What is claimed is:

1. A method of generating at least one of H_2 and Fischer Tropsch liquids, the method comprising:

receiving feedstock into an initial reformer;

reforming, in the initial reformer, at least a portion of the feedstock with steam to produce an input gas, wherein an amount of the input gas is syngas;

transferring the input gas from the initial reformer to a main reformer;

reforming, in the main reformer, the input gas with steam to increase the amount of syngas, wherein the syngas includes CO, H_2 and H_2O;

transferring the syngas from the main reformer to a Fischer Tropsch module;

using the syngas in a Fischer Tropsch reaction; and

extracting from the Fischer Tropsch module H_2O, CO, H_2, and CO_2 generated by the Fisher Tropsch reaction and Fischer Tropsch liquids generated by the Fischer Tropsch reaction; and

transferring CO, H_2 and CO_2 generated by the Fischer Tropsch reaction directly to the main reformer.

2. The method of claim 1, further comprising transferring hydrocarbons containing at least five carbon atoms generated by the Fischer Tropsch reaction to the main reformer.

3. The method of claim 1, wherein transferring the syngas from the main reformer into the Fischer Tropsch module further comprises condensing H_2O from the syngas prior to the syngas entering the Fischer Tropsch module.

4. The method of claim 1, wherein the syngas, when transferred into the Fischer Tropsch module, has a H_2/CO ratio between 1.5 to 3.5.

5. The method of claim 3, wherein the H_2/CO ratio is about 2.16.

6. The method of claim 3, wherein the H_2/CO ratio is about 2.3

7. The method of claim 1, wherein the syngas is transferred into the Fischer Tropsch module at a pressure not more than 125 psig.

8. The method of claim 1, wherein the initial reformer is a rotary reformer.

9. The method of claim 8, wherein the rotary reformer has a rotary reformer operating temperature, and wherein the main reformer has a main reformer operating temperature greater than the rotary reformer operating temperature.

10. The method of claim 8, further comprising extracting sulfur from the input gas by contacting the input gas with lime in the rotary reformer.

11. The method of claim 10, further comprising removing lime, using the rotary reformer.

12. The method of claim 1, wherein the feedstock comprises at least one of municipal solid waste, medical waste, digestate, and natural gas.

13. The method of claim 12, wherein the feedstock further comprises biogas and is substantially oxygen-free.

14. The method of claim 12, wherein the digestate has a moisture content of 24% to 70% by weight.

15. The method of claim 1, wherein the initial reformer is a cyclonic separator, and wherein the feedstock further comprises natural gas.

16. The method of claim 15, wherein the cyclonic separator has a cyclonic separator operating temperature, and wherein the main reformer has a main reformer operating temperature greater than the cyclonic separator operating temperature.

17. The method of claim 1, wherein the main reformer has a main reformer operating temperature equal to or less than 1600°F.

18. The method of claim 1, wherein combustion fails to occur in the initial reformer and in the main reformer.

19. The method of claim 1, wherein pressure in the initial reformer and the main reformer is maintained at about one atmosphere.