**CLAIMS:**

1. A method for making lubricant base stock, comprising:

a) performing solvent deasphalting using a $C_{4+}$ solvent under effective solvent deasphalting conditions on a feedstock having a T5 boiling point of at least 370°C, the effective solvent deasphalting conditions producing a yield of deasphalted oil of at least 50 wt% of the feedstock;

b) hydroprocessing at least a portion of the deasphalted oil under first effective hydroprocessing conditions comprising first hydrocracking conditions to form a hydroprocessed effluent, the at least a portion of the deasphalted oil having an aromatics content of at least 50 wt%;

c) separating the hydroprocessed effluent to form at least a fuels boiling range fraction, a first fraction having a $T_5$ distillation point of at least 370°C, and a second fraction having a $T_5$ distillation point of at least 370°C, the second fraction having a higher kinematic viscosity at 100°C than the first fraction;

d) hydroprocessing at least a portion of the first fraction under second effective hydroprocessing conditions, the second effective hydroprocessing conditions comprising exposing the first fraction to a medium pore dewaxing catalyst to form a first catalytically dewaxed effluent comprising a 370°C+ portion having a first kinematic viscosity at 100°C; and

e) hydroprocessing at least a portion of the second fraction under third effective hydroprocessing conditions, the third effective hydroprocessing conditions comprising exposing the second fraction to the medium pore dewaxing catalyst to form a second catalytically dewaxed effluent comprising a 370°C+ portion having a second kinematic viscosity at 100°C that is greater than the first kinematic viscosity at 100°C,

wherein the first hydroprocessing conditions further comprise first aromatic saturation conditions, the first aromatic saturation conditions comprising exposing the at least a portion of the deasphalted oil to a demetallization catalyst, the at least a portion of the deasphalted oil being exposed to the demetallization catalyst after exposing the at least a portion of the deasphalted oil to a hydrocracking catalyst;

wherein the second effective hydroprocessing conditions are different from the third effective hydroprocessing conditions; and

wherein the 370°C+ portion of the second catalytically dewaxed effluent is a Group II base stock comprising 40 wt% or more naphthenes, at least 90 wt% saturates and less than 0.03 wt% sulfur, and having a viscosity index of at least 80 and less than 120, a kinematic viscosity at 100°C of 30 cSt or more, a pour point of -9°C or less, and a cloud point that is lower than the pour point.

2. The method of claim 1, wherein the medium pore dewaxing catalyst comprises ZSM-5; wherein the medium pore dewaxing catalyst comprises 0.05 wt% or less of Group VIII metals; wherein the at least a portion of the deasphalted oil comprises a sulfur content of 300 wppm or more, or a combination thereof.

3. The method of claim 1, wherein:

during step b), the hydroprocessed effluent comprises a sulfur content of 300 wppm or less, a nitrogen content of 100 wppm or less, or a combination thereof;

during step d), the at least a portion of the first fraction is exposed to second aromatic saturation conditions prior to second catalytic dewaxing conditions, and the second aromatic saturation conditions optionally comprises exposing the at least a portion of the first fraction to an amorphous aromatic saturation catalyst; and

during step e), the at least a portion of the second fraction is exposed to third aromatic saturation conditions prior to the third catalyst dewaxing conditions.

4. The method of any of claims 1 to 3, wherein the second effective hydroprocessing conditions and third effective hydroprocessing conditions are different based on a difference in at least one of a hydrocracking pressure, a hydrocracking temperature, a dewaxing pressure, and a dewaxing temperature.

5. The method of any of claims 1 to 4, wherein at least a portion of the first fraction, at least a portion of the second fraction, at least a portion of the first catalytically dewaxed effluent, at least a portion of the second catalytically dewaxed effluent, or a combination thereof is used as a feed for a steam cracker; or wherein at least a portion of the second catalytically dewaxed effluent is used as an asphalt blend component; or a combination thereof.

6. The method of any of claims 1 to 5, wherein separating the hydroprocessed effluent further comprises forming an additional fraction having a $T_5$ distillation point of at least 370°C, the method further comprising:

hydroprocessing at least a portion of the additional fraction under fourth effective hydroprocessing conditions, the fourth effective hydroprocessing conditions comprising catalytic dewaxing conditions, to form a third catalytically dewaxed effluent comprising a 370°C+ portion having a kinematic viscosity at 100°C of 3.5 cSt or more.

7. The method of any of claims 1 to 6, wherein the hydroprocessing at least a portion of the first fraction and the hydroprocessing at least a portion of the second fraction comprise block operation of a processing system.

8. The method of any of claims 1 to 7, further comprising recycling at least a portion of the second catalytically dewaxed effluent as part of the at least a portion of the deasphalted oil, as part of the at least a portion of the first fraction, or a combination thereof.