

Description

The invention relates to a process for the preparation of a coagulé, i.e. a coagulated material obtained by impregnating a textile cloth in an impregnating bath containing at least a coagulable polymer latex, followed by coagulation in a coagulating bath.

According to the current procedure, a textile cloth is impregnated with a polyurethane by immersing it in a solution of polyurethane in DMF. Then the polyurethane polymer on the cloth is coagulated by placing the obtained impregnated cloth in a water bath. The apolar polyurethane polymer flocks out in this very polar medium, whereas the DMF is taken up in the water.

It should be noted that according to the known method the textile cloth is impregnated in an organic medium. As organic solvent only DMF is used. Because during coagulation the solvent is taken up in the water, both for economical and environment-hygienic reasons it is required to separate the solvents from the water. Usually, this separation occurs by distillation of the water/DMF mixture. It is clear that this separation is complicated and expensive, reasons why a coagulation process is needed, wherein no organic solvent is used.

It should be clear that in such a process one should start from a polymer which is dissolved in water or dispersed in water, whereupon anyhow the polymer should be coagulated again from the water phase.

It is known that by the use of heat-coagulable polymer, latices may be coagulated at temperatures above the cloud point of the heat-coagulant.

Furthermore it is known that polymer latices may be coagulated by means of the addition of electrolytes and/or by adapting the pH.

By the use of the known processes up to now, one was not able to achieve the desired coagulation structure. It is believed that such a desired coagulation structure is obtained because the polyurethane polymer is deposited on the fibers in a discontinuous way resulting in a microcellular structure. Such a microcellular structure renders the coagulated cloth the softness and absorption characteristics, which are characteristic for a coagulé.

By coagulation from the water phase the desired coagulation structure may be obtained by the use of heat-coagulants and/or by adding an electrolyte solution and/or by adapting the pH, which coagulation structure, however, is destroyed during drying, wherein the remaining water is removed under obtaining a continuous film.

The cloth thus obtained is very hard and it has characteristics which are different from those of a conventional coagulated material.

This "film forming" is due to the highly polar character of the polyurethane polymer or an other polymer dispersed in water together with the highly polar coagulant and/or electrolyte.

The remaining water is strongly bound in this system and it acts as a softener and decreases therefore the film forming temperature essentially.

The invention aims now to provide a process, wherein the above-mentioned disadvantages are removed effectively.

Accordingly, the invention provides a process for the preparation of a coagulé by impregnating a textile cloth in an impregnating bath containing a coagulable polymer dispersion composition, followed by coagulation in an aqueous coagulating bath, characterized in that the impregnating bath contains a physical foaming agent which is insoluble in water, wherein foaming occurs simultaneously with the coagulation or immediately thereafter at a temperature above 70°C.

It is surprisingly found that according to the present process a high quality coagulé is obtained, which is comparable with the coagulé, obtained according to conventional processes.

The undesired film forming does not occur according to the invention, which is mainly due to the use of the physical foaming agent in an aqueous system, which foaming agent renders the coagulated polymer coating a foamed character during or immediately after the coagulation process under obtaining a desired coagulation structure.

The coagulation and/or foaming of the polymer dispersion occurs according to the invention by heating the impregnated textile cloth, preferably in the presence of a heat-coagulant.

Usually, the coagulation and/or foaming occurs in an aqueous coagulating bath at a temperature of at least 15°C, wherein until a temperature of about 70°C usually only coagulation takes place, whereas at a temperature higher than about 70°C both coagulation and foaming occur.

Preferably, the coagulation is carried out in an aqueous coagulating bath of above 70°C, wherein both coagulation and foaming take place.

Furthermore, the coagulation and foaming of the polymer dispersion may be carried out according to the invention in a steam chamber at 100°—130°C, and preferably at 100°—110°C.

Furthermore, the coagulation and foaming may be carried out in a quick heat transfer oven, for instance in a so-called microwave oven or in an infrared dryer.

Finally, the coagulation of the polymer dispersion according to the invention may be carried out successfully by means of a suitable electrolyte and/or a pH, which is adapted to the used polymer dispersion.

In particular, those polymer dispersions are useful in this process, which are dispersed in water by means of an essentially anionic emulsifying system.

In case of anionic polymer dispersions a quick coagulation occurs at a pH < 7, whereas in case of cationic polymer dispersions the coagulation occurs preferably at a pH > 7.

The coagulated polymer dispersion thus obtained is subsequently foamed by heating in a

water bath, steam bath or in a quick heat transfer oven, at the above-mentioned temperatures.

As disclosed above, the desired results according to the invention are obtained by the fact that the foaming of the coagulated polymer coating occurs simultaneously with the coagulation process or immediately thereafter.

In practice, the process according to the invention may usually be carried out in two ways.

According to the first way, a textile cloth is impregnated in an impregnating bath, containing a coagulate polymer dispersion and a heat-coagulant, or a polymer dispersion, wherein the heat-coagulant is built in the polymer chain, and a physical foaming agent, followed by coagulation, wherein the entire impregnation and coagulation process is carried out from the water phase, whereupon subsequently or during the coagulation process the foaming of the polymer dispersion, already coagulated on the textile cloth, occurs.

According to the other way, a textile cloth is impregnated in an impregnating bath containing at least one electrolyte instable polymer dispersion of highly anionic or highly cationic character and a physical foaming agent. Hereafter coagulation takes place at a pH <7, if an anionic polymer dispersion is used, or at a pH >7, if there is used a cationic polymer dispersion, wherein, if desired, one or more electrolytes may be added. Coagulation may occur, too, by means of electrolytes only without pH adaption.

Immediately after the coagulation of the polymer dispersion on the textile cloth foaming occurs by heating to the proper temperature.

Both ways result in a high quality coagulated material.

The undesired film forming does not occur, which is mainly due to the use of a physical foaming agent, which renders the coagulated polymer coating during or immediately after the coagulation process, dependent on the chosen embodiment, a foaming character by immersing it in a hot water bath under obtaining a desired coagulation structure.

The desired coagulation structure also may be obtained by coagulating the impregnated textile cloth, if the process according to the invention is carried out according to the first way, directly in an instantaneous heat transfer oven, such as a microwave oven or IR-dryer, wherein simultaneously a foaming structure is obtained.

The coagulation according to the invention according to the first way is carried out as follows:

An in water coagulable polymer dispersion composition is applied onto a textile cloth, woven or non-woven. This application may be effectuated by immersing it in an impregnating bath of a proper pH, preferably <7, with at least the proper components according to the invention.

The amount of polymer, which is applied dur-

ing impregnation, depends on the used impregnating techniques, which are known to those skilled in the art, and on the absorption ability of the used textile cloth and it may furthermore be controlled by means of a foulard or a knife over roll. The amount of polymer to be applied is highly dependent on the use of the coagulated cloth thus obtained.

The in water coagulable polymer dispersion composition according to the invention may be applied by means of known coating techniques, such as amongst others reverse roll coating techniques, the screen printing techniques or a knife over roll, flow coat application techniques, spray application techniques. Dependent on the use of the polymer dispersion the composition may be applied on the cloth on one side or on both sides.

The properties of the coagulé, such as feel, colour, may be modified by adding the usual additives to the polymer dispersion.

An additional advantage of the application of the process according to the invention is that as substrate for a coagulé materials may be used, which are not resistant against DMF. In the known procedure, DMF is used in the impregnating bath as solvent, which means that those materials to which DMF is too aggressive, may not be used as substrate for a coagulé according to the known procedure.

As substrate for a coagulé according to the invention the following materials may be used: wovens based on natural or synthetic fibers, such as polyester, polyamide and acryl fibers as well as blends thereof. The invention is also suited for non-woven substrates.

After application of the polymer dispersion composition according to the invention by means of one of the above-disclosed ways onto the textile cloth the coagulation is carried out by conveying the textile cloth thus obtained through a heated water bath, at a temperature of more than 70°C and preferably at 85°—100°C, or in a steam chamber, usually at 100°—130°C, and preferably at 100°—110°C, wherein the coagulation process and the foaming process of the polymer dispersion coating essentially simultaneously occur.

According to the invention it is also possible to carry out the coagulation phase and the foaming phase separately, the one after the other.

By doing so, first the polymer dispersion composition is coagulated in a heated water bath at a temperature of more than 70°C, whereupon the foaming of the polymer latex film occurs by conveying the obtained coagulated cloth through a heated water bath, usually at a temperature of at least 85°C and preferably at 90°—100°C, or in a steam chamber, usually at 100°—130°C, and preferably at 100°—110°C.

According to an embodiment of the process according to the invention the coagulation and foaming are carried out by means of an instantaneous heat transfer oven. Herein a textile

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cloth, which is provided with the polymer latex composition of the invention is directly placed in a microwave oven.

Accordingly, coagulation, foaming and drying may take place simultaneously.

The advantage of this embodiment is clear: a coagulating bath and foaming bath are superfluous.

The coagulation according to the other way of the invention is carried out as follows:

According to the above-described application technique there is applied on a textile cloth a polymer dispersion composition suitable according to the invention, which composition is electrolyte instable in water and which is a highly anionic polymer dispersion or a highly cationic polymer dispersion.

After applying a polymer dispersion composition according to the invention on a cloth by means of the above-described processes, the coagulation is carried out.

The thus treated textile cloth is conveyed through a water bath of 15–75°C, but preferably at 40–60°C. The bath is adjusted to a pH < 7, if a highly anionic polymer dispersion is applied, or to a pH > 7 if a highly cationic polymer dispersion is used.

Furthermore, the coagulating bath contains, if required, one or more electrolytes, pH-range concentration and type of electrolyte are dependent on the type of polymer dispersion.

After having provided the textile cloth with a coagulated polymer dispersion composition, the coagulated coating is foamed by conveying the treated textile cloth through a hot water bath, whether or not at the same pH as the coagulating bath, usually at a temperature of more than 70°C and preferably at 85–100°C, or in a steam chamber, usually at 100–130°C, and preferably at 100–110°C.

The foaming may also be carried out by means of an intensive heat transfer oven, such as a microwave oven or a IR drying oven.

The advantage of this embodiment compared with the first-described embodiment is that coagulation may take place at room temperature and without making use of heat-coagulants.

However, the coagulation process and the foaming process do not take place simultaneously but the one after the other, so that the foaming requires an additional bath.

According to the invention, in the first embodiment there is used a polymer dispersion, which is coagulable by means of a heat-coagulant, such as for instance polymer dispersions of the type: polybutadiene latex, polybutadiene styrene copolymer latex, polybutadiene acrylonitrile copolymer latex, polystyrene butadiene acrylonitrile terpolymer latex, polychloroprene latex, polyacrylate latex, polyvinyl acetate latex, polyurethane latex or a mixture thereof.

Because of the specific polymer characteristics of the polyurethane polymer preferably polyurethane latex is used.

The polyurethane latex is prepared according to

a technology, which is amongst others disclosed in the U.S. Patent Specifications 4,046,729 and 4,066,591, both of PPG-Industries Inc., and in the Netherlands Patent Specification 140,881 and 141,914 of Bayer AG.

The polyurethane polymer might be built up from an aliphatic, cycloaliphatic or an aromatic diisocyanate, a polyol based on a polyester diol having a molecular weight of 500–5000, preferably 1000–2000, and polyether diol having a molecular weight of 400–6000, preferably 1000–2000, a polycarbonate diol having a molecular weight of 500–5000, preferably 1000–2000, whether or not with other types of polydiols and mixtures, or low molecular diols, such as: neopentyl glycol, 1,2-ethane diol, 1,3-butane diol, 1,4-butane diol and others and mixtures thereof and a diamine such as: 1,2-ethane diamine, 1,3-propane diamine and isophorone diamine.

The coagulation is preferably carried out in an impregnating bath containing 5–30%, by weight, preferably 5–15%, by weight, of the polymer dispersion.

By using the coagulation according to the heat-coagulant process good results are obtained according to the invention when as heat-coagulant alkoxylated amines, preferably with a molecular weight of 800–6000, are used; organopolysiloxanes or derivatives thereof, polyvinyl alkylethers or derivatives thereof, polyacetals, polythio ethers, poly(ethylene oxide) or derivatives thereof, poly(propylene/ethylene oxide) or derivatives thereof.

In particular, when poly(ethylene oxide) is used as heat-coagulant, the heat-coagulable polyurethane dispersion may be obtained by introducing the poly(ethylene oxide) component in the polymer chain of the polyurethane polymer. In this connection a polyurethane dispersion is prepared according to a technology, which is amongst others disclosed in the above-mentioned U.S. Patent Specifications.

The introduction of the poly(ethylene oxide) component is carried out according to a known process, wherein both OH groups of the poly(ethylene oxide) component are reacted in the polymer chain by means of the reaction with the NCO groups of the used diisocyanate.

According to the invention good results are obtained if as a starting material a poly(ethylene oxide) component is used having a molecular weight of 600–4000, preferably 1000–2000. Furthermore, mixtures of the poly(ethylene oxide) components having different molecular weights may be used.

According to the invention good results may be obtained if 0.5–10 mole % of the poly(ethylene oxide) diol component is introduced into the polyurethane polymer. Preferably, 1.5–5.0 mole % is built into the polyurethane polymer.

The heat coagulant is used in a concentration of 2–30%, by weight and preferably of 2–10%, by weight, based on the solid components of the polymer dispersion.

By use of the coagulation by means of the

addition of electrolytes and/or adaption of the acidity of electrolyte instable polymer dispersion of highly anionic or highly cationic character; respectively, good results are obtained if it is started from the salts of the alkali and earth alkaline metals of hydrogen chloride, nitric acid, sulphuric acid or water soluble salts of aluminum, iron, manganese, cobalt, cadmium and chromium.

The adaption of the acidity of the coagulating baths and/or foaming bath may occur by adding suitable known acids and bases, respectively. The acidity, type and concentration of the electrolyte are highly dependent on the starting polymer dispersion and it may only be determined experimentally per polymer dispersion composition.

It appeared according to the invention that the combination of both above-mentioned embodiments yields good results.

The favourable foaming, required for the achievement of the desired coagulation structure, occurs in the coagulating bath if it is desirable to have the coagulation and the foaming of the coagulated polymer dispersion coating taking place in one single phase. Good results are obtained by carrying out the foaming after the coagulation.

In this case the textile cloth, which is provided with a coagulated polymer dispersion, is conveyed in a second heated water bath. The temperature of this foaming bath is highly dependent on the used foaming agent and is more than 70°C. Foaming also may occur by conveying the coagulated cloth through a steam chamber, usually at 100°—130°C, and preferably at 100°—110°C.

Foaming may also occur by conveying the coagulated cloth through an instantaneous heat transfer oven, such as a microwave oven or infrared radiators.

According to the invention a water insoluble physical foaming agent having a boiling point between -40°C and +50°C, and preferably between -20°C and +30°C, is used.

Good results are obtained according to the invention when use is made of a water insoluble solvent, such as halogenated saturated or unsaturated aliphatic or aromatic hydrocarbons, whether or not encapsulated in a polymer film.

The invention comprises furthermore the coagulé obtained by the use of the present process. This coagulé has very favourable characteristics and is essentially similar with the coagulé manufactured by the known processes.

The invention is now illustrated by means of the following examples.

Example I

In an impregnating bath having the dimensions of 200×200×250 mm a polyethyl acrylate dispersion, known as RA—2, commercially available from Stahl Chemical Industries B.V. at Waalwijk, Netherlands, was introduced. This resin was then diluted with water to a solids contents in the impregnating bath of 20%, by weight.

Then 20%, by weight, based on the solids, of an alkoxyated amine, known as Cartafix U, commercially available from Sandoz A.G., Basel, Switzerland, is added to this resin.

Then the pH was adjusted to 4.7, whereupon while stirring 5% of 1,2-dibromo 1,1,2,2-tetrafluoroethane was added.

A textile cloth, which was made rough on both sides and having a weight of 180 g/m² and dimensions of 100×100 mm, was impregnated by immersion in the impregnating bath during 10 seconds.

Subsequently, the impregnated cloth was squeezed by means of a knife over roll in such a way that the cloth contained 1200 g acrylate dispersion composition per m².

Hereafter the impregnated cloth was conveyed in a coagulating bath, having dimensions of 200×200×250 mm, containing water of 95°C. The residence time in the coagulating bath was 30 seconds.

Finally, the water was removed from the obtained coagulated cloth by means of foulard and a drying oven at a temperature of 150°C.

The resulting substrate had the same appearance and absorption ability as a coagulé obtained by the conventional procedure.

Example II

Analogous to Example I, provided that the polyethyl acrylate latex was replaced by a polychloroprene latex, known as Neoprene Latex from Dupont-U.S.A.

The obtained coagulé had the appearance and the absorption ability which was comparable with the coagulé obtained according to the conventional procedure.

Example III

Analogous to Example II.

The polychloroprene latex was replaced by an acrylonitrile butadiene latex, known as No. 840, commercially available from Synthomer Chemie G.m.b.H., West Germany, whereas the 1,2-dibromo 1,1,2,2-tetrafluoroethane was replaced by trichloro fluoromethane. By doing so, a coagulé is obtained with an excellent flexibility.

Example IV

Analogous to the procedure of Example III.

The acrylonitrile butadiene latex was replaced by an anionic polyurethane latex, known as UE—9002, commercially available from Stahl Chemical Industries B.V., Waalwijk, Netherlands.

The obtained coagulé had the appearance, the flexibility, the absorption ability and furthermore the physical characteristics of a coagulé obtained according to the conventional procedure.

Example V

Analogous to the procedure of Example IV.

The alkoxyated amine was replaced by polyvinyl methylether, wherein the ratio coagulant/latex was changed to 30%, by weight, of coagulant, based on the solids of the latex. This was

necessary, because of the less effectiveness in coagulating properties compared with the formerly used alkoxylated amine.

A substrate was obtained having an absorption ability and physical characteristics similar to a coagulé obtained according to the conventional procedure.

Example VI

In an impregnating bath having the dimensions of 200×200×200 mm a polyurethane dispersion having the following composition, was introduced. A prepolymer was prepared according to a process as disclosed in the U.S. Patent Specifications 4,046,729 and 4,066,591, wherein 9 mole % of a poly (ethyleneoxide) diol having a molecular weight of 1000, was built into the prepolymer. As polyester diol a hexane diol adipate, having a molecular weight of 2000, is used in a mole % of 47. As diisocyanate the hexamethylene diisocyanate was used.

The formulation occurred such, that the NCO/OH ratio was 1.8. As extending agent isophorone diamine was used. Solids contents of the dispersion was 30%, by weight.

This resin was diluted with water to a solids contents in the impregnating bath of 12%, by weight.

The pH of the impregnating bath was adjusted to 4 by means of acetic acid. Subsequently, 5% trichloro fluoromethane was mixed in.

A cotton cloth, both sides of which were made rough, having a weight of 180 g/m² and dimensions of 100×100 mm, was impregnated by immersing it in the impregnating bath during 10 seconds.

Then the impregnated cloth was squeezed by means of a knife over roll, in such a way that the cloth contained 1000 g polyurethane dispersion composition per m².

Then the impregnated cloth was conveyed in a coagulating bath of 200×200×250 mm, containing water of 80°C. The immersion time in the coagulating bath was 30 seconds.

The excess of water was now removed by means of foulard and a drying oven at a temperature of 150°C.

The resulting substrate had the same appearance, absorption ability, flexibility and physical characteristics as a coagulé obtained according to the conventional procedure.

Example VII

In an impregnating bath of 200×200×250 mm an anionic polyurethane dispersion, known as CE-9002, commercially available from Stahl Chemical Industries B.V., Waalwijk, Netherlands, was introduced. This resin was diluted with water to a solid content in the impregnating bath of 12%, by weight. Then 5% 1,2-dibromo 1,1,2,2-tetrafluoroethane was mixed in.

A cotton cloth, both sides of which were made rough, and having a weight of 180 g/m², dimensions 100×100 mm, was impregnated by immersing it in the impregnating bath during 10 seconds.

Then the excess of polyurethane dispersion composition was squeezed by means of a knife over roll (to 1500 g/m²).

Hereafter this impregnated cloth was conveyed into a coagulating bath of 200×200×250 mm, containing water of 80°C, whereas the pH of said bath was adjusted to 3 by means of acetic acid. The coagulation and the foaming were carried out by immersion during 60 seconds.

The resulting substrate had excellent physical characteristics, flexibility and appearance, which were similar to a coagulé obtained according to the conventional procedure.

Example VIII

Analogous to the process of Example VII.

The acetic acid in the coagulating bath was replaced by 5%, by weight, of magnesium chloride, whereas the temperature of the foaming bath was 90°C instead of 80°C.

The obtained coagulé had the physical characteristics and the absorption ability similar to a coagulé obtained according to the conventional procedure.

Example IX

Analogous to the process of Example VIII.

The polyurethane latex was replaced by a polyethyl acrylate dispersion, known as RA-2, commercially available from Stahl Chemical Industries B.V., Waalwijk, Netherlands.

The percentage of magnesium chloride could be reduced to 1%.

The obtained substrate had similar characteristics as disclosed under Example II.

Example X

Analogous to the process of Example IV.

The impregnated cloth was heated in a microwave oven during 5 minutes after the impregnating phase and the water removal.

Accordingly, a coagulé was obtained having a foam structure with characteristics and appearance essentially similar with the coagulé structure of the preceding examples.

Claims

1. A process for the preparation of a coagulé by impregnating a textile cloth in an impregnating bath containing a coagulable polymer dispersion composition, followed by coagulation in an aqueous coagulation bath, characterized in that the impregnating bath contains a physical foaming agent which is insoluble in water and wherein simultaneously with the coagulation or immediately thereafter foaming occurs at a temperature above 70°C.

2. The process according to claim 1, characterized in that the coagulation and/or the foaming are carried out by heating the impregnated textile cloth.

3. The process according to claim 2, characterized in that the coagulation is carried out by means of a heat-coagulant.

necessary, because of the less effectiveness in coagulating properties compared with the formerly used alkoxylated amine.

A substrate was obtained having an absorption ability and physical characteristics similar to a coagulé obtained according to the conventional procedure.

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The formulation occurred such, that the NCO/OH ratio was 1.8. As extending agent isophorone diamine was used. Solids contents of the dispersion was 30%, by weight.

This resin was diluted with water to a solids contents in the impregnating bath of 12%, by weight.

The pH of the impregnating bath was adjusted to 4 by means of acetic acid. Subsequently, 5% trichloro fluoromethane was mixed in.

A cotton cloth, both sides of which were made rough, having a weight of 180 g/m² and dimensions of 100×100 mm, was impregnated by immersing it in the impregnating bath during 10 seconds.

Then the impregnated cloth was squeezed by means of a knife over roll, in such a way that the cloth contained 1000 g polyurethane dispersion composition per m².

Then the impregnated cloth was conveyed in a coagulating bath of 200×200×250 mm, containing water of 80°C. The immersion time in the coagulating bath was 30 seconds.

The excess of water was now removed by means of foulard and a drying oven at a temperature of 150°C.

The resulting substrate had the same appearance, absorption ability, flexibility and physical characteristics as a coagulé obtained according to the conventional procedure.

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A cotton cloth, both sides of which were made rough, and having a weight of 180 g/m², dimensions 100×100 mm, was impregnated by immersing it in the impregnating bath during 10 seconds.

Then the excess of polyurethane dispersion composition was squeezed by means of a knife over roll (to 1500 g/m²).

Hereafter this impregnated cloth was conveyed into a coagulating bath of 200×200×250 mm, containing water of 80°C, whereas the pH of said bath was adjusted to 3 by means of acetic acid. The coagulation and the foaming were carried out by immersion during 60 seconds.

The resulting substrate had excellent physical characteristics, flexibility and appearance, which were similar to a coagulé obtained according to the conventional procedure.

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Analogous to the process of Example VII.

The acetic acid in the coagulating bath was replaced by 5%, by weight, of magnesium chloride, whereas the temperature of the foaming bath was 90°C instead of 80°C.

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Accordingly, a coagulé was obtained having a foam structure with characteristics and appearance essentially similar with the coagulé structure of the preceding examples.

Claims

1. A process for the preparation of a coagulé by impregnating a textile cloth in an impregnating bath containing a coagulable polymer dispersion composition, followed by coagulation in an aqueous coagulation bath, characterized in that the impregnating bath contains a physical foaming agent which is insoluble in water and wherein simultaneously with the coagulation or immediately thereafter foaming occurs at a temperature above 70°C.

2. The process according to claim 1, characterized in that the coagulation and/or the foaming are carried out by heating the impregnated textile cloth.

3. The process according to claim 2, characterized in that the coagulation is carried out by means of a heat-coagulant.



4. The process according to claim 3, characterized in that the coagulation and foaming are carried out at a temperature of 85—100°C.

5. The process according to claim 2, characterized in that the coagulation and foaming are carried out in a steam chamber at 100—130°C.

6. The process according to claim 5, characterized in that the coagulation and foaming are carried out in a steam chamber at 100—110°C.

7. The process according to claim 2, characterized in that the coagulation and foaming are carried out in a quick heat transfer oven.

8. The process according to claim 1, characterized in that the coagulation is carried out by means of a suitable electrolyte and a pH, which is adapted to the polymer dispersion to be used.

9. The process according to claim 8, characterized in that the coagulation is carried out at a pH < 7 by the use of anionic polymer dispersions.

10. The process according to claim 8, characterized in that the coagulation is carried out at a pH > 7 by the use of cationic polymer dispersions.

11. The process according to claims 8 to 10, characterized in that the coagulation is carried out at a temperature of 15—75°C.

12. The process according to claim 11, characterized in that the coagulation is carried out at 40—60°C.

13. The process according to claims 8 to 12 as disclosed in claims 5 to 7, characterized in that the coagulated polymer dispersion is foamed by heating in a warm water bath, steam bath or a quick heat transfer oven, as disclosed in claims 5—8.

14. The process according to claims 1 to 13, characterized in that polybutadiene latex, polybutadiene styrene copolymer latex, polybutadiene acrylonitrile copolymer latex, polystyrene butadiene acrylonitrile terpolymer latex, polychloroprene latex, polyacrylate latex, polyvinyl acetate latex, polyurethane latex or a mixture thereof is used as polymer dispersion.

15. The process according to claim 14, characterized in that polyurethane latex is used as polymer dispersion.

16. The process according to claim 3 to 15, characterized in that the heat-coagulant is built into the polymer backbone.

17. The process according to claim 16, characterized in that 0.5—10 mole % of a poly (ethylene oxide) diol is built into the polyurethane molecule as heat-coagulant.

18. The process according to claim 17, characterized in that 1.5—5.0 mole % is built in.

19. The process according to claims 14 to 18, characterized in that an impregnating bath is used, which contains 5—30%, by weight, of the polymer dispersion.

20. The process according to claim 19, characterized in that the impregnating bath contains 5—15%, by weight, of the polymer dispersion.

21. The process according to claim 3 or 16, characterized in that polyvinyl alkyl ether or a derivative thereof, a polyacetal, a polythio ether, a poly (ethylene oxide) or a derivative thereof, or

poly (propylene/ethylene oxide) or a derivative thereof is used as heat-coagulant.

22. The process according to claims 3 and 21, characterized in that the heat-coagulant is used in a concentration of 2—30%, by weight, based on the solid components of the polymer dispersion.

23. The process according to claim 22, characterized in that the heat-coagulant is used in a concentration of 2—10%, by weight.

24. The process according to claim 1, characterized in that a water insoluble solvent having a boiling point between -40°C and +50°C is used as physical foaming agent.

25. The process according to claim 24, characterized in that a water insoluble solvent having a boiling point between -20°C and +30°C is used.

26. The process according to claims 24 or 25, characterized in that a halogenated saturated or unsaturated hydrocarbon, a saturated or unsaturated aromatic hydrocarbon, whether or not encapsulated in a polymer film, is used as water insoluble solvent.

27. Coagulé obtained by the use of the process according to any one of the preceding claims.

Patentansprüche

1. Verfahren zur Herstellung eines koagulierten Materials durch Imprägnieren eines Textilgewebes in einem eine koagulierbare Polymerdispersion-Zusammensetzung enthaltenden Imprägnierbades und anschließende Koagulation in einem wässrigen Koagulationsbad, dadurch gekennzeichnet, daß das Imprägnierungsbad ein physikalisches Schäumungsmittel enthält, welches in Wasser unlöslich ist und in welchem gleichzeitig mit der Koagulation oder sofort danach ein Schäumen bei einer Temperatur oberhalb 70°C auftritt.

2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß die Koagulation und/oder das Schäumen durch Erhitzen des imprägnierten Textilgewebes durchgeführt werden.

3. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die Koagulation mit Hilfe eines Wärme-koagulierungsmittels durchgeführt wird.

4. Verfahren nach Anspruch 3, dadurch gekennzeichnet, daß die Koagulation und das Schäumen bei einer Temperatur von 85 bis 100°C durchgeführt werden.

5. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die Koagulation und das Schäumen in einer Dampfkammer bei 100 bis 130°C durchgeführt werden.

6. Verfahren nach Anspruch 5, dadurch gekennzeichnet, daß die Koagulation und das Schäumen in einer Dampfkammer bei 100 bis 110°C durchgeführt werden.

7. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die Koagulation und das Schäumen in einem Schnellwärmeübertragungssofen durchgeführt werden.

8. Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß die Koagulation mit Hilfe eines geeigneten Elektrolyten und bei einem pH-Wert



durchgeführt wird, der in Verbindung mit der Polymerdispersion benutzbar ist.

9. Verfahren nach Anspruch 8, dadurch gekennzeichnet, daß die Koagulation bei einem pH < 7 durch Verwendung von anionischen Polymerdispersionen durchgeführt wird.

10. Verfahren nach Anspruch 8, dadurch gekennzeichnet, daß die Koagulation bei einem pH > 7 durch Verwendung kationischer Polymerdispersionen durchgeführt wird.

11. Verfahren nach den Ansprüchen 8 bis 10, dadurch gekennzeichnet, daß die Koagulation bei einer Temperatur von 15 bis 75°C durchgeführt wird.

12. Verfahren nach Anspruch 11, dadurch gekennzeichnet, daß die Koagulation bei 40 bis 60°C durchgeführt wird.

13. Verfahren nach den Ansprüchen 8 bis 12, dadurch gekennzeichnet, daß die koagulierte Polymerdispersion durch Erhitzen in einem Warmwasserbad, Dampfbad oder einem Schnellwärmeübertragungssofen geschäumt wird, wie es in den Ansprüchen 5 bis 7 angegeben ist.

14. Verfahren nach den Ansprüchen 1 bis 13, dadurch gekennzeichnet, daß Polybutadienlatex, Polybutadienstyrolcopolymerlatex, Polybutadienacrylnitrilcopolymerlatex, Polystyrolbutadienacrylnitrilcopolymerlatex, Polychloroprenlatex, Polyacrylatlatex, Polyvinylacetatlatex, Polyurethanlatex oder Mischungen davon als Polymerdispersion verwendet werden.

15. Verfahren nach Anspruch 14, dadurch gekennzeichnet, daß Polyurethanlatex als Polymerdispersion verwendet wird.

16. Verfahren nach Anspruch 3 oder 15, dadurch gekennzeichnet, daß das Wärmekoagulationsmittel in das Polymerrückgrat eingebaut ist.

17. Verfahren nach Anspruch 16, dadurch gekennzeichnet, daß 0,5 bis 10 mol.% eines Poly(äthylenoxid)diol in das Polyurethanmolekül als Wärmekoagulationsmittel eingebaut ist.

18. Verfahren nach Anspruch 17, dadurch gekennzeichnet, daß 1,5 bis 5,0 mol.% eingebaut sind.

19. Verfahren nach den Ansprüchen 14 bis 18, dadurch gekennzeichnet, daß ein Imprägnierungsbad verwendet wird, das 5 bis 30 Gew.% der Polymerdispersion enthält.

20. Verfahren nach Anspruch 19, dadurch gekennzeichnet, daß das Imprägnierungsbad 5 bis 15 Gew.% der Polymerdispersion enthält.

21. Verfahren nach den Ansprüchen 3 oder 16, dadurch gekennzeichnet, daß Polyvinylalkyläther oder ein Derivat davon, ein Polyacetal, ein Polythioäther, ein Poly(äthylenoxid) oder ein Derivat davon, oder Poly(propylen/äthylenoxid) oder ein Derivat davon als Wärmekoagulationsmittel benutzt wird.

22. Verfahren nach den Ansprüchen 3 und 21, dadurch gekennzeichnet, daß das Wärmekoagulationsmittel in einer Konzentration von 2 bis 30 Gew.%, bezogen auf die festen Komponenten der Polymerdispersion, benutzt wird.

23. Verfahren nach Anspruch 22, dadurch

gekennzeichnet, daß das Wärmekoagulationsmittel in einer Konzentration von 2 bis 10 Gew.% verwendet wird.

24. Verfahren nach den Ansprüchen 1, dadurch gekennzeichnet, daß ein wasserunlösliches Lösungsmittel mit einem Siedepunkt zwischen -40°C und +50°C als physikalisches Schäumungsmittel verwendet wird.

25. Verfahren nach Anspruch 24, dadurch gekennzeichnet, daß ein wasserunlösliches Lösungsmittel mit einem Siedepunkt zwischen -20°C und +30°C verwendet wird.

26. Verfahren nach den Ansprüchen 24 bis 25, dadurch gekennzeichnet, daß ein halogenerter gesättigter oder ungesättigter Kohlenwasserstoff, ein gesättigter oder ungesättigter aromatischer Kohlenwasserstoff, ggf. eingebettet in einen Polymerfilm, als wasserunlösliches Lösungsmittel verwendet wird.

27. Koaguliertes Material erhalten unter Verwendung des Verfahrens nach einem der vorhergehenden Ansprüche.

Revendications

1. Procédé de préparation d'un matériau coagulé par imprégnation d'un tissu textile dans un bain d'imprégnation contenant une composition d'un polymère coagulable dispersé, suivie de la coagulation dans un bain de coagulation aqueux, caractérisé en ce que le bain d'imprégnation contient un agent moussant physique, qui est insoluble dans l'eau, et en ce que le moussage se produit simultanément avec la coagulation ou immédiatement après à une température supérieure à 70°C.

2. Procédé selon la revendication 1, caractérisé en ce que la coagulation et/ou le moussage sont mis en oeuvre par chauffage du tissu textile imprégné.

3. Procédé selon la revendication 2, caractérisé en ce que la coagulation est mise en oeuvre au moyen d'un coagulant à chaud.

4. Procédé selon la revendication 3, caractérisé en ce que la coagulation et le moussage sont mis en oeuvre à une température de 85—100°C.

5. Procédé selon la revendication 2, caractérisé en ce que la coagulation et le moussage sont mis en oeuvre dans une enceinte à vapeur à 100—130°C.

6. Procédé selon la revendication 5, caractérisé en ce que la coagulation et le moussage sont mis en oeuvre dans une enceinte à vapeur à 100—110°C.

7. Procédé selon la revendication 2, caractérisé en ce que la coagulation et le moussage sont mis en oeuvre dans un four de transfert thermique rapide.

8. Procédé selon la revendication 1, caractérisé en ce que la coagulation est mise en oeuvre au moyen d'un électrolyte convenable et à un pH qui est adapté à la dispersion de polymère à utiliser.

9. Procédé selon la revendication 8, caractérisé en ce que la coagulation est mise en oeuvre à un pH inférieur à 7 en utilisant des dispersions de



polymère anioniques.

10. Procédé selon la revendication 8, caractérisé en ce que la coagulation est mise en oeuvre à un pH supérieur à 7 en utilisant des dispersions de polymère cationiques.

11. Procédé selon l'une quelconque des revendications 8 à 10, caractérisé en ce que la coagulation est mise en oeuvre à une température de 15—75°C.

12. Procédé selon la revendication 11, caractérisé en ce que la coagulation est mise en oeuvre à 40—60°C.

13. Procédé selon les revendications 8 à 12, caractérisé en ce que la dispersion de polymère coagulé est transformée en mousse par chauffage dans un bain d'eau chaude, un bain de vapeur ou un four de transfert thermique rapide selon les revendications 5 à 7.

14. Procédé selon les revendications 1 à 13, caractérisé en ce que l'on utilise, comme dispersion de polymère, du latex de polybutadiène, du latex de copolymère polybutadiène styrène, du latex de copolymère polybutadiène acrylonitrile, du latex de terpolymère polystyrène-butadiène-acrylonitrile, du latex de polychloroprène, du latex polyacrylate, du latex poly(acétate de vinyle) du latex de polyuréthane ou un mélange de ceux-ci.

15. Procédé selon la revendication 14, caractérisé en ce que l'on utilise du latex de polyuréthane comme dispersion de polymère.

16. Procédé selon la revendication 3 ou 15, caractérisé en ce que le coagulant à chaud est incorporé dans le squelette polymère.

17. Procédé selon la revendication 16, caractérisé en ce que 0,5 à 10% en mole d'un poly(oxyde d'éthylène) diol est incorporé dans la molécule de polyuréthane comme coagulant à chaud.

18. Procédé selon la revendication 17, caractérisé en ce que 1,5 à 5% en mole est incorporé.

19. Procédé selon les revendications 14 à 18, caractérisé en ce que l'on utilise un bain d'imprégnation qui contient de 5 à 30% en poids de la dispersion de polymère.

20. Procédé selon la revendication 19, caractérisé en ce que le bain d'imprégnation contient de 5 à 15% en poids de la dispersion de polymère.

21. Procédé selon les revendications 3 ou 16, caractérisé en ce que l'on utilise, comme coagulant à chaud, un éther de polyvinylalkyle ou un dérivé de celui-ci, un polyacétal, un polythioéther, un poly(oxyde d'éthylène) ou un dérivé de celui-ci, un poly(oxyde de propylène/éthylène) ou un dérivé de celui-ci.

22. Procédé selon les revendications 3 et 21, caractérisé en ce que le coagulant à chaud est utilisé à une concentration de 2 à 30% en poids par rapport aux composants solides de la dispersion de polymère.

23. Procédé selon la revendication 22, caractérisé en ce que le coagulant à chaud est utilisé à une concentration de 2 à 10% en poids.

24. Procédé selon la revendication 1, caractérisé en ce que l'on utilise un solvant hydro-insoluble ayant un point d'ébullition compris entre -40°C et +50°C comme agent moussant physique.

25. Procédé selon la revendication 24, caractérisé en ce que l'on utilise un solvant hydro-insoluble ayant un point d'ébullition compris entre -20°C et +30°C.

26. Procédé selon les revendications 24 à 25, caractérisé en ce que l'on utilise, comme solvant hydro-insoluble, un hydrocarbure saturé ou insaturé halogéné, un hydrocarbure aromatique saturé ou insaturé encapsulé ou non dans un film de polymère.

27. Matériau coagulé issu de la mise en oeuvre du procédé selon l'une quelconque des revendications précédentes.

