CLAIMS:

1. A method for treating a distillate boiling range feed, comprising:

exposing a distillate boiling range feed to a hydrotreating catalyst under effective hydrotreating conditions to form a hydrotreated effluent; and

exposing at least a portion of the hydrotreated effluent having an organic nitrogen content of about 10 wppm to about 60 wppm to a dewaxing catalyst under effective dewaxing conditions to form a dewaxed effluent comprising a diesel boiling range product, the dewaxing catalyst comprising one or more hydrogenation metals supported on a bound molecular sieve having a MEL framework structure, the effective dewaxing conditions comprising a H_2 pressure of about 800 psig or less;

wherein the dewaxing catalyst comprises about 3 wt % to about 30 wt % of one or more Group 6 metals, one or more Group 8-10 non-noble metals, or a combination thereof; and

wherein the one or more hydrogenation metals are impregnated using an impregnation solution comprising a dispersion agent, the dispersion agent comprising 2-10 carbon atoms and having a carbon to oxygen ratio of about 0.6 to about 2.

2. The method of claim 1, wherein the dewaxing catalyst has a ratio of molecular sieve to binder by weight of about 1.0 or less.

3. The method of claim 1, wherein the molecular sieve comprises ZSM-11.

4. The method of claim 1, wherein the H_2 pressure is between 150 psig and 800 psig.

5. The method of claim 1, wherein the organic nitrogen content is between 10 wppm and 30 wppm.

6. The method of claim 1, wherein the at least a portion of the hydrotreated effluent comprises at least about 100 wppm of sulfur in the form of organic sulfur compounds.

7. The method of claim 1, wherein the dewaxing catalyst comprises about 0.1 wt % to about 5.0 wt % of one or more Group 8-10 noble metals.

8. The method of claim 1, wherein the at least a portion of the hydrotreated effluent comprises about 50 wppm or less of sulfur in the form of organic sulfur compounds.

9. The method of claim 1, wherein the dewaxing catalyst has an external surface area of 250 m^2/g or less.

10. The method of claim 1, wherein the distillate boiling range feed comprises at least about 0.1 wt % sulfur in the form of organic sulfur compounds, or a combination thereof.

11. The method of claim 1, wherein the at least a portion of the hydrotreated effluent is quenched prior to exposing to the dewaxing catalyst.

12. The method of claim 1, wherein the at least a portion of the hydrotreated effluent is cascaded to the dewaxing catalyst.

13. The method of claim 1, wherein the, the molecular sieve has a molar ratio of silica to alumina of about 35 to about 55, the dewaxing catalyst having an alpha value of at least about 380, and the molecular sieve having a total surface area of at least about 350 m^2/g.

14. The method of claim 7, wherein the Group 8-10 noble metal comprises Pt and/or Pd.

15. The method of claim 13, wherein the dewaxing catalyst has an alpha value of at least about 400.

16. The method of claim 13, wherein the molecular sieve has a total surface area of at least about 380 m^2/g.

17. The method of claim 2, wherein the dewaxing catalyst has a ratio of molecular sieve to binder by weight of about 0.8 or less.

18. The method of claim 1, wherein the dewaxing catalyst has a ratio of molecular sieve to binder by weight of at least about 2.0.