What is claimed is:

1. A method of generating at least one of H_2 and Fischer Tropsch liquids, the method comprising:

receiving feedstock into an initial reformer;

reforming, in the initial reformer, at least a portion of the feedstock with steam to produce an input gas, wherein an amount of the input gas is syngas;

transferring the input gas from the initial reformer to a main reformer;

reforming, in the main reformer, the input gas with steam to increase the amount of syngas, wherein the syngas includes CO, H_2 and H_2O;

transferring the syngas from the main reformer to a Fischer Tropsch module;

using the syngas in a Fischer Tropsch reaction; and

extracting from the Fischer Tropsch module H_2O, CO, H_2, and CO_2 generated by the Fisher Tropsch reaction and ~~at least one of~~ Fischer Tropsch liquids generated by the Fischer Tropsch reaction; and ~~H2 generated by the Fischer Tropsch reactions.~~

~~2.~~ ~~The method of claim 1, further comprising~~ transferring CO, H_2 and CO_2 generated by the Fischer Tropsch reaction directly to the main reformer.

~~3~~2. The method of claim ~~2~~1, further comprising transferring hydrocarbons containing at least five carbon atoms generated by the Fischer Tropsch reaction to the main reformer.

~~4~~3. The method of claim 1, wherein transferring the syngas from the main reformer into the Fischer Tropsch module further comprises condensing H_2O from the syngas prior to the syngas entering the Fischer Tropsch module.

~~5~~4. The method of claim 1, wherein the syngas, when transferred into the Fischer Tropsch module, has a H_2/CO ratio between 1.5 to 3.5.

~~6~~5. The method of claim ~~4~~3, wherein the H_2/CO ratio is about 2.16.

~~7~~6. The method of claim ~~4~~3, wherein the H_2/CO ratio is about 2.3

~~8~~7. The method of claim 1, wherein the syngas is transferred into the Fischer Tropsch module at a pressure not more than 125 psig.

~~9~~8. The method of claim 1, wherein the initial reformer is a rotary reformer.

~~10~~9. The method of claim ~~9~~8, wherein the rotary reformer has a rotary reformer operating temperature, and wherein the main reformer has a main reformer operating temperature greater than the rotary reformer operating temperature.

~~11~~10. The method of claim ~~9~~8, further comprising extracting sulfur from the input gas by contacting the input gas with lime in the rotary reformer.

~~12~~11. The method of claim ~~11~~10, further comprising removing lime, using the rotary reformer.

~~13~~12. The method of claim 1, wherein the feedstock comprises at least one of municipal solid waste, medical waste, digestate, and natural gas.

~~14~~13. The method of claim ~~13~~12, wherein the feedstock further comprises biogas and is substantially oxygen-free.

~~15~~14. The method of claim ~~13~~12, wherein the digestate has a moisture content of 24% to 70% by weight.

~~16~~15. The method of claim 1, wherein the initial reformer is a cyclonic separator, and wherein the feedstock further comprises natural gas.

~~17~~16. The method of claim ~~16~~15, wherein the cyclonic separator has a cyclonic separator operating temperature, and wherein the main reformer has a main reformer operating temperature greater than the cyclonic separator operating temperature.

~~18~~17. The method of claim 1, wherein the main reformer has a main reformer operating temperature equal to or less than 1600°F.

~~19~~18. The method of claim 1, wherein combustion fails to occur in the initial reformer and in the main reformer.

~~20~~19. The method of claim 1, wherein pressure in the initial reformer and the main reformer is maintained at about one atmosphere.