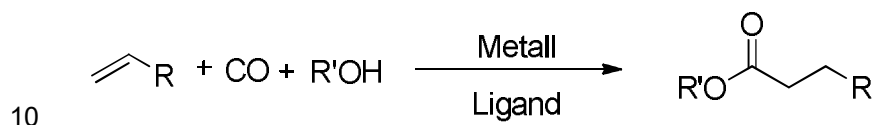


Alkoxy carbonylation of trivinylcyclohexane

The present invention relates to a process for the alkoxy carbonylation of trivinylcyclohexane.

- 5 The alkoxy carbonylation of ethylenically unsaturated compounds is a process of increasing significance. An alkoxy carbonylation is understood to mean the reaction of ethylenically unsaturated compounds such as olefins with carbon monoxide and alcohols in the presence of a metal or a metal complex and a ligand to give the corresponding esters:



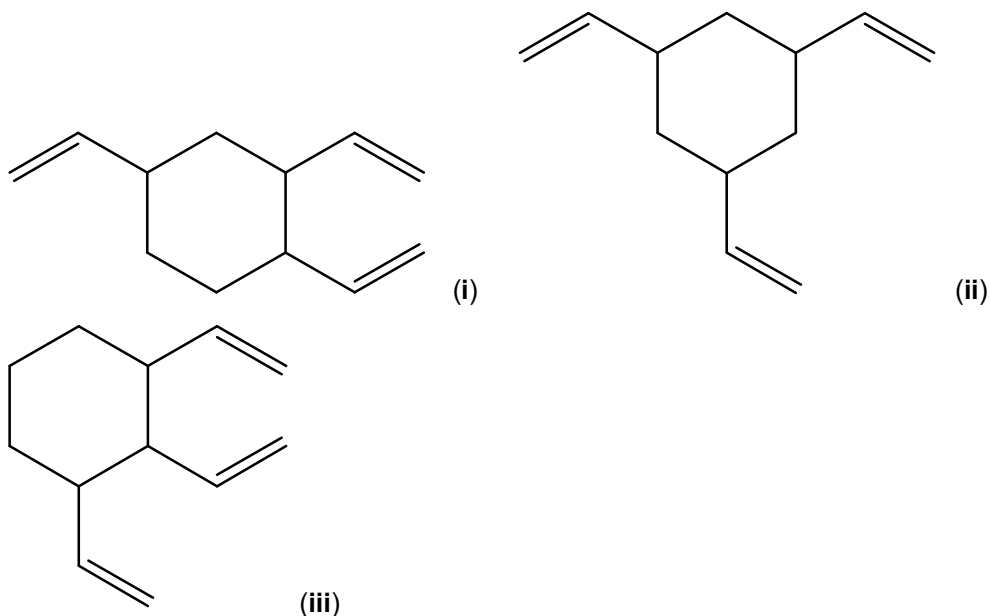
The problem addressed by the present invention was that of providing a process for the alkoxy carbonylation of trivinylcyclohexane. All three vinyl groups can be converted into esters using this process.

- 15 In addition, a rapidly gelling plasticizer for plastics, especially for PVC, is intended to be provided which enables a low processing temperature.

This object is achieved by a process according to Claim 1.

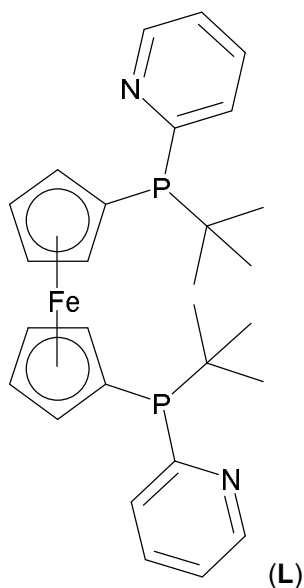
- 20 Process comprising the process steps of:

a) initially charging one of the compounds (i), (ii), (iii) or a mixture of at least two of these compounds:



25

b) adding the ligand (L) and a compound comprising Pd, or adding a complex comprising Pd and the ligand (L):



- c) adding an alcohol having 1 to 12 carbon atoms;
 d) feeding in CO;
 e) heating the reaction mixture of a) to d), wherein the compound/the mixture of a) is converted to a triester.

In one variant of the process, the compound (i) is initially charged in process step a).

In one variant of the process, the compound (ii) is initially charged in process step a).

In one variant of the process, the alcohol in process step c), besides the oxygen, does not comprise any further heteroatoms and contains no multiple bonds.

In one variant of the process, the alcohol in process step c) is selected from:

methanol, ethanol, *n*butanol, methylpropanol, *n*pentanol, *iso*pentanol, 2-methylbutanol, 3-methylbutanol, *n*hexanol, *iso*hexanol, *n*heptanol, *iso*heptanol, *n*octanol, *iso*octanol, 2-ethylhexanol, *n*nonanol, *iso*nonanol, *n*decanol, *iso*decanol, 2-propylheptanol.

In one variant of the process, the alcohol in process step c) is methanol.

In one variant of the process, CO is fed in in process step d) up to a pressure in the range from 20 bar to 60 bar.

In one variant of the process, CO is fed in in process step d) up to a pressure in the range from 30 bar to 50 bar.

In one variant of the process, the heating in process step e) is carried out at a temperature in the range from 90°C to 130°C.

In one variant of the process, the heating in process step e) is carried out at a temperature in the range from 100°C to 120°C.

In one variant of the process, this process comprises the additional process step f):

5 f) purifying the triester.

In one variant of the process, this process comprises the additional process step g):

g) reacting the purified triester with NaOMe and H₂ to give the triol.

10 In one variant of the process, the reaction in process step g) is catalyzed with Ru-MACHO-BH.

In one variant of the process, the reaction in process step g) is carried out at a H₂ pressure in the range of 30 bar to 70 bar.

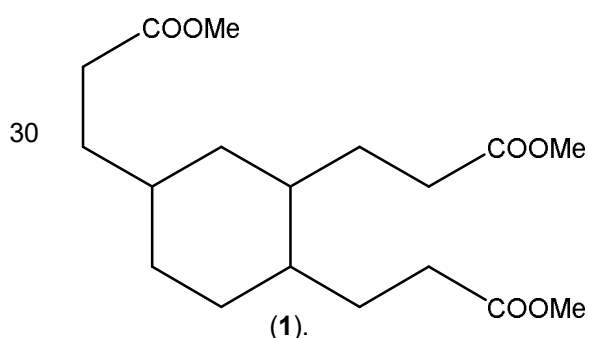
15 In one variant of the process, the reaction in process step g) is carried out at a H₂ pressure in the range of 40 bar to 60 bar.

In one variant of the process, the reaction in process step g) is carried out at a temperature in the range from 80°C to 120°C.

20 In one variant of the process, the reaction in process step g) is carried out at a temperature in the range from 90°C to 110°C.

In addition to the process, a compound is also claimed.

25 Compound according to the formula (1):

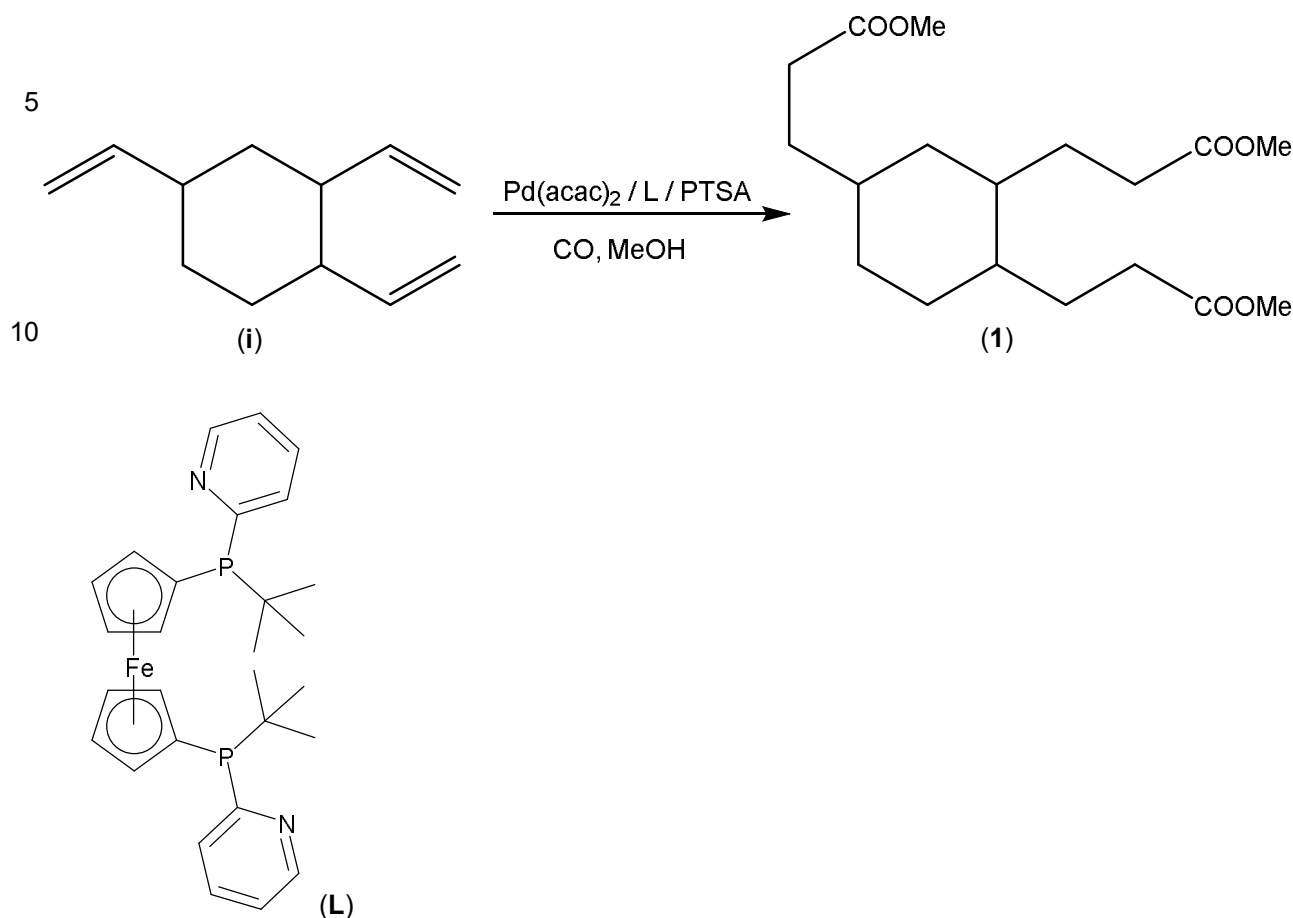


The compound is preferably prepared according to the process described herein.

Compound prepared by the process described above.

The invention is to be illustrated in detail hereinafter by a working example.

Synthesis of trimethyl 3,3',3''-(cyclohexane-1,2,4-triyl)tripropionate (**1**) ("triester")



[$\text{Pd}(\text{acac})_2$] (15.2 mg, 0.1 mol%), **L** (103 mg, 0.4 mol%) and para-toluenesulfonic acid (PTSA, 143 mg, 1.5 mol%) were placed in a 100 ml steel autoclave under an argon atmosphere. Then, MeOH (30 ml) and trivinylcyclohexane (**i**) (8.1 g, 50 mmol) were injected by syringe. The autoclave was flushed three times with CO and then pressurized at a CO pressure of 40 bar. The reaction was carried out at 110°C over 10 h. Subsequently, the autoclave was cooled down to room temperature and decompressed. The desired product was purified by distillation (165°C at 10^{-3} bar) and characterized by ^1H -, ^{13}C -NMR and HR-MS (15.6 g, 91% yield).

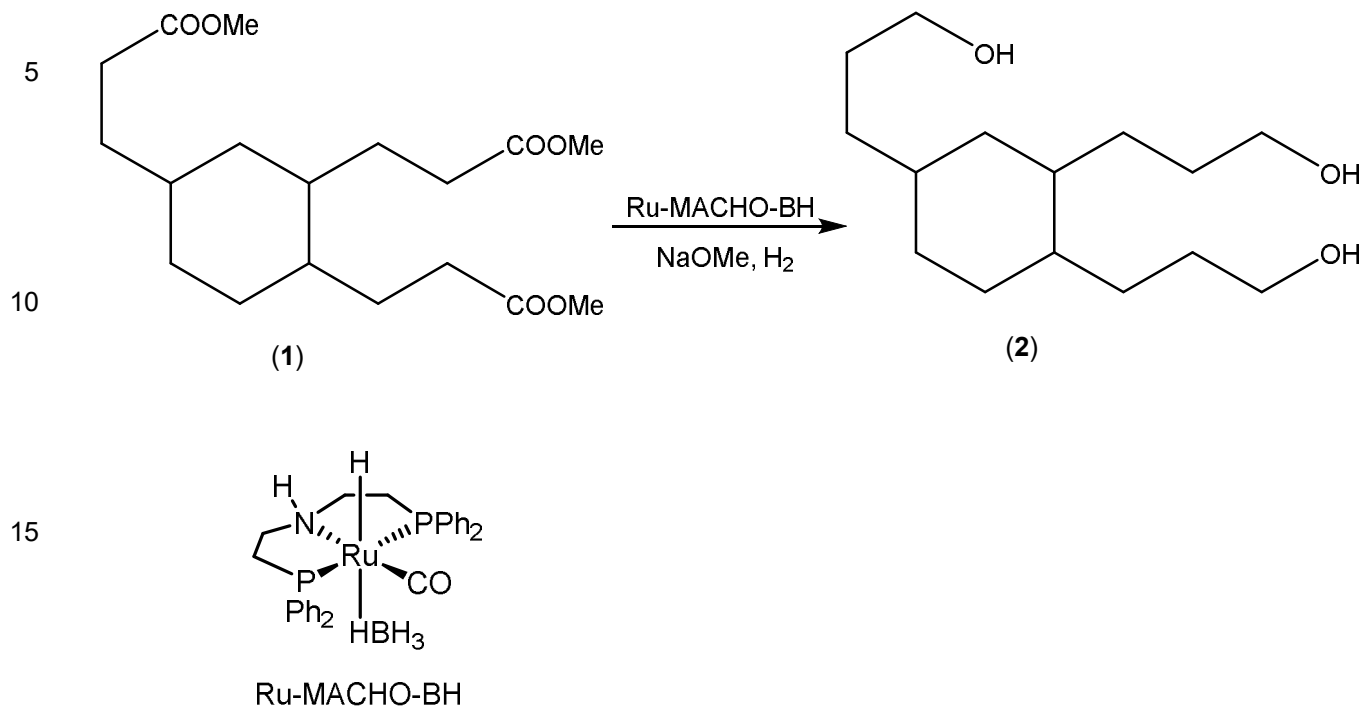
^1H -NMR (300 MHz, C_6D_6) δ = 3.39-3.37 (m, 9H), 2.24-1.86 (m, 7H), 1.48-0.27 (m, 14 H).

^{13}C -NMR (75 MHz, C_6D_6) δ = 173.68-173.54 (m), 51.04, 40.60-40.47 (m), 38.24, 38.14, 37.51, 37.07, 36.54, 36.10, 35.52, 35.14, 33.87, 32.70, 32.55, 32.51, 32.38, 32.29, 32.23, 32.08, 31.97, 31.86, 31.76, 31.68, 31.63, 31.43, 30.98, 30.79, 30.75, 29.31, 28.52, 28.47, 28.34, 28.13, 28.11, 27.13, 26.58, 25.12, 20.79, 19.74.

MS (EI): 311 (13.40), 293 (3.65), 269 (75.76), 237 (60.40), 219 (25.13), 205 (100), 191 (17.62), 177 (14.83), 145 (24.59).

HR-MS (ESI): Calculated $\text{C}_{18}\text{H}_{30}\text{O}_6$ $[\text{M} + \text{H}]^+$: 343.21152, found: 343.21113.

Synthesis of 3,3',3''-(cyclohexane-1,2,4-triyl)tris(propan-1-ol) (2) ("triol")



Ru-MACHO-BH (59 mg, 2 mol%) and NaOMe (27 mg, 10 mol%) were placed in a 25 ml steel autoclave under an argon atmosphere. Then, MeOH (8 ml) and the triester (1) (1.93 g, 5.67 mmol) were injected by syringe. The autoclave was flushed three times with H₂ and then pressurized at a H₂ pressure of 50 bar. The reaction was carried out at 100°C over 10 h. The autoclave was then cooled to room temperature and decompressed. The desired product was purified by filtration over silica gel and characterized by ¹H-, ¹³C-NMR and HR-MS (1.4 g, 96% yield).

¹H-NMR (400 MHz, CD₃OD) δ = 3.32-3.30 (m, 6H), 1.85-1.77 (m, 2H), 1.63-0.62 (m, 19H). ¹³C-NMR (100 MHz, CD₃OD) δ = 63.53-63.29 (m), 42.69, 42.53, 42.39, 42.31, 40.34, 40.24, 39.28, 38.89, 38.12, 38.02, 37.58, 37.27, 35.89, 34.78, 34.72, 34.53, 34.37, 33.17, 31.52, 31.50, 31.40, 31.38, 31.05, 30.60, 30.48, 30.41, 30.32, 30.24, 30.17, 28.77, 28.22, 26.61, 22.53, 21.45. MS (EI): 222 (1.06), 194 (1.14), 181 (2.96), 163 (11.54), 135 (9.81), 121 (17.04), 107 (15.25), 93 (32.69). HR-MS (ESI): Calculated C₁₅H₃₀O₃ [M + H]⁺: 259.22677, found: 259.2269.

Production of plastisols

PVC plastisols were produced, as used, for example, for the manufacture of topcoat films for floor coverings. The figures in the plastisol formulation are each in parts by mass. The formulation of the polymer composition is listed in Table 1.

Table 1: Plastisol formulation

	phr
PVC (Vestolit B 7021 – Ultra; from Vestolit)	100
Plasticizer	50
Epoxidized soybean oil as costabilizer (Drapex 39, from Galata)	3
Thermal stabilizer based on Ca/Zn (Reagent CLX/759/6PF)	2

Figures in phr (phr = parts per hundred parts resin)

5 First the liquid constituents and then the pulverulent constituents are weighed out into a PE beaker. The mixture is stirred manually with an ointment spatula in such a way that no unwetted powder is present any longer. The mixing beaker is then clamped into the clamping device of a dissolver stirrer. After switching on the stirrer, the speed is slowly increased to ca. 2000 rpm. Meanwhile, the plastisol is carefully deaerated, the pressure being kept below 20 mbar.

10 As soon as the plastisol has reached a temperature of ca. 30°C, the speed is lowered to ca. 350 rpm. Henceforth, the plastisol is deaerated for 9 minutes at this speed and a pressure below 20 mbar. This ensured that the plastisol was homogenized with a defined energy input. Thereafter, the plastisol is immediately equilibrated to 25.0°C in a climate-controlled cabinet for further studies.

15 Gelation characteristics of the plastisols

The gelation characteristics of the pastes were examined with a Physica MCR 101 in oscillation mode using a parallel plate analysis system (PP25), which was operated under shear stress control. An additional heating hood was connected to the system in order to achieve a homogeneous heat distribution and uniform sample temperature.

20 The following parameters were set:

Mode: Temperature gradient

Start temperature 25°C

End temperature 180°C

Heating/cooling rate 5°C / min

25 Oscillation frequency 4-0.1 Hz logarithmic ramp

Cycle frequency omega: 10 1/s

Number of measurement points: 63

Measurement point duration: 0.5 min

Automatic gap adjustment F: 0 N

Constant measurement point duration

Gap width 0.5 mm

Analysis procedure:

- 5 The spatula is used to apply a few grams of the paste to be analysed, free from air bubbles, to the lower plate of the analysis system. In doing so, it is ensured that, after the analysis system had been assembled, it is possible for some paste to exude uniformly out of the analysis system (not more than 6 mm in any direction). The heating hood is subsequently positioned over the sample and the analysis is started. The complex viscosity of the paste is determined after 24 h (storage of the paste at 25°C in a
- 10 temperature control cabinet from Memmert) as a function of temperature.

A distinct rise in the complex viscosity is considered to be a measure of gelation. The comparative value used is therefore the temperature on attainment of a paste viscosity of 1000 Pas.

The experiment was repeated with three comparative plastisols in which another plasticizer was used in each case.

- 15 Table 2: Gelling of the plastisols after 24 h, temperature in °C on attainment of a paste viscosity of 10^3 Pa·s:

Experiment	Plasticizer	Gelling temperature [°C]
1*	Trimethyl 3,3',3''-(cyclohexane-1,2,4-triyl)tripropionate (1)	65
2	Diisononyl phthalate (DINP), VESTINOL 9 from Evonik Performance Materials GmbH	83
3	Diisononyl 1,2-cyclohexanedicarboxylate (DINCH), ELATUR CH from Evonik Performance Materials GmbH	101
4	Diisopentyl terephthalate (DPT), ELATUR DPT from Evonik Performance Materials GmbH	70

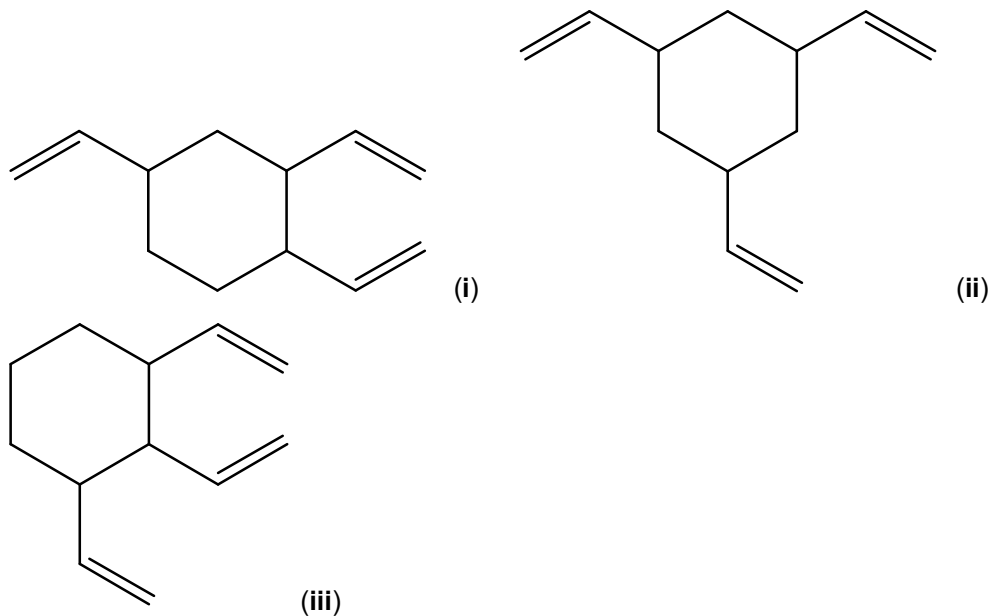
* experiment with inventive compound

- 20 The target value of 1000 Pa*s could already be achieved with the compound (**1**) according to the invention at 65°C. Such low gelling temperatures are advantageous for the processing procedure. They enable plastisol processing at lower temperatures.

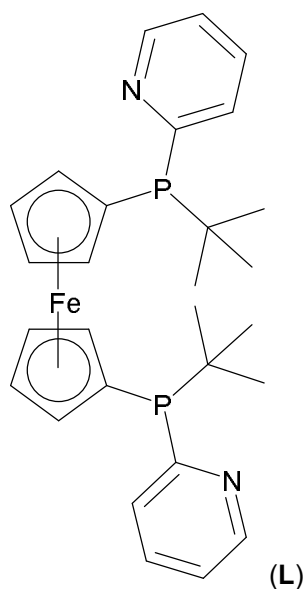
Claims

1. Process comprising the process steps of:

a) initially charging one of the compounds (i), (ii), (iii) or a mixture of at least two of these compounds:



b) adding the ligand (L) and a compound comprising Pd, or adding a complex comprising Pd and the ligand (L):



c) adding an alcohol having 1 to 12 carbon atoms;

d) feeding in CO;

e) heating the reaction mixture of a) to d), wherein the compound/the mixture of a) is converted to a triester.

2. Process according to Claim 1,

wherein the compound (i) is initially charged in process step a).

3. Process according to Claim 1,
wherein the compound (ii) is initially charged in process step a).

5 4. Process according to any of Claims 1 to 3,
wherein the alcohol in process step c), besides the oxygen, does not comprise any further
heteroatoms and contains no multiple bonds.

5. Process according to any of Claims 1 to 4,
10 wherein the alcohol in process step c) is selected from:
methanol, ethanol, *n*butanol, methylpropanol, *n*pentanol, *iso*pentanol, 2-methylbutanol, 3-methylbutanol,
*n*hexanol, *iso*hexanol, *n*heptanol, *iso*heptanol, *n*octanol, *iso*octanol, 2-ethylhexanol, *n*nonanol, *iso*nonanol,
*n*decanol, *iso*decanol, 2-propylheptanol.

15 6. Process according to any of Claims 1 to 5,
wherein the alcohol in process step c) is methanol.

7. Process according to any of Claims 1 to 6,
wherein CO is fed in in process step d) up to a pressure in the range from 20 bar to 60 bar.

20 8. Process according to any of Claims 1 to 7,
wherein the heating in process step e) is carried out at a temperature in the range from 90°C to 130°C.

9. Process according to any of Claims 1 to 8,
25 comprising the additional process step f):
f) purifying the triester.

10. Process according to Claim 9,
comprising the additional process step g):
30 g) reacting the purified triester with NaOMe and H₂ to give the triol.

11. Process according to Claim 10,
wherein the reaction in process step g) is catalyzed with Ru-MACHO-BH.

35 12. Process according to either of Claims 10 and 11,
wherein the reaction in process step g) is carried out at a H₂ pressure in the range of 30 bar to 70 bar.

13. Process according to any of Claims 10 to 12,
40 wherein the reaction in process step g) is carried out at a temperature in the range from 80°C to
120°C.

14. Compound according to the formula (1):

