## Description

This invention relates to processes for the production of polymer sheet materials from oriented polymer fibres and to the products of such processes.

One method which is widely used to produce high modulus polymer sheets is the formation of fibre reinforced composites using, e.g. oriented polyethylene fibres in order to reinforce the polymer matrix. The manufacture of such composites is a complex operation and in particular requires careful mixing of the polymer and the fibres if the composite is to exhibit homogeneous mechanical properties.

There have been proposals to produce polymeric sheets by compression of networks of polymer fibres at elevated temperatures most notably in relation to thermotropic liquid crystal polymers. European Patent 354285 and United States Patents 4384016 both describe processes in which fibres of a liquid crystal polymer are hot pressed to produce an oriented polymer sheet. European Patent Application 116845, describes a process in which a network of fibres of ultra-high molecular weight polyethylene are hot compressed to form polymer sheets. In the processes taught in this document the fibres are compressed and heated simultaneously. The products retain a significant proportion of the properties of the fibres in the direction in which the fibres are aligned but the mechanical properties of the products in the direction transverse to that in which the fibres are aligned is less than ideal. These processes are relatively unaffected by the choice of compaction temperature. The polymer fibres do not melt during the process. In addition, EP-A-0201029 discloses a process for the production of films and mouldings in which thermotropic polymer fibres or filaments are arranged to give a sheet-like structure and this is heated to obtain an anisotropic melt and compacted at elevated temperature under pressure from the anisotropic melt.

We have now discovered a novel process whereby an assembly of fibres of oriented polymer may be hot compressed to form a sheet having superior mechanical properties particularly in the direction transverse to that in which the fibres are aligned. The novel processes are distinguished from those of EPA 116845 by an initial processing step in which the fibres are brought to and held at the compaction temperature whilst subject to a pressure sufficient to maintain the fibres in contact, the contact pressure, and thereafter compacted at a higher pressure, the compaction pressure. In the processes of this invention the compaction temperature does influence the mechanical properties of the compacted product. In the processes of this invention a proportion of the polymer material in the fibres melts and subsequently recrystallises and it is this melt phase which serves to bind the fibres together.

Accordingly from one aspect this invention provides a process for the production of a polymer sheet in which an assembly of oriented polymer fibres is maintained in intimate contact at an elevated temperature sufficient to melt a proportion of the polymer and subsequently compressed so as to produce a coherent polymer sheet.

In the preferred processes of this invention the conditions and more particularly the temperature at which the fibres are compacted will be such as to cause a portion of the polymer to be selectively melted. On cooling the molten materials recrystalise to give a phase with a lower melting pint than the original fibre. The presence of a second phase in the compacted product may readily be detected e.g. by D.S.C. measurements. In general the amount of material melted is preferably at least 5% and usually at least 10% of the original. The applicants believe that this minimum amount is required in order fill the spaces between fibres upon compaction and hence produce a product which does not contain trapped air. Processes in which a greater proportion of the polymer material is melted at the contact stage are useful in so far as the mechanical properties of the product in the direction transverse to the alignment of the fibres may be improved but this improvement is achieved at the expense of the properties in the direction of the alignment of the fibres. We have discovered that the improvements in the transverse direction are not directly proportional to the losses in the direction of alignment and that the loss is greater than the improvement. For most applications of the products of this invention the preferred processes are those which are carried out in a manner which selectively melts from 5 to 10% by weight of the polymer material although processes which melt from 10 to 20% by weight of the polymer or even up to 50% by weight may be useful.

In a preferred embodiment the temperature at which the fibres are conpacted is not greater than the peak temperature of melting i.e. the temperature of which the endotherm measured by Differential Scanning Calorimetry (DSC) of the polymer fibres reaches its highest point. The minimum temperature at which the fibres should be contacted is preferably that at which the leading edge of the endotherm extrapolated to zero intersects the temperature axis.

The pressure at which the assembly of fibres is maintained during this stage of the process will be such as to maintain the individual fibres in intimate contact but not such as will compact them and in particular not inhibit the selective melting of the polymer. In general pressures in the range 0.5 to 2.0 MPa are

preferred. The precise value is not normally critical.

The compaction pressure exerted upon the heated assembly of oriented polymer fibres should be sufficient to produce a homogeneous product but should not be so great as to cause the assembly to be extruded. If necessary a closed mould may be used to prevent extrusion and thus allows the use of higher temperatures or pressures if required. In general, pressures in the range of 40 to 50 MPa have been found to be useful. The minimum pressure required to process an assembly of a particular polymer fibre at a particular temperature may be determined by routine experiment.

The time required for the processes of this invention may be determined by empirical means. The time required to bring the assembly of fibres up to the requisite temperature will vary with the nature and size of the assembly, the nature of the polymer and the heating means which are employed. The time is not critical provided it is sufficient to enable the selective melting to be achieved.

The time required for the compaction step is also non-critical except in so far as it must be sufficiently long to enable the assembly to be compacted. At the preferred temperatures the minimum time may be of the order of seconds although longer times may be utilised. Processes which utilise shorter compaction times e.g. 5 to 30 seconds may be advantageous in so far as they may conveniently be operated upon a continuous basis for example a uniaxially aligned assembly of heated fibres may be passed between a pair of rollers.

The products of the processes of this invention preferably retain at least 50% and more preferably at least 75% of the mechanical properties, especially the modulus of the oriented fibres in the direction in which those fibres are aligned. The products exhibit a homogeneous appearance to the eye. Products which when stressed in the direction transverse to that in which the fibres are aligned fibrillate, i.e. break whilst leaving the polymer fibres essentially intact are not homogeneous. The products of this invention exhibit homogeneous behaviour when stressed in this transverse direction. Preferably they will be such that the attenuation of an ultrasonic C scan shows not more than a 20% variation and preferably not more than a 10% variation over the whole sample.

The assembly of oriented polymeric fibres which may be utilised in the processes of this invention may take a variety of forms. In particular they may be arranged as an uniaxially aligned bundle or a twisted bundle of fibres or an assembly of chopped fibres or as a mat of interwoven bundles or a mat formed by layering of bundles of fibres wherein the bundles in each layer are aligned at an angle, e.g. conveniently perpendicular to one another. The products obtained by processing such mats may thus retain the majority of the properties of the oriented fibres in more than one direction. The bundles may be assembled and pressed into any convenient shape. The products may be flat sheets, rods, bars, any of which may be shaped so as to be suitable for particular applications.

The oriented polymer fibres may be obtained by any of the known manufacturing processes. In particular, fibres which have been produced by melt spinning and drawing and gel spinning and drawing. Typically such fibres will have a diameter in the range 0.005 to 0.05 mm.

The processes of this invention may be carried out using conventional equipment. Conveniently, the fibre assembly may be placed in a suitable mould and placed under contact pressure. The assembly may then be preheated to the desired temperature at such a rate as to ensure that there is no significant temperature gradient across the assembly. The desired compaction pressure is then applied and maintained for sufficiently long for the fibres to cohere. The hot compacted materials are preferably cooled to ambient temperature under controlled conditions. Rapid cooling is less preferred. The most convenient techniques is to allow the compacts to stand in the air until they have cooled to ambient temperature.

The processes of the present invention may utilise any polymer fibres which can be selectively melted. The susceptibility of particular polymers and particular grades of that polymer to selective melting varies and their suitability for use in the processes of this invention may be determined empirically.

The processes of the present invention find particular application in the production of oriented polyolefin articles especially oriented polyethylene articles. The polyethylene (which may be a homo or copolymer of polyethylene) may have a weight average molecular weight Mw of from 50,000 to 3,000,000. For polyethylene articles the temperature to which the assembly is preheated is preferably within 5°C and more preferably within 2°C of the peak temperature of melting. Oriented polyethylene products of the processes of this invention preferably have a transverse (i.e. in the direction perpendicular to that in which the fibres are aligned) strength of at least 15 MPa and more preferably at least 25 MPa.

Gel spun polyethylenes having a weight average molecular weight of at least 500,000 may exhibit extremely high axial tensile modulus. This corresponds to an extremely high degree of alignment of the polymer molecules within the fibres. These highly oriented gel spun materials may be processed according to this invention and may be preferred where it is desired to produce a product which exhibits high strength in the direction of the fibre alignment. However the strength in the direction transverse to this alignment

may be limited unless relatively high proportion of the axial strength is sacrificed by allowing the polymer to melt. Polymer fibres which are not so highly oriented may be preferable in so far as the selective melting which characterises the processes of this invention may affect the axial properties to a lesser degree whilst producing useful strengths in the transverse direction.

Homo-and copolymers of polyethylene having a weight average molecular weight of from 50,000 to 500,000 particularly those which can be produced by melt-spinning from a preferred raw material for use in the processes of this invention. Such polymers appear to be more amenable to the selective melting process either by virtue of their comprising some polymer having a relatively low molecular weight or by virtue of their having a surface layer which melts at a lower temperature. Whatever the mechanism which is involved those polymers are preferred because they can form compacts which retain a large proportion of the properties of the fibre (in the direction of alignment of that fibre) whilst producing products having superior properties in the direction transverse to that alignment.

Other classes of polymer fibres which may be useful in the processes of this invention include any of the known orientable polymers. In particular the oriented polymer may be an unsubstituted or mono or poly halo substitued vinyl polymer, an unsubstituted or hydroxy substituted polyester, a polyamide, a polyether-ketone or a polyacetal. Suitable examples include vinyl chloride polymers, vinyl fluoride or vinylidene fluoride polymers PHB, PEEK and homo and copolymers of polyoxymethylene. Particular examples of polyesters useful in the processes of this invention include those derivable by the reaction of at least one polyhydric alcohol, e.g. a linear polyhydric alcohol preferably a diol with at least one poly basic acid, suitably a polycarboxylic acid. The alcohol is preferably an alicyclic or aliphatic alcohol such as cyclohex-ane-dimethanol or a linear alkylene diol such as ethylene glycol, 1,3 propylene glycol or 1,4 butylene glycol. The preferred acids include o, m or ter phthalic acids, 2,6 and 1,5 napthalene dicarboxylic acid and 1,2 dihydroxy benzoic acid.

The compacted products of the present invention normally have a density less than that of the original fibre. This reduction is caused primarily by the retention of air within the compacted material but also by any reduction in the content of crystalline material within the polymer caused by any molten polymer cooling to form an amorphous phase. Both these factors detract from the properties of the product and the preferred processes of this invention produce products in which the density is at least 90% more preferably at least 95% and most preferably substantially the same as that of the polymer fibre. This reflects the fact that the compaction should preferably be carried out in a manner which expels any trapped air from the product and that in the more preferred embodiment the compact will be cooled in a manner which results in the molten material forming a crystalline phase on cooling.

The processes of this invention enable complicated and precisely shaped polymeric articles having high stiffness and high strength to be manufactured. The products may also exhibit good energy absorbing properties. The products find use in a wide variety of applications, particular examples being as orthodontic brackets, as bone implants and as high impact energy absorbing materials, e.g. in body armour.

The invention is illustrated by the following examples:

The tests used in these examples are defined as follows:

The fibre modulus and strength were measured on a 20cm long sample at a displacement rate of 20 cm/min.

The flexure modulus of the samples produced from the process were measured under the guidelines of ASTM D790.

The flexure strengths of the samples produced from the process were measured under the guidelines of ASTM D790.

The short beam shear strength of the samples measured under the guidelines of ASTM D2344.

The densities of the compacted materials were measured using a density bottle.

Ultrasonic elastic properties were measured using an immersion method at a frequency of 2.25 MHz. A full description of the technique can be found in S.R.A. Dyer, D. Lord, I.J. Hutchinson, I.M. Ward and R.A. Duckett, J. Phys. D:Apply. Phys. 25 (1992) 66.

The fibres used were polyethylene fibres having the following particulars:

| Sample | Fibre | Molecular Weight | | Process | Breaking Strength GPa | Tensile initial secant GPa | modulus 2% GPa |
|---|---|---|---|---|---|---|---|
| | | Mw | Mn | | | | |
| 1 | CELANESE | 61,000 | 28,000 | melt spun | 1.0 | 54 | 36 |
| 2 | SNIA FIBRE | 130,000 | 12,000 | melt spun | 1.3 | 58 | 43 |
| 3 | TEKMILON | 700,000 | 54,000 | solvent spun | 2.1 | 80 | 70 |
| 4 | SPECTRA 1000 | 1,500,000 | 75,000 | gel spun | 2.9 | 130 | 115 |

Example 1

A sheet of dimensions 3mm x 5cm x 10cm was prepared by hot pressing a unidirectionally aligned bundle of melt spun SNIA high modulus polyethylene fibres having a diameter of 0.015mm in an open ended matched metal mould. The fibres were preheated for 10 minutes under contact pressure of 0.5MPa at 139 ± 0. 5°C and then a pressure 400MPa was applied for 10 seconds. The resulting product was a homogeneous translucent sheet with the following properties.

| | | |
|---|---|---|
| Tensile modulus in fibre direction<br>Transverse to fibre direction | 57 GPa<br>4.2 GPa | measured ultrasonically |
| Flexure modulus in fibre direction<br>Transverse to fibre direction | 35 GPa<br>3.2 GPa | ASTM D790 |
| Short beam shear strength | 29 GPa | ASTM D2344 |
| Flexure strength in fibre direction<br>Transverse to fibre direction | 110 MPa<br>31 MPa | ASTM D790 |

An ultrasonic immersion 'C' scan of the product showed only a 2% change in attenuation over the sample and is taken as a measure of the homogeneity of the product.

A DSC trace of the compacted material showed that 8% of the original fibre phase had been melted and had recrystallised forming a second lower melting point phase.

The density of the compacted material was 90% of the original fibre density.

Example 2

A bar of 3mm square cross section was prepared by hot pressing a twisted bundle of melt spun SNIA high modulus polyethylene fibres having a diameter of 0.015mm in an open ended matched metal mould. The fibres were preheated at 139 ± 0. 5°C for 10 minutes and then pressed for 30 seconds at a pressure of 50 MPa. The resulting product was a homogeneous translucent bar with a flexural modulus (ASTM D790) of 32 GPa.

Example 3

An orthotropic material was made by compacting a number of layers of a woven mat of melt spun SNIA high modulus polyethylene fibres in an open ended matched metal mould. The laminated mat was maintained at 139 ± 0.5°C for 10 minutes at 0.5 MPa before applying a high pressure of 50 MPa for 30 seconds. The flexure modulus was the same in both the axes in the plane of the plate, with a value of 11 GPa. The flexure strength was also similar in the two axes in the plane of the plate with a value of 85 MPa. We can conclude that using a woven mat for compaction results in a substantial improvement in transverse strength at the expense of stiffness.

Example 4

A three dimensional shape was formed by compacting a number of layers of a woven mat of melt spun SNIA high modulus polyethylene fibre between male and female hemispherical moulds. The compaction conditions were identical to those shown in example 3. The compacted material was formed into the

required shape in a single process.

Example 5

A laminated sheet 3mm thick and 55mm square was made by sandwiching a uniaxially aligned bundle of melt spun SNIA polyethylene fibres between two layers of a woven mat of melt spun SNIA polyethylene fibres. The sandwich was then compacted using conditions given in example 3. The result was a translucent sheet with the following properties.

| | | |
|---|---|---|
| Tensile modulus in fibre direction<br>Transverse to main fibre direction | 52 GPa<br>4.9 GPA | measured ultrasonically |
| Flexure modulus in main fibre direction<br>Flexure strength transverse to main fibre direction | 18 GPa<br>75 GPa | ASTM D790<br>ASTM D790 |

Lamination allows a better compromise to be achieve between stiffness and strength, especially in tension.

Example 6

2.0 grams of chopped melt spun SNIA high modulus polyethylene fibre was placed in a cylindrical mould which was 12mm in diameter and 30mm long. Compaction of the fibre assembly proceeded according to the conditions described in example 3. The resulting cylindrical bar was an isotropic material having a modulus of 5 GPa. A DSC trace of the product showed that 12% of the original fibre had been melted.

Example 7

A bar of 25mm square cross section and 100mm long was prepared by hot pressing a number of cold compacted layers of melt spun SNIA high modulus polyethylene fibres in a closed matched metal mould using conditions described in example 3. DSC traces taken through the compacted blocks showed that a reasonably even heat distribution had been achieved.

Example 8

3.0 grams of melt spun CELANESE high modulus polyethylene fibre with a diameter of 0.015mm was compacted in an open ended rectangular section steel mould at a compaction temperature of 134 ± 0.5°C. A contact pressure of 0.5 MPa was held for 10 minutes and then a pressure of 40 MPa was applied for 30 seconds. The sample had the appearance of a solid polyethylene rod with a well defined cross section measuring 3.34mm x 3.11mm. The bending modulus was 19.7 GPa.

Example 9

To demonstrate the criticality of the moulding temperature, a sample identical to that used in example 8 was compressed in the same mould at the higher temperature of 138°C. The resulting sample again had the appearance of a solid polyethylene rod but the low bending modulus of 1.2 GPa showed that the properties of the fibre had been lost due to substantial melting of the original fibre phase. Further evidence of the critical nature of the temperature was shown by compressing an identical sample to examples 8 and 9 but at the lower temperature of 127°C. The resulting product had a high stiffness but poor transverse properties due to almost total retention of the original fibre phase.

Example 10

The role of pressure was examined by carrying out an identical experiment to example 1 except that high pressure (40 MPa) was applied from the very start of the procedure, including the warm up period. The resulting product had a high longitudinal stiffness of 60 GPa but a poor transverse strength of 12 MPa. A DSC trace of the compacted material showed no evidence of any 'second phase': the compacted material was composed entirely of the original fibre phase.

We can therefore conclude that applying high pressure from the beginning of the compaction process inhibits the selective melting which is necessary for optimum control of the properties of the final product.

Example 11

A sheet of dimensions 3mm x 55mm x 55mm was prepared by compacting a unidirectionally aligned bundle of gel spun SPECTRA high modulus polyethylene fibres in a matched metal mould. The processing conditions were identical to example 3 apart from raising the compaction temperature to 152 ± 0.5°C, which is midway between the onset of melting and the end of melting.

The resulting compacted sheet was homogeneous and had a longitudinal modulus of 35 GPa and a transverse strength of 17 MPa. A DSC trace of the compacted material showed around 35% of a 'second phase' formed by melting of the original fibre.

**Claims**

1. A process for the production of a homogeneous polymeric monolith characterised in that an assembly of oriented polymer fibres is maintained in intimate contact at an elevated temperature sufficient to melt a proportion of the polymer and subsequently compressed.

2. A process according to Claim 1 characterised in that the assembly is maintained at a temperature at least that at which an extrapolation of the leading edge of the endotherm of the oriented fibres measured by differential scanning calorimetry intersects the temperature axis.

3. A process according to either of Claims 1 to 2 characterised in that the temperature at which the assembly is maintained is less than the peak temperature of melting of the polymer fibres as measured by differential scanning calorimetry.

4. A process according to any of Claims 1 to 3 characterised in that the assembly is maintained at a temperature such that at least 5% by weight of the polymer is melted.

5. A process according to any of the preceding claims characterised in that the assembly is maintained at a temperature such that no more than 20% by weight of the polymer is melted.

6. A process according to either of Claims 4 or 5 characterised in that the assembly is maintained at a temperature such that from 5 to 10% by weight of the polymer is melted.

7. A process according to any of the preceding claims characterised in that the assembly is maintained under contact pressure.

8. A process according to any of the preceding claims characterised in that the heated assembly is compressed under a compaction pressure of from 0.5 to 2.0 MPa.

9. A process according to Claim 8 characterised in that the compaction pressure is maintained for a period of at least 5 seconds.

10. A process according to any of the preceding claims characterised in that the hot compressed material is allowed to cool to ambient temperature by standing in air.

11. A process according to any of the preceding claims characterised in that the polymer fibres are homo or copolymers of a polyolefin.

12. A process according to Claim 11 characterised in that the polymer fibres are polyethylene fibres.

13. A process according to either of Claim 11 or 12 characterised in that the polymer has a weight average molecular weight of from 50,000 to 3,000,000.

14. A process according to any Claims 11 to 13 characterised in that the polymer has a weight average molecular weight of from 500,000 to 3,000,000.

We can therefore conclude that applying high pressure from the beginning of the compaction process inhibits the selective melting which is necessary for optimum control of the properties of the final product.

Example 11

A sheet of dimensions 3mm x 55mm x 55mm was prepared by compacting a unidirectionally aligned bundle of gel spun SPECTRA high modulus polyethylene fibres in a matched metal mould. The processing conditions were identical to example 3 apart from raising the compaction temperature to 152 ± 0.5°C, which is midway between the onset of melting and the end of melting.

The resulting compacted sheet was homogeneous and had a longitudinal modulus of 35 GPa and a transverse strength of 17 MPa. A DSC trace of the compacted material showed around 35% of a 'second phase' formed by melting of the original fibre.

**Claims**

1. A process for the production of a homogeneous polymeric monolith characterised in that an assembly of oriented polymer fibres is maintained in intimate contact at an elevated temperature sufficient to melt a proportion of the polymer and subsequently compressed.

2. A process according to Claim 1 characterised in that the assembly is maintained at a temperature at least that at which an extrapolation of the leading edge of the endotherm of the oriented fibres measured by differential scanning calorimetry intersects the temperature axis.

3. A process according to either of Claims 1 to 2 characterised in that the temperature at which the assembly is maintained is less than the peak temperature of melting of the polymer fibres as measured by differential scanning calorimetry.

4. A process according to any of Claims 1 to 3 characterised in that the assembly is maintained at a temperature such that at least 5% by weight of the polymer is melted.

5. A process according to any of the preceding claims characterised in that the assembly is maintained at a temperature such that no more than 20% by weight of the polymer is melted.

6. A process according to either of Claims 4 or 5 characterised in that the assembly is maintained at a temperature such that from 5 to 10% by weight of the polymer is melted.

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9. A process according to Claim 8 characterised in that the compaction pressure is maintained for a period of at least 5 seconds.

10. A process according to any of the preceding claims characterised in that the hot compressed material is allowed to cool to ambient temperature by standing in air.

11. A process according to any of the preceding claims characterised in that the polymer fibres are homo or copolymers of a polyolefin.

12. A process according to Claim 11 characterised in that the polymer fibres are polyethylene fibres.

13. A process according to either of Claim 11 or 12 characterised in that the polymer has a weight average molecular weight of from 50,000 to 3,000,000.

14. A process according to any Claims 11 to 13 characterised in that the polymer has a weight average molecular weight of from 500,000 to 3,000,000.



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15. A process according to any of Claims 11 to 13 characterised in that the polymer has a weight average molecular weight of from 50,000 to 300,000.

16. A process according to any of Claims 11 to 15 characterised in that the fibre is a melt spun fibre.

17. A process according to any of Claims 11 to 16 characterised in that the assembly is maintained at a temperature which is no more than 5 °C below the peak temperature of melting of the polymer fibre.

18. A process according to any of Claims 11 to 17 characterised in that the assembly is maintained at a temperature which is no more than 2 °C below the peak temperature of melting of the polymer.

19. A process according to any of the preceding claims characterised in that the compressed product has a density which is at least 90% of the original fibre density.

**Patentansprüche**

1. Verfahren zur Herstellung eines homogenen polymeren Monolithen, **dadurch gekennzeichnet**, daß ein Gefüge orientierter Polymerfasern in engem Kontakt gehalten wird bei einer erhöhten Temperatur, welche ausreicht. um einen Teil des Polymeren zu schmelzen, und anschließend komprimiert wird.

2. Verfahren gemäß Anspruch 1, **dadurch gekennzeichnet**, daß das Gefüge mindestens auf einer Temperatur gehalten wird, bei welcher die Extrapolation von der Anstiegsflanke der Endothermen der orientierten Fasern, gemessen mit einem Differentialscanningkalorimeter, die Temperaturachse schneidet.

3. Verfahren nach mindestens einem der Ansprüche 1 bis 2, **dadurch gekennzeichnet**, daß die Temperatur, auf der das Gefüge gehalten wird, niedriger als die Temperaturspitze für das Schmelzen der Polymerfasern ist, die mit einem Differentialscanningkalorimeter gemessen wurde.

4. Verfahren nach mindestens einem der Ansprüche 1 bis 3, **dadurch gekennzeichnet**, daß das Gefüge auf einer solchen Temperatur gehalten wird, daß mindestens 5 Gew.-% des Polymeren geschmolzen werden.

5. Verfahren nach mindestens einem der vorhergehenden Ansprüche, **dadurch gekennzeichnet**, daß das Gefüge auf einer solchen Temperatur gehalten wird, daß nicht mehr als 20 Gew.-% des Polymeren geschmolzen werden.

6. Verfahren nach mindestens einem der Ansprüche 4 oder 5, **dadurch gekennzeichnet**, daß das Gefüge auf einer solchen Temperatur gehalten wird, daß 5 bis 10 Gew.-% des Polymeren geschmolzen werden.

7. Verfahren nach mindestens einem der vorhergehenden Ansprüche, **dadurch gekennzeichnet**, daß das Gefüge unter Kontaktdruck gehalten wird.

8. Verfahren gemäß mindestens einem der vorhergehenden Ansprüche, **dadurch gekennzeichnet**, daß das erwärmte Gefüge unter einem Verdichtungsdruck von 0,5 bis 2,0 MPa komprimiert wird.

9. Verfahren nach Anspruch 8, **dadurch gekennzeichnet**, daß der Verdichtungsdruck mindestens 5 Sekunden lang aufrechterhalten wird.

10. Verfahren nach mindestens einem der vorhergehenden Verfahren, **dadurch gekennzeichnet**, daß man das wärmekomprimierte Material durch Stehenlassen in der Luft auf Umgebungstemperatur abkühlen läßt.

11. Verfahren nach mindestens einem der vorhergehenden Ansprüche, **dadurch gekennzeichnet**, daß die Polymerfasern Homo- oder Copolymerfasern eines Polyolefins sind.



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12. Verfahren nach Anspruch 11, **dadurch gekennzeichnet**, daß die Polymerfasern Polyethylenfasern sind.

13. Verfahren nach mindestens einem der Ansprüche 11 oder 12, **dadurch gekennzeichnet**, daß das Polymer ein gewichtsmittleres Molekulargewicht von 50 000 bis 3 000 000 hat.

14. Verfahren nach mindestens einem der Ansprüche 11 bis 13, **dadurch gekennzeichnet**, daß das Polymer ein gewichtsmittleres Molekulargewicht von 500 000 bis 3 000 000 hat.

15. Verfahren nach mindestens einem der Ansprüche 11 bis 13, **dadurch gekennzeichnet**, daß das Polymer ein gewichtsmittleres Molekulargewicht von 50 000 bis 300 000 hat.

16. Verfahren nach mindestens einem der Ansprüche 11 bis 15, **dadurch gekennzeichnet**, daß die Faser eine schmelzgesponnene Faser ist.

17. Verfahren nach mindestens einem der Ansprüche 11 bis 16, **dadurch gekennzeichnet**, daß das Gefüge auf einer Temperatur gehalten wird, welche nicht mehr als 5 °C unterhalb der Temperaturspitze für das Schmelzen der Polymerfaser liegt.

18. Verfahren nach mindestens einem der Ansprüche 11 bis 17, **dadurch gekennzeichnet**, daß das Gefüge auf einer Temperatur gehalten wird, welche nicht mehr als 2 °C unterhalb der Temperaturspitze für das Schmelzen des Polymeren liegt.

19. Verfahren nach mindestens einem der vorhergehenden Ansprüche, **dadurch gekennzeichnet**, daß das verdichtete Produkt eine Dichte hat. welche mindestens 90 % der ursprünglichen Faserdichte beträgt.

**Revendications**

1. Procédé de production d'un monolithe polymère homogène, caractérisé en ce qu'un ensemble de fibres polymères orientées est maintenu en contact intime à une température élevée, suffisante pour taire fondre une partie du polymère, et ensuite, est compressé.

2. Procédé selon la revendication 1, caractérisé en ce que l'ensemble est maintenu à une température au moins égale à celle pour laquelle une extrapolation de la partie croissante de l'endotherme des fibres orientées, mesurée par analyse calorimétrique différentielle, coupe l'axe des températures.

3. Procédé selon l'une quelconque des revendications 1 à 2, caractérisé en ce que la température à laquelle l'ensemble est maintenu est inférieure à la température de pic de fusion des fibres polymères, tel que mesuré par analyse calorimétrique différentielle.

4. Procédé selon l'une quelconque des revendications 1 à 3, caractérisé en ce que l'ensemble est maintenu à une température telle qu'au moins 5 % en poids du polymère soit fondu.

5. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que l'ensemble est maintenu à une température telle que la proportion de polymère fondu ne dépasse pas 20 % en poids.

6. Procédé selon l'une quelconque des revendications 4 ou 5, caractérisé en ce que l'ensemble est maintenu à une température telle qu'une proportion de 5 à 10 % en poids du polymère soit fondue.

7. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que l'ensemble est maintenu sous pression de contact.

8. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que l'ensemble chauffé est compressé sous une pression de compactage de 0,5 à 2,0 MPa.

9. Procédé selon la revendication 8, caractérisé en ce que la pression de compactage est maintenue pendant une période d'au moins 5 secondes.



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10. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce qu'on laisse refroidir à la température ambiante le matériau chaud compressé en le laissant à l'air.

11. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que les fibres polymères sont des homo- ou copolymères d'une polyoléfine.

12. Procédé selon la revendication 11, caractérisé en ce que les fibres polymères sont des fibres de polyéthylène.

13. Procédé selon l'une quelconque des revendications 11 et 12, caractérisé en ce que le polymère présente une masse moléculaire moyenne en poids de 50 000 à 3 000 000.

14. Procédé selon l'une quelconque des revendications 11 à 13, caractérisé en ce que le polymère présente une masse moléculaire moyenne en poids de 500 000 à 3 000 000.

15. Procédé selon l'une quelconque des revendications 11 à 13, caractérisé en ce que le polymère présente une masse moléculaire moyenne en poids de 50 000 à 300 000.

16. Procédé selon l'une quelconque des revendications 11 à 15, caractérisé en ce que la fibre est une fibre filée en fusion.

17. Procédé selon l'une quelconque des revendications 11 à 16, caractérisé en ce que l'ensemble est maintenu à une température qui n'est pas inférieure de plus de 5 °C à la température de pic de fusion de la fibre polymère.

18. Procédé selon l'une quelconque des revendications 11 à 17, caractérisé en ce que l'ensemble est maintenu à une température qui n'est pas inférieure de plus de 2 °C à la température de pic de fusion du polymère.

19. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que le produit compressé présente une densité qui est au moins égale à 90 % de la densité initiale de la fibre.



* C L M S *