2.72
	Packed density, g/cc	0.50
	Pore volume, cc/g	0.48
	Zeolite/iron wt. ratio	3.8
Particle size, μm		Wt. %
55	0—20	0.6
	0—30	9.6
	0—40	28.2
	0—60	61.1
60	0—80	78.1
	0—100	86.2
	Mean particle diameter	53.0 μm

65 (Examples 24 through 27 illustrate the use of fluid silica-alumina of different ratios and optionally a clay weighting agent as catalyst matrices).

Example 24

A gel matrix with a $\text{SiO}_2/\text{Al}_2\text{O}_3/\text{clay}$ ratio of 60:20:20 was prepared by adding 8333 grams Q-Brand sodium silicate to a slurry of 930 grams WP kaolin clay in 40 kg (87.4 lbs) of water. After heating to 49°C (120°F) 786.5 grams of 70% H_2SO_4 was added. After one hour at 49°C (120°F) a solution containing 4665 grams aluminum sulfate in 18,659 cc H_2O was added and the gel stirred overnight at pH 4.5. The gel was then filtered and washed with 4 volumes of 5% $(\text{NH}_4)_2\text{SO}_4$ solution, followed by water until the washings were free of sulfate. One third of the gel matrix which contained 10.92% solids was mixed with 1177 grams $\text{FeC}_2\text{O}_4 \cdot 2\text{H}_2\text{O}$ + 4000 cc H_2O and 3409 grams low sodium ZSM-5 (30.6% solids) + 2000 cc H_2O , and the mixture was homogenized and spray-dried. The calcined (538°C (1000°F)/3 hr) catalyst contained 11.9% iron. Other properties are listed in the following Table.

TABLE

Pore volume, cc/g	0.76
Packed density, g/cc	0.31
Real density, g/cc	2.52
Particle density, g/cc	1.3
Surface area, m^2/g (BET)	399
Particle size, μm	Wt. %
0—20	3.3
0—30	5.3
0—40	9.7
0—60	26.6
0—80	50.5
0—100	72.6
Mean particle diameter	80.7 μm

Example 25

A gel with a $\text{SiO}_2/\text{Al}_2\text{O}_3/\text{clay}$ ratio of 69.75:5.25:25 was prepared in the manner of Example 24. After washing, 72.8 grams of the gel containing 13.88% solids was homogenized with 7.7 grams $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ in 30 cc H_2O , 5.2 grams $\text{H}_2\text{C}_2\text{O}_4 \cdot 2\text{H}_2\text{O}$ in 35 cc H_2O , and 3.0 grams ammonium ZSM-5. The dried catalyst was exchanged twice with 23 grams $(\text{NH}_4)_2\text{SO}_4$ in 150 cc H_2O and washed until sulfate-free. The dried, finished catalyst contained 5.0% iron.

Example 26 (Comparative)

In this example a spray-dried catalyst with a $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratio (clay-free) of 87:13 was prepared by cogelling sodium silicate and aluminum sulfate and adding 40 wt. % HZSM-5. Ten grams of the ammonium sulfate exchanged, washed and calcined (482°C (900°F)) catalyst was then impregnated with 12.5 grams $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ in 6 cc H_2O and dried. After calcining for 3 hours at 538°C (1000°F) the finished catalyst contained approximately 13% iron.

Example 27 (Comparative)

This example illustrates a ferric nitrate impregnated version of a mixed $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3$ sol catalyst for comparison with Example 23.

A spray-dried $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3 \cdot \text{clay}$ matrix was prepared in a manner similar to that of Example 23 with the exception that ferrous oxalate was not added. The matrix properties are shown in the following Table.

TABLE

Matrix composition, wt. %	
SiO_2	29
Al_2O_3	24
Clay	12
HZSM-5	40
Pore volume, cc/g	0.58
Packed density, g/cc	0.53
Particle size, μm	Wt. %
0—20	13.1
0—30	26.8
0—40	40.0
0—60	60.6
0—80	74.1
0—100	82.7
Mean particle diameter	71.2 μm

Fifteen grams of this matrix was impregnated with 15.2 gm $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ dissolved in 9 cc deionized water. After drying and calcining for 3 hours at 538°C (1000°F) in air, the finished catalyst contained 10.7% iron.

The catalysts were evaluated for the conversion of syngas to gasoline at 1480 kPa (200 psig) and a 1:1 CO/H_2 ratio. The following table gives the results obtained during the second day (except as noted) of the evaluation after the catalysts has been conditioned in CO/H_2 for the times and temperatures listed in the table.

Example	2	3	4
10	day 1		
Run time, hours	42	18	18
GHSV	591	604	627
15 WHSV	0.94	0.98	0.92
Temp., °C, average	291 (556°F)	294 (562°F)	288 (550°F)
Hot spot	301 (574°F)	301 (574°F)	298 (568°F)
CO Conversion, wt. %	51.4	48.6	83.9
H ₂ Conversion, wt. %	55.9	54.7	68.1
20 % wt. C Converted to:			
Hydrocarbon	66.9	67.5	57.3
Product yield, wt. %			
HC	16.4	14.2	23.4
H ₂ O	16.7	12.0	7.4
25 H ₂	3.3	3.6	2.5
CO	44.9	47.3	14.9
CO ₂	24.7	22.9	51.9
Hydrocarbon composition, wt. %			
C ₁	21.8	22.0	20.3
30 C ₂	7.2	5.4	11.3
C ₃	4.8	7.8	5.6
C ₄	10.7	14.5	7.2
C ₅	9.4	7.4	7.5
C ₆ ⁺	55.5	43.0	48.1
35 Olefins, wt. % by C No.			
C ₂ =	14.8	23.8	5.3
C ₃ =	5.6	0	0.2
C ₄ =	9.3	1.0	21.3
C ₅ =	11.9	10.9	38.8
40 C ₅ Olefin distribution, wt. %			
C ₅ =1 (1-pentene)	1.6	1.7	1.8
2MIC ₄ =(2-methylbutene-1)	14.7	13.8	16.1
3MIC ₄ =(3-methylbutene-1)	1.1	0.9	1.2
T2C ₅ =(trans-pentene-2)	12.5	12.9	11.3
45 C ₂ C ₃ =(cis-pentene-2)	4.9	5.2	5.3
2M2C ₄ =(2-methylbutene-2)	65.2	65.5	64.5
C ₆ ⁺ Aromatics, wt. %	21.2	19.9	12.2
Liq. prod. 90% pt., °C (ASTM D-2887)	182—22 (360°F)	197—22 (387°F)	195 (383°F)
50 Conditioned in 1:1 CO/H ₂ °C/hr.	315—55 (600°F)/65	315—55 (600°F)/65	325—55 (618°F)/16
55 Example	5	6	7a (comparative)
Run time, hours	18	42	18
GHSV	708	741	994
WHSV	0.97	0.94	1.02
60 Temp., °C, average	280 (537°F)	280 (537°F)	285 (546°F)
Hot spot	296 (565°F)	296 (565°F)	296 (566°F)
CO Conversion, wt. %	90.5	86.3	49.4
H ₂ Conversion, wt. %	71.4	70.7	56.3
65 % Wt. C converted to Hydrocarbon	56.8	58.0	60.1

Example	5	6	7a (comparative)
Product yield, wt. %			
5 HC	25.7	25.4	14.9
H ₂ O	6.6	7.3	6.3
H ₂	2.2	2.3	3.2
CO	8.8	12.6	46.8
CO ₂	56.6	52.4	28.7
Hydrocarbon composition, wt. %			
10 C ₁	19.1	16.3	20.4
C ₂	11.1	10.3	13.2
C ₃	5.3	5.9	19.3
C ₄	7.0	7.1	13.5
15 C ₅	8.6	10.6	3.8
C ₆ ⁺	48.9	49.9	29.8
Olefins, wt. % by C no.			
C ₂ =	3.1	9.4	24.1
C ₃ =	12.2	21.3	59.2
20 C ₄ =	33.6	56.8	71.5
C ₅ =	47.2	72.0	89.0
C₅ Olefin distribution, wt. %			
C ₅ =1	1.6	1.8	4.6
25 2MIC ₄ =	16.9	16.0	9.8
3MIC ₄ =	1.3	1.3	0.7
T2C ₅ =	10.9	11.9	28.1
C ₂ C ₅ =	5.3	5.8	14.0
2M2C ₄ =	64.0	63.1	42.8
C ₆ ⁺ Aromatics, wt. %	5.9	0.4	0.4
30 Liq. product 90% pt., °C (D-2887)	199 (391°F)	202 (396°F)	179 (354°F)
Conditioned in 1:1 CO/H₂, °C			
	324 (616°F)/18.5	324 (615°F)/18.5	320 (609°F)/17
7b (comparative)			
Example	9	10	
Run time, hours			
18	18	18	
40 GHSV	670	583	477
WHSV	1.02	1.13	1.07
Temp., °C average	291 (555°F)	295 (563°F)	291 (555°F)
Hot spot	297 (567°F)	301 (574°F)	298 (568°F)
CO Conversion, wt. %	47.2	71.0	75.4
45 H ₂ Conversion, wt. %	54.0	62.5	65.3
% Wt. C converted to:			
Hydrocarbon	66.9	59.6	58.1
Product yield, wt. %			
50 HC	14.8	20.5	21.2
H ₂ O	10.0	7.8	7.3
H ₂	3.3	2.7	2.5
CO	49.1	27.0	22.8
CO ₂	22.8	42.0	46.2
Hydrocarbon composition, wt. %			
55 C ₁	20.7	18.8	21.3
C ₂	10.1	8.5	13.9
C ₃	4.3	5.7	5.8
C ₄	9.6	9.9	8.1
C ₅	8.0	7.6	7.7
60 C ₆ ⁺	47.4	49.6	43.2
Olefins, wt. % by C no.			
C ₂ =	15.3	10.6	5.9
C ₃ =	20.4	3.6	3.1
C ₄ =	25.0	17.4	29.5
65 C ₅ =	30.8	25.1	46.9

Example		7b (comparative)	9	10
C ₅ Olefin distribution, wt. %				
5	C ₅ =1	1.1	1.8	1.3
	2MIC ₄ =	12.9	14.4	13.7
	3MIC ₄ =	0.8	1.0	1.0
	T2C ₅ =	11.6	12.8	11.0
	C ₂ C ₅ =	5.0	5.9	5.0
10	2M2C ₄ =	68.6	64.1	67.9
C ₆ ⁺ Aromatics, wt. %		14.8	18.1	8.5
Liq. prod. 90% pt., °C (D-2887)		171 (340°F)	193 (379°F)	177 (351°F)
Conditioned in 1:1 CO/H ₂ , °C		321 (609°F)/17	321 (610°F)/17	316 (600°F)/17
Example		11	12	14
Run time, hours		18	18	18
20	GHSV	563	612	661
	WHSV	1.21	0.96	0.97
Temp., °C average		283 (542°F)	291 (556°F)	291 (556°F)
Hot spot		298 (568°F)	299 (571°F)	299 (570°F)
CO Conversion, wt. %		79.15	61.6	74.5
25	H ₂ Conversion, wt. %	67.25	66.1	68.9
% Wt. C converted to:				
Hydrocarbon		58.0	61.2	57.5
Product yield, wt. %				
HC		21.4	18.1	20.9
30	H ₂ O	8.3	9.1	7.3
	H ₂	2.3	2.7	2.5
	CO	19.4	35.4	23.5
	CO ₂	48.6	34.5	45.8
Hydrocarbon composition, wt. %				
35	C ₁	17.9	16.8	17.8
	C ₂	11.2	6.6	9.5
	C ₃	6.9	3.6	4.4
	C ₄	5.7	9.1	8.2
	C ₅	7.2	9.7	9.3
40	C ₆ ⁺	51.2	54.1	50.7
Olefins wt. % by C no.				
C ₂ =		9.1	21.8	16.6
C ₃ =		49.2	20.3	16.1
C ₄ =		52.5	25.9	39.9
45	C ₅ =	61.8	34.0	57.1
C ₅ Olefin distribution, wt. %				
C ₅ =1		1.5	1.3	2.0
2MIC ₄ =		14.9	13.4	16.9
3MIC ₄ =		1.0	1.0	1.3
50	T2C ₅ =	11.3	12.4	12.1
C ₂ C ₅ =		5.3	5.5	6.0
2M2C ₄ =		66.1	66.4	61.6
C ₆ ⁺ Aromatics, wt. %		6.3	15.0	8.7
Liq. prod. 90% pt., °C (D-2887)		209 (408°F)	193 (380°F)	189 (373°F)
Conditioned in 1:1 CO/H ₂ , °C		320 (609°F)/17	321 (610°F)/17	321 (610°F)/17
Example		15	16	18
Run time, hours		18	20.8	18
60	GHSV	541	1042	688
	WHSV	0.99	1.01	0.99
Temp., °C average		292 (558°F)	287 (548°F)	287 (548°F)
65	Hot spot	298 (568°F)	296 (564°F)	298 (568°F)

Example	15	16	18
CO Conversion, wt. %	53.0	60.7	61.9
H ₂ Conversion, wt. %	50.1	59.7	64.0
5 % Wt. C converted to:			
Hydrocarbon	56.0	62.0	64.4
Product yield, wt. %			
HC	13.4	17.3	19.2
H ₂ O	5.5	9.6	10.7
10 H ₂	3.8	2.8	2.6
CO	43.6	36.6	35.4
CO ₂	34.0	33.7	32.2
Hydrocarbon composition, wt. %			
C ₁	30.8	15.7	18.1
15 C ₂	22.1	10.1	9.3
C ₃	6.9	15.8	8.4
C ₄	10.3	12.0	9.9
C ₅	5.2	10.7	10.7
C ₆ ⁺	24.8	35.8	43.6
20 Olefins, wt. % by C no.			
C ₂ =	8.8	28.0	38.8
C ₃ =	0	74.6	64.2
C ₄ =	26.6	77.2	78.6
C ₅ =	37.4	78.0	84.2
25 C ₅ Olefin distribution, wt. %			
C ₅ =1	1.2	26.9	3.4
2MIC ₄ =	14.8	4.3	14.6
3MIC ₄ =	0.8	3.1	1.2
T2C ₅ =	11.3	35.8	19.6
30 C ₂ C ₅ =	5.1	21.5	9.6
2M2C ₄ =	66.8	8.5	51.5
C ₆ ⁺ Aromatics, wt. %	7.3	0.2	0.4
Liq. prod. 90% pt., °C (D-2887)	199 (391°F)	231 (448°F)	195 (383°F)
35 Conditioned in 1:1 CO/H ₂ , °C	322 (612°F)/17	318 (604°F)/16	323 (613°F)/15

Example	19	20	21 (comparative)
40 Run time, hours	20.5	40.5	18
GHSV	680	997	891
WHSV	0.98	1.02	1.01
Temp., °C average	287 (548°F)	282 (539°F)	294 (562°F)
45 Hot spot	301 (574°F)	298 (568°F)	298 (568°F)
CO Conversion, wt. %	81.7	92.0	27.3
H ₂ Conversion, wt. %	69.6	75.1	36.4
% Wt. C converted to:			
Hydrocarbon	57.3	57.5	73.7
50 Product yield, wt. %			
HC	22.0	26.1	8.7
H ₂ O	7.9	7.7	8.7
H ₂	2.1	1.8	4.5
CO	17.1	7.4	67.6
55 CO ₂	50.9	57.1	10.5
Hydrocarbon composition, wt. %			
C ₁	18.2	16.5	22.2
C ₂	10.6	7.9	7.5
C ₃	16.0	4.5	6.6
60 C ₄	11.7	7.4	16.6
C ₅	9.9	11.4	8.2
C ₆ ⁺	33.7	52.4	38.9
Olefins, wt. % by C no.			
C ₂ =	22.0	9.3	28.0
65 C ₃ =	65.6	14.8	0

Example	19	20	21 (comparative)
5 C ₄ =	78.9	46.0	11.2
C ₅ =	78.5	62.3	13.2
C ₅ Olefin distribution, wt. %			
C ₅ =1	18.6	1.9	1.1
2MIC ₄ =	3.8	17.4	14.9
3MIC ₄ =	4.1	1.5	0
10 T2C ₅ =	39.5	11.5	13.8
C ₂ C ₅ =	21.6	5.7	6.4
2M2C ₄ =	12.4	62.0	63.8
C ₈ + Aromatics, wt. %	0.2	1.3	18.4
Liq. prod. 90% pt., °C (D-2887)	247 (477°F)	193 (379°F)	(358°F)
15 Conditioned in 1:1 CO/H ₂ °C/hr.	322 (612°F)/64.5	381 (605°F)/64	321 (610°F)/22
Example	22	23	24
20 Run time, hours	18	18	18
GHSV	821	831	788
WHSV	0.96	0.99	1.06
Temp., °C average	289 (553°F)	289 (552°F)	290 (554°F)
25 Hot spot	297 (566°F)	299 (570°F)	299 (570°F)
CO Conversion, wt. %	25.2	87.3	58.2
H ₂ Conversion, wt. %	51.5	70.3	50.7
% Wt. C converted to:			
Hydrocarbon	86.2	56.1	62.3
30 Product yield, wt. %			
HC	10.2	23.5	16.4
H ₂ O	12.0	6.9	9.1
H ₂	3.9	2.3	3.3
CO	68.9	11.7	39.0
35 CO ₂	5.0	55.6	32.2
Hydrocarbon composition, wt. %			
C ₁	15.3	17.9	20.7
C ₂	5.5	6.8	6.5
C ₃	4.1	5.5	5.7
40 C ₄	11.7	10.0	12.0
C ₅	10.3	5.6	4.0
C ₈ +	53.1	54.1	51.2
Olefins, wt. % by C no.			
C ₂ =	48.3	5.6	21.5
45 C ₃ =	36.2	12.8	0
C ₄ =	41.8	13.4	5.1
C ₅ =	55.8	17.6	6.3
C ₅ Olefin distribution, wt. %			
C ₅ =1	1.7	1.3	0
50 2MIC ₄ =	16.7	15.6	15.4
3MIC ₄ =	1.2	0.9	0
T2C ₅ =	11.6	12.1	12.8
C ₂ C ₅ =	5.8	5.6	5.1
2M2C ₄ =	63.0	64.5	66.7
55 C ₈ + Aromatics, wt. %	11.1	19.2	33.8
Liq. prod. 90% pt., °C (D-2887)	184 (364°F)	197 (387°F)	196 (385°F)
Conditioned in 1:1 CO/H ₂ °C/hr.	321 (615°F)/17	321 (610°F)/17	322 (610°F)/17
60			
Example	25	26 (comparative)	27 (comparative)
Run time, hours	18	18	18
65 GHSV	906	626	928

Example	25	26 (comparative)	27 (comparative)
WHSV	0.97	0.98	1.06
5 Temp., °C average	287 (548°F)	292 (557°F)	293 (559°F)
Hot spot	291 (566°F)	297 (567°F)	301 (574°F)
CO Conversion, wt. %	75.2	33.4	43.6
H ₂ Conversion, wt. %	65.8	45.8	48.2
% Wt. C converted to:			
10 Hydrocarbon	59.4	74.3	
Product yield, wt. %			
HC	21.9	11.3	15.1
H ₂ O	8.5	9.4	12.7
H ₂	2.7	3.8	3.4
15 CO	22.9	61.9	52.7
CO ₂	44.1	13.6	16.2
Hydrocarbon composition, wt. %			
C ₁	18.2	19.7	13.4
C ₂	12.1	9.3	5.6
20 C ₃	6.5	3.6	3.7
C ₄	8.5	11.6	18.8
C ₅	9.6	8.7	13.9
C ₆ ⁺	45.1	47.1	44.7
Olefin, wt. % by C no.			
25 C ₂ =	7.5	21.4	
C ₃ =	21.1	36.1	
C ₄ =	47.2	27.9	
C ₅ =	60.8	29.1	
C ₅ Olefin distribution, wt. %			
30 C ₅ =1	2.0	1.4	
2MIC ₄ =	17.4	15.8	
3MIC ₄ =	1.5	1.1	
T2C ₅ =	12.1	11.6	
C ₂ C ₅ =	6.0	5.6	
35 2M2C ₄ =	61.1	64.6	
C ₆ ⁺ Aromatics, wt. %	4.4	12.0	13.6
Liq. prod. 90% pt., °C (D-2887)	188 (370°F)	188 (371°F)	192 (378°F)
40 Conditioned in 1:1 CO/H ₂ , °C/hr.	316 (600°F)/17	316 (600°F)/15	322 (612°F)/17

The data presented in the above table vividly demonstrates the superiority of the catalyst prepared in accordance with the instant invention.

Thus, Example 2 is a catalyst prepared in accordance with the instant invention using ferrous oxalate. Example 7a and 7b use the water soluble compound ferric oxalate. Note that Example 2 yielded 64.9 wt. % C₅⁺ whereas Example 7a gave 33.6 wt. % and Example 7b 55.4 wt. %.

Note that the in situ formation of ferrous oxalate resulted in more active catalysts than adding ferrous oxalate directly. Compare Examples 2 and 4 wherein it can be seen that the in situ preparation (Example 4) was more active in that it converted 83.9 wt. % CO as opposed to 51.4 wt. % and yielded more hydrocarbons, i.e. 23.4 wt. % as opposed to 16.4 wt. %.

Note that the catalyst of Example 27, i.e. CO conversion of 87.3 wt. % as opposed to 43.6. Total hydrocarbons were 23.5 wt. % versus only 15.1 wt. %.

Claims

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1. A catalyst composition prepared by forming a mixture of an iron compound, a matrix material and an acidic crystalline aluminosilicate zeolite having a silica-to-alumina ratio of at least 12, a pore size greater than about 5 Angstrom units and a constraint index of about 1 to 12, characterised in that the iron compound is a water-insoluble derivative of an organic compound and said mixture is dried and treated with carbon monoxide or mixtures containing the same at temperatures of 288 to 343°C for a period of time from $\frac{1}{2}$ hour to 24 hours.

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2. A composition according to claim 1 which has been spray-dried to produce particles of a size range appropriate for use in a fluidized-bed reactor.

3. A composition according to claim 1 or claim 2 wherein said iron compound is ferrous oxalate.

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4. A composition according to claim 3 wherein said iron oxalate is formed in situ.

Example	25	26 (comparative)	27 (comparative)
WHSV	0.97	0.98	1.06
5 Temp., °C average	287 (548°F)	292 (557°F)	293 (559°F)
Hot spot	291 (566°F)	297 (567°F)	301 (574°F)
CO Conversion, wt. %	75.2	33.4	43.6
H ₂ Conversion, wt. %	65.8	45.8	48.2
% Wt. C converted to:			
10 Hydrocarbon	59.4	74.3	
Product yield, wt. %			
HC	21.9	11.3	15.1
H ₂ O	8.5	9.4	12.7
H ₂	2.7	3.8	3.4
15 CO	22.9	61.9	52.7
CO ₂	44.1	13.6	16.2
Hydrocarbon composition, wt. %			
C ₁	18.2	19.7	13.4
C ₂	12.1	9.3	5.6
20 C ₃	6.5	3.6	3.7
C ₄	8.5	11.6	18.8
C ₅	9.6	8.7	13.9
C ₆ ⁺	45.1	47.1	44.7
Olefin, wt. % by C no.			
25 C ₂ =	7.5	21.4	
C ₃ =	21.1	36.1	
C ₄ =	47.2	27.9	
C ₅ =	60.8	29.1	
C ₅ Olefin distribution, wt. %			
30 C ₅ =1	2.0	1.4	
2MIC ₄ =	17.4	15.8	
3MIC ₄ =	1.5	1.1	
T2C ₅ =	12.1	11.6	
C ₂ C ₅ =	6.0	5.6	
35 2M2C ₄ =	61.1	64.6	
C ₆ ⁺ Aromatics, wt. %	4.4	12.0	13.6
Liq. prod. 90% pt., °C (D-2887)	188 (370°F)	188 (371°F)	192 (378°F)
40 Conditioned in 1:1 CO/H ₂ , °C/hr.	316 (600°F)/17	316 (600°F)/15	322 (612°F)/17

The data presented in the above table vividly demonstrates the superiority of the catalyst prepared in accordance with the instant invention.

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Claims

1. A catalyst composition prepared by forming a mixture of an iron compound, a matrix material and an acidic crystalline aluminosilicate zeolite having a silica-to-alumina ratio of at least 12, a pore size greater than about 5 Angstrom units and a constraint index of about 1 to 12, characterised in that the iron compound is a water-insoluble derivative of an organic compound and said mixture is dried and treated with carbon monoxide or mixtures containing the same at temperatures of 288 to 343°C for a period of time from $\frac{1}{2}$ hour to 24 hours.
2. A composition according to claim 1 which has been spray-dried to produce particles of a size range appropriate for use in a fluidized-bed reactor.
3. A composition according to claim 1 or claim 2 wherein said iron compound is ferrous oxalate.
4. A composition according to claim 3 wherein said iron oxalate is formed in situ.



5. A composition according to any preceding claim wherein said matrix material is siliceous.
6. A composition according to any of claims 1 to 4 wherein said matrix material comprises alumina.
7. A composition according to any preceding claim wherein said matrix material comprises silica-alumina.
8. A composition according to any of claims 1 to 6 wherein colloidal dispersions of silica and alumina are used.
9. A composition according to any preceding claim wherein the zeolite is ZSM-5.
10. A process for converting synthesis gas which comprises contacting said synthesis gas at a temperature of from 260°C (500°F) to 315°C (600°F) and at a pressure of from 446—6996 kPa (50—1000 psig) characterised in that a catalyst composition as claimed in any of claims 1 to 9 is employed.

Patentansprüche

1. Katalysatorzusammensetzung, hergestellt durch Bilden eines Gemisches aus einer Eisenverbindung, einem Matrixmaterial und einem sauren kristallinen Aluminosilica-Zeolithen mit einem Siliciumdioxid/Aluminiumoxid-Verhältnis von wenigstens 12, einer Porengröße von mehr als etwa 5 Angströmeinheiten und einem Zwangsindex von 1 bis 12, dadurch gekennzeichnet, daß die Eisenverbindung ein wasserunlösliches Derivat einer organischen Verbindung ist und das Gemisch getrocknet und mit Kohlenmonoxid oder dieses enthaltenden Gemischen bei Temperaturen von 288 bis 343°C während einer Zeitdauer von 0,5 h bis 24 h behandelt wird.
2. Zusammensetzung nach Anspruch 1, dadurch gekennzeichnet, daß sie zur Erzeugung von Teilchen eines Größenbereiches, der für die Anwendung in einem Reaktor mit fluidisiertem Bett geeignet ist, sprühtrocknet worden ist.
3. Zusammensetzung nach Anspruch 1 oder 2, dadurch gekennzeichnet, daß die Eisenverbindung Eisen-II-Oxalat ist.
4. Zusammensetzung nach Anspruch 3, dadurch gekennzeichnet, daß das Eisenoxalat in situ gebildet worden ist.
5. Zusammensetzung nach einem der vorhergehenden Ansprüche, dadurch gekennzeichnet, daß das Matrixmaterial siliciumhaltig ist.
6. Zusammensetzung nach einem der Ansprüche 1 bis 4, dadurch gekennzeichnet, daß das Matrixmaterial Aluminiumoxid enthält.
7. Zusammensetzung nach einem der vorhergehenden Ansprüche, dadurch gekennzeichnet, daß das Matrixmaterial Siliciumdioxid/Aluminiumoxid enthält.
8. Zusammensetzung nach einem der Ansprüche 1 bis 6, dadurch gekennzeichnet, daß kolloidale Dispersionen von Siliciumdioxid und Aluminiumoxid verwendet worden sind.
9. Zusammensetzung nach einem der vorhergehenden Ansprüche, dadurch gekennzeichnet, daß der Zeolith ZSM-5 ist.
10. Verfahren zur Umwandlung von Synthesegas, wobei das Synthesegas bei einer Temperatur von 260°C (500°F) bis 315°C (600°F) und bei einem Druck von 446 bis 6996 kPa (50 bis 1000 psig) der Berührung unterworfen wird, dadurch gekennzeichnet, daß eine Katalysatorzusammensetzung gemäß den vorhergehenden Ansprüchen 1 bis 9 verwendet wird.

Revendications

1. Composition catalytique préparée par formation d'un mélange d'un composé de fer, d'une matière de matrice et d'une zéolite d'aluminosilicate cristallin acide ayant un rapport silice/alumine d'au moins 12, une dimension de pores de plus d'environ 5 Å et un indice de contrainte de 1 à 12, caractérisée en ce que le composé de fer est un dérivé insoluble dans l'eau d'un acide organique et ledit mélange est séché et traité par du monoxyde de carbone ou des mélanges le contenant à des températures de 288 à 343°C pendant une durée de 1/2 h à 24 h.
2. Composition selon la revendication 1, qui a été séchée par pulvérisation pour produire des particules d'une granulométrie appropriée pour l'utilisation dans un réacteur à lit fluidisé.
3. Composition selon la revendication 1 ou la revendication 2, dans laquelle ledit composé de fer est l'oxalate ferreux.
4. Composition selon la revendication 3, dans laquelle ledit oxalate de fer est formé in situ.
5. Composition selon l'une quelconque des revendications précédentes, dans laquelle ladite matière de matrice est siliceuse.
6. Composition selon l'une quelconque des revendications 1 à 4, dans laquelle ladite matière de matrice consiste en alumine.
7. Composition selon l'une quelconque des revendications précédentes, dans laquelle ladite matière de matrice consiste en silice-alumine.
8. Composition selon l'une quelconque des revendications 1 à 6, dans laquelle on utilise des dispersions colloïdales de silice et d'alumine.



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9. Composition selon l'une quelconque des revendications précédentes, dans laquelle la zéolite est la ZSM-5.

10. Procédé pour convertir un gaz de synthèse qui consiste à mettre en contact ledit gaz de synthèse à une température de 260°C (500°F) à 315°C (600°F) et sous une pression de 446—6996 kPa (50—1000 psig), caractérisée en ce qu'on utilise une composition catalytique telle que revendiquée dans l'une quelconque des revendications 1 à 9.

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