

**CATALYST COMPONENT AND CATALYST FOR OLEFIN
POLYMERIZATION, AND APPLICATION THEREOF**

Cross-reference to Related Applications

The present application claims the priorities to the following patent applications
filed on October 19, 2018.

1. Chinese patent application CN201811224580.7 entitled “Catalyst component
and catalyst for olefin polymerization and use thereof, and olefin polymerization
method”;

2. Chinese patent application CN201811224578.X entitled “Catalyst component
and catalyst for olefin polymerization and use thereof, and olefin polymerization
method”;

3. Chinese patent application CN201811223634.8 entitled “Catalyst component
and catalyst for olefin polymerization and use thereof, and olefin polymerization
method”; and

4. Chinese patent application CN201811223600.9 entitled “Catalyst component
and catalyst for olefin polymerization and use thereof, and olefin polymerization
method”.

The entire contents of the above patent applications are incorporated herein by
reference.

Field of the Invention

The present invention belongs to the field of petrochemical engineering, and in
particular relates to a catalyst component for olefin polymerization, a catalyst

comprising the catalyst component, and use thereof.

Background of the Invention

5 In plastic processing, melt flow rate is an important indicator used to evaluate fluidity of a plastic melt, and it is also an important factor in selecting materials and grades of materials for plastic processing. Melt flow rate depends mainly on the molecular weight of a polymer, and a low-molecular weight polymer has a high melt flow rate. In order to obtain an olefin polymer with a high melt flow rate, it is usually
10 necessary to add a large amount of hydrogen during polymerization to enable the polymer to have a low molecular weight. However, an upper limit of the amount of hydrogen that can be added is limited by pressure resistance of a polymerization reactor. Partial pressure of an olefin gas that is polymerized has to be lowered in order to add more hydrogen, in which case productivity will be decreased. Besides, the
15 addition of a large amount of hydrogen can lead to low isotacticity of an obtained polypropylene, thereby resulting in unqualified products. It is therefore in an urgent need to develop a catalyst having a high hydrogen response (i.e., use of a small amount of hydrogen can result in a polymer with a high melt flow rate) and a high stereospecificity (i.e., under a polymerization condition with the presence of a large
20 amount of hydrogen, the polymer can still exhibit high isotacticity).

US4298718 and US4495338 disclose a Ziegler-Natta catalyst using a magnesium halide as a carrier. The catalyst produced by reacting the carrier with titanium tetrachloride exhibits a relatively high catalytic activity in catalyzing the
25 polymerization of propylene, but isotacticity of the obtained polypropylene is relatively low. This indicates that the catalyst has low stereospecificity. Later, by adding an electron donor compound (such as ethyl benzoate or phthalate) during the preparation of the Ziegler-Natta catalyst to form a solid titanium catalyst, and by adding another electron donor (alkoxysilane compound) during olefin polymerization,
30 researchers obtains polypropylene with relatively high isotacticity when propylene polymerization is catalyzed. This indicates that the addition of the electron donor compound improves the stereospecificity of the catalyst. Compared with a monoester internal electron donor, a diester internal electron donor is more helpful in improving the stereospecificity of the catalyst. However, this type of catalyst does not have

sufficient hydrogen response, and can hardly be used to produce products with a high melt index by a direct hydrogen regulation method. Further, according to research, phthalate compounds (plasticizers) can cause serious damage to the growth and development as well as the reproductive system of animals, and may also have similar effects on humans.

CN1580034A, CN1580035A, CN1580033A, CN1436766A, and CN1552740A each disclose use of diol ester compound as an electron donor of a Ziegler-Natta catalyst for propylene polymerization. The catalyst is characterized by a high polymerization activity and the polymerization product has a wide molecular weight distribution. But when a spherical catalyst comprising a carboxylate diol ester internal electron donor is used for propylene polymerization, the catalyst exhibits relatively low stereospecificity and results in polypropylene having low isotacticity.

Summary of the Invention

In order to overcome the above-mentioned defects in the existing technologies, the present invention provides a catalyst component for olefin polymerization, a catalyst comprising the catalyst component, and an olefin polymerization method. The catalyst component has both high hydrogen response and high stereospecificity, and does not comprise a phthalate compound (a plasticizer).

The inventor of the present invention unexpectedly found during research that when the internal electron donor comprises a monocarboxylic ester compound and a diether compound, and when a molar ratio of the monocarboxylic ester compound to the diether compound is in a specific range namely (0.0035-0.7):1, the two internal electron donors can work together perfectly to improve the hydrogen response and stereospecificity of the catalyst in a more effective way. Especially when compared with a catalyst that comprises a monocarboxylic ester compound alone as an internal electron donor or a catalyst that comprises a diether compound alone as an internal electron donor, a catalyst comprising a monocarboxylic ester compound and a diether compound with a molar ratio of the monocarboxylic ester compound to the diether compound being (0.0035-0.7):1 has a significantly improved stereospecificity. That is, the two internal electron donors realize a synergistic effect in improving the

stereospecificity of the catalyst. Meanwhile, the hydrogen response of the catalyst is still maintained at a high level.

Based on the above, the present invention, in its first aspect, provides a catalyst component for olefin polymerization. The catalyst component comprises magnesium, titanium, a halogen, and an internal electron donor. The internal electron donor comprises a monocarboxylic ester compound and a diether compound. A molar ratio of the monocarboxylic ester compound to the diether compound is (0.0035-0.7):1.

The present invention, in its second aspect, provides a catalyst for olefin polymerization. The catalyst comprises:

- (1) the catalyst component according to the first aspect of the present invention;
- (2) at least one alkyl aluminum compound; and
- (3) an optional external electron donor compound.

The present invention, in its third aspect, provides use of the catalyst according to the second aspect of the present invention in olefin polymerization.

The present invention, in its fourth aspect, provides an olefin polymerization method. The method comprises contacting one or more olefins with the catalyst according to the second aspect of the present invention under an olefin polymerization condition.

Brief Description of the Drawings

Exemplary embodiments of the present invention will be described in more detail with reference to the accompanying drawings.

Fig. 1 is an optical microscope photograph of a spherical carrier (i.e., a magnesium source) for an olefin polymerization catalyst prepared in Preparation Example 1.

Fig. 2 is an optical microscope photograph of a spherical carrier (i.e., a magnesium source) for an olefin polymerization catalyst prepared in Preparation

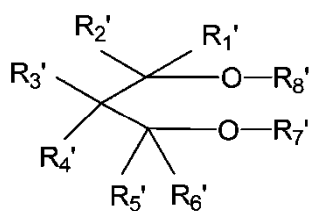
Example 4.

Detailed Description of the Embodiments

5 The present invention, in its first aspect, provides a catalyst component for olefin polymerization. The catalyst component comprises magnesium, titanium, a halogen, and an internal electron donor. The internal electron donor comprises a monocarboxylic ester compound and a diether compound. A molar ratio of the monocarboxylic ester compound to the diether compound is (0.0035-0.7):1.

10 According to some embodiments of the catalyst component of the present invention, the molar ratio of the monocarboxylic ester compound to the diether compound is (0.004-0.7):1, preferably (0.0045-0.6):1, more preferably (0.005-0.5):1, further more preferably (0.01-0.35):1. According to a most preferred embodiment, the
15 molar ratio of the monocarboxylic ester compound to the diether compound is (0.02-0.25):1. When the molar ratio of the monocarboxylic ester compound to the diether compound is within the foregoing specific range, the two internal electron donors can work perfectly together to more effectively improve hydrogen response and stereospecificity of a catalyst, and in particular significantly improve the
20 stereospecificity of the catalyst, i.e., significantly improve the isotacticity of a prepared polymer. The molar ratio of the monocarboxylic ester compound to the diether compound may exemplarily be 0.0035:1, 0.004:1, 0.0045:1, 0.005:1, 0.008:1, 0.01:1, 0.012:1, 0.015:1, 0.020:1, 0.023:1, 0.03:1, 0.04:1, 0.05:1, 0.06:1, 0.07:1, 0.08:1, 0.09:1, 0.10:1, 0.11:1, 0.12:1, 0.15:1, 0.18:1, 0.20:1, 0.23:1, 0.24:1, 0.25:1,
25 0.28:1, 0.30:1, 0.32:1, 0.34:1, 0.36:1, 0.40: 1. 0.42:1, 0.44:1, 0.46:1, 0.48:1, 0.50:1, 0.55:1, 0.60:1, 0.65:1, etc.

 According to some embodiments of the catalyst component of the present invention, the diether compound is a 1,3-diether compound, preferably a diether
30 compound as shown in Formula I.



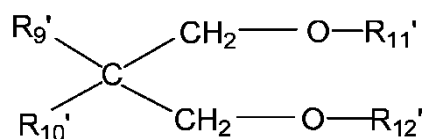
Formula I

In formula I,

R_1' , R_2' , R_3' , R_4' , R_5' and R_6' are identical to or different from each other, each independently selected from a group consisting of hydrogen, halogen, substituted or unsubstituted C_1 - C_{20} linear or branched alkyl, substituted or unsubstituted C_3 - C_{20} cycloalkyl, substituted or unsubstituted C_6 - C_{20} aryl, substituted or unsubstituted C_7 - C_{20} aralkyl, and substituted or unsubstituted C_7 - C_{20} alkaryl, preferably selected from a group consisting of hydrogen, halogen, substituted or unsubstituted C_1 - C_{18} linear or branched alkyl, substituted or unsubstituted C_3 - C_{18} cycloalkyl, substituted or unsubstituted C_6 - C_{18} aryl, substituted or unsubstituted C_7 - C_{18} aralkyl, and substituted or unsubstituted C_7 - C_{18} alkaryl; or, two or more of R_1' , R_2' , R_3' , R_4' , R_5' and R_6' are bonded to each other to form a ring.

R_7' and R_8' are identical to or different from each other, each independently selected from a group consisting of substituted or unsubstituted C_1 - C_{20} linear or branched alkyl, substituted or unsubstituted C_3 - C_{20} cycloalkyl, substituted or unsubstituted C_6 - C_{20} aryl, substituted or unsubstituted C_7 - C_{20} aralkyl, and substituted or unsubstituted C_7 - C_{20} alkaryl, preferably selected from a group consisting of substituted or unsubstituted C_1 - C_{10} linear or branched alkyl, substituted or unsubstituted C_3 - C_{10} cycloalkyl, substituted or unsubstituted C_6 - C_{15} aryl, substituted or unsubstituted C_7 - C_{15} aralkyl, and substituted or unsubstituted C_7 - C_{15} alkaryl.

According to some preferred embodiments of the catalyst component of the present invention, the diether compound is a 1,3-diether compound as shown in Formula II.



Formula II

In Formula II, R₉' and R₁₀' are identical to or different from each other, each independently selected from a group consisting of hydrogen, halogen, substituted or unsubstituted C₁-C₁₈ linear or branched alkyl, substituted or unsubstituted C₃-C₁₈ cycloalkyl, substituted or unsubstituted C₆-C₁₈ aryl, substituted or unsubstituted C₇-C₁₈ aralkyl, and substituted or unsubstituted C₇-C₁₈ alkaryl, preferably selected from a group consisting of hydrogen, halogen, substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₅ aryl, substituted or unsubstituted C₇-C₁₅ aralkyl, and substituted or unsubstituted C₇-C₁₅ alkaryl; or, R₉' and R₁₀' are bonded to each other to form a ring; preferably R₉' and R₁₀' are bonded to each other to form a fluorene ring;

R₁₁' and R₁₂' are identical to or different from each other, each independently being substituted or unsubstituted C₁-C₁₀ linear or branched alkyl.

According to the present invention, examples of the diether compound may include but be not limited to: 2-(2-ethylhexyl)-1,3-dimethoxypropane, 2-isopropyl-1,3-dimethoxypropane, 2-butyl-1,3-dimethoxypropane, 2-sec-butyl-1,3-dimethoxypropane, 2-cyclohexyl-1,3-dimethoxypropane, 2-phenyl-1,3-dimethoxypropane, 2-(2-phenylethyl)-1,3-dimethoxypropane, 2-(2-cyclohexylethyl)-1,3-dimethoxypropane, 2-(p-chlorophenyl)-1,3-dimethoxypropane, 2-(diphenylmethyl)-1,3-dimethoxypropane, 2,2-dicyclohexyl-1,3-dimethoxypropane, 2,2-dicyclopentyl-1,3-dimethoxypropane, 2,2-diethyl-1,3-dimethoxypropane, 2,2-dipropyl-1,3-dimethoxypropane, 2,2-diisopropyl-1,3-dimethoxypropane, 2,2-dibutyl-1,3-dimethoxypropane, 2-methyl-2-propyl-1,3-dimethoxypropane, 2-methyl-2-benzyl-1,3-dimethoxypropane, 2-methyl-2-ethyl-1,3-dimethoxypropane, 2-methyl-2-isopropyl-1,3-dimethoxypropane, 2-methyl-2-phenyl-1,3-dimethoxypropane, 2-methyl-2-cyclohexyl-1,3-dimethoxypropane, 2,2-bis(2-cyclohexylethyl)-1,3-dimethoxypropane, 2-methyl-2-isobutyl-1,3-dimethoxypropane, 2-methyl-2-(2-ethylhexyl)-1,3-dimethoxypropane, 2,2-diisobutyl-1,3-dimethoxypropane, 2,2-diphenyl-1,3-dimethoxypropane, 2,2-dibenzyl-1,3-dimethoxypropane,

2,2-bis(cyclohexylmethyl)-1,3-dimethoxypropane,
 2-isobutyl-2-isopropyl-1,3-dimethoxypropane,
 2-(1-methylbutyl)-2-isopropyl-1,3-dimethoxypropane,
 2-isopropyl-2-isopentyl-1,3-dimethoxypropane,
 5 2-phenyl-2-isopropyl-1,3-dimethoxypropane,
 2-phenyl-2-sec-butyl-1,3-dimethoxypropane,
 2-benzyl-2-isopropyl-1,3-dimethoxypropane,
 2-cyclopentyl-2-isopropyl-1,3-dimethoxypropane, 2-cyclopentyl-2-sec-butyl
 1,3-dimethoxypropane, 2-cyclohexyl-2-isopropyl-1,3-dimethoxypropane,
 10 2-cyclohexyl-2-sec-butyl-1,3-dimethoxypropane,
 2-isopropyl-2-sec-butyl-1,3-dimethoxypropane,
 2-cyclohexyl-2-cyclohexylmethyl-1,3-dimethoxypropane, and
 9,9-dimethoxymethylfluorene.

15 Most preferably, the diether compound is
 2-isopropyl-2-isopentyl-1,3-dimethoxypropane and/or 9,9-dimethoxymethylfluorene.

In the present invention, the 1,3-diether compound may be synthesized by a
 method which can be found in the disclosure of CN1020448C, CN100348624C and
 20 CN1141285A. Contents disclosed by all these patent applications are incorporated
 herein by reference, and will not be repeated herein.

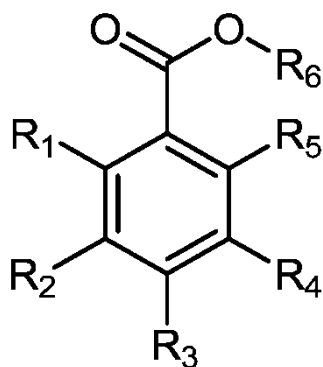
According to some embodiments of the catalyst component of the present
 invention, the monocarboxylic ester compound is selected from an aromatic
 25 monocarboxylic ester and an aliphatic monocarboxylic ester. Preferably, the aliphatic
 monocarboxylic ester is a monoester formed by an aliphatic monocarboxylic acid
 having 2-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15
 carbon atoms or an aromatic alcohol having 6-15 carbon atoms. Preferably, the
 aromatic monocarboxylic ester is a monoester formed by an aromatic monocarboxylic
 30 acid having 7-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having
 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms.

According to some embodiments of the catalyst component of the present
 invention, the aliphatic monocarboxylic ester is a monoester formed by an aliphatic

monocarboxylic acid having 2-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms.

According to some embodiments of the catalyst component of the present invention, the aromatic monocarboxylic ester is a monoester formed by an aromatic monocarboxylic acid having 7-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms.

According to some embodiments of the catalyst component of the present invention, the aromatic monocarboxylic ester is an aromatic monocarboxylic ester as shown in Formula III.



Formula III

In Formula III, R₁- R₅ are identical to or different from each other, each independently selected from a group consisting of hydrogen, hydroxyl, halogen, amino, substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₁-C₁₀ alkoxy, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl; or any two of R₁-R₅ form an aromatic ring or an aliphatic ring; R₆ is selected from a group consisting of substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl, preferably selected from substituted or unsubstituted C₁-C₆ linear or branched alkyl.

The aromatic monocarboxylic ester may specifically be at least one selected from a group consisting of benzoate, o-hydroxybenzoate, o-methoxybenzoate, and

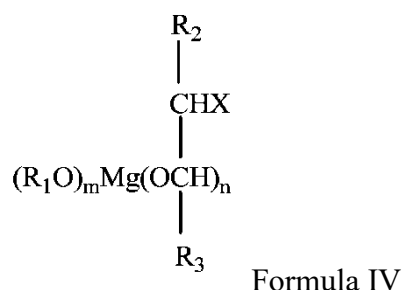
o-ethoxybenzoate.

According to the present invention, the internal electron donor comprises a diether compound and a monocarboxylic ester compound. The diether compound and the monocarboxylic ester compound may produce a certain synergistic effect. Based on an amount of the internal electron donor, a total amount of the monocarboxylic ester compound and the diether compound is preferably 70-100% by weight, more preferably 80-100% by weight, further more preferably 90-100% by weight, most preferably 100% by weight.

According to some embodiments of the catalyst component of the present invention, the catalyst component is a product resulted from a reaction of a magnesium source, a titanium source, and the internal electron donor.

According to some embodiments of the catalyst component of the present invention, the magnesium source comprises one or more magnesium compounds selected from a group consisting of magnesium dihalide, magnesium alkoxide, magnesium alkyl, a hydrate or alcoholate of magnesium dihalide, and a derivative derived by substituting a halogen atom in a formula of magnesium dihalide with alkoxy or halogenated alkoxy.

According to some embodiments of the catalyst component of the present invention, the magnesium source comprises a magnesium compound as shown in Formula IV.



In Formula IV,

R₁ is selected from a group consisting of substituted or unsubstituted C₁-C₁₀ linear alkyl, substituted or unsubstituted C₃-C₁₀ branched alkyl, substituted or

unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl; preferably, R₁ is selected from a group consisting of substituted or unsubstituted C₁-C₈ linear alkyl, substituted or unsubstituted C₃-C₈ branched alkyl, substituted or unsubstituted C₃-C₈ cycloalkyl, substituted or unsubstituted C₆-C₁₅ aryl, substituted or unsubstituted C₇-C₁₅ aralkyl, and substituted or unsubstituted C₇-C₁₅ alkaryl; more preferably, R₁ is selected from a group consisting of substituted or unsubstituted C₁-C₆ linear alkyl, substituted or unsubstituted C₃-C₆ branched alkyl, substituted or unsubstituted C₃-C₆ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl.

R₂ and R₃ are identical to or different from each other, each independently selected from a group consisting of hydrogen, substituted or unsubstituted C₁-C₁₀ linear alkyl, substituted or unsubstituted C₃-C₁₀ branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl; preferably, R₂ and R₃ are each independently selected from a group consisting of hydrogen, substituted or unsubstituted C₁-C₁₀ linear alkyl, substituted or unsubstituted C₃-C₈ branched alkyl, substituted or unsubstituted C₃-C₈ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl; more preferably, R₂ and R₃ are each independently selected from a group consisting of hydrogen, substituted or unsubstituted C₁-C₆ linear alkyl, substituted or unsubstituted C₃-C₆ branched alkyl, substituted or unsubstituted C₃-C₆ cycloalkyl, substituted or unsubstituted C₆-C₈ aryl, substituted or unsubstituted C₇-C₉ aralkyl, and substituted or unsubstituted C₇-C₉ alkaryl.

X is a halogen, preferably chlorine or bromine.

m is 0.1-1.9; n is 0.1-1.9; and m+n=2.

According to some embodiments of the catalyst component of the present invention, the titanium source comprises titanium halide, titanium alkoxide halide, and titanium alkoxide. More preferably, the titanium source comprises a compound represented by a general formula Ti(OR')_{3-a}Z_a and/or Ti(OR')_{4-b}Z_b, where R' is C₁-C₂₀

alkyl; Z is F, Cl, Br or I; a is an integer from 1 to 3; and b is an integer from 1 to 4.

According to some embodiments of the catalyst component of the present invention, the magnesium source further comprises sulfur. A molar ratio of sulfur to magnesium in the magnesium source is $q:1$, where $0 < q \leq 0.5$, preferably $0.001 < q \leq 0.2$. The inventor of the present invention unexpectedly found in research that sulfur added during preparation of a carrier (a magnesium source) for an olefin polymerization catalyst can reduce collision probability among unshaped particles and reduce adhesion among carrier particles, so that resulting carrier particles have a small particle size, a narrow particle size distribution, and good morphology. The carrier particles prepared in this way are good in morphology and smooth at surface, and among them there are basically no nonspherical particles. Besides, the particle size of the carrier particles can be less than 20 microns, and the particle size distribution is narrow.

According to some embodiments of the catalyst component of the present invention, the magnesium source is prepared by a method including the following steps:

(1) A mixture is prepared. The mixture comprises elemental sulfur, a magnesium halide represented by a general formula MgX_1Y , a compound represented by a general formula R_1OH , an optional inert liquid medium, and an optional surfactant. Preferably, the mixture is obtained by mixing the elemental sulfur, the magnesium halide represented by the general formula MgX_1Y , the compound represented by the general formula R_1OH , the optional inert liquid medium, and the optional surfactant together at one time or step by step and then heating a resulting mixture.

(2) The mixture obtained in step (1) is subjected to a contact reaction with an ethylene oxide compound.

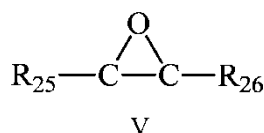
In the general formula MgX_1Y , X_1 is halogen, preferably chlorine or bromine; Y is selected from a group consisting of halogen, substituted or unsubstituted C_1 - C_{10} linear alkyl, substituted or unsubstituted C_3 - C_{10} branched alkyl, substituted or

unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₁-C₁₀ alkoxy, substituted or unsubstituted C₆-C₂₀ aryloxy, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl.

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In the general formula R₁OH, R₁ is selected from a group consisting of substituted or unsubstituted C₁-C₁₀ linear alkyl, substituted or unsubstituted C₃-C₁₀ branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl; preferably, R₁ is selected from a group consisting of substituted or unsubstituted C₁-C₈ linear alkyl, substituted or unsubstituted C₃-C₈ branched alkyl, substituted or unsubstituted C₃-C₈ cycloalkyl, substituted or unsubstituted C₆-C₁₅ aryl, substituted or unsubstituted C₇-C₁₅ aralkyl, and substituted or unsubstituted C₇-C₁₅ alkaryl; more preferably, R₁ is selected from a group consisting of substituted or unsubstituted C₁-C₆ linear alkyl, substituted or unsubstituted C₃-C₆ branched alkyl, substituted or unsubstituted C₃-C₆ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl.

20 The ethylene oxide compound has a structure shown in Formula V.



In Formula V, R₂₅ and R₂₆ are each independently selected from a group consisting of hydrogen, substituted or unsubstituted C₁-C₁₀ linear alkyl, substituted or unsubstituted C₃-C₁₀ branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl; preferably, R₂₅ and R₂₆ are each independently selected from a group consisting of hydrogen, substituted or unsubstituted C₁-C₈ linear alkyl, substituted or unsubstituted C₃-C₈ branched alkyl, substituted or unsubstituted C₃-C₈ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl; more preferably, R₂₅ and R₂₆ are each independently selected from a group consisting of hydrogen, substituted or unsubstituted C₁-C₆ linear alkyl, substituted or

unsubstituted C₃-C₆ branched alkyl, substituted or unsubstituted C₃-C₆ cycloalkyl, substituted or unsubstituted C₆-C₈ aryl, substituted or unsubstituted C₇-C₉ aralkyl, and substituted or unsubstituted C₇-C₉ alkylaryl.

5 According to some embodiments of the catalyst component of the present invention, in the general formula MgX_1Y , X_1 is chlorine or bromine, and Y is chlorine, bromine, C₁-C₅ alkoxy or C₆-C₁₀ aryloxy. Preferably, the magnesium halide represented by the general formula MgX_1Y is at least one selected from a group consisting of magnesium chloride, magnesium bromide, phenoxymagnesium chloride,
10 isopropoxymagnesium chloride, and n-butoxymagnesium chloride.

 According to some embodiments of the catalyst component of the present invention, in the general formula R_1OH , R_1 is C₁-C₈ alkyl. Preferably, the compound represented by the general formula R_1OH is at least one selected from a group
15 consisting of ethanol, n-propanol, isopropanol, n-butanol, isobutanol, n-pentanol, isopentanol, n-hexanol, 2-ethylhexanol, and n-octanol.

 According to some embodiments of the catalyst component of the present invention, in the ethylene oxide compound having the structure represented by
20 Formula V, R_{25} and R_{26} are each independently hydrogen, C₁-C₃ alkyl, or C₁-C₃ halogenated alkyl. Preferably, the ethylene oxide compound is at least one selected from a group consisting of ethylene oxide, epoxyp propane, epoxybutane, epoxychloropropane, epoxychlorobutane, epoxybromopropane, and epoxybromobutane.

25 According to the present invention, contents of the above-mentioned components in the magnesium source of the catalyst for olefin polymerization may be selected and varied within a relatively wide range. Preferably, based on 1 mol of the magnesium halide represented by the general formula MgX_1Y , the elemental sulfur is present in
30 an amount of 0.0001-0.5 mol, the compound represented by the general formula R_1OH is present in an amount of 4-30 mol, and the ethylene oxide compound is present in an amount of 1-10 mol. More preferably, based on 1 mol of the magnesium halide represented by the general formula MgX_1Y , the compound represented by the general formula R_1OH is present in an amount of 6-20 mol, and the ethylene oxide

compound is present in an amount of 2-6 mol.

According to the present invention, in step (1), conditions for heating the mixture of the elemental sulfur, the magnesium halide represented by the general formula MgX_1Y , the compound represented by the general formula R_1OH , and the optional inert liquid medium and/or the surfactant are not limited, so long as the conditions for the heating are such that the magnesium halide represented by the general formula MgX_1Y melts and sufficiently reacts with sulfur. According to some embodiments of the catalyst component of the present invention, in step (1), the heating is conducted at a temperature of 80-120°C for a time period of 0.5-5 hours, preferably at a temperature of 80-100°C for 0.5-3 hours.

According to the present invention, in step (2), conditions for the contact reaction of the mixture with the ethylene oxide compound may be any existing conditions that can be used to form a carrier for an olefin polymerization catalyst. According to some embodiments of the catalyst component of the present invention, in step (2), the conditions for the contact reaction include reacting at temperature of 40-120°C for a time period of 15-60 minutes, preferably reacting at a temperature of 60-100°C for a time period of 20-50 minutes.

According to the present invention, the method may further include subjecting the product obtained from the contact reaction to solid-liquid separation, and washing and drying a solid phase product obtained from the separation. The solid-liquid separation may be realized by any existing method capable of separating a solid phase from a liquid phase, such as suction filtration, filter pressing, or centrifugal separation. Preferably, the method of the solid-liquid separation is filter pressing. Conditions for the filter pressing are not particularly limited in the present invention so long as a solid phase and a liquid phase can be separated as fully as possible. The washing may be realized by a method well known to those skilled in the art which can be used to wash the obtained solid phase product. For example, an inert hydrocarbon solvent (such as pentane, hexane, heptane, petroleum ether, and gasoline) may be used to wash the obtained solid phase product. Conditions for the drying are not particularly limited in the present invention. For example, the drying may be conducted at a temperature of 20-70°C for a period of time of 0.5-10 hours. According to the present

invention, the drying may be conducted at a normal pressure or a reduced pressure.

Preferably, solid component particles obtained in the above process of preparing the solid component are washed with an inert hydrocarbon solvent (such as hexane, 5 heptane, octane, decane, toluene, etc.) and dried, and then used in a subsequent step (2) to prepare the catalyst component for olefin polymerization.

In the present invention, the elemental sulfur may be any subtype of elemental sulfur, including but not limited to at least one of α -sulfur, β -sulfur, γ -sulfur, and 10 polymeric sulfur. The elemental sulfur may be anhydrous elemental sulfur or elemental sulfur containing bound water. The elemental sulfur may be commercially available.

According to the present invention, the inert liquid medium may be any liquid 15 medium commonly used in the art that does not chemically react with reactants and products of the reaction. According to some embodiments of the catalyst component of the present invention, the inert liquid medium is a silicone oil solvent and/or a hydrocarbon solvent. Preferably, the inert liquid medium is at least one selected from a group consisting of kerosene, paraffin oil, petrolatum oil, white oil, methyl silicone 20 oil, ethyl silicone oil, methyl ethyl silicone oil, phenyl silicone oil, and methyl phenyl silicone.

According to some embodiments of the catalyst component of the present invention, based on 1 mol of the magnesium halide represented by the general 25 formula MgX_1Y , the inert liquid medium is present in an amount of 0.8-10 L.

According to some embodiments of the catalyst component of the present invention, the surfactant is at least one selected from a group consisting of polyvinylpyrrolidone, polyethylene glycol, polyvinyl alcohol, polyacrylic acid, 30 polyacrylate, polyacrylamide, polystyrene sulfonate, naphthalenesulfonic acid formaldehyde condensate, condensed alkyl phenyl ether sulfate, condensed alkyl phenol polyoxyethylene ether phosphate, oxyalkyl acrylate copolymer modified polyethyleneimine, 1-dodeca-4-vinylpyridine bromide polymer, polyvinylbenzyltrimethylamine salt, polyethylene oxide propylene oxide block

copolymer, polyvinylpyrrolidone vinyl acetate copolymer, alkyl phenyl polyoxyethylene ether, and polyalkyl methacrylate.

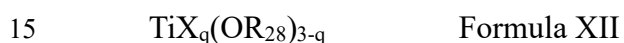
According to some embodiments of the catalyst component of the present invention, based on 1 mol of the magnesium halide represented by the general formula MgX_1Y , the surfactant is present in an amount of 1-20 g.

An average particle size of the spherical carrier for the olefin polymerization catalyst of the present invention may be controlled within a wide range, for example, within a range of 10-100 microns. According to a preferred embodiment of the present invention, an average particle diameter (D50) of the spherical carrier for the olefin polymerization catalyst of the present invention may be controlled to be less than or equal to 30 microns, preferably less than or equal to 20 microns, and a particle size distribution ((D90-D10)/D50) thereof may be controlled to be less than 1.2, preferably less than or equal to 0.8. In this preferred embodiment, the catalyst prepared from the spherical carrier for the olefin polymerization catalyst can be used to obtain an olefin polymer having a higher bulk density. In the present invention, the average particle diameter and a particle size distribution of the spherical carrier for the olefin polymerization catalyst may be measured with a particle size analyzer namely Master Sizer 2000 laser (manufactured by Malvern Instruments Ltd).

When the solid component (the carrier for the olefin polymerization catalyst) is spherical particles, the catalyst component obtained by reacting the carrier with the titanium compound, the monocarboxylic ester compound, and the diether compound is also spherical particles. Moreover, due to the smaller particle size and the narrow particle size distribution of the spherical carrier, the prepared catalyst component also has a relatively small particle size and a relatively narrow particle size distribution.

According to the present invention, the spherical carrier for the olefin polymerization catalyst may contain water coming from a trace water carried by a raw material used in the synthesis and a reaction media. According to the present invention, the trace water in the above-mentioned reactants may also participate in the reaction to form the spherical carrier for the olefin polymerization catalyst.

In the present invention, in the catalyst component for olefin polymerization, contents of magnesium, titanium, the halogen, and the internal electron donor are not particularly limited, and can be reasonably selected according to conventional used amounts in the art. Preferably, in the catalyst component, a weight ratio of titanium as
5 titanium element, to magnesium as magnesium element, to the halogen, and to the internal electron donor is 1:(2-15):(8-30):(2-15), preferably 1:(3-12):(10-25):(3-13). More preferably, a weight ratio of titanium as titanium element, to magnesium as magnesium element, and to the internal electron donor is 1:(4-10):(4-10). In the present invention, the titanium compound may be a titanium compound commonly
10 used in the art. Preferably, the titanium compound is a compound represented by Formula XI and/or Formula XII.



In Formula XI and Formula XII, X is a halogen; R_{27} and R_{28} are each independently $\text{C}_1\text{-C}_{20}$ alkyl; p is an integer from 1 to 4; and q is an integer from 1 to 3.

20 Further preferably, the titanium compound is one or more selected from a group consisting of titanium tetrachloride, titanium tetrabromide, titanium tetraiodide, tributoxy titanium chloride, dibutoxy titanium dichloride, butoxy titanium trichloride, triethoxy titanium chloride, diethoxy titanium dichloride, ethoxy titanium trichloride, and titanium trichloride. Most preferably, the titanium compound is titanium
25 tetrachloride.

A method for preparing the catalyst component for olefin polymerization of the present invention may include the following steps. A magnesium compound and a titanium compound are subjected to a reaction. In one or more time periods before,
30 during, and after the reaction of the magnesium compound with the titanium compound, an internal electron donor is added. The internal electron donor comprises the above-mentioned monocarboxylic ester compound and the above-mentioned diether compound. In the present invention, the reaction of the magnesium compound and the titanium compound may be carried out by a method disclosed in the prior arts.

For example, the titanium compound may be cooled to a temperature below 0°C (preferably to a temperature ranging from -5°C to -25°C), followed by adding the magnesium compound. A resulting mixture is stirred and mixed at this temperature for 10-60 minutes, and then heated to a reaction temperature (preferably 60-130°C) and maintained at this reaction temperature for 0.5-10 hours. During the heating, the monocarboxylic ester compound and the diether compound are added. Then, the titanium compound is added, and a resulting mixture is treated one or more times. Finally, the treated mixture is washed with an inert solvent multiple times to obtain the catalyst component. Examples of the inert solvent may include but are not limited to hexane, heptane, octane, decane, and toluene.

In the method for preparing the catalyst component for olefin polymerization, the internal electron donor component is added in one or more time periods before, during, and after the reaction of the magnesium compound with the titanium compound. A time period before the reaction of the magnesium compound with the titanium compound refers to a time period after the magnesium compound is added to a reactor but before the temperature is raised to the reaction temperature.

In one embodiment, in order that the prepared catalyst component can be used in olefin polymerization to obtain an olefin polymer having higher isotacticity, step (2) includes adding an internal electron donor at least comprising a monocarboxylic ester compound and a diether compound in one or more time periods before, during, and after the reaction of the solid component with the titanium compound. The internal electron donor at least comprising the monocarboxylic ester compound and the diether compound may be added at one time, or may be added separately in different time periods. Preferably, the internal electron donor at least comprising the monocarboxylic ester compound and the diether compound is added during heating the mixture of the solid component and the titanium compound.

Preferably, after the reaction of the solid component with the titanium compound, the method for preparing the catalyst component further includes: filtering off a liquid and recovering a solid, and then treating the recovered solid with a liquid titanium compound (such as titanium tetrachloride) one or more times, preferably two to four times; and then washing the obtained solid catalyst component multiple times with a

hydrocarbon solvent. The hydrocarbon solvent may be selected from aliphatic hydrocarbons, aromatic hydrocarbons or alicyclic hydrocarbons, such as hexane, heptane, octane, decane, toluene, etc.

5 According to the present invention, in preparing the catalyst component, a molar ratio of the magnesium compound, to the titanium compound, and to the internal electron donor component is not particularly limited, and a content of each of these components may be varied in a wide range. Preferably, the molar ratio of the magnesium compound as magnesium element, to the titanium compound as titanium
10 element, and to the internal electron donor is 1:(5-200):(0.04-0.6). More preferably, the molar ratio of the magnesium compound as magnesium element, to the titanium compound as titanium element, and to the internal electron donor is 1:(10-160):(0.07-0.5). Most preferably, the molar ratio of the magnesium compound as magnesium element, to the titanium compound as titanium element, and to the
15 internal electron donor is 1:(15-120):(0.1-0.4).

In the present invention, examples of C₁-C₂₀ linear or branched alkyl may include but are not limited to: methyl, ethyl, n-propyl, isopropyl, n-butyl, sec-butyl, isobutyl, tert-butyl, n-pentyl, 1-ethylpropyl, 2-methylbutyl, 3-methylbutyl,
20 2,2-dimethylpropyl, n-hexyl, 2-methylpentyl, 3-methylpentyl, 4-methylpentyl, n-heptyl, 2-methylhexyl, 3-methylhexyl, 4-methylhexyl, 5-methylhexyl, n-heptyl, n-octyl, n-nonyl, n-decyl, tetrahydrogeranyl, n-dodecyl, n-tridecyl, n-tetradecyl, n-pentadecyl, n-hexadecyl, n-octadecyl, n-nonadecyl, and n-eicosyl.

25 In the present invention, examples of C₂-C₂₀ linear or branched alkenyl may include but are not limited to: vinyl, allyl, isopropenyl, 1-propenyl, 2-methyl-1-propenyl, 1-butenyl, 2-butenyl, 3-butenyl, 2-ethyl-1-butenyl, 3-methyl-2-butenyl, 1-pentenyl, 2-pentenyl, 3-pentenyl, 4-pentenyl, 4-methyl-3-pentenyl, 1-hexenyl, 2-hexenyl, 3-hexenyl, 4-hexenyl, 5-hexenyl,
30 1-heptenyl, 1-octenyl, phenylvinyl, phenyl-n-butenyl, geranyl, 1-decenyl, 1-tetradecenyl, 1-octadecenyl, 9-octadecenyl, 1-eicosenyl, and 3,7,11,15-tetramethyl-1-hexadecenyl.

In the present invention, examples of C₃-C₂₀ cycloalkyl may include but are not

limited to: cyclopropyl, cyclobutyl, cyclopentyl, cyclohexyl, 4-methylcyclohexyl, 4-ethylcyclohexyl, 4-n-propylcyclohexyl, 4-n-butylcyclohexyl, cycloundecyl, and cyclododecyl.

5 In the present invention, C₆-C₂₀ aryl includes C₆-C₂₀ phenyl and C₁₀-C₂₀ fused aryl, and its examples may include but are not limited to: phenyl, naphthyl, methylnaphthyl, ethylnaphthyl, anthryl, methylantrhy, ethylantrhy, phenanthryl, methylphenanthryl, ethylphenanthryl, pyrenyl, indenyl, o-tolyl, m-tolyl, p-tolyl, o-ethylphenyl, m-ethylphenyl, p-ethylphenyl, and naphthyl.

10

In the present invention, C₇-C₂₀ aralkyl refers to an alkyl group having an aryl substituent with 7-20 carbon atoms. Examples of C₇-C₂₀ aralkyl may include but are not limited to: phenylmethyl, phenylethyl, phenyl n-propyl, phenyl n-butyl, phenyl t-butyl, phenylisopropyl, and phenyl n-pentyl.

15

In the present invention, C₇-C₂₀ alkaryl refers to an aryl group having an alkyl substituent with 7-20 carbon atoms. Examples of substituted or unsubstituted C₇-C₂₀ alkaryl may include but are not limited to: methylphenyl, ethylphenyl, n-propylphenyl, n-butylphenyl, tert-butylphenyl, isopropylphenyl, and n-pentylphenyl.

20

In the present invention, examples of C₁-C₆ alkoxy may include but are not limited to: methoxy, ethoxy, n-propoxy, isopropoxy, n-butoxy, sec-butoxy, isobutoxy, tert-butoxy, n-pentoxy, isopentoxy, tert-pentoxy, and hexyloxy.

25 In the present invention, C₆-C₁₀ aryloxy may be, for example, phenoxy or naphthoxy.

30 In the present invention, the term “substituted” means that one or more hydrogen atoms on a carbon atom of a described group can be substituted by a common substituent, which can be alkyl, alkoxy, halogen, amino, hydroxyl, etc., such as C₁-C₆ alkyl, C₁-C₆ alkoxy, halogen, amino, hydroxyl, etc.

In the present invention, the elemental sulfur may be any subtype of elemental sulfur, including but not limited to at least one of α -sulfur, β -sulfur, γ -sulfur, and

polymeric sulfur. The elemental sulfur may be anhydrous elemental sulfur or elemental sulfur containing bound water. The elemental sulfur may be commercially available.

5 In the present invention, halogen is selected from fluorine, chlorine, bromine, and iodine.

In the present invention, C₆-C₁₀ aryloxy may be, for example, phenoxy or naphthoxy.

10

In the present invention, C₃-C₈ cycloalkyl may be, for example, cyclopentyl, cyclopentylmethyl, cyclopentylethyl, cyclohexyl, or cyclohexylmethyl.

The present invention, in its second aspect, provides a catalyst for olefin
15 polymerization. The catalyst comprises:

- (1) the catalyst component according to the first aspect of the present invention;
- (2) at least one alkyl aluminum compound; and
- (3) and an optional external electron donor compound.

20 According to the present invention, in the above-mentioned catalyst for olefin polymerization, the alkyl aluminum compound may be any alkyl aluminum compound commonly used in the field of olefin polymerization that can be used as a co-catalyst for a catalyst for olefin polymerization. Preferably, the alkyl aluminum compound is a compound represented by Formula XIII

25

$AlR'_nX'_{3-n'}$ Formula XIII

In Formula XIII, R' is C₁-C₈ alkyl or halogenated alkyl; X' is a halogen, preferably one or more selected from chlorine, bromine, and iodine, more preferably
30 chlorine; and n' is an integer from 1 to 3.

More preferably, the alkyl aluminum compound is one or more selected from a group consisting of triethyl aluminum, tripropyl aluminum, tri-n-butyl aluminum, tri-isobutyl aluminum, tri-n-hexyl aluminum, tri-n-octyl aluminum, tri-isobutyl

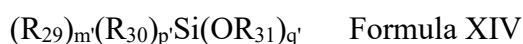
aluminum, monohydrogen diethyl aluminum, monohydrogen diisobutyl aluminum, diethyl aluminum chloride, diisobutyl aluminum chloride, ethyl aluminum dichloride, $\text{Al}(\text{n-C}_6\text{H}_{13})_3$, and $\text{Al}(\text{n-C}_8\text{H}_{17})_3$.

5 Most preferably, the alkyl aluminum compound is triethyl aluminum and/or triisobutyl aluminum.

According to the present invention, an amount of the alkyl aluminum compound may be a conventional amount in the art. Preferably, a molar ratio of aluminum in the
10 alkyl aluminum compound to titanium in the catalyst component is 1-2000:1. More preferably, the molar ratio of aluminum in the alkyl aluminum compound to titanium in the catalyst component is 10-500:1.

In the present invention, a type and a content of the external electron donor in the
15 catalyst for olefin polymerization are not particularly limited. Preferably, a molar ratio of aluminum in the alkyl aluminum compound to the external electron donor compound is 1-200:1, more preferably 2.5-100:1.

According to the present invention, the use of the external electron donor
20 compound in combination with the monocarboxylic ester compound and the diether compound can further increase the isotactic index of an olefin polymer obtained by the method of the present invention. The external electron donor compound may be any external electron donor compound commonly used in the art that can achieve the above purpose, and may be, for example, one or more selected from carboxylic acid,
25 carboxylic acid anhydride, carboxylic acid ester, ketone, ether, alcohol, lactone, organophosphorus compounds and organosilicon compounds. Preferably, the external electron donor compound is an organosilicon compound represented by Formula XIV.



30

In Formula XIV, R_{29} , R_{30} , and R_{31} are each independently $\text{C}_1\text{-C}_{18}$ hydrocarbon, and each optionally containing heteroatoms, the heteroatoms being one or more selected from F, Cl, Br, N and I; m' and p' are each independently an integer from 0 to 2; q' is an integer from 1 to 3; and a sum of m' , p' , and q' is 4.

Preferably, R₂₉ and R₃₀ are each independently selected from a group consisting of C₃-C₁₀ linear or branched alkyl, C₃-C₁₀ linear or branched alkenyl, substituted or unsubstituted C₃-C₁₀ alkylene, substituted or unsubstituted C₃-C₁₀ cycloalkyl, and substituted or unsubstituted C₆-C₁₀ aryl, and each optionally containing heteroatoms, the heteroatoms being one or more of F, Cl, Br, N, and I; and R₃₁ is C₁-C₁₀ linear or branched alkyl, more preferably methyl.

According to the present invention, specific examples of the external electron donor compound may include but are not limited to one or more selected from a group consisting of cyclohexylmethyldimethoxysilane, diisopropyldimethoxysilane, di-n-butyldimethoxysilane, diisobutyldimethoxysilane, diphenyldimethoxysilane, methyltert-butyldimethoxysilane, cyclohexyltrimethoxysilane, tert-butyldimethoxysilane, tert-hexyltrimethoxysilane, dicyclopentyldimethoxysilane, 2-ethylpiperidyl-2-tert-butyldimethoxysilane, (1,1,1-trifluoro-2-propyl)-2-ethylpiperidyldimethoxysilane, and (1,1,1-trifluoro-2-propyl)-methyldimethoxysilane. These external electron donors may be used alone or in combinations.

More preferably, the external electron donor compound is cyclohexylmethyldimethoxysilane and/or dicyclopentyldimethoxysilane.

According to the present invention, during the preparation of the catalyst for olefin polymerization, the alkyl aluminum and the optional external electron donor compound may be mixed and reacted respectively with the catalyst component for olefin polymerization, or the alkyl aluminum and the optional external electron donor compound may be mixed first and then mixed and reacted with the catalyst component for olefin polymerization.

According to the present invention, when the catalyst for olefin polymerization is used in polymerization of an olefin, the catalyst component for olefin polymerization, the alkyl aluminum, and the optional external electron donor may be separately added to a polymerization reactor, or may be mixed first and then added to the polymerization reactor, or may be added to the polymerization reactor after the olefin

is pre-polymerized according to a pre-polymerization method known in the art.

The present invention, in its third aspect, provides use of the above-mentioned catalyst in olefin polymerization.

5

The present invention, in its fourth aspect, provides an olefin polymerization method, comprising: contacting one or more olefins with the above-mentioned catalyst under olefin polymerization conditions. An improvement that is made in the present invention is the use of a new catalyst component and a new catalyst for olefin polymerization, and therefore specific types of the olefin(s) and methods and conditions of the polymerization reaction can all be the same as used in the existing technologies. The olefin is at least one olefin represented by a formula $\text{CH}_2=\text{CHR}$, where R is hydrogen or $\text{C}_1\text{-C}_6$ linear or branched alkyl. Specific examples of the olefin represented by the formula $\text{CH}_2=\text{CHR}$ may include: ethylene, propylene, 1-n-butene, 1-n-pentene, 1-n-hexene, 1-n-octene, 4-methyl-1-pentene. Preferably, the olefin represented by the formula $\text{CH}_2=\text{CHR}$ is ethylene, propylene, 1-n-butene, 1-n-hexene, and 4-methyl-1-pentene. More preferably, the olefin represented by the formula $\text{CH}_2=\text{CHR}$ is propylene.

20 The olefin polymerization method of the present invention may be homopolymerization of a single olefin or copolymerization of a plurality of olefins.

According to the present invention, the polymerization reaction of the olefin can be carried out according to an existing method. Specifically, the polymerization reaction is carried out under the protection of an inert gas, in a liquid phase monomer or an inert solvent comprising a polymerized monomer, or in a gas phase, or in a combined polymerization process in a gas-liquid phase. The polymerization reaction may be carried out usually at a temperature of $0\text{-}150^\circ\text{C}$, preferably at a temperature of $60\text{-}90^\circ\text{C}$. The polymerization reaction may be carried out at a normal pressure or a higher pressure, which may be, for example, $0.01\text{-}10\text{ MPa}$, preferably $0.01\text{-}6\text{ MPa}$, more preferably $0.1\text{-}4\text{ MPa}$. The pressure in the present invention refers to a gauge pressure. During the polymerization, hydrogen may be added to the reaction system as a polymer molecular weight regulator to adjust the molecular weight and the melt index of the polymer. In addition, during the polymerization reaction of the olefin,

types and amounts of the inert gas and the solvent are well known to those skilled in the art, and will not be repeated herein.

5 The catalyst component for olefin polymerization of the present invention, by using the diether compound and the monocarboxylic ester compound as the internal electron donor, can effectively improve the hydrogen response and stereospecificity of the catalyst.

10 Other features and advantages of the present invention will be described in detail in the following specific embodiments.

The present invention is further illustrated by way of the following embodiments.

15 The specific embodiments of the present invention will be described in detail below. It should be appreciated that the specific embodiments described herein are only used to illustrate and explain, rather than limiting, the present invention.

In the following examples and comparative examples:

20 1. Average particle diameters and particle size distributions of a catalyst component and a carrier thereof for olefin polymerization were measured by a particle size analyzer namely Masters Sizer 2000 (manufactured by Malvern Instruments Ltd).

25 2. Apparent morphology of a carrier for an olefin polymerization catalyst was observed with an optical microscope namely Eclipse E200 purchased from Nikon.

3. Polymer melt index was measured according to the method provided in ASTM D1238-99.

30 4. Isotactic index of a polymer was measured by a heptane extraction method (extraction with boiling heptane for 6 hours). Specifically, 2 g of a dried polymer sample was placed in an extractor and extracted with boiling heptane for 6 hours. Resulting residual was dried to a constant weight to obtain a polymer. The isotactic index was a ratio of a weight (g) of the polymer to 2 (g).

Preparation Example 1

8.0 g (0.08 mol) of magnesium chloride, 56 mL (0.96 mol) of ethanol, 1g (0.03
5 mol) of α -sulfur, and 1 g of PVP (polyvinylpyrrolidone) as a surfactant were added to
a 0.6-L reactor, heated under stirring to 90°C and reacted at 90°C for 2 hours,
followed by adding 38 mL (0.48 mol) of epoxychloropropane, and then again reacted
at 90°C for 0.5 hour. After that, a resulting mixture was subjected to filter pressing. A
product resulted from the filter pressing was washed with hexane five times. Finally, a
10 resulting product was vacuum dried to obtain a spherical carrier Z1 of an olefin
polymerization catalyst.

The spherical carrier Z1 of the olefin polymerization catalyst had an average
particle diameter (D50) of 15 microns, and a particle size distribution
15 ((D90-D10)/D50) of 0.6. As shown in Fig. 1, as it is observed through an optical
microscope, particles of the spherical carrier Z1 of the olefin polymerization catalyst
have relatively regular morphology and smooth surfaces, are basically all spherical,
and have a relatively narrow particle size distribution, and among them are basically
no non-spherical particles.

20

According to gas chromatography-mass spectrometry, elemental analysis, and
nuclear magnetic characterization, components of Z1 include a magnesium-containing

compound represented by a structural formula
$$\begin{array}{c} \text{CH}_2\text{Cl} \\ | \\ (\text{C}_2\text{H}_5\text{O})\text{Mg}(\text{OCH}) \\ | \\ \text{CH}_2\text{Cl} \end{array}$$
 and sulfur. A
molar ratio of magnesium in the magnesium-containing compound to sulfur is 1:0.2.

25

Preparation Example 2

300 mL of white oil, 8.0 g (0.08 mol) of magnesium chloride, 28 mL (0.48 mol)
of ethanol, 0.3 g (0.009 mol) of β -sulfur, and 1 g of PVP (polyvinylpyrrolidone) as a
30 surfactant were added to a 0.6-L reactor, heated under stirring to 100°C and reacted at
100°C for 1 hour, followed by adding 12.5 mL (0.16 mol) of epoxychloropropane, and
then again reacted at 100°C for 20 minutes. After that, a resulting mixture was

subjected to filter pressing. A product resulted from the filter pressing was washed with hexane five times. Finally, a resulting product was vacuum dried to obtain a spherical carrier Z2 of an olefin polymerization catalyst.

5 The spherical carrier Z2 of the olefin polymerization catalyst had an average particle diameter (D50) of 18 microns, and a particle size distribution ((D90-D10)/D50) of 0.7. As it is observed through an optical microscope, particles of the spherical carrier Z2 of the olefin polymerization catalyst have relatively regular morphology and smooth surfaces, are basically all spherical, and have a relatively
10 narrow particle size distribution, and among them are basically no non-spherical particles.

According to gas chromatography-mass spectrometry, elemental analysis, and nuclear magnetic characterization, components of Z2 include a magnesium-containing

15 compound represented by a structural formula
$$\begin{array}{c} \text{CH}_2\text{Cl} \\ | \\ (\text{C}_2\text{H}_5\text{O})\text{Mg}(\text{OCH}) \\ | \\ \text{CH}_2\text{Cl} \end{array}$$
 and sulfur. A molar ratio of magnesium in the magnesium-containing compound to sulfur is 1:0.01.

Preparation Example 3

20 300 mL of white oil, 8.0 g (0.08 mol) of magnesium chloride, 28 mL (0.48 mol) of ethanol, 0.2 g (0.006 mol) of α -sulfur, and 1 g of PVP (polyvinylpyrrolidone) as a surfactant were added to a 0.6-L reactor, heated under stirring to 100°C and reacted at 100°C for 1 hour, followed by adding 12.5 mL (0.16 mol) of epoxychloropropane, and then again reacted at 100°C for 20 minutes. After that, a resulting mixture was
25 subjected to filter pressing. A product resulted from the filter pressing was washed with hexane five times. Finally, a resulting product was vacuum dried to obtain a spherical carrier Z3 of an olefin polymerization catalyst.

30 The spherical carrier Z3 of the olefin polymerization catalyst had an average particle diameter (D50) of 20 microns, and a particle size distribution ((D90-D10)/D50) of 0.8. As it is observed through an optical microscope, particles of the spherical carrier Z3 of the olefin polymerization catalyst have relatively regular

morphology and smooth surfaces, are basically all spherical, and have a relatively narrow particle size distribution, and among them are basically no non-spherical particles.

5 According to gas chromatography-mass spectrometry, elemental analysis, and nuclear magnetic characterization, components of Z3 include a magnesium-containing

compound represented by a structural formula
$$\begin{array}{c} \text{CH}_2\text{Cl} \\ | \\ (\text{C}_2\text{H}_5\text{O})\text{Mg}(\text{OCH}) \\ | \\ \text{CH}_2\text{Cl} \end{array}$$
 and sulfur. A molar ratio of magnesium in the magnesium-containing compound to sulfur is 1:0.007.

10

Preparation Example 4

0.08 mol of magnesium chloride, 0.96 mol of ethanol, and 1 g of PVP (polyvinylpyrrolidone) as a surfactant were added to a 0.6-L reactor, heated under stirring to 90°C and reacted at 90°C for 2 hours, followed by adding 38 mL (0.48 mol) of epoxychloropropane, and then again reacted at 90°C for 0.5 hour. After that, a resulting mixture was subjected to filter pressing. A product resulted from the filter pressing was washed with hexane five times. Finally, a resulting product was vacuum dried to obtain a carrier DZ1 of an olefin polymerization catalyst.

20

The carrier DZ1 of the olefin polymerization catalyst had an average particle diameter (D50) of 60 microns, and a particle size distribution ((D90-D10)/D50) of 1.3. Morphology of particles of the carrier observed through an optical microscope is as shown in Fig. 2. As can be seen from Fig. 2, among the particles of the carrier DZ1 of the olefin polymerization catalyst, there are non-spherical particles, and surfaces of the particles of the carrier DZ1 are relatively rough.

25

Example 1

30 (1) Preparation of a catalyst component for olefin polymerization:

90 ml of titanium tetrachloride was added to a 300-mL glass reaction flask,

cooled to -20°C, followed by adding 8 g of the above spherical carrier Z1, and heated to 110°C. During the heating, 2 mmol of ethyl benzoate and 7 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. After a resulting mixture was maintained at 110°C for 30 minutes, a liquid was filtered off. A resulting product
5 was washed with titanium tetrachloride twice and washed with hexane five times, and then vacuum dried to obtain a solid catalyst component Cat-1.

(2) Propylene polymerization:

10 Liquid phase bulk polymerization of propylene was carried out in a 5-L stainless steel autoclave. Under the protection of nitrogen, 1 ml of triethylaluminum in hexane (at a concentration of 0.5 mmol/ml), 0.1 ml of cyclohexylmethyldimethoxysilane (CHMMS) in hexane (at a concentration of 0.1 mmol/ml), and 6 mg of the above solid catalyst component Cat-1 were added successively to the autoclave. After the
15 autoclave was closed, 6.5 L of hydrogen (standard volume) and 2.3 L of liquid propylene were added. A resulting mixture was heated to 70°C, reacted for 1 hour, and then cooled, followed by pressure release and discharging.

An obtained propylene homopolymer was dried and then weighed and analyzed.
20 Results are shown in Table 1.

Example 2

(1) Preparation of a catalyst component for olefin polymerization:

25 90 ml of titanium tetrachloride was added to a 300-mL glass reaction flask, cooled to -20°C, followed by adding 8 g of the above solid component Z2, and heated to 110°C. During the heating, 2 mmol of ethyl o-methoxybenzoate and 9 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. After a resulting mixture
30 was maintained at 110°C for 30 minutes, a liquid was filtered off. A resulting product was washed with titanium tetrachloride twice and washed with hexane five times, and then vacuum dried to obtain a solid catalyst component Cat-2.

(2) Propylene polymerization:

Liquid phase bulk polymerization of propylene was carried out in a 5-L stainless steel autoclave. Under the protection of nitrogen, 1 ml of triethylaluminum in hexane (at a concentration of 0.5 mmol/ml), 0.1 ml of cyclohexylmethyldimethoxysilane (CHMMS) in hexane (at a concentration of 0.1 mmol/ml), and 6 mg of the above solid catalyst component Cat-2 were added successively to the autoclave. After the autoclave was closed, 6.5 L of hydrogen (standard volume) and 2.3 L of liquid propylene were added. A resulting mixture was heated to 70°C, reacted for 1 hour, and then cooled, followed by pressure release and discharging.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 3

(1) Preparation of a catalyst component for olefin polymerization:

90 ml of titanium tetrachloride was added to a 300-mL glass reaction flask, cooled to -20°C, followed by adding 8 g of the above solid component Z3, and heated to 110°C. During the heating, 0.5 mmol of ethyl o-methoxybenzoate and 7 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. After a resulting mixture was maintained at 110°C for 30 minutes, a liquid was filtered off. A resulting product was washed with titanium tetrachloride twice and washed with hexane five times, and then vacuum dried to obtain a solid catalyst component Cat-3.

(2) Propylene polymerization:

Liquid phase bulk polymerization of propylene was carried out in a 5-L stainless steel autoclave. Under the protection of nitrogen, 1 ml of triethylaluminum in hexane (at a concentration of 0.5 mmol/ml), 0.1 ml of cyclohexylmethyldimethoxysilane (CHMMS) in hexane (at a concentration of 0.1 mmol/ml), and 6 mg of the above solid catalyst component Cat-3 were added successively to the autoclave. After the autoclave was closed, 6.5 L of hydrogen (standard volume) and 2.3 L of liquid propylene were added. A resulting mixture was heated to 70°C, reacted for 1 hour, and

then cooled, followed by pressure release and discharging.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

5

Example 4

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that that
10 amounts of ethyl o-methoxybenzoate and 2-isopropyl-2-isopentyl-1,3-dimethoxypropane added during the heating were 5.6 mmol and 8 mmol, respectively. The obtained catalyst component for olefin polymerization was Cat-4.

15 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 5

20 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that what were added during the heating were 1.1 mmol of ethyl o-methoxybenzoate and 7.3 mmol of 9,9-dimethoxymethylfluorene rather than o-methoxybenzoate and 2-isopropyl-2-isopentyl-1,3-dimethoxypropane. The obtained catalyst component for
25 olefin polymerization was Cat-5.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 6

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 2.8 mmol of ethyl o-methoxybenzoate and 8 mmol of

9,9-dimethoxymethylfluorene were added. The obtained catalyst component for olefin polymerization was Cat-6.

An obtained propylene homopolymer was dried and then weighed and analyzed.

5 Results are shown in Table 1.

Example 7

10 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 0.8 mmol of ethyl o-methoxybenzoate and 8 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. The obtained catalyst component for olefin polymerization was Cat-7.

15 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 8

20 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 5 mmol of ethyl o-methoxybenzoate and 7 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. The obtained catalyst component for olefin polymerization was Cat-8.

25 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 9

30 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 2.5 mmol of ethyl o-methoxybenzoate and 8.5 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. The obtained catalyst

component for olefin polymerization was Cat-9.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

5

Example 10

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 3 mmol of ethyl o-methoxybenzoate and 8 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. The obtained catalyst component for olefin polymerization was Cat-10.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

15

Example 11

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 2.3 mmol of ethyl o-hydroxybenzoate and 8.7 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. The obtained catalyst component for olefin polymerization was Cat-11.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

25

Example 12

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that during the heating 4 mmol of ethyl benzoate and 7 mmol of 9,9-dimethoxymethylfluorene were added. The obtained catalyst component for olefin polymerization was Cat-12.

30

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 13

(1) Preparation of a catalyst component

90 ml (820 mmol) of titanium tetrachloride was added to a 300-ml glass reaction flask, and cooled to -20°C, followed by adding 37 mmol (based on magnesium element) of a magnesium halide carrier (prepared according to the method disclosed in Example 1 of CN1330086A), and then heated to 110°C. During the heating, 2.5 mmol of ethyl o-ethoxybenzoate and 7.1 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane were added. After a resulting mixture was maintained at 110°C for 30 minutes, a liquid was filtered off. A resulting product was washed with titanium tetrachloride twice and washed with hexane five times, and then vacuum dried to obtain a catalyst component Cat-13 for olefin polymerization.

(2) Liquid phase bulk polymerization of propylene

Liquid phase bulk polymerization of propylene was carried out in a 5-L stainless steel autoclave. Under the protection of nitrogen, 1 ml of triethylaluminum in hexane (at a concentration of 0.5 mmol/ml), 0.1 ml of cyclohexylmethyldimethoxysilane (CHMMS) in hexane (at a concentration of 0.1 mmol/ml), and 8 mg of the above catalyst component Cat-13 for olefin polymerization were added successively to the autoclave. After the autoclave was closed, 6.5 L of hydrogen (standard volume) and 2.3 L of liquid propylene were added. A resulting mixture was heated to 70°C, reacted for 1 hour, and then cooled, followed by pressure release and discharging. An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Example 14

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 13, except that the

internal electron donor added during the heating was 1.5 mmol of ethyl o-ethoxybenzoate and 10 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane. The obtained catalyst component for olefin polymerization was Cat-14.

- 5 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Comparative Example 1

- 10 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that the internal electron donor added during the heating was 9 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane. The obtained catalyst component for olefin polymerization was Com-Cat-1.

- 15 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Comparative Example 2

- 20 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that the internal electron donor added during the heating was 9 mmol of ethyl o-methoxybenzoate. The obtained catalyst component for olefin polymerization was
- 25 Com-Cat-2.

 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Comparative Example 3

 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that the internal electron donor added during the heating was 9 mmol of ethyl benzoate. The

obtained catalyst component for olefin polymerization was Com-Cat-3.

An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

5

Comparative Example 4

A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 13, except that the
10 internal electron donor added during the heating was 0.3 mmol of ethyl o-ethoxybenzoate and 8.5 mmol of 9,9-dimethoxymethylfluorene. The obtained catalyst component for olefin polymerization was Com-Cat-4.

An obtained propylene homopolymer was dried and then weighed and analyzed.
15 Results are shown in Table 1.

Comparative Example 5

A catalyst component was prepared and liquid phase bulk polymerization of
20 propylene was carried out in a same way as those in Example 2, except that the internal electron donor added during the heating was 7 mmol of ethyl o-methoxybenzoate and 9 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane. The obtained catalyst component for olefin polymerization was Com-Cat-5.

25 An obtained propylene homopolymer was dried and then weighed and analyzed. Results are shown in Table 1.

Comparative Example 6

30 A catalyst component was prepared and liquid phase bulk polymerization of propylene was carried out in a same way as those in Example 2, except that the internal electron donor added during the heating was 5 mmol of ethyl o-ethoxybenzoate and 5 mmol of 2-isopropyl-2-isopentyl-1,3-dimethoxypropane. The obtained catalyst component for olefin polymerization was Com-Cat-6.

An obtained propylene homopolymer was dried and then weighed and analyzed.
Results are shown in Table 1.

5

Table 1

	Catalyst component	Internal electron donor A added during preparation	Internal electron donor B added during preparation	Molar ration of A to B in catalyst component	Isotactic index of polymer I.I (%)	Melt index of polymer M.I (g/10min)
Example 1	Cat-1	ethyl benzoate	ether	0.05:1	98.0	73
Example 2	Cat-2	ethyl o-methoxybenzoate	ether	0.03:1	98.1	76
Example 3	Cat-3	ethyl o-methoxybenzoate	ether	0.008:1	97.2	79
Example 4	Cat-4	ethyl o-methoxybenzoate	ether	0.40:1	97.2	70
Example 5	Cat-5	ethyl o-ethoxybenzoate	fluorene ether	0.09:1	97.6	74
Example 6	Cat-6	ethyl o-methoxybenzoate	fluorene ether	0.23:1	97.5	70
Example 7	Cat-7	ethyl o-methoxybenzoate	ether	0.005:1	97.0	76
Example 8	Cat-8	ethyl o-methoxybenzoate	ether	0.64:1	96.9	69
Example 9	Cat-9	ethyl o-methoxybenzoate	ether	0.05:1	98.2	75
Example 10	Cat-10	ethyl o-methoxybenzoate	ether	0.09:1	98.3	73
Example 11	Cat-11	ethyl o-hydroxybenzoate	ether	0.12:1	98.1	75
Example 12	Cat-12	ethyl benzoate	fluorene ether	0.34:1	97.4	72
Example 13	Cat-13	ethyl o-ethoxybenzoate	ether	0.12:1	97.6	80
Example 14	Cat-14	ethyl o-ethoxybenzoate	ether	0.10:1	97.3	79
Comparative Example 1	Com- Cat-1	0	ether		95.3	79
Comparative	Com- Cat-2	ethyl	0		91.0	40

Example 2		o-methoxybenzoate				
Comparative Example 3	Com- Cat-3	ethyl benzoate	0		90.2	36
Comparative Example 4	Com- Cat-4	ethyl o-ethoxybenzoate	fluorene ether	0.003:1	95.2	68
Comparative Example 5	Com- Cat-5	ethyl o-methoxybenzoate	ether	0.75:1	94.5	45
Comparative Example 6	Com- Cat-6	ethyl o-ethoxybenzoate	ether	0.80:1	94.5	38

In Table 1, “ether” represents “2-isopropyl-2-isopentyl-1,3-dimethoxypropane”; “fluorenyl ether” represents “9,9-dimethoxymethylfluorene”; contents of internal electron donors A and B in the catalyst component were measured by a gas chromatograph (thermoelectric Trace GC Ultra).

Table 2

	Average particle diameter of catalyst particles (μm)
Example 1	13
Example 2	17
Example 3	18
Example 4	16
Example 5	17
Example 6	16

As can be seen from the results of the Examples and Comparative Examples in Table 1, when the catalyst component of the present invention in which the internal electron donor comprises both a monocarboxylic ester compound and a diether compound, especially when the molar ratio of the monocarboxylic ester compound to the diether compound is (0.0035-0.7):1, preferably (0.0040-0.7):1, more preferably (0.0045-0.060):1, further more preferably (0.005-0.5):1, still more preferably (0.01-0.35):1, is used, the prepared polypropylene has a significantly improved isotactic index as well as a high melt index. In other words, the catalyst of the present

invention can be used to prepare a polymer with both a high isotactic index and a high melt flow index.

5 The catalyst of the present invention free of a phthalate compound (plasticizer) has characteristics of high stereospecificity and high hydrogen response.

10 It should be noted that the above described embodiments are only used to explain the present invention and do not constitute any limitation to the present invention. The present invention may be modified within the scope of the claims of the present invention as required, and may be revised without departing from the scope and spirit of the present invention. Although the present invention described herein relates to specific methods, materials, and embodiments, it does not mean that the present invention is limited to the specific embodiments disclosed therein. On the contrary, the present invention can be extended to all other methods and applications with the same functions.

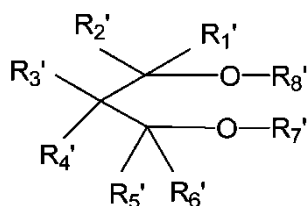
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Claims

1. A catalyst component for olefin polymerization, comprising magnesium, titanium, a halogen, and an internal electron donor, wherein the internal electron donor comprises a monocarboxylic ester compound and a diether compound, a molar ratio of the monocarboxylic ester compound to the diether compound being (0.0035-0.7):1.

2. The catalyst component according to claim 1, wherein the molar ratio of the monocarboxylic ester compound to the diether compound is (0.0040-0.7):1, preferably (0.0045-0.060):1, more preferably (0.005-0.5):1, further more preferably (0.01-0.35):1, most preferably (0.02-0.25):1.

3. The catalyst component according to claim 1 or 2, wherein the diether compound is a 1,3-diether compound, preferably a diether compound as shown in Formula I,



Formula I

wherein in Formula I,

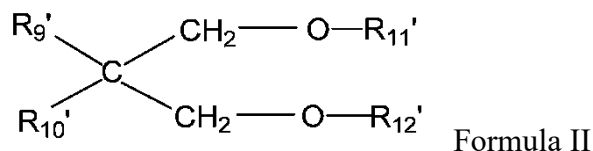
R₁', R₂', R₃', R₄', R₅' and R₆' are identical to or different from each other, each independently selected from the group consisting of hydrogen, halogen, substituted or unsubstituted C₁-C₂₀ linear or branched alkyl, substituted or unsubstituted C₃-C₂₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl, preferably selected from the group consisting of hydrogen, halogen, substituted or unsubstituted C₁-C₁₈ linear or branched alkyl, substituted or unsubstituted C₃-C₁₈ cycloalkyl, substituted or unsubstituted C₆-C₁₈ aryl, substituted or unsubstituted C₇-C₁₈ aralkyl, and substituted or unsubstituted C₇-C₁₈ alkaryl; or, two or more of R₁', R₂', R₃', R₄', R₅' and R₆' are bonded to each other to form a ring;

R₇' and R₈' are identical to or different from each other, each independently selected from the group consisting of substituted or unsubstituted C₁-C₂₀ linear or

branched alkyl, substituted or unsubstituted C₃-C₂₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl, preferably selected from the group consisting of substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₅ aryl, substituted or unsubstituted C₇-C₁₅ aralkyl, and substituted or unsubstituted C₇-C₁₅ alkaryl; and

the monocarboxylic ester compound is selected from an aromatic monocarboxylic ester and an aliphatic monocarboxylic ester; preferably, the aliphatic monocarboxylic ester is a monoester formed by an aliphatic monocarboxylic acid having 2-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms; preferably, the aromatic monocarboxylic ester is a monoester formed by an aromatic monocarboxylic acid having 7-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms.

4. The catalyst component according to any one of claims 1 to 3, wherein the diether compound is a 1,3-diether compound as shown in Formula II,



wherein in Formula II,

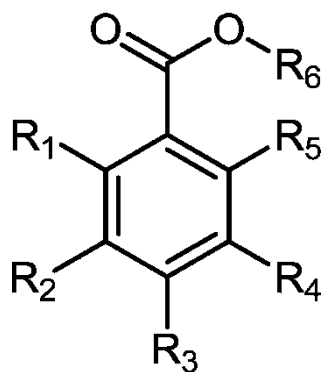
R₉' and R₁₀' are identical to or different from each other, each independently selected from the group consisting of hydrogen, halogen, substituted or unsubstituted C₁-C₁₈ linear or branched alkyl, substituted or unsubstituted C₃-C₁₈ cycloalkyl, substituted or unsubstituted C₆-C₁₈ aryl, substituted or unsubstituted C₇-C₁₈ aralkyl, and substituted or unsubstituted C₇-C₁₈ alkaryl, preferably selected from the group consisting of hydrogen, halogen, substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₅ aryl, substituted or unsubstituted C₇-C₁₅ aralkyl, and substituted or unsubstituted C₇-C₁₅ alkaryl; or, R₉' and R₁₀' are bonded to each other to form a ring; preferably R₉' and R₁₀' are bonded to each other to form a fluorene ring; and

R₁₁' and R₁₂' are identical to or different from each other, each independently being substituted or unsubstituted C₁-C₁₀ linear or branched alkyl.

5. The catalyst component according to any one of claims 1 to 4, wherein the aliphatic monocarboxylic ester is a monoester formed by an aliphatic monocarboxylic acid having 2-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms; and

the aromatic monocarboxylic ester is a monoester formed by an aromatic monocarboxylic acid having 7-10 carbon atoms and an aliphatic mono- or polyhydric alcohol having 1-15 carbon atoms or an aromatic alcohol having 6-15 carbon atoms.

6. The catalyst component according to any one of claims 1 to 5, wherein the aromatic monocarboxylic ester is an aromatic monocarboxylic ester as shown in Formula III:



Formula III

wherein in Formula III,

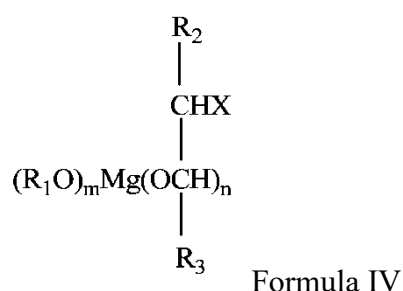
R₁-R₅ are identical to or different from each other, each independently selected from the group consisting of hydrogen, hydroxyl, halogen, amino, substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₁-C₁₀ alkoxy, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl; or any two of R₁-R₅ form an aromatic ring or an aliphatic ring; R₆ is selected from the group consisting of substituted or unsubstituted C₁-C₁₀ linear or branched alkyl, substituted or unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl, preferably selected from substituted or unsubstituted C₁-C₆ linear or branched alkyl.

7. The catalyst component according to any one of claims 1 to 6, wherein the

catalyst component is a product produced from a reaction of a magnesium source, a titanium source, and the internal electron donor;

preferably, the magnesium source comprises one or more magnesium compounds selected from the group consisting of magnesium dihalide, magnesium alkoxide, magnesium alkyl, a hydrate or alcoholate of magnesium dihalide, and a derivative
5 derived by substituting a halogen atom in a formula of magnesium dihalide with alkoxy or halogenated alkoxy.

8. The catalyst component according to claim 7, wherein the magnesium source
10 comprises a magnesium compound as shown in Formula IV,



wherein in Formula IV,

R₁ is selected from the group consisting of substituted or unsubstituted C₁-C₁₀ linear alkyl, substituted or unsubstituted C₃-C₁₀ branched alkyl, substituted or
15 unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl;
preferably, R₁ is selected from the group consisting of substituted or unsubstituted C₁-C₈ linear alkyl, substituted or unsubstituted C₃-C₈ branched alkyl, substituted or
unsubstituted C₃-C₈ cycloalkyl, substituted or unsubstituted C₆-C₁₅ aryl, substituted or
20 unsubstituted C₇-C₁₅ aralkyl, and substituted or unsubstituted C₇-C₁₅ alkaryl; more
preferably, R₁ is selected from the group consisting of substituted or unsubstituted C₁-C₆ linear alkyl, substituted or unsubstituted C₃-C₆ branched alkyl, substituted or
unsubstituted C₃-C₆ cycloalkyl, substituted or unsubstituted C₆-C₁₀ aryl, substituted or
unsubstituted C₇-C₁₀ aralkyl, and substituted or unsubstituted C₇-C₁₀ alkaryl;

25 R₂ and R₃ are identical to or different from each other, each independently
selected from the group consisting of hydrogen, substituted or unsubstituted C₁-C₁₀
linear alkyl, substituted or unsubstituted C₃-C₁₀ branched alkyl, substituted or
unsubstituted C₃-C₁₀ cycloalkyl, substituted or unsubstituted C₆-C₂₀ aryl, substituted
or unsubstituted C₇-C₂₀ aralkyl, and substituted or unsubstituted C₇-C₂₀ alkaryl;

preferably, R_2 and R_3 are each independently selected from the group consisting of hydrogen, substituted or unsubstituted C_1 - C_{10} linear alkyl, substituted or unsubstituted C_3 - C_8 branched alkyl, substituted or unsubstituted C_3 - C_8 cycloalkyl, substituted or unsubstituted C_6 - C_{10} aryl, substituted or unsubstituted C_7 - C_{10} aralkyl, and substituted or unsubstituted C_7 - C_{10} alkaryl; more preferably, R_2 and R_3 are each independently selected from the group consisting of hydrogen, substituted or unsubstituted C_1 - C_6 linear alkyl, substituted or unsubstituted C_3 - C_6 branched alkyl, substituted or unsubstituted C_3 - C_6 cycloalkyl, substituted or unsubstituted C_6 - C_8 aryl, substituted or unsubstituted C_7 - C_9 aralkyl, and substituted or unsubstituted C_7 - C_9 alkaryl;

10 X is a halogen, preferably chlorine or bromine;
 m is 0.1-1.9; n is 0.1-1.9; and $m+n=2$;
 preferably, the titanium source comprises titanium halide, titanium alkoxide halide, and titanium alkoxide; more preferably, the titanium source comprises a compound represented by a general formula $Ti(OR')_{3-a}Z_a$ and/or $Ti(OR')_{4-b}Z_b$, wherein
 15 R' is C_1 - C_{20} alkyl; Z is F, Cl, Br or I; a is an integer from 1 to 3; and b is an integer from 1 to 4.

9. The catalyst component according to claim 7 or 8, wherein the magnesium source further comprises sulfur, a molar ratio of sulfur to magnesium in the
 20 magnesium source is $q:1$, wherein $0 < q \leq 0.5$, preferably $0.001 < q \leq 0.2$.

10. The catalyst component according to any one of claims 7 to 9, wherein the magnesium source is prepared by a method comprising the following steps:

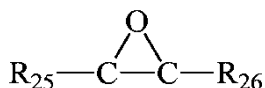
(1) preparing a mixture, wherein the mixture comprises elemental sulfur, a
 25 magnesium halide represented by a general formula MgX_1Y , a compound represented by a general formula R_1OH , an optional inert liquid medium, and an optional surfactant; preferably, the mixture is obtained by mixing the elemental sulfur, the magnesium halide represented by the general formula MgX_1Y , the compound represented by the general formula R_1OH , the optional inert liquid medium, and the
 30 optional surfactant together at one time or step by step and then heating a resulting mixture; and

(2) subjecting the mixture obtained in step (1) to a contact reaction with an ethylene oxide compound;

wherein in the general formula MgX_1Y , X_1 is a halogen, and is preferably chlorine or bromine; Y is selected from the group consisting of halogen, substituted or unsubstituted C_1-C_{10} linear alkyl, substituted or unsubstituted C_3-C_{10} branched alkyl, substituted or unsubstituted C_3-C_{10} cycloalkyl, substituted or unsubstituted C_6-C_{20} aryl, substituted or unsubstituted C_1-C_{10} alkoxy, substituted or unsubstituted C_6-C_{20} aryloxy, substituted or unsubstituted C_7-C_{20} aralkyl, and substituted or unsubstituted C_7-C_{20} alkaryl;

in the general formula R_1OH , R_1 is selected from the group consisting of substituted or unsubstituted C_1-C_{10} linear alkyl, substituted or unsubstituted C_3-C_{10} branched alkyl, substituted or unsubstituted C_3-C_{10} cycloalkyl, substituted or unsubstituted C_6-C_{20} aryl, substituted or unsubstituted C_7-C_{20} aralkyl, and substituted or unsubstituted C_7-C_{20} alkaryl; preferably, R_1 is selected from the group consisting of substituted or unsubstituted C_1-C_8 linear alkyl, substituted or unsubstituted C_3-C_8 branched alkyl, substituted or unsubstituted C_3-C_8 cycloalkyl, substituted or unsubstituted C_6-C_{15} aryl, substituted or unsubstituted C_7-C_{15} aralkyl, and substituted or unsubstituted C_7-C_{15} alkaryl; more preferably, R_1 is selected from the group consisting of substituted or unsubstituted C_1-C_6 linear alkyl, substituted or unsubstituted C_3-C_6 branched alkyl, substituted or unsubstituted C_3-C_6 cycloalkyl, substituted or unsubstituted C_6-C_{10} aryl, substituted or unsubstituted C_7-C_{10} aralkyl, and substituted or unsubstituted C_7-C_{10} alkaryl;

the ethylene oxide compound has a structure shown in Formula V:



Formula V

wherein in Formula V, R_{25} and R_{26} are each independently selected from the group consisting of hydrogen, substituted or unsubstituted C_1-C_{10} linear alkyl, substituted or unsubstituted C_3-C_{10} branched alkyl, substituted or unsubstituted C_3-C_{10} cycloalkyl, substituted or unsubstituted C_6-C_{20} aryl, substituted or unsubstituted C_7-C_{20} aralkyl, and substituted or unsubstituted C_7-C_{20} alkaryl; preferably, R_{25} and R_{26} are each independently selected from the group consisting of hydrogen, substituted or unsubstituted C_1-C_8 linear alkyl, substituted or unsubstituted C_3-C_8 branched alkyl, substituted or unsubstituted C_3-C_8 cycloalkyl, substituted or unsubstituted C_6-C_{10} aryl, substituted or unsubstituted C_7-C_{10} aralkyl, and substituted or unsubstituted C_7-C_{10}

alkaryl; more preferably, R₂₅ and R₂₆ are each independently selected from the group consisting of hydrogen, substituted or unsubstituted C₁-C₆ linear alkyl, substituted or unsubstituted C₃-C₆ branched alkyl, substituted or unsubstituted C₃-C₆ cycloalkyl, substituted or unsubstituted C₆-C₈ aryl, substituted or unsubstituted C₇-C₉ aralkyl, and substituted or unsubstituted C₇-C₉ alkylaryl.

11. The catalyst component according to claim 10, wherein based on 1 mol of the magnesium halide represented by the general formula MgX₁Y, the elemental sulfur is present in an amount of 0.0001-0.5 mol, the compound represented by the general formula R₁OH is present in an amount of 4-30 mol, and the ethylene oxide compound is present in an amount of 1-10 mol;

preferably, based on 1 mol of the magnesium halide represented by the general formula MgX₁Y, the compound represented by the general formula R₁OH is present in an amount of 6-20 mol, and the ethylene oxide compound is present in an amount of 2-6 mol.

12. The catalyst component according to claim 10 or 11, wherein in step (1), the heating is conducted at a temperature of 80-120°C for a time period of 0.5-5 hours, preferably at a temperature of 80-100°C for a time period of 0.5-3 hours; and

in step (2), the contact reaction is carried out at conditions comprising reacting at a temperature of 40-120°C for a time period of 15-60 minutes, preferably at a temperature of 60-100°C for a time period of 20-50 minutes.

13. The catalyst component according to any one of claims 10 to 12, wherein the inert liquid medium is a silicone oil solvent and/or a hydrocarbon solvent; preferably, the inert liquid medium is at least one selected from the group consisting of kerosene, paraffin oil, petrolatum oil, white oil, methyl silicone oil, ethyl silicone oil, methyl ethyl silicone oil, phenyl silicone oil, and methyl phenyl silicone oil; and/or

based on 1 mol of the magnesium halide represented by the general formula MgX₁Y, the inert liquid medium is present in an amount of 0.8-10 L.

14. The catalyst component according to any one of claims 10 to 13, wherein the surfactant is at least one selected from the group consisting of polyvinylpyrrolidone, polyethylene glycol, polyvinyl alcohol, polyacrylic acid, polyacrylate, polyacrylamide,

polystyrene sulfonate, naphthalenesulfonic acid formaldehyde condensate, condensed alkyl phenyl ether sulfate, condensed alkyl phenol polyoxyethylene ether phosphate, oxyalkyl acrylate copolymer modified polyethyleneimine, 1-dodeca-4-vinylpyridine bromide polymer, polyvinylbenzyltrimethylamine salt, polyethylene oxide propylene
5 oxide block copolymer, polyvinylpyrrolidone vinyl acetate copolymer, alkyl phenyl polyoxyethylene ether, and polyalkyl methacrylate; and/or

based on 1 mol of the magnesium halide represented by the general formula MgX_1Y , the surfactant is present in an amount of 1-20 g.

10 15. The catalyst component according to any one of claims 10 to 14, wherein in the general formula MgX_1Y , X_1 is chlorine or bromine, and Y is chlorine, bromine, C_1 - C_5 alkoxy or C_6 - C_{10} aryloxy; preferably, the magnesium halide represented by the general formula MgX_1Y is at least one selected from the group consisting of magnesium chloride, magnesium bromide, phenoxymagnesium chloride,
15 isopropoxymagnesium chloride, and n-butoxymagnesium chloride; and/or

in the general formula R_1OH , R_1 is C_1 - C_8 alkyl; preferably, the compound represented by the general formula R_1OH is at least one selected from the group consisting of ethanol, n-propanol, isopropanol, n-butanol, isobutanol, n-pentanol, isopentanol, n-hexanol, 2-ethylhexanol, and n-octanol; and/or

20 in the ethylene oxide compound having the structure shown in Formula V, R_5 and R_6 are each independently hydrogen, C_1 - C_3 alkyl, or C_1 - C_3 halogenated alkyl; preferably, the ethylene oxide compound is at least one selected from the group consisting of ethylene oxide, epoxyp propane, epoxybutane, epoxychloropropane, epoxychlorobutane, epoxybromopropane, and epoxybromobutane.

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16. The catalyst component according to any one of claims 1 to 15, wherein in the catalyst component, a weight ratio of titanium as titanium element, to magnesium as magnesium element, to the halogen, and to the internal electron donor is 1:2-15:8-30:2-15, preferably 1:3-12:10-25:3-13.

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17. A catalyst for olefin polymerization, comprising:

- (1) the catalyst component according to any one of claims 1 to 16;
- (2) at least one alkyl aluminum compound; and
- (3) an optional external electron donor compound.

18. Use of the catalyst according to claim 17 in polymerization of an olefin, wherein, preferably, the olefin comprises at least one olefin represented by a formula $\text{CH}_2=\text{CHR}$, R being hydrogen or C_1 - C_6 linear or branched alkyl.

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19. An olefin polymerization method, comprising: contacting the olefin with an catalyst according to claim 17 under olefin polymerization condition, wherein, preferably, the olefin comprises at least one of olefin represented by a formula $\text{CH}_2=\text{CHR}$, R being hydrogen or C_1 - C_6 linear or branched alkyl.