CLAIMS

1. A method for cracking a hydrocarbon feed stream, the method comprising:

contacting the hydrocarbon feed stream with a cracking catalyst in a reactor unit, where the hydrocarbon feed stream has an API gravity of at least 40 degrees, and where the cracking catalyst comprises:

one or more binder materials in an amount of from 5 wt.% to 30 wt.% of the cracking catalyst;

one or more matrix materials in an amount of from 30 wt.% to 60 wt.% of the cracking catalyst;

*BEA framework zeolite in an amount of from 5 wt.% to 30 wt.% of the cracking catalyst;

FAU framework zeolite in an amount of from 5 wt.% to 45 wt.% of the cracking catalyst;

MFI framework zeolite in an amount of from 5 wt.% to 45 wt.% of the cracking catalyst; and

where the *BEA framework zeolite comprises less than 0.5 wt.% of transition metal.

2. The method of claim 1, where the hydrocarbon feed stream has an API gravity of from 45 degrees to 60 degrees.

3. The method of claim 1, where the amount of the FAU framework zeolite is from 10 wt.% to 20 wt.% of the total cracking catalyst.

4. The method of claim 1, where the amount of the MFI framework zeolite is from 10 wt.% to 20 wt.% of the total cracking catalyst.

5. The method of claim 1, where one or more of the MFI framework zeolite, *BEA framework zeolite, and FAU framework zeolite comprise phosphorus pentoxide.

6. The method of claim 1, where at least one of the one or more binder materials is pseudoboehmite.

7. The method of claim 1, where the amount of the one or more binder materials is from 10 wt.% to 20 wt.% of the cracking catalyst.

8. The method of claim 1, where one or more of the matrix materials is kaolin.

9. The method of claim 1, where cracking catalyst comprises the one or more matrix materials in an amount of from 30 wt.% to 50 wt.% of the cracking catalyst.

10. The method of claim 1, where the catalyst to oil weight ratio is from 7 to 10.

11. The method of claim 1, where the MFI framework zeolite comprises ZSM-5.

12. The method of claim 1, where the FAU framework zeolite comprise zeolite Y.

13. The method of claim 1, where the *BEA framework zeolite comprises zeolite Beta.

14. The method of claim 1, where the contacting of the hydrocarbon feed stream with the cracking catalyst produces a product stream comprising at least 20 wt.% of light olefins selected from ethylene, propylene, and butene.

15. The method of claim 1, where the hydrocarbon feed stream is gas condensate.

16. The method of claim 1, where the hydrocarbon feed stream has a 5 wt.% boiling temperature of from 0°C to 100°C, a 25 wt.% boiling temperature of from 75°C to 175°C, a 50 wt.% boiling temperature of from 150°C to 250°C, a 75 wt.% boiling temperature of from 250°C to 350°C, and a 95 wt.% boiling temperature of from 450°C to 550°C.

17. The method of claim 1, where the FAU framework zeolite comprises less than 1 wt.% of transition metal.

18. The method of claim 1, where the MFI framework zeolite comprises less than 1 wt.% of transition metal.

19. The method of claim 1, where the *BEA framework zeolite comprises less than or equal to 0.1 wt.% of transition metal.