In a preferred embodiment of the present invention, said second evaporation step (d) may be carried out at a temperature ranging from 30°C to 150°C, preferably ranging from 40°C to 130°C.

In a preferred embodiment of the present invention, said second evaporation step (d) may be carried out at a pressure ranging from 1 mbar to 100 mbar, preferably ranging from 8 mbar to 80 mbar.

Any type of evaporator known in the art may advantageously be used for the purpose of the aforementioned step (d). Specific examples of evaporators which may advantageously be used are those reported above. Preferably, a wiped-film evaporator may be used in said step (d).

At the end of said second evaporation step (d), a concentrated solution is obtained comprising bio-1,3-butanediol, water and traces of heavy organic compounds [for example, 4-hydroxy-2-butanone (4-OH-2B)], of unconverted sugars and of any unremoved salts, which is sent to the third evaporation step (e), as well as an aqueous phase comprising primarily water, organic compounds having a boiling point lower than that of bio-1,3-butanediol, and traces of bio-1,3-butanediol which may be sent directly to a water treatment plant.

In a preferred embodiment of the present invention, said third evaporation step (e) may be carried out at a temperature ranging from 30°C to 150°C, preferably ranging from 40°C to 130°C.

In a preferred embodiment of the present invention, said third evaporation step (e) may be carried out at a pressure ranging from 5 mbar to 100 mbar, preferably ranging from 8 mbar to 80 mbar.

Any type of evaporator known in the art may advantageously be used for the purpose of the aforementioned step (e). Specific examples of evaporators which may