

Claims:

1. A process for production of a hydrocarbon fraction suitable for use as jet fuel (124) from an oxygenate feedstock (102), comprising the steps of
 - a. combining the feedstock (102) with an amount of a liquid diluent (128) to form a combined feedstock (104), directing said combined feedstock (104) to contact a material catalytically active in hydrodeoxygenation (HDO) under hydrotreating conditions to provide a hydrodeoxygenated intermediate product (106),
 - b. separating said hydrodeoxygenated intermediate product (106) in at least two fractions including a vapor fraction and a liquid fraction (108),
 - c. optionally providing at least an amount of said liquid fraction (108) as said liquid diluent (128),
 - d. directing at least an amount of said liquid fraction (108) to contact a material catalytically active in isomerization (ISOM) under isomerization conditions to provide an isomerized intermediate product (112),
 - e. directing at least an amount of said isomerized intermediate product (112) and a stream comprising sulfur (114) to contact a material catalytically active in hydrocracking (HDC) under hydrocracking conditions to provide a hydrocracked intermediate product (118), and
 - f. fractionating said hydrocracked intermediate product (116) providing at least said hydrocarbon fraction suitable for use as jet fuel (124).
2. The process according to claim 1, wherein said hydrocarbon fraction suitable for use as jet fuel (124) has a final boiling point according to ASTM D86 being less than 300°C.
3. The process according to claim 1 or 2, wherein the volume of hydrogen sulfide relative to the volume of molecular hydrogen in the gas phase of the combined feedstock (104) directed to contact the material catalytically active in hydrodeoxygenation is at least 50 ppm_v, 100 ppm_v or 200 ppm_v, optionally by adding a stream comprising one or more sulfur compounds, such as dimethyl disulfide or fossil fuels.
4. The process according to claim 1, 2, or 3, wherein the volume of hydrogen sulfide relative to the volume of molecular hydrogen in the gas phase of the total stream

(116) directed to contact the material catalytically active in hydrocracking (HDC) is at least 50 ppm_v, 100 ppm_v or 200 ppm_v, possibly originating from added an stream (114) comprising one or more sulfur compounds, such as dimethyl disulfide or fossil fuels.

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5. The process according to claim 1, 2, 3, or 4, wherein said feedstock (102) comprises at least 50%wt triglycerides or fatty acids.

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6. The process according to claim 1, 2, 3, 4, or 5, wherein hydrodeoxygenation conditions involve a temperature in the interval 250-400°C, a pressure in the interval 30-150 Bar, and a liquid hourly space velocity (LHSV) in the interval 0.1-2 and wherein the material catalytically active in hydrodeoxygenation comprises one or more sulfided metals taken from the group of nickel, cobalt, molybdenum or tungsten, supported on a carrier comprising one or more refractory oxides, such as alumina, silica or titania.

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7. The process according to claim 1, 2, 3, 4, 5, or 6, wherein hydrocracking conditions involve a temperature in the interval 250-425°C, a pressure in the interval 30-150 Bar, and a liquid hourly space velocity (LHSV) in the interval 0.5-4, optionally together with intermediate cooling by quenching with cold hydrogen, feed or product and wherein the material catalytically active in hydrocracking comprises (a) one or more active metals taken from the group platinum, palladium, nickel, cobalt, tungsten and molybdenum, (b) an acidic support taken from the group of a molecular sieve showing high cracking activity, and having a topology such as MFI, BEA and FAU and amorphous acidic oxides such as silica-alumina and (c) a refractory support such as alumina, silica or titania, or combinations thereof.

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8. The process according to claim 1, 2, 3, 4, 5, 6, or 7, wherein the amount of material boiling above 300°C in said hydrocracked intermediate product (118) is reduced by at least 20%wt, 50%wt or 80%wt or more compared to said isomerized intermediate product (116).

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9. The process according to claim 1, 2, 3, 4, 5, 6, 7, or 8, wherein at least an amount of said isomerized intermediate product (112) or said hydrocracked intermediate

product (118) is directed to contact a material catalytically active in hydrodearomatization (HDA) under hydrodearomatization conditions to provide a hydrodearomatized product comprising less than 1 wt/wt%, 0.5 wt/wt% or 0.1 wt/wt%, calculated by total mass of the aromatic molecules relative to all hydrocarbons in the stream, where said hydrodearomatized product is fractionated in place of said hydrocracked intermediate product (116) in step (f).

10. The process according to claim 9, wherein hydrodearomatization conditions involve a temperature in the interval 200-350°C, a pressure in the interval 30-150 Bar, and a liquid hourly space velocity (LHSV) in the interval 0.5-8 and wherein said material catalytically active in hydrodearomatization comprises an active metal taken from the group comprising platinum, palladium, nickel, cobalt, tungsten and molybdenum, preferably one or more sulfided base metals such as nickel, cobalt, tungsten and molybdenum and a refractory support, preferably amorphous silica-alumina, alumina, silica or titania, or combinations thereof.

11. The process according to claim 8, 9, or 10, wherein a hydrogen rich stream comprising at least 90 vol/vol% hydrogen is directed to contact the material catalytically active in hydrodearomatization.

12. The process according to claim 1, 2, 3, 4, 5, 6, 7, 8, 9, 10, or 11, wherein isomerization conditions involves a temperature in the interval 250-350°C, a pressure in the interval 30-150 Bar, and a liquid hourly space velocity (LHSV) in the interval 0.5-8 and wherein the material catalytically active in isomerization comprises an active metal taken from the group comprising platinum, palladium, nickel, cobalt, tungsten and molybdenum, preferably one or more elemental noble metals such as platinum or palladium, an acidic support preferably a molecular sieve, more preferably having a topology taken from the group comprising MOR, FER, MRE, MWW, AEL, TON and MTT and an amorphous refractory support comprising one or more oxides taken from the group comprising alumina, silica and titania or combinations thereof.

13. A process plant for production of a hydrocarbon fraction suitable for use as jet fuel (124) from a feedstock (102) being a renewable feedstock or an oxygenate feedstock, said process plant comprising a hydrodeoxygenation section (HDO), a separation section (SEP), an isomerization section (ISOM), a hydrocracking section (HDC) and a fractionation section (FRAC), said process plant being configured for
- 5 a. directing the feedstock (102) and a liquid diluent (128) to the hydrodeoxygenation section (HDO) to provide a hydrodeoxygenated intermediate product (106),
- 10 b. separating said hydrodeoxygenated intermediate product (106) in a vapor fraction and a liquid fraction (108) in said separation section (SEP),
- 15 c. directing at least an amount of said hydrodeoxygenated intermediate product (108) to contact a material catalytically active in isomerization (ISOM) under isomerization conditions providing an isomerized intermediate product (112), and
- 20 d. directing at least an amount of said isomerized intermediate product (116) an a stream comprising sulfur (114) to contact a material catalytically active in hydrocracking (HDC) under hydrocracking conditions to provide the hydrocracked intermediate product (118),
- 25 e. fractionating said isomerized intermediate product (116) in said fractionation section (FRAC) to provide at least a hydrocarbon fraction suitable for use as jet fuel (124).
14. A process plant according to claim 13 further comprising a recycle connection being configured for providing an amount of said liquid hydrodeoxygenated product (108) as liquid diluent (128).