

ETHYLENIC POLYMER AND ITS USE

CROSS-REFERENCE TO RELATED APPLICATIONS

[0001] This application claims priority from U.S. provisional patent application serial number 61/222,379, filed July 1, 2009, the disclosure of which is incorporated herein by reference for purposes of U.S. practice.

5 BACKGROUND OF THE INVENTION

[0002] Metallocene-catalyzed polymers have been commercial for several years, and are used in many end-use applications, such as packaging, personal hygiene, automotive, flooring, adhesives, fibers, nonwovens, films, sheets, and fabrics. The metallocene-catalyzed polymers have certain advantages, such as narrow
10 molecular weight distributions. Some of the metallocene-catalyzed polymers are homogeneous polymers that have long chain branching which enhances their processability. However, metallocene-catalyzed polymers are still subject to degradation under ultraviolet light and have cross-linking characteristics that make their use in certain applications more challenging. Further, those metallocene-
15 catalyzed polymers which have relatively high levels of long chain branching typically exhibit poor hot tack strength and/or a narrow sealing window, which renders them less useful in certain film applications.

[0003] Known metallocene-catalyzed polymers include both (a) the homogeneous-branched, substantially linear ethylene polymers ("SLEP") which are
20 prepared using constrained geometry catalysts ("CGC Catalyst"), such as disclosed in USP 5,272,236 and USP 5,278,272, and WO93/08221, as well as the homogeneous linear ethylene polymers ("LEP") which are prepared using other metallocene (called "bis-CP catalysts"). Various grades of SLEPs, having a variety of densities and melt flow rates, are commercially available from The Dow Chemical Company as
25 ENGAGE™ polyolefin elastomers or AFFINITY™ plastomers. Various grades of LEPs are commercially available from ExxonMobil Chemical Company as EXACT™ or EXCEED™ polymers.

[0004] A characteristic of metallocene-catalyzed polymers is that they have a significant level (typically in excess of 300 wppm) of residual unsaturation, with that
30 unsaturation being in various combinations and amounts of one or more of the following unsaturated groups:

Vinyl, vinylidene, vinylene, vinyl-3, and tri-substituted vinyls.

[0005] Such residual unsaturations, and particularly the vinyl-3 groups, are believed to contribute to long-term polymer degradation, as well as to difficulties in controlling either or both of desired cross-linking in some applications or undesired cross-linking (such as the formation of gels) in other end-use applications (such as films).

[0006] Further, for film applications, it is desirable to have a broad thermal bonding window (temperature range) as well as relatively low hot tack initiation temperature.

BRIEF SUMMARY

[0007] In one aspect, there is provided an ethylenic polymer comprising an overall polymer density of not more than 0.905 g/cm³; total unsaturation of not more than 125 per 100,000 carbons; and a GI200 gel rating of not more than 15; up to 3 long chain branches/1000 carbons; vinyl-3 content of less than 5 per 100,000 carbons; and a total number of vinyl groups/1000 carbons of less than the quantity (8000/M_n), wherein the vinyl-3 content and vinyl group measurements are measured by gel permeation chromatography (145°C) and ¹H-NMR (125°C).

[0008] The ethylenic polymer preferably comprises a ratio of vinyl groups to total olefin groups according to the formula:

$$VG/TOG > (\text{comonomer mole percentage}/0.1)^a \times 10^a \times 0.8$$

where a = -0.24, VG = vinyl groups, and TOG = total olefin groups.

[0009] In another aspect, there is provided an ethylenic polymer comprising total unsaturation of from about 10 to about 125 per 100,000 carbons total unsaturation; and up to 3 long chain branches/1000 carbons; and a GI200 gel rating of not more than 15.

[00010] The ethylenic polymer can also comprise a vinyls amount and a total unsaturation amount, wherein the ratio of vinyls amount:total unsaturation amount is at least 0.2:1, preferably at least 0.3:1, more preferably at least from about 0.4:1 to about 0.8:1; and the ethylenic polymer can have less than 5 per 100,000 carbons of vinyl-3 content. The ethylenic polymer can also have less than 5 per 100,000 carbons of vinyl-3 content.

[00011] In another aspect, there is provided a composition comprising, or made from, at least one ethylenic polymer as defined above, wherein at least a portion of the ethylenic polymer has been cross-linked.

[00011a] In another aspect, there is provided a composition comprising, or made from, at least one ethylenic polymer as defined above, wherein at least a portion of the ethylenic polymer has been functionalized.

[00012] In another aspect, there is provided a composition comprising, or made from, at least one ethylenic polymer as defined above and at least one other natural or synthetic polymer. The natural or synthetic polymer may be preferably selected from the group consisting of at least one thermoplastic, at least one elastomeric olefin polymer and at least one styrenic block copolymer, are also contemplated. In another aspect, there is provided a composition comprising, or made from, at least one ethylenic polymer as defined above and at least one other component selected from the group consisting of a tackifier, a wax, and an oil.

[00013] In another aspect, there is provided a composition comprising a dispersion or emulsion of particles in a fluid, wherein the particles comprise, or are made from, at least one ethylenic polymer as defined above.

[00014] In another aspect, there is provided an ethylenic polymer comprising an overall polymer density of not more than 0.9 g/cm^3 ; total unsaturation of not more than 125 per 100,000 carbons; a GI200 gel rating of not more than 15; vinyl-3 content of less than 5 per 100,000 carbons; and a vinyls amount and a total unsaturation amount, wherein the ratio of vinyls amount:total unsaturation amount is between 0.4:1 and 0.8:1.

[00015] In another aspect, there is provided a fabricated article in which at least one layer or portion of the fabricated article comprises, or is made from, at least one ethylenic polymer as defined above and in which the fabricated article comprises a film, a sheet, a fiber, a nonwoven, a laminate, or a composite.

DETAILED DESCRIPTION OF THE INVENTION

Definitions

[00016] “Composition,” as used, includes a mixture of materials which comprise the composition, as well as reaction products and decomposition products formed from the materials of the composition.

“Blend” or “polymer blend,” as used, mean an intimate physical mixture (that is, without reaction) of two or more polymers. A blend may or may not be miscible (not phase separated at molecular level). A blend may or may not be phase separated. A blend may or may not contain one or more domain configurations, as determined from transmission electron spectroscopy, light scattering, x-ray scattering, and other

methods known in the art. The blend may be effected by physically mixing the two or more polymers on the macro level (for example, melt blending resins or compounding) or the micro level (for example, simultaneous forming within the same reactor).

5 “Linear,” as used, refers to polymers where the polymer backbone of the polymer lacks measurable or demonstrable long chain branches, for example, the polymer is substituted with an average of less than 0.01 long branch per 1000 carbons.

 “Polymer” refers to a polymeric composition prepared by polymerizing monomers, whether of the same or a different type. The generic term “polymer” thus
10 embraces the term “homopolymer,” usually employed to refer to polymers prepared from only one type of monomer, and the term “interpolymer” as defined. The terms “ethylene/ α -olefin polymer” is indicative of interpolymers as described.

 “Interpolymer,” as used, refers to polymers prepared by the polymerization of at least two different types of monomers. The generic term interpolymer includes
15 copolymers (usually employed to refer to polymers prepared from two different monomers) and polymers prepared from more than two different types of monomers.

 “Ethylenic polymer” refers to a polymer that contains more than 50 mole percent polymerized ethylene monomer (based on the total amount of polymerizable monomers) and, optionally, may contain one or more comonomers.

20 The term “ethylene/ α -olefin interpolymer” refers to an interpolymer that contains more than 50 mole percent polymerized ethylene monomer (based on the total amount of polymerizable monomers) and at least one α -olefin.

Test Methods and Measurements

25 [00017] *Density:* The density of a polymer (g/cm^3) is measured according to ASTM-D 792-03, Method B, in isopropanol. Specimens are measured within 1 hour of molding after conditioning in the isopropanol bath at 23°C for 8 min to achieve thermal equilibrium prior to measurement. The specimens are compression molded according to ASTM D-4703-00 Annex A with a 5 min initial heating period at about
30 190°C and a 15°C/min cooling rate per Procedure C. The specimen is cooled to 45°C in the press with continued cooling until “cool to the touch.”

 [00018] *Melt Indices and Melt Index Ratio:* The melt index (I_2) of a polymer is measured in accordance with ASTM D 1238, Condition 190 °C/2.16 kg, and is reported in grams eluted per 10 minutes, and the melt index (I_{10}) is measured in

accordance with ASTM D 1238, Condition 190 °C/10 kg, and is reported in grams eluted per 10 minutes. The melt index ratio (I_{10}/I_2) is a ratio of these two melt indices.

[00019] **Differential Scanning Calorimetry:** Differential Scanning Calorimetry (DSC) can be used to measure the melting and crystallization behavior of a polymer over a wide range of temperature. For example, the TA Instruments Q1000 DSC, equipped with an RCS (refrigerated cooling system) and an autosampler is used to perform this analysis. During testing, a nitrogen purge gas flow of 50 ml/min is used. Each sample is melt pressed into a thin film at about 175 °C; the melted sample is then air-cooled to room temperature (~25 °C). A 3-10 mg, 6 mm diameter specimen is extracted from the cooled polymer, weighed, placed in a light aluminum pan (ca 50 mg), and crimped shut. Analysis is then performed to determine its thermal properties. The thermal behavior of the sample is determined by ramping the sample temperature up and down to create a heat flow versus temperature profile. First, the sample is rapidly heated to 180 °C and held isothermal for 3 minutes in order to remove its thermal history. Next, the sample is cooled to -40 °C at a 10 °C/minute cooling rate and held isothermal at -40 °C for 3 minutes. The sample is then heated to 150 °C (this is the “second heat” ramp) at a 10 °C/minute heating rate. The cooling and second heating curves are recorded. The cool curve is analyzed by setting baseline endpoints from the beginning of crystallization to -20 °C. The heat curve is analyzed by setting baseline endpoints from -20 °C to the end of melt. The values determined are peak melting temperature (T_m), peak crystallization temperature (T_c), heat of fusion (H_f) (in Joules per gram), and the calculated % crystallinity for polyethylene samples using:

$$\% \text{ Crystallinity} = ((H_f)/(292 \text{ J/g})) \times 100.$$

The heat of fusion (H_f) and the peak melting temperature are reported from the second heat curve. Peak crystallization temperature is determined from the cooling curve.

[00020] **Molecular Weight Measurements by Gel Permeation Chromatography (GPC):** The GPC system consists of a Waters (Milford, MA) 150C high temperature chromatograph (other suitable high temperatures GPC instruments include Polymer Laboratories (Shropshire, UK) Model 210 and Model 220) equipped with an on-board differential refractometer (RI). Additional detectors can include an IR4 infra-red detector from Polymer ChAR (Valencia, Spain), Precision Detectors (Amherst, MA) 2-angle laser light scattering detector Model 2040, and a Viscotek (Houston, TX) 150R 4-capillary solution viscometer. A GPC

with the last two independent detectors and at least one of the first detectors is sometimes referred to as “3D-GPC”, while the term “GPC” alone generally refers to conventional GPC. Depending on the sample, either the 15-degree angle or the 90-degree angle of the light scattering detector is used for calculation purposes. Data collection is performed using Viscotek TriSEC software, Version 3, and a 4-channel Viscotek Data Manager DM400. The system is also equipped with an on-line solvent degassing device from Polymer Laboratories (Shropshire, UK). Suitable high temperature GPC columns can be used such as four 30 cm long Shodex HT803 13 micron columns or four 30 cm Polymer Labs columns of 20-micron mixed-pore-size packing (MixA LS, Polymer Labs). The sample carousel compartment is operated at 140 °C and the column compartment is operated at 150 °C. The samples are prepared at a concentration of 0.1 grams of polymer in 50 milliliters of solvent. The chromatographic solvent and the sample preparation solvent contain 200 ppm of butylated hydroxytoluene (BHT). Both solvents are sparged with nitrogen. The polyethylene samples are gently stirred at 160 °C for four hours. The injection volume is 200 microliters. The flow rate through the GPC is set at 1 ml/minute.

[00021] The GPC column set is calibrated before running the polymer by running twenty-one narrow molecular weight distribution polystyrene standards. The molecular weight (MW) of the standards ranges from 580 to 8,400,000 grams per mole, and the standards are contained in 6 “cocktail” mixtures. Each standard mixture has at least a decade of separation between individual molecular weights. The standard mixtures are purchased from Polymer Laboratories (Shropshire, UK). The polystyrene standards are prepared at 0.025 g in 50 mL of solvent for molecular weights equal to or greater than 1,000,000 grams per mole and 0.05 g in 50 ml of solvent for molecular weights less than 1,000,000 grams per mole. The polystyrene standards were dissolved at 80 °C with gentle agitation for 30 minutes. The narrow standards mixtures are run first and in order of decreasing highest molecular weight component to minimize degradation. The polystyrene standard peak molecular weights are converted to polyethylene M_w using the Mark-Houwink K and a (sometimes referred to as α) values mentioned later for polystyrene and polyethylene.

[00022] With 3D-GPC absolute weight average molecular weight (“ $M_{w, Abs}$ ”) and intrinsic viscosity are also obtained independently from suitable narrow polyethylene standards using the same conditions mentioned previously. These

narrow linear polyethylene standards may be obtained from Polymer Laboratories (Shropshire, UK; Part No.'s PL2650-0101 and PL2650-0102).

[00023] The systematic approach for the determination of multi-detector offsets is performed in a manner consistent with that published by Balke, Mourey, et al. (Mourey and Balke, *Chromatography Polym.*, Chapter 12, (1992)) (Balke, Thitiratsakul, Lew, Cheung, Mourey, *Chromatography Polym.*, Chapter 13, (1992)), optimizing triple detector log (M_w and intrinsic viscosity) results from Dow 1683 broad polystyrene (American Polymer Standards Corp.; Mentor, OH) or its equivalent to the narrow standard column calibration results from the narrow polystyrene standards calibration curve. The molecular weight data, accounting for detector volume off-set determination, are obtained in a manner consistent with that published by Zimm (Zimm, B.H., *J. Chem. Phys.*, 16, 1099 (1948)) and Kratochvil (Kratochvil, P., *Classical Light Scattering from Polymer Solutions*, Elsevier, Oxford, NY (1987)). The overall injected concentration used in the determination of the molecular weight is obtained from the mass detector area and the mass detector constant derived from a suitable linear polyethylene homopolymer, or one of the polyethylene standards. The calculated molecular weights are obtained using a light scattering constant derived from one or more of the polyethylene standards mentioned and a refractive index concentration coefficient, dn/dc , of 0.104. Generally, the mass detector response and the light scattering constant should be determined from a linear standard with a molecular weight in excess of about 50,000 daltons. The viscometer calibration can be accomplished using the methods described by the manufacturer or alternatively by using the published values of suitable linear standards such as Standard Reference Materials (SRM) 1475a, 1482a, 1483, or 1484a. The chromatographic concentrations are assumed low enough to eliminate addressing 2nd viral coefficient effects (concentration effects on molecular weight).

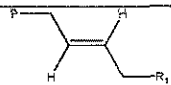
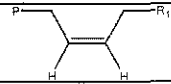
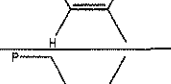
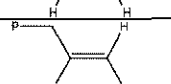
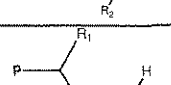
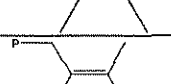
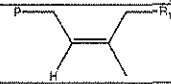
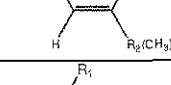
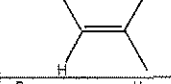
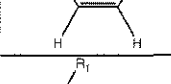
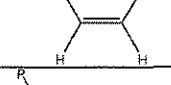
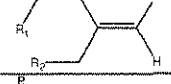
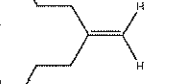
[00024] **C^{13} NMR Comonomer Content:** It is well known to use NMR spectroscopic methods for determining polymer composition. ASTM D 5017-96, J. C. Randall et al., in "NMR and Macromolecules" ACS Symposium series 247, J. C. Randall, Ed., Am. Chem. Soc., Washington, D.C., 1984, Ch. 9, and J. C. Randall in "Polymer Sequence Determination", Academic Press, New York (1977) provide general methods of polymer analysis by NMR spectroscopy. Polymer samples for ^{13}C NMR analysis were prepared as 6 wt% solutions. The solvent was a 5/95 (wt/wt) mixture of paradichlorobenzene- d_4 and orthodichlorobenzene with 0.025 M

chromium actetylacetonate added as the relaxation agent. Typically, 0.2 g of polymer was dissolved in 2.5 g of the solvent mixture in a 10 mm NMR tube. After N₂ purge, the NMR tube was capped and heated in a heating block set at 150 °C to dissolve the polymer. Samples were vortexed during heating to facilitate sample homogenization. Once the sample/solvent achieved the appearance of a single phase and flowed consistently, the sample tube was left in the heating block for more than 24 hours for homogenization purpose.

[00025] A Varian Inova 400 MHz system was used to take ¹³C NMR spectra. The following parameters were used: temperature at 400K, 25,000 Hz spectral width, 1.3 second acquisition time, 90 degree pulse, 6 seconds relaxation delay, 8000 scans, and inverse gated decoupling with Waltz modulation. The free induction decay (FID) files were processed using NUTS. The spectrum was apodized with a cosine function. It was then zero filled once and Fourier Transformed. The spectrum was phased and baseline corrected manually. A pre-defined integral range was applied to generate a list of integrals in the chemical shift ranges specified in XH. Qiu, O.D. Redwine, G. Gobbi, A. Nuamthanom, P.L. Rinaldi, *Macromolecules*, **40**, 6879 (2007). The “linear least-squares analysis with the constraint” (in M.R. Seger, G.E. Maciel, *Anal. Chem.*, **76**, 5734 (2004)) was used to analyze the integral list for composition and triad distribution.

[00026] **Residual Unsaturations determined by ¹H Nuclear Magnetic Resonance (NMR):** Samples for ¹H NMR experiments were prepared by dissolving polymers in a solvent mixture, tetrachloroethane-d₂/perchloroethylene (50/50 v/v), in standard NMR tubes. The tubes were then heated in a heating block set at 115 °C until polymers are completely dissolved. The ¹H NMR spectra were taken on a Varian Inova 600 MHz spectrometer using a broadband inverse probe. For each sample, two experiments were performed. The first is a standard single pulse ¹H NMR experiment to quantify the polymer peak relative to the solvent peak. The second is a presaturated ¹H NMR experiment to suppress the polymer backbone peak (~1.4ppm). The end groups were then quantified by referencing to the same solvent peak. The following acquisition parameters were used: 5*T₁ relaxation delay, 90 degree pulse of 8 μs, 2 s acquisition time, 0.5 second presaturation time with satpwr = 1, 128-256 scans. The spectra are centered at 4 ppm with a spectral width of 10000 Hz. All measurements were taken without sample spinning at 110 ± 1 °C. The ¹H

NMR spectra were referenced to 5.99 ppm for the resonance peak of the solvent (residual protonated tetrachloroethane).

Group	Structure	Notation	δ (ppm)	J (± 0.5 Hz)
Vinylene		Vy1- <i>trans</i>	5.49	Triplet (3.8)
		Vy1- <i>cis</i>	5.44	Triplet (4.4)
		Vy2- <i>trans</i>	~5.52	multiplet
		Vy2- <i>cis</i>	~5.49	multiplet
		Vy3	5.43 5.26	Dual-triplet (15.0, 7.0) Dual-doublet (15.3, 7.8)
Trisubstituted unsaturation		T1- <i>trans</i>	5.28	Quartet (6.4)
		T2- <i>cis</i>	5.23	Triplet (6.5)
		T2- <i>trans</i>	5.22	Triplet (6.5)
		T3 T4 T5	5.23 5.20 5.18	Triplet (6.2) Triplet (~6) Triplet (?)
		T6	4.95	
				
Vinyl		V1	5.90 5.07 5.01	Dual-dual-triplet Doublet (17.1) Doublet (10.3)
		V2	5.67 ~5.03	
Vinylidene		Vd1	4.86 4.81	Singlet Singlet
		Vd2	4.83 4.76	Singlet Singlet
		Vd3	4.80	Singlet

Gel rating of the polymers

Gels

- 5 **[00027]** Method/Description of GI200 test
- Extruder: Model OCS ME 20 available from OCS Optical Control Systems GmbH
Wullener Feld 36, 58454 Witten, Germany or equivalent.

	Parameter	Standard Screw
10	L/D	25/1
	Coating	Chrome
	Compression ratio	3/1
	Feed Zone	10D
	Transition Zone	3D
15	Metering Zone	12D
	Mixing Zone	---

- 20 Cast Film Die: ribbon die, 150 x 0.5 mm, available from OCS Optical Control Systems GmbH, or equivalent.

- Air Knife: OCS air knife to pin the film on the chill roll, available from OCS Optical Control Systems GmbH, or equivalent.

- 25 Cast Film Chill Rolls and Winding Unit: OCS Model CR-8, available from OCS Optical Control Systems GmbH, or equivalent.

Profile Number		070	071	072
MELT INDEX	dg/min	0.1-1.2	1.2-3.2	3.2-32
Density	g/cm ³	ALL	ALL	ALL
Throat	°C	25 ± 3	25 ± 3	25 ± 3
Zone 1	°C	180 ± 5	160 ± 5	140 ± 5
Zone 2	°C	240 ± 5	190 ± 5	170 ± 5
Zone 3	°C	260 ± 5	200 ± 5	175 ± 5
Zone 4	°C	260 ± 5	210 ± 5	175 ± 5
Adapter	°C	260 ± 5	225 ± 5	180 ± 5
Die	°C	260 ± 5	225 ± 5	180 ± 5
Screw Type		Standard	Standard	Standard
Screw Speed	RPM	70 ± 2	70 ± 2	70 ± 2
Air Knife Flow	Nm ³ /h	6 ± 2	6 ± 2	6 ± 2
Die to Chill Roll	mm	6 ± 1	6 ± 1	6 ± 1
Die to Air Knife	mm	6 ± 1	6 ± 1	6 ± 1
Chill Speed	m/min.	3 ± 1	3 ± 1	3 ± 1

Chill Temp.	°C	20 ± 2	20 ± 2	20 ± 2
Tension Speed	m/min.	6 ± 2	6 ± 2	6 ± 2
Winder Torque	N	8 ± 1	8 ± 1	8 ± 1
Lab Temperature	°C	23 ± 2	23 ± 2	23 ± 2
Lab Humidity	%	<70	<70	<70
Width	mm	108 ± 18	108 ± 18	108 ± 18
Thickness	µm	76 ± 5	76 ± 5	76 ± 5

5 Gel Counter: OCS FS-3 line gel counter consisting of a lighting unit, a CCD detector and an image processor with the Gel counter software version 3.65e 1991-1999, available from OCS Optical Control Systems GmbH, or equivalent. The OCS FS-5 gel counter is equivalent.

[00028] Instantaneous GI200

10 *Note: GI stands for "gel index". GI200 includes all gels ≥ 200 µm in diameter.*

The instantaneous GI200 is the sum of the area of all the size classes in one analysis cycle:

$$15 \quad X_j = \sum_{k=1}^4 A_{T,j,k}$$

where:

X_j = instantaneous GI200 (mm²/24.6 cm³) for analysis cycle j

20 4 = total number of size clauses

GI200

GI200 is defined as the trailing average of the last twenty instantaneous GI200 values:

$$25 \quad \langle X \rangle = \frac{\sum_{j=1}^{20} X_j}{20}$$

where:

$$\langle X \rangle = \text{GI200}(\text{mm}^2/24.6\text{cm}^3)$$

30 One analysis cycle inspects 24.6 cm³ of film. The corresponding area is 0.324m² for a film thickness of 76 µm and 0.647 m² for a film thickness of 38 µm.

[00029] Gel Content Measurement: When the ethylene interpolymers, either alone or contained in a composition is at least partially crosslinked, the degree of crosslinking may be measured by dissolving the composition in a solvent for specified

duration, and calculating the percent gel or unextractable component. The percent gel normally increases with increasing crosslinking levels.

[00030] **Long chain branching per 1000 carbons:** The presence of long chain branching can be determined in ethylene homopolymers by using ¹³C nuclear magnetic resonance (NMR) spectroscopy and is quantified using the method described by Randall (Rev. *Macromol. Chem. Phys.*, C29, V. 2&3, 285-297). There are other known techniques useful for determining the presence of long chain branches in ethylene polymers, including ethylene/1-octene interpolymers. Two such exemplary methods are gel permeation chromatography coupled with a low angle laser light scattering detector (GPC-LALLS) and gel permeation chromatography coupled with a differential viscometer detector (GPC-DV). The use of these techniques for long chain branch detection and the underlying theories have been well documented in the literature. See, for example, Zimm, G. H. and Stockmayer, W. H., *J. Chem. Phys.*, 17, 1301 (1949), and Rudin, A., *Modern Methods of Polymer Characterization*, John Wiley & Sons, New York (1991) 103-112.

[00031] **Ethylenic polymers of this Invention:** The ethylenic polymers of this invention are relatively high molecular weight, relatively low density polymers that have a unique combination of (A) a relatively low total amount of unsaturation, and (B) a relatively high ratio of vinyl groups to total unsaturated groups in the polymer chain, as compared to known metallocene-catalyzed ethylenic polymers. This combination is believed to result in lower gels for end-use applications (such as films) where low gels are important, better long-term polymer stability and, for end-use applications requiring cross-linking, better control of that cross-linking, in each case while maintaining a good balance of other performance properties.

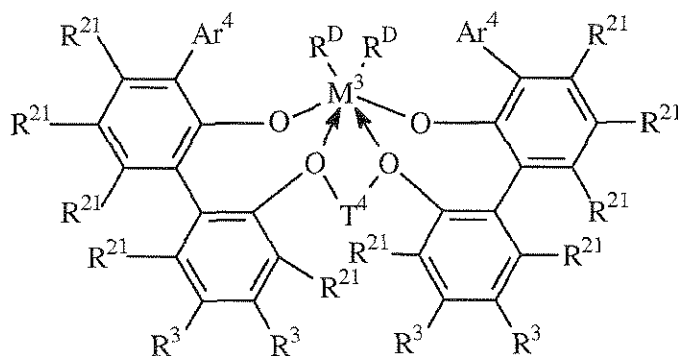
[00032] The novel polymers of this invention are interpolymers of ethylene with at least 0.1 mole percent of one or more comonomers, preferably at least one α -olefin comonomer. The α -olefin comonomer(s) may have, for example, from 3 to 20 carbon atoms. Preferably, the α -olefin comonomer may have 3 to 8 carbon atoms. Exemplary α -olefin comonomers include, but are not limited to, propylene, 1-butene, 3-methyl-1-butene, 1-pentene, 3-methyl-1-pentene, 4-methyl-1-pentene, 1-hexene, 1-heptene, 4,4-dimethyl-1-pentene, 3-ethyl-1-pentene, 1-octene, 1-nonene, 1-decene, 1-dodecene, 1-tetradecene, 1-hexadecene, 1-octadecene and 1-eicosene.

Preparation of an Ethylenic Polymer of this Invention

[00033] For producing the ethylenic polymers of this invention, a solution-phase polymerization process may be used. Typically, such a process occurs in a well-stirred reactor such as a loop reactor or a sphere reactor at temperature from about 150 to about 300 °C, preferably from about 160 to about 180 °C, and at pressures from about 30 to about 1000 psi, preferably from about 30 to about 750 psi. The residence time in such a process is typically from about 2 to about 20 minutes, preferably from about 10 to about 20 minutes. Ethylene, solvent, catalyst, and one or more comonomers are fed continuously to the reactor. Exemplary solvents include, but are not limited to, isoparaffins. For example, such solvents are commercially available under the name ISOPAR E from ExxonMobil Chemical Co., Houston, Texas. The resultant mixture of ethylene-based polymer and solvent is then removed from the reactor and the polymer is isolated. Solvent is typically recovered via a solvent recovery unit, that is, heat exchangers and vapor liquid separator drum, and is recycled back into the polymerization system.

[00034] Suitable catalysts for use in preparing the novel polymers of this invention include any compound or combination of compounds that is adapted for preparing such polymers in the particular type of polymerization process, such as solution-polymerization, slurry-polymerization or gas-phase-polymerization processes.

[00035] In one embodiment, an ethylenic polymer of this invention is prepared in a solution-polymerization process using a polymerization catalyst that is a metal complex of a polyvalent aryloxyether corresponding to the formula:



where M^3 is Ti, Hf or Zr, preferably Zr;

[00036] Ar^4 independently each occurrence is a substituted C_{9-20} aryl group, wherein the substituents, independently each occurrence, are selected from the group consisting of alkyl; cycloalkyl; and aryl groups; and halo-, trihydrocarbylsilyl- and halohydrocarbyl-

substituted derivatives thereof, with the proviso that at least one substituent lacks co-planarity with the aryl group to which it is attached;

T^4 independently each occurrence is a C_{2-20} alkylene, cycloalkylene or cycloalkenylene group, or an inertly substituted derivative thereof;

5 R^{21} independently each occurrence is hydrogen, halo, hydrocarbyl, trihydrocarbysilyl, trihydrocarbysilylhydrocarbyl, alkoxy or di(hydrocarbyl)amino group of up to 50 atoms not counting hydrogen;

R^3 independently each occurrence is hydrogen, halo, hydrocarbyl, trihydrocarbysilyl, trihydrocarbysilylhydrocarbyl, alkoxy or amino of up to 50 atoms not counting hydrogen, or
10 two R^3 groups on the same arylene ring together or an R^3 and an R^{21} group on the same or different arylene ring together form a divalent ligand group attached to the arylene group in two positions or join two different arylene rings together; and

R^D , independently each occurrence is halo or a hydrocarbyl or trihydrocarbysilyl group of up to 20 atoms not counting hydrogen, or 2 R^D groups
15 together are a hydrocarbylene, hydrocarbadiyl, diene, or poly(hydrocarbyl)silylene group.

[00037] Such polyvalent aryloxyether metal complexes and their synthesis are described in WO 2007/136496 or WO 2007/136497, using the synthesis procedures disclosed in US-A-2004/0010103. Among the preferred polyvalent aryloxyether
20 metal complexes are those disclosed as example 1 in WO 2007/136496 and as example A10 in WO 2007/136497. Suitable cocatalysts and polymerization conditions for use of the preferred polyvalent aryloxyether metal complexes are also disclosed in WO 2007/136496 or WO 2007/136497.

[00038] The metal complex polymerization catalyst may be activated to form
25 an active catalyst composition by combination with one or more cocatalysts, preferably a cation forming cocatalyst, a strong Lewis acid, or a combination thereof. Suitable cocatalysts for use include polymeric or oligomeric aluminoxanes, especially methyl aluminoxane, as well as inert, compatible, noncoordinating, ion forming compounds. So-called modified methyl aluminoxane (MMAO) or triethyl aluminum
30 (TEA) is also suitable for use as a cocatalyst. One technique for preparing such modified aluminoxane is disclosed in U.S. Patent No. 5,041,584 (Crapo et al.). Aluminoxanes can also be made as disclosed in U.S. Patent Nos. 5,542,199 (Lai et al.); 4,544,762 (Kaminsky et al.); 5,015,749 (Schmidt et al.); and 5,041,585 (Deavenport et al.).

[00039] *Polymeric Blends or Compounds of this invention:* Various natural or synthetic polymers, and/or other components, may be blended or compounded with the novel polymers of this invention to form the polymeric compositions of this invention. Suitable polymers for blending with the embodiment ethylenic polymer include thermoplastic and non-thermoplastic polymers including natural and synthetic polymers. Suitable synthetic polymers include both ethylene-based polymers, such as high pressure, free-radical low density polyethylene (LDPE), and ethylene-based polymers prepared with Ziegler-Natta catalysts, including high density polyethylene (HDPE) and heterogeneous linear low density polyethylene (LLDPE), ultra low density polyethylene (ULDPE), and very low density polyethylene (VLDPE), as well as multiple-reactor ethylenic polymers ("in reactor" blends of Ziegler-Natta PE and metallocene PE, such as products disclosed in U.S. Patent Nos. 6,545,088 (Kolthammer et al.); 6,538,070 (Cardwell et al.); 6,566,446 (Parikh et al.); 5,844,045 (Kolthammer et al.); 5,869,575 (Kolthammer et al.); and 6,448,341 (Kolthammer et al.)). Commercial examples of linear ethylene-based polymers include ATTANE™ Ultra Low Density Linear Polyethylene Copolymer, DOWLEX™ Polyethylene Resins, and FLEXOMER™ Very Low Density Polyethylene, all available from The Dow Chemical Company. Other suitable synthetic polymers include polypropylene, (both impact modifying polypropylene, isotactic polypropylene, atactic polypropylene, and random ethylene/propylene copolymers), ethylene/diene interpolymers, ethylene-vinyl acetate (EVA), ethylene/vinyl alcohol copolymers, polystyrene, impact modified polystyrene, ABS, styrene/butadiene block copolymers and hydrogenated derivatives thereof (SBS and SEBS), and thermoplastic polyurethanes. Homogeneous olefin-based polymers such as ethylene-based or propylene-based plastomers or elastomers can also be useful as components in blends or compounds made with the ethylenic polymers of this invention. Commercial examples of homogeneous metallocene-catalyzed, ethylene-based plastomers or elastomers include AFFINITY™ polyolefin plastomers and ENGAGE™ polyolefin elastomers, both available from The Dow Chemical Company, and commercial examples of homogeneous propylene-based plastomers and elastomers include VERSIFY™ performance polymers, available from The Dow Chemical Company, and VISTAMAX™ polymers available from ExxonMobil Chemical Company.

[00040] The polymeric compositions of this invention include compositions comprising, or made from, the ethylenic polymer of this invention in combination

(such as blends or compounds, including reaction products) with one or more other components, which other components may include, but are not limited to, natural or synthetic materials, polymers, additives, reinforcing agents, ignition resistant additives, fillers, waxes, tackifiers, antioxidants, stabilizers, colorants, extenders, crosslinkers, blowing agents, and/or plasticizers. Such polymeric compositions may include thermoplastic polyolefins (TPO), thermoplastic elastomers (TPE), thermoplastic vulcanizates (TPV) and/or styrenic/ethylenic polymer blends. TPEs and TPVs may be prepared by blending or compounding one or more ethylenic polymers of this invention (including functionalized derivatives thereof) with an optional elastomer (including conventional block copolymers, especially an SBS or SEBS block copolymer, or EPDM, or a natural rubber) and optionally a crosslinking or vulcanizing agent. A TPO polymeric composition of this invention would be prepared by blending or compounding one or more of the ethylenic polymers of this invention with one or more polyolefins (such as polypropylene). A TPE polymeric composition of this invention would be prepared by blending or compounding one or more of the ethylenic polymers of this invention with one or more elastomers (such as a styrenic block copolymer or an olefin block copolymer, such as disclosed in U.S. Patent No. 7,355,089 (Chang et al.)). A TPV polymeric composition of this invention would be prepared by blending or compounding one or more of the ethylenic polymers of this invention with one or more other polymers and a vulcanizing agent. The foregoing polymeric compositions may be used in forming a molded object, and optionally crosslinking the resulting molded article. A similar procedure using different components has been previously disclosed in U.S. Patent No. 6,797,779 (Ajbani, et al.).

25 **[00041] Processing Aids:** In certain aspects of the invention, processing aids, such as plasticizers, can also be included in the polymeric composition. These aids include, but are not limited to, the phthalates (such as dioctyl phthalate and diisobutyl phthalate), natural oils (such as lanolin, and paraffin, naphthenic and aromatic oils obtained from petroleum refining), and liquid resins from rosin or petroleum feedstocks. Exemplary classes of oils useful as processing aids include white mineral oil such as KAYDOL® oil (Chemtura Corp.; Middlebury, Conn.) and SHELLFLEX® 371 naphthenic oil (Shell Lubricants; Houston, Tex.). Another suitable oil is TUFFLO® oil (Lyondell Lubricants; Houston, Tex).

[00042] **Stabilizers and other additives:** In certain aspects of the invention, the ethylenic polymers are treated with one or more stabilizers, for example, antioxidants, such as IRGANOX® 1010 and IRGAFOS® 168 (Ciba Specialty Chemicals; Glattbrugg, Switzerland). In general, polymers are treated with one or more

5 stabilizers before an extrusion or other melt processes. For example, the compounded polymeric composition may comprise from 200 to 600 wppm of one or more phenolic antioxidants, and/or from 800 to 1200 wppm of a phosphite-based antioxidant, and/or from 300 to 1250 wppm of calcium stearate. In other aspects of the invention, other polymeric additives are blended or compounded into the polymeric compositions,

10 such as ultraviolet light absorbers, antistatic agents, pigments, dyes, nucleating agents, fillers, slip agents, fire retardants, plasticizers, processing aids, lubricants, stabilizers, smoke inhibitors, viscosity control agents, and/or anti-blocking agents. The polymeric composition may, for example, comprise less than 10 percent by the combined weight of one or more of such additives, based on the weight of the

15 ethylenic polymer.

[00043] **Other additives:** Various other additives and adjuvants may be blended or compounded with the ethylenic polymers of this invention to form polymeric compositions, including fillers (such as organic or inorganic particles, including nano-size particles, such as clays, talc, titanium dioxide, zeolites, powdered

20 metals), organic or inorganic fibers (including carbon fibers, silicon nitride fibers, steel wire or mesh, and nylon or polyester cording), tackifiers, waxes, and oil extenders (including paraffinic or naphthelene oils), sometimes in combination with other natural and/or synthetic polymers.

[00044] **Cross-linking Agents:** For those end-use applications in which it is

25 desired to fully or partially cross-link the ethylenic polymer of this invention, any of a variety of cross-linking agents may be used. Some suitable cross-linking agents are disclosed in Zweifel Hans et al., "Plastics Additives Handbook," Hanser Gardner Publications, Cincinnati, Ohio, 5th edition, Chapter 14, pages 725-812 (2001); Encyclopedia of Chemical Technology, Vol. 17, 2nd edition, Interscience Publishers

30 (1968); and Daniel Seern, "Organic Peroxides," Vol. 1, Wiley-Interscience, (1970). Non-limiting examples of suitable cross-linking agents include peroxides, phenols, azides, aldehyde-amine reaction products, substituted ureas, substituted guanidines; substituted xanthates; substituted dithiocarbamates; sulfur-containing compounds, such as thiazoles, sulfenamides, thiuramidisulfides, paraquinonedioxime,

dibenzoparaquinonediimine, sulfur; imidazoles; silanes and combinations thereof.

Non-limiting examples of suitable organic peroxide cross-linking agents include alkyl peroxides, aryl peroxides, peroxyesters, peroxycarbonates, diacylperoxides,

peroxyketals, cyclic peroxides and combinations thereof. In some embodiments, the

5 organic peroxide is dicumyl peroxide, t-butylisopropylidene peroxybenzene, 1,1-di-t-butyl peroxy-3,3,5-trimethylcyclohexane, 2,5-dimethyl-2,5-di(t-butyl peroxy) hexane, t-butyl-cumyl peroxide, di-t-butyl peroxide, 2,5-dimethyl-2,5-di-(t-butyl peroxy)

hexyne or a combination thereof. In one embodiment, the organic peroxide is

dicumyl peroxide. Additional teachings regarding organic peroxide cross-linking

10 agents are disclosed in C. P. Park, "Polyolefin Foam", Chapter 9 of *Handbook of Polymer Foams and Technology*, edited by D. Klemperer and K. C. Frisch, Hanser Publishers, pp. 198-204, Munich (1991). Non-limiting examples of suitable azide

cross-linking agents include azidoformates, such as tetramethylenebis(azidoformate); aromatic polyazides, such as 4,4'-diphenylmethane diazide; and sulfonazides, such as

15 p,p'-oxybis(benzene sulfonyl azide). The disclosure of azide cross-linking agents can

be found in U.S. Patent Nos. 3,284,421 and 3,297,674. In some embodiments, the cross-linking agents are silanes. Any silane that can effectively graft to and/or cross-link the ethylene/ α -olefin interpolymers or the polymer blend disclosed herein can be used. Non-limiting examples of suitable silane cross-linking agents include

20 unsaturated silanes that comprise an ethylenically unsaturated hydrocarbyl group, such as a vinyl, allyl, isopropenyl, butenyl, cyclohexenyl or gamma-(meth)acryloxy allyl group, and a hydrolyzable group such as a hydrocarbyloxy, hydrocarbonyloxy, and hydrocarbylamino group. Non-limiting examples of suitable hydrolyzable

25 groups include methoxy, ethoxy, formyloxy, acetoxy, propionyloxy, alkyl and arylamino groups. In other embodiments, the silanes are the unsaturated alkoxy

silanes which can be grafted onto the interpolymers. Some of these silanes and their preparation methods are more fully described in U.S. Pat. No. 5,266,627. The

amount of the cross-linking agent can vary widely, depending upon the nature of the ethylenic polymer or the polymeric composition to be cross-linked, the particular

30 cross-linking agent employed, the processing conditions, the amount of grafting initiator, the ultimate application, and other factors. For example, when

vinyltrimethoxysilane (VTMOS) is used, the amount of VTMOS is generally at least about 0.1 weight percent, at least about 0.5 weight percent, or at least about 1 weight

percent, based on the combined weight of the cross-linking agent and the ethylenic polymer or the polymeric composition.

[00045] *End Use Applications:* The ethylenic polymer of this invention may be employed in a variety of conventional thermoplastic fabrication processes to
5 produce useful articles, including objects comprising at least one film layer, such as a monolayer film, or at least one layer in a multilayer film, which films may be prepared by cast, blown, calendered, or extrusion coating processes; molded articles, such as blow molded, injection molded, or rotomolded articles; extrusions; fibers; woven or non-woven fabrics; and composite or laminate structures made with any of
10 the foregoing articles.

[00046] The ethylenic polymers of this invention (either alone or in blends or compounds with other components) may be used in producing fibers, such as staple fibers, tow, multicomponent, sheath/core, twisted, and monofilament fibers. Suitable fiber-forming processes include spunbonded and melt blown techniques, as disclosed
15 in U.S. Patent Nos. 4,340,563 (Appel et al.), 4,663,220 (Wisneski et al.), 4,668,566 (Nohr et al.), and 4,322,027 (Reba), gel spun fibers as disclosed in U.S. Patent No. 4,413,110 (Kavesh et al.), woven and nonwoven fabrics, as disclosed in U.S. Patent No. 3,485,706 (May), or structures made from or with such fibers, including blends with other fibers (such as polyester, nylon or cotton, and drawn, twisted, or crimped
20 yarns or fibers) or in composition or laminated structures with fibrous or non-fibrous materials (such as nonwovens or films).

[00047] The ethylenic polymers of this invention (either alone or in blends or compounds with other components) may be used in a variety of films, including but not limited to clarity shrink films, collation shrink films, cast stretch films, silage
25 films, stretch hooder films, sealants (including heat sealing films), stand-up-pouch films, liner films, and diaper backsheets.

[00048] The ethylenic polymers of this invention (either alone or in blends or compounds with other components) are also useful in other direct end-use applications, such as for wire and cable coatings, in sheet extrusion for vacuum
30 forming operations, and forming molded articles, including articles made via any of the known thermoplastic molding technologies, including injection molding, blow molding, or rotomolding processes. The polymeric compositions of this invention can also be formed into fabricated articles using other conventional polyolefin processing techniques.

[00049] Other suitable applications for the ethylenic polymers of this invention (either alone or in blends or compounds with other components) include films and fibers; soft touch goods, such as tooth brush handles and appliance handles; gaskets and profiles; adhesives (including hot melt adhesives and pressure sensitive
5 adhesives); footwear (including shoe soles and shoe liners); auto interior or exterior parts and profiles; foam goods (both open and closed cell); impact modifiers for other thermoplastic polymers such as high density polyethylene, isotactic polypropylene, or other olefin polymers; coated fabrics (such as artificial leather); hoses; tubing; weather stripping; cap liners; flooring (such as hard or soft flooring and artificial turf);
10 and viscosity index modifiers, as well as pour point modifiers, for lubricants.

[00050] Further treatment of the ethylenic polymers or polymeric compositions of this invention may be performed to render them more suitable for other end uses. For example, dispersions (both aqueous and non-aqueous) can also be formed using ethylenic polymers or polymeric compositions of this invention, such as by a
15 dispersion-manufacturing process. Frothed foams comprising the embodiment ethylenic polymer can also be formed, as disclosed in PCT Publication No. 2005/021622. The ethylenic polymers or polymeric compositions of this invention may also be crosslinked by any known means, such as the use of peroxide, electron beam, silane, azide, or other cross-linking technique. The ethylenic polymers or
20 polymeric compositions of this invention can also be chemically modified, such as by grafting (for example by use of maleic anhydride (MAH), silanes, or other grafting agent), halogenation, amination, sulfonation, or other chemical modification.

[00051] All applications, publications, patents, test procedures, and other documents cited, including priority documents, are fully incorporated by reference to
25 the extent such disclosure is not inconsistent with the disclosed compositions and methods and for all jurisdictions in which such incorporation is permitted.

EXAMPLES

[00052] All raw materials (ethylene, 1-octene) and the process solvent (a
30 narrow boiling range high-purity isoparaffinic solvent trademarked Isopar E and commercially available from Exxon Mobil Corporation) are purified with molecular sieves before introduction into the reaction environment. Hydrogen is supplied in pressurized cylinders as a high purity grade and is not further purified. The reactor monomer feed (ethylene) stream is pressurized via mechanical compressor to above

reaction pressure at 525 psig. The solvent and comonomer (1-octene) feed is pressurized via mechanical positive displacement pump to above reaction pressure at 525 psig. The individual catalyst components are manually batch diluted to specified component concentrations with purified solvent (Isopar E) and pressured to above
5 reaction pressure at 525 psig. All reaction feed flows are measured with mass flow meters and independently controlled with computer automated valve control systems.

[00053] The continuous solution polymerization reactor consists of a liquid full, non-adiabatic, isothermal, circulating, and independently controlled loop. The reactor has independent control of all fresh solvent, monomer, comonomer, hydrogen,
10 and catalyst component feeds. The combined solvent, monomer, comonomer and hydrogen feed to the reactor is temperature controlled to anywhere between 5°C to 50°C and typically 25°C by passing the feed stream through a heat exchanger. The fresh comonomer feed to the polymerization reactor is fed in with the solvent feed. The total fresh feed to each polymerization reactor is injected into the reactor at two
15 locations with roughly equal reactor volumes between each injection location. The fresh feed is controlled typically with each injector receiving half of the total fresh feed mass flow. The catalyst components are injected into the polymerization reactor through specially designed injection stingers and are each separately injected into the same relative location in the reactor with no contact time prior to the reactor. The
20 primary catalyst component feed is computer controlled to maintain the reactor monomer concentration at a specified target. The two cocatalyst components are fed based on calculated specified molar ratios to the primary catalyst component. Immediately following each fresh injection location (either feed or catalyst), the feed streams are mixed with the circulating polymerization reactor contents with Kenics
25 static mixing elements. The contents of each reactor are continuously circulated through heat exchangers responsible for removing much of the heat of reaction and with the temperature of the coolant side responsible for maintaining isothermal reaction environment at the specified temperature. Circulation around each reactor loop is provided by a screw pump.

30 [00054] The effluent from the first polymerization reactor (containing solvent, monomer, comonomer, hydrogen, catalyst components, and molten polymer) exits the first reactor loop and passes through a control valve (responsible for maintaining the pressure of the first reactor at a specified target). As the stream exits the reactor it is contacted with water to stop the reaction. In addition, various additives such as anti-

oxidants, can be added at this point. The stream then goes through another set of Kenics static mixing elements to evenly disperse the catalyst kill and additives.

[00055] Following additive addition, the effluent (containing solvent, monomer, comonomer, hydrogen, catalyst components, and molten polymer) passes through a heat exchanger to raise the stream temperature in preparation for separation of the polymer from the other lower boiling reaction components. The stream then enters a two stage separation and devolatilization system where the polymer is removed from the solvent, hydrogen, and unreacted monomer and comonomer. The recycled stream is purified before entering the reactor again. The separated and devolatilized polymer melt is pumped through a die specially designed for underwater pelletization, cut into uniform solid pellets, dried, and transferred into a hopper. After validation of initial polymer properties the solid polymer pellets are manually dumped into a box for storage. Each box typically holds ~1200 pounds of polymer pellets.

[00056] The non-polymer portions removed in the devolatilization step pass through various pieces of equipment which separate most of the ethylene which is removed from the system to a vent destruction unit (it is recycled in manufacturing units). Most of the solvent is recycled back to the reactor after passing through purification beds. This solvent can still have unreacted co-monomer in it that is fortified with fresh co-monomer prior to re-entry to the reactor. This fortification of the co-monomer is an essential part of the product density control method. This recycle solvent can still have some hydrogen which is then fortified with fresh hydrogen to achieve the polymer molecular weight target. A very small amount of solvent leaves the system as a co-product due to solvent carrier in the catalyst streams and a small amount of solvent that is part of commercial grade co-monomers.

[00057] Unless otherwise stated, implicit from the context or conventional in the art, all parts and percentages are based on weight.

[00058] Table 1 describes the polymerization conditions used to produce each of the copolymers.

[00059] Unless otherwise stated, implicit from the context or conventional in the art, all parts and percentages are based on weight.

[00060] *Comparative Samples A through D and Examples 1 through 4:* Eight ethylenic polymers are prepared in order to compare the properties of four ethylene-octene polymers (Comparative Samples A through D) prepared using a known

metallocene catalyst to the properties of five ethylene-octene polymers (Examples 1 through 4) of this invention.

- [00061] Table 1 describes the polymerization conditions used to produce each of the copolymers, with those conditions being set to produce pairs of polymers (e.g.,
- 5 Comparative Sample A and Example 1 are one pair) with comparable melt indices (I2) and densities

Table 1

Run	Product	Example	Catalyst	MI (12)	Density	Reactor Temp (C)	Solvent/ C2 Ratio	C2 Conv (%)	Corrected Exit C2 (g/L)	Reactor Poly Conc. (Wt%)	H2 Mole %	Octene/ Olefin Ratio
2007C28R04	8200	Comp A	1301/RIB S2/MMA O	4.7	0.8686	120.1	4.6	86.7	15.75	24.5	0.17	47.7
2007C28R06		1	6114/RIB S2/MMA O	4.3	0.8715	190	4.79	84.8	16.06	26.4	0.32	62.3
2007C28R01	8150	Comp B	1301/RIB S2/MMA O	0.5	0.868	103	6.23	83.4	16	19.6	--	--
2007C28R12		2	6114/RIB S2/MMA O	0.5	0.8684	169.6	6.23	80.9	14.55	21.4	0.2	66.5
2007C28R02	8100	Comp C	1301/RIB S2/MMA O	1	0.87	110	5.22	84.6	17	22.5	--	--
2007C28R10		3	6114/RIB S2/MMA O	0.9	0.8709	185	5.22	82.5	17.2	23.3	0.21	64.6
2007C28R03	8452	Comp D	1301/RIB S2/MMA O	3	0.875	115	5.22	87.3	14	22.4	--	--
2007C28R11		4	6114/RIB S2/MMA O	2.8	0.8764	180	5.22	86.3	13.74	23.6	0.32	57.8

CAS name for RIBS-2: Amines, bis(hydrogenated tallow alkyl)methyl, tetrakis(pentafluorophenyl)borate(1-)

CAS name for DOC-6114: Zirconium, [2,2"-[1,3-propanediylbis(oxy-κO)]bis[3",5,5"-tris(1,1-dimethylethyl)-5'-methyl[1,1':3',1"-terphenyl]-2'-olato-

5 κO]]dimethyl-, (OC-6-33)-

MMAO = modified methyl aluminoxane

CAS numbers for CGC 1301: 199876-48-7 and 200074-30-2

Table 2: Summary of properties of Comp A-D and Examples 1-4

Example	Catalyst	Melt Flow Ratio I10/I2	Mw	Mn	Mw/Mn	Total unsaturation per 1000 C	Vinyl groups/ Olefin groups	Octene mol% by C ¹³ NMR	Vinyls/ 1000 carbons	Sum of unsaturation per 100000 C
Comp A	1301/RIBS2/MMAO	7.7	91100	37346	2.44	0.148	0.18	12.62	0.03	148
1	6114/RIBS2/MMAO	7.45	92530	38376	2.41	0.122	0.52	11.65	0.06	122
Comp B	1301/RIBS2/MMAO	7.9	151250	62793	2.41	0.0825	0.17	12.64	0.01	82.5
2	6114/RIBS2/MMAO	7.98	147010	66333	2.22	0.0845	0.49	14.18	0.04	84.5
Comp C	1301/RIBS2/MMAO	7.6	124860	52795	2.36	0.085	0.16	12.13	0.01	85
3	6114/RIBS2/MMAO	8.33	126490	55977	2.26	0.118	0.52	11.85	0.06	118
Comp D	1301/RIBS2/MMAO	7.6	93540	35174	2.66	0.114	0.18	11.09	0.02	114
4	6114/RIBS2/MMAO	7.4	94390	40946	2.31	0.0835	0.58	10.48	0.05	83.5

Table 3: Details of H^1 NMR data on unsaturations for examples of Tables 1 and 2

Structure Name	Vinylene (<i>trans</i>)	Vinylene (<i>cis</i>)	Internal Vinylene	Trisubstitute (internal)	Vinyl	Symmetric Vinylidene	Asymmetric Vinylidene	
Structure Code	Vy1- <i>trans</i> Vy2- <i>trans</i>	Vy1- <i>cis</i> Vy2- <i>cis</i>	Vy3	T3, T4 (mainly T4)	V1	Vd3	Vd1	
Peak position	5.49	5.44	5.43 5.26	5.28-5.18	5.04 5.90	4.80	4.86 4.81	Example Number
	Per 1000000 C's	Per 1000000 C's	Per 1000000 C's	Per 1000000 C's	Per 1000000 C's	Per 1000000 C's	Per 1000000 C's	
2007C28R04	40.5	12.5	13.5	21.5	26	27.5	6.5	Comp A
2007C28R06	10	9	0	13.5	63	14.5	12	1
2007C28R01	30	5.5	6	9.5	14	14	3.5	Comp B
2007C28R12	7.5	6	0	11	41.5	8	10.5	2
2007C28R02	31.5	6.5	6.5	8	14	15.5	3	Comp C
2007C28R10	10	7.5	0	12.5	61	13.5	13.5	3
2007C28R03	32.5	10	8	15	20	23.5	5	Comp D
2007C28R11	7	5.5	0	8.5	48.5	7	7	4

We Claim:

1. An ethylenic polymer comprising an overall polymer density of not more than 0.905 g/cm³; total unsaturation of not more than 125 per 100,000 carbons; and a GI200 gel rating of not more than 15; up to 3 long chain branches/1000 carbons; vinyl-3 content of less than 5 per 100,000 carbons; and a total number of vinyl groups/1000 carbons of less than the quantity (8000/M_n), wherein the vinyl-3 content and vinyl group measurements are measured by gel permeation chromatography (145°C) and ¹H-NMR (125°C).

2. The ethylenic polymer of claim 1 further comprising a ratio of vinyl groups to total olefin groups according to the formula:

$$VG/TOG > (\text{comonomer mole percentage}/0.1)^a \times 10^a \times 0.8$$

where a = -0.24, VG = vinyl groups, and TOG = total olefin groups.

3. An ethylenic polymer comprising total unsaturation of from about 10 to about 125 per 100,000 carbons total unsaturation; and up to 3 long chain branches/1000 carbons; and a GI200 gel rating of not more than 15.

4. The ethylenic polymer of claim 1 further comprising a vinyls amount and a total unsaturation amount, wherein the ratio of vinyls amount:total unsaturation amount is at least 0.2:1, and wherein the ethylenic polymer has less than 5 per 100,000 carbons of vinyl-3 content.

5. The ethylenic polymer of claim 1 further comprising a vinyls amount and a total unsaturation amount, wherein the ratio of vinyls amount:total unsaturation amount is at least 0.3:1.

6. The ethylenic polymer of claim 5 wherein the ratio of vinyls amount:total unsaturation amount is from about 0.4:1 to about 0.8:1.

7. The ethylenic polymer of claim 1, wherein the polymer has less than 5 per 100,000 carbons of vinyl-3 content.

8. A composition comprising, or made from, at least one ethylenic polymer of claim 1, wherein at least a portion of the ethylenic polymer has been cross-linked.

9. A composition comprising, or made from, at least one ethylenic polymer of claim 1, in which at least a portion of the ethylenic polymer has been functionalized.

10. A composition comprising, or made from, at least one ethylenic polymer of claim 1 and at least one other natural or synthetic polymer.

11. The composition of claim 10 in which at least one of the other natural or synthetic polymer(s) is selected from the group consisting of at least one thermoplastic, at least one elastomeric olefin polymer and at least one styrenic block copolymer.

12. A composition comprising, or made from, at least one ethylenic polymer of claim 1 and at least one other component selected from the group consisting of a tackifier, a wax, and an oil.

13. A composition comprising a dispersion or emulsion of particles in a fluid, wherein the particles comprise, or are made from, at least one ethylenic polymer of claim 1.

14. An ethylenic polymer comprising an overall polymer density of not more than 0.9 g/cm³; total unsaturation of not more than 125 per 100,000 carbons; a GI200 gel rating of not more than 15; vinyl-3 content of less

than 5 per 100,000 carbons; and a vinyls amount and a total unsaturation amount, wherein the ratio of vinyls amount:total unsaturation amount is between 0.4:1 and 0.8:1.

- 5 15. A fabricated article in which at least one layer or portion of the fabricated article comprises, or is made from, at least one ethylenic polymer of claim 1 and in which the fabricated article comprises a film, a sheet, a fiber, a nonwoven, a laminate, or a composite.

ETHYLENIC POLYMER AND ITS USE

ABSTRACT

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Ethylenic polymers comprising low levels of total unsaturation are disclosed. Compositions using such ethylene polymers and fabricated articles made from them are also disclosed.

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No Suitable Figure