

POLYOLEFIN POWDER

The present invention relates to polyolefin compositions and processes for polymerising olefins, and more specifically to particulate polyolefins having a defined particle size distribution.

5 In catalytic processes for polymerizing olefinic monomers, it is well known that the properties of the polymer powder which exits the reactor are very important. Polymer powders having a high fines content can cause problems such as accumulation of fines in the recycling units, and during the transfer and packing of the powder and sampling; also risk of accumulation of static electricity in the conveyors and the storage tanks.

10 It is well known to overcome some of these problems by using a catalyst with an appropriate granulometry. For example, WO 05/082962 discloses a process for polymerising olefin in the presence of a Ziegler-Natta catalyst system which is characterised in that the Ziegler-Natta catalyst has a particular particle size distribution. However, the polyethylene powders produced according to this invention still have
15 relatively large particle sizes: 50% have a diameter (D50) of at least 400µm.

WO 05/032714 is concerned with new catalyst systems, which are said to give a low level of fines in the resultant polymer. However the number of large particles in the polymers produced with these catalysts is relatively large, with D50 values in the Examples all greater than 230µm, and most substantially greater.

20 WO 05/021610 of the present applicants is also partly concerned with reducing fines in the polymer, which it achieves by using a pretreatment step in the preparation of the catalyst system. Although low levels of fines are indeed achieved, we have found that the average diameter of the polymer particles produced (not disclosed in this document) was above 230µm.

25 However we have found that high proportions of large polymer particles can also lead to problems, particularly with the final product (such as a pipe or film), which may contain excessive quantities of gels or white spots. In addition to being disfiguring in black and coloured compounds, the white spots may adversely influence the strength of the composition. Gel particles with a size of about 0.01-1 mm can appear as disfiguring
30 heterogeneities in the finished film or extruded pipe. Furthermore, gels and white spots are good proxies for the degree of homogeneity in the final product: even if the gels and white spots are not themselves a problem, the associated inhomogeneity of the product may be

associated with poorer physical properties. This is particularly the case in pipes for example.

Co-pending application EP 1719788A discloses bimodal polyethylene compositions having a relatively narrow particle size distribution. However the proportion of large particles in the polymer powder (as measured by D95) is higher than in the present invention, and the ratio (D90-D10)/D50 is also higher than in the present invention, where D10, D50, D90 and D95 are as defined below.

We have now found that the incidence of gels and white spots can be reduced if not only the width of the particle size distribution but particularly the proportion of large particles in a polyolefin are reduced, despite the content of fines remaining low.

Accordingly, in a first aspect the present invention provides an uncompounded polyolefin powder having a particle size distribution such that D95 is less than 355 μ m and (D90-D10)/D50 is less than 1.2, where D95, D90, D50 and D10 are defined such that 95wt%, 90wt%, 50wt% or 10wt% of the polymer particles have a diameter of less than D95, D90, D50 and D10 respectively.

A further aspect of the invention provides a process for polymerising olefins in a polymerisation reactor, characterised in that the polymer powder recovered from the reactor has a particle size distribution such that D95 is less than 355 μ m and (D90-D10)/D50 is less than 1.2.

The relationship (D90 – D10)/ D50 is usually referred to as the span, and the D values are measured by sieving granulometry. They are expressed in μ m, and may alternatively be defined as follows:

D5 : value under which 5% by weight of the particles are collected;

D10 : value under which 10% by weight of the particles are collected;

D50 : value under which 50% by weight of the particles are collected;

D90 : value under which 90% by weight of the particles are collected.

D95 : value under which 95% by weight of the particles are collected.

Typically the polyolefin is polyethylene or polypropylene, such as that intended for use in pipes and films . Both aspects of the present invention are especially advantageous when the polymer is a multimodal polyethylene, especially one produced in at least two reactors. By “multimodal” in this context is meant a polymer comprising at least two blocks of different molecular weights and/or compositions (ie comonomer content).

In the case of multimodal polyethylenes produced in at least two reactors, it is often found that the largest particles exiting the final polymerisation reactor consist mainly of polymer made in the reactor producing the highest molecular weight fraction (eg this is usually the second block in a bimodal reaction). A problem with particularly large particles is that they may require longer to be fully compounded in an extruder than the residence time of the extruder; thus they exit the extruder as inhomogeneities in the compounded product, which can lead to gels or white spots. The present invention is based on an appreciation of the existence of this problem, and the fact that it can be reduced by taking steps to minimise the proportion of such very large particles.

The invention also has the advantage that despite the reduction in the proportion of very large particles, the fines content - which can be defined as the fraction of particles smaller than 50 μ m (alternatively represented by D5) - is not increased, but remains generally unchanged. Hence D5 is preferably at least 50 μ m, more preferably at least 60 μ m.

A consequent advantage of the present invention is that reducing the number of very large particles in the polymer can permit a reduction in the degree of homogenisation required in the compounding step to reach a specified levels of gels and white spots. The invention is capable of producing a polymer powder that can be pelletised and if blown into a 200 μ m thickness blown film, has a gel count, expressed as the number of gels (larger than 200 μ m) per square metre of film, of less than 500, preferably less than 200, and more preferably less than 100. The gel count is measured by image analysis using a film quality testing system FS-3, available from OCS® GmbH, Film. This low gel count can be achieved after pelletisation with a specific energy of no more than 0.40 kWh/kg, in preferred cases no more than 0.30 kWh/kg, and in particularly preferred cases no more than 0.25 kWh/kg. The residence time in the pelletisation extruder may be no more than 45 seconds, particularly no more than 30 seconds and in some cases less than 20 seconds. By "specific energy" is meant the total specific energy applied to the composition, which is the difference between the sum of all the specific energies applied to the composition at any point in the extruder and any specific cooling energy. Films and pipes can thus be made from such pellets which have good homogeneity despite the relatively low specific energy employed during pelletisation.

We have also found that polymer powder bulk densities of greater than 350 kg/m³, typically 380-450 kg/m³ can be achieved even when the span (D90 - D10)/ D50 of the

polymer is less than 1.2. It has been found that bulk densities are particularly enhanced in polymer produced with a catalyst having a productivity of greater than 4 kgPE/g catalyst, particularly greater than 8 kgPE/g catalyst, and especially greater than 10 kgPE/g catalyst.

It is preferred that the D95 of the polyolefin powder is less than 300 μ m, more preferably less than 250 μ m, and most preferably less than 210 μ m. The span (D90 – D10)/D50 of the polymer is preferably less than 1.0, and more preferably less than 0.9.

The uncompounded polymer powder of the invention may be a multimodal polymer, particularly a bimodal polymer. In such a case, it is preferably made by a process which comprises the steps of introducing ethylene, a polymerisation catalyst and optionally an alpha-olefin containing from 3 to 12 carbon atoms into a first reactor, polymerising the ethylene in said first reactor to form a first polymer, then transferring a mixture comprising said polymer and the catalyst where further polymerisation takes place, optionally in the presence of a further alpha-olefin containing from 3 to 12 carbon atoms, to form a second ethylene polymer, wherein the weight ratio of the two polymers is (30 to 70):(70 to 30). In one embodiment the first polymer is a low molecular weight polymer and the second polymer is a high molecular weight polymer (as determined by GPC). In an alternative embodiment, the first polymer is a high molecular weight polymer and the second polymer is a low molecular weight polymer.

In one embodiment of the invention, the polymer is a multimodal ethylene polymer having a density greater than 940 kg/m³ and a melt flow index MI₅ of 0.05 to 50 g/10min, said ethylene polymer comprising :

from 30 to 70wt%, based on the total weight of the ethylene polymer, of a first polyethylene fraction having a density of at least 950 kg/m³ and a melt flow index MI₂ of at least 10 g/10 min, and

from 70 to 30wt%, based on the total weight of the multimodal ethylene polymer, of a second polyethylene fraction comprising units of ethylene and optionally up to 5mol% of at least one other alpha-olefin containing from 3 to 12 carbon atoms, and a melt flow index MI₂ of less than 10 g/10min.

An alternative polymer is a multimodal ethylene polymer having a density between 900 and 930 kg/m³ and a melt flow index MI₂ of 0.1 to 20 g/10min, said ethylene polymer comprising:

from 30 to 70wt%, based on the total weight of the ethylene polymer, of a first polyethylene fraction having a density of less than 950 kg/m^3 and a melt flow index MI_2 of at least 10 g/10 min, and

from 70 to 30wt%, based on the total weight of the multimodal ethylene polymer, of a second polyethylene fraction comprising units of ethylene, from 0.1 to 20 mol% of an alpha-olefin containing from 3 to 12 carbon atoms, and a melt flow index MI_2 of less than 10 g/10min.

The invention also includes in another aspect pipes and films made from the polyolefin powder defined above.

Regarding the process of the invention, the particle size distribution of the invention can be achieved in a number of ways. One method is to grind the polymer after it exits the polymerisation reactor (or final polymerisation reactor in the case of multi-reactor polymerisations). Mechanical grinding of the powder can be performed in a pulverising system using disc mills, pin mills, turbo mills, knife mills or hammer mills. Alternatively, jet mills or air swept pulverisers may be used. The grinding machine may be equipped with different screening systems so as to achieve the desired powder properties. The grinding can be performed in a continuous process or batchwise. The temperature during the grinding operations is usually ambient temperature or higher, but a cryogenic grinding is also suitable.

An alternative is to select a specific catalyst which has been found to give the desired particle size distribution. The advantage of catalyst systems which provide the desired particle size distribution is that they can be used at high productivity: generally the higher the productivity (as measured in g polymer per g of catalyst) the larger the individual polymer particles formed. Thus the present invention permits the use of catalyst systems having productivity of at least 5000g polyolefin/g of catalyst, and typically at least 10000g polyolefin/g of catalyst.

A preferred catalytic system for use in the process of the present invention comprises :

(a) a catalytic solid comprising magnesium, at least one transition metal selected from the group consisting of titanium and zirconium and halogen, prepared by successively :

- reacting, in a first step (1), at least one magnesium compound (M) chosen from oxygen-containing organic magnesium compounds with at least one compound (T) selected from the group consisting of oxygen-containing organic tetravalent titanium and zirconium compounds, until a liquid complex is obtained;
 - treating, in a second step (2), the complex obtained in step (1) with a halogen-containing aluminic compound of formula AlR_nX_{3-n} , in which R is a hydrocarbon radical comprising up to 20 carbon atoms, X is a halogen and n is less than 3, and
- (b) an organometallic compound of a metal chosen from lithium, magnesium, zinc, aluminium or tin.

The preparation of the solid catalytic complex comprises the step (2), the main function of which is to reduce the valency of the transition metal and simultaneously additionally halogenate, if necessary, the magnesium compound and/or the transition metal compound: thus most of the alkoxy groups still present in the magnesium compound and/or in the transition metal compound are substituted by halogens, such that the liquid complex obtained after step (1) is transformed in a catalytically active solid. The reduction and possible further halogenation are performed simultaneously using the halogen-containing aluminic compound which thus acts as a reductive halogenating agent.

The treatment using the halogen-containing aluminic compound in step (2) of the preparation of the catalytic solid may be carried out by any suitable known means, and preferably by gradually adding the halogen-containing organoaluminium compound to the liquid complex obtained in step (1).

The treatment using the halogen-containing aluminic compound in step (2) may be carried out either in one step or in two successive steps as disclosed in EP-A-0703248. The temperature at which step (2) is performed should not exceed 40°C, temperatures of no more than 35°C being the most advantageous. The preferred temperature range is 25-40°C, with the most preferable range being 30-35°C.

The process of the invention is usually a suspension polymerisation process, typically using as diluent a C3-C8 hydrocarbon, and most commonly a C3-C6 hydrocarbon such as butane or hexane. The process may be performed in one or more reactors, and may utilise a single site catalyst, dual site catalyst or multisite catalyst.

EXAMPLES

The Examples which follow are intended to illustrate the invention. The meaning of the symbols used in these examples, the units expressing the mentioned properties and the methods of measuring these properties are explained herebelow.

Span : this is a measure of the particle size distribution, defined by the relationship $(D_{90} - D_{10})/D_{50}$ wherein the meanings of the respective D, measured by laser granulometry and expressed in μm are :

D10 : value under which 10 % by weight of the particles are collected;

D50 : value under which 50 % by weight of the particles are collected;

D90 : value under which 90 % by weight of the particles are collected.

The density of the polyethylene was measured according to ISO 1183-1. MI_2 and MI_5 were measured using the procedures of ISO 1133 at 190°C using loads of 2 kg and 5 kg respectively.

The sieving operations were performed with a set of 12 calibrated sieves (45, 63, 90, 125, 180, 250, 355, 500, 710, 1000, 1400 and 2000 μm) according to ASTM D-1921 particle (sieve analysis) of Plastic Materials, Method A.

The bulk densities of the polymers were measured according to the principle set forth in ASTM standard D-1895, method A (1979) and ISO 60 (1977) by using the following procedure: the polymer powder is poured into a cylindrical container with a capacity of 50ml, taking care not to pack it down, from a hopper whose lower edge is arranged 20mm above the upper edge of the container. The container filled with powder is then weighed, the tare is deducted from the read weight and the result obtained (expressed in g) is divided by 50 in order to obtain the polymer bulk density expressed in kg/litre.

The gels were quantified by image analysis (Film quality testing system FS-3, available from OCS® GmbH, Film) performed on 200 microns thickness blown film. The gels count is expressed as the number of gels (larger than 200 μm) per square metre of film.

The white spots quotation was determined by microscopy in accordance with ISO 18553. Image analyses were performed with the assistance of NOESIS-Visilog® software.

EXAMPLE 1 (according to the invention)

A. Catalyst preparation

In a 50 L stainless steel agitated autoclave, 6.7 moles of magnesium diethoxide were reacted with 13.4 moles of titanium tetrabutoxide for 4 hours at 150°C. The reaction product thus obtained was subsequently diluted by 10 L of hexane, and 37.2 moles of ethylaluminium dichloride (EADC) were added at 30°C. The addition was performed in 4 hours. Subsequently, the slurry reaction mixture was heated up to 60°C, then kept at this temperature for 45 min. The resulting brown solid was decanted and washed with several fractions of hexane so as to remove at least 75 % of the reaction by-products present in the supernatant solution. The solid thus collected from the suspension comprised (% by weight): Ti: 17; Cl: 36; Al: 2; Mg: 4.

B. Polymerisation

The manufacture of a composition according to the invention was carried out in suspension in hexane in two loop reactors of volume 200L and 300L respectively, connected in series and separated by a device making it possible to continuously carry out a reduction in pressure.

Hexane, ethylene, hydrogen, triethylaluminium (30-50ppm) and the above catalyst were continuously introduced into the first loop reactor and the polymerization of ethylene was carried out in this mixture in order to form the homopolymer (A). The said mixture, additionally comprising the homopolymer (A), was continuously withdrawn from the said first reactor and was subjected to a reduction in pressure (~60°C, 0.06 MPa), so as to remove at least a portion of the hydrogen. The resulting mixture, at least partially degassed of hydrogen, was then continuously introduced into a second polymerization reactor, at the same time as ethylene, butene, hexane and hydrogen, and the copolymerization of ethylene and butene was carried out therein in order to form the ethylene/1-butene copolymer (B). The suspension comprising the ethylene polymer composition was continuously withdrawn from the second reactor and this suspension was subjected to a final reduction in pressure and to steam stripping, so as to evaporate the reactants and the solvent. The composition was recovered in the form of a powder, which was subjected to further drying in a fluid bed dryer.

The detailed polymerisation conditions are specified in Table 1. The particle size distribution is determined by sieving technique, and the powder morphology is characterized by a median diameter D50 of 115 µm (Table 2 and Chart 1).

C. Compounding

To 100 parts of the polyethylene composition, 0.3 parts of antioxidant Irganox® B225, 0.1 parts of calcium stearate and 2.25 parts of carbon black were added. The resulting composition was extruded on a twin-screw extruder (commercial Werner® ZSK 40 extruder, comprising a twin-screw of 40 mm diameter, 1040 mm length) and a strand pelletiser, in the conditions specified in Table 3. The pellets of the resulting compounds were recovered and examined.

EXAMPLE 2 (comparative)

A. Catalyst preparation

In a 50 L stainless steel agitated autoclave, 6.7 moles of magnesium diethoxide were reacted with 13.4 moles of titanium tetrabutoxide for 4 hours at 150°C. The reaction product thus obtained was subsequently diluted by 19 L of hexane, and 37.2 moles of ethylaluminium dichloride (EADC) were added at 45°C. The addition was performed in 2 hours. Subsequently, the slurry reaction mixture was heated up to 60°C, then kept at this temperature for 45 min. The resulting brown solid was decanted and washed with several fractions of hexane so as to remove at least 75 % of the reaction by-products present in the supernatant solution. The solid thus collected from the suspension comprised (% by weight): Ti: 17; Cl: 38; Al: 2; Mg: 4.

B. Polymerisation

The composition was prepared in the same procedure as described in example 1.B, but with using catalyst of example 2.A. The detailed of the polymerisation conditions are given in Table 1. The particle size distribution was determined by sieving technique, and the powder morphology was characterized by a median diameter D50 of 202 µm (Table 2 and Chart 1).

C. Compounding

Compounding was carried out as in Example 1, but under different compounding conditions. These conditions are described in Table 3. The pellets of the resulting compounds were collected and examined.

EXAMPLE 3 (according to the invention)

The manufacture of a composition according to the invention was carried out in suspension in isobutane in two loop reactors of volume 200L and 300L respectively, connected in series and separated by a device making it possible to continuously carry out a reduction in pressure.

5 Isobutane, ethylene, hydrogen, triethylaluminium (30-50ppm) and the catalyst prepared in Example 2-A were continuously introduced into the first loop reactor and the polymerisation of ethylene was carried out in this mixture in order to form the homopolymer (A). The mixture, additionally comprising the homopolymer (A), was continuously withdrawn from the said first reactor and was subjected to a reduction in
10 pressure (~50°C, 0.6 MPa), so as to remove at least a portion of the hydrogen. The resulting mixture, at least partially degassed of hydrogen, was then continuously introduced into a second polymerisation reactor, at the same time as ethylene, hexene, isobutane and hydrogen, and the copolymerisation of ethylene and hexene was carried out therein in order to form the ethylene/1-hexene copolymer (B). The suspension comprising
15 the composition comprising ethylene polymers was continuously withdrawn from the second reactor and this suspension was subjected to a final reduction in pressure, so as to flash the isobutane and the reactants present (ethylene, hexene and hydrogen) and to recover the composition in the form of a dry powder, which was subsequently degassed to pursue the removal of residual hydrocarbons. The other polymerisation conditions are
20 specified in Table 1.

200 g of the resulting powder were introduced continuously in a grinder Retsch ZM1 provided with a sieving grid calibrated at 0.20 mm. The stirring speed of the mixer was set to 10000 rpm. The internal part of the mixer was checked after the grinding operation to ensure that the entire sample went through the calibrated grid. The powder
25 particle size distribution after grinding was analysed by sieving technique and the results are summarised in Table 2 and Figure 1.

The resulting ground powder was mixed with 2.25 % wt of carbon black and Irganox® B215 antioxydant, and then extruded under different conditions on a lab-scale DSM Research 15 mL Micro-Compounder. The extrudate of the resulting compounds was
30 recovered and examined by microscopy.

EXAMPLE 4 (comparative)

The powder obtained before grinding in Example 3 was mixed with 2.25 % wt of carbon black and Irganox® B215 antioxidant, and then extruded under different conditions on a lab-scale DSM Research 15 mL Micro-Compounder. The pelletised extrudate was recovered and examined by microscopy.

5 EXAMPLE 5 (according to the invention)

The manufacture of a composition according to the invention was carried out in suspension in isobutane in two loop reactors of volume 200L and 300L respectively, connected in series and separated by a device making it possible to continuously carry out a reduction in pressure.

10 Isobutane, ethylene, hydrogen, triethylaluminium (30-50ppm) and the catalyst prepared in Example 1-A were continuously introduced into the first loop reactor and the polymerisation of ethylene was carried out in this mixture in order to form the homopolymer (A). The mixture, additionally comprising the homopolymer (A), was continuously withdrawn from the said first reactor and was subjected to a reduction in
15 pressure (~50°C, 0.6 MPa), so as to remove at least a portion of the hydrogen. The resulting mixture, at least partially degassed of hydrogen, was then continuously introduced into a second polymerisation reactor, at the same time as ethylene, hexene, isobutane and hydrogen, and the copolymerisation of ethylene and hexene was carried out therein in order to form the ethylene/1-hexene copolymer (B). The suspension comprising
20 the composition comprising ethylene polymers was continuously withdrawn from the second reactor and this suspension was subjected to a final reduction in pressure, so as to flash the isobutane and the reactants present (ethylene, hexene and hydrogen) and to recover the composition in the form of a dry powder, which was subsequently degassed to pursue the removal of residual hydrocarbons. The other polymerisation conditions are
25 specified in Table 1.

As for Examples 1 and 2, different compounding conditions were applied. These conditions are described in Table 3. The pellets of the resulting compounds were collected and examined.

Table 2 shows the D95 and span $(D90-D10)/D50$ values for the resins made in Examples 1-5. It can be seen that the Examples of the invention have a much lower values than the comparative Examples. This is also shown graphically in Figure 1, which shows the full particle size distributions of the four resins. Examples 1, 3 and 5 show that the
5 particle size distribution of the invention can be obtained in more than one way.

Tables 3 and 4 show how the above particle size distributions affect the appearance of gels and white spots in the compounded resins. Table 3 compares Example 1 and 5 with comparative Example 2: it can be seen that the levels of gels and white spots are lower in Example 1 and 5. Figure 2 plots the gel count against the specific energy of extrusion for
10 Examples 1, 2 and 5. This shows that the gel count for Examples 1 and 5 is low regardless of the specific energy: however, for comparative Example 2 the gel count is always significantly higher – at least double that of Example 1 and 5, and especially so at low specific energies.

Table 4 shows that the white spots quotation for comparative Example 4 is higher
15 than that for Example 3 under equivalent compounding conditions.

TABLE 1

EXAMPLE	1	2	3	5
Diluent	Hexane	Hexane	Isobutane	Isobutane
<u>Reactor 1</u>				
C ₂ (g/kg)	12.9	12	18.1	15.2
H ₂ /C ₂ (mole/mole)	0.38	0.37	0.50	0.507
T (°C)	85	85	90	90
Residence time (h)	1.79	1.79	1.52	1.62
Polymer A fraction (% wt)	50.5	50.4	49.1	50.1
<u>Reactor 2</u>				
C ₂ (g/kg)	13.2	9.8	19.4	29
Comonomer nature	Butene	Butene	Hexene	Hexene
Comonomer/C ₂ (mole/mole)	0.587	0.547	2.039	2.532
H ₂ /C ₂ (mole/mole)	0.0043	0.0036	0.0050	0.0029
T (°C)	75	75	75	80
Residence time (h)	1.64	1.64	1.43	1.44
Polymer MI ₅ (g/10 min)	0.31	0.29	0.30	0.32
Polymer density (kg/m ³)	949.4	947.7	948.8	948.5
Productivity (kg PE/g catalyst)	13.9	15.5	15.8	23.0

TABLE 2

EXAMPLE	1	2 (comparative)	3	4 (comparative)	5
D5, μm	66	75	57	68	75
D10, μm	75	90	67	82	91
D50, μm	115	202	95	220	130
D90, μm	170	495	145	690	180
D95, μm	200	608	162	840	222
Span: (D90-D10)/D50	0.83	2.00	0.82	2.76	0.68
% wt > 250 μm	1.9	38.8	0	43.4	2.0
% wt > 355 μm	1.2	23.6	0	30.4	0.7
Bulk density (kg/m ³)	420	430	390	380	406

TABLE 3

Example	Extruder rate (kg/h)	Screw speed (rpm)	Specific energy (kWh/kg)	Gels (m²)	White spots quotation
1	30	265	0.349	88	3.2
	30	300	0.369	69	3.3
	30	333	0.391	129	3
	65	333	0.270	75	5.4
	50	265	0.284	46	5.3
	50	300	0.300	49	4.3
	50	333	0.317	46	4.6
	60	265	0.255	131	4.8
	60	300	0.272	59	5.3
	60	333	0.287	97	4.8
2 (comp)	30	333	0.397	476	4.2
	30	300	0.370	614	4.5
	30	265	0.356	681	3.8
	70	333	0.266	2236	8.8
	50	265	0.275	1441	6.3
	50	300	0.288	823	7.4
	50	333	0.311	778	5.4
	60	265	0.254	1627	9.1
	60	300	0.267	1638	7.3
	60	333	0.284	1107	7.8
5	30	333	0.430	30	3.1
	30	300	0.401	26	2.8
	30	265	0.376	47	3.3
	50	333	0.321	90	3.8
	50	300	0.307	125	3.8
	50	265	0.289	40	3.1
	55	333	0.306	35	4.2
	55	300	0.292	85	4.3
	55	265	0.273	90	3.9
	60	333	0.295	80	4.3
	60	300	0.279	80	4.6

TABLE 4

EXAMPLE	Screw speed (rpm)	Residence time (s)	White spots quotation
3	50	120	5.9
	100	60	5.1
4 (comparative)	50	120	7.6
	100	60	7.7

CLAIMS

1. Uncompounded polyolefin powder having a particle size distribution such that D95 is less than 355 μ m and (D90-D10)/D50 is less than 1.2, where D95, D90, D50 and D10 are defined such that 95wt%, 90wt%, 50wt% or 10wtl% of the polymer particles have a diameter of less than D95, D90, D50 and D10 respectively.
2. Uncompounded polyolefin powder according to claim 1, which is polyethylene or polypropylene.
3. Uncompounded polyolefin powder according to claim 1 or 2, having a D95 of less than 300 μ m, preferably less than 250 μ m, and more preferably less than 210 μ m.
4. Uncompounded polyolefin powder according to any preceding claim, having a span (D90 – D10)/ D50 of less than 1.0, preferably less than 0.9.
5. Uncompounded polyolefin powder according to any preceding claim, having a D5 of at least 50 μ m, preferably at least 60 μ m.
6. Uncompounded polyolefin powder according to any preceding claim, which is a multimodal polyethylene.
7. Uncompounded polyolefin powder according to claim 6, which is a multimodal ethylene polymer having a density greater than 940 kg/m³ and a melt flow index MI₅ of 0.05 to 50 g/10min, said ethylene polymer comprising- from 30 to 70wt%, based on the total weight of the ethylene polymer, of a first polyethylene fraction having a density of at least 950 kg/m³ and a melt flow index MI₂ of at least 10 g/10 min, and from 70 to 30wt%, based on the total weight of the multimodal ethylene polymer, of a second polyethylene fraction comprising units of ethylene and optionally up to 5mol% of at least one other alpha-olefin containing from 3 to 12 carbon atoms, and a melt flow index MI₂ of less than 10 g/10min.

8. Uncompounded polyolefin powder according to claim 6, which is a multimodal ethylene polymer having a density between 900 and 930 kg/m³ and a melt flow index MI₂ of 0.1 to 20 g/10min, said ethylene polymer comprising:
- 5 from 30 to 70wt%, based on the total weight of the ethylene polymer, of a first polyethylene fraction having a density of less than 950 kg/m³ and a melt flow index MI₂ of at least 10 g/10 min, and
- 10 from 70 to 30wt%, based on the total weight of the multimodal ethylene polymer, of a second polyethylene fraction comprising units of ethylene, from 0.1 to 20 mol% of an alpha-olefin containing from 3 to 12 carbon atoms, and a melt flow index MI₂ of less than 10 g/10min.
9. Uncompounded polymer powder according to any preceding claim, which has a bulk density (according to ASTM D-1895, method A) of greater than 350 kg/m³, preferably greater than 380 kg/m³, most preferably between 400 and 460 kg/m³.
- 15 10. Uncompounded polymer powder according to any preceding claim, which when compounded and blown into a 200µm thickness film has a gel count, expressed as the number of gels larger than 200µm per square metre of film, of less than 500, preferably less than 200, and more preferably less than 100.
- 20 11. Blown film made from a polymer powder as defined in any preceding claim, which for a 200µm thickness film has a gel count, expressed as the number of gels larger than 200µm per square metre of film, of less than 500, preferably less than 200, and more preferably less than 100.
- 25 12. Pipe made from a polymer powder as defined in any of claims 1 to 10 which has been compounded.
- 30 13. Process for producing an uncompounded polyolefin powder as defined in any of claims 1 to 10, comprising the steps of performing a polymerisation reaction, and then grinding the polymer powder exiting the polymerisation reactor.

14. Process for producing an uncompounded polyethylene powder as defined in any of claims 2 to 10, comprising the steps of introducing ethylene, a polymerisation catalyst and optionally an alpha-olefin containing from 3 to 12 carbon atoms into a first reactor, polymerising the ethylene in said first reactor to form a first polymer, then transferring a mixture comprising said polymer and the catalyst where further polymerisation takes place, optionally in the presence of a further alpha-olefin containing from 3 to 12 carbon atoms, to form a second ethylene polymer, wherein the weight ratio of the two polymers is (30 to 70):(70 to 30).
15. Process according to claim 14, wherein the first polymer is a low molecular weight polymer and the second polymer is a high molecular weight polymer (as determined by GPC), or the first polymer is a high molecular weight polymer and the second polymer is a low molecular weight polymer (as determined by GPC).
16. Process for producing an uncompounded polyethylene powder as defined in any of claims 2 to 10, or a process according to any one of claims 14 to 15, comprising performing a polymerisation reaction using a catalyst system comprising :
- (a) a catalytic solid which comprises magnesium, at least one transition metal selected from the group consisting of titanium and zirconium, and a halogen, prepared by successively :
- reacting, in a first step (1), at least one magnesium compound (M) chosen from oxygen-containing organic magnesium compounds with at least one compound (T) selected from the group consisting of oxygen-containing organic tetravalent titanium and zirconium compounds, until a liquid complex is obtained;
 - treating, in a second step (2) at a temperature of from 25 to 40°C, the complex obtained in step (1) with a halogen-containing aluminic compound of formula AlR_nX_{3-n} , in which R is a hydrocarbon radical comprising up to 20 carbon atoms, X is a halogen and n is less than 3, and
- (b) an organometallic compound of a metal chosen from lithium, magnesium, zinc, aluminium or tin.

17. Process according to any one of claims 13 to 16, wherein the polymerisation process is performed using a catalytic system which has a productivity of at least 5000g polyolefin/g of catalyst, preferably at least 10000g polyolefin/g of catalyst.
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18. Process for making a film or a pipe, comprising performing a process as defined in any of claims 13 to 16 to make an uncompounded polyethylene powder, compounding the powder to form pellets, and then forming the pellets into a film or pipe, wherein the compounding to form pellets utilises a specific energy of no more than 0.40 kWh/kg, preferably no more than 0.30 kWh/kg, and more preferably no more than 0.25 kWh/kg, and additionally or alternatively the residence time in the pelletisation extruder is no more than 45 seconds, preferably no more than 30 seconds and more preferably less than 20 seconds.
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