

as originally filed

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Preparation of acrylic acid and methacrylic acid

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The present invention relates to a process for preparing acrylic acid or methacrylic acid.

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Acrylic acid is a major basic chemical product. Owing to its very reactive double bond and the acid function, it is particularly useful as a monomer for preparing polymers. The bulk of acrylic acid monomer production is esterified prior to polymerization, for example to make adhesives, dispersions or coatings. Just a fraction of acrylic acid monomer production is polymerized directly, for example to make superabsorbents. Whereas, in general, the direct polymerization of acrylic acid requires high purity monomer, acrylic acid purity requirements are not so high if the acrylic acid is esterified before it is polymerized.

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It is common knowledge that acrylic acid can be produced by heterogeneously catalyzed gas phase oxidation of propene with molecular oxygen over solid catalysts at from 200 to 400°C in one or two stages via acrolein (cf. eg. DE-A-1 962 431, DE-A-2 943 707, DE-C-1 205 502, DE-A-195 08 558, EP-A-0 257 565, EP-A-0 253 409, DE-A-2 251 364, EP-A-0 117 146, GB-B-1 450 986 and EP-A-0 293 224). The catalysts used are oxidic multicomponent catalysts based, for example, on oxides of the elements molybdenum, bismuth and iron (in stage 1) or molybdenum and vanadium (in stage 2).

DE-C-2 136 396 discloses removing the acrylic acid from the reaction gases obtained by catalytic gas phase oxidation of propene or acrolein by countercurrent absorption with a mixture of about 75% by weight of diphenyl ether and about 5 25% by weight of biphenyl. DE-A-2 449 780 describes cooling the hot reaction gas by partial evaporation of the solvent in a direct condenser (quench apparatus) prior to the countercurrent absorption. The problem here is, as with further process steps, the production of solids in the apparatus, reducing plant availability. According to DE-A-4 308 087, this production of solids can be reduced by adding a polar 10 solvent such as dimethyl phthalate in an amount of from 0.1 to 25% by weight to the relatively apolar solvent mixture of diphenyl ether and biphenyl.

In addition to the above-described absorption of the reaction product comprising acrylic acid into a high boiling solvent mixture, other known processes envisage a 15 total condensation of acrylic acid and of the water of reaction formed in the course of the catalytic oxidation. This gives rise to an aqueous acrylic acid solution which can be further worked up via distillation with an azeotrope (cf. DE-C-3 429 391, JP-A-1 124 766, JP-A-7 118 766, JP-A-7 118 966-R, JP-A-7 118 968-R, JP-A- 7 241 885) or via an extraction process (cf. DE-A-2 164 767, JP-A-5 81 40-039 20 and JP-A-4 80 91 013). In EP-A-0 551 111, the mixture of acrylic acid and by-products produced by means of catalytic gas phase oxidation is contacted with water in an absorption tower and the resulting aqueous solution is distilled in the presence of a solvent that forms an azeotrope with polar low boilers such as water or acetic acid. DE-C-2 323 328 describes removing acrylic acid from an aqueous 25 butanol/acrylic acid esterification waste liquor by extraction with a specific mixture of organic solvents.

The processes described above have the disadvantage of employing for the extraction or absorption an organic solvent which has to be removed again in a

further operation, such as a rectification, under high thermal stress. This may cause the acrylic acid to polymerize.

JP-A-07 082 210 describes a process for purifying an acrylic acid comprising
5 acetic acid, propionic acid, acrolein and furfural as well as acrylic acid. This process comprises adding water and then crystallizing under reduced pressure to obtain a purity of 99.6% for the acrylic acid crystals after removal and washing. Japanese Patent 45-32417 discloses a process wherein an aqueous acrylic or methacrylic acid solution additionally comprising acetic acid and propionic acid is
10 extracted with heptane or toluene before water is removed from the extract by distillation. In the next step, the remaining extract is cooled down to -20 to -80°C to bring about a crystallization of acrylic acid or methacrylic acid. The crystals are removed, and the mother liquor is recycled into the extraction process. According to this patent, it is necessary to use an organic solvent or extractant, since the
15 solution otherwise solidifies on cooling without forming crystals. This process is disadvantageous in that, as well as requiring the addition of an organic solvent, a distillation has to be carried out to remove water. Canadian Patent 790 625 relates to a further purification process for crude acrylic acid by fractional crystallization. In this process, if propionic acid is the main impurity in the crude acrylic acid, the
20 temperature is not reduced below the peritectic temperature of the acrylic acid/propionic acid system, whereas it is not reduced below the eutectic temperature of the acrylic acid/acetic acid system when acetic acid is the main impurity. The acrylic acid used for crystallization in this process is prepared by conventional processes, for example by gas phase oxidation of propene or acrolein,
25 and then subjected to a prepurification by conventional known processes, for example extraction. The crystallization of acrylic acid is said to be preferably carried out in the substantial absence of water.

EP-A-0 616 998 describes a process for purifying acrylic acid by a combination of dynamic and static crystallization of a prepurified acrylic acid, for example an acrylic acid which has been prepurified by distillation.

5 Common to the processes described in the above documents is that they require a (pre)purification of the acrylic acid prior to crystallization. Since the prepurification generally utilizes organic solvents which have to be subsequently separated off again under high thermal stress, there is always the risk of the acrylic acid undergoing premature polymerization.

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EP-A-0 002 612, which relates to a process for purifying acrylic acid in aqueous solution by fractional crystallization, discloses the addition of salts to the acrylic acid solution so as to break up the water/acrylic acid eutectic system which exists at an acrylic acid content of 63% by volume.

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EP-A-0 675 100 describes a process for preparing α,β -unsaturated C₃-C₆-carboxylic acids, eg. methacrylic acid, by oxidative dehydrogenation of the corresponding saturated C₃-C₆-carboxylic acid, followed by melt crystallization with subsequent fractional distillation or followed by fractional distillation with
20 subsequent melt crystallization.

It is an object of the present invention to provide a process for obtaining acrylic acid or methacrylic acid in high purity without complex operations.

25 This object is achieved on the basis of the process for removing acrylic acid or methacrylic acid from a gaseous mixture which, as well as acrylic acid or methacrylic acid, additionally includes at least one further component.

The novel process for removing acrylic acid or methacrylic acid comprises

- a) condensing said gaseous mixture,
- b) crystallizing acrylic acid or methacrylic acid from the solution obtained in
5 step a),
- c) removing the resulting crystals from the mother liquor of step b), and
- d) after removal recycling at least a portion of said mother liquor from step c)
into step a).

10 The invention also provides a process for preparing acrylic acid or methacrylic acid. This process is based on the catalytic gas phase oxidation of C₃-/C₄-alkanes, -alkenes, -alkanols and/or -alkanals and/or precursors thereof to form a crude product which, as well as acrylic acid or methacrylic acid, additionally includes at least one component selected from the group consisting of unconverted starting
15 materials and by-products. The preparative process of the invention comprises working up the gaseous crude product by the above novel process for removing acrylic acid or methacrylic acid.

20 We have found that this object is achieved by a process whereby acrylic acid or methacrylic acid from a gaseous product mixture which has been subjected to a condensation can be crystallized directly from the solution formed in the condensation. Of particular significance here is the fact that the process found requires no further purifying step and no addition of assistants.

25 In a preferred embodiment, the condensation of step (a) is carried out in a column. Further preferred embodiments of the invention will be apparent from the description which follows, and the Example.

In the process of the present invention, acrylic acid or methacrylic acid is crystallized directly and unmediatedly without further intermediary or purifying steps and without addition of assistants from the solution which is formed in the course of the condensation of the product mixture. This product mixture has essentially the composition of a reaction product formed in a catalytic gas phase oxidation process to form acrylic acid or methacrylic acid.

The sole figure illustrates a preferred embodiment of carrying out the process of the present invention.

Preparation of a gaseous product mixture including acrylic acid or methacrylic acid

First of all, a gaseous product mixture is produced which essentially has the composition of a reaction mixture of the catalytic gas phase oxidation of C₃- or C₄-alkanes, -alkenes, -alkanols and/or -alkanals and/or precursors thereof to form acrylic acid or methacrylic acid. It is particularly advantageous for the gaseous product mixture to be prepared by catalytic gas phase oxidation of propene, propane, acrolein, tert-butanol, isobutene, isobutane, isobutyraldehyde, methacrolein, isobutyric acid or methyl tert-butyl ether. Suitable starting compounds include all precursors of the abovementioned C₃/C₄ compounds from which the actual C₃/C₄ starting compound is formed as an intermediate during the gas phase oxidation. Examples which may be mentioned here are methyl tert-butyl ether and isobutyric acid for the production of methacrylic acid. Both acrylic acid and methacrylic acid can be produced directly from propane and isobutane, respectively.

The crude product is preferably a gaseous mixture of the catalytic gas phase oxidation of C₃-/C₄-alkanes, -alkenes, -alkanols and/or -alkanals and/or precursors thereof to form acrylic acid or methacrylic acid.

5 A particularly advantageous source of the gaseous product mixture to be used in the process of the present invention is the catalytic gas phase conversion of propene and/or acrolein into acrylic acid using molecular oxygen according to known processes, especially as described in the above-cited references. This gas phase reaction is preferably carried out at from 200 to 450°C with or without
10 superatmospheric pressure. The heterogeneous catalysts used are preferably oxidic multicomponent catalysts based on the oxides of molybdenum, bismuth and iron in the first stage (oxidation of propene to acrolein) and the oxides of molybdenum and vanadium in the second stage (oxidation of acrolein to acrylic acid). These reactions are carried out, for example, as single-stage or two-stage processes.
15 When propane is used as a starting material, it can be converted into a propene/propane mixture by: catalytic oxydehydrogenation as described, for example, in Catalysis Today 24 (1995), 307-313, or US-A-5 510 558; by homogeneous oxydehydrogenation, as described for example, in CN-A-1 105 352; or by catalytic dehydrogenation as described, for example, in EP-A-0 253 409, DE-
20 A-195 08 558, EP-A-0 293 224 or EP-A-0 117 146. Further suitable propene/propane mixtures are refinery propene (70% of propene and 30% of propane) or cracker propene (95% of propene and 5% of propane). In principle, propene/propane mixtures such as those mentioned above can be oxidized with oxygen or air or a mixture of oxygen and nitrogen of any composition to acrolein
25 and acrylic acid. When a propene/propane mixture is used, propane acts as diluent and/or reactant. A suitable process is also described in EP-B-0 608 838, wherein propane as reactant is directly converted into acrylic acid.

The conversion of propene into acrylic acid is strongly exothermic. The reaction
30 gas, which as well as the starting materials and the products advantageously

includes an inert diluent gas, for example recycle gas (see below), atmospheric nitrogen, one or more saturated C₁-C₆-hydrocarbons, especially methane and/or propane, and/or water vapor, can therefore absorb only a small fraction of the heat of reaction. Although the type of reactor used is not subject to any restriction per se, it is common to use tube bundle heat exchangers packed with the oxidation catalyst, since with this type of apparatus the predominant fraction of the heat of reaction can be removed to the cooled tube walls by convection and radiation.

The catalytic gas phase oxidation process produces not pure acrylic acid, but a gaseous mixture which, as well as acrylic acid, may essentially include as secondary components unconverted acrolein and/or propene, water vapor, carbon monoxide, carbon dioxide, nitrogen, propane, oxygen, acetic acid, propionic acid, formaldehyde, further aldehydes and maleic anhydride. The reaction product mixture customarily comprises (each percentage based on the total reaction mixture) from 1 to 30% by weight of acrylic acid, from 0.05 to 1% by weight of propene and from 0.05 to 1% by weight of acrolein, from 0.05 to 10% by weight of oxygen, from 0.05 to 2% by weight of acetic acid, from 0.01 to 2% by weight of propionic acid, from 0.05 to 1% by weight of formaldehyde, from 0.05 to 2% by weight of aldehydes, from 0.01 to 0.5% by weight of maleic anhydride and from 20 to 98% by weight, preferably from 50 to 98% by weight, of inert diluent gases. The inert diluent gases present include, in particular, saturated C₁-C₆-hydrocarbons, such as from 0 to 90% by weight of methane and/or propane, and also from 1 to 30% by weight of water vapor, from 0.05 to 15% by weight of carbon oxides and from 0 to 90% by weight of nitrogen, each percentage being based on 100% by weight of diluent gas.

Methacrylic acid can be prepared similarly to acrylic acid by catalytic gas phase reaction of C₄ starting compounds with molecular oxygen. A particularly advantageous way to obtain methacrylic acid is, for example, by catalytic gas phase oxidation of isobutene, isobutane, tert-butanol, isobutyraldehyde, methacrolein or

5 methyl tert-butyl ether. The catalysts used are again transition metal mixed oxide catalysts (eg. Mo, V, W and/or Fe), and the reaction is carried out, for example, as single-stage processes or as multi-stage processes. Particularly suitable processes for producing methacrylic acid are those which are based on methacrolein, especially when the methacrolein is produced by gas phase catalytic oxidation of tert-butanol, isobutane or isobutene or by reaction of formaldehyde with propionaldehyde as described in EP-B-0 092 097 or EP-B-0 058 927. It is thus possible to prepare methacrylic acid in two stages by (I) condensation of propionaldehyde with formaldehyde (in the presence of a secondary amine as catalyst) to form methacrolein and (II) subsequent oxidation of the methacrolein to methacrylic acid. A further suitable process is described in EP-B-0 608 838, wherein isobutane as reactant can be converted directly into methacrylic acid.

15 As with the production of acrylic acid, the product is not pure methacrylic acid, but a gaseous mixture which, as well as methacrylic acid, may essentially include as secondary components unconverted methacrolein and/or water vapor, carbon monoxide, carbon dioxide, nitrogen, oxygen, acetic acid, propionic acid, further aldehydes and maleic anhydride. The process of the present invention is used especially when the reaction mixture comprises from 0.02 to 2% by weight of methacrolein, based on the total reaction mixture, and otherwise essentially the same corresponding constituents as with the production of acrylic acid.

Step (a):

25 Step (a) subjects the gaseous product mixture including acrylic acid or methacrylic acid to a condensation, particularly to a partial or total condensation, to obtain a solution.

The condensation is preferably carried out in a column. The column used has separatory internals, especially ordered packings, random packings and/or trays, preferably bubblecap trays, sieve trays, valve trays and/or dual-flow trays. In the column, the condensible components of the gaseous product mixture produced are condensed out fractionally by cooling. Since the gas mixture as a result of contamination and diluent gases comprises a high boilers fraction, a medium boilers fraction and a low boilers fraction as well as uncondensable components, the column can be provided with one or more sidestream takeoffs at appropriate locations. Unlike a conventional condensation, condensation in a column even provides for a separation into the individual components. Suitable columns comprise at least one cooling means. Suitable cooling means include all heat transferors or heat exchangers in which the heat released in the course of the condensation is removed indirectly (externally). Tube bundle heat exchangers, plate heat exchangers and air coolers are preferred. Suitable cooling media are air in the case of an air cooler and cooling liquids, especially water, in the case of other cooling means. If only one cooling means is provided, it is installed at the top of a column in which the low boilers fraction is condensed out. Since the acrylic or methacrylic acid gas mixture has a plurality of fractions, it is advantageous to install a plurality of cooling means in various sections of the column, for example a cooling means in the lower section of the column to condense out the high boilers fraction and a cooling means at the top of the column to condense out the low boilers fraction. The fraction with the acrylic or methacrylic acid is withdrawn in the middle part of the column via one or more sidestream takeoffs. The solution crystallized in step (b) is thus withdrawn as medium boilers fraction in the course of the condensation. The pressure in the column depends on the amount of uncondensable components and is preferably 0.5-5 bar absolute, especially 0.8-3 bar absolute. The exact operating conditions for the column, such as temperature and pressure profile, interconnection and disposition of the cooling means, disposition of the sidestream takeoff(s) to take off the acrylic or methacrylic acid, choice of column height and of column diameter, number and spacing of separatory internals in the column or type of separatory column internals, can be determined by a

person of ordinary skill in the art in the course of the customary experiments conducted in the course of the design of a separation process. In a preferred embodiment, the hot gas mixture is cooled down directly or indirectly prior to the condensing out. When the gas mixture is cooled directly, it is preferably cooled
5 down using the high boilers fraction condensed out of the gas mixture. Alternatively, an assistant is introduced into the process, but it has to be worked up again. In apparatus terms, this precooling can take place integrated in the bottom region of the column (with or without column internals) or away from the column in a separate apparatus, for example a gas cooler, a quench or a flash top. In a
10 particularly preferred embodiment of the invention, the condensation of the gaseous reaction mixture takes place in a column as follows, the column being divisible into various sections in which different technical objectives are achieved:

- Bottom region:

15 Cooling the hot gas mixture

The hot gas mixture is introduced and cooled down in the bottom region. This can be accomplished by indirect cooling, for example heat exchangers, or direct cooling with high boilers fraction condensed in the next section of the column as
20 cooling medium.

- First cooling circuit:

Condensing the high boilers fraction

25 In the region of the first cooling circuit, the heat of condensation is removed externally via the first cooling circuit by means of a heat exchanger utilizing, for example, water as cooling medium by discharging condensed high boilers fraction from the column, cooling it with the aid of the heat exchanger and returning a

portion of the cooled, condensed high boilers fraction into the column, while the other portion, customarily less than 1% by weight, based on 100% by weight of condensate in the sidestream takeoff, is removed from the system. The returned, condensed high boilers fraction is passed countercurrently to the ascending gas.

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- First cooling circuit to sidestream takeoff:

High boilers enrichment

10 The column section between the first cooling circuit and the sidestream takeoff is where the high boilers fraction is distillatively enriched and condensed out of the countercurrently upwardly moving gas stream in the direction of the first cooling circuit.

- Sidestream takeoff:

15 Taking off the acid

The sidestream takeoff is where the acrylic or methacrylic acid is removed.

- Sidestream takeoff to second cooling circuit:

20 Enriching the medium boilers fraction

The column region between the sidestream takeoff and the second cooling circuit is where the medium boilers fraction is enriched from the countercurrently upwardly moving gas stream, the medium boilers fraction being enriched in the direction of the sidestream takeoff.

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- Second cooling circuit:

Condensing the low boilers fraction

5 The region of the second cooling circuit is where the low boilers fraction is condensed out of the countercurrently upwardly moving gas stream. The heat of condensation is removed externally via the second cooling circuit by means of a heat exchanger utilizing, for example, water as cooling medium by discharging condensed low boilers fraction, cooling it and returning a portion of the cooled, condensed low boilers fraction into the column, while the other portion is removed
10 from the system. The uncondensed components, which are preferably nitrogen, carbon monoxide, carbon dioxide, oxygen, methane, propane and propene, are withdrawn from the column overhead.

15 The condensation can also be effected in one or more stages according to customary processes, in which case the type of condensation is not subject to any special restriction. The condensation is advantageously carried out in a direct condenser where previously produced condensate is contacted with the hot gaseous reaction product. Suitable apparatuses for the condensation are in particular spray scrubbers, Venturi scrubbers, bubble columns or apparatuses having betrickled
20 surfaces.

The mixture obtained by partial or total condensation of the reaction product of the gaseous product mixture produced, especially the column condensate of the medium boilers fraction, preferably comprises from 60 to 99.5% by weight of acrylic or methacrylic acid, from 0.1 to 40% by weight of water, and also from 0.1
25 to 15% by weight of impurities, especially, each percentage being based on 100% by weight of condensate, from 0.01 to 5% weight of (meth)acrolein, from 0.05 to 5% by weight of acetic acid, from 0.01 to 5% by weight of propionic acid, from 0.01 to 5% by weight of formaldehyde, from 0.01 to 5% by weight of further

aldehydes and from 0.01 to 5% by weight of maleic acid. It is particularly preferable for the condensation to afford a mixture comprising from 93 to 98% by weight of acrylic or methacrylic acid, from 1 to 5% by weight of water, and also from 0.5 to 5% by weight of impurities, especially, each percentage being based on 100% by weight of condensate, from 0.01 to 3% by weight of acrolein or methacrolein, from 0.1 to 3% by weight of acetic acid, from 0.01 to 3% by weight of propionic acid, from 0.01 to 3% by weight of formaldehyde, from 0.01 to 3% by weight of further aldehydes and from 0.01 to 3% by weight of maleic acid.

10 Step (b):

Step (b) crystallizes the solution obtained in step (a), which comprises acrylic acid or methacrylic acid. Thus, the solution obtained in the condensation step is fed directly to the crystallization step. No solvent is added, especially no organic solvent. The crystallization process used is not subject to any restriction. The crystallization can be carried out continuously or batchwise, in one or more stages. The crystallization is preferably carried out in a single stage. In another preferred embodiment of the invention, the crystallization is carried out as a fractional crystallization. In the art of fractional crystallization it is customary to term all stages which produce a crystallizate which is purer than aqueous acrylic or methacrylic acid solution feed purifying stages and all other stages stripping stages. Multi-stage fractional crystallization processes are advantageously operated according to the countercurrent principle whereby the crystallizate is separated from the mother liquor in each stage and fed to the particular stage having the next higher degree of purity, while the crystallization residue is fed to the particular stage having the next lower degree of purity.

The temperature of the solution during the crystallization is advantageously within the range from +5°C to +14°C, especially within the range from 8°C to 12°C. The

solids content in the crystallizer is advantageously within the range from 0 to 80 g of solids/100 g, preferably within the range from 15 to 35 g of solids/100 g.

In an advantageous embodiment of the invention, the crystallizing is effected by cooling apparatus walls or by evaporating the solution under reduced pressure. In the case of the crystallizing by cooling, the heat is removed via scrape coolers connected to a stirred tank or to a vessel without stirrer. The circulation of the crystal suspension is ensured in this case by means of a pump. Alternatively, it is possible to remove the heat via the walls of a stirred tank having a close-clearance stirrer. A further preferred embodiment of cooling crystallization involves the use of cooling disc crystallizers as manufactured for example by Gouda (Netherlands). In a further suitable variant for crystallization by cooling, the heat is removed via conventional heat transferors (preferably tube bundle or plate heat transferors). These apparatuses, unlike scraped-surface coolers, stirred tanks having close-clearance stirrers or cooling disc crystallizers, have no means for avoiding crystal layers on the heat-transferring surfaces. If, in operation, a state is reached where the heat transfer resistance has become too high due to crystal layer formation, the operation is switched over to a second apparatus. During operation of the second apparatus, the first apparatus is regenerated (preferably by melting off the crystal layer or by flushing the apparatus through with unsaturated solution). If heat transfer resistance becomes too high in the second apparatus, operation is switched back again to the first apparatus, etc. This variant can also be operated with more than two apparatuses in alternation. In addition, the crystallization can be effected by conventional evaporation of the solution under reduced pressure. In a further advantageous embodiment of the invention, a crystallization takes place in apparatuses in which the crystals grow on cooled surfaces within the crystallization apparatus, ie. are immobilized in the apparatus (eg. layer crystallization process of Sulzer Chemtech (Switzerland) or static crystallization process of BEFS PROKEM (France)).

Step (c):

Step (c) separates the acrylic or methacrylic acid crystals obtained in step (b) from the mother liquor. For a layer crystallization or a static crystallization, the separation of the crystals from the mother liquor can take place in the crystallization apparatus itself, since the crystals are immobilized in the apparatus and the mother liquor can be removed from the apparatus by letting it flow out. The crystals are removed from the crystallization apparatus by melting the crystals and then letting the melt flow out. For a suspension crystallization, any known solid-liquid separation is suitable. In a preferred embodiment of the invention, the crystals are separated from the mother liquor by filtration and/or centrifugation. Advantageously, the filtration or centrifugation is preceded by a (pre)thickening of the suspension, for example by means of one or more hydrocyclones. Centrifugation can be carried out in any known centrifuge which works batchwise or continuously. It is very advantageous to use push air centrifuges which can be operated in one or more stages. Also suitable are screw sieve centrifuges or screw discharge centrifuges (decanter). A filtration is advantageously effected by means of press filters which can be operated batchwise or continuously, with or without stirrer or by means of belt filters. In general, filtration can be effected under superatmospheric pressure or under reduced pressure.

The solid-liquid separation may be accompanied and/or followed by further process steps for increasing the purity of the crystals or of the crystal cake. In a particularly advantageous embodiment of the invention, the separation of the crystals from the mother liquor is followed by a single- or multiple-stage washing and/or sweating of the crystals or of the crystal cake. In washing, the quantity of wash liquor is suitably within the range from 0 to 500 g of wash liquor/100 g of crystallizate, preferably within the range from 30 to 200 g of wash liquor/100 g of crystallizate. The wash liquor used is not subject to any restriction. It is advantageous, however, to wash with pure product, ie. with an acrylic or methacrylic

acid liquid whose purity is greater than that of the crystal cake to be washed. A wash with water is also possible. The wash can take place in customary apparatus for the purpose. It is advantageous to use wash columns in which the removal of the mother liquor and the washing take place in one and the same apparatus, centrifuges, which can be operated in one or more stages, or press filters or belt filters. The washing can be carried out on centrifuges or belt filters in one or more stages. The wash liquor can be passed in countercurrent to the crystal cake.

Sweating describes a local melting-off of impure regions. The sweat quantity is advantageously within the range from 0 to 100 g of molten-off crystallizate/100 g of crystallizate prior to sweating, preferably within the range from 5 to 35 g of molten-off crystallizate/100 g of crystallizate. It is particularly preferable to carry out the sweating on centrifuges or belt filters. A combined wash and sweat in one apparatus can also be suitable.

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The acrylic acid crystals and methacrylic acid crystals after the solid-liquid separation and any further washing and/or sweating constitute the purified acid obtained from the process. The purity of the crystals obtained is generally within the range from 97 to 99.99% by weight of acrylic acid or methacrylic acid, especially within the range from 98.5 to 99.9% by weight of acrylic acid or methacrylic acid. The crystals prepared by the process of the present invention include only very minimal amounts of impurities, such as acetic acid, maleic acid or aldehydes.

25 If desired, the purified acid can be esterified by known methods or further purified by known methods.

Step (d):

5 Step (d) recycles the mother liquor of step (c), which remains after the crystals have been separated off, at least partly directly into the condensation step (a). The proportion of recycled mother liquor is within the range from 0 to 100% by weight, especially within the range from 80 to 100% by weight, and is preferably 100% by weight.

10 The figure illustrates a preferred embodiment of the process of the present invention. The line 2 and compressor 3 supply air to the synthesis reactors 4 and 5. In addition, reactor 4 is supplied via line 9 with recycled gas which has been compressed by compressor 6 and which consists essentially of nitrogen, carbon
15 oxides and unconverted starting materials, together with propene or isobutene from line 1. The synthesis reactor 4 is where the first stage of the two-stage gas phase oxidation, namely the oxidation of propene or isobutene to the corresponding acrolein, takes place. The acrolein is then oxidized to the corresponding acid in synthesis reactor 5. This gives rise to a gaseous product mixture which, as well as the acid, comprises impurities mentioned above. This gaseous product mixture is
20 fed via line 7 to the condenser 8, where it is cooled down and condensed. Condenser 8 is constructed as a column in the figure. The uncondensed portion of the product mixture is removed via line 9, which recycles a portion as recycled gas, as described above, into reactor 4, while the other portion, preferably 50% of the total stream of line 9, is removed from the plant as a waste gas via line 10. The
25 condensed high boilers fraction is removed via line 18, while the condensed low boilers fraction is removed via line 19. The condensed medium boilers fraction, which comprises the largest proportion of the acrylic acid or methacrylic acid, is fed via line 11 (sidestream takeoff) to the crystallizer 12, where the crystallization is carried out. The mother liquor of the crystallization is fed together with the

crystallizate via line 13 to a suitable apparatus 14 for solid-liquid separation, the crystallizate being removed via line 15 and the mother liquor via line 16. At least some of the mother liquor is fed via line 17 into the condenser 8, preferably in the region of the sidestream takeoff (line 11), and thus reintroduced into the condensation step. Thus, the purified crude acid is removed via line 15.

By returning the mother liquor into the condensation stage, the present invention enables a high yield of up to 99.5% to be obtained. The process of the present invention is particularly useful for separating acrylic acid or methacrylic acid from such reaction gas mixtures as include significant amounts of water vapor.

The process of the present invention has the further advantage over existing processes that, after condensation of the product mixture produced in the gas phase oxidation, the solution formed in the condensation yields a very high quality crude acid directly by crystallization. When using a crystallization having more than one purification stage, it is possible to produce a pure acid directly, without a prepurification having to be carried out in departure from the above-cited references, Canadian Patent 790 625, JP-A-0 07 082 210-A and EP-A-0 616 998.

It is a further important advantage of the process of the present invention that the process is carried out at a relatively low temperature, ie. that the main stream of acrylic acid is removed directly as product via condensation and crystallization. Since, in contradistinction to the prior art, no assistant is added and thus no high thermal stress (especially in the case of high acrylic acid contents) is needed to remove this assistant, polymerization problems and the use of process stabilizers as in the prior art are minimized. In addition, fouling is avoided or reduced as well as a result. It is surprising that it is possible to crystallize acrylic acid solutions or methacrylic acid solutions obtained by gas phase oxidation and condensation

directly and that the products obtained have very high purity. It is particularly surprising that this is possible with aqueous condensates.

5 The Example which follows, which describes a preferred embodiment of the invention, illustrates the invention.

Example

10 Catalytic gas phase oxidation of propene generated the following gaseous product mixture at 270°C:

Table 1

Component	Concentration % by weight
Water	4.358
Formaldehyde	0.20
Acetic acid	0.43
Acrylic acid	10.1
Maleic anhydride	0.07
Benzoic acid	0.02
Acrolein	0.1
Phthalic anhydride	0.01
Propionic acid	0.002
Maleic acid	0
Allyl acrylate	0.001
Benzaldehyde	0.001
Furfural	0.002
Phenothiazine	0
Nitrogen	76.4
Oxygen	3.6
Carbon monoxide	0.75
Carbon dioxide	2.62
Propene	0.52
Propane	0.73

The mixture (10,931 g/h) was fed into condensation stage (a). The condensation apparatus used was a column equipped with 27 bubble cap trays. The temperature at the base of the column was 100°C. The heat of condensation was removed via heat transferors at trays 1 and 27. Phenothiazine was added as stabilizer at the top of the column. At tray 27, a 425 g/h stream of the following composition was taken off:

Table 2

Component	Concentration % by weight
Water	89.47
Formaldehyde	0.125
Acetic acid	6.345
Acrylic acid	4.0
Maleic anhydride	< 0.0001
Benzoic acid	< 0.0001
Acrolein	0.0541
Phthalic anhydride	< 0.0001
Propionic acid	< 0.0001
Maleic acid	< 0.0001
Allyl acrylate	0.0012
Benzaldehyde	< 0.0001
Furfural	< 0.0001
Phenothiazine	< 0.0001
Nitrogen	0

Component	Concentration % by weight
Oxygen	0
Carbon monoxide	0
Carbon dioxide	0
Propene	0
Propane	0

At the base of the column, a 2 g/h stream of the following composition was taken off:

5 Table 3

Component	Concentration % by weight
Water	1.21
Formaldehyde	0.0036
Acetic acid	0.879
Acrylic acid	39.45
Maleic anhydride	34.55
Benzoic acid	10.931
Acrolein	0.0103
Phthalic anhydride	5.465
Propionic acid	0.0477
Maleic acid	< 0.0001
Allyl acrylate	0.0113

Component	Concentration % by weight
Benzaldehyde	< 0.2673
Furfural	< 0.3639
Phenothiazine	6.8039
Nitrogen	0
Oxygen	0
Carbon monoxide	0
Carbon dioxide	0
Propene	0
Propane	0

The waste gas had the following composition:

5 Table 4

Component	Concentration % by weight
Water	0.982
Formaldehyde	0.239
Acetic acid	0.0305
Acrylic acid	0.0103
Maleic anhydride	< 0.0001
Benzoic acid	< 0.0001

Component	Concentration % by weight
Acrolein	0.1253
Phthalic anhydride	< 0.0001
Propionic acid	< 0.0001
Maleic acid	< 0.0001
Allyl acrylate	< 0.0001
Benzaldehyde	< 0.0001
Furfural	< 0.0001
Phenothiazine	< 0.0001
Nitrogen	89.054
Oxygen	4.1797
Carbon monoxide	0.873
Carbon dioxide	3.050
Propene	0.6054
Propane	0.850

The condensation column waste gas was recycled into the reaction (60% by weight) or removed from the process (40% by weight).

- 5 At tray 11, a 4657 g/h liquid stream at 84.5°C was taken off the column and then crystallized. This stream had the following composition:

Table 5

Component	Concentration % by weight
Water	2.52
Formaldehyde	0.0062
Acetic acid	5.899
Acrylic acid	90.972
Maleic anhydride	0.399
Benzoic acid	< 0.0001
Acrolein	0.0128
Phthalic anhydride	< 0.0001
Propionic acid	0.0564
Maleic acid	< 0.0001
Allyl acrylate	0.0548
Benzaldehyde	0.0006
Furfural	0.0492
Phenothiazine	0.0300
Nitrogen	0
Oxygen	0
Carbon monoxide	0
Carbon dioxide	0
Propene	0

Component	Concentration % by weight
Propane	0

The mixture from tray 11 was crystallized in a 10 l stirred vessel equipped with a helical stirrer. The heat of crystallization was removed via the jacket of the vessel. The equilibrium temperature of the solution was 4.8°C. The suspension (30 g of solids/100 g of suspension) produced in the crystallization stage was separated into crystals and mother liquor on a centrifuge at 2000 rpm (centrifuge diameter 250 mm) for one min. The crystals (1281 g/h) were then washed with molten crystallize (296 g/h) at 2000 rpm for 1 min.

10 The mother liquor (3376 g/h) was recycled onto tray 10 of the condensation column together with the wash liquor. Analysis of the crystals revealed the following composition:

Table 6

Component	Concentration % by weight
Water	0.1066
Formaldehyde	0.0003
Acetic acid	0.9619
Acrylic acid	98.8816
Maleic anhydride	0.0225
Benzoic acid	< 0.0001
Acrolein	0.0009
Phthalic anhydride	< 0.0001

Component	Concentration % by weight
Propionic acid	0.0162
Maleic acid	< 0.0001
Allyl acrylate	0.0031
Benzaldehyde	< 0.0001
Furfural	0.0028
Phenothiazine	0.0041
Nitrogen	0
Oxygen	0
Carbon monoxide	0
Carbon dioxide	0
Propene	0
Propane	0

As can be seen in Table 6, the process of the present invention makes it possible to prepare high purity acrylic acid.



We claim:

1. A process for removing acrylic acid or methacrylic acid from a gaseous mixture which, as well as acrylic acid or methacrylic acid, includes at least one further component, which comprises
 - a) condensing said gaseous mixture,
 - b) crystallizing acrylic acid or methacrylic acid from the solution obtained in step a),
 - c) removing the resulting crystals from the mother liquor of step b),
 - d) recycling at least a portion of said mother liquor from step c) into
2. A process as claimed in claim 1, wherein said gaseous mixture is the crude product of the catalytic gas phase oxidation of C₃-/C₄-alkanes, -alkenes, -alkanols and/or -alkanals and/or precursors thereof to form acrylic acid or methacrylic acid.
3. A process for preparing acrylic acid or methacrylic acid by catalytic gas phase oxidation of C₃-/C₄-alkanes, -alkenes, -alkanols and/or -alkanals and/or precursors thereof to form a crude product which, as well as acrylic acid or methacrylic acid, additionally includes at least one component selected from the group consisting of unconverted starting materials and by-products, which comprises working up said gaseous crude product by the process of claim 1.



4. A process as claimed in any of claims 1 to 3, wherein said condensing of step (a) is carried out in a column having separatory internals.
- 5 5. A process as claimed in claim 4, wherein said condensing is effected by withdrawing the solution which is crystallized in step (b) as the medium boilers fraction.
6. A process as claimed in any of claims 1 to 5, wherein said crystallizing of step (b) is effected in one or more stages.
- 10 7. A process as claimed in any of claims 1 to 6, wherein said crystallizing of step (b) is effected at a temperature of said solution within the range from +5°C to +14°C.
- 15 8. A process as claimed in any of claims 1 to 7, wherein said crystallizing of step (b) is effected by removing the heat by cooling apparatus walls or by evaporating said solution under reduced pressure.
- 20 9. A process as claimed in any of claims 1 to 8, wherein said crystals of step (c) are removed from said mother liquor by filtration and/or centrifugation.
10. A process as claimed in any of claims 1 to 9, wherein said crystals removed in step (c) are subjected to at least one washing and/or sweating step.
- 25 11. A process as claimed in any of claims 1 to 10, wherein said recycling of step (d) is effected by recycling from 0 to 100% by weight, preferably 100% by weight, of said mother liquor from step (c) into step (a).

Abstract

5 A process for preparing acrylic acid or methacrylic acid comprises preparing a gaseous product mixture having essentially the composition of a reaction mixture of the catalytic gas phase oxidation of C₃-/C₄-alkanes, -alkenes, -alkanols and/or -alkanals and/or precursors thereof to form acrylic acid or methacrylic acid. The product is removed from the gaseous product mixture by a process comprising the following steps:

10

- (a) condensing said gaseous product mixture,
- (b) crystallizing acrylic acid or methacrylic acid from the solution obtained in step (a),
- (c) removing the resulting crystals from the mother liquor, and
- 15 (d) recycling at least a portion of said mother liquor from step (c) into step (a).

