

## **A METHOD AND DEVICE FOR CLEANING NON-FIXED MEDIA FILTERS**

### **BACKGROUND OF THE INVENTION**

#### **5           1. Field of the Invention**

The present invention relates generally to the field of liquid filtration using unfixed filter media, and more specifically to a method and system for removing filtered contaminants from these type filter beds during periodic cleaning cycles.

10

#### **2. The Prior Art**

Various types of methods and systems have been used in the prior art to remove accumulated contaminants from a bed of granular filter medium. The methods utilized to date generally have these common processing steps: 1) providing an agitation means to break-up agglomerations of filter media and contaminants typically formed during the filtration process, 2) flowing a carrier medium through the agitated granules to mobilize the contaminants away from the filter media, 3) retaining the filter media within the filter while allowing contaminants to flow out, and 4) returning the cleaned filter media back to its normal state. These four steps can be condensed to the following: 1) agitation, 2) washing, 3) separating, and 4) reforming.

With regard to common Step 1, various means are disclosed to agitate the filter media such as rotary blades and high-velocity liquid jets (See U.S. Patent Nos. 2,521,396 and 3,992,291 / 3,953,333). However, both of these methods create at least two significant problems. First, rotary blade systems often have mechanical seals that require frequent maintenance. Second, the high-velocity liquid jets produce large volumes of dirty backwash water that must be stored and recycled through the process. What is needed in the art is an agitating means that does not require rotating internal baffles or impellers and minimizes liquid usage.

With regard to common step 2, the carrier medium used to flush the filter media is most commonly the clean filtrate fluid. In many systems, large volume storage of clean filtrate is required to provide surge capacity when the backwash cycle draws a high-volume rate to flush the media during this step. Some methods utilize the high-volume water jets to both agitate and back flush, which is a combination of common steps 1 and 2. However, such systems still generate large volumes of backwash liquid that must be stored and recycled back through the process. Also, it would be preferred to utilize contaminated process fluid for backwashing instead of clean filtrate. This would avoid having to have clean filtrate storage vessels and pumps specifically for periodic backwashing cycles.

With regard to common step 3, separation of the contaminants from the filter media is typically done by flowing the slurry in a continuous flow path over a cleaning element, located external to the filter housing, where interspersed larger particulates are removed from the slurry, and returning the withdrawn filter material back to the filter housing (See U.S. Patent Nos. 3,992,291 and 3,953,333). This method adds significant cost and size to the filter since it requires various external conduits, vessels, valves and equipment. U.S. Patent No. 4,787,987 discloses an in-situ method of separating the contaminants from the filter media by a screen, of size slightly smaller than the filter media size, contained within the vessel below the filter media. That method agitates and slurrifies the media and contaminants by action of a high-volume liquid pump. During this agitation step, make-up liquid is added to the vessel at substantially the same rate that the concentrated contaminated liquid is removed through the screen means while the filter media is retained within the filter housing.

The present invention is directed in part, to a novel means of in-situ agitation and fluidization of filter media granules to sufficiently liberate collected contaminants as rapidly as possible and flushing those contaminants from the filter housing using the least amount of liquid necessary. Other advantages that are inherent in the disclosed and claimed invention will be apparent of those of ordinary skill in the art.

## SUMMARY OF THE INVENTION

The inventors present a novel method of in-situ cleaning of agglomerated contaminants from granular filter media. This method combines a low rate of contaminated liquid with a gas, such as air or natural gas, to create a jetting stream. This jetting stream is dispersed into the filter media through one or more radial nozzles disposed within the filter media. The gas exits the radial nozzles as a bubble dispersion within the liquid. As the jetting stream rises up through the filter media, it expands the bed to break large contaminant agglomerations and fluidizes the individual filter media granules to dislodge and mobilize smaller contaminant agglomerations within the interstitial spaces of the filter media. This fluidizing action provides the requisite degree of agitation of the media to loosen and mobilize contaminant agglomerations without the need for high liquid space velocities common to other filter cleaning methods.

This method provides the benefit of allowing use of contaminated process liquid in the jetting stream, which eliminates the need for storing clean filtrate for use during backwash cycles.

This method provides the further benefit of minimizing the volume of contaminant-laden liquid water that must be reprocessed. Other filter cleaning methods require large liquid volume rates, up to 1.5 times the incoming liquid rate during normal operation, to provide sufficient interstitial velocity to mobilize contaminants away from the filter media. Lower backwash volumes reduce ancillary equipment costs and reprocessing costs.

This method provides the further benefit of reducing the cleaning cycle time. Other filter cleaning methods flow the gas separately through the filter media to break contaminant agglomerations followed by liquid flow through the media to flush contaminants away. By combining the agitation step with the flushing step, cleaning cycle times can be significantly reduced. Shorter cleaning cycle times will provide improved overall performance of the filter system.

This method provides the further benefit of allowing optimization of media cleaning cycle for a variety of filtering process. By adjusting the ratio of gas to liquid in the jetting stream and, if necessary, the size and location of the radial jetting

nozzles, the cleaning cycle can accommodate a broader variety of contaminate loading rates, agglomeration tendencies, and physical characteristics.

In a preferred embodiment of the invention, a granular media filter is  
5 described that is comprised of a filter housing in which the media is contained and settled by gravity onto the bottom of the filter housing to form a bed. The filter housing bottom has an outlet port to which is attached a mechanical sieve, such as wedge-wire or slotted pipe. The mechanical sieve slots are smaller than the filter media granules so that as the process liquid flows through the filter, the clean filtrate  
10 exits the outlet port while the filter granules are retained within the filter housing. During normal filter operation, contaminated liquid flows from an inlet port connected to distributor and mechanical sieve and flows through the filter media bed, depositing contaminants on top of, within the interstitial spaces of and the surface of the filter media.

15 When sufficient levels of contaminants are trapped within the filter housing, normal flow to the filter housing is stopped and a cleaning cycle is initiated. The embodiment filter housing has a single radial nozzle, or a plurality of evenly spaced radial nozzles depending on the filter housing diameter, placed just above the bottom of the filter bed. A conduit or pipe runs from a nozzle with a connection on the  
20 outside of the filter housing to the radial nozzle. During the cleaning cycle, a controlled rate of a jetting stream flows through the radial nozzles, up through the filter media, and up towards the inlet port distributor/mechanical sieve. The jetting stream is comprised of a mixture of gas and liquid formed outside of the filter housing and transported to the radial nozzles via the connecting conduit. The radial nozzle is  
25 designed to create an optimum dispersion of the gas and liquid components so that the mixture can simultaneously agitate the filter granules and flush out contaminants from the interstitial spaces of the media.

As the jetting stream, liberated contaminants, and some fluidized filter granules flow towards the inlet port, the mechanical sieve retains the fluidized  
30 granules within the filter housing while allowing the jetting stream and contaminants to exit the filter housing. The embodiment further includes a vent port at the top of

the filter housing to allow trapped gas from the jetting stream to escape prior to returning the filter to normal operation.

The rate of gas and liquid mixed to form the jetting stream and used to agitate  
5 and flush the contaminants from the filter housing should be selected to account for  
the following considerations: (1) adequate nozzle exit velocity to produce a uniform  
gas dispersion within the liquid and substantial coverage of the jetting stream across  
the media bed cross-section, (2) adequate vertical gas velocity to expand the media  
bed in order to break large contaminant agglomerations; (3) adequate gas velocity to  
10 fluidize and agitate the media granules, and (4) adequate liquid momentum to  
mobilize and carry liberated contaminants away from the filter bed.

The number and location of the radial nozzles within the filter housing should  
be selected to account for the following considerations: (1) even distribution of the  
15 jetting stream across the filter bed cross-section and minimizing "blind-spots" or the  
volume of filter media uncontacted by the jetting stream; and (2) close enough to the  
bottom of the media bed so that the nozzle outflow contacts the bottom outlet port  
mechanical sieve to clean the sieve of filter media collected thereon;

20 Although the invention has been summarized as including a method and  
apparatus for removing contaminants from a bed of granular filter media, other uses  
within the scope of the invention may become apparent to those in the filtration art.

## 25 DESCRIPTION OF THE DRAWINGS

FIG. 1 is a vertical sectional view of a non-fixed media housing, which forms  
a part of the present invention, showing internal members used to carry out the medial  
cleaning method herein described..

30

FIG. 2 is horizontal sectional view across the filter housing diameter, which forms part of the present invention, showing one embodiment position of the jetting nozzles in a 45° angle between the filtrate outlet sieve manifold.

5

FIG. 3 is a three-dimensional sectional view of FIG. 2 embodiment as viewed from the underside of the filter housing vessel. This view provides further detail of the embodiment presented in FIG. 2.

10

FIG. 4 is a top cross-sectional view similar to that shown in FIG. 2 but with the radial nozzles located just above and aligned with the outlet sieve manifold members showing an alternate location of the radial nozzles for use in the present invention.

15

FIG. 5 shows a detailed, three-dimensional view of a radial nozzle and its subcomponents. Dashed lines extend from the annular space of the radial nozzle indicating general motion of the jetting stream from the nozzle and the effect the jetting stream has on the fluids surrounding the nozzle.

20

FIG. 6 shows vertical cross-sectional view of an alternate embodiment of the radial nozzle where the nozzle plates are modified to enhance uniformity of jetting stream distribution and reduce media plugging of the nozzle when inactive.

25

FIG. 7 shows three-dimensional, top-side view of a further alternative embodiment of the present invention where the radial nozzles are located underneath the filtrate outlet sieve manifold members in order to provide cleaning of the sieve manifold screen as well as the filter media in the housing during the cleaning method described herein.

30

FIG. 8 shows an alternate embodiment of the present invention where a plurality of filter housings, each incorporating the internal members required to carry

out the cleaning method herein, is incorporated into one horizontal filter housing separated into individual compartments by internal baffles.

### DETAILED DESCRIPTION

5

Referring to FIG. 1, a filter vessel 10 is illustrated for housing a bed 12 of granular filter medium. The filter housing is a pressure-rated vessel having a 2:1 ellipsoidal upper and lower heads. Other filter vessel shapes and designs may be used and will not effect the principle operation of the invention. The granular filter media 10 12 may be any of a number of materials chosen based upon the characteristics of the liquid to be filtered and the properties of the contaminants. For filtration of water containing suspended oil droplets and solids contaminants, granulated black walnut shells are commonly used. A space 14 exists above the filter bed 12 to provide room for the bed to expand during the cleaning cycle. It will be understood, of course, that 15 any suitable filter housing may be utilized for confining the bed of granular filter material.

The filter vessel 10 also includes inlet distributors 20 for the introduction of contaminated liquid from an exterior conduit and dispersing the liquid substantially 20 uniformly across the cross-section of the filter vessel. A backwash outlet header 22 is also installed in the top of the filter vessel for receiving flow of jetting stream and liberated contaminants during the cleaning cycle. The outlet header also contains a mechanical sieve means 23, shown here as slotted pipe or wedge-wire where the open slots are of a diameter less than the smallest media granule size and prevent any 25 mobilized filter media from escaping the vessel during the backwash cycle. Although this figure shows separate process fluid inlet and backwash outlet means, many inlet distributor designs combine both process fluid distribution and backwash extraction. The description of the inlet is exemplary of a preferred embodiment and that other feed inlets may be utilized depending on the characteristics of the liquid to be filtered 30 and the contaminants contained therein.

FIG. 1 also shows an outlet header 30 to which attached are mechanical sieve means 33, shown here as slotted pipe or wedge-wire. After passing through the filter bed, the cleaned filtrate exits the filter vessel through the openings in the sieve. The diameter of the sieve openings is smaller than the smallest filter media granule diameter so that the media is retained inside the vessel during operation.

FIGS. 1 and 2 shows a plurality of radial nozzles 40 having outlets just below the bottom tangent of the mechanical sieves. In the embodiment shown in FIG. 2, the mechanical sieves means 33 is comprised of four wedge-wire screens forming a cross-shaped outlet header. In this configuration, four radial nozzles 40 are placed within the spaces between the four mechanical sieves 33 in the outlet header. Of course, it is to be understood to those skilled in the art that the size and shape of the outlet sieve means and the number of radial nozzles employed will be dependent on the diameter of the filter housing.

The radial nozzles 40 shown in FIGS. 1 and 2 are comprised of two horizontal circular discs spaced-apart to create a void through which the jetting stream flows into the filter media bed during the cleaning cycle. The elevation of the radial nozzle outlet void is shown approximately even with the bottom tangent of the mechanical sieve pipes 33. In many filter vessels, the bottom vessel head is filled with a solid material, such as grout or concrete, up to the bottom of the mechanical sieve pipes. This solid material acts as a support base for the filter media granules during normal filter operations since filter media below the mechanical sieve pipes is essentially of no effective use. Normally, the radial nozzle outlet voids are placed near the bottom tangent of the sieves pipes 33 so that filter media near the base of the tank can be contacted by the jetting stream. The placement of nozzles near the base of the filter media bed also allows the jetting stream to clear the openings of the sieve slots of possible media or contaminant obstructions. For applications where contact with the media near the base or jetting of the sieve is not required or desired, the height of the outlet voids of the radial nozzles may be elevated above the outlet manifold so that the jetting dispersion can penetrate to the full extremities of the vessel without interference from the outlet manifold or sieve screens.

The jetting stream, comprised of a mixture of liquid and gas premixed outside of the filter housing, is carried to the radial nozzle via a conduit 35. This conduit is shown in the drawing as a straight pipe segment connected to a pipe 90° elbow  
5 turning down and connected to the top circular disc of radial nozzle.

For most filter vessel sizes shown in FIG. 2, four radial nozzles placed in the proximate center of each quadrant formed by the cross-shaped outlet manifold and sieve pipes will provide adequate to provide coverage of the jetting stream throughout  
10 the filter bed cross-section. The lateral extent to which the radial nozzles disperse the jetting stream is predominantly set by the rate of water and gas premixed outside of the filter housing by the filter operator. Therefore, the balance between increasing the water/gas flow rate to each radial nozzle or increasing the number of radial nozzles across the vessel cross-section is largely a question of economics. The inventors have  
15 found satisfactory economics by designing each jetting nozzle to clear a region of approximately 1.5 to 3 feet lateral radius from the nozzle centerline. The number of nozzles is increased as needed to substantially cover the cross-section of the filter vessel, while the placement of the nozzles is largely dictated by cross-sectional symmetry.

20

FIG. 2 shows the placement of the plurality of nozzles across the vessel cross-section in relation to a vessel/nozzle centerline radius  $R$ . This vessel nozzle radius  $R$  will vary with filter media type, filter vessel diameter, contaminant loading, and contaminant physical properties. The inventors have found that for water filtration of  
25 oil and solids using black walnut shells, an  $R$  value in the range of 25% to 36% of the vessel diameter  $D$  will provide adequate coverage of the jetting stream for effective media agitation cleaning.

FIG. 4 shows an alternate location of the four nozzles shown as dotted circles  
30 42 rotated 45° from the positions shown in FIG. 2 and located just above the mechanical sieve screens 33. By rotating the radial nozzles in line with the mechanical sieve screens and elevating them just above the top tangent of the circular

size screens, the jetting stream will have the least degree of interference with from the sieve screens. This location may, for example, be more desirable for filter applications where the majority of the contaminants collect in the first few feet of filter media depth and the filter media does not tend to plug the openings of the sieve screens. The benefit of this arrangement is that "blind-spots" are minimized since the vertical movement of the jetting stream is not impeded by contact with the sieve screen members as may occur in other embodiments shown.

Alternatively, as shown in FIG. 7, the radial nozzles may be placed below and aligned with the outlet sieve screens so that the jetting stream comes in direct contact with the sieve screens to flush and clean filter media and contaminants away from the sieve openings. This nozzle orientation may be preferred in some applications where jetting of the sieve screens is required to agitate media around the sieve screens for contaminant removal and to flush away any media that may have become lodged within the sieve screen openings.

FIG. 5 shows a single radial nozzle element contemplated by the inventors for dispersing the jetting stream. The radial nozzle is comprised of a top circular plate 50 and a bottom circular plate 51 into which an opening 52 is placed for connection to a conduit transporting the jetting stream to the nozzle. Each circular plate is of diameter  $D$ . The nozzle plates are spaced apart by a gap  $h$ , which can be of variable dimension based on the size of the vessel, the filter media being cleaned, and the jetting radius desired. The inventors have found satisfactory performance for a nozzle gap  $h$  within the range of 2 mm for small filter systems to 30 mm for large industrial filter applications. In general, the gap diameter  $h$  should be smaller than the smallest sized filter media granule in order to prevent said granules from plugging the gap when the nozzle is not in operation. The diameter  $D$  of the circular plates typically ranges from 100 mm for small filter systems to 400 mm for large industrial filter systems.

30

In further reference to FIG. 5, as the jetting stream flows through the void between the plates and exits the outer boundary of the plates, the jetting stream

pressure suddenly drops to that of the filter vessel. The gas within the liquid portion of the jetting stream forms a continuous high-velocity bubble dispersion extending away from the nozzle shown in FIG. 5 as the dashed straight lines. As this jetting stream moves away from the nozzle and into the filter media, it causes liquid within the area around the nozzle to circulate, shown in FIG. 5 as the curved dashed lines with arrows on the end. By causing circulation of the internal liquid, the amount of liquid added to the jetting stream can be reduced, thereby reducing the overall volume of backwash liquid requiring disposal or reprocessing.

For applications involving high-pressure filter housing, there may be a tendency of filter media to pack into the void space between the plates of the radial nozzle and into the jetting stream conduit. FIG. 6 shows a modified nozzle embodiment that includes a top plate 64 that has diameter slightly larger than the bottom plate 65 to reduce granule packing into the nozzle outlet caused by weight pressure of the media on top of the nozzle. This nozzle also has a tapered plate spacing that is comprised of a narrowing section H1 that is smaller than the outlet height H2. The tapered and non-parallel faces of the top plate 64 and bottom plate 65 also aid in the jetting stream clearing the radial void between the plates when jetting cycle is initiated. The embodiment shown in FIG. 6 also shows a dividing cone 66 that is comprised of a cone extending away from the underside of the bottom plate and into the conduit opening of the top plate. The axial center of the cone is aligned with the axial center of the conduit opening to provide more even distribution of the jetting stream throughout the radial void space between the nozzle plates.

In reference to FIG. 8, an embodiment is presented wherein several filter housings, containing the internal members described herein for carrying out the cleaning method and shown in the previous Figures, are placed inside a singular horizontal vessel 80 and separated by a plurality of dividing baffles 84. Note that for clarification purposes, the component numbers of the embodiment in the figure is shown for one chamber and it is to be understood that each chamber has identical components. Each filter chamber contains a process inlet nozzle 82 and a process outlet nozzle 81. A plurality of piping conduits may be connected to these inlet and

outlet connections so that the process fluid may flow into each chamber in parallel. In such a filter, a large fluid processing volume is allowed without requiring a large number of radial nozzles to be installed to ensure adequate jetting coverage as might be required if the filtration were carried out in a single large filter vessel.

- 5 Alternatively, the piping conduits connecting the chambers may be done so that the fluid to be filtered flows through each chamber in a series manner. Such a flow pattern may be advantageous where each chamber contains a different media type that has a unique affinity for a particular fluid contaminant or particle size. In this type of filter arrangement, the amount of jetting stream required to break-up and mobilize the  
10 contaminants during the cleaning cycle may be varied independently to each chamber to optimize the cleaning cycle.

- In the present invention, the jetting stream flowing to the radial nozzles inside the filter housing is comprised of a pre-mixed stream of a compressed gas and liquid  
15 flowing to each nozzle from a common header. Connected to this common header is a source of a pressurized gas and pressurized liquid. Each of these stream flows into the common distribution header through a control element and metering means such that the filter operator can adjust the rate of gas and liquid flowing to the nozzles. Typical gas sources are compressed air or natural gas. However, any inert gas would  
20 be applicable. For economic reasons, the liquid source typically used by the inventors is the incoming contaminated process fluid.

- The amount of liquid and gas flowing into the common header is largely dependent on the overall size of the filter housing. The inventors have determined that  
25 approximately 9 gpm (gallons per minute) of water per square foot of bed area and 0.7 SCFM (standard cubic feet per minute) of gas per cubic foot of bed provide adequate performance for cleaning black walnut shells filtering oil and solids from produced water. Converting these values to a common volumetric units gives and typical value of 1.7 cubic feet of liquid per square feet of bed area per standard cubic feet of gas per  
30 cubit feet of filter media inside the housing. This ratio will vary to some extent based on the size of the vessel, the number of radial nozzles used, the size and volume of filter media being cleaned, and the physical characteristics of the contaminants.

Therefore, it is understood that part of the operation of this type of filter is adjusting the liquid and gas stream rates to optimize the media cleaning cycle performance while minimizing the amount of contaminated liquid remaining for disposal or recycling.

5

It will be understood that the foregoing description of the invention is merely exemplary, and that various means and modifications may be employed to carry out the intent of the inventors without departing from the scope of the invention.

CLAIMS

We claim:

- 5           1.       A method of filtering contaminants from a liquid stream using a granular filter medium contained within a housing, having an inlet nozzle and an outlet media retention screen, wherein the contaminants are first agglomerated on the surface or interstitial spaces around the filter granules and periodically removing collected contaminants by the steps of:
- 10                       interrupting the flow of contaminated fluid entering the housing,
- establishing a flow of a jetting stream comprised of a mixture of a pressurized gas and liquid such that the jetting stream is substantially evenly dispersed
- 15                   throughout the filter media,
- withdrawing the jetting stream and mobilized contaminants through a screened outlet port inside the housing,
- 20                   ceasing flow of the jetting stream to allow the cleaned media to settle to the bottom of the housing, and
- reestablishing flow of contaminated fluid into the vessel.

25

2. The method of claim 1, wherein the step of establishing a flow of a jetting stream is further comprised of

combining a controlled rate of a liquid with a controlled rate of an agitating gas in a pressurized conduit external to the filter housing,

transporting the jetting stream into the filter housing,

distributing the jetting stream to a plurality of radial nozzles located within the filter media such that the jetting stream is substantially evenly distributed across the filter housing cross-section.

3. The method of claim 2, wherein the radial nozzles are comprised of a circular top plate and a circular bottom plate, spaced apart to create cylindrical void though which the jetting stream flows, with one plate member having a central opening connected to a conduit transporting the jetting stream from a pressurized source.

4. The method of claim 3, wherein the spacing between the top and bottom plates is equal to or between 2 millimeters and 30 millimeters.

5. The method of claim 3 where the top and plates are of equal diameter and between 100 and 400 millimeters in diameter length inclusive.

6. The method of claim 3 where the inside diameter of the central opening conduit is equal to or between 50 and 150 millimeters.

7. The method of claim 3 where the spacing between the top and bottom plates is substantially equal across the radius of the cylindrical void.

8. The method of claim 3 where the spacing between the top and bottom plates increases with radial distance away from the axial center of the plates.

5

9. The method of claim 3 where the top plate member has a diameter slightly larger than the bottom plate member to reduce the tendency of the filter media to lodge within the cylindrical void when the jetting stream is not flowing.

10

10. The method of claim 3 where jetting stream flowing through the conduit opening of one plate member contacts a dividing cone having a circular base connected to the other plate member and a distal point extending away from the surface of the other plate member along the common axis of the plate members for reducing hydraulic pressure loss of the jetting stream through the radial nozzle and distributing the flow of the jetting stream more evenly through the cylindrical void.

15

11. The method of claim 2 where the discharge height of the radial nozzles above the base of the filter housing is equal to or below the mid-point height of the granular filter medium bed.

20

12. The method of claim 2 where rate of water added to the jetting stream is between 8 and 10 gallons per minute per square foot of bed area inclusive.

13. The method of claim 2 where the rate of gas added to the jetting stream is between 0.5 and 0.9 standard cubic feet per cubic foot of filter media inclusive.

25

14. The method of claim 2 where the jetting stream is comprised of a mixture of a gas and a liquid in the ratio equal to or between 1.0 and 2.0 cubic feet of water per minute per foot of bed area per cubic foot of gas per minute per cubic foot of filter media within the housing.

30

15. The method of claim 2, wherein the amount of agitating gas introduced into the radial nozzles produces a centerline jet velocity exiting the nozzle of at least  
5 0.05 meters per second.

16. A deep bed filter comprising:

a housing defining an internal space for containing a liquid to be  
10 filtered;

a bed of granular filter media disposed inside the housing;

an inlet connection and distribution means for receiving a  
15 contaminated liquid and distributing that liquid substantially uniformly across the housing cross section;

an outlet connection and extraction means for means for discharging filtered liquid from the housing while retaining the granular filter media within the  
20 housing;

at least one radial nozzle, or a plurality of evenly spaced radial nozzles, within the housing located near the outlet connection and extraction means, said radial nozzles used for dispersing a controlled mixture of gas and liquid for  
25 purposes of agitating and fluidizing the granular filter media during a regeneration cycle; and

a conduit disposed within the housing for transporting the controlled mixture of gas and liquid to the radial nozzle.

17. A filtering process for removing contaminants suspended in a liquid to be filtered, comprising the steps of:

5

disposing a bed of granular filter media in a tank so as to form a deep bed filter;

10

passing liquid through said bed of granular media to remove said contaminants there from;

collecting filtered liquid passed through said bed and directing the same out of said tank for use;

15

periodically interrupting filtering of said liquid to remove accumulated contaminants from said granular filter media, by a cleaning process comprising the steps of fluidizing and agitating the filter media in said tank using a jetting stream comprised of a controlled mixture of a gas and liquid dispersed substantially evenly throughout the filter media from a plurality of radial nozzles interposed within the filter media;

20

inducing an outflow of liquid and contaminants out of said tank through said separator openings; and

25

venting accumulated jetting gas from the tank space prior to returning to normal filtration;

18. A deep bed filter comprising:

5 a primary external housing containing a plurality of separate chambers where each chamber defines an internal space for containing a bed of granular filter media and receiving a liquid to be filtered;

10 an inlet connection and distribution means in each chamber for receiving a contaminated liquid and distributing that liquid uniformly across the chamber cross-section;

15 an outlet connection and extraction means for means for each chamber for discharging filtered liquid from the chamber while retaining the granular filter media within the chamber;

20 at least one radial nozzle, or a plurality of evenly spaced radial nozzles placed within each chamber for dispersing a controlled mixture of gas and liquid throughout the granular filter media during a regeneration cycle; and

a conduit connected to each radial nozzle and extending outside of the filter housing for receiving and transporting a controlled mixture of gas and liquid for use during a regeneration cycle;

25 19. The filter of claim 18 further comprising a plurality of conduits connected to the inlet and outlet connections of each chamber for allowing the contaminated liquid being filtered to flow through the plurality of chambers within the filter housing either in parallel or in series;

30 20. The filter of claim 19 where the contaminated fluid flows in a series direction through the plurality of chambers and where the average particle size of the granular filter media in each chamber decreases in each subsequent chamber in the direction of flow.