

PROCESS FOR INDUSTRIALLY PRODUCING AN AROMATIC CARBONATE

Technical Field

The present invention relates to an industrial process for the production of an aromatic carbonate. More particularly, the present invention relates to an industrial process for the production of a large amount of an aromatic carbonate containing diaryl carbonate as a main product, which is useful as a raw material of a transesterification method polycarbonate by subjecting a dialkyl carbonate and an aromatic monohydroxy compound to transesterification reaction in two continuous multi-stage distillation columns in each of which a catalyst is present.

Background Art

An aromatic carbonates is important as a raw material for the production of aromatic polycarbonate which is the most widely used engineering plastic, without using toxic phosgene. As a process for producing an aromatic carbonate, a process of reacting an aromatic monohydroxy compound with phosgene has been known from long ago, and has also been the subject of a variety of studies in recent years. However, this process has the problem of using phosgene, and in addition chlorinated impurities that are difficult to separate out are present in the aromatic carbonate produced using this process, and hence the aromatic carbonate cannot be used as the raw material for the production of the aromatic polycarbonate. Because such chlorinated impurities markedly inhibit the polymerization reaction in the transesterification method which is carried out in the presence of an extremely small amount of a basic catalyst; for example, even if such chlorinated impurities are present in an amount of only 1 ppm, the polymerization hardly proceeds at all. To make the aromatic carbonate capable of being used as the raw material of

polycarbonate of the transesterification method, troublesome multi-stage separation/purification processes such as enough washing with a dilute aqueous alkaline solution and hot water, oil/water separation, distillation and so on are thus required. Furthermore, the yield of the aromatic carbonate decreases due to hydrolysis loss during this separation/purification processes. Therefore, there are many problems in carrying out this method economically on an industrial scale.

On the other hand, a process for producing aromatic carbonates through transesterification reactions between a dialkyl carbonate and an aromatic monohydroxy compound is also known. However, such transesterification reactions are all equilibrium reactions. Since the equilibriums are biased extremely toward the original system and the reaction rates are slow, and hence there have been many difficulties in producing aromatic carbonates industrially in large amounts using this method. Several proposals have been made to improve on the above difficulties, but most of these have related to development of a catalyst to increase the reaction rate. Many metal compounds have been proposed as catalysts for this type of transesterification reaction. For example, Lewis acids such as a transition metal halide and Lewis acid-forming compounds (see Patent Documents 1:

Japanese Patent Application Laid-Open No. 51-105032, Japanese Patent Application Laid-Open No. 56-123948, Japanese Patent Application Laid-Open No. 56-123949 (corresponding to West German Patent Application No. 2528412, British Patent No. 1499530, and U.S. Patent No. 4182726), Japanese Patent Application Laid-Open No. 51-75044 (corresponding to West German Patent Application No. 2552907, and U.S. Patent No. 4045464)), tin compounds such as an organo-tin alkoxide and an organo-tin oxides (see Patent Documents 2: Japanese Patent Application Laid-Open No. 54-48733 (corresponding to West German Patent Application No. 2736062), Japanese Patent Application Laid-Open No. 54-63023, Japanese Patent Application

Laid-Open No. 60-169444 (corresponding to U.S. Patent No. 4554110), Japanese Patent Application Laid-Open No. 60-169445 (corresponding to U.S. Patent No. 4552704), Japanese Patent Application Laid-Open No. 62-277345, Japanese Patent Application Laid-Open No. 1-265063, Japanese Patent Application Laid-Open No.

- 5 60-169444 (corresponding to U.S. Patent No. 4554110), Japanese Patent Application Laid-Open No. 60-169445 (corresponding to U.S. Patent No. 4552704), Japanese Patent Application Laid-Open No. 62-277345, Japanese Patent Application Laid-Open No. 1-265063), salts and alkoxides of alkali metals and alkaline earth metals (see Patent Document 3: Japanese Patent Application Laid-Open No.
- 10 57-176932), lead compounds (see Patent Documents 4: Japanese Patent Application Laid-Open No. 57-176932, Japanese Patent Application Laid-Open No. 1-93560), complexes of metals such as copper, iron and zirconium (see Patent Document 5: Japanese Patent Application Laid-Open No. 57-183745), titanate acid esters (see Patent Documents 6: Japanese Patent Application Laid-Open No.
- 15 58-185536 (corresponding to U.S. Patent No. 4410464), Japanese Patent Application Laid-Open No. 1-265062), mixtures of a Lewis acid and a protonic acid (see Patent Document 7: Japanese Patent Application Laid-Open No. 60-173016 (corresponding to U.S. Patent No. 4609501)), compounds of Sc, Mo, Mn, Bi, Te or the like (see Patent Document 8: Japanese Patent Application Laid-Open No.
- 20 1-265064), ferric acetate (see Patent Document 9: Japanese Patent Application Laid-Open No. 61-172852), and so on have been proposed. However, the problem of the disadvantageous equilibrium cannot be solved merely by developing the catalyst, and hence there are very many issues to be solved including the reaction system in order to provide a process for the industrial production aiming for mass
- 25 production.

Attempts have also been made to devise a reaction system so as to shift the

equilibrium toward the product system as much as possible, and thus improve the yield of the aromatic carbonates. For example, for the reaction between dimethyl carbonate and phenol, there have been proposed a method in which by-produced methanol is distilled off by azeotropy together with an azeotrope-forming agent (see

- 5 Patent Document 10: Japanese Patent Application Laid-Open No. 54-48732 (corresponding to West German Patent Application No. 736063, and U.S. Patent No. 4252737)), and a method in which the methanol produced as the by-product is removed by being adsorbed onto a molecular sieve (see Patent Document 11: Japanese Patent Application Laid-Open No. 58-185536 (corresponding to U.S. Patent No. 410464)). Moreover, a method has also been proposed in which, using an apparatus in which a distillation column is provided on top of a reactor, an alcohol produced as the by-product in the reaction is separated off from the reaction mixture, and at the same time unreacted starting material that evaporates is separated off by distillation (see Patent Documents 12: examples in Japanese Patent Application
- 15 Laid-Open No. 56-123948 (corresponding to U.S. Patent No. 4182726), examples in Japanese Patent Application Laid-Open No. 56-25138, examples in Japanese Patent Application Laid-Open No. 60-169444 (corresponding to U.S. Patent No. 4554110), examples in Japanese Patent Application Laid-Open No. 60-169445 (corresponding to U.S. Patent No. 4552704), examples in Japanese Patent Application Laid-Open
- 20 No. 60-173016 (corresponding to U.S. Patent No. 4609501), examples in Japanese Patent Application Laid-Open No. 61-172852, examples in Japanese Patent Application Laid-Open No. 61-291545, examples in Japanese Patent Application Laid-Open No. 62-277345).

However, these reaction systems are basically batch system or switchover

25 system. Because there is the limitation in the improvement of the reaction rate through catalyst development for such a transesterification reaction, and the reaction

rate is still slow, and thus it has been thought that a batch system is preferable to a continuous system. Of these, a continuous stirring tank reactor (CSTR) system in which a distillation column is provided on top of a reactor has been proposed as a continuous system, but there are problems such as the reaction rate being slow, and
5 a gas-liquid interface in the reactor being small, based on the volume of the liquid. Hence it is not possible to make the conversion high. Accordingly, it is difficult to attain the object of producing the aromatic carbonate continuously in large amounts stably for a prolonged period of time by means of the above-mentioned methods, and many issues remain to be resolved before economical industrial implementation
10 is possible.

The present inventors have developed reactive distillation methods in which such a transesterification reaction is carried out in a continuous multi-stage distillation column simultaneously with separation by distillation, and have been the first in the world to disclose that such a reactive distillation system is useful for such
15 a transesterification reaction, for example a reactive distillation method in which a dialkyl carbonate and an aromatic hydroxy compound are continuously fed into a multi-stage distillation column, and the reaction is carried out continuously inside the column in which a catalyst is present, while continuously withdrawing a low boiling point component containing an alcohol produced as a by-product by distillation and
20 continuously withdrawing a component containing a produced alkyl aryl carbonate from a lower portion of the column (see Patent Document 13: Japanese Patent Application Laid-Open No. 3-291257), a reactive distillation method in which an alkyl aryl carbonate is continuously fed into the multi-stage distillation column, and the reaction is carried out continuously inside the column in which a catalyst is present,
25 while continuously withdrawing by distillation a low boiling point component containing a dialkyl carbonate produced as a by-product and continuously

withdrawing a component containing a produced diaryl carbonate from a lower portion of the column (see Patent Document 14: Japanese Patent Application Laid-Open No. 4-9358), a reactive distillation method in which these reactions are carried out using two continuous multi-stage distillation columns, and hence a diaryl carbonate is produced continuously while efficiently recycling a dialkyl carbonate produced as a by-product (see Patent Document 15: Japanese Patent Application Laid-Open No. 4-211038), and a reactive distillation method in which a dialkyl carbonate and an aromatic hydroxy compound or the like are continuously fed into the multi-stage distillation column, and a liquid that flows down through the column is withdrawn from a side outlet provided at an intermediate stage and/or a lowermost stage of the distillation column, and is introduced into a reactor provided outside the distillation column so as to bring about reaction, and is then introduced back in through a circulating inlet provided at a stage above the stage where the outlet is provided, whereby reaction is carried out in both the reactor and the distillation column (see Patent Documents 16: Japanese Patent Application Laid-Open No. 4-224547, Japanese Patent Application Laid-Open No. 4-230242, Japanese Patent Application Laid-Open No. 4-235951).

These reactive distillation methods proposed by the present inventors are the first to enable aromatic carbonates to be produced continuously and efficiently, and many similar reactive distillation systems based on the above disclosures have been proposed thereafter (see Patent Documents 17 to 32: Patent Document 17: International Publication No. 00/18720 (corresponding to U.S. Patent No. 5362901), Patent Document 18: Italian Patent No. 01255746, Patent Document 19: Japanese Patent Application Laid-Open No. 6-9506 (corresponding to European Patent No. 0560159, and U.S. Patent No. 5282965), Patent Document 20: Japanese Patent Application Laid-Open No. 6-41022 (corresponding to European Patent No. 0572870,

and U.S. Patent No. 5362901), Patent Documents 21: Japanese Patent Application Laid-Open No. 6-157424 (corresponding to European Patent No. 0582931, and U.S. Patent No. 5334742), Japanese Patent Application Laid-Open No. 6-184058 (corresponding to European Patent No. 0582930, and U.S. Patent No. 5344954),

5 Patent Document 22: Japanese Patent Application Laid-Open No. 7-304713, Patent Document 23: Japanese Patent Application Laid-Open No. 9-40616, Patent Document 24: Japanese Patent Application Laid-Open No. 9-59225, Patent Document 25: Japanese Patent Application Laid-Open No. 9-110805, Patent Document 26: Japanese Patent Application Laid-Open No. 9-165357, Patent

10 Document 27: Japanese Patent Application Laid-Open No. 9-173819, Patent Documents 28: Japanese Patent Application Laid-Open No. 9-176094, Japanese Patent Application Laid-Open No. 2000-191596, Japanese Patent Application Laid-Open No. 2000-191597, Patent Document 29: Japanese Patent Application Laid-Open No. 9-194436 (corresponding to European Patent No. 0785184, and U.S.

15 Patent No. 5705673), Patent Document 30: International Publication No. 00/18720 (corresponding to U.S. Patent No. 6093842), Patent Documents 31: Japanese Patent Application Laid-Open No. 2001-64234, Japanese Patent Application Laid-Open No. 2001-64235, Patent Document 32: International Publication No. 02/40439 (corresponding to U.S. Patent No. 6596894, U.S. Patent No. 6596895, and

20 U.S. Patent No. 6600061)).

Among reactive distillation systems, the present applicants have further proposed, as a method that enables highly pure aromatic carbonates to be produced stably for a prolonged period of time without a large amount of a catalyst being required, a method in which high boiling point material containing a catalyst

25 component is reacted with an active substance and then separated off, and the catalyst component is recycled (see Patent Documents 31: Japanese Patent

Application Laid-Open No. 2001-64234, Japanese Patent Application Laid-Open No. 2001-64235), and a method carried out while keeping a weight ratio of a polyhydric aromatic hydroxy compound in the reaction system to a catalyst metal at not more than 2.0 (see Patent Document 32: International Publication No. 02/40439

5 (corresponding to U.S. Patent No. 6596894, U.S. Patent No. 6596895, and U.S. Patent No. 6600061)). Furthermore, the present inventors have proposed a method in which 70 to 99 % by weight of phenol produced as a by-product in a polymerization process is used as a starting material, and diphenyl carbonate can be produced by means of the reactive distillation method. This diphenyl carbonate can
10 be used as the raw material for polymerization of aromatic polycarbonates (see Patent Document 33: International Publication No. 97/11049 (corresponding to European Patent No. 0855384, and U.S. Patent No. 5872275)).

However, in all of these prior art documents in which the production of aromatic carbonates using the reactive distillation method is proposed, there is no
15 disclosure whatsoever of a specific process or apparatus enabling mass production on an industrial scale (e.g. not less than 1 ton per hour), nor is there any description suggesting such a process or apparatus. For example, the descriptions regarding the heights (H_1 and H_2 , respectively: cm), the diameters (D_1 and D_2 , respectively: cm), the numbers of stages (n_1 and n_2 , respectively) of the pair of reactive distillation
20 columns and the feeding rates of the raw material (Q_1 and Q_2 , respectively: kg/hr) disclosed for producing diphenyl carbonate (DPC) from dimethyl carbonate and phenol are as summarized in the following table.

Table 1

H_1	D_1	n_1	Q_1	H_2	D_2	n_2	Q_2	PATENT DOCUMENT
600	25	20	66	600	25	20	23	15
350	2.8	-	0.2	305	5~10	15+ PACKING	0.6	21
500	5	50	0.6	400	8	50	0.6	23
100	4	-	1.4	200	4	-	0.8	24
300	5	40	1.5	-	5	25	0.7	28
1200	20	40	86	600	25	20	31	33 34
600	-	20	66	600	-	20	22	35

See Patent Document 34: Japanese Patent Application Laid-Open No. 11-92429
(corresponding to European Patent No. 1016648, and U.S. Patent No. 6262210)

- 5 See Patent document 35: Japanese Patent Application Laid-Open No. 9-255772
(corresponding to European Patent No. 0892001, and U.S. Patent No. 5747609)

In other words, a pair of the biggest continuous multi-stage distillation columns used when carrying out this reaction using the reactive distillation system are those disclosed by the present applicants in Patent Documents 33 and 34. As can be seen from Table 1, the maximum values of the various conditions for the continuous multi-stage distillation columns disclosed for the above reaction are $H_1 = 1200$ cm, $H_2 = 600$ cm, $D_1 = 20$ cm, $D_2 = 25$ cm, $n_1 = n_2 = 50$ (Patent Document 23), $Q_1 = 86$ kg/hr, and $Q_2 = 31$ kg/hr, and the amount of diphenyl carbonate produced has not exceeded approximately 6.7 kg/hr, which is not an amount produced on an industrial scale.

Disclosure of the Invention

It is an object of the present invention to provide a specific process that

enables aromatic carbonates containing a diaryl carbonate as a main product to be produced with high selectivity and high productivity stably for a prolonged period of time on an industrial scale of not less than 1 ton per hour using two continuous multi-stage distillation columns from a dialkyl carbonate and an aromatic monohydroxy compound containing specific amounts of an alcohol and an aromatic carbonate.

Since the present inventors disclosed a process for producing aromatic carbonates using a continuous multi-stage distillation column, various proposals regarding processes for the production of aromatic carbonates by means of a reactive distillation method have been made. However, these have all been on a small scale and short operating time laboratory level, and there have been no disclosures whatsoever on a specific process or apparatus enabling mass production on an industrial scale. In view of these circumstances, the present inventors carried out studies aimed at discovering a specific process enabling an aromatic carbonate containing a diaryl carbonate as a main product to be produced with high selectivity and high productivity stably for a prolonged period of time on an industrial scale of not less than 1 ton per hour. As a result, the present inventors have reached to the present invention.

That is, in the first aspect of the present invention, there is provided:

1. A process for the production of an aromatic carbonate containing a diaryl carbonate as a main product from a dialkyl carbonate and an aromatic monohydroxy compound as a starting material, which comprises the steps of:

(i) continuously feeding said starting material into a first continuous multi-stage distillation column in which a catalyst is present;

(ii) carrying out the reaction in said first column to produce an alcohol and an alkyl aryl carbonate;

(iii) continuously withdrawing a first column low boiling point reaction mixture containing a produced alcohol from an upper portion of said first column in a gaseous form while continuously withdrawing a first column high boiling point reaction mixture containing an alkyl aryl carbonate from a lower portion of said first column in a liquid form;

(IV) continuously feeding said first column high boiling point reaction mixture into a second continuous multi-stage distillation column in which a catalyst is present and which is connected to said first column while carrying out the reaction in said second column to produce a dialkyl carbonate and a diaryl carbonate;

(V) continuously withdrawing a second column low boiling point reaction mixture containing said produced dialkyl carbonate from an upper portion of said second column in a gaseous form while continuously withdrawing a second column high boiling point reaction mixture containing said produced diaryl carbonate from a lower portion of said second column in a liquid form; wherein

(a) said starting material which is fed continuously into said first continuous multi-stage distillation column

(1) has a molar ratio of the dialkyl carbonate to the aromatic monohydroxy compound is in a range of from 0.1 to 10; and

(2) contains 0.01 to 5 % by weight of said alcohol and 0.01 to 5 % by weight of said alkyl aryl carbonate and/or said diaryl carbonate, based on the total weight of said starting material;

(b) said first continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_1 (cm) and an inside diameter D_1 (cm), and having an internal with a number of stages n_1 thereinside, and has a gas outlet having an inside diameter d_{11} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid

outlet having an inside diameter d_{12} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

5 (1) said length L_1 (cm) satisfies the following formula (1),

$$1500 \leq L_1 \leq 8000 \quad (1),$$

(2) said inside diameter D_1 (cm) of the column satisfies the following formula (2),

$$100 \leq D_1 \leq 2000 \quad (2),$$

10 (3) a ratio of said length L_1 (cm) to said inside diameter D_1 (cm) of the column satisfies the following formula (3),

$$2 \leq L_1 / D_1 \leq 40 \quad (3),$$

(4) said number of stages n_1 satisfies the following formula (4),

$$20 \leq n_1 \leq 120 \quad (4),$$

15 (5) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{11} (cm) of the gas outlet satisfies the following formula (5),

$$5 \leq D_1 / d_{11} \leq 30 \quad (5), \text{ and}$$

(6) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{12} (cm) of the liquid outlet satisfies the following formula (6),

20 $3 \leq D_1 / d_{12} \leq 20 \quad (6);$

(c) said second continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_2 (cm) and an inside diameter D_2 (cm), and having an internal with a number of stages n_2 therein, and has a gas outlet having an inside diameter d_{21} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet having an inside diameter d_{22} (cm) at the bottom of the column or in a

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lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_2 (cm) satisfies the following formula (7),

$$1500 \leq L_2 \leq 8000 \quad (7),$$

(2) said inside diameter D_2 (cm) of the column satisfies the following formula (8),

$$100 \leq D_2 \leq 2000 \quad (8),$$

(3) a ratio of the length L_2 (cm) to said inside diameter D_2 (cm) of the column satisfies the following formula (9),

$$2 \leq L_2 / D_2 \leq 40 \quad (9),$$

(4) said number of stages n_2 satisfies the following formula (10),

$$10 \leq n_2 \leq 80 \quad (10),$$

(5) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{21} (cm) of the gas outlet satisfies the following formula (11),

$$2 \leq D_2 / d_{21} \leq 15 \quad (11), \text{ and}$$

(6) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{22} (cm) of the liquid outlet satisfies the following formula (12),

$$5 \leq D_2 / d_{22} \leq 30 \quad (12),$$

2. The process according to item 1, wherein distillation is carried out simultaneously in said step (ii) and said step (iv),

3. The process according to item 1 or 2, wherein an amount of said diaryl carbonate produced is not less than 1 ton per hour.

In another aspect of the process according to the present invention, there is provided:

4. In a process for the production of an aromatic carbonate containing a diaryl

carbonate as a main product in which the aromatic carbonate containing the diaryl carbonate as the main product are produced continuously by taking a mixture of a dialkyl carbonate and an aromatic monohydroxy compound as a starting material, continuously feeding the starting material into a first continuous multi-stage

5 distillation column in which a catalyst is present, carrying out the reaction and the distillation simultaneously said the first column, continuously withdrawing a first column low boiling point reaction mixture containing a produced alcohol from an upper portion of said first column in a gaseous form, continuously withdrawing a first column high boiling point reaction mixture containing a produced alkyl aryl carbonate
10 from a lower portion of said first column in a liquid form, continuously feeding the first column high boiling point reaction mixture into a second continuous multi-stage distillation column in which a catalyst is present, carrying out the reaction and the distillation simultaneously in said second column, continuously withdrawing a second column low boiling point reaction mixture containing a produced dialkyl carbonate
15 from an upper portion of said second column in a gaseous form, continuously withdrawing a second column high boiling point reaction mixture containing a produced diaryl carbonate from a lower portion of said second column in a liquid form while continuously feeding the second column low boiling point reaction mixture containing the dialkyl carbonate into the first continuous multi-stage distillation
20 column, the improvement in which:

(a) said starting material which is fed continuously into said first continuous multi-stage distillation column

(1) has a molar ratio of the dialkyl carbonate to the aromatic monohydroxy compound is in a range of from 0.1 to 10; and

25 (2) contains 0.01 to 5 % by weight of said alcohol and 0.01 to 5 % by weight of said alkyl aryl carbonate and/or said diaryl carbonate, based on the total

weight of said starting material;

(b) said first continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_1 (cm) and an inside diameter D_1 (cm), and having an internal with a number of stages n_1 thereinside, and has a gas outlet having an inside diameter d_{11} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet having an inside diameter d_{12} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_1 (cm) satisfies the following formula (1),

$$1500 \leq L_1 \leq 8000 \quad (1),$$

(2) said inside diameter D_1 (cm) of the column satisfies the following formula (2),

$$100 \leq D_1 \leq 2000 \quad (2),$$

(3) a ratio of said length L_1 (cm) to said inside diameter D_1 (cm) of the column satisfies the following formula (3),

$$2 \leq L_1 / D_1 \leq 40 \quad (3),$$

(4) said number of stages n_1 satisfies the following formula (4),

$$20 \leq n_1 \leq 120 \quad (4),$$

(5) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{11} (cm) of the gas outlet satisfies the following formula (5),

$$5 \leq D_1 / d_{11} \leq 30 \quad (5), \text{ and}$$

(6) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{12} (cm) of the liquid outlet satisfies the following formula (6),

$$3 \leq D_1 / d_{12} \leq 20 \quad (6);$$

(c) said second continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_2 (cm) and an inside diameter D_2 (cm), and having an internal with a number of stages n_2 thereinside, and has a gas outlet having an inside diameter d_{21} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet having an inside diameter d_{22} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_2 (cm) satisfies the following formula (7),

$$1500 \leq L_2 \leq 8000 \quad (7),$$

(2) said inside diameter D_2 (cm) of the column satisfies the following formula (8),

$$100 \leq D_2 \leq 2000 \quad (8),$$

(3) a ratio of the length L_2 (cm) to said inside diameter D_2 (cm) of the column satisfies the following formula (9),

$$2 \leq L_2 / D_2 \leq 40 \quad (9),$$

(4) said number of stages n_2 satisfies the following formula (10),

$$10 \leq n_2 \leq 80 \quad (10),$$

(5) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{21} (cm) of the gas outlet satisfies the following formula (11),

$$2 \leq D_2 / d_{21} \leq 15 \quad (11), \text{ and}$$

(6) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{22} (cm) of the liquid outlet satisfies the following formula (12),

$$5 \leq D_2 / d_{22} \leq 30 \quad (12),$$

5. The process according to item 4, wherein an amount produced of the diaryl

carbonate is not less than 1 ton per hour,

6. The process according to any one of items 1 to 5, wherein said starting material further contains 0.5 to 15 % by weight of alkyl aryl ether, based on the total weight of said starting material.

5 7. The process according to any one of items 1 to 6, wherein d_{11} and d_{12} satisfy the following formula (13), and d_{21} and d_{22} satisfy the following formula (14)

$$1 \leq d_{12} / d_{11} \leq 5 \quad (13)$$

$$1 \leq d_{21} / d_{22} \leq 6 \quad (14),$$

8. The process according to any one of items 1 to 7, wherein L_1 , D_1 , L_1 / D_1 , n_1 , D_1 / d_{11} , and D_1 / d_{12} for said first continuous multi-stage distillation column satisfy the following formulae: $2000 \leq L_1 \leq 6000$, $150 \leq D_1 \leq 1000$, $3 \leq L_1 / D_1 \leq 30$, $30 \leq n_1 \leq 100$, $8 \leq D_1 / d_{11} \leq 25$, and $5 \leq D_1 / d_{12} \leq 18$, respectively, and

15 L_2 , D_2 , L_2 / D_2 , n_2 , D_2 / d_{21} , and D_2 / d_{22} for said second continuous multi-stage distillation column satisfy the following formulae: $2000 \leq L_2 \leq 6000$, $150 \leq D_2 \leq 1000$, $3 \leq L_2 / D_2 \leq 30$, $15 \leq n_2 \leq 60$, $2.5 \leq D_2 / d_{21} \leq 12$, and $7 \leq D_2 / d_{22} \leq 25$, respectively,

9. The process according to any one of items 1 to 8, wherein L_1 , D_1 , L_1 / D_1 , n_1 , D_1 / d_{11} , and D_1 / d_{12} for said first continuous multi-stage distillation column satisfy the following formulae: $2500 \leq L_1 \leq 5000$, $200 \leq D_1 \leq 800$, $5 \leq L_1 / D_1 \leq 15$, $40 \leq n_1 \leq 90$, $10 \leq D_1 / d_{11} \leq 25$, and $7 \leq D_1 / d_{12} \leq 15$, respectively, and

25 L_2 , D_2 , L_2 / D_2 , n_2 , D_2 / d_{21} , and D_2 / d_{22} for said second continuous multi-stage distillation column satisfy the following formulae: $2500 \leq L_2 \leq 5000$, $200 \leq D_2 \leq 800$, $5 \leq L_2 / D_2 \leq 15$, $20 \leq n_2 \leq 50$, $3 \leq D_2 / d_{21} \leq 10$, and $9 \leq D_2 / d_{22} \leq 20$, respectively,

10. The process according to any one of items 1 to 9, wherein each of said first

continuous multi-stage distillation column and said second continuous multi-stage distillation column is a distillation column having a tray and/or a packing as the internal,

11. The process according to item 10, wherein said first continuous multi-stage distillation column is a plate-type distillation column having the tray as the internal, and said second continuous multi-stage distillation column is a distillation column having both the packing and the tray as the internal,

12. The process according to item 10 or 11, wherein each of the trays in said first continuous multi-stage distillation column and said second continuous multi-stage distillation column is a sieve tray having a sieve portion and a down comer portion,

13. The process according to item 12, wherein said sieve tray has 100 to 1000 holes/m² in the sieve portion,

14. The process according to item 12 or 13, wherein the cross-sectional area per hole of said sieve tray is in a range of from 0.5 to 5 cm²,

15. The process according to item 10 or 11, wherein said second continuous multi-stage distillation column is a distillation column having, as said internal, the packing in an upper portion of the column, and the tray in a lower portion of the column,

16. The process according to any one of items 10 to 15, wherein said packing of said internal in said second continuous multi-stage distillation column is one or more of a structured packing,

17. The process according to item 16, wherein said structured packing in said second continuous multi-stage distillation column is of at least one selected from the group consisting of Mellapak, Gempak, TECHNO-PAK, FLEXI-PAK, a Sulzer packing, a Goodroll packing and a Glitchgrid,

18. The process according to any one of items 1 to 17, wherein said first

continuous multi-stage distillation column comprises two or more of distillation columns,

19. The process according to any one of items 1 to 18, wherein said second continuous multi-stage distillation column comprises two or more of distillation
5 columns.

In the second aspect of the present invention, there is provided:

20. An aromatic carbonate comprising a halogen content of not more than 0.1 ppm, produced by the process according to any one of items 1 to 19.

10 Advantageous Effects of the Invention

It has been discovered that according to the present invention, from a dialkyl carbonate and an aromatic monohydroxy compound, an aromatic carbonate containing a diaryl carbonate as a main product can be produced on an industrial scale of not less than 1 ton per hour, preferably not less than 2 tons per hour, more
15 preferably not less than 3 tons per hour, with a high selectivity of not less than 95%, preferably not less than 97%, more preferably not less than 99%, stably for a prolonged period of time of not less than 2000 hours, preferably not less than 3000 hours, more preferably not less than 5000 hours. A diaryl carbonate obtained by
20 subjecting the aromatic carbonates containing the diaryl carbonate as a main component obtained through the present invention to separation/purification through distillation or the like is of high purity, and is useful as a raw material of a transesterification method polycarbonate or polyester carbonate or the like, or as a raw material of a non-phosgene method isocyanate or urethane or the like.
Moreover, according to the present invention, because a starting material and
25 catalyst not containing a halogen are generally used, the diaryl carbonate obtained has a halogen content of not more than 0.1 ppm, preferably not more than 10 ppb,

more preferably not more than 1 ppb.

Brief Description of the Drawing

FIG. 1 is a schematic view of a first continuous multi-stage distillation column for carrying out the present invention, the distillation column having an internal provided inside a trunk portion thereof;

FIG. 2 is a schematic view of a second continuous multi-stage distillation column preferable for carrying out the present invention, the distillation column having, provided inside a trunk portion thereof, an internal comprising a structured packing (6-1) in an upper portion and a sieve tray (6-2) in a lower portion; and

FIG. 3 is a schematic view of an apparatus suitable for carrying out the present invention.

Description of Reference Numerals:

1: gas outlet, 2: liquid outlet, 3, 4, 15, 19, 25, 29: inlet, 5: end plate, 6: internal, 6-1: internal (packing), 6-2: internal (tray), 7: trunk portion, L_1 , L_2 : length of trunk portion (cm), D_1 , D_2 : inside diameter of trunk portion (cm), d_{11} , d_{21} : inside diameter of gas outlet (cm), d_{12} , d_{22} : inside diameter of liquid outlet (cm), 101: the first multi-stage distillation column, 201: the second multi-stage distillation column, 11, 12, 21: inlet, 13, 23: a column top gas outlet, 14, 24, 18, 28: heat exchanger, 15, 25: reflux liquid inlet, 16, 26: a column top component outlet, 17, 27: a column bottom liquid outlet, 31: a column bottom component outlet of the second multi-stage distillation column.

Best Mode for Carrying out the Invention

In the following, the present invention is described in detail.

A dialkyl carbonate used in the present invention is a compound represented

by the following formula (15).



wherein R^1 represents an alkyl group having 1 to 10 carbon atoms, an alicyclic group having 3 to 10 carbon atoms, or an aralkyl group having 6 to 10 carbon atoms.

- 5 Examples of R^1 include alkyl groups such as methyl, ethyl, propyl (isomers), allyl, butyl (isomers), butenyl (isomers), pentyl (isomers), hexyl (isomers), heptyl (isomers), octyl (isomers), nonyl (isomers), decyl (isomers) and cyclohexylmethyl; alicyclic groups such as cyclopropyl, cyclobutyl, cyclopentyl, cyclohexyl and cycloheptyl; and aralkyl groups such as benzyl, phenethyl (isomers), phenylpropyl (isomers),
10 phenylbutyl (isomers) and methylbenzyl (isomers). The above-mentioned alkyl groups, alicyclic groups and aralkyl groups may be substituted with other substituents such as a lower alkyl group, a lower alkoxy group, a cyano group or a halogen atom, and may also contain an unsaturated bond.

- Examples of dialkyl carbonates having such R^1 include dimethyl carbonate,
15 diethyl carbonate, dipropyl carbonate (isomers), diallyl carbonate, dibutenyl carbonate (isomers), dibutyl carbonate (isomers), dipentyl carbonate (isomers), dihexyl carbonate (isomers), diheptyl carbonate (isomers), dioctyl carbonate (isomers), dinonyl carbonate (isomers), didecyl carbonate (isomers), dicyclopentyl carbonate, dicyclohexyl carbonate, dicycloheptyl carbonate, dibenzyl carbonate,
20 diphenethyl carbonate (isomers), di(phenylpropyl) carbonate (isomers), di(phenylbutyl) carbonate (isomers), di(chlorobenzyl) carbonate (isomers), di(methoxybenzyl) carbonate (isomers), di(methoxymethyl) carbonate, di(methoxyethyl) carbonate (isomers), di(chloroethyl) carbonate (isomers) and di(cyanoethyl) carbonate (isomers).

- 25 Of these dialkyl carbonates, ones preferably used in the present invention are dialkyl carbonates in which R^1 is an alkyl group having not more than four carbon

atoms and not containing a halogen atom. A particularly preferable one is dimethyl carbonate. Moreover, of preferable dialkyl carbonates, particularly preferable ones are dialkyl carbonates produced in a state substantially not containing a halogen atom, for example, ones produced from an alkylene carbonate substantially not
 5 containing a halogen atom and an alcohol substantially not containing a halogen atom.

An aromatic monohydroxy compound used in the present invention is a compound represented by the following formula (16). The type of the aromatic monohydroxy compound is not limited, so long as the hydroxyl group is directly
 10 bonded to the aromatic group;



wherein Ar^1 represents an aromatic group having 5 to 30 carbon atoms. Examples of aromatic monohydroxy compounds having such Ar^1 include phenol; various alkylphenols such as cresol (isomers), xlenol (isomers), trimethylphenol (isomers),
 15 tetramethylphenol (isomers), ethylphenol (isomers), propylphenol (isomers), butylphenol (isomers), diethylphenol (isomers), methylethylphenol (isomers), methylpropylphenol (isomers), dipropylphenol (isomers), methylbutylphenol (isomers), pentylphenol (isomers), hexylphenol (isomers) and cyclohexylphenol (isomers); various alkoxyphenols such as methoxyphenol (isomers) and
 20 ethoxyphenol (isomers); arylalkylphenols such as phenylpropylphenol (isomers); naphthol (isomers) and various substituted naphthols; and heteroaromatic monohydroxy compounds such as hydroxypyridine (isomers), hydroxycoumarin (isomers) and hydroxyquinoline (isomers).

Of these aromatic monohydroxy compounds, ones preferably used in the
 25 present invention are aromatic monohydroxy compounds in which Ar^1 is an aromatic group having 6 to 10 carbon atoms. Phenol is particularly preferable. Moreover, of

these aromatic monohydroxy compounds, ones substantially not containing a halogen are preferably used in the present invention.

The molar ratio of the dialkyl carbonate to the aromatic monohydroxy compound used as the starting material of the present invention must be in a range of from 0.1 to 10. Outside this range, an amount of unreacted material remaining, based on a prescribed amount of the alkyl aryl carbonate produced becomes high, which is not efficient for the production of the aromatic carbonate. Moreover, much energy is required to recover the alkyl aryl carbonate. For such reasons, the above molar ratio is preferably in a range of from 0.5 to 5.0, more preferably 0.8 to 3.0, yet more preferably from 1.0 to 2.0.

In the present invention, not less than 1 ton per hour of the diaryl carbonate is produced continuously. The minimum amount of the aromatic monohydroxy compound fed in continuously for the above production is generally 15P ton/hr, preferably 13P ton/hr, more preferably 10P ton/hr, based on the amount of the aromatic carbonate (P ton/hr) to be produced. More preferably, this amount can be made to be less than 8.0P ton/hr.

The dialkyl carbonate and the aromatic monohydroxy compound as the starting material used in the present invention must contain specified amounts of the alcohol and the aromatic carbonate which are reaction products. Since the present reaction is an equilibrium reaction, it has been thought in the past that use of the starting material containing the alcohol and the aromatic carbonate which are the reaction products would be disadvantageous in terms of chemical equilibrium. However, it was discovered that in the case of using the continuous multi-stage distillation column according to the present invention, even if the starting material contains 0.01 to 5 % by weight of the alcohol and 0.01 to 5 % by weight of the aromatic carbonate, based on the total weight of the starting material, then

surprisingly the alcohol and the aromatic carbonate have hardly any influence on the production of the aromatic carbonate. A more preferable alcohol content is 0.05 to 3 % by weight, with 0.1 to 1 % by weight being yet more preferable. Moreover, a more preferable aromatic carbonate content is 0.1 to 4 % by weight, with 0.5 to 3 %
5 by weight being yet more preferable.

The reaction between the aromatic carbonate and the alcohol which is the reverse reaction to the present reaction has a very high equilibrium constant, and the reaction rate is high. With a batch reaction system in which the gas-liquid interfacial area is small, it can thus be easily understood that use of the starting material
10 containing the alcohol and the aromatic carbonate which are the reaction products would be very disadvantageous in terms of chemical equilibrium for producing the aromatic carbonate for which the reverse reaction readily occurs. Moreover, with a small-scale reactive distillation system, the residence time of the reaction liquid is generally short, and hence it is clear that use of the starting material containing the
15 alcohol and the aromatic carbonate which are the reaction products would be disadvantageous in terms of chemical equilibrium for producing the aromatic carbonate, since there would be little decrease in the concentrations of the alcohol and the aromatic carbonate in the reaction liquid.

However, it was discovered that if the first and second continuous multi-stage
20 distillation columns according to the present invention are used, surprisingly this disadvantageous effect hardly occurs at all. The precise reason for this is unclear, but it is supposed that this is because the aromatic carbonate as the starting material introduced into the upper portion of the first continuous multi-stage distillation column reacts with the alcohol which is present at a high concentration at the stage in the
25 upper portion of the column, and is thus rapidly converted into the dialkyl carbonate and the aromatic monohydroxy compound. It is also supposed that this is because

in the first continuous multi-stage distillation column according to the present invention, the residence time is sufficiently long for this reaction to take place in the upper portion of the column. Moreover, it is supposed that some or most of the alcohol in the starting material fed into the first continuous multi-stage distillation column is used in this reaction, and the remainder moves into the vapor phase efficiently. This effect has been discovered for the first time through prolonged continuous stable operation using the industrial-scale continuous multi-stage distillation column according to the present invention.

When implementing the present reaction industrially, besides fresh dialkyl carbonate and aromatic monohydroxy compound newly introduced into the reaction system, it is preferable to be able to use as the starting material a material containing mainly the dialkyl carbonate and the aromatic monohydroxy compound that has been recovered in this process and/or another process. That is, in the process according to the present invention, a column top component that comprises a low boiling point reaction mixture in the second continuous multi-stage distillation column is fed into the first continuous multi-stage distillation column. In this case, the second column low boiling point reaction mixture may be fed into the first continuous multi-stage distillation column as is, or after some of the components thereof have been separated out. Accordingly, in the present invention which is implemented industrially, it is preferable for the starting material fed into the first continuous multi-stage distillation column to contain specified amounts of the alcohol, and aromatic carbonates such as the alkyl aryl carbonate and the diaryl carbonate, as described above.

Furthermore, the starting material used in the present invention may contain compounds and reaction by-products, for example an alkyl aryl ether and high boiling point by-products, which are produced in this process and/or another process. It

has been found that a starting material containing 0.5 to 15 % by weight of the alkyl aryl ether is preferable when implementing the present invention. A more preferable range for the alkyl aryl ether content in the starting material is 2 to 12 % by weight, with 4 to 10 % by weight being yet more preferable. Examples of the high boiling point by-products include Fries rearrangement products of the alkyl aryl carbonate and diaryl carbonate, and derivatives thereof. It is preferable for the starting material to contain small amounts of such high boiling point by-products.

This means, for example, that in the case of producing methyl phenyl carbonate and diphenyl carbonate using as the starting material a mixture of dimethyl carbonate as the dialkyl carbonate and phenol as the aromatic monohydroxy compound, it is preferable for this starting material to contain specified amounts as described above of methyl alcohol, and methyl phenyl carbonate and diphenyl carbonate, which are the reaction products. Further, it is preferable for the starting material to contain a specified amount as described above of anisole, which is a reaction by-product. Furthermore, the starting material may contain small amounts of phenyl salicylate and methyl salicylate, and high boiling point by-products derived therefrom.

The aromatic carbonates produced in the present invention refer to an alkyl aryl carbonate, or a diaryl carbonate, or a mixture thereof, obtainable through the transesterification reaction between the dialkyl carbonate and the aromatic monohydroxy compound. Included under this transesterification reaction are a reaction in which one or two of the alkoxy groups of the dialkyl carbonate is/are exchanged with the aryloxy group of the aromatic monohydroxy compound so as to eliminate an alcohol, and a reaction in which two molecules of the alkyl aryl carbonate produced are converted into the diaryl carbonate and the dialkyl carbonate through a transesterification reaction therebetween, i.e. a

disproportionation reaction. In the present invention, in the first continuous multi-stage distillation column, the alkyl aryl carbonate is mainly obtained, and in the second continuous multi-stage distillation column, the aromatic carbonates containing the diaryl carbonate as a main product are mainly obtainable through the disproportionation reaction of the alkyl aryl carbonate. In the present invention, it is particularly preferable for a starting material and catalyst not containing a halogen to be used; in this case, the diaryl carbonate produced does not contain a halogen at all, and hence it is important as a raw material when industrially producing a polycarbonate by means of a transesterification method. The reason for this is that if a halogen is present in the raw material for the polymerization even in a small amount of less than 1 ppm, then this may inhibit the polymerization reaction, or cause a deterioration of the properties of, or discoloration of, the polycarbonate produced.

As a catalyst used in the first continuous multi-stage distillation column and/or the second continuous multi-stage distillation column according to the present invention, for example, a metal-containing compound selected from the following compounds can be used:

<Lead compounds>

Lead oxides such as PbO , PbO_2 and Pb_3O_4 ; lead sulfides such as PbS and Pb_2S ; lead hydroxides such as $\text{Pb}(\text{OH})_2$ and $\text{Pb}_2\text{O}_2(\text{OH})_2$; plumbites such as Na_2PbO_2 , K_2PbO_2 , NaHPbO_2 and KHPbO_2 ; plumbates such as Na_2PbO_3 , $\text{Na}_2\text{H}_2\text{PbO}_4$, K_2PbO_3 , $\text{K}_2[\text{Pb}(\text{OH})_6]$, K_4PbO_4 , Ca_2PbO_4 and CaPbO_3 ; lead carbonates and basic salts thereof such as PbCO_3 and $2\text{PbCO}_3\cdot\text{Pb}(\text{OH})_2$; lead salts of organic acids, and carbonates and basic salts thereof, such as $\text{Pb}(\text{OCOCH}_3)_2$, $\text{Pb}(\text{OCOCH}_3)_4$ and $\text{Pb}(\text{OCOCH}_3)_2\cdot\text{PbO}\cdot 3\text{H}_2\text{O}$, organolead compounds such as Bu_4Pb , Ph_4Pb , Bu_3PbCl , Ph_3PbBr , Ph_3Pb (or Ph_6Pb_2), Bu_3PbOH and Ph_3PbO (wherein Bu

represents a butyl group, and Ph represents a phenyl group); alkoxylead compounds and aryloxylead compounds such as $\text{Pb}(\text{OCH}_3)_2$, $(\text{CH}_3\text{O})\text{Pb}(\text{OPh})$ and $\text{Pb}(\text{OPh})_2$; lead alloys such as Pb-Na, Pb-Ca, Pb-Ba, Pb-Sn and Pb-Sb; lead minerals such as galena and zinc blende; and hydrates of such lead compounds;

5 <Copper family metal compounds>

Salts and complexes of copper family metals such as CuCl , CuCl_2 , CuBr , CuBr_2 , CuI , CuI_2 , $\text{Cu}(\text{OAc})_2$, $\text{Cu}(\text{acac})_2$, copper oleate, Bu_2Cu , $(\text{CH}_3\text{O})_2\text{Cu}$, AgNO_3 , AgBr , silver picrate, $\text{AgC}_6\text{H}_6\text{ClO}_4$, $[\text{AuC}\equiv\text{C}-\text{C}(\text{CH}_3)_3]_n$ and $[\text{Cu}(\text{C}_7\text{H}_8)\text{Cl}]_4$ (wherein acac represents an acetylacetone chelate ligand);

10 <Alkali metal complexes>

Alkali metal complexes such as $\text{Li}(\text{acac})$ and $\text{LiN}(\text{C}_4\text{H}_9)_2$;

<Zinc complexes>

Zinc complexes such as $\text{Zn}(\text{acac})_2$;

<Cadmium complexes>

15 Cadmium complexes such as $\text{Cd}(\text{acac})_2$;

<Iron family metal compounds>

Complexes of iron family metals such as $\text{Fe}(\text{C}_{10}\text{H}_8)(\text{CO})_5$, $\text{Fe}(\text{CO})_5$, $\text{Fe}(\text{C}_4\text{H}_6)(\text{CO})_3$, $\text{Co}(\text{mesitylene})_2$, $(\text{PEt}_2\text{Ph})_2$, $\text{CoC}_5\text{F}_5(\text{CO})_7$, $\text{Ni}-\pi-\text{C}_5\text{H}_5\text{NO}$ and ferrocene;

20 <Zirconium complexes>

Zirconium complexes such as $\text{Zr}(\text{acac})_4$ and zirconocene;

<Lewis acid type compounds>

Lewis acids and Lewis acid-forming transition metal compounds such as AlX_3 , TiX_3 , TiX_4 , VOX_3 , VX_5 , ZnX_2 , FeX_3 and SnX_4 (wherein X represents a halogen atom, an acetoxy group, an alkoxy group or an aryloxy group); and

<Organo-tin compounds>

Organo-tin compounds such as $(\text{CH}_3)_3\text{SnOCOCH}_3$, $(\text{C}_2\text{H}_5)_3\text{SnOCOC}_6\text{H}_5$,
 $\text{Bu}_3\text{SnOCOCH}_3$, $\text{Ph}_3\text{SnOCOCH}_3$, $\text{Bu}_2\text{Sn}(\text{OCOCH}_3)_2$, $\text{Bu}_2\text{Sn}(\text{OCOC}_{11}\text{H}_{23})_2$,
 $\text{Ph}_3\text{SnOCH}_3$, $(\text{C}_2\text{H}_5)_3\text{SnOPh}$, $\text{Bu}_2\text{Sn}(\text{OCH}_3)_2$, $\text{Bu}_2\text{Sn}(\text{OC}_2\text{H}_5)_2$, $\text{Bu}_2\text{Sn}(\text{OPh})_2$,
 $\text{Ph}_2\text{Sn}(\text{OCH}_3)_2$, $(\text{C}_2\text{H}_5)_3\text{SnOH}$, Ph_3SnOH , Bu_2SnO , $(\text{C}_8\text{H}_{17})_2\text{SnO}$, Bu_2SnCl_2 and
5 $\text{BuSnO}(\text{OH})$.

Each of these catalysts may be a solid catalyst fixed inside the multi-stage distillation column, or may be a soluble catalyst that dissolves in the reaction system.

Each of these catalyst components may of course have been reacted with an organic compound present in the reaction system such as an aliphatic alcohol, the
10 aromatic monohydroxy compound, the alkyl aryl carbonate, the diaryl carbonate or the dialkyl carbonate, or may have been subjected to heating treatment with the starting material or products prior to the reaction.

In the case of carrying out the present invention with a soluble catalyst that dissolves in the reaction system, the catalyst is preferably one having a high
15 solubility in the reaction liquid under the reaction conditions. Examples of preferable catalysts in this sense include PbO , $\text{Pb}(\text{OH})_2$ and $\text{Pb}(\text{OPh})_2$; TiCl_4 , $\text{Ti}(\text{OMe})_4$, $(\text{MeO})\text{Ti}(\text{OPh})_3$, $(\text{MeO})_2\text{Ti}(\text{OPh})_2$, $(\text{MeO})_3\text{Ti}(\text{OPh})$ and $\text{Ti}(\text{OPh})_4$; SnCl_4 , $\text{Sn}(\text{OPh})_4$, Bu_2SnO and $\text{Bu}_2\text{Sn}(\text{OPh})_2$; FeCl_3 , $\text{Fe}(\text{OH})_3$ and $\text{Fe}(\text{OPh})_3$; and such catalysts that have been treated with phenol, the reaction liquid or the like.

20 Fig. 1 shows a schematic view of the first continuous multi-stage distillation column for carrying out a production process according to the present invention. The continuous multi-stage distillation column 101 used in the present invention comprises a structure having a pair of end plates 5 above and below a cylindrical trunk portion 7 having a length L_1 (cm) and an inside diameter D_1 (cm), and having an
25 internal 6 with a number of stages n thereinside, and has a gas outlet 1 having an inside diameter d_{11} (cm) at the top of the column or in an upper portion of the column

near to the top, a liquid outlet 2 having an inside diameter d_{12} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet 3 provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet 4 provided in the lower portion of the column above the liquid outlet.

More specifically, the following are required for the first continuous multi-stage distillation column 101 according to the present invention:

(1) the length L_1 (cm) must satisfy formula (1),

$$1500 \leq L_1 \leq 8000 \quad (1),$$

(2) the inside diameter D_1 (cm) of the column must satisfy formula (2),

$$100 \leq D_1 \leq 2000 \quad (2),$$

(3) a ratio of the length L_1 (cm) to the inside diameter D_1 (cm) of the column must satisfy formula (3),

$$2 \leq L_1 / D_1 \leq 40 \quad (3),$$

(4) the number of stages n_1 must satisfy formula (4),

$$20 \leq n_1 \leq 120 \quad (4),$$

(5) a ratio of the inside diameter D_1 (cm) of the column to the inside diameter d_{11} (cm) of the gas outlet must satisfy formula (5),

$$5 \leq D_1 / d_{11} \leq 30 \quad (5), \text{ and}$$

(6) a ratio of the inside diameter D_1 (cm) of the column to the inside diameter d_{12} (cm) of the liquid outlet must satisfy formula (6),

$$3 \leq D_1 / d_{12} \leq 20 \quad (6).$$

Fig. 2 shows a schematic view of the second continuous multi-stage distillation column for carrying out a production process according to the present invention. The second continuous multi-stage distillation column 201 used in the present invention comprises a structure having a pair of end plates 5 above and

below a cylindrical trunk portion 7 having a length L_2 (cm) and an inside diameter D_2 (cm), and having an internal (6-1: packing, 6-2: tray) with a number of stages n_2 thereinside, and has a gas outlet 1 having an inside diameter d_{21} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet 2 having an inside diameter d_{22} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet 3 provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet 4 provided in the lower portion of the column above the liquid outlet.

More specifically, the following are required for the second continuous multi-stage distillation column 201 according to the present invention:

(1) the length L_2 (cm) must satisfy formula (7),

$$1500 \leq L_2 \leq 8000 \quad (7),$$

(2) the inside diameter D_2 (cm) of the column must satisfy formula (8),

$$100 \leq D_2 \leq 2000 \quad (8),$$

(3) a ratio of the length L_2 (cm) to the inside diameter D_2 (cm) of the column must satisfy formula (9),

$$2 \leq L_2 / D_2 \leq 40 \quad (9),$$

(4) the number of stages n_2 must satisfy formula (10),

$$10 \leq n_2 \leq 80 \quad (10),$$

(5) a ratio of the inside diameter D_2 (cm) of the column to the inside diameter d_{21} (cm) of the gas outlet must satisfy formula (11),

$$2 \leq D_2 / d_{21} \leq 15 \quad (11), \text{ and}$$

(6) a ratio of the inside diameter D_2 (cm) of the column to the inside diameter d_{22} (cm) of the liquid outlet must satisfy formula (12),

$$5 \leq D_2 / d_{22} \leq 30 \quad (12).$$

Note that since Figs. 1 and 2 show embodiments of the continuous

multi-stage distillation columns according to the present invention, arrangement of the internal is not limited to that of Figs.1 and 2. It should be noted that the term "in an upper portion of the column near to the top" refers to the portion extending downwardly from the top of the column to the location measuring about $0.25 L_1$ or $0.25 L_2$, and the term "in a lower portion of the column near to the bottom" refers to the portion extending upwardly from the bottom of the column to the location measuring about $0.25 L_1$ or $0.25 L_2$. Note that L_1 and L_2 are defined above.

It has been discovered that by using the first continuous multi-stage distillation column and the second continuous multi-stage distillation column that simultaneously satisfy formulae (1) to (12), aromatic carbonates containing a diaryl carbonate as a main product can be produced from a dialkyl carbonate and an aromatic monohydroxy compound on an industrial scale of not less than 1 ton per hour with high selectivity and high productivity stably for a prolonged period of time, for example not less than 2000 hours, preferably not less than 3000 hours, more preferably not less than 5000 hours. The reason why it has become possible to produce aromatic carbonates on an industrial scale with such excellent effects by implementing the process of the present invention is not clear, but this is supposed to be due to a combined effect brought about when the conditions of formulae (1) to (12) are combined. Preferable ranges for the respective factors are described below.

If each of L_1 (cm) and L_2 (cm) is less than 1500, then the conversion decreases and hence it is not possible to attain the desired production amount. Moreover, to keep down the equipment cost while securing the conversion enabling the desired production amount to be attained, each of L_1 and L_2 must be made to be not more than 8000. More preferable ranges for L_1 (cm) and L_2 (cm) are $2000 \leq L_1 \leq 6000$ and $2000 \leq L_2 \leq 6000$, respectively with $2500 \leq L_1 \leq 5000$

and $2500 \leq L_2 \leq 5000$ being yet more preferable.

If each of D_1 (cm) and D_2 (cm) is less than 100, then it is not possible to attain the desired production amount. Moreover, to keep down the equipment cost while attaining the desired production amount, each of D_1 and D_2 must be made to be not more than 2000. More preferable ranges for D_1 (cm) and D_2 (cm) are $150 \leq D_1 \leq 1000$ and $150 \leq D_2 \leq 1000$, respectively with $200 \leq D_1 \leq 800$ and $200 \leq D_2 \leq 800$ being yet more preferable. For the first continuous multi-stage distillation column and the second continuous multi-stage distillation column, so long as D_1 and D_2 are within the above ranges, each of the columns may have the same inside diameter from the upper portion thereof to the lower portion thereof, or the inside diameter may differ from different portions. For example, for each of the continuous multi-stage distillation columns, the inside diameter of the upper portion of the column may be smaller than, or larger than, the inside diameter of the lower portion of the column.

If each of L_1 / D_1 and L_2 / D_2 is less than 2 or greater than 40, then stable operation becomes difficult. In particular, if L_1 / D_1 or L_2 / D_2 is greater than 40, then the pressure difference between the top and bottom of the column becomes too great, and hence prolonged stable operation becomes difficult. Moreover, it becomes necessary to increase the temperature in the lower portion of the column, and hence side reactions become liable to occur, bringing about a decrease in the selectivity. More preferable ranges for L_1 / D_1 and L_2 / D_2 are $3 \leq L_1 / D_1 \leq 30$ and $3 \leq L_2 / D_2 \leq 30$, respectively with $5 \leq L_1 / D_1 \leq 15$ and $5 \leq L_2 / D_2 \leq 15$ being yet more preferable.

If n_1 is less than 20, then the conversion decreases and it is not possible to attain the desired production amount for the first continuous multi-stage distillation column. Moreover, to keep down the equipment cost while securing the conversion

enabling the desired production amount to be attained, n_1 must be made to be not more than 120. Furthermore, if n_1 is greater than 120, then the pressure difference between the top and bottom of the column becomes too great, and hence prolonged stable operation of the first continuous multi-stage distillation column becomes

5 difficult. Moreover, it becomes necessary to increase the temperature in the lower portion of the column, and hence side reactions become liable to occur, bringing about a decrease in the selectivity. A more preferable range for n_1 is $30 \leq n_1 \leq 100$, with $40 \leq n_1 \leq 90$ being yet more preferable. Moreover, if n_2 is less than 10, then the conversion decreases and it is not possible to attain the desired production

10 amount for the second continuous multi-stage distillation column. Moreover, to keep down the equipment cost while securing the conversion enabling the desired production amount to be attained, n_2 must be made to be not more than 80.

Furthermore, if n_2 is greater than 80, then the pressure difference between the top and bottom of the column becomes too great, and hence prolonged stable operation
15 of the second continuous multi-stage distillation column becomes difficult. Moreover, it becomes necessary to increase the temperature in the lower portion of the column, and hence side reactions become liable to occur, bringing about a decrease in the selectivity. A more preferable range for n_2 is $15 \leq n_2 \leq 60$, with $20 \leq n_2 \leq 50$ being yet more preferable.

20 If D_1 / d_{11} is less than 5, then the equipment cost for the first continuous multi-stage distillation column becomes high. Moreover, large amounts of gaseous components are readily released to the outside of the system, and hence stable operation of the first continuous multi-stage distillation column becomes difficult. If D_1 / d_{11} is greater than 30, then the gaseous component withdrawal amount becomes
25 relatively low, and hence stable operation becomes difficult, and moreover a decrease in the conversion is brought about. A more preferable range for D_1 / d_{11} is

$8 \leq D_1 / d_{11} \leq 25$, with $10 \leq D_1 / d_{11} \leq 20$ being yet more preferable.

Furthermore, if D_2 / d_{21} is less than 2, then the equipment cost for the second continuous multi-stage distillation column becomes high. Moreover, large amounts of gaseous components are readily released to the outside of the system, and hence stable operation of the second continuous multi-stage distillation column becomes difficult. If D_2 / d_{21} is greater than 15, then the gaseous component withdrawal amount becomes relatively low, and hence stable operation becomes difficult, and moreover a decrease in the conversion is brought about. A more preferable range for D_2 / d_{21} is $5 \leq D_2 / d_{21} \leq 12$, with $3 \leq D_2 / d_{21} \leq 10$ being yet more preferable.

If D_1 / d_{12} is less than 3, then the equipment cost for the first continuous multi-stage distillation column becomes high. Moreover, the liquid withdrawal amount becomes relatively high, and hence stable operation of the first continuous multi-stage distillation column becomes difficult. If D_1 / d_{12} is greater than 20, then the flow rate through the liquid outlet and piping becomes excessively fast, and hence erosion becomes liable to occur, bringing about corrosion of the apparatus. A more preferable range for D_1 / d_{12} is $5 \leq D_1 / d_{12} \leq 18$, with $7 \leq D_1 / d_{12} \leq 15$ being yet more preferable. Furthermore, if D_2 / d_{22} is less than 5, then the equipment cost for the second continuous multi-stage distillation column becomes high. Moreover, the liquid withdrawal amount becomes relatively high, and hence stable operation of the second continuous multi-stage distillation column becomes difficult. If D_2 / d_{22} is greater than 30, then the flow rate through the liquid outlet and piping becomes excessively fast, and hence erosion becomes liable to occur, bringing about corrosion of the apparatus. A more preferable range for D_2 / d_{22} is $7 \leq D_2 / d_{22} \leq 25$, with $9 \leq D_2 / d_{22} \leq 20$ being yet more preferable.

Furthermore, it has been found that in the present invention it is further

preferable for d_{11} and d_{12} to satisfy the formula (13), and for d_{21} and d_{22} to satisfy the formula (14).

$$1 \leq d_{12} / d_{11} \leq 5 \quad (13)$$

$$1 \leq d_{21} / d_{22} \leq 6 \quad (14).$$

5 The term "prolonged stable operation" used in the present invention means that operation can be carried out continuously in a steady state based on the operating conditions with no clogging of piping or erosion for not less than 1000 hours, preferably not less than 3000 hours, more preferably not less than 5000 hours, and a prescribed amount of the aromatic carbonates containing the diaryl carbonate
10 as a main product can be produced while maintaining high selectivity.

A characteristic feature of the present invention is that the aromatic carbonates can be produced stably for a prolonged period of time with high selectivity and with a high productivity of not less than 1 ton per hour, preferably not less than 2 tons per hour, more preferably not less than 3 tons per hour. Moreover,
15 another characteristic feature of the present invention is that in the case that L_1 , D_1 , L_1 / D_1 , n_1 , D_1 / d_{11} , and D_1 / d_{12} for the first continuous multi-stage distillation column satisfy the following formulae: $2000 \leq L_1 \leq 6000$, $150 \leq D_1 \leq 1000$, $3 \leq L_1 / D_1 \leq 30$, $30 \leq n_1 \leq 100$, $8 \leq D_1 / d_{11} \leq 25$, and $5 \leq D_1 / d_{12} \leq 18$, respectively, and L_2 , D_2 , L_2 / D_2 , n_2 , D_2 / d_{21} and D_2 / d_{22} for the second continuous
20 multi-stage distillation column satisfy the following formulae: $2000 \leq L_2 \leq 6000$, $150 \leq D_2 \leq 1000$, $3 \leq L_2 / D_2 \leq 30$, $15 \leq n_2 \leq 60$, $2.5 \leq D_2 / d_{21} \leq 12$, and $7 \leq D_2 / d_{22} \leq 25$, respectively, not less than 2 tons per hour, preferably not less than 2.5 tons per hour, more preferably not less than 3 tons per hour of the aromatic carbonates can be produced. Furthermore, another
25 characteristic feature of the present invention is that in the case that L_1 , D_1 , L_1 / D_1 , n_1 , D_1 / d_{11} , and D_1 / d_{12} for the first continuous multi-stage distillation column satisfy the

following formulae: $2500 \leq L_1 \leq 5000$, $200 \leq D_1 \leq 800$, $5 \leq L_1/D_1 \leq 15$,
 $40 \leq n_1 \leq 90$, $10 \leq D_1/d_{11} \leq 25$, and $7 \leq D_1/d_{12} \leq 15$, respectively
 and L_2 , D_2 , L_2/D_2 , n_2 , D_2/d_{21} , and D_2/d_{22} for the second continuous multi-stage
 distillation column satisfy the following formulae: $2500 \leq L_2 \leq 5000$, $200 \leq D_2$
 5 ≤ 800 , $5 \leq L_2/D_2 \leq 10$, $20 \leq n_2 \leq 50$, $3 \leq D_2/d_{21} \leq 10$, and $9 \leq$
 $D_2/d_{22} \leq 20$, respectively, not less than 3 tons per hour, preferably not less than
 3.5 tons per hour, more preferably not less than 4 tons per hour of the aromatic
 carbonates can be produced.

“Selectivity for the aromatic carbonates” in the present invention is based on
 10 the aromatic monohydroxy compound reacted. In the present invention, a high
 selectivity of not less than 95% can generally be attained, preferably not less than
 97%, more preferably not less than 98%.

Each of the first continuous multi-stage distillation column and the second
 continuous multi-stage distillation column used in the present invention is preferably
 15 a distillation column having a tray and/or a packing as the internal. The term
 “internal” used in the present invention means the parts in the distillation column
 where gas and liquid are actually brought into contact with one another. As the tray,
 for example, a bubble-cap tray, a sieve tray, a valve tray, a counterflow tray, a
 Superfrac tray, a Maxfrac tray, or the like are preferable. As the packing, a random
 20 packing such as a Raschig ring, a Lessing ring, a Pall ring, a Berl saddle, an Intalox
 saddle, a Dixon packing, a McMahon packing or a Heli-Pak, or a structured packing
 such as Mellapak, Gempak, TECHNO-PAK, FLEXI-PAK, a Sulzer packing, a
 Goodroll packing or a Glitchgrid are preferable. The multi-stage distillation column
 having both a tray portion and a portion packed with the packing can also be used.
 25 Note that the term “number of stages (n) of an internal” used in the present invention
 means that the total number of trays in the case of a tray, and the theoretical number

of stages in the case of a packing. Therefore, in the case of the multi-stage column having both the tray portion and the portion packed with the packing, n means the sum of the total number of trays and the theoretical number of stages of the packing.

In the first continuous multi-stage distillation column of the present invention,
5 a reaction in which the alkyl aryl carbonate is produced from the dialkyl carbonate and the aromatic monohydroxy compound mainly occurs. This reaction has an extremely low equilibrium constant, and the reaction rate is slow, and hence it has been discovered that a plate-type distillation column having the tray as the internal is particularly preferable as the first continuous multi-stage distillation column used in
10 the reactive distillation. Moreover, in the second continuous multi-stage distillation column, it is mainly a disproportionation reaction of the alkyl aryl carbonate that occurs. This reaction also has a low equilibrium constant, and a slow reaction rate. It has been discovered that a distillation column having both the packing and the tray as the internal is preferable as the second continuous multi-stage distillation column
15 used in the reactive distillation. Furthermore, it has been discovered that a distillation column having the packing installed in the upper portion thereof and the tray installed in the lower portion thereof is preferable as the second continuous multi-stage distillation column. It has been discovered that the packing in the second continuous multi-stage distillation column is preferably structured packing.
20 Of the structured packing, Mellapak is particularly preferable.

Furthermore, it has been discovered that, as each of the tray installed in the first continuous multi-stage distillation column and the second continuous multi-stage distillation column, a sieve tray having a sieve portion and a down comer portion is particularly good in terms of the relationship between performance and equipment
25 cost. It has also been discovered that the sieve tray preferably has 100 to 1000 holes/m² in the sieve portion. A more preferable number of holes is 120 to 900

holes/m², yet more preferably 150 to 800 holes/m². Moreover, it has been discovered that the cross-sectional area per hole of the sieve tray is preferably in a range of from 0.5 to 5 cm². A more preferable cross-sectional area per hole is 0.7 to 4 cm², yet more preferably 0.9 to 3 cm². Furthermore, it has been discovered that it is particularly preferable if the sieve tray has 100 to 1000 holes/m² in the sieve portion and the cross-sectional area per hole is in a range of from 0.5 to 5 cm². It has been shown that by adding the above conditions to the continuous multi-stage distillation columns, the object of the present invention can be attained more easily.

When carrying out the present invention, aromatic carbonates containing a diaryl carbonate as a main product are continuously produced by continuously feeding a dialkyl carbonate and an aromatic monohydroxy compound which are the starting material into the first continuous multi-stage distillation column in which a catalyst is present, carrying out the reaction and the distillation simultaneously in the first column, continuously withdrawing a first column low boiling point reaction mixture containing a produced alcohol from an upper portion of the first column in a gaseous form, continuously withdrawing a first column high boiling point reaction mixture containing a produced alkyl aryl carbonate from a lower portion of the first column in a liquid form, continuously feeding the first column high boiling point reaction mixture into the second continuous multi-stage distillation column in which a catalyst is present, carrying out the reaction and the distillation simultaneously in the second column, continuously withdrawing a second column low boiling point reaction mixture containing a produced dialkyl carbonate from an upper portion of the second column in a gaseous form, continuously withdrawing a second column high boiling point reaction mixture containing a produced diaryl carbonate from a lower portion of the second column in a liquid form while continuously feeding the second column low boiling point reaction mixture containing the dialkyl carbonate into the first continuous

multi-stage distillation column.

As described above, the starting material may contain the alcohol, the alkyl aryl carbonate and the diaryl carbonate that are reaction products, and reaction by-products such as an alkyl aryl ether and high boiling point compounds. Taking into consideration the equipment and cost required for separation and purification in other processes, when actually implementing the present invention industrially, it is preferable for the starting material to contain small amounts of such compounds.

In the present invention, when continuously feeding the dialkyl carbonate and the aromatic monohydroxy compound which are the starting material into the first continuous multi-stage distillation column, this starting material may be fed into the first distillation column in a liquid form and/or a gaseous form from inlet(s) provided in one or more of positions in the upper portion or the middle portion of the first distillation column below the gas outlet in the upper portion of the first distillation column. It is also preferable to feed a starting material containing a large proportion of the aromatic monohydroxy compound into the first distillation column in a liquid form from an inlet provided in the upper portion of the first distillation column, and feed a starting material containing a large proportion of the dialkyl carbonate into the first distillation column in a gaseous form from an inlet provided in the lower portion of the first distillation column above the liquid outlet in the lower portion of the first distillation column.

Moreover, in the present invention, the first column high boiling point reaction mixture containing the alkyl aryl carbonate continuously withdrawn from the lower portion of the first continuous multi-stage distillation column is continuously fed into the second continuous multi-stage distillation column. In this case, the first column high boiling point reaction mixture is preferably fed into the second distillation column in a liquid form and/or a gaseous form from inlet(s) provided in one or more of

positions in the upper portion or the middle portion of the second distillation column below the gas outlet in the upper portion of the second distillation column.

Moreover, in the case of using, as the second distillation column, a distillation column having a packing portion in the upper portion thereof and a tray portion in the lower portion thereof, which is a preferable embodiment of the present invention, it is preferable for at least one inlet to be installed between the packing portion and the tray portion. Moreover, in the case that the packing comprise a plurality of structured packings, it is preferable for an inlet to be installed in a space between the structured packings.

Moreover, in the present invention, it is also preferable to carry out a reflux operation of condensing the gaseous component withdrawn from the top of each of the first continuous multi-stage distillation column and the second continuous multi-stage distillation column, and then returning some of this component into the upper portion of that distillation column. In this case, the reflux ratio for the first continuous multi-stage distillation column is in a range of from 0 to 10, and the reflux ratio for the second continuous multi-stage distillation column is in a range of from 0.01 to 10, preferably 0.08 to 5, more preferably 0.1 to 2. For the first continuous multi-stage distillation column, not carrying out such a reflux operation (i.e. reflux ratio = 0) is also a preferable embodiment.

In the present invention, the method of making the catalyst be present in the first continuous multi-stage distillation column may be any method. In the case that the catalyst is a solid that is insoluble in the reaction liquid, it is preferable for the catalyst to be fixed inside the column by, for example, being installed on a plate inside the first continuous multi-stage distillation column or being installed in the form of a packing. In the case of a catalyst that dissolves in the starting material or the reaction liquid, it is preferable to feed the catalyst into the first distillation column from

a position above the middle portion of the first distillation column. In this case, the catalyst liquid dissolved in the starting material or reaction liquid may be introduced into the column together with the starting material, or may be introduced into the column from a different inlet to the starting material. The amount of the catalyst used in the first continuous multi-stage distillation column in the present invention varies depending on the type of catalyst used, the types and proportions of the starting material compounds, and reaction conditions such as the reaction temperature and the reaction pressure. The amount of the catalyst is generally in a range of from 0.0001 to 30 % by weight, preferably 0.005 to 10 % by weight, more preferably 0.001 to 1 % by weight, based on the total weight of the starting material.

Moreover, in the present invention, the method of making the catalyst be present in the second continuous multi-stage distillation column may be any method. In the case that the catalyst is a solid that is insoluble in the reaction liquid, it is preferable for the catalyst to be fixed inside the column by, for example, being installed on a plate inside the second continuous multi-stage distillation column or being installed in the form of a packing. In the case of a catalyst that dissolves in the starting material or the reaction liquid, it is preferable to feed the catalyst into the second distillation column from a position above the middle portion of the second distillation column. In this case, the catalyst liquid dissolved in the starting material

or reaction liquid may be introduced into the column together with the starting material, or may be introduced into the column from a different inlet to the starting material. The amount of the catalyst used in the second continuous multi-stage distillation column in the present invention varies depending on the type of catalyst used, the types and proportions of the starting material compounds, and reaction conditions such as the reaction temperature and the reaction pressure. The amount of the catalyst is generally in a range of from 0.0001 to 30 % by weight, preferably

0.005 to 10 % by weight, more preferably 0.001 to 1 % by weight, based on the total weight of the starting material.

In the present invention, the catalyst used in the first continuous multi-stage distillation column and the catalyst used in the second continuous multi-stage distillation column may be the same or different, but are preferably the same. More preferably, the same catalyst is used in both columns, this catalyst being one that dissolves in the reaction liquid in both columns. In this case, the catalyst dissolved in the high boiling point reaction mixture in the first continuous multi-stage distillation column is generally withdrawn from the lower portion of the first distillation column together with the alkyl aryl carbonate and so on, and fed into the second continuous multi-stage distillation column as is; this is a preferable embodiment. If necessary, the catalyst can be newly added into the second continuous multi-stage distillation column.

The reaction times for the transesterification reactions carried out in the present invention are considered to equate to the average residence times of the reaction liquids in the first continuous multi-stage distillation column and the second continuous multi-stage distillation column. Each of these reaction times varies depending on the form of the internal in the distillation column and the number of stages, the amount of the starting material fed into the column, the type and amount of the catalyst, the reaction conditions, and so on. The reaction time in each of the first continuous multi-stage distillation column and the second continuous multi-stage distillation column is generally in a range of from 0.01 to 10 hours, preferably 0.05 to 5 hours, more preferably 0.1 to 3 hours.

The reaction temperature in the first continuous multi-stage distillation column varies depending on the type of the starting material compounds used, and the type and amount of the catalyst. This reaction temperature is generally in a

range of from 100 to 350°C. It is preferable to increase the reaction temperature so as to increase the reaction rate. However, if the reaction temperature is too high, then side reactions become liable to occur, for example production of by-products such as an alkyl aryl ether increases, which is undesirable. For this reason, the
5 reaction temperature in the first continuous multi-stage distillation column is preferably in a range of from 130 to 280°C, more preferably 150 to 260°C, yet more preferably 180 to 250°C.

The reaction temperature in the second continuous multi-stage distillation column varies depending on the type of the starting material compounds used, and
10 the type and amount of the catalyst. This reaction temperature is generally in a range of from 100 to 350°C. It is preferable to increase the reaction temperature so as to increase the reaction rate. However, if the reaction temperature is too high, then side reactions become liable to occur, for example production of by-products such as an alkyl aryl ether, and Fries rearrangement products of the starting material
15 compounds and the produced alkyl aryl carbonate and diaryl carbonate, and derivatives thereof increases, which is undesirable. For this reason, the reaction temperature in the second continuous multi-stage distillation column is preferably in a range of from 130 to 280°C, more preferably 150 to 260°C, yet more preferably 180 to 250°C.

20 Moreover, the reaction pressure in the first continuous multi-stage distillation column varies depending on the type of the starting material compounds used and the composition of the starting material, the reaction temperature, and so on. The first continuous multi-stage distillation column may be at any of a reduced pressure, normal pressure, or an applied pressure. The pressure at the top of the column is
25 generally in a range of from 0.1 to 2×10^7 Pa, preferably 10^5 to 10^7 Pa, more preferably 2×10^5 to 5×10^6 Pa.

The reaction pressure in the second continuous multi-stage distillation column varies depending on the type of the starting material compounds used and the composition of the starting material, the reaction temperature, and so on. The second continuous multi-stage distillation column may be at any of a reduced
5 pressure, normal pressure, or an applied pressure. The pressure at the top of the column is generally in a range of from 0.1 to 2×10^7 Pa, preferably 10^3 to 10^6 Pa, more preferably 5×10^3 to 10^5 Pa.

Note that the first continuous multi-stage distillation column may comprise two or more of the distillation column. In this case, two or more of the distillation
10 column may be connected in series or in parallel. Two or more of the distillation column may also be connected in combination of in series and in parallel.

Moreover, the second continuous multi-stage distillation column may comprise two or more of the distillation column. In this case, two or more of the distillation column may be connected in series or in parallel. Two or more of the
15 distillation column may also be connected in combination of in series and in parallel.

The material constituting each of the first continuous multi-stage distillation column and the second continuous multi-stage distillation column used in the present invention is generally a metallic material such as carbon steel or stainless steel. In terms of the quality of the aromatic carbonates produced, stainless steel is
20 preferable.

Hereinbelow, the present invention will be described in more detail with reference to the following Examples, but the present invention is not limited to the following Examples.

Examples

25 Following is a more detailed description of the present invention with reference to Examples. However, the present invention is not limited to the

following Examples.

The halogen content was measured by means of an ion chromatography method.

Example 1:

5 <First continuous multi-stage distillation column 101>

A continuous multi-stage distillation column as shown in FIG. 1 having $L_1 = 3300$ cm, $D_1 = 500$ cm, $L_1 / D_1 = 6.6$, $n_1 = 80$, $D_1 / d_{11} = 17$, and $D_1 / d_{12} = 9$ was used. In this Example, the sieve tray having the cross-sectional area per hole being approximately 1.5 cm^2 and the number of holes being approximately $250/\text{m}^2$ were
10 used as the internal.

<Second continuous multi-stage distillation column 201>

A continuous multi-stage distillation column as shown in FIG. 2 having $L_2 = 3100$ cm, $D_2 = 500$ cm, $L_2 / D_2 = 6.2$, $n_2 = 30$, $D_2 / d_{21} = 3.85$, and $D_2 / d_{22} = 11.1$ was used. In this Example, as the internal, two sets of Mellapak (total number of stages
15 11) were installed in the upper portion, and the sieve tray having the cross-sectional area per hole being approximately 1.3 cm^2 and the number of holes being approximately $250/\text{m}^2$ were used in the lower portion.

<Reactive distillation>

Diphenyl carbonate was produced by carrying out reactive distillation using
20 an apparatus in which the first continuous multi-stage distillation column 101 and the second continuous multi-stage distillation column 201 were connected together as shown in FIG. 3.

A starting material 1 containing phenol and dimethyl carbonate in a weight ratio of phenol / dimethyl carbonate = 1.9 was introduced continuously in a liquid
25 form at a flow rate of 50 ton/hr from an upper inlet 11 of the first continuous multi-stage distillation column 101. The starting material 1 contained 0.3 % by

weight of methyl alcohol, 0.9 % by weight of methyl phenyl carbonate, 0.4 % by weight of diphenyl carbonate, and 7.3 % by weight of anisole. On the other hand, a starting material 2 containing dimethyl carbonate and phenol in a weight ratio of dimethyl carbonate / phenol = 3.6 was introduced continuously in a gaseous form at a flow rate of 50 ton/hr from a lower inlet 12 of the first continuous multi-stage distillation column 101. The starting material 2 contained 0.2 % by weight of methyl alcohol, 1.1 % by weight of methyl phenyl carbonate, and 5.1 % by weight of anisole. The molar ratio for the starting materials introduced into the first continuous multi-stage distillation column 101 was dimethyl carbonate / phenol = 1.35. The overall starting materials introduced into the first continuous multi-stage distillation column 101 contained 0.25 % by weight of methyl alcohol, 1.0 % by weight of methyl phenyl carbonate, 0.2 % by weight of diphenyl carbonate, and 6.2 % by weight of anisole. The starting materials substantially did not contain halogens (outside the detection limit for the ion chromatography, i.e. 1 ppb or less). Pb(OPh)_2 as a catalyst was introduced from the upper inlet 11 of the first continuous multi-stage distillation column 101 such that a concentration thereof in the reaction liquid would be approximately 100 ppm. Reactive distillation was carried out continuously under conditions of a temperature at the bottom of the first continuous multi-stage distillation column 101 being 225°C and a pressure at the top of the column being 7×10^5 Pa. A first column low boiling point reaction mixture containing methyl alcohol, dimethyl carbonate, phenol and so on was continuously withdrawn in a gaseous form from the top 13 of the first column, was passed through a heat exchanger 14, and was withdrawn at a flow rate of 34 ton/hr from an outlet 16. On the other hand, a first column high boiling point reaction mixture containing methyl phenyl carbonate, dimethyl carbonate, phenol, diphenyl carbonate, the catalyst and so on was continuously withdrawn in a liquid form from the bottom outlet 17 of the

first column.

A stable steady state was attained after 24 hours. The first column high boiling point reaction mixture was then fed continuously into the second continuous multi-stage distillation column 201 at a flow rate of 66 ton/hr from a starting material inlet 21 installed between the Mellapak and the sieve tray. The liquid fed into the second continuous multi-stage distillation column 201 contained 18.2 % by weight of methyl phenyl carbonate and 0.8 % by weight of diphenyl carbonate. Reactive distillation was carried out continuously under conditions of a temperature at the bottom of the second continuous multi-stage distillation column 201 being 210°C, a pressure at the top of the column being 3×10^4 Pa, and a reflux ratio being 0.3. It was possible to attain stable steady state operation after 24 hours. A second column low boiling point reaction mixture containing 35 % by weight of dimethyl carbonate and 56 % by weight of phenol was continuously withdrawn from the column top 23 of the second column, the flow rate at an outlet 26 being 55.6 ton/hr. The second column low boiling point reaction mixture was continuously fed into the first continuous multi-stage distillation column 101 from the inlet 11 and/or the inlet 12. At this time, the amounts of fresh dimethyl carbonate and phenol newly fed into the first continuous multi-stage distillation column 101 were adjusted so as to maintain the above-mentioned compositions and amounts of the starting material 1 and the starting material 2, taking into consideration the composition and amount of the second column low boiling point reaction mixture.

A second column high boiling point reaction mixture containing 38.4 % by weight of methyl phenyl carbonate and 55.6 % by weight of diphenyl carbonate was continuously withdrawn from the column bottom 27 of the second column. It was found that the amount of diphenyl carbonate produced per hour was 5.74 tons. The selectivity for the diphenyl carbonate based on the phenol reacted was 98%.

Prolonged continuous operation was carried out under these conditions.

The amounts of diphenyl carbonate produced per hour at 500 hours, 2000 hours, 4000 hours, 5000 hours, and 6000 hours after attaining stable steady state

(excluding the diphenyl carbonate contained in the starting material) were 5.74 tons,

5 5.75 tons, 5.74 tons, 5.74 tons, and 5.75 tons respectively, and the selectivities were 98%, 98%, 98%, 98%, and 98% respectively, and hence the operation was very stable. Moreover, the aromatic carbonates produced substantially did not contain halogens (1 ppb or less).

Example 2:

10 Reactive distillation was carried out under the following conditions using the same first and second continuous multi-stage distillation columns as in Example 1.

A starting material 1 containing phenol and dimethyl carbonate in a weight ratio of phenol / dimethyl carbonate = 1.1 was introduced continuously in a liquid form at a flow rate of 40 ton/hr from the upper inlet 11 of the first continuous

15 multi-stage distillation column 101. The starting material 1 contained 0.3 % by weight of methyl alcohol, 1.0 % by weight of methyl phenyl carbonate, and 5.6 % by weight of anisole. On the other hand, a starting material 2 containing dimethyl

carbonate and phenol in a weight ratio of dimethyl carbonate / phenol = 3.9 was introduced continuously in a gaseous form at a flow rate of 43 ton/hr from the lower

20 inlet 12 of the first continuous multi-stage distillation column 101. The starting material 2 contained 0.1 % by weight of methyl alcohol, 0.2 % by weight of methyl phenyl carbonate, and 4.4 % by weight of anisole. The molar ratio for the starting materials introduced into the first continuous multi-stage distillation column 101 was dimethyl carbonate / phenol = 1.87. The overall starting materials introduced into

25 the first continuous multi-stage distillation column 101 contained 0.2 % by weight of methyl alcohol, 0.59 % by weight of methyl phenyl carbonate, and 5.0 % by weight of

anisole. The starting materials substantially did not contain halogens (outside the detection limit for the ion chromatography, i.e. 1 ppb or less). Pb(OPh)_2 as a catalyst was introduced from the upper portion of the column such that a concentration thereof in the reaction liquid would be approximately 250 ppm.

5 Reactive distillation was carried out continuously under conditions of a temperature at the bottom of the first continuous multi-stage distillation column 101 being 235°C and a pressure at the top of the column being 9×10^5 Pa. It was possible to attain stable steady state operation after 24 hours. A first column low boiling point reaction mixture containing methyl alcohol, dimethyl carbonate, phenol and so on
10 was continuously withdrawn in a gaseous form from the column top 13 of the first column, was passed through a heat exchanger 14, and was withdrawn at a flow rate of 43 ton/hr from the outlet 16. On the other hand, a first column high boiling point reaction mixture containing methyl phenyl carbonate, dimethyl carbonate, phenol, diphenyl carbonate, the catalyst and so on was continuously withdrawn in a liquid
15 form from the column bottom 17 of the first column.

A stable steady state was attained after 24 hours. The first column high boiling point reaction mixture was then fed continuously into the second continuous multi-stage distillation column 201 at a flow rate of 40 ton/hr from the starting material inlet 21 installed between the Mellapak and the sieve tray. The liquid fed
20 into the second continuous multi-stage distillation column 201 contained 20.7 % by weight of methyl phenyl carbonate and 1.0 % by weight of diphenyl carbonate. Reactive distillation was carried out continuously under conditions of a temperature at the bottom of the second continuous multi-stage distillation column 201 being 205°C , a pressure at the top of the column being 2×10^4 Pa, and a reflux ratio being
25 0.5. It was possible to attain stable steady state operation after 24 hours. A second column low boiling point reaction mixture was continuously withdrawn from

the column top 23 of the second column, the flow rate at the outlet 26 being 33.3 ton/hr. The second column low boiling point reaction mixture was continuously fed into the first continuous multi-stage distillation column 101 from the inlet 11 and/or the inlet 12. At this time, the amounts of fresh dimethyl carbonate and phenol newly fed into the first continuous multi-stage distillation column 101 were adjusted so as to maintain the above-mentioned compositions and amounts of the starting material 1 and the starting material 2, taking into consideration the composition and amount of the second column low boiling point reaction mixture.

A second column high boiling point reaction mixture containing 35.5 % by weight of methyl phenyl carbonate and 61.2 % by weight of diphenyl carbonate was continuously withdrawn from the column bottom 27 of the second column. It was found that the amount of diphenyl carbonate produced per hour was 4.1 tons. The selectivity for the diphenyl carbonate based on the phenol reacted was 97%.

Prolonged continuous operation was carried out under these conditions. The amounts of diphenyl carbonate produced per hour at 500 hours, 1000 hours, and 2000 hours after attaining stable steady state were 4.1 tons, 4.1 tons, and 4.1 tons respectively, and the selectivities based on the reacted phenol were 97%, 97%, and 97% respectively, and hence the operation was very stable. Moreover, the aromatic carbonates produced substantially did not contain halogens (1 ppb or less).

Example 3:

Reactive distillation was carried out under the following conditions using the same apparatus as in Example 1 except that the cross-sectional area per hole of each of the sieve trays in the second continuous multi-stage distillation column 201 was made to be approximately 1.8 cm^2 .

A starting material 1 containing phenol and dimethyl carbonate in a weight ratio of phenol / dimethyl carbonate = 1.7 was introduced continuously in a liquid

form at a flow rate of 86 ton/hr from the upper inlet 11 of the first continuous multi-stage distillation column 101. The starting material 1 contained 0.3 % by weight of methyl alcohol, 0.9 % by weight of methyl phenyl carbonate, 0.4 % by weight of diphenyl carbonate, and 7.3 % by weight of anisole. On the other hand, a

5 starting material 2 containing dimethyl carbonate and phenol in a weight ratio of dimethyl carbonate / phenol = 3.5 was introduced continuously in a gaseous form at a flow rate of 90 ton/hr from the lower inlet 12 of the first continuous multi-stage distillation column 101. The starting material 2 contained 0.2 % by weight of methyl alcohol, 1.1 % by weight of methyl phenyl carbonate, and 5.1 % by weight of anisole.

10 The molar ratio for the starting materials introduced into the first continuous multi-stage distillation column 101 was dimethyl carbonate / phenol = 1.44. The overall starting materials introduced into the first continuous multi-stage distillation column 101 contained 0.25 % by weight of methyl alcohol, 1.1 % by weight of methyl phenyl carbonate, 0.195 % by weight of diphenyl carbonate, and 6.17 % by weight of

15 anisole. The starting materials substantially did not contain halogens (outside the detection limit for the ion chromatography, i.e. 1 ppb or less). $\text{Pb}(\text{OPh})_2$ as a catalyst was introduced from the upper inlet 11 of the first continuous multi-stage distillation column 101 such that a concentration thereof in the reaction liquid would be approximately 150 ppm. Reactive distillation was carried out continuously under

20 conditions of a temperature at the bottom of the first continuous multi-stage distillation column 101 being 220°C and a pressure at the top of the column being 8×10^5 Pa. A first column low boiling point reaction mixture containing methyl alcohol, dimethyl carbonate, phenol and so on was continuously withdrawn in a gaseous form from the column top 13 of the first column, was passed through a heat

25 exchanger 14, and was withdrawn at a flow rate of 82 ton/hr from the outlet 16. On the other hand, a first column high boiling point reaction mixture containing methyl

phenyl carbonate, dimethyl carbonate, phenol, diphenyl carbonate, the catalyst and so on was continuously withdrawn in a liquid form from the column bottom 17 of the first column.

A stable steady state was attained after 24 hours. The first column high boiling point reaction mixture was then fed continuously into the second continuous multi-stage distillation column 201 at a flow rate of 94 ton/hr from the starting material inlet 21 installed between the Mellapak and the sieve tray. The liquid fed into the second continuous multi-stage distillation column 201 contained 16.0 % by weight of methyl phenyl carbonate and 0.5 % by weight of diphenyl carbonate.

Reactive distillation was carried out continuously under conditions of a temperature at the bottom of the second continuous multi-stage distillation column 201 being 215°C, a pressure at the top of the column being 2.5×10^4 Pa, and a reflux ratio being 0.4. It was possible to attain stable steady state operation after 24 hours. A second column low boiling point reaction mixture was continuously withdrawn from the top 23 of the second column, the flow rate at the outlet 26 being 81.7 ton/hr.

The second column low boiling point reaction mixture was continuously fed into the first continuous multi-stage distillation column 101 from the inlet 11 and/or the inlet 12. At this time, the amounts of fresh dimethyl carbonate and phenol newly fed into the first continuous multi-stage distillation column 101 were adjusted so as to maintain the above-mentioned compositions and amounts of the starting material 1 and the starting material 2, taking into consideration the composition and amount of the second column low boiling point reaction mixture.

A second column high boiling point reaction mixture containing 35.5 % by weight of methyl phenyl carbonate and 59.5 % by weight of diphenyl carbonate was continuously withdrawn from the column bottom 27 of the second column. It was found that the amount of diphenyl carbonate produced per hour was 7.32 tons. The

selectivity for the diphenyl carbonate based on the phenol reacted was 98%.

Prolonged continuous operation was carried out under these conditions.

The amounts of diphenyl carbonate produced per hour at 500 hours, 1000 hours, and 2000 hours after attaining stable steady state were 7.32 tons, 7.33 tons, and

7.33 tons respectively, and the selectivities based on the reacted phenol were 98%, 98%, and 98% respectively, and hence the operation was very stable. Moreover, the aromatic carbonates produced substantially did not contain halogens (1 ppb or less).

10 Industrial Applicability

The present invention is suitable as a specific process that enables aromatic carbonates containing diaryl carbonate as a main product to be produced with high selectivity and high productivity stably for a prolonged period of time on an industrial scale of not less than 1 ton per hour using two continuous multi-stage distillation columns from a dialkyl carbonate and an aromatic monohydroxy compound.

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CLAIMS

We claim:

1. A process for the production of an aromatic carbonate containing a diaryl carbonate as a main product from a dialkyl carbonate and an aromatic monohydroxy compound as a starting material, which comprises the steps of:

(i) continuously feeding said starting material into a first continuous multi-stage distillation column in which a catalyst is present;

(ii) carrying out the reaction in said first column to produce an alcohol and an alkyl aryl carbonate;

(iii) continuously withdrawing a first column low boiling point reaction mixture containing a produced alcohol from an upper portion of said first column in a gaseous form while continuously withdrawing a first column high boiling point reaction mixture containing an alkyl aryl carbonate from a lower portion of said first column in a liquid form;

(IV) continuously feeding said first column high boiling point reaction mixture into a second continuous multi-stage distillation column in which a catalyst is present and which is connected to said first column while carrying out the reaction in said second column to produce a dialkyl carbonate and a diaryl carbonate;

(V) continuously withdrawing a second column low boiling point reaction mixture containing said produced dialkyl carbonate from an upper portion of said second column in a gaseous form while continuously withdrawing a second column high boiling point reaction mixture containing said produced diaryl carbonate from a lower portion of said second column in a liquid form; wherein

(a) said starting material which is fed continuously into said first continuous multi-stage distillation column

(1) has a molar ratio of the dialkyl carbonate to the aromatic monohydroxy compound is in a range of from 0.1 to 10; and

(2) contains 0.01 to 5 % by weight of said alcohol and 0.01 to 5 % by weight of said alkyl aryl carbonate and/or said diaryl carbonate, based on the total weight of said starting material;

(b) said first continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_1 (cm) and an inside diameter D_1 (cm), and having an internal with a number of stages n_1 thereinside, and has a gas outlet having an inside diameter d_{11} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet having an inside diameter d_{12} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_1 (cm) satisfies the following formula (1),

$$1500 \leq L_1 \leq 8000 \quad (1),$$

(2) said inside diameter D_1 (cm) of the column satisfies the following formula (2),

$$100 \leq D_1 \leq 2000 \quad (2),$$

(3) a ratio of said length L_1 (cm) to said inside diameter D_1 (cm) of the column satisfies the following formula (3),

$$2 \leq L_1 / D_1 \leq 40 \quad (3),$$

(4) said number of stages n_1 satisfies the following formula (4),

$$20 \leq n_1 \leq 120 \quad (4),$$

(5) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{11} (cm) of the gas outlet satisfies the following formula (5),

$$5 \leq D_1 / d_{11} \leq 30 \quad (5), \text{ and}$$

(6) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{12} (cm) of the liquid outlet satisfies the following formula (6),

$$3 \leq D_1 / d_{12} \leq 20 \quad (6);$$

5 (c) said second continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_2 (cm) and an inside diameter D_2 (cm), and having an internal with a number of stages n_2 thereinside, and has a gas outlet having an inside diameter d_{21} (cm) at the top of the column or in an upper portion of the column near to the top, a
10 liquid outlet having an inside diameter d_{22} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_2 (cm) satisfies the following formula (7),

$$15 \quad 1500 \leq L_2 \leq 8000 \quad (7),$$

(2) said inside diameter D_2 (cm) of the column satisfies the following formula (8),

$$100 \leq D_2 \leq 2000 \quad (8),$$

(3) a ratio of the length L_2 (cm) to said inside diameter D_2 (cm) of the column
20 satisfies the following formula (9),

$$2 \leq L_2 / D_2 \leq 40 \quad (9),$$

(4) said number of stages n_2 satisfies the following formula (10),

$$10 \leq n_2 \leq 80 \quad (10),$$

(5) a ratio of said inside diameter D_2 (cm) of the column to said inside
25 diameter d_{21} (cm) of the gas outlet satisfies the following formula (11),

$$2 \leq D_2 / d_{21} \leq 15 \quad (11), \text{ and}$$

(6) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{22} (cm) of the liquid outlet satisfies the following formula (12),

$$5 \leq D_2 / d_{22} \leq 30 \quad (12).$$

5 2. The process according to claim 1, wherein distillation is carried out simultaneously in said step (ii) and said step (iv).

3. The process according to claim 1 or 2, wherein an amount of said diaryl carbonate produced is not less than 1 ton per hour.

10 4. In a process for the production of an aromatic carbonate containing a diaryl carbonate as a main product in which the aromatic carbonate containing the diaryl carbonate as the main product are produced continuously by taking a mixture of a dialkyl carbonate and an aromatic monohydroxy compound as a starting
15 material, continuously feeding the starting material into a first continuous multi-stage distillation column in which a catalyst is present, carrying out the reaction and the distillation simultaneously said the first column, continuously withdrawing a first column low boiling point reaction mixture containing a produced alcohol from an upper portion of said first column in a gaseous form, continuously withdrawing a first
20 column high boiling point reaction mixture containing a produced alkyl aryl carbonate from a lower portion of said first column in a liquid form, continuously feeding the first column high boiling point reaction mixture into a second continuous multi-stage distillation column in which a catalyst is present, carrying out the reaction and the distillation simultaneously in said second column, continuously withdrawing a second
25 column low boiling point reaction mixture containing a produced dialkyl carbonate from an upper portion of said second column in a gaseous form, continuously

withdrawing a second column high boiling point reaction mixture containing a produced diaryl carbonate from a lower portion of said second column in a liquid form while continuously feeding the second column low boiling point reaction mixture containing the dialkyl carbonate into the first continuous multi-stage distillation

5 column, the improvement in which:

(a) said starting material which is fed continuously into said first continuous multi-stage distillation column

(1) has a molar ratio of the dialkyl carbonate to the aromatic monohydroxy compound is in a range of from 0.1 to 10; and

10 (2) contains 0.01 to 5 % by weight of said alcohol and 0.01 to 5 % by weight of said alkyl aryl carbonate and/or said diaryl carbonate, based on the total weight of said starting material;

(b) said first continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a
15 length L_1 (cm) and an inside diameter D_1 (cm), and having an internal with a number of stages n_1 therein, and has a gas outlet having an inside diameter d_{11} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet having an inside diameter d_{12} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper
20 portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_1 (cm) satisfies the following formula (1),

$$1500 \leq L_1 \leq 8000 \quad (1),$$

(2) said inside diameter D_1 (cm) of the column satisfies the following formula

25 (2),

$$100 \leq D_1 \leq 2000 \quad (2),$$

(3) a ratio of said length L_1 (cm) to said inside diameter D_1 (cm) of the column satisfies the following formula (3),

$$2 \leq L_1 / D_1 \leq 40 \quad (3),$$

(4) said number of stages n_1 satisfies the following formula (4),

5
$$20 \leq n_1 \leq 120 \quad (4),$$

(5) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{11} (cm) of the gas outlet satisfies the following formula (5),

$$5 \leq D_1 / d_{11} \leq 30 \quad (5), \text{ and}$$

(6) a ratio of said inside diameter D_1 (cm) of the column to said inside diameter d_{12} (cm) of the liquid outlet satisfies the following formula (6),

10
$$3 \leq D_1 / d_{12} \leq 20 \quad (6);$$

(c) said second continuous multi-stage distillation column comprises a structure having a pair of end plates above and below a cylindrical trunk portion having a length L_2 (cm) and an inside diameter D_2 (cm), and having an internal with a number of stages n_2 thereinside, and has a gas outlet having an inside diameter d_{21} (cm) at the top of the column or in an upper portion of the column near to the top, a liquid outlet having an inside diameter d_{22} (cm) at the bottom of the column or in a lower portion of the column near to the bottom, at least one inlet provided in the upper portion and/or a middle portion of the column below the gas outlet, and at least one inlet provided in the lower portion of the column above the liquid outlet, wherein

(1) said length L_2 (cm) satisfies the following formula (7),

$$1500 \leq L_2 \leq 8000 \quad (7),$$

(2) said inside diameter D_2 (cm) of the column satisfies the following formula (8),

25
$$100 \leq D_2 \leq 2000 \quad (8),$$

(3) a ratio of the length L_2 (cm) to said inside diameter D_2 (cm) of the column

satisfies the following formula (9),

$$2 \leq L_2 / D_2 \leq 40 \quad (9),$$

(4) said number of stages n_2 satisfies the following formula (10),

$$10 \leq n_2 \leq 80 \quad (10),$$

5 (5) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{21} (cm) of the gas outlet satisfies the following formula (11),

$$2 \leq D_2 / d_{21} \leq 15 \quad (11), \text{ and}$$

(6) a ratio of said inside diameter D_2 (cm) of the column to said inside diameter d_{22} (cm) of the liquid outlet satisfies the following formula (12),

10
$$5 \leq D_2 / d_{22} \leq 30 \quad (12).$$

5. The process according to claim 4, wherein an amount produced of the diaryl carbonate is not less than 1 ton per hour.

15 6. The process according to any one of claims 1 to 5, wherein said starting material further contains 0.5 to 15 % by weight of alkyl aryl ether, based on the total weight of said starting material.

7. The process according to any one of claims 1 to 6, wherein d_{11} and d_{12}
20 satisfy the following formula (13), and d_{21} and d_{22} satisfy the following formula (14)

$$1 \leq d_{12} / d_{11} \leq 5 \quad (13)$$

$$1 \leq d_{21} / d_{22} \leq 6 \quad (14).$$

8. The process according to any one of items 1 to 7, wherein L_1 , D_1 , L_1 / D_1 ,
25 n_1 , D_1 / d_{11} , and D_1 / d_{12} for said first continuous multi-stage distillation column satisfy the following formulae: $2000 \leq L_1 \leq 6000$, $150 \leq D_1 \leq 1000$, $3 \leq L_1 / D_1$

≤ 30 , $30 \leq n_1 \leq 100$, $8 \leq D_1/d_{11} \leq 25$, and $5 \leq D_1/d_{12} \leq 18$, respectively, and

L_2 , D_2 , L_2/D_2 , n_2 , D_2/d_{21} , and D_2/d_{22} for said second continuous multi-stage distillation column satisfy the following formulae: $2000 \leq L_2 \leq 6000$, $150 \leq D_2$
 5 ≤ 1000 , $3 \leq L_2/D_2 \leq 30$, $15 \leq n_2 \leq 60$, $2.5 \leq D_2/d_{21} \leq 12$, and $7 \leq D_2/d_{22} \leq 25$, respectively.

9. The process according to any one of claims 1 to 8, wherein L_1 , D_1 , L_1/D_1 , n_1 , D_1/d_{11} , and D_1/d_{12} for said first continuous multi-stage distillation column satisfy
 10 the following formulae: $2500 \leq L_1 \leq 5000$, $200 \leq D_1 \leq 800$, $5 \leq L_1/D_1 \leq 15$, $40 \leq n_1 \leq 90$, $10 \leq D_1/d_{11} \leq 25$, and $7 \leq D_1/d_{12} \leq 15$, respectively, and

L_2 , D_2 , L_2/D_2 , n_2 , D_2/d_{21} , and D_2/d_{22} for said second continuous multi-stage distillation column satisfy the following formulae: $2500 \leq L_2 \leq 5000$, $200 \leq D_2$
 15 ≤ 800 , $5 \leq L_2/D_2 \leq 15$, $20 \leq n_2 \leq 50$, $3 \leq D_2/d_{21} \leq 10$, and $9 \leq D_2/d_{22} \leq 20$, respectively.

10. The process according to any one of claims 1 to 9, wherein each of said first continuous multi-stage distillation column and said second continuous
 20 multi-stage distillation column is a distillation column having a tray and/or a packing as the internal.

11. The process according to claim 10, wherein said first continuous multi-stage distillation column is a plate-type distillation column having the tray as the
 25 internal, and said second continuous multi-stage distillation column is a distillation column having both the packing and the tray as the internal.

12. The process according to claim 10 or 11, wherein each of the trays in said first continuous multi-stage distillation column and said second continuous multi-stage distillation column is a sieve tray having a sieve portion and a down
5 comer portion.

13. The process according to claim 12, wherein said sieve tray has 100 to 1000 holes/m² in the sieve portion.

10 14. The process according to claim 12 or 13, wherein the cross-sectional area per hole of said sieve tray is in a range of from 0.5 to 5 cm².

15 15. The process according to claim 10 or 11, wherein said second continuous multi-stage distillation column is a distillation column having, as said internal, the packing in an upper portion of the column, and the tray in a lower portion of the column.

20 16. The process according to any one of claims 10 to 15, wherein said packing of said internal in said second continuous multi-stage distillation column is one or more of a structured packing.

25 17. The process according to claim 16, wherein said structured packing in said second continuous multi-stage distillation column is of at least one selected from the group consisting of Mellapak, Gempak, TECHNO-PAK, FLEXI-PAK, a Sulzer packing, a Goodroll packing and a Glitchgrid.

18. The process according to any one of claims 1 to 17, wherein said first continuous multi-stage distillation column comprises two or more of distillation columns.

5 19. The process according to any one of claims 1 to 18, wherein said second continuous multi-stage distillation column comprises two or more of distillation columns.

20. An aromatic carbonate comprising a halogen content of not more than
10 0.1 ppm, produced by the process according to any one of claims 1 to 19.