

TITLE

HYBRID VAPOR COMPRESSION-ABSORPTION CYCLE

5 This application claims the benefit of U.S. Provisional Application No. 60/682,191, filed May 18, 2005, which is incorporated in its entirety as a part hereof for all purposes.

10 Technical Field

 The present invention relates to a hybrid vapor compression - absorption cooling or heating system utilizing a refrigerant pair comprising at least one refrigerant and at least one absorbent, wherein the absorbent in a preferred embodiment may be at least one ionic liquid.

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Background of the Invention

 As a new type of solvent with immeasurable vapor pressure, room-temperature ionic liquids are being used for chemical separation and unique
20 reaction media. Solvent phase behavior is an important factor in the attractiveness of using ionic liquids in these applications as well as in new applications such as absorption cooling or heating.

 Vapor compression and absorption refrigeration cycles are well-known
25 methods of cooling and are described by Haaf, S. and Henrici, H. in "Refrigeration Technology" (*Ullmann's Encyclopedia of Industrial Chemistry*, Sixth Edition, Wiley-VCH Verlag GmbH, Weinheim, Germany, Volume 31, pages 269-312). The basic cooling cycle is the same for the absorption and vapor compression systems. Both systems use a low-temperature liquid refrigerant that
30 absorbs heat from water, air or any medium to be cooled, and converts to a vapor phase (in the evaporator section). The refrigerant vapors are then compressed to a higher pressure (by a compressor or a generator), converted back into a liquid by rejecting heat to the external surroundings (in the condenser section), and then

expanded to a low-pressure mixture of liquid and vapor (in the expander section) that goes back to the evaporator section and the cycle is repeated. The basic difference between the vapor compression system and absorption system is that a vapor compression system uses an electric motor for operating a compressor used for raising the pressure of refrigerant vapors, and an absorption system uses heat for compressing refrigerant vapors to a high-pressure.

Absorption chillers have been combined with vapor compression chillers in "hybrid" central plants to provide cooling at the lowest energy costs; for example the absorption chiller will be operated during high electric peak load when charges are high, whereas the vapor compression chiller will be operated during low electric peak load when charges are low, resulting in a more economical system. It would be desirable to have one system that integrates components of both the vapor compression and absorption cycles.

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Vapor compression systems generally use ammonia or fluorocarbon derivatives as refrigerants, whereas absorption cycles generally use ammonia/water or lithium bromide/water. The two systems are not compatible in that fluorocarbon derivatives are not very soluble in water. While ammonia could be used for both systems, the toxicity and flammability associated with ammonia makes this option less desirable.

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Although U.S. Patent Application No. 11/346,028, which is incorporated in its entirety as a part hereof for all purposes, discloses an absorption cycle wherein refrigerant pairs comprising at least one refrigerant and at least one ionic liquid are utilized, a need remains for systems to run a hybrid vapor compression – absorption cycle utilizing a refrigerant pair comprising at least one refrigerant and at least one ionic liquid.

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Summary

This invention provides for the execution or performance of a hybrid vapor compression - absorption cycle by operating or running a system or other

equipment or apparatus that are suitable to accomplish heating or cooling in view of the heat rejected and absorbed during the repetition of the cycle.

One embodiment of this invention provides an apparatus for temperature adjustment that includes (a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent; (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor; (c) a condenser that receives the vapor from the generator and condenses the vapor under pressure to a liquid; (d) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant; (e) an evaporator that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form first and second portions of refrigerant vapor; (f) a compressor that receives the first portion of the refrigerant vapor, increases the pressure thereof, and passes the first portion of the refrigerant vapor to the condenser; and (g) a conduit that passes the second portion of the refrigerant vapor leaving the evaporator to the absorber.

Another embodiment of this invention provides an apparatus for temperature adjustment that includes (a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent; (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor; (c) a compressor that receives the vapor from the generator and further increases its pressure; (d) a condenser that receives the vapor from the compressor and condenses the vapor under pressure to a liquid; (e) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant; (f) an evaporator that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form refrigerant vapor; and (g) a conduit that passes the refrigerant vapor leaving the evaporator to the absorber.

In either of these embodiments, the apparatus may be used for heating by locating the condenser in proximity to an object, medium or space to be heated, or the apparatus may be used for cooling by locating the evaporator in proximity to an object, medium or space to be cooled.

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In a further embodiment, this invention provides a process for adjusting the temperature of an object, medium or a space by (a) absorbing refrigerant vapor with an absorbent to form a mixture; (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor; (c) condensing the refrigerant vapor under pressure to a liquid; (d) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form first and second portions of refrigerant vapor; (e-1) mechanically increasing the pressure of the first portion of refrigerant vapor, and then repeating step (c) to subject the first portion of refrigerant vapor to condensation to liquid; and (e-2) repeating step (a) to re-absorb, with the absorbent, the second portion of refrigerant vapor.

In yet another embodiment, this invention provides a process for adjusting the temperature of an object, medium or a space comprising (a) absorbing refrigerant vapor with an absorbent to form a mixture; (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor; (c) further increasing the pressure of the refrigerant vapor mechanically; (d) condensing the refrigerant vapor under pressure to a liquid; (e) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form refrigerant vapor; and (f) repeating step (a) to re-absorb the refrigerant vapor with the absorbent.

In either of these process embodiments, the temperature adjustment performed by the process may be an increase in temperature, and for that purpose refrigerant vapor is condensed to a liquid in proximity to an object, medium or space to be heated; or the temperature adjustment performed by the process may be a decrease in temperature, and for that purpose liquid refrigerant is evaporated in proximity to an object, medium or space to be cooled.

In any of the above embodiments, the refrigerant may be selected from one or more members of the group consisting of a hydrofluorocarbon, a hydrochlorofluorocarbon, a chlorofluorocarbon, a fluorocarbon, N₂, O₂, CO₂, NH₃, Ar, H₂, H₂O, and a non-fluorinated hydrocarbon, wherein the non-fluorinated hydrocarbon is selected from the group consisting of C₁ to C₄ straight-chain, branched or cyclic alkanes and C₁ to C₄ straight-chain, branched or cyclic alkenes; and/or the absorbent may be one or more ionic liquids.

10 Brief Description of the Drawings

FIG. 1 shows a schematic diagram of a system to run a simple vapor compression cycle.

FIG. 2 shows a schematic diagram of a system to run a simple absorption
15 cycle.

FIG. 3 shows a schematic diagram of a system to run a simple hybrid vapor compression - absorption cycle (parallel configuration).

FIG. 4 shows a schematic diagram of a system to run a simple hybrid
20 vapor compression - absorption cycle (series configuration).

FIG. 5 shows measured isothermal solubility data (in mole fraction) for HFC-32 in [bmim][PF₆] as a function of pressure. Filled circles (●) represent
25 measured isothermal data at 10 °C, filled triangles (▲) represent measured isothermal data at 25 °C, filled squares (■) represent measured isothermal data at 50 °C, and filled diamonds (◆) represent measured isothermal data at 75 °C. Solid lines represent data trends.

FIG. 6 shows measured isothermal solubility data (in mole fraction) for HFC-125 in [bmim][PF₆] as a function of pressure. Filled circles (●) represent
30 measured isothermal data at 10 °C, filled triangles (▲) represent measured isothermal data at 25 °C, filled squares (■) represent measured isothermal data at

50 °C, and filled diamonds (◆) represent measured isothermal data at 75 °C. Solid lines represent data trends.

FIG. 7 shows measured isothermal solubility data (in mole fraction) for HFC-134a in [bmim][PF₆] as a function of pressure. Filled circles (●) represent measured isothermal data at 10 °C, filled triangles (▲) represent measured isothermal data at 25 °C, filled squares (■) represent measured isothermal data at 50 °C, and filled diamonds (◆) represent measured isothermal data at 75 °C. Solid lines represent data trends.

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FIG. 8 shows measured isothermal solubility data (in mole fraction) for HFC-143a in [bmim][PF₆] as a function of pressure. Filled circles (●) represent measured isothermal data at 10 °C, filled triangles (▲) represent measured isothermal data at 25 °C, filled squares (■) represent measured isothermal data at 50 °C, and filled diamonds (◆) represent measured isothermal data at 75 °C. Solid lines represent data trends.

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FIG. 9 shows measured isothermal solubility data (in mole fraction) for HFC-152a in [bmim][PF₆] as a function of pressure. Filled circles (●) represent measured isothermal data at 10 °C, filled triangles (▲) represent measured isothermal data at 25 °C, filled squares (■) represent measured isothermal data at 50 °C, and filled diamonds (◆) represent measured isothermal data at 75 °C. Solid lines represent data trends.

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FIG. 10 shows measured isothermal solubility data (in mole fraction) for HFC-32 in [bmim][BF₄] as a function of pressure. Filled circles (●) represent measured isothermal data at 10 °C, filled triangles (▲) represent measured isothermal data at 25 °C, filled squares (■) represent measured isothermal data at 50 °C, and filled diamonds (◆) represent measured isothermal data at 75 °C. Solid lines represent data trends.

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FIG. 11 shows measured isothermal solubility data at 25 °C of the systems HFC-32 + eight different ionic liquids as a function of pressure for comparison. Open diamonds (◇) represent measured isothermal data for HFC-32 + 1-ethyl-3-methylimidazolium bis(pentafluoroethylsulfonyl)imide at 25 °C, pen circles (○)

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represent measured isothermal data for HFC-32 + 1-propyl-2,3-dimethylimidazolium tris(trifluoromethylsulfonyl)methide at 25 °C, open squares ($\square$) represent measured isothermal data for HFC-32 + 1-propyl-2,3-dimethylimidazolium bis(trifluoromethylsulfonyl)imide at 25 °C, closed diamonds ($\blacklozenge$) represented measured isothermal data for HFC-32 + 3-methyl-1-propylpyridinium bis(trifluoromethylsulfonyl)imide, open triangles ($\triangle$) represent measured isothermal data for HFC-32 + 1-butyl-3-methylimidazolium hexafluorophosphate at 25 °C, filled circles ($\bullet$) represent measured isothermal data for HFC-32 + 1-butyl-3-methylimidazolium tetrafluoroborate at 25 °C, filled squares ($\blacksquare$) represent measured isothermal data for HFC-32 + 1,3-dioctylimidazolium iodide at 25 °C, and filled triangles ($\blacktriangle$) represent measured isothermal data for HFC-32 + 1-octyl-3-methylimidazolium iodide at 25 °C. Solid lines represent data trends.

FIG. 12 shows measured isothermal solubility data (in mole fraction) at 10 °C of the systems HFC-32, HFC-152a, HFC-134a, HFC-125, and HFC-143a + [bmim][PF₆] in terms of absolute pressure divided by the gas saturation pressure at 10 °C shown by ratio (P/P_0). Open cross hatch (x) represents measured isothermal data for HFC-32 at 10 °C with $P_0 = 11.069$ bar, filled diamonds ($\blacklozenge$) represents measured isothermal data for HFC-152a at 10 °C with $P_0 = 3.7277$ bar, filled circles ($\bullet$) represent measured isothermal data for HFC-134a at 10 °C with $P_0 = 4.1461$ bar, filled triangles ($\blacktriangle$) represent measured isothermal data for HFC-125 at 10 °C with $P_0 = 9.0875$ bar, filled squares ($\blacksquare$) represent measured isothermal data for HFC-143a at 10 °C with $P_0 = 8.3628$ bar. Solid lines represent data trend and dashed line represents Raoult's Law.

FIG. 13 shows a schematic diagram of the gravimetric microbalance used for measuring gas absorption in the ionic liquids. In the diagram j_1 , j_2 , and j_3 refer to the counter-weight, hook and chain, respectively; i_1 , i_2 and i_3 refer to the sample container, wire and chain, respectively, W_g refers to the force due to gravity; and B refers to the force due to buoyancy.

Detailed Description

In this disclosure, definitions are provided for various terms as set forth in the following list and elsewhere below:

The term “ionic liquid” is defined as an organic salt that is fluid at or
5 below about 100 °C.

The term “fluorinated ionic liquid” is defined as an ionic liquid having at least one fluorine on either the cation or the anion. A “fluorinated cation” or “fluorinated anion” is a cation or anion, respectively, comprising at least one
10 fluorine.

The terms “refrigerant pair” and “refrigerant/ionic liquid pair” are used interchangeably and refer to a pair or mixture comprising both a refrigerant and an ionic liquid. A “refrigerant pair composition” is a composition comprising a
15 refrigerant pair. A “mixed refrigerant” is a refrigerant composition comprising at least two refrigerants.

A “refrigerant” is a fluidic substance such as a fluorocarbon (FC), hydrofluorocarbon (HFC), chlorofluorocarbon (CFC), hydrochlorofluorocarbon
20 (HCFC), or ammonia, alkanes, alkenes, aromatics, carbon dioxide, or other gas such as hydrogen, oxygen, nitrogen, and argon that may be used as a thermal energy transfer vehicle. A refrigerant, when it changes phase from liquid to vapor (evaporates), removes heat from the surroundings; and when it changes phase from vapor to liquid (condenses), it adds heat to the surroundings. Although the
25 term refrigerant may carry the connotation of a substance used only for cooling, the term is used herein in the generic sense of a thermal energy transfer vehicle or substance that is applicable for use in a system or apparatus that may be used for heating or cooling.

30 The term “fluorinated refrigerant” or “fluorine-containing refrigerant” refers to a fluorocarbon, hydrofluorocarbon, chlorofluorocarbon, or hydrochlorofluorocarbon.

The term “vacuum” refers to pressures less than about 1 bar but greater than about 10^{-4} bar for practical use in absorption cycles.

The term “alkane” refers to a saturated hydrocarbon having the general formula C_nH_{2n+2} that may be a straight-chain, branched or cyclic. A cyclic compound requires a minimum of three carbons.

The term “alkene” refers to an unsaturated hydrocarbon that contains one or more C=C double bonds and that may be a straight-chain, branched or cyclic. An alkene requires a minimum of two carbons. A cyclic compound requires a minimum of three carbons.

The term “aromatic” refers to benzene and compounds that resemble benzene in chemical behavior.

A “heteroatom” is an atom other than carbon in the structure of an alkanyl, alkenyl, cyclic or aromatic compound.

“Heteroaryl” refers to an alkyl group having a heteroatom.

An “azeotropic” or “constant boiling” mixture of two or more refrigerants is a mixture wherein the composition of the vapor and liquid phases are substantially the same at a temperature and pressure encountered in a cooling or heating cycle. Included in the definition of a constant boiling mixture is a “near-azeotropic” mixture, which, as described in U.S. Pat. No. 5,709,092, maintains a substantially constant vapor pressure even after evaporative losses, thereby exhibiting constant boiling behavior.

Hybrid vapor compression – absorption cycles

The present invention relates to a hybrid vapor compression - absorption cooling and heating system that utilizes refrigerant pairs comprising at least one refrigerant and at least one absorbent. In preferred embodiments, the absorbent may be one or more ionic liquids. The invention also provides a process for

temperature adjustment, either cooling or heating, utilizing refrigerant/absorbent pairs in a hybrid vapor compression - absorption cooling or heating system.

Vapor compression and absorption cycles, and systems in which they are run, are described in Application Guide for Absorption Cooling/Refrigeration Using Recovered Heat [Dorgan *et al* (American Society of Heating, Refrigeration and Air Conditioning Engineers, Inc., 1995, Atlanta, GA, Chapter 5)]. A schematic diagram for a system in which a simple vapor compression cycle is run is shown in Figure 1. The system is composed of condenser and evaporator units with an expansion valve, and a vapor compressor that is capable of mechanically increasing the pressure of a refrigerant vapor. A schematic diagram for a simple absorption cycle is shown in Figure 2. The system is composed of condenser and evaporator units with an expansion valve similar to an ordinary vapor compression cycle shown in Figure 1, but an absorber-generator solution circuit replaces the compressor. The circuit may be composed of an absorber, a generator, a heat exchanger, a pressure control device (A) and a pump for circulating the solution. In some embodiments, the heat released by the absorber upon the absorption of the refrigerant by the absorbent may be used to heat a mixture of refrigerant and absorbent in the generator to separate the refrigerant in vapor form from the absorbent.

A schematic diagram for a system running a simple hybrid vapor compression-absorption cycle with a parallel configuration is shown in Figure 3. The system is composed of a condenser unit and an evaporator unit with an expansion valve similar to an ordinary vapor compression cycle as shown in Figure 1, a compressor, an absorber-generator solution circuit, which has a vapor absorber, a gas generator, a heat exchanger, a pressure control (reducing) valve (A), a solution liquid pump, and isolation valves to direct the refrigerant flow path (B-E).

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The parallel configuration can operate in three modes. Mode 1 operates like a conventional absorption cycle where isolation valves D and E are closed and isolation valves B and C are open, which reassembles the same flow path as shown in Figure 2. Mode 2 operates like a conventional vapor compression cycle

where isolation valves D and E are open and isolation valves B and C are closed, which reassembles the same flow path as shown in Figure 1. Mode 3 combines the use of both the vapor compression and the absorption cycles where isolation valves B, C, D, and E are all open, as shown in Figure 3. The system is referred to as a “hybrid” system because the same configuration of the equipment and/or apparatus can be run with or without the involvement of the compressor.

A schematic diagram for a system running a simple hybrid vapor compression-absorption cycle with a series configuration is shown in Figure 4. The system is composed of a condenser unit and an evaporator unit with an expansion valve (similar to an ordinary vapor compression cycle as shown in Figure 1), a compressor, an absorber-generator solution circuit, which has a vapor absorber, a gas generator, a heat exchanger, a pressure control (reducing) valve (A), a solution liquid pump, and isolation valves to direct the refrigerant flow path (B-E).

The series configuration can also operate in three modes. Mode 1 operates like a conventional absorption cycle where isolation valves D and E are closed and isolation valves B and C are open, which reassembles the same flow path as shown in Figure 2. Mode 2 operates like a conventional vapor compression cycle where isolation valve E is open and isolation valves B, C, and D are closed, which reassembles the same flow path as shown in Figure 1. In this case the results are identical to those described in the previous case for parallel configuration Mode 2. Mode 3 combines the use of both the vapor compression and the absorption cycles where isolation valves C and D are open and isolation valves B and E are closed as shown in Figure 4. The system is referred to as a “hybrid” system because in one configuration of the equipment and/or apparatus (Mode 3), the pressure of the refrigerant vapor can be increased by both a generator and a compressor.

When an ionic liquid is used as the absorbent, the two cycles (absorption and vapor compression) may be directly linked because the same refrigerant gas can be used in both cycles, and this eliminates the need of a secondary heat exchanger and increases the overall cycle efficiency.

The present invention also provides an apparatus for adjusting temperature that executes a hybrid vapor compression-absorption cycle as described herein to cool or heat an object (for example a conduit or a container), a medium (for example a fluid such as air or water) or a space. The apparatus may include components such as an absorber-generator solution circuit (which by the outflow and inflow of heat increases the pressure of refrigerant vapor as a compressor does mechanically) where the circuit may be composed of an absorber, a generator, a heat exchanger, a pressure control device and a pump for circulating the solution. The apparatus also is composed of condenser and evaporator units with an expansion valve similar to equipment used in an ordinary vapor compression cycle. As this is a hybrid system, a conventional compressor is used in parallel or series configuration with the above described elements of an absorption refrigeration cycle. The apparatus hereof is capable of executing a hybrid vapor compression-absorption cycle using any one or more of the refrigerants described herein and/or any one or more absorbents, including for example any of the ionic liquids described herein. The apparatus hereof is capable of executing any one or more of the processes as described herein. Yet another embodiment of this invention is an apparatus substantially as shown or described in either of Figures 3 and 4.

An apparatus of this invention may be deployed for use in, or fabricated or operated as, a refrigerator, a freezer, an ice machine, an air conditioner, an industrial cooling system, a heater or heat pump. Each of these instruments may be situated in a residential, commercial or industrial setting, or may be incorporated into a mobilized device such as a car, truck, bus, train, airplane, or other device for transportation, or may be incorporated into a piece of equipment such as a medical instrument.

This invention also provides an apparatus for heating an object, medium or space that includes (a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent; (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor; (c) a condenser,

located in proximity to the object, medium or space to be heated, that receives the vapor from the generator and condenses the vapor under pressure to a liquid; (d) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant; (e) an evaporator that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form first and second portions of refrigerant vapor; (f) a compressor that receives the first portion of the refrigerant vapor, increases the pressure thereof, and passes the first portion of the refrigerant vapor to the condenser; and (g) a conduit that passes the second portion of the refrigerant vapor leaving the evaporator to the absorber.

This invention also provides an apparatus for cooling an object, medium or space that includes (a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent; (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor; (c) a condenser that receives the vapor from the generator and condenses the vapor under pressure to a liquid; (d) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant; (e) an evaporator, located in proximity to the object, medium or space to be cooled, that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form first and second portions of refrigerant vapor; (f) a compressor that receives the first portion of the refrigerant vapor, increases the pressure thereof, and passes the first portion of the refrigerant vapor to the condenser; and (g) a conduit that passes the second portion of the refrigerant vapor leaving the evaporator to the absorber.

This invention also provides an apparatus for heating an object, medium or space that includes (a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent; (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor; (c) a compressor

that receives the vapor from the generator and further increases its pressure; (d) a condenser, located in proximity to the object, medium or space to be heated, that receives the vapor from the compressor and condenses the vapor under pressure to a liquid; (e) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant; (f) an evaporator that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form refrigerant vapor; and (g) a conduit that passes the refrigerant vapor leaving the evaporator to the absorber.

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This invention also provides an apparatus for cooling an object, medium or space that includes (a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent; (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor; (c) a compressor that receives the vapor from the generator and further increases its pressure; (d) a condenser that receives the vapor from the compressor and condenses the vapor under pressure to a liquid; (e) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant; (f) an evaporator, located in proximity to the object, medium or space to be cooled, that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form refrigerant vapor; and (g) a conduit that passes the refrigerant vapor leaving the evaporator to the absorber.

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This invention also provides a process for heating an object, medium or a space comprising (a) absorbing refrigerant vapor with an absorbent to form a mixture; (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor; (c) condensing the refrigerant vapor under pressure to a liquid in proximity to the object, medium or space to be heated; (d) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form first and second portions of refrigerant vapor; (e-1) mechanically increasing the pressure of the first portion of refrigerant vapor, and then repeating step (c) to subject the first portion of refrigerant vapor to

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condensation to liquid; and (e-2) repeating step (a) to re-absorb, with the absorbent, the second portion of refrigerant vapor.

5 This invention also provides a process for cooling an object, medium or a space comprising (a) absorbing refrigerant vapor with an absorbent to form a mixture; (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor; (c) condensing the refrigerant vapor under pressure to a liquid; (d) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant, in proximity to the object,
10 medium or space to be cooled, to form first and second portions of refrigerant vapor; (e-1) mechanically increasing the pressure of the first portion of refrigerant vapor, and then repeating step (c) to subject the first portion of refrigerant vapor to condensation to liquid; and (e-2) repeating step (a) to re-absorb, with the absorbent, the second portion of refrigerant vapor.

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This invention also provides a process for heating an object, medium or a space comprising (a) absorbing refrigerant vapor with an absorbent to form a mixture; (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor; (c) further increasing
20 the pressure of the refrigerant vapor mechanically; (d) condensing the refrigerant vapor under pressure to a liquid in proximity to the object, medium or space to be heated; (e) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form refrigerant vapor; and (f) repeating step (a) to re-absorb the refrigerant vapor with the absorbent.

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This invention also provides a process for cooling an object, medium or a space comprising (a) absorbing refrigerant vapor with an absorbent to form a mixture; (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor; (c) further increasing
30 the pressure of the refrigerant vapor mechanically; (d) condensing the refrigerant vapor under pressure to a liquid; (e) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form refrigerant vapor in proximity to the object, medium or space to be cooled; and (f) repeating step (a) to re-absorb the refrigerant vapor with the absorbent.

This invention also provides a process for heating an object, medium or a space in an apparatus that executes a hybrid vapor compression-absorption cycle by (a) forming in an absorber a mixture of a refrigerant and an absorbent; (b) passing the mixture to a generator where the mixture is heated to separate refrigerant, in vapor form, from the absorbent, and the pressure of the refrigerant vapor is increased; (c) passing the refrigerant vapor to a condenser where the vapor is condensed under pressure to a liquid in proximity to the object, medium or space to be heated; (d) passing the liquid refrigerant to an expansion device where the pressure of the liquid refrigerant is reduced to form a mixture of liquid and vapor refrigerant; (e) passing the mixture of liquid and vapor refrigerant to an evaporator where the remaining liquid is evaporated to form first and second portions of refrigerant vapor; (f-1) passing the first portion of the refrigerant vapor to a compressor to increase the pressure thereof, and then passing the first portion of the refrigerant vapor to the condenser where the vapor is condensed under pressure to a liquid by repeating step (c); and (f-2) passing the second portion of the refrigerant vapor to the absorber to repeat step (a) and form a mixture of the second portion of the refrigerant vapor and the absorbent.

This invention also provides a process for cooling an object, medium or a space in an apparatus that executes a hybrid vapor compression-absorption cycle by (a) forming in an absorber a mixture of a refrigerant and an absorbent; (b) passing the mixture to a generator where the mixture is heated to separate refrigerant, in vapor form, from the absorbent, and the pressure of the refrigerant vapor is increased; (c) passing the refrigerant vapor to a condenser where the vapor is condensed under pressure to a liquid; (d) passing the liquid refrigerant to an expansion device where the pressure of the liquid refrigerant is reduced to form a mixture of liquid and vapor refrigerant; (e) passing the mixture of liquid and vapor refrigerant to an evaporator in proximity to the object, medium or space to be cooled where the remaining liquid is evaporated to form first and second portions of refrigerant vapor; (f-1) passing the first portion of the refrigerant vapor to a compressor to increase the pressure thereof, and then passing the first portion of the refrigerant vapor to the condenser where the vapor is condensed under pressure to a liquid by repeating step (c); and (f-2) passing the second

portion of the refrigerant vapor to the absorber to repeat step (a) and form a mixture of the second portion of the refrigerant vapor and the absorbent.

This invention also provides a process for heating an object, medium or a space in an apparatus that executes a hybrid vapor compression-absorption cycle by (a) forming in an absorber a mixture of a refrigerant and an absorbent; (b) passing the mixture to a generator where the mixture is heated to separate refrigerant, in vapor form, from the absorbent, and the pressure of the refrigerant vapor is increased; (c) passing the refrigerant vapor to a compressor to further increase its pressure; (d) passing the refrigerant vapor to a condenser in proximity to the object, medium or space to be heated where the vapor is condensed under pressure to a liquid; (e) passing the liquid refrigerant to an expansion device where the pressure of the liquid refrigerant is reduced to form a mixture of liquid and vapor refrigerant; (f) passing the mixture of liquid and vapor refrigerant to an evaporator where the remaining liquid is evaporated to form refrigerant vapor; and (g) passing the refrigerant vapor leaving the evaporator to the absorber to repeat step (a) and re-form a mixture of the refrigerant vapor and the absorbent.

This invention also provides a process for cooling an object, medium or a space in an apparatus that executes a hybrid vapor compression-absorption cycle by (a) forming in an absorber a mixture of a refrigerant and an absorbent; (b) passing the mixture to a generator where the mixture is heated to separate refrigerant, in vapor form, from the absorbent, and the pressure of the refrigerant vapor is increased; (c) passing the refrigerant vapor to a compressor to further increase its pressure; (d) passing the refrigerant vapor to a condenser where the vapor is condensed under pressure to a liquid; (e) passing the liquid refrigerant to an expansion device where the pressure of the liquid refrigerant is reduced to form a mixture of liquid and vapor refrigerant; (f) passing the mixture of liquid and vapor refrigerant to an evaporator in proximity to the object, medium or space to be cooled where the remaining liquid is evaporated to form refrigerant vapor; and (g) passing the refrigerant vapor leaving the evaporator to the absorber to repeat step (a) and re-form a mixture of the refrigerant vapor and the absorbent.

In any process as described above, the absorbent separated from refrigerant in step (b) may be recirculated for use in a later step.

5 Refrigerant/Absorbent Pairs:

Refrigerants:

The present invention provides refrigerant pair compositions for use in hybrid vapor compression - absorption cycles. Hybrid vapor compression - absorption cycles can be used for cooling, or for generating heat, depending on the application. One member of the refrigerant pair comprises at least one refrigerant selected from the group consisting of hydrofluorocarbon, hydrochlorofluorocarbon, chlorofluorocarbon, fluorocarbon, nitrogen (N₂), oxygen (O₂), carbon dioxide (CO₂), ammonia (NH₃), argon (Ar), hydrogen (H₂), water (H₂O), and non-fluorinated hydrocarbon, wherein the non-fluorinated hydrocarbon is selected from the group consisting of C₁ to C₄ straight-chain, branched or cyclic alkanes and C₁ to C₄ straight-chain, branched or cyclic alkenes. The second member of the refrigerant pair comprises at least one ionic liquid.

Hydrofluorocarbon refrigerants may include compounds having any combination of hydrogen and fluorine with carbon and include compounds with carbon-carbon double bonds with normal boiling points below 0 °C. Examples of hydrofluorocarbon refrigerants useful for the invention include difluoromethane (HFC-32), pentafluoroethane (HFC-125), 1,1,2,2-tetrafluoroethane (HFC-134), 1,1,1,2-tetrafluoroethane (HFC-134a), 1,1,1-trifluoroethane (HFC-143a), 1,1-difluoroethane (HFC-152a) and fluoroethane (HFC-161). In one embodiment of the invention, the hydrofluorocarbon refrigerants are selected from the group consisting of difluoromethane (HFC-32), pentafluoroethane (HFC-125), 1,1,1,2-tetrafluoroethane (HFC-134a), 1,1,1-trifluoroethane (HFC-143a) and 1,1-difluoroethane (HFC-152a).

30

Chlorofluorocarbon refrigerants may include compounds having any combination of chlorine and fluorine with carbon and include compounds with carbon-carbon double bonds with normal boiling points below 0 °C. An example

of a chlorofluorocarbon refrigerant useful for the invention is dichlorodifluoromethane (CFC-12).

Hydrochlorofluorocarbon refrigerants may include compounds with any combination of hydrogen, chlorine and fluorine with carbon and include compounds with carbon-carbon double bonds with normal boiling points below 0 °C. An example of a hydrochlorofluorocarbon refrigerant useful for the invention includes chlorodifluoromethane (HCFC-22).

Fluorocarbon refrigerants may include compounds with any combination of fluorine and carbon and include compounds with carbon-carbon double bonds with normal boiling points below 0 °C. Examples of fluorocarbon refrigerants useful for the invention include perfluoromethane (FC-14) and perfluoroethane (FC-116).

Non-fluorinated hydrocarbon refrigerants useful for the invention may include methane, ethane, ethylene, propane, cyclopropane, propylene, butane, butene and isobutane.

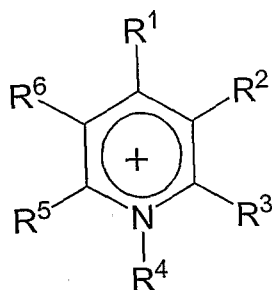
A refrigerant as used herein may also be selected from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, methane, ethane, propane, cyclopropane, propylene, butane, butene, and isobutane.

Mixtures of refrigerants are also useful for achieving proper boiling temperature or pressure appropriate for absorption equipment. In particular mixtures which form azeotropes or constant boiling mixtures are preferred because minimal to no fractionation of the mixture will occur if the refrigerant leaks from the absorption cooling system. U.S. Patent No. 5,709,092, for example, discloses azeotropic or constant boiling compositions of difluoromethane (HFC-32), pentafluoroethane (HFC-125), and 1,1,1,2-tetrafluoroethane (HFC-134a), for use as refrigerants.

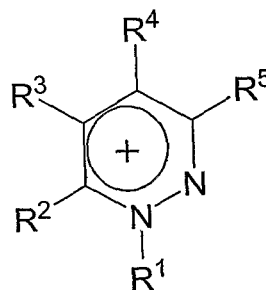
Absorbents:

In a preferred embodiment, the absorbent used in this invention is an ionic liquid. The ionic liquid useful for the invention in principle can be any ionic liquid that absorbs the refrigerant gas. Ionic liquids that have minimal absorption of the refrigerant gas will be less effective as absorption cycle working fluids. Ideally, high absorption and diffusivity are required to achieve a high-energy efficiency absorption cycle. Ionic liquids, which are described in WO 05/113,702 (and references therein cited), may be synthesized by salt metathesis, by an acid-base neutralization reaction or by quaternizing a selected nitrogen-containing compound; or they may be obtained commercially from several companies such as Merck (Darmstadt, Germany) or BASF (Mount Olive, NJ). A cation or anion of an ionic liquid of the invention can in principle be any cation or anion such that the cation and anion together form an organic salt that is liquid at or below about 100 °C.

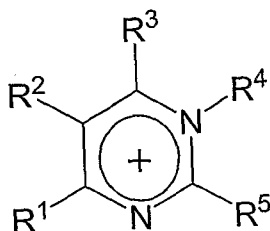
In one embodiment of the invention, ionic liquids may have cations selected from the following Formulae:



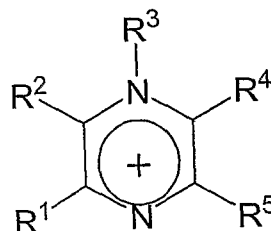
Pyridinium



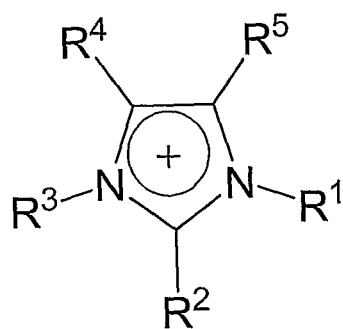
Pyridazinium



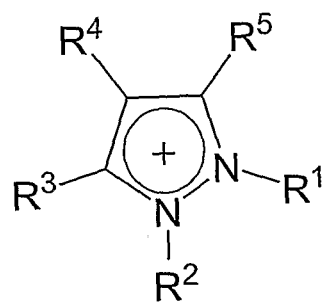
Pyrimidinium



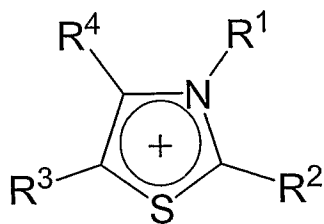
Pyrazinium



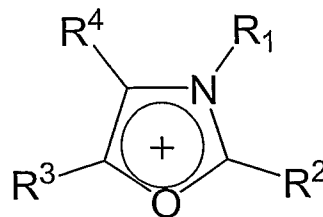
Imidazolium



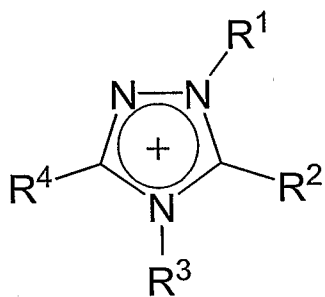
Pyrazolium



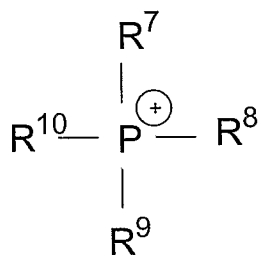
Thiazolium



Oxazolium

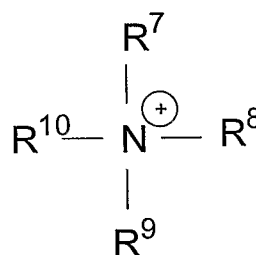


Triazolium



Phosphonium

and



Ammonium

wherein R^1 , R^2 , R^3 , R^4 , R^5 and R^6 are each independently selected from the group consisting of:

- (i) H;
- (ii) halogen;
- (iii) $-CH_3$, $-C_2H_5$, or C_3 to C_{25} straight-chain, branched or cyclic alkane or alkene, optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH_2 and SH;
- (iv) $-CH_3$, $-C_2H_5$, or C_3 to C_{25} straight-chain, branched or cyclic alkane or alkene comprising one to three heteroatoms selected from the group consisting of O, N, Si and S, and

- optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH;
- 5 (v) C₆ to C₂₀ unsubstituted aryl, or C₃ to C₂₅ unsubstituted heteroaryl having one to three heteroatoms independently selected from the group consisting of O, N, Si and S; and
- (vi) C₆ to C₂₅ substituted aryl, or C₃ to C₂₅ substituted heteroaryl having one to three heteroatoms independently selected from the group consisting of O, N, Si and S; wherein said substituted aryl or substituted heteroaryl has
- 10 one to three substituents independently selected from the group consisting of:
- (1) -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or cyclic alkane or alkene, optionally substituted with at least one member selected from the group consisting of
- 15 Cl, Br, F, I, OH, NH₂ and SH,
- (2) OH,
- (3) NH₂, and
- (4) SH; and
- wherein R⁷, R⁸, R⁹, and R¹⁰ are each independently selected from the group
- 20 consisting of:
- (vii) -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or cyclic alkane or alkene, optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH;
- 25 (viii) -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or cyclic alkane or alkene comprising one to three heteroatoms selected from the group consisting of O, N, Si and S, and optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH;
- 30 (ix) C₆ to C₂₅ unsubstituted aryl, or C₃ to C₂₅ unsubstituted heteroaryl having one to three heteroatoms independently selected from the group consisting of O, N, Si and S; and
- (x) C₆ to C₂₅ substituted aryl, or C₃ to C₂₅ substituted heteroaryl having one to three heteroatoms independently selected

from the group consisting of O, N, Si and S;
wherein said substituted aryl or substituted heteroaryl has
one to three substituents independently selected from the
group consisting of:

- 5 (1) -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or
cyclic alkane or alkene, optionally substituted with at
least one member selected from the group consisting of
Cl, Br, F, I, OH, NH₂ and SH,
- (2) OH,
- 10 (3) NH₂, and
- (4) SH; and

wherein optionally at least two of R¹, R², R³, R⁴, R⁵, R⁶, R⁷, R⁸, R⁹, and R¹⁰ can
together form a cyclic or bicyclic alkanyl or alkenyl group.

15 In another embodiment, an ionic liquid useful for the invention may
comprise a fluorinated cation wherein any one of, or any group of more than one
of, R¹, R², R³, R⁴, R⁵, R⁶, R⁷, R⁸, R⁹ and R¹⁰ comprises F⁻.

In a further embodiment, an ionic liquid may have an anion selected from
20 the group consisting of [CH₃CO₂]⁻, [HSO₄]⁻, [CH₃OSO₃]⁻, [C₂H₅OSO₃]⁻, [AlCl₄]⁻,
[CO₃]²⁻, [HCO₃]⁻, [NO₂]⁻, [NO₃]⁻, [SO₄]²⁻, [PO₄]³⁻, [HPO₄]²⁻, [H₂PO₄]⁻, [HSO₃]⁻,
[CuCl₂]⁻, Cl⁻, Br⁻, I⁻, SCN⁻; and any fluorinated anion. Fluorinated anions useful
herein may include [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻,
[CF₃HFCCF₂SO₃]⁻, [HCClFCF₂SO₃]⁻, [(CF₃SO₂)₂N]⁻, [(CF₃CF₂SO₂)₂N]⁻,
25 [(CF₃SO₂)₃C]⁻, [CF₃CO₂]⁻, [CF₃OCFHCF₂SO₃]⁻, [CF₃CF₂OCFHCF₂SO₃]⁻,
[CF₃CFHOCF₂CF₂SO₃]⁻, [CF₂HCF₂OCF₂CF₂SO₃]⁻, [CF₂ICF₂OCF₂CF₂SO₃]⁻,
[CF₃CF₂OCF₂CF₂SO₃]⁻, [(CF₂HCF₂SO₂)₂N]⁻, [(CF₃CFHCF₂SO₂)₂N]⁻; and F⁻.

In a further embodiment, an ionic liquid may comprise a cation selected
30 from the group consisting of pyridinium, pyridazinium, pyrimidinium,
pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium, triazolium,
phosphonium, and ammonium cations; and an anion selected from the group
consisting of [CH₃CO₂]⁻, [HSO₄]⁻, [CH₃OSO₃]⁻, [C₂H₅OSO₃]⁻, [AlCl₄]⁻, [CO₃]²⁻,
[HCO₃]⁻, [NO₂]⁻, [NO₃]⁻, [SO₄]²⁻, [PO₄]³⁻, [HPO₄]²⁻, [H₂PO₄]⁻, [HSO₃]⁻, [CuCl₂]⁻,

Cl⁻, Br⁻, I⁻, SCN⁻, and any fluorinated anion. In yet another embodiment, an ionic liquid may comprise a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium, triazolium, phosphonium, and ammonium cations; and an anion selected from the group consisting of [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻, [CF₃HFCCF₂SO₃]⁻, [HCClFCF₂SO₃]⁻, [(CF₃SO₂)₂N]⁻, [(CF₃CF₂SO₂)₂N]⁻, [(CF₃SO₂)₃C]⁻, [CF₃CO₂]⁻, [CF₃OCFHCF₂SO₃]⁻, [CF₃CF₂OCFHCF₂SO₃]⁻, [CF₃CFHOFCF₂CF₂SO₃]⁻, [CF₂HCF₂OCF₂CF₂SO₃]⁻, [CF₂ICF₂OCF₂CF₂SO₃]⁻, [CF₃CF₂OCF₂CF₂SO₃]⁻, [(CF₂HCF₂SO₂)₂N]⁻, [(CF₃CFHCF₂SO₂)₂N]⁻, and F⁻.

In a further embodiment, an ionic liquid may comprise a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium, triazolium, phosphonium, and ammonium cations as defined above, wherein any one of, or any group of more than one of, R¹, R², R³, R⁴, R⁵, R⁶, R⁷, R⁸, R⁹, and R¹⁰ comprises F⁻; and an anion selected from the group consisting of [CH₃CO₂]⁻, [HSO₄]⁻, [CH₃OSO₃]⁻, [C₂H₅OSO₃]⁻, [AlCl₄]⁻, [CO₃]²⁻, [HCO₃]⁻, [NO₂]⁻, [NO₃]⁻, [SO₄]²⁻, [PO₄]³⁻, [HPO₄]²⁻, [H₂PO₄]⁻, [HSO₃]⁻, [CuCl₂]⁻, Cl⁻, Br⁻, I⁻, SCN⁻; and any fluorinated anion. In still another embodiment, an ionic liquid may comprise a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium, triazolium, phosphonium, and ammonium cations as defined above, wherein any one of, or any group of more than one of, R¹, R², R³, R⁴, R⁵, R⁶, R⁷, R⁸, R⁹, and R¹⁰ comprises F⁻; and an anion selected from the group consisting of [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻, [CF₃HFCCF₂SO₃]⁻, [HCClFCF₂SO₃]⁻, [(CF₃SO₂)₂N]⁻, [(CF₃CF₂SO₂)₂N]⁻, [(CF₃SO₂)₃C]⁻, [CF₃CO₂]⁻, [CF₃OCFHCF₂SO₃]⁻, [CF₃CF₂OCFHCF₂SO₃]⁻, [CF₃CFHOFCF₂CF₂SO₃]⁻, [CF₂HCF₂OCF₂CF₂SO₃]⁻, [CF₂ICF₂OCF₂CF₂SO₃]⁻, [CF₃CF₂OCF₂CF₂SO₃]⁻, [(CF₂HCF₂SO₂)₂N]⁻, [(CF₃CFHCF₂SO₂)₂N]⁻, and F⁻.

In a further embodiment, an ionic liquid may comprise a cation selected from 1,2-dimethyl-3-propylimidazolium, 3-methyl-1-propylpyridinium, 1-ethyl-3-

- methylimidazolium, 1-propyl-2,3-dimethylimidazolium, 1-propyl-3-methylpyridinium, 1-butyl-3-methylimidazolium, 1-butyl-3-methylpyridinium, 1-heptyl-3-methylimidazolium, 1-octyl-3-methylimidazolium, 1,3-dioctylimidazolium, 1-dodecyl-3-methylimidazolium,
- 5 tetradecyl(trihexyl)phosphonium, and tributyl(tetradecyl)phosphonium cations; and an anion selected from the group consisting of $[\text{CH}_3\text{CO}_2]^-$, $[\text{HSO}_4]^-$, $[\text{CH}_3\text{OSO}_3]^-$, $[\text{C}_2\text{H}_5\text{OSO}_3]^-$, $[\text{AlCl}_4]^-$, $[\text{CO}_3]^{2-}$, $[\text{HCO}_3]^-$, $[\text{NO}_2]^-$, $[\text{NO}_3]^-$, $[\text{SO}_4]^{2-}$, $[\text{PO}_4]^{3-}$, $[\text{HPO}_4]^{2-}$, $[\text{H}_2\text{PO}_4]^-$, $[\text{HSO}_3]^-$, $[\text{CuCl}_2]^-$, Cl^- , Br^- , I^- , SCN^- , $[\text{BF}_4]^-$, $[\text{PF}_6]^-$, $[\text{SbF}_6]^-$, $[\text{CF}_3\text{SO}_3]^-$, $[\text{HCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{HFCCF}_2\text{SO}_3]^-$, $[\text{HCClCF}_2\text{SO}_3]^-$,
- 10 $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{CF}_2\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{SO}_2)_3\text{C}]^-$, $[\text{CF}_3\text{CO}_2]^-$, $[\text{CF}_3\text{OCFHCF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{CF}_2\text{OCFHCF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{CFHOCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_2\text{HCF}_2\text{OCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_2\text{ICF}_2\text{OCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{CF}_2\text{OCF}_2\text{CF}_2\text{SO}_3]^-$, $[(\text{CF}_2\text{HCF}_2\text{SO}_2)_2\text{N}]^-$, and $[(\text{CF}_3\text{CFHCF}_2\text{SO}_2)_2\text{N}]^-$.

In a further embodiment, an ionic liquid suitable for use herein may be selected from the group consisting of

- 1-butyl-3-methylimidazolium hexafluorophosphate [bmim][PF₆],
- 1-butyl-3-methylimidazolium tetrafluoroborate [bmim][BF₄],
- 1,2-dimethyl-3-propylimidazolium
- tris(trifluoromethylsulfonyl)methide [dmpim][TMeM],
- 1-octyl-3-methylimidazolium iodide [omim][I],
- 1,3-dioctylimidazolium iodide [doim][I],
- 1-ethyl-3-methylimidazolium bis(pentafluoroethylsulfonyl)imide
- [emim][BEI],
- 1,2-dimethyl-3-propylimidazolium
- bis(trifluoromethylsulfonyl)imide [dmpim][BMeI],
- 3-methyl-1-propylpyridinium bis(trifluoromethylsulfonyl)imide
- [pmpy][BMeI],
- 1-ethyl-3-methylimidazolium hexafluorophosphate [emim][PF₆],
- 1-ethyl-3-methylimidazolium bis(trifluoroethylsulfonyl)imide
- [emim][BMeI],
- 1-butyl-3-methylpyridinium bis(trifluoromethylsulfonyl)imide
- [bmpy][BMeI],
- 1-ethyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate
- [emim][TFES],
- 1-butyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate
- [bmim][TFES],
- 1-dodecyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate
- [dmim][TFES],
- 1-heptyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate
- [hmim][TFES],
- 1-butyl-3-methylimidazolium acetate [bmim][Ac],
- 1-butyl-3-methylimidazolium 2-(1,2,2,2-tetrafluoroethoxy)-
- 1,1,2,2-tetrafluoroethanesulfonate [bmim][FS],
- 1-butyl-3-methylimidazolium 1, 1, 2, 3, 3, 3-
- hexafluoropropanesulfonate [bmim][HFPS],
- 1-butyl-3-methylimidazolium methyl sulfonate [bmim][MeSO₄],
- 1-butyl-3-methylimidazolium thiocyanate [bmim][SCN],

- 1-butyl-3-methylimidazolium 1, 1, 2-trifluoro-2-(perfluoroethoxy)ethanesulfonate [bmim][TPES],
 1-butyl-3-methylimidazolium 1, 1, 2-trifluoro-2-(trifluoromethoxy)ethanesulfonate [bmim][TTES],
 1-butyl-3-methylimidazolium 1,1,2-trifluoro-2-(trifluoromethoxy)ethanesulfonate [bmim][TTES],
 1-butyl-3-methylimidazolium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate [bmim][TPES],
 1-ethyl-3-methylimidazolium bis(pentafluoroethylsulfonyl)imide
 [emim][BEI],
 1-butyl-3-methylimidazolium 1,1,2,3,3-hexafluoropropanesulfonate [bmim][HFPS],
 tetradecyl(trihexyl) phosphonium 1,1,2-trifluoro-2-(perfluoroethoxy) ethanesulfonate [6,6,6,14-P][TPES], and
 tributyl(tetradecyl)phosphonium 1,1,2,3,3,3-hexafluoropropanesulfonate [4,4,4,14-P][HFPS].

Refrigerant/Ionic Liquid Pairs:

Hybrid vapor compression-absorption cycles of the invention comprise refrigerant pairs consisting of at least one refrigerant selected from the group consisting of hydrofluorocarbon, hydrochlorofluorocarbon, chlorofluorocarbon, fluorocarbon, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, and non-fluorinated hydrocarbon selected from the group consisting of C₁ to C₄ straight-chain, branched or cyclic alkanes and C₁ to C₄ straight-chain, branched or cyclic alkenes; and at least one ionic liquid. In another embodiment, refrigerant pairs consist of at least one refrigerant selected from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, methane, ethane, propane, cyclopropane, propylene, butane, butene, and isobutane; and at least one ionic liquid.

In a further embodiment, refrigerant pairs may include at least one refrigerant selected from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, methane, ethane, propane, cyclopropane,

propylene, butane, butene, and isobutane; and at least one ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations. In a further embodiment, refrigerant pairs may include at least

5 one refrigerant selected from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, methane, ethane, propane, cyclopropane, propylene, butane, butene, and isobutane; and at least one ionic liquid having an anion selected from the group consisting of

10 [CH₃CO₂]⁻, [HSO₄]⁻, [CH₃OSO₃]⁻, [C₂H₅OSO₃]⁻, [AlCl₄]⁻, [CO₃]²⁻, [HCO₃]⁻, [NO₂]⁻, [NO₃]⁻, [SO₄]²⁻, [PO₄]³⁻, [HPO₄]²⁻, [H₂PO₄]⁻, [HSO₃]⁻, [CuCl₂]⁻, Cl⁻, Br⁻, I⁻, SCN⁻, [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻, [CF₃HFCCF₂SO₃]⁻, [HCClCF₂SO₃]⁻, [(CF₃SO₂)₂N]⁻, [(CF₃CF₂SO₂)₂N]⁻, [(CF₃SO₂)₃C]⁻, [CF₃CO₂]⁻, [CF₃OCFHCF₂SO₃]⁻, [CF₃CF₂OCFHCF₂SO₃]⁻, [CF₃CFHOCF₂CF₂SO₃]⁻, [CF₂HCF₂OCF₂CF₂SO₃]⁻, [CF₂ICF₂OCF₂CF₂SO₃]⁻, [CF₃CF₂OCF₂CF₂SO₃]⁻, [(CF₂HCF₂SO₂)₂N]⁻, [(CF₃CFHCF₂SO₂)₂N]⁻, and F⁻.

15

Refrigerant pairs useful herein may include at least one refrigerant selected from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, methane, ethane, propane, cyclopropane, propylene, butane, butene, and isobutane; and at least one ionic liquid selected from the group consisting of:

20

a) an ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations;

25

b) an ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations as described above wherein at least one of R¹ through R⁶ comprises fluorine;

30

c) an ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations, and having an anion selected from the group consisting of [CH₃CO₂]⁻,

[HSO₄]⁻, [CH₃OSO₃]⁻, [C₂H₅OSO₃]⁻, [AlCl₄]⁻, [CO₃]⁻, [HCO₃]⁻, [NO₂]⁻, [NO₃]⁻, [SO₄]²⁻, [PO₄]³⁻, [HPO₄]²⁻, [H₂PO₄]⁻, [HSO₃]⁻, [CuCl₂]⁻, Cl⁻, Br⁻, I⁻, and any fluorinated anion;

d) an ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations, and having an anion selected from the group consisting of [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻, [CF₃HFCCF₂SO₃]⁻, [HCClCF₂SO₃]⁻, [(CF₃SO₂)₂N]⁻, [(CF₃CF₂SO₂)₂N]⁻, [(CF₃SO₂)₃C]⁻, [CF₃CO₂]⁻, and F⁻;

e) an ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations as described above wherein at least one of R¹ through R⁶ comprises fluorine, and having an anion selected from the group consisting of [CH₃CO₂]⁻, [HSO₄]⁻, [CH₃OSO₃]⁻, [C₂H₅OSO₃]⁻, [AlCl₄]⁻, [CO₃]²⁻, [HCO₃]⁻, [NO₂]⁻, [NO₃]⁻, [SO₄]²⁻, [PO₄]³⁻, [HPO₄]²⁻, [H₂PO₄]⁻, [HSO₃]⁻, [CuCl₂]⁻, Cl⁻, Br⁻, I⁻, and any fluorinated anion; and

f) an ionic liquid having a cation selected from the group consisting of pyridinium, pyridazinium, pyrimidinium, pyrazinium, imidazolium, pyrazolium, thiazolium, oxazolium and triazolium cations as described above wherein at least one of R¹ through R⁶ comprises fluorine, and having an anion selected from the group consisting of [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻, [CF₃HFCCF₂SO₃]⁻, [HCClCF₂SO₃]⁻, [(CF₃SO₂)₂N]⁻, [(CF₃CF₂SO₂)₂N]⁻, [(CF₃SO₂)₃C]⁻, [CF₃CO₂]⁻, and F⁻.

Additional examples of useful refrigerant pairs include those having at least one refrigerant selected from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12, NH₃, CO₂, N₂, O₂, H₂, Ar, H₂O, methane, ethane, propane, cyclopropane, propylene, butane, butene, and isobutane; and at least one ionic liquid selected from the group consisting of:

g) an ionic liquid having an imidazolium cation or a fluorinated imidazolium cation and an anion selected from the group consisting of [BF₄]⁻, [PF₆]⁻, [SbF₆]⁻, [CF₃SO₃]⁻, [HCF₂CF₂SO₃]⁻,

an ionic liquid having a cation selected from the group consisting of $[\text{CF}_3\text{HFCCF}_2\text{SO}_3]^+$, $[\text{HCCIFCF}_2\text{SO}_3]^+$, $[(\text{CF}_3\text{SO}_2)_2\text{N}]^+$, $[(\text{CF}_3\text{SO}_2)_3\text{C}]^+$, and $[\text{CF}_3\text{CO}_2]^+$;

h) an ionic liquid having 1-ethyl-3-methylimidazolium as the cation and $[(\text{CF}_3\text{CF}_2\text{SO}_2)_2\text{N}]^-$ as the anion;

5 i) an ionic liquid having a 1-butyl-3-methylimidazolium cation or a fluorinated 1-butyl-3-methylimidazolium cation and an anion selected from the group consisting of $[\text{BF}_4]^-$, $[\text{PF}_6]^-$, $[\text{SbF}_6]^-$, $[\text{CF}_3\text{SO}_3]^-$, $[\text{HCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{HFCCF}_2\text{SO}_3]^-$, $[\text{HCCIFCF}_2\text{SO}_3]^-$, $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{CF}_2\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{SO}_2)_3\text{C}]^-$, and $[\text{CF}_3\text{CO}_2]^-$;

10 j) an ionic liquid having a 1-propyl-2,3-dimethylimidazolium cation or a fluorinated 1-propyl-2,3-dimethylimidazolium cation and an anion selected from the group consisting of $[\text{BF}_4]^-$, $[\text{PF}_6]^-$, $[\text{SbF}_6]^-$, $[\text{CF}_3\text{SO}_3]^-$, $[\text{HCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{HFCCF}_2\text{SO}_3]^-$, $[\text{HCCIFCF}_2\text{SO}_3]^-$, $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{CF}_2\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{SO}_2)_3\text{C}]^-$, and $[\text{CF}_3\text{CO}_2]^-$; and preferably from the group consisting of $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$ and $[(\text{CF}_3\text{SO}_2)_3\text{C}]^-$.

15 k) an ionic liquid having a 1-propyl-3-methylimidazolium cation or a fluorinated 1-propyl-3-methylimidazolium cation and an anion selected from the group consisting of $[\text{BF}_4]^-$, $[\text{PF}_6]^-$, $[\text{SbF}_6]^-$, $[\text{CF}_3\text{SO}_3]^-$, $[\text{HCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{HFCCF}_2\text{SO}_3]^-$, $[\text{HCCIFCF}_2\text{SO}_3]^-$, $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{CF}_2\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{SO}_2)_3\text{C}]^-$, and $[\text{CF}_3\text{CO}_2]^-$; and preferably $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$ as the anion; and

20 l) an ionic liquid having a cation selected from the group consisting of 1,3-dioctylimidazolium, 1-octyl-3-methylimidazolium, fluorinated 1,3-dioctylimidazolium, or fluorinated 1-octyl-3-methylimidazolium, and $[\text{I}]^-$ as the anion.

25 Refrigerant pairs useful for the invention may constitute a composition comprising at least one refrigerant and at least one ionic liquid containing about 0.05 to about 99.95 mole percent of a refrigerant over a temperature range from the evaporator temperature to the generator temperature at a pressure from vacuum to the critical pressure. Systems running absorption cycles operate at varying evaporator temperatures and heating temperatures depending on the application. A system running a typical absorption cycle for chilling water may

operate with an evaporator temperature of 5 to 10 °C, or for chilling brine or ethylene glycol to even lower temperatures (i.e. 0 to -40 °C) and the generator can operate over a temperature range from 75 to 240 °C depending on the heat source and the number of stages used. A system running a hybrid vapor compression –
5 absorption cycle could run under the same range of operating temperatures.

In another embodiment, however, a composition comprising a refrigerant and an ionic liquid may contain from about 0.1 to about 99.9 mole percent of a refrigerant over a temperature range from the evaporator temperature (e.g. 5 to
10 10°C as used for chilling water) to the generator temperature [e.g. 75 to 90°C for half effect, 75 to 90°C for single effect, 150 to 180°C for double effect, and 200 to 240°C for triple effect (where half effect, single effect, and double effect are described in *Application Guide for Absorption Cooling/Refrigeration Using Recovered Heat*, Dorgan *et al*, American Society of Heating, Refrigeration and
15 Air Conditioning Engineers, Inc., 1995, Atlanta, GA)] at a pressure from vacuum to the critical pressure. For example,

compositions comprising HFC-32 and ionic liquids comprise from about 0.1 to about 99.9 mole percent of HFC-32 over a temperature range from -40 to 240°C at a pressure from vacuum to 57.8 bar;

20 compositions comprising HFC-125 and ionic liquids comprise from about 0.1 to about 99.9 mole percent of HFC-125 over a temperature range from -40 to 240°C at a pressure from vacuum to 36.2 bar;

compositions comprising HFC-134a and ionic liquids comprise from about 0.1 to about 99.9 mole percent of HFC-134a over a
25 temperature range from -40 to 240°C at a pressure from vacuum to 40.6 bar;

compositions comprising HFC-143a and ionic liquids comprise from about 0.1 to about 99.9 mole percent of HFC-143a over a temperature range from -40 to 240°C at a pressure from vacuum to 37.6
30 bar; and

compositions comprising HFC-152a and ionic liquids comprise from about 0.1 to about 99.9 mole percent of HFC-152a over a

temperature range from -40 to 240°C at a pressure from vacuum to 45.2 bar.

5 Examples of other compositions suitable as a refrigerant pair for use herein in a system running a hybrid vapor compression – absorption cooling or heating system include those in which

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.3 to about 81.2 mole percent of HFC-32 over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 10 bar.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 65.1 mole percent of HFC-125 over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 10 bar.

15 the one ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 72.1 mole percent of HFC-134a over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 3.5 bar.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 23.5 mole percent of HFC-143a over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 10 bar.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.5 to about 79.7 mole percent of HFC-152a over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 4.5 bar.

the ionic liquid is [bmim][BF₄], and the refrigerant pair contains from about 0.1 to about 76.5 mole percent of HFC-32 over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 10 bar.

the ionic liquid is [dmpim][tTFMSmethide], and the refrigerant pair contains from about 0.4 to about 80.2 mole percent of HFC-32 over a

temperature range from about 10 to about 75 °C at a pressure from about 0.1 to about 10 bar.

the ionic liquid is [omim][I], and the refrigerant pair contains from about 0.4 to about 41.6 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to about 10 bar.

the ionic liquid is [doim][I], and the refrigerant pair contains from about 0.7 to about 46.8 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to about 10 bar.

the ionic liquid is [emim][bPFESimide], and the refrigerant pair contains from about 1.0 to about 66.6 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to about 10 bar.

the ionic liquid is [dmpim][bTFMSimide], and the refrigerant pair contains from about 0.8 to about 64.5 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to about 10 bar.

the ionic liquid is [pmpp][bTFMSimide], and the refrigerant pair contains from about 1.0 to about 63.9 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to about 10 bar.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to 63 mole percent of HFC-32 at about 10 °C and P/P₀ from about 0.1 to about 0.63.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 65 mole percent of HFC-125 at about 10 °C and P/P₀ from about 0.1 to about 0.88.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 72 mole percent of HFC-134a at about 10 °C and P/P₀ from about 0.1 to about 0.84.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 25 mole percent of HFC-143a at about 10 °C and P/P₀ from about 0.1 to about 0.90.

the ionic liquid is [bmim][PF₆], and the refrigerant pair contains from about 0.1 to about 80 mole percent of HFC-152a at about 10 °C and P/P₀ from about 0.1 to about 0.86.

Additional examples of refrigerants useful in a composition with an ionic liquid, wherein the refrigerant comprises from about 0.1 to 99 mole percent of the composition, are shown in the following Table 1, along with the normal boiling point temperature, critical point temperature and critical point pressure of each refrigerant. The data in Table 1 were obtained from Reid *et al, supra*; and from REFPROP Version 7, Lemmon *et al*, [NIST reference: Fluid Thermodynamic and Transport Properties – REFPROP, Version 7.0 User's Guide (U.S. Department of Commerce, Technology Administration, National Institute of Standards and Technology, Standard Reference Data Program, Gaithersburg, Maryland, 2002)].

Table 1

Refrigerant	Boiling Point Temperature (°C)	Critical Point Temperature (°C)	Critical Point Pressure (bar)
Perfluoromethane (FC-14)	-128.1	-45.6	37.5
Perfluoroethane (FC-116)	-78.2	19.9	30.5
Perfluoropropane (FC-218)	-36.8	72.0	26.7
Dichlorodifluoromethane (CFC-12)	-29.8	112.0	41.4
Hydrochlorodifluoromethane (HCFC-22)	-40.8	96.1	49.9
Fluoromethane (HFC-41)	-78.1	44.1	59.0
1,1,1,3,3,3-hexafluoropropane (HFC-236fa)	-1.4	124.9	32.0
1,1,1,2,3,3,3-heptafluoropropane (HFC-227ea)	-16.5	101.7	29.3
Carbon Dioxide	-78.4	30.9	73.7
Ammonia	-33.3	132.3	113.3
Nitrogen	-195.8	-147.0	33.9
Oxygen	-183	-118.6	50.4
Hydrogen	-252.8	-240.0	13.2
Argon	-185.9	-122.5	46.0
Methane	-161.5	-82.6	46.0
Ethane	-88.6	32.2	48.7
Ethylene	-103.9	9.3	50.4
Propane	-42.1	96.7	42.4
Propylene	-47.7	92.4	46.6
Cyclopropane	-32.9	124.7	54.9
Butane	-0.6	152.0	37.9
Isobutane	-11.7	134.7	36.4
H ₂ O	100	374	220

The refrigerant pair compositions may be prepared by any convenient method, including mixing or combining the desired amounts of the at least one refrigerant and the at least one ionic liquid in an appropriate container.

Additives, such as lubricants, corrosion inhibitors, stabilizers, dyes, and other appropriate materials may be added to the refrigerant pair compositions for a variety of purposes provided they do not have an adverse influence on the composition, for their intended applications.

To evaluate the performance of an absorption cycle, thermodynamic property charts such as temperature-pressure-concentration (*TPX*) and enthalpy-temperature (*HT*) diagrams are useful. These charts correspond to the familiar *PH* (pressure-enthalpy) or *TS* (temperature-entropy) diagram in vapor compression cycle analysis. However, these charts may not be applicable to an absorption cycle in the same manner as they are to vapor compression with a compressor, where the compression process is theoretically a single isentropic path, while the absorption cycle employs the so-called generator-absorber solution circuit, and several thermodynamic processes are involved.

The *PH* or *TS* diagram in the vapor compression cycle is constructed using equations of state (EOS), and the cycle performance and all thermodynamic properties can be calculated. The thermodynamic charts for the absorption cycle are usually made by empirical correlation equations, which are fitted to experimental solubility and heat capacity data for solution properties, while the vapor phase properties are calculated with the refrigerant EOS. Sometimes, the solubility data are correlated using theoretical solution (often called "activity") models, such as those disclosed in Nezu *et al* (*Natural Working Fluids*, 2002, IIR Gustav Lorentzen Conf. 5th, China, Sept. 17-20, 2002, 446-453); Fatouh *et al* (*Renewable Energy*, 1993, 3, 31-37); Bhatt *et al* (*Heat Recovery System & CHP*, 1992, 12, 225-233]; and Ness *et al* (*Classical Thermodynamics of Nonelectrolyte Solutions with Applications to Phase Equilibria*, 1982, MacGraw-Hill, New York). However, such models are limited in their use to temperatures well below the refrigerant critical temperature, and modeling solutions at high generator temperatures may become invalid. Thus, the combined use of empirical fitting equations or partially correct equations with the gas phase EOS may not always be completely consistent. Therefore, it is desirable to model the absorption cycle process with more thermodynamically sound EOS. Perhaps, one of the most

significant benefits of using EOS is that, even above the critical temperature of refrigerants, thermodynamic properties can be correctly calculated, as discussed in Yokozeki, *Int. J. Refrigeration*, 2004, April (submitted).

Although modeling refrigerant mixtures with EOS is familiar, refrigerant and non-volatile compound mixtures are traditionally treated with empirical correlation models by air conditioning and refrigeration engineers, with regard for example to refrigerant-lubricant oil solubility. One of the difficult problems in using EOS for such mixtures would be to set up EOS parameters for non-volatile compounds without much information about the critical parameters and vapor pressure data. EOS models have been successfully applied to refrigerant-lubricant oil solubility data, however, as disclosed in Yokozeki, *Proc. Int. Compressor Eng. Conf. at Purdue*, 1994, 1, 335-340; Yokozeki, *Int. J. Thermophys.*, 2001, 22, 1057-1071; and Yokozeki, *Applied Energy*, 2005, 80, 383-399. EOS models similar to these, and also as described in Tillner-Roth, *J. Phys. Chem. Ref. Data*, 1998, 27, 63-96, can therefore be used to calculate thermodynamic properties consistently, and to demonstrate that refrigerants and ionic liquids are useful in this invention as absorption cycle refrigerant pairs

For modeling of refrigerant/ionic liquid compositions, a generic Redlich-Kwong (RK) type of cubic equations of state (EOS), as discussed in Shiflett *et al*, *Ind. Eng. Chem. Res.*, 2004 (submitted), was employed:

$$P = \frac{RT}{\tilde{V} - b} - \frac{a(T)}{\tilde{V}(\tilde{V} + b)}$$

(1)

$$a(T) = 0.427480 \frac{R^2 T_c^2}{P_c} \alpha(T)$$

(2)

$$b = 0.08664 \frac{RT_c}{P_c}$$

(3)

The temperature-dependent part of the a parameter in the EOS for pure compounds is modeled by the following empirical form, as discussed in Yokozeki,

Int. J. Thermophys., 2001, 22, 1057-107; Yokozeki, *Applied Energy*, 2005, 80, 383-399; and Shiflett *et al*, *Ind. Eng. Chem. Res.*, 2004 (submitted).

$$\alpha(T) = \sum_{k=0}^{\leq 3} \beta_k \left(\frac{T_c}{T} - \frac{T}{T_c} \right)^k$$

(4)

- 5 The coefficients, β_k , are determined so as to reproduce the vapor pressure of each pure compound.

For absorbents, however, usually no vapor pressure data are available, or vapor pressures are practically zero at application temperatures, and furthermore,
10 no data for the critical parameters (T_c and P_c) exist. The critical parameters of absorbents can be estimated in various ways, as discussed in Reid *et al* in *The Properties of Gases & Liquids*, 4th edn. (McGraw-Hill, New York 1987). As discussed by Yokozeki, *Int. J. Thermophys.*, 2001, 22, 1057-1071, estimates of critical parameters for high boiling-point compounds are sufficient for correlating
15 solubility (PTx) data. On the other hand, the temperature-dependent part of the a parameter for absorbents is significant when the PTx data of refrigerant-absorbent mixtures are correlated, although the vapor pressure of absorbents is essentially zero at the temperature of interest. Here, $\alpha(T)$ for an absorbent is modeled by only two terms in eq 4, as applied for the case of refrigerant-lubricant oil
20 mixtures:

$$k_{ij} = \frac{l_{ij}l_{ji}(x_i + x_j)}{l_{ji}x_i + l_{ij}x_j} \quad \text{where } k_{ii} = 0$$

(5)

$$\alpha(T) = 1 + \beta_1 \left(\frac{T_c}{T} - \frac{T}{T_c} \right)$$

(6)

- 25 The coefficient β_1 in eq 6 will be treated as an adjustable fitting parameter.

Then, the a and b parameters for general N -component mixtures are modeled in terms of binary interaction parameters (as discussed in Yokozeki A

[*Applied Energy*, 2005, 80, 383-399]; and Shiflett MB and YOKOZEKI A, *supra*),

which may be regarded as a modified van der Waals-Berthelot mixing formula.

$$a(T) = \sum_{i,j=1}^N \sqrt{a_i a_j} (1 - f(T) k_{ij}) x_i x_j, \quad a_i = 0.427480 \frac{R^2 T_{ci}^2}{P_{ci}} \alpha_i(T) \quad (7)$$

$$f(T) = 1 + \tau_{ij} / T, \quad \text{where } \tau_{ij} = \tau_{ji}, \text{ and } \tau_{ii} = 0 \quad (8)$$

$$b = \frac{1}{2} \sum_{i,j=1}^N (b_i + b_j) (1 - m_{ij}) x_i x_j, \quad b_i = 0.08664 \frac{RT_{ci}}{P_{ci}}, \quad \text{where } m_{ij} = m_{ji}, m_{ii} = 0 \quad (9)$$

T_{ci} : critical temperature of i -th species.

10 P_{ci} : critical pressure of i -th species.

x_i : mole fraction of i -th species.

In the present model, there are four binary interaction parameters: l_{ij} , l_{ji} , m_{ij} , and τ_{ij} for each binary pair. It should be noted that when $l_{ij} = l_{ji}$ in eq 5 and $\tau_{ij} = 0$ in eq 8, eq 7 becomes the ordinary quadratic-mixing rule for the a parameter. The present EOS model has been successfully applied to mixtures that are highly non-symmetric with respect to polarity and size, such as various refrigerant/oil mixtures (see, for example, Yokozeki A, 2001, *supra*); and ammonia/butane mixtures (see, for example, Yokozeki A [*Proc. Int. Congress of Refrigeration*, Washington, D.C. 2003]; and EcoLibriumTM [2004, 3, 20-24]).

20

For phase equilibrium (solubility) calculations, the fugacity coefficient ϕ_i for each compound is needed and derived for the present mixing rule in this manner:

$$\ln \phi_i = -\ln \frac{PV}{RT} \left(1 - \frac{b}{V} \right) + \frac{b'_i}{V-b} - \frac{ab'_i}{bRT(V+b)} + \frac{a}{bRT} \left(\frac{a'_i}{a} - \frac{b'_i}{b} + 1 \right) \ln \frac{V}{V+b}, \quad (10)$$

25

where b'_i and a'_i are given by:

$$b'_i = \sum_{j=1}^N (b_i + b_j)(1 - m_{ij})x_j - b \quad (11)$$

$$a'_i = 2 \sum_{j=1}^N \sqrt{a_i a_j} x_j \left\{ 1 - k_{ij} - \frac{x_i x_j (l_{ji} - l_{ij})(1 + \tau_{ij}/T)}{(l_{ji} x_i + l_{ij} x_j)^2} \right\} \quad (12)$$

5

A thermodynamically derived function relevant to the present study is an enthalpy (H), which is given, in a general form:

$$H = \sum_{i=1}^N C_{pi}^0 x_i dT + \left(\frac{a}{b} - \frac{T}{b} \frac{da}{dT} \right) \ln \frac{V}{V+b} + RT \left(\frac{PV}{RT} - 1 \right) - \frac{RT^2}{V-b} \frac{db}{dT} + \frac{a}{b} \frac{db}{dT} \left[\frac{1}{V+b} - \frac{1}{b} \ln \left(1 + \frac{b}{V} \right) \right] + C, \quad (13)$$

10

where C is an arbitrary constant, which can be any value of choice but must be the same constant for any component mixtures within the system in question. The ideal-gas heat capacity for each compound C_{pi}^0 in eq 13 is modeled with a polynomial form:

$$C_p^0 = C_0 + C_1 T + C_2 T^2 + C_3 T^3. \quad (14)$$

15

Theoretical cycle performances for the system running the absorption refrigeration cycle shown in Figure 2 are modeled as follows. The overall energy balance gives:

20

$$Q_g + Q_e + W_p = Q_c + Q_a \quad (15)$$

From the material balance in the absorber or generator:

25

$$m_s x_a = (m_s - m_r) x_g; \quad (16)$$

this provides a mass-flow-rate ratio, f , as defined by:

$$f \equiv \frac{m_s}{m_r} = \frac{x_g}{x_g - x_a},$$

(17)

where x is a mass fraction of an absorbent in solution, the subscripts a and g stand for the absorber and generator solutions, and m_r and m_s are mass flow rates of gaseous refrigerant and absorber-exit solution (or solution pumping rate), respectively.

When a heat transfer efficiency of unity in the heat exchanger unit is assumed, the energy balance equation becomes:

$$Q_h \equiv (H_2 - H_3)(m_s - m_r) = (H_1 - H_4)m_s - W_p,$$

(18)

where H is an enthalpy, and the subscript numbers (1, 2, 3, and 4) correspond to the locations shown in Figure 2. From eq 18, the generator-inlet enthalpy, H_1 , can be obtained:

$$H_1 = H_4 + (H_2 - H_3)(1 - 1/f) + W_p / m_r.$$

(19)

From the energy balance around the generator, the generator heat input, Q_g , is given by,

$$Q_g = H_5 m_r + H_2 (m_s - m_r) - H_1 m_s.$$

(20)

By eliminating H_1 from this equation with eq 19, eq 20 can be written as:

$$Q_g / m_r = H_5 - H_4 f + H_3 (f - 1) - W_p / m_r.$$

(21)

Similarly, the heat rejection in the absorber, Q_a , is given by,

$$Q_a / m_r = H_3 (f - 1) + H_7 - H_4 f.$$

(22)

Condenser and evaporator heats per unit mass flow, respectively, are:

$$Q_c / m_r = H_5 - H_6$$

(23)

$$Q_e / \dot{m}_r = H_7 - H_6.$$

(24)

Then, the system performance is defined by a *heat ratio*, η , (output power divided by input power):

$$\eta = \frac{Q_e}{Q_g + W_p}.$$

However, the solution pumping power, W_p , is usually much smaller than Q_g , and it is customary to use a COP (coefficient of performance) defined as:

$$COP = \frac{Q_e}{Q_g}.$$

(25)

This can be expressed in terms of H and f :

$$COP = \frac{H_7 - H_6}{H_5 + H_3(f - 1) - H_4 f}.$$

(26)

Enthalpies at all locations and solubility in the absorber and generator units are calculated in a thermodynamically consistent way by use of the EOS model discussed above.

The pure component EOS constants for refrigerants have been taken from Yokozeki A (2001, *supra*), Yokozeki A (*Proc. Int. Congress of Refrigeration*, Washington, D.C. 2003), and EcoLibriumTM (2004, 3, 20-24), and are listed in Example 1, Table 2. For selected absorbents in this study, the critical parameters have been estimated from group contribution methods (as discussed in Reid RC, *et al.*, *supra*) and are also shown in Example 1, Table 2. The accuracy in critical parameters for these high boiling-point materials is of relatively less importance for correlating solubility data (see, for example, Yokozeki A, 2001, *supra*), but the β_1 parameter (in eq 6 as mentioned earlier) is important, and will be treated as an adjustable parameter in the analysis of binary solubility data.

In order to calculate thermal properties with EOS, the ideal gas heat capacity for each pure compound is needed as a function of temperature (see eq 14). The coefficients for eq 14 are listed in Example 1, Table 3, where those for absorbents have been all estimated from group contribution methods (as discussed in Reid RC, *et al, supra*). Next, the solubility (VLE: vapor-liquid equilibrium) data of fluorocarbon/ionic liquid binary mixtures is analyzed in order to determine the EOS parameters for mixtures. The four binary interaction parameters, l_{ij} , l_{ji} , m_{ij} , and τ_{ij} , and the absorbent β_1 parameter for each binary pair have been determined by non-linear least squares analyses with an object function of relative pressure differences. The results for selected binary mixtures are shown in Example 1, Table 4.

The performance of the absorption refrigeration cycle is based on a system running a simple ideal cycle as shown in Figure 2, and the present theoretical model. Here, the pumping power W_p is neglected, since it is usually insignificant with respect to other thermal powers. In addition, several assumptions are made:

- (1) There is no pressure drop in connecting lines.
- (2) The refrigerant expansion process from the condenser to the evaporator is isenthalpic, as usually done in vapor compression cycle calculations. The condition at Point 7 in Figure 2 (exit of evaporator) is a pure refrigerant dew point with $T = T_{eva}$.
- (3) The condition at Point 6 is a refrigerant bubble point and there is no subcooled liquid. The condition at Point 5 (inlet to condenser) is a superheated state of a pure refrigerant with $P = P_{con}$ and $T = T_g$.
- (4) Pressures in the condenser and the generator (P_{con} and P_g) are the same, and similarly evaporator and absorber pressures (P_{eva} and P_a) are equal.
- (5) The condition at Point 3 (solution inlet to the absorber) is a solution's bubble point specified with the absorber pressure (P_a) and a solution concentration of the generator (x_g).
- (6) Temperatures in the generator (T_g), absorber (T_a), condenser (T_{con}), and evaporator (T_{eva}) are specified as a given cycle condition.

(7) The refrigerant gas flow rate (m_r) is set to be $1 \text{ kg} \cdot \text{s}^{-1}$, without loss of generality, and the absorbent vapor is neglected.

The first step of cycle calculations is to obtain P_{eva} and P_{con} as saturated vapor pressures of a pure refrigerant at given temperatures, using for example a Bubble-Point P routine (as discussed in Ness, HCV *et al*, *supra*). Then, using a usual TP (Temperature-Pressure) Flash routine (as discussed in Ness, HCV *et al*, *supra*), absorbent compositions, x_g and x_a , in the generator and absorber units are calculated. This provides f (flow rate ratio) in eq 17. The thermodynamic properties at Point 3 are determined from the assumption (5), a Bubble-Point T routine (as discussed in Ness, HCV *et al*, *supra*). The enthalpy at Point 1 is obtained from eq 19. Enthalpies at all other points are easily calculated with known T , P , and compositions. Thus, the necessary quantities for the performance evaluation can be obtained using the listed equations. Cycle performances for the present binary systems are summarized in Example 1, Table 5 with selected thermodynamic quantities, where the specified temperatures for the cycle condition are: $T_g / T_{con} / T_a / T_{eva} = 100 / 40 / 30 / 10 \text{ } ^\circ\text{C}$, and $m_r = 1 \text{ kg} \cdot \text{s}^{-1}$.

Properties for the well-known refrigerant-absorbent pairs, $\text{NH}_3/\text{H}_2\text{O}$ and $\text{H}_2\text{O}/\text{LiBr}$, have also been calculated, and are shown in Example 1, Table 5, for comparison. In the case of $\text{NH}_3/\text{H}_2\text{O}$, the absorbent H_2O has a non-negligible vapor pressure at the generator exit, and in practical applications a rectifier (distillation) unit is required in order to separate the refrigerant from absorbent water. The effects of vapor pressure and extra power requirement due to the rectifier have been ignored; thus, the calculated COP is over-estimated for the present performance comparison. For $\text{H}_2\text{O}/\text{LiBr}$, empirical correlation diagrams for the thermodynamic properties (in the manner presented in the temperature-pressure-concentration diagram and enthalpy-temperature diagram in Stoecker *et al*, *Refrigeration and Air Conditioning* [McGraw-Hill, New York, 1982, 328-350]) were employed instead of an EOS model.

Cycle calculations for an absorption refrigeration cycle may be obtained in the manner set forth herein, but evaluation of the results is different from the case of an ordinary vapor compression cycle. In the latter case, a high

pressure/temperature refrigerant gas is produced by a vapor compressor, where the thermodynamic process is theoretically a single isentropic step: inlet and exit enthalpies of the compressor are sufficient for describing the compressor work. In the absorption cycle, however, the process generating the corresponding high
5 pressure/temperature gas involves enthalpies at several different locations as well as refrigerant-absorbent solubility differences at the absorber and generator units (related to the f value), as seen in eqs. 17, 21 and 22.

Performance of the condenser and evaporator is the same for both cycles at
10 given temperatures, and may be properly viewed in terms of the latent heat of vaporization (or condensation). In general, the refrigerating effect is the latent heat at the evaporator, which increases with an increase in the temperature difference between T_c and T_{eva} . Thus, at a given T_{eva} , the latent heat is larger for a refrigerant with a higher T_c . In addition, the *molar latent heat* (J/mol) is generally
15 not so much different among refrigerants at their boiling point (or far away from T_c), while the *specific latent heat* (J/kg) can be significantly different due to a large difference in molar masses. These factors affect the differences in the calculated refrigerating power Q_e among refrigerants as shown in Example 1, Table 5.

20

An absorbent is a compound that, desirably, has high solubility for a refrigerant and also a very high boiling point relative to the refrigerant. For example the systems HFC-32 + [bmim][PF₆], HFC-32 + [bmim][BF₄],
HFC-134a + [bmim][PF₆], HFC-152a + [bmim][PF₆] and
25 HFC-125 + [bmim][PF₆] have COP/f values of 0.385/7.35, 0.330/6.41, 0.254/10.66, 0.300/13.27, and 0.128/16.49, respectively (see Example 1, Table 5).

A schematic diagram for a system running a simple hybrid vapor compression-absorption cycle with a parallel configuration is shown in Figure 3.
30 The system is composed of a condenser unit and an evaporator unit with an expansion valve similar to an ordinary vapor compression cycle as shown in Figure 1, a compressor, an absorber-generator solution circuit, which has a vapor absorber, a gas generator, a heat exchanger, a pressure control (reducing) valve (A), a solution liquid pump, and isolation valves to direct the refrigerant flow path

(B-E). The advantage of such a combined cycle is that, when the heating or cooling capacity requirements are high, the vapor compressor can assist with the high capacity demand. The advantage of using an ionic liquid with high gas solubility for fluorocarbons allows the two cycles (absorption and vapor compression) to be directly linked because the same refrigerant gas can be used in both cycles, and this eliminates the need of a secondary heat exchanger and increases the overall cycle efficiency. In addition, as the ionic liquid has zero measurable vapor pressure, little or no cross-over of the ionic liquid from the generator into the refrigerant is expected. This reduces the need for secondary separation equipment, such as rectifiers, which can reduce the overall energy efficiency of the absorption cycle.

The parallel configuration can operate in three modes. Mode 1 operates like a conventional absorption cycle where isolation valves D and E are closed and isolation valves B and C are open, which reassembles the same flow path as shown in Figure 2, and has performance characteristics as shown in Example 1, Table 5. Mode 2 operates like a conventional vapor compression cycle where isolation valves D and E are open and isolation valves B and C are closed, which reassembles the same flow path as shown in Figure 1, and has performance characteristics as shown in Example 2, Table 6. Mode 3 combines the use of both the vapor compression and the absorption cycles where isolation valves B, C, D, and E are all open, as shown in Figure 3, and has performance characteristics as shown in Example 2, Table 6.

A schematic diagram for a system running a simple hybrid vapor compression-absorption cycle with a series configuration is shown in Figure 4. The system is composed of a condenser unit and an evaporator unit with an expansion valve (similar to an ordinary vapor compression cycle as shown in Figure 1), a compressor, an absorber-generator solution circuit, which has a vapor absorber, a gas generator, a heat exchanger, a pressure control (reducing) valve (A), a solution liquid pump, and isolation valves to direct the refrigerant flow path (B-E). As mentioned above, the advantage of such a combined cycle is that, when the heating or cooling capacity requirements are high, the vapor compressor can assist with the high capacity demand. Using an ionic liquid with high gas

solubility for fluorocarbons allows the two cycles (absorption and vapor compression) to be directly linked because the same refrigerant gas can be used in both cycles, which eliminates the need for a secondary heat exchanger and increases the overall cycle efficiency. In addition, as the ionic liquid has zero measurable vapor pressure, little or no cross-over of the ionic liquid from the generator into the refrigerant is expected. This reduces the need for secondary separation equipment, such as rectifiers, which also reduce the overall energy efficiency of the absorption cycle.

The series configuration can also operate in three modes. Mode 1 operates like a conventional absorption cycle where isolation valves D and E are closed and isolation valves B and C are open, which reassembles the same flow path as shown in Figure 2, and has performance characteristics as shown in Example 1, Table 5. Mode 2 operates like a conventional vapor compression cycle where isolation valve E is open and isolation valves B, C, and D are closed, which reassembles the same flow path as shown in shown in Figure 1, and has performance characteristics as shown in Example 2, Table 6. In this case the results are identical to those described in the previous case for parallel configuration Mode 2. Mode 3 combines the use of both the vapor compression and the absorption cycles where isolation valves C and D are open and isolation valves B and E are closed as shown in Figure 4, and has performance characteristics as shown in Example 2, Table 6.

For each refrigerant/ionic liquid pair tested, in both the parallel and series configurations, the results for the system running the hybrid vapor compression – absorption cycle (as shown in Example 2, Table 6) has a higher COP than the results for the system running the absorption cycle alone (as shown in Example 1, Table 5). The solubility curves for these refrigerant pairs are shown in Figures 5 to 10 at constant T of 10, 25, 50, and 75 °C. Indeed, the good solubility at the absorbent-rich side, which is indicative of concave-upward or near linear vapor pressures, corresponds to good performance.

Where an apparatus or process of this invention is stated or described as comprising, including, containing, having, being composed of or being constituted by certain features, components or steps, it is to be understood, unless the statement or description explicitly provides to the contrary, that one or more features, components or steps in addition to those explicitly stated or described may be present in the apparatus or process. In an alternative embodiment, however, the apparatus or process of this invention may be stated or described as consisting essentially of certain features, components or steps, in which embodiment features, components or steps that would materially alter the principle of operation or the distinguishing characteristics of the apparatus or process are not present therein. In a further alternative embodiment, the apparatus or process of this invention may be stated or described as consisting of certain features, components or steps, in which embodiment features, components or steps other than as named are not present therein.

15

In the various embodiments of this invention, where the indefinite article “a” or “an” is used with respect to a statement or description of the presence of a feature, component or step in an apparatus or process of this invention, it is to be understood, unless the statement or description explicitly provides to the contrary, that the use of such indefinite article does not limit the presence of the feature, component or step in the apparatus or process to one in number.

20

In alternative embodiments of this invention, a refrigerant may be any one or more of all of the members of the total group of refrigerants disclosed herein. In those embodiments, the refrigerant may also, however, be any one or more of those members of a subgroup of the total group of refrigerants disclosed herein, where the subgroup is formed by excluding any one or more other members from the total group. As a result, the refrigerant in those embodiments may not only be any one or more of the refrigerants in any subgroup of any size that may be selected from the total group of refrigerants in all the various different combinations of individual members of the total group, but the members in any subgroup may thus be used in the absence of one or more of the members of the total group that have been excluded to form the subgroup. The subgroup formed by excluding various members from the total group of refrigerants may,

30

moreover, be an individual member of the total group such that that refrigerant is used in the absence of all other members of the total group except the selected individual member.

5 Correspondingly, in further alternative embodiments of this invention, an ionic liquid may be any one or more of all of the members of the total group of ionic liquids disclosed herein. In those embodiments, the liquid may also, however, be any one or more of those members of a subgroup of the total group of ionic liquids disclosed herein, where the subgroup is formed by excluding any one
10 or more other members from the total group. As a result, the ionic liquid in those embodiments may not only be any one or more of the ionic liquids in any subgroup of any size that may be selected from the total group of ionic liquids in all the various different combinations of individual members of the total group, but the members in any subgroup may thus be used in the absence of one or more
15 of the members of the total group that have been excluded to form the subgroup. The subgroup formed by excluding various members from the total group of ionic liquids may, moreover, be an individual member of the total group such that that ionic liquid is used in the absence of all other members of the total group except the selected individual member.

20

As a result, in yet other alternative embodiments of this invention, refrigerant pairs may be formed from (i) any one or more of all of the members of the total group of refrigerants disclosed herein, selected as described above as a single member or any subgroup of any size taken from the total group of
25 refrigerants in all the various different combinations of individual members of that total group, together with (ii) any one or more of all of the members of the total group of ionic liquids disclosed herein, selected as described above as a single member or any subgroup of any size taken from the total group of ionic liquids in all the various different combinations of individual members of that total group.

30

The following examples are presented to illustrate the advantages of the present invention and to assist one of ordinary skill in making and using the same.

These examples are not intended in any way otherwise to limit the scope of the disclosure.

GENERAL METHODS AND MATERIALS

5 1-Butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆], C₈H₁₅N₂F₆P, 284 g mol⁻¹), 1-butyl-3-methylimidazolium tetrafluoroborate ([bmim][BF₄], C₈H₁₅N₂F₄B, 226 g mol⁻¹), 1,2-dimethyl-3-propylimidazolium tris(trifluoromethylsulfonyl)methide ([dmpim][tTFMSmethide], C₁₂H₁₅N₂F₉O₆S₃, 550 g mol⁻¹), 1,2-dimethyl-3-propylimidazolium
10 bis(trifluoromethylsulfonyl)imide ([dmpim][bTFMSimide], C₁₀H₁₅N₃F₆O₄S₂, 419 g mol⁻¹), 1-ethyl-3-methylimidazolium bis(pentafluoroethylsulfonyl)imide ([emim][bPFESimide], C₁₀H₁₁N₃F₁₀O₄S₂, 491.33 g mol⁻¹), and 1-propyl-3-methylpyridinium bis(trifluoromethylsulfonyl)imide ([pmpy][bTFMSimide], C₁₁H₁₄N₂F₆O₄S₂, 416.36 g mol⁻¹) were each obtained from Fluka Chemika (may
15 be obtained from Sigma-Aldrich, St. Louis, Missouri) with a purity of >96 to 97% each.

Difluoromethane (HFC-32, CH₂F₂, 52.02 g mol⁻¹), pentafluoroethane (HFC-125, C₂HF₅, 120.02 g mol⁻¹), 1,1,1,2-tetrafluoroethane (HFC-134a, C₂H₂F₄,
20 102.03 g mol⁻¹), 1,1,1-trifluoroethane (HFC-143a, C₂H₃F₃, 82.04 g mol⁻¹), and 1,1-difluoroethane (HFC-152a, C₂H₄F₂, 66.05 g mol⁻¹) were obtained from DuPont Fluorochemicals (Wilmington, Delaware), with a minimum purity of 99.99%. A molecular sieve trap was installed to remove trace amounts of water
25 from the gases and each of the ionic liquids tested were degassed prior to making solubility measurements.

In the following description, (A)-(D) provide syntheses for anions of ionic liquids that are useful for the invention, and (E)-(W) provide syntheses for ionic liquids useful for the invention.

30

Preparation of Anions Not Generally Available Commercially

(A) Synthesis of potassium 1,1,2,2-tetrafluoroethanesulfonate (TFES-K) ([HCF₂CF₂SO₃]⁻):

A 1-gallon Hastelloy® C276 reaction vessel was charged with a solution of potassium sulfite hydrate (176 g, 1.0 mol), potassium metabisulfite (610 g, 2.8 mol) and deionized water (2000 ml). The pH of this solution was 5.8. The vessel was cooled to 18 degrees C, evacuated to 0.10 MPa, and purged with nitrogen.

5 The evacuate/purge cycle was repeated two more times. To the vessel was then added tetrafluoroethylene (TFE, 66 g), and it was heated to 100 degrees C at which time the inside pressure was 1.14 MPa. The reaction temperature was increased to 125 degrees C and kept there for 3 h. As the TFE pressure decreased due to the reaction, more TFE was added in small aliquots (20-30 g each) to

10 maintain operating pressure roughly between 1.14 and 1.48 MPa. Once 500 g (5.0 mol) of TFE had been fed after the initial 66 g precharge, the vessel was vented and cooled to 25 degrees C. The pH of the clear light yellow reaction solution was 10-11. This solution was buffered to pH 7 through the addition of potassium metabisulfite (16 g).

15 The water was removed *in vacuo* on a rotary evaporator to produce a wet solid. The solid was then placed in a freeze dryer (Virtis Freezemobile 35xl; Gardiner, NY) for 72 hr to reduce the water content to approximately 1.5 wt % (1387 g crude material). The theoretical mass of total solids was 1351 g. The

20 mass balance was very close to ideal and the isolated solid had slightly higher mass due to moisture. This added freeze drying step had the advantage of producing a free-flowing white powder whereas treatment in a vacuum oven resulted in a soapy solid cake that was very difficult to remove and had to be chipped and broken out of the flask.

25 The crude TFES-K can be further purified and isolated by extraction with reagent grade acetone, filtration, and drying.

¹⁹F NMR (D₂O) δ, -122.0 (dt, $J_{FH} = 6$ Hz, $J_{FF} = 6$ Hz, 2F); -136.1 (dt, $J_{FH} = 53$ Hz, 2F).

30

¹H NMR (D₂O) δ, 6.4 (tt, $J_{FH} = 53$ Hz, $J_{FH} = 6$ Hz, 1H).

% Water by Karl-Fisher titration: 580 ppm.

Analytical calculation for C₂HO₃F₄SK: C, 10.9: H, 0.5: N, 0.0 Experimental results: C, 11.1: H, 0.7: N, 0.2.

Mp (DSC): 242 degrees C.

TGA (air): 10% wt. loss @ 367 degrees C, 50% wt. loss @ 375 degrees C.

TGA (N₂): 10% wt. loss @ 363 degrees C, 50% wt. loss @ 375 degrees C.

5

(B) Synthesis of potassium-1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate (TPES-K):

A 1-gallon Hastelloy® C276 reaction vessel was charged with a solution of potassium sulfite hydrate (88 g, 0.56 mol), potassium metabisulfite (340 g, 1.53 mol) and deionized water (2000 ml). The vessel was cooled to 7 degrees C, evacuated to 0.05 MPa, and purged with nitrogen. The evacuate/purge cycle was repeated two more times. To the vessel was then added perfluoro(ethylvinyl ether) (PEVE, 600 g, 2.78 mol), and it was heated to 125 degrees C at which time the inside pressure was 2.31 MPa. The reaction temperature was maintained at 125 degrees C for 10 hr. The pressure dropped to 0.26 MPa at which point the vessel was vented and cooled to 25 degrees C. The crude reaction product was a white crystalline precipitate with a colorless aqueous layer (pH = 7) above it.

The ¹⁹F NMR spectrum of the white solid showed pure desired product, while the spectrum of the aqueous layer showed a small but detectable amount of a fluorinated impurity. The desired isomer is less soluble in water so it precipitated in isomerically pure form.

The product slurry was suction filtered through a fritted glass funnel, and the wet cake was dried in a vacuum oven (60 degrees C, 0.01 MPa) for 48 hr. The product was obtained as off-white crystals (904 g, 97% yield).

¹⁹F NMR (D₂O) δ -86.5 (s, 3F); -89.2, -91.3 (subsplit ABq, *J*_{FF} = 147 Hz, 2F); -119.3, -121.2 (subsplit ABq, *J*_{FF} = 258 Hz, 2F); -144.3 (dm, *J*_{FH} = 53 Hz, 1F).
¹H NMR (D₂O) δ 6.7 (dm, *J*_{FH} = 53 Hz, 1H).

Mp (DSC) 263 degrees C.

Analytical calculation for C₄HO₄F₈SK: C, 14.3; H, 0.3 Experimental results: C, 14.1; H, 0.3.

TGA (air): 10% wt. loss @ 359 degrees C, 50% wt. loss @ 367 degrees C.

TGA (N₂): 10% wt. loss @ 362 degrees C, 50% wt. loss @ 374 degrees C.

(C) Synthesis of potassium-1,1,2-trifluoro-2-
 5 (trifluoromethoxy)ethanesulfonate (TTES-K)

A 1-gallon Hastelloy® C276 reaction vessel was charged with a solution of potassium sulfite hydrate (114 g, 0.72 mol), potassium metabisulfite (440 g, 1.98 mol) and deionized water (2000 ml). The pH of this solution was 5.8. The vessel was cooled to -35 degrees C, evacuated to 0.08 MPa, and purged with
 10 nitrogen. The evacuate/purge cycle was repeated two more times. To the vessel was then added perfluoro(methylvinyl ether) (PMVE, 600 g, 3.61 mol) and it was heated to 125 degrees C at which time the inside pressure was 3.29 MPa. The reaction temperature was maintained at 125 degrees C for 6 hr. The pressure dropped to 0.27 MPa at which point the vessel was vented and cooled to 25
 15 degrees C. Once cooled, a white crystalline precipitate of the desired product formed leaving a colorless clear aqueous solution above it (pH = 7).

The ¹⁹F NMR spectrum of the white solid showed pure desired product, while the spectrum of the aqueous layer showed a small but detectable amount of
 20 a fluorinated impurity.

The solution was suction filtered through a fritted glass funnel for 6 hr to remove most of the water. The wet cake was then dried in a vacuum oven at 0.01 MPa and 50 degrees C for 48 h. This gave 854 g (83% yield) of a white powder.
 25 The final product was isomerically pure (by ¹⁹F and ¹H NMR) since the undesired isomer remained in the water during filtration.

¹⁹F NMR (D₂O) δ -59.9 (d, J_{FH} = 4 Hz, 3F); -119.6, -120.2 (subsplit ABq, J = 260 Hz, 2F); -144.9 (dm, J_{FH} = 53 Hz, 1F).

30 ¹H NMR (D₂O) δ 6.6 (dm, J_{FH} = 53 Hz, 1H).

% Water by Karl-Fisher titration: 71 ppm.

Analytical calculation for C₃HF₆SO₄K: C, 12.6: H, 0.4: N, 0.0 Experimental results: C, 12.6: H, 0.0: N, 0.1.

Mp (DSC) 257 degrees C.

TGA (air): 10% wt. loss @ 343 degrees C, 50% wt. loss @ 358 degrees C.

TGA (N₂): 10% wt. loss @ 341 degrees C, 50% wt. loss @ 357 degrees C.

(D) Synthesis of sodium 1,1,2,3,3,3-hexafluoropropanesulfonate (HFPS-Na)

5 A 1-gallon Hastelloy® C reaction vessel was charged with a solution of anhydrous sodium sulfite (25 g, 0.20 mol), sodium bisulfite 73 g, (0.70 mol) and of deionized water (400 ml). The pH of this solution was 5.7. The vessel was cooled to 4 degrees C, evacuated to 0.08 MPa, and then charged with hexafluoropropene (HFP, 120 g, 0.8 mol, 0.43 MPa). The vessel was heated with
10 agitation to 120 degrees C and kept there for 3 hr. The pressure rose to a maximum of 1.83 MPa and then dropped down to 0.27 MPa within 30 minutes. At the end, the vessel was cooled and the remaining HFP was vented, and the reactor was purged with nitrogen. The final solution had a pH of 7.3.

15 The water was removed *in vacuo* on a rotary evaporator to produce a wet solid. The solid was then placed in a vacuum oven (0.02 MPa, 140 degrees C, 48 hr) to produce 219 g of white solid, which contained approximately 1 wt % water. The theoretical mass of total solids was 217 g.

20 The crude HFPS-Na can be further purified and isolated by extraction with reagent grade acetone, filtration, and drying.

¹⁹F NMR (D₂O) δ: -74.5 (m, 3F); -113.1, -120.4 (ABq, *J* = 264 Hz, 2F); -211.6 (dm, 1F).

25 ¹H NMR (D₂O) δ: 5.8 (dm, *J*_{FH} = 43 Hz, 1H).

Mp (DSC) 126 degrees C.

TGA (air): 10% wt. loss @ 326 degrees C, 50% wt. loss @ 446 degrees C.

TGA (N₂): 10% wt. loss @ 322 degrees C, 50% wt. loss @ 449 degrees C.

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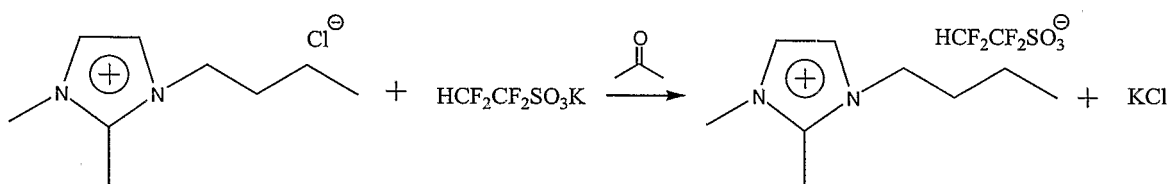
Preparation of Ionic LiquidsE) Synthesis of 1-butyl-2,3-dimethylimidazolium 1,1,2,2-tetrafluoroethanesulfonate

5 1-Butyl-2,3-dimethylimidazolium chloride (22.8 g, 0.121 moles) was mixed with reagent-grade acetone (250 ml) in a large round-bottomed flask and stirred vigorously. Potassium 1,1,2,2-tetrafluoroethanesulfonate (TFES-K, 26.6 g, 0.121 moles), was added to reagent grade acetone (250 ml) in a separate round-bottomed flask, and this solution was carefully added to the 1-butyl-2,3-

10 dimethylimidazolium chloride solution. The large flask was lowered into an oil bath and heated at 60 degrees C under reflux for 10 hours. The reaction mixture was then filtered using a large frit glass funnel to remove the white KCl precipitate formed, and the filtrate was placed on a rotary evaporator for 4 hours to remove the acetone.

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The reaction scheme is shown below:



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F) Synthesis of 1-butyl-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate

1-Butyl-3-methylimidazolium chloride (60.0 g) and high purity dry acetone (>99.5%, Aldrich, 300 ml) were combined in a 1l flask and warmed to reflux with magnetic stirring until the solid completely dissolved. At room

25 temperature in a separate 1l flask, potassium-1,1,2,2-tetrafluoroethanesulfonate (TFES-K, 75.6 g) was dissolved in high purity dry acetone (500 ml). These two solutions were combined at room temperature and allowed to stir magnetically for 2 hr under positive nitrogen pressure. The stirring was stopped and the KCl precipitate was allowed to settle, then removed by suction filtration through a

30 fritted glass funnel with a celite pad. The acetone was removed *in vacuo* to give a

yellow oil. The oil was further purified by diluting with high purity acetone (100 ml) and stirring with decolorizing carbon (5 g). The mixture was again suction filtered and the acetone removed *in vacuo* to give a colorless oil. This was further dried at 4 Pa and 25 degrees C for 6 hr to provide 83.6 g of product.

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^{19}F NMR (DMSO- d_6) δ -124.7 (dt, $J = 6$ Hz, $J = 8$ Hz, 2F); -136.8 (dt, $J = 53$ Hz, 2F).

^1H NMR (DMSO- d_6) δ 0.9 (t, $J = 7.4$ Hz, 3H); 1.3 (m, 2H); 1.8 (m, 2H); 3.9 (s, 3H); 4.2 (t, $J = 7$ Hz, 2H); 6.3 (dt, $J = 53$ Hz, $J = 6$ Hz, 1H); 7.4 (s, 1H); 7.5 (s, 1H); 8.7 (s, 1H).

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% Water by Karl-Fisher titration: 0.14 %.

Analytical calculation for $\text{C}_9\text{H}_{12}\text{F}_6\text{N}_2\text{O}_3\text{S}$: C, 37.6: H, 4.7: N, 8.8. Experimental Results: C, 37.6: H, 4.6: N, 8.7.

15 TGA (air): 10% wt. loss @ 380 degrees C, 50% wt. loss @ 420 degrees C.
TGA (N_2): 10% wt. loss @ 375 degrees C, 50% wt. loss @ 422 degrees C.

G) Synthesis of 1-ethyl-3-methylimidazolium 1,1,2,2-tetrafluoroethane sulfonate

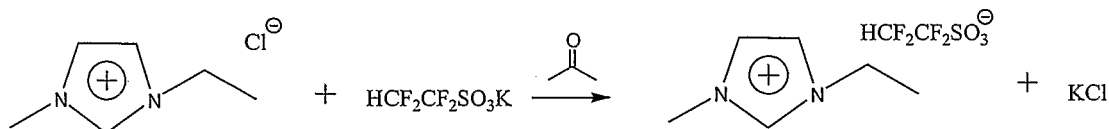
20 To a 500 ml round bottom flask was added 1-ethyl-3-methylimidazolium chloride (Emim-Cl, 98%, 61.0 g) and reagent grade acetone (500 ml). The mixture was gently warmed (50 degrees C) until almost all of the Emim-Cl dissolved. To a separate 500 ml flask was added potassium 1,1,2,2-tetrafluoroethanesulfonate (TFES-K, 90.2 g) along with reagent grade acetone
25 (350 ml). This second mixture was stirred magnetically at 24 degrees C until all of the TFES-K dissolved.

These solutions were combined in a 1 l flask producing a milky white suspension. The mixture was stirred at 24 degrees C for 24 hrs. The KCl
30 precipitate was then allowed to settle leaving a clear green solution above it.

The reaction mixture was filtered once through a celite/acetone pad and again through a fritted glass funnel to remove the KCl. The acetone was removed

in vacuo first on a rotovap and then on a high vacuum line (4 Pa, 25 degrees C) for 2 hr. The product was a viscous light yellow oil (76.0 g, 64% yield).

5 The reaction scheme is shown below:



^{19}F NMR (DMSO- d_6) δ -124.7 (dt, $J_{\text{FH}} = 6$ Hz, $J_{\text{FF}} = 6$ Hz, 2F); -138.4 (dt, $J_{\text{FH}} = 53$ Hz, 2F).

10 ^1H NMR (DMSO- d_6) δ 1.3 (t, $J = 7.3$ Hz, 3H); 3.7 (s, 3H); 4.0 (q, $J = 7.3$ Hz, 2H);

6.1 (tt, $J_{\text{FH}} = 53$ Hz, $J_{\text{FH}} = 6$ Hz, 1H); 7.2 (s, 1H); 7.3 (s, 1H); 8.5 (s, 1H).

% Water by Karl-Fisher titration: 0.18 %.

Analytical calculation for $\text{C}_8\text{H}_{12}\text{N}_2\text{O}_3\text{F}_4\text{S}$: C, 32.9; H, 4.1; N, 9.6 Found: C,

15 33.3; H, 3.7; N, 9.6.

Mp 45-46 degrees C.

TGA (air): 10% wt. loss @ 379 degrees C, 50% wt. loss @ 420 degrees C.

TGA (N_2): 10% wt. loss @ 378 degrees C, 50% wt. loss @ 418 degrees C.

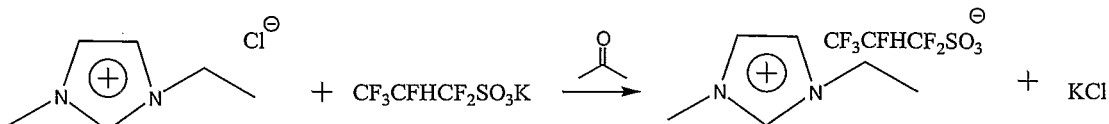
20 H) Synthesis of 1-ethyl-3-methylimidazolium 1,1,2,3,3,3-hexafluoropropanesulfonate

To a 1l round bottom flask was added 1-ethyl-3-methylimidazolium chloride (Emim-Cl, 98%, 50.5 g) and reagent grade acetone (400 ml). The mixture was gently warmed (50 degrees C) until almost all of the Emim-Cl dissolved. To a separate 500 ml flask was added potassium 1,1,2,3,3,3-hexafluoropropanesulfonate (HFPS-K, 92.2 g) along with reagent grade acetone (300 ml). This second mixture was stirred magnetically at room temperature until all of the HFPS-K dissolved.

30 These solutions were combined and stirred under positive N_2 pressure at 26 degrees C for 12 hr producing a milky white suspension. The KCl precipitate was allowed to settle overnight leaving a clear yellow solution above it.

The reaction mixture was filtered once through a celite/acetone pad and again through a fritted glass funnel. The acetone was removed *in vacuo* first on a rotovap and then on a high vacuum line (4 Pa, 25 degrees C) for 2 hr. The product was a viscous light yellow oil (103.8 g, 89% yield).

The reaction scheme is shown below:



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^{19}F NMR (DMSO- d_6) δ -73.8 (s, 3F); -114.5, -121.0 (ABq, $J = 258$ Hz, 2F); -210.6 (m, 1F, $J_{\text{HF}} = 41.5$ Hz).

^1H NMR (DMSO- d_6) δ 1.4 (t, $J = 7.3$ Hz, 3H); 3.9 (s, 3H); 4.2 (q, $J = 7.3$ Hz, 2H);

15 5.8 (m, $J_{\text{HF}} = 41.5$ Hz, 1H); 7.7 (s, 1H); 7.8 (s, 1H); 9.1 (s, 1H).

% Water by Karl-Fisher titration: 0.12 %.

Analytical calculation for $\text{C}_9\text{H}_{12}\text{N}_2\text{O}_3\text{F}_6\text{S}$: C, 31.5; H, 3.5; N, 8.2. Experimental Results: C, 30.9; H, 3.3; N, 7.8.

TGA (air): 10% wt. loss @ 342 degrees C, 50% wt. loss @ 373 degrees C.

20 TGA (N_2): 10% wt. loss @ 341 degrees C, 50% wt. loss @ 374 degrees C.

I) Synthesis of 1-hexyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate

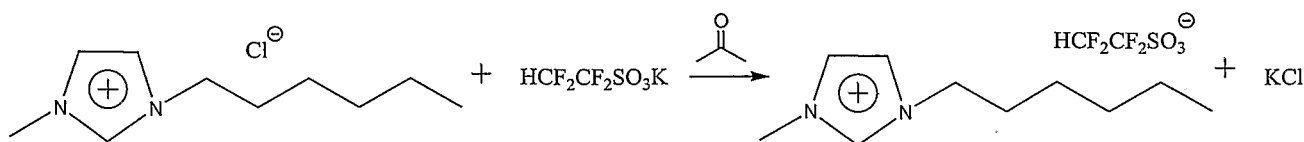
25 1-Hexyl-3-methylimidazolium chloride (10 g, 0.0493 moles) was mixed with reagent-grade acetone (100 ml) in a large round-bottomed flask and stirred vigorously under a nitrogen blanket. Potassium 1,1,2,2-tetrafluoroethane sulfonate (TFES-K, 10 g, 0.0455 moles) was added to reagent grade acetone (100 ml) in a separate round-bottomed flask, and this solution was carefully added to the 1-hexyl-3-methylimidazolium chloride/acetone mixture. The mixture was left to stir overnight. The reaction mixture was then filtered using a large frit glass

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funnel to remove the white KCl precipitate formed, and the filtrate was placed on a rotary evaporator for 4 hours to remove the acetone.

The reaction scheme is shown below:

5



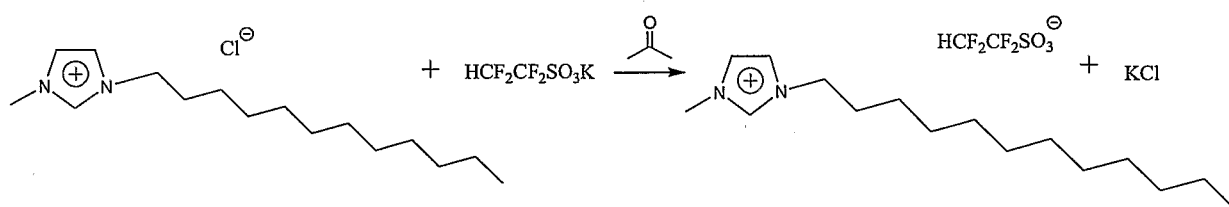
J) Synthesis of 1-dodecyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate

10 1-Dodecyl-3-methylimidazolium chloride (34.16 g, 0.119 moles) was partially dissolved in reagent-grade acetone (400 ml) in a large round-bottomed flask and stirred vigorously. Potassium 1,1,2,2-tetrafluoroethanesulfonate (TFES-K, 26.24 g, 0.119 moles) was added to reagent grade acetone (400 ml) in a separate round-bottomed flask, and this solution was carefully added to the 1-

15 dodecyl-3-methylimidazolium chloride solution. The reaction mixture was heated at 60 degrees C under reflux for approximately 16 hours. The reaction mixture was then filtered using a large frit glass funnel to remove the white KCl precipitate formed, and the filtrate was placed on a rotary evaporator for 4 hours to remove the acetone.

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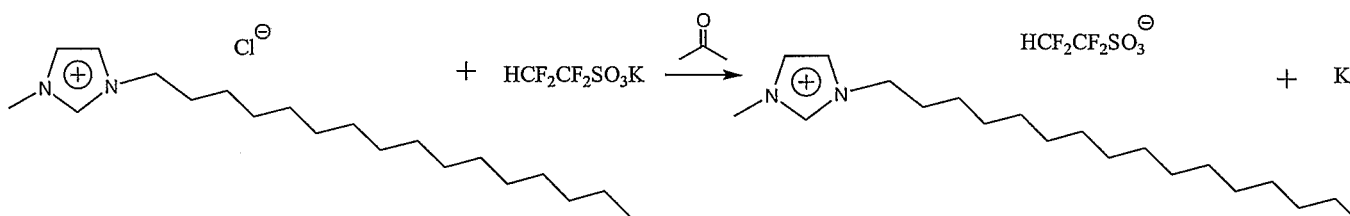
The reaction scheme is shown below:



25 K) Synthesis of 1-hexadecyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate

1-Hexadecyl-3-methylimidazolium chloride (17.0 g, 0.0496 moles) was partially dissolved in reagent-grade acetone (100 ml) in a large round-bottomed flask and stirred vigorously. Potassium 1,1,2,2-tetrafluoroethanesulfonate (TFES-K, 10.9 g, 0.0495 moles) was added to reagent grade acetone (100 ml) in a separate round-bottomed flask, and this solution was carefully added to the 1-hexadecyl-3-methylimidazolium chloride solution. The reaction mixture was heated at 60 degrees C under reflux for approximately 16 hours. The reaction mixture was then filtered using a large frit glass funnel to remove the white KCl precipitate formed, and the filtrate was placed on a rotary evaporator for 4 hours to remove the acetone.

The reaction scheme is shown below:



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20 L) Synthesis of 1-octadecyl-3-methylimidazolium 1,1,2,2-tetrafluoroethanesulfonate

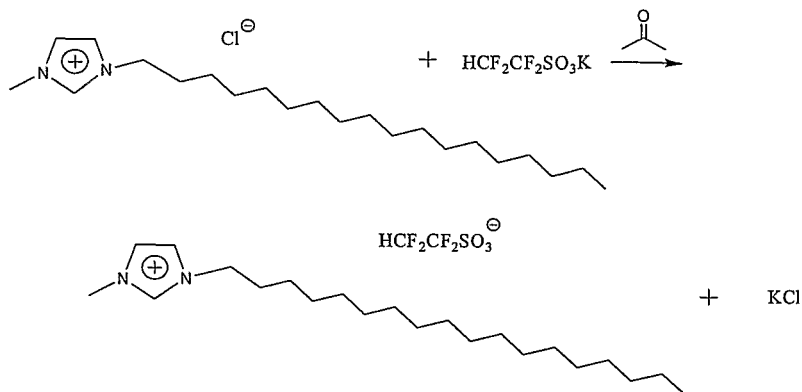
1-Octadecyl-3-methylimidazolium chloride (17.0 g, 0.0458 moles) was partially dissolved in reagent-grade acetone (200 ml) in a large round-bottomed flask and stirred vigorously. Potassium 1,1,2,2-tetrafluoroethanesulfonate (TFES-K, 10.1 g, 0.0459 moles), was added to reagent grade acetone (200 ml) in a separate round-bottomed flask, and this solution was carefully added to the 1-octadecyl-3-methylimidazolium chloride solution. The reaction mixture was heated at 60 degrees C under reflux for approximately 16 hours. The reaction mixture was then filtered using a large frit glass funnel to remove the white KCl

precipitate formed, and the filtrate was placed on a rotary evaporator for 4 hours to remove the acetone.

The reaction scheme is shown below:

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M) Synthesis of 1-propyl-3-(1,1,2,2-TFES) imidazolium 1,1,2,2-tetrafluoroethanesulfonate

Imidazole (19.2 g) was added to of tetrahydrofuran (80 mls). A glass shaker tube reaction vessel was filled with the THF-containing imidazole solution. The vessel was cooled to 18°C, evacuated to 0.08 MPa, and purged with nitrogen. The evacuate/purge cycle was repeated two more times. Tetrafluoroethylene (TFE, 5 g) was then added to the vessel, and it was heated to 100 degrees C, at which time the inside pressure was about 0.72 MPa. As the TFE pressure decreased due to the reaction, more TFE was added in small aliquots (5 g each) to maintain operating pressure roughly between 0.34 MPa and 0.86 MPa. Once 40 g of TFE had been fed, the vessel was vented and cooled to 25 degrees C. The THF was then removed under vacuum and the product was vacuum distilled at 40 degrees C to yield pure product as shown by ¹H and ¹⁹F NMR (yield 44 g). Iodopropane (16.99 g) was mixed with

1-(1,1,2,2-tetrafluoroethyl)imidazole (16.8 g) in dry acetonitrile (100 ml), and the mixture was refluxed for 3 days. The solvent was removed *in vacuo*, yielding a yellow waxy solid (yield 29 g). The product, 1-propyl-3-(1,1,2,2-tetrafluoroethyl)imidazolium iodide was confirmed by ¹H NMR (in CD₃CN) [0.96 (t, 3H); 1.99 (m, 2H); 4.27 (t, 2H); 6.75 (t, 1H); 7.72 (d, 2H); 9.95 (s, 1H)].

Iodide (24 g) was then added to 60 ml of dry acetone, followed by 15.4 g of potassium 1,1,2,2-tetrafluoroethanesulfonate in 75 ml of dry acetone. The mixture was heated at 60 degrees C overnight and a dense white precipitate was formed (potassium iodide). The mixture was cooled, filtered, and the solvent from the filtrate was removed using a rotary evaporator. Some further potassium iodide was removed under filtration. The product was further purified by adding 50 g of acetone, 1 g of charcoal, 1 g of celite and 1 g of silica gel. The mixture was stirred for 2 hours, filtered and the solvent removed. This yielded 15 g of a liquid, shown by NMR to be the desired product.

N) Synthesis of 1-butyl-3-methylimidazolium 1,1,2,3,3,3-hexafluoropropanesulfonate (Bmim-HFPS)

1-Butyl-3-methylimidazolium chloride (Bmim-Cl, 50.0 g) and high purity dry acetone (>99.5%, 500 ml) were combined in a 1l flask and warmed to reflux with magnetic stirring until the solid all dissolved. At room temperature in a separate 1l flask, potassium-1,1,2,3,3,3-hexafluoropropanesulfonate (HFPS-K) was dissolved in high purity dry acetone (550 ml). These two solutions were combined at room temperature and allowed to stir magnetically for 12 hr under positive nitrogen pressure. The stirring was stopped, and the KCl precipitate was allowed to settle. This solid was removed by suction filtration through a fritted glass funnel with a celite pad. The acetone was removed *in vacuo* to give a yellow oil. The oil was further purified by diluting with high purity acetone (100 ml) and stirring with decolorizing carbon (5 g). The mixture was suction filtered and the acetone removed *in vacuo* to give a colorless oil. This was further dried at 4 Pa and 25 degrees C for 2 hr to provide 68.6 g of product.

^{19}F NMR (DMSO- d_6) δ -73.8 (s, 3F); -114.5, -121.0 (ABq, J = 258 Hz, 2F); -210.6 (m, J = 42 Hz, 1F).

^1H NMR (DMSO- d_6) δ 0.9 (t, J = 7.4 Hz, 3H); 1.3 (m, 2H); 1.8 (m, 2H); 3.9 (s, 3H); 4.2 (t, J = 7 Hz, 2H); 5.8 (dm, J = 42 Hz, 1H); 7.7 (s, 1H); 7.8 (s, 1H); 9.1 (s, 1H).

% Water by Karl-Fisher titration: 0.12 %.

Analytical calculation for $C_9H_{12}F_6N_2O_3S$: C, 35.7: H, 4.4: N, 7.6. Experimental Results: C, 34.7: H, 3.8: N, 7.2.

TGA (air): 10% wt. loss @ 340 degrees C, 50% wt. loss @ 367 degrees C.

TGA (N_2): 10% wt. loss @ 335 degrees C, 50% wt. loss @ 361 degrees C.

5 Extractable chloride by ion chromatography: 27 ppm.

O) Synthesis of 1-butyl-3-methylimidazolium 1,1,2-trifluoro-2-(trifluoromethoxy)ethanesulfonate (Bmim-TTES)

1-Butyl-3-methylimidazolium chloride (Bmim-Cl, 10.0 g) and deionized
10 water (15 ml) were combined at room temperature in a 200 ml flask. At room temperature in a separate 200 ml flask, potassium 1,1,2-trifluoro-2-(trifluoromethoxy)ethanesulfonate (TTES-K, 16.4 g) was dissolved in deionized water (90 ml). These two solutions were combined at room temperature and allowed to stir magnetically for 30 min. under positive nitrogen pressure to give a
15 biphasic mixture with the desired ionic liquid as the bottom phase. The layers were separated, and the aqueous phase was extracted with 2 x 50 ml portions of methylene chloride. The combined organic layers were dried over magnesium sulfate and concentrated *in vacuo*. The colorless oil product was dried at for 4 hr at 5 Pa and 25 degrees C to afford 15.0 g of product.

20

^{19}F NMR (DMSO- d_6) δ -56.8 (d, $J_{FH} = 4$ Hz, 3F); -119.5, -119.9 (subsplit ABq, $J = 260$ Hz, 2F); -142.2 (dm, $J_{FH} = 53$ Hz, 1F).

1H NMR (DMSO- d_6) δ 0.9 (t, $J = 7.4$ Hz, 3H); 1.3 (m, 2H); 1.8 (m, 2H); 3.9 (s, 3H); 4.2 (t, $J = 7.0$ Hz, 2H); 6.5 (dt, $J = 53$ Hz, $J = 7$ Hz, 1H); 7.7 (s, 1H); 7.8 (s,
25 1H); 9.1 (s, 1H).

% Water by Karl-Fisher titration: 613 ppm.

Analytical calculation for $C_{11}H_{16}F_6N_2O_4S$: C, 34.2: H, 4.2: N, 7.3. Experimental Results: C, 34.0: H, 4.0: N, 7.1.

TGA (air): 10% wt. loss @ 328 degrees C, 50% wt. loss @ 354 degrees C.

30 TGA (N_2): 10% wt. loss @ 324 degrees C, 50% wt. loss @ 351 degrees C.

Extractable chloride by ion chromatography: < 2 ppm.

P) Synthesis of 1-butyl-3-methylimidazolium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate (Bmim-TPES)

1-Butyl-3-methylimidazolium chloride (Bmim-Cl, 7.8 g) and dry acetone (150 ml) were combined at room temperature in a 500 ml flask. At room temperature in a separate 200 ml flask, potassium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate (TPES-K, 15.0 g) was dissolved in dry acetone (300 ml). These two solutions were combined and allowed to stir magnetically for 12 hr under positive nitrogen pressure. The KCl precipitate was then allowed to settle leaving a colorless solution above it. The reaction mixture was filtered once through a celite/acetone pad and again through a fritted glass funnel to remove the KCl. The acetone was removed *in vacuo* first on a rotovap and then on a high vacuum line (4 Pa, 25 degrees C) for 2 hr. Residual KCl was still precipitating out of the solution, so methylene chloride (50 ml) was added to the crude product, which was then washed with deionized water (2 x 50 ml). The solution was dried over magnesium sulfate, and the solvent was removed *in vacuo* to give the product as a viscous light yellow oil (12.0 g, 62% yield).

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^{19}F NMR (CD_3CN) δ -85.8 (s, 3F); -87.9, -90.1 (subsplit ABq, $J_{\text{FF}} = 147$ Hz, 2F); -120.6, -122.4 (subsplit ABq, $J_{\text{FF}} = 258$ Hz, 2F); -142.2 (dm, $J_{\text{FH}} = 53$ Hz, 1F).

^1H NMR (CD_3CN) δ 1.0 (t, $J = 7.4$ Hz, 3H); 1.4 (m, 2H); 1.8 (m, 2H); 3.9 (s, 3H);

4.2 (t, $J = 7.0$ Hz, 2H); 6.5 (dm, $J = 53$ Hz, 1H); 7.4 (s, 1H); 7.5 (s, 1H); 8.6 (s, 1H).

% Water by Karl-Fisher titration: 0.461.

Analytical calculation for $\text{C}_{12}\text{H}_{16}\text{F}_8\text{N}_2\text{O}_4\text{S}$: C, 33.0; H, 3.7. Experimental Results: C, 32.0; H, 3.6.

TGA (air): 10% wt. loss @ 334 degrees C, 50% wt. loss @ 353 degrees C.

TGA (N_2): 10% wt. loss @ 330 degrees C, 50% wt. loss @ 365 degrees C.

Q) Synthesis of tetradecyl(tri-*n*-butyl)phosphonium 1,1,2,3,3,3-hexafluoropropanesulfonate ([4.4.4.14]P-HFPS)

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To a 4l round bottomed flask was added the ionic liquid tetradecyl(tri-*n*-butyl)phosphonium chloride (Cyphos® IL 167, 345 g) and deionized water (1000 ml). The mixture was magnetically stirred until it was one phase. In a separate

2l flask, potassium 1,1,2,3,3,3-hexafluoropropanesulfonate (HFPS-K, 214.2 g) was dissolved in deionized water (1100 ml). These solutions were combined and stirred under positive N₂ pressure at 26 degrees C for 1 hr producing a milky white oil. The oil slowly solidified (439 g) and was removed by suction filtration and then dissolved in chloroform (300 ml). The remaining aqueous layer (pH = 2) was extracted once with chloroform (100 ml). The chloroform layers were combined and washed with an aqueous sodium carbonate solution (50 ml) to remove any acidic impurity. They were then dried over magnesium sulfate, suction filtered, and reduced *in vacuo* first on a rotovap and then on a high vacuum line (4 Pa, 100 degrees C) for 16 hr to yield the final product as a white solid (380 g, 76% yield).

¹⁹F NMR (DMSO-d₆) δ -73.7 (s, 3F); -114.6, -120.9 (ABq, *J* = 258 Hz, 2F); -210.5 (m, *J*_{HF} = 41.5 Hz, 1F).

¹H NMR (DMSO-d₆) δ 0.8 (t, *J* = 7.0 Hz, 3H); 0.9 (t, *J* = 7.0 Hz, 9H); 1.3 (br s, 20H); 1.4 (m, 16H); 2.2 (m, 8H); 5.9 (m, *J*_{HF} = 42 Hz, 1H).

% Water by Karl-Fisher titration: 895 ppm.

Analytical calculation for C₂₉H₅₇F₆O₃PS: C, 55.2; H, 9.1; N, 0.0.

Experimental Results: C, 55.1; H, 8.8; N, 0.0.

TGA (air): 10% wt. loss @ 373 degrees C, 50% wt. loss @ 421 degrees C.

TGA (N₂): 10% wt. loss @ 383 degrees C, 50% wt. loss @ 436 degrees C.

R) Synthesis of tetradecyl(tri-*n*-hexyl)phosphonium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate ([6.6.6.14]P-TPES)

To a 500 ml round bottomed flask was added acetone (Spectroscopic grade, 50 ml) and ionic liquid tetradecyl(tri-*n*-hexyl)phosphonium chloride (Cyphos® IL 101, 33.7 g). The mixture was magnetically stirred until it was one phase. In a separate 1l flask, potassium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate (TPES-K, 21.6 g) was dissolved in acetone (400 ml). These solutions were combined and stirred under positive N₂ pressure at 26 degrees C for 12 hr producing a white precipitate of KCl. The precipitate was removed by suction filtration, and the acetone was removed *in vacuo* on a rotovap to produce the crude product as a cloudy oil (48 g). Chloroform (100 ml) was

added, and the solution was washed once with deionized water (50 ml). It was then dried over magnesium sulfate and reduced *in vacuo* first on a rotovap and then on a high vacuum line (8 Pa, 24 degrees C) for 8 hr to yield the final product as a slightly yellow oil (28 g, 56% yield).

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^{19}F NMR (DMSO- d_6) δ -86.1 (s, 3F); -88.4, -90.3 (subsplit ABq, $J_{\text{FF}} = 147$ Hz, 2F); -121.4, -122.4 (subsplit ABq, $J_{\text{FF}} = 258$ Hz, 2F); -143.0 (dm, $J_{\text{FH}} = 53$ Hz, 1F).

^1H NMR (DMSO- d_6) δ 0.9 (m, 12H); 1.2 (m, 16H); 1.3 (m, 16H); 1.4 (m, 8H);

10 1.5 (m, 8H); 2.2 (m, 8H); 6.3 (dm, $J_{\text{FH}} = 54$ Hz, 1H).

% Water by Karl-Fisher titration: 0.11.

Analytical calculation for C₃₆H₆₉F₈O₄PS: C, 55.4: H, 8.9: N, 0.0.

Experimental Results: C, 55.2: H, 8.2: N, 0.1.

TGA (air): 10% wt. loss @ 311 degrees C, 50% wt. loss @ 339 degrees C.

15 TGA (N₂): 10% wt. loss @ 315 degrees C, 50% wt. loss @ 343 degrees C.

S) Synthesis of tetradecyl(tri-*n*-hexyl)phosphonium 1,1,2-trifluoro-2-(trifluoromethoxy)ethanesulfonate ([6.6.6.14]P-TTES)

To a 100 ml round bottomed flask was added acetone (Spectroscopic
20 grade, 50 ml) and ionic liquid tetradecyl(tri-*n*-hexyl)phosphonium chloride (Cyphos® IL 101, 20.2 g). The mixture was magnetically stirred until it was one phase. In a separate 100 ml flask, potassium 1,1,2-trifluoro-2-(trifluoromethoxy)ethanesulfonate (TTES-K, 11.2 g) was dissolved in acetone (100 ml). These solutions were combined and stirred under positive N₂ pressure at
25 26 degrees C for 12 hr producing a white precipitate of KCl.

The precipitate was removed by suction filtration, and the acetone was removed *in vacuo* on a rotovap to produce the crude product as a cloudy oil. The product was diluted with ethyl ether (100 ml) and then washed once with
30 deionized water (50 ml), twice with an aqueous sodium carbonate solution (50 ml) to remove any acidic impurity, and twice more with deionized water (50 ml). The ether solution was then dried over magnesium sulfate and reduced *in vacuo* first

on a rotovap and then on a high vacuum line (4 Pa, 24 degrees C) for 8 hr to yield the final product as an oil (19.0 g, 69% yield).

¹⁹F NMR (CD₂Cl₂) δ -60.2 (d, *J*_{FH} = 4 Hz, 3F); -120.8, -125.1 (subsplit ABq, *J* = 260 Hz, 2F); -143.7 (dm, *J*_{FH} = 53 Hz, 1F).

¹H NMR (CD₂Cl₂) δ 0.9 (m, 12H); 1.2 (m, 16H); 1.3 (m, 16H); 1.4 (m, 8H); 1.5 (m, 8H); 2.2 (m, 8H); 6.3 (dm, *J*_{FH} = 54 Hz, 1H).

% Water by Karl-Fisher titration: 412 ppm.

Analytical calculation for C₃₅H₆₉F₆O₄PS: C, 57.5; H, 9.5; N, 0.0.

Experimental results: C, 57.8; H, 9.3; N, 0.0.

TGA (air): 10% wt. loss @ 331 degrees C, 50% wt. loss @ 359 degrees C.

TGA (N₂): 10% wt. loss @ 328 degrees C, 50% wt. loss @ 360 degrees C.

15

T) Synthesis of 1-ethyl-3-methylimidazolium 1,1,2,2-tetrafluoro-2-(pentafluoroethoxy)sulfonate (Emim-TPENTAS)

To a 500 ml round bottomed flask was added 1-ethyl-3-methylimidazolium chloride (Emim-Cl, 98%, 18.0 g) and reagent grade acetone (150 ml). The mixture was gently warmed (50 degrees C) until all of the Emim-Cl dissolved. In a separate 500 ml flask, potassium 1,1,2,2-tetrafluoro-2-(pentafluoroethoxy)sulfonate (TPENTAS-K, 43.7 g) was dissolved in reagent grade acetone (450 ml).

These solutions were combined in a 1 l flask producing a white precipitate (KCl). The mixture was stirred at 24 degrees C for 8 hr. The KCl precipitate was then allowed to settle leaving a clear yellow solution above it. The KCl was removed by filtration through a celite/acetone pad. The acetone was removed *in vacuo* to give a yellow oil, which was then diluted with chloroform (100 ml). The chloroform was washed three times with deionized water (50 ml), dried over magnesium sulfate, filtered, and reduced *in vacuo* first on a rotovap and then on a

high vacuum line (4 Pa, 25 degrees C) for 8 hr. The product was a light yellow oil (22.5 g).

^{19}F NMR (DMSO- d_6) δ -82.9 (m, 2F); -87.3 (s, 3F); -89.0 (m, 2F); -118.9 (s, 2F).

5 ^1H NMR (DMSO- d_6) δ 1.5 (t, $J = 7.3$ Hz, 3H); 3.9 (s, 3H); 4.2 (q, $J = 7.3$ Hz, 2H);
7.7 (s, 1H); 7.8 (s, 1H); 9.1 (s, 1H).

% Water by Karl-Fisher titration: 0.17 %.

Analytical calculation for $\text{C}_{10}\text{H}_{11}\text{N}_2\text{O}_4\text{F}_9\text{S}$: C, 28.2: H, 2.6: N, 6.6

10 Experimental results: C, 28.1: H, 2.9: N, 6.6.

TGA (air): 10% wt. loss @ 351 degrees C, 50% wt. loss @ 401 degrees C.

TGA (N_2): 10% wt. loss @ 349 degrees C, 50% wt. loss @ 406 degrees C.

15

U) Synthesis of tetrabutylphosphonium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate (TBP-TPES)

To a 200 ml round bottomed flask was added deionized water (100 ml)
20 and tetra-*n*-butylphosphonium bromide (Cytec Canada Inc., 20.2 g). The mixture was magnetically stirred until the solid all dissolved. In a separate 300 ml flask, potassium 1,1,2-trifluoro-2-(perfluoroethoxy)ethanesulfonate (TPES-K, 20.0 g) was dissolved in deionized water (400 ml) heated to 70 degrees C. These solutions were combined and stirred under positive N_2 pressure at 26 degrees C for 2 hr
25 producing a lower oily layer. The product oil layer was separated and diluted with chloroform (30 ml), then washed once with an aqueous sodium carbonate solution (4 ml) to remove any acidic impurity, and three times with deionized water (20 ml). It was then dried over magnesium sulfate and reduced *in vacuo* first on a rotovap and then on a high vacuum line (8 Pa, 24 degrees C) for 2 hr to
30 yield the final product as a colorless oil (28.1 g, 85% yield).

^{19}F NMR (CD_2Cl_2) δ -86.4 (s, 3F); -89.0, -90.8 (subsplit ABq, $J_{\text{FF}} = 147$ Hz, 2F); -119.2, -125.8 (subsplit ABq, $J_{\text{FF}} = 254$ Hz, 2F); -141.7 (dm, $J_{\text{FH}} = 53$ Hz, 1F).

¹H NMR (CD₂Cl₂) δ 1.0 (t, *J* = 7.3 Hz, 12H); 1.5 (m, 16H); 2.2 (m, 8H); 6.3 (dm, *J*_{FH} = 54 Hz, 1H).

% Water by Karl-Fisher titration: 0.29.

- 5 Analytical calculation for C₂₀H₃₇F₈O₄PS: C, 43.2: H, 6.7: N, 0.0.
Experimental results: C, 42.0: H, 6.9: N, 0.1.
Extractable bromide by ion chromatography: 21 ppm.

10 (V) Preparation of 1,3-dioctylimidazolium iodide [doim][I]

1,3-Dioctylimidazolium iodide [ooim][I] was prepared as described by L. Xu, *et al.*, Journal of Organometallic Chemistry, 2000, 598, 409-416:

- Imidazole (2.72 g; 0.04 mmol) and octyl bromide (3.1 g; 0.016 mmol) were dissolved in 55 ml of ethyl acetate. The mixture was refluxed under a nitrogen blanket. Initially, the solution was clear and colorless, however upon refluxing approximately 1 hour the mixture became cloudy with a tannish color. The mixture was allowed to reflux overnight. The mixture was then cooled to room temperature (RT) upon which a white precipitate formed. The mixture was extracted with water (2x: 30ml). After drying the solvent with magnesium sulfate, the solvent was removed using a vacuum, yielding a tannish oil.

- To the oily residue was added 60 ml of toluene followed by 1-iodooctane (4.8 g; 0.02). The mixture was refluxed overnight under a nitrogen blanket, resulting in a dark yellow mixture. The yellow oil was collected via a separation funnel rinsed with toluene (2x: 20 ml) and dried under vacuum.

(W) Preparation of 1-methyl-3-octylimidazolium iodide [omim][I]

1-Methyl-3-octylimidazolium iodide [omim][I] was prepared as described by L. Xu, *et al.* (Journal of Organometallic Chemistry, 2000, 598, 409-416):

- 30 1-Methylimidazole (1.65 g; 0.02 mmol) and 1-iodooctane (5.31 g; 0.022 mmol) were dissolved in 30 ml of toluene. The reaction was refluxed, whereupon the mixture immediately became yellow in color and cloudy. The mixture was refluxed overnight, during which a yellowish oily precipitate formed. The yellowish oil was collected and dried under vacuum.

The following nomenclature and abbreviations are used:

- a_i = generic RK EOS parameter of the i -th species ($\text{m}^6 \bullet \text{MPa} \bullet \text{mol}^{-2}$)
- 5 b_i = generic RK EOS parameter of i -th species ($\text{m}^3 \bullet \text{mol}^{-1}$)
- C = concentration ($\text{mol} \bullet \text{m}^{-3}$)
- C_b = buoyancy force (N)
- C_f = correction factor (kg)
- C_{pi}^0 = ideal gas heat capacity of i -th species ($\text{J} \bullet \text{mol}^{-1} \bullet \text{K}^{-1}$)
- 10 C_0 = initial concentration ($\text{mol} \bullet \text{m}^{-3}$)
- C_s = saturation concentration ($\text{mol} \bullet \text{m}^{-3}$)
- $\langle C \rangle$ = space-averaged concentration ($\text{mol} \bullet \text{m}^{-3}$)
- COP = coefficient of performance
- D = diffusion constant ($\text{m}^2 \bullet \text{s}^{-1}$)
- 15 g = gravitational acceleration ($9.80665 \text{ m} \bullet \text{s}^{-2}$)
- f = mass flow rate ratio
- $f(T)$ = temperature dependent term of binary interaction parameter, $1 + \tau_{ij}/T$
- H_i = enthalpy at point i ($\text{J} \bullet \text{kg}^{-1}$)
- $k_{ij}, k_{ji}, l_{ij}, l_{ji}$ = binary interaction parameters
- 20 L = length (m)
- m_a = mass absorbed (kg)
- m_i = mass of i -th species on sample side of balance (kg)
- m_j = mass of j -th species on counterweight side of balance (kg)
- m_{ij} = binary interaction parameter
- 25 m_s = mass flow rate of solution ($\text{kg} \bullet \text{sec}^{-1}$)
- m_r = mass flow rate of refrigerant ($\text{kg} \bullet \text{sec}^{-1}$)
- m_{IL} = mass of ionic liquid sample (kg)
- MW_i = molecular weight of i -th species ($\text{kg} \bullet \text{mol}^{-1}$)
- N = n -th number component

- P = pressure (MPa)
 P_{ci} = critical pressure of i -th species (MPa)
 P_0 = initial pressure (MPa)
 Q_i = heat (kW)
- 5 R = gas constant ($8.31434 \text{ m}^3 \cdot \text{Pa} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$)
 t = time (s)
 T_{ci} = critical temperature of i -th species (K)
 T_i = temperature of i -th species (K)
 T_j = temperature of j -th species (K)
- 10 T_s = temperature of sample (K)
 V_i = volume of i -th species (m^3)
 V_{IL} = volume of ionic liquid (m^3)
 V_m = liquid sample volume (m^3)
 $\tilde{V}_g$ = molar volume of gas ($\text{m}^3 \cdot \text{mol}^{-1}$)
- 15 $\tilde{V}_i$ = molar volume of i -th species ($\text{m}^3 \cdot \text{mol}^{-1}$)
 $\tilde{V}_{IL}$ = molar volume of ionic liquid ($\text{m}^3 \cdot \text{mol}^{-1}$)
 $\tilde{V}_m$ = molar volume of mixture ($\text{m}^3 \cdot \text{mol}^{-1}$)
 $\tilde{V}_0$ = initial molar volume ($\text{m}^3 \cdot \text{mol}^{-1}$)
 $\Delta \tilde{V}$ = change in molar volume ($\text{m}^3 \cdot \text{mol}^{-1}$)
- 20 W_i = work (kW)
 x_i = mole fraction of i -th species
 z = depth (m)
 α = EOS temperature dependence parameter
 β_k = coefficient of temperature dependence parameter
- 25 λ_n = eigenvalue (m^{-1})
 ρ_g = density of gas ($\text{kg} \cdot \text{m}^{-3}$)
 ρ_i = density of i -th component on sample side of balance ($\text{kg} \cdot \text{m}^{-3}$)
 ρ_j = density of j -th component on counter weight side of balance ($\text{kg} \cdot \text{m}^{-3}$)

ρ_{air} = density of air ($\text{kg}\cdot\text{m}^{-3}$)

ρ_s = density of sample ($\text{kg}\cdot\text{m}^{-3}$)

η = heat ratio, output power divided by input power

τ_{ij} = binary interaction parameter (K) for temperature dependence term, $f(T)$

5

Units

Pa $\equiv$ Pascal

MPa $\equiv$ Mega Pascal

mol $\equiv$ mole

10 m $\equiv$ meter

cm $\equiv$ centimeter

kW $\equiv$ kilowatt

K $\equiv$ Kelvin

N $\equiv$ Newton

15 J $\equiv$ Joule

kJ $\equiv$ kilojoule

kg $\equiv$ kilogram

mg $\equiv$ milligram

μg $\equiv$ microgram

20 T $\equiv$ temperature

P $\equiv$ pressure

mbar $\equiv$ millibar

min $\equiv$ minute

$^{\circ}\text{C}$ $\equiv$ degrees centigrade

25 sec $\equiv$ second

The gas solubility and diffusivity measurements were made using a gravimetric microbalance (Hiden Isochema Ltd, IGA 003, Warrington, UK). The IGA design integrates precise computer-control and measurement of weight change, pressure and temperature to enable fully automatic and reproducible determination of gas adsorption-desorption isotherms and isobars. The microbalance consists of an electrobalance with sample and counterweight components inside a stainless steel pressure-vessel as shown in Figure 13 and described in Example 16, Table 20. The balance has a weight range of 0-100 mg with a resolution of 0.1 μg . An enhanced pressure stainless steel (SS316LN) reactor capable of operation to 20.0 bar and 100 °C was installed. Approximately 60 mg of ionic liquid sample was added to the sample container and the reactor was sealed. The sample was dried and degassed by first pulling a coarse vacuum on the sample with a diaphragm pump (Pfeiffer, model MVP055-3, Asstar, Germany) and then fully evacuating the reactor to 10^{-8} bar with a turbopump (Pfeiffer, model TSH-071). While under deep vacuum, the sample was heated to 75 °C for 10 hr with an external water jacket connected to a remote-controlled constant-temperature bath (Huber Ministat, model cc-S3, Offenburg, Germany). A 30 percent ethylene glycol and 70 percent water mixture by volume was used as the recirculating fluid with a temperature range of 5 to 90 °C. The sample mass slowly decreased as residual water and gases were removed. Once the mass had stabilized for at least 60 min, the sample dry mass was recorded. The percent weight loss for the various ionic liquids tested was in the range of 1 to 3%.

The IGA003 can operate in both dynamic and static mode. Dynamic mode operation provides a continuous flow of gas (max. $500 \text{ cm}^3 \text{ min}^{-1}$) past the sample and the exhaust valve controls the set-point pressure. Static mode operation introduces gas into the top of the balance away from the sample and both the admittance and exhaust valves control the set-point pressure. All absorption measurements were performed in static mode. The sample temperature was measured with a type K thermocouple with an accuracy of ± 0.1 °C. The thermocouple was located inside the reactor next to the sample container. The water jacket maintained the set-point temperature automatically to within a typical regulation accuracy of ± 0.1 °C. Four isotherms (at 10, 25, 50, and 75 °C)

were measured beginning with 10 °C. Once the desired temperature was achieved and stable, the admittance and exhaust valves automatically opened and closed to adjust the pressure to the first set-point. Pressures from 10^{-9} to 10^{-1} bar were measured using a capacitance manometer (Pfeiffer, model PKR251), and pressures from 10^{-1} to 20.0 bar were measured using a piezo-resistive strain gauge (Druck, model PDCR4010, New Fairfield, CT). Regulation maintained the reactor pressure set-point to within ± 4 to 8 mbar. The pressure ramp rate was set at $200 \text{ mbar min}^{-1}$ and the temperature ramp rate was set at 1 °C min^{-1} . The upper pressure limit of the stainless steel reactor was 20.0 bar, and several isobars up to 10 bar (i.e., 0.1, 0.5, 1, 4, 7, 10 bar) were measured. To ensure sufficient time for gas-liquid equilibrium, the ionic liquid samples were maintained at set-point for a minimum of 3 hr with a maximum time-out of 8 hr.

The IGA method exploits the relaxation behavior following pressure and temperature changes to simultaneously evaluate the time-dependent absorption and asymptotic uptake. The real-time processor was used to determine the end-point for each isotherm. The percent relaxation used as an end point for the real-time analysis was 99 percent. The minimum weight change for real-time analysis was set at 1 μg , the acceptable average deviation of the model from the acquired data was set at 7 μg , and the target interval for weight acquisition was set at a typical value of 1 μg . The temperature variation during an isotherm was maintained less than 0.1 °C min^{-1} .

Safety features of the IGA003 included a pressure relief valve and over-temperature control for the reactor. The factory-installed relief valve was replaced with a DuPont guideline relief valve (Circle-Seal, set-point pressure 24.5 bar; DuPont, Wilmington, Delaware). To further protect the microbalance system from over-pressure, additional relief valves were installed on the custom gas manifold and on each gas cylinder; these relief valves were set to open if the pressure exceeded 25 bar. The reactor over-temperature interlock controller that comes standard on the IGA003 was set to turn off the water bath if the temperature exceeded 100 °C. Due to the fact that some of the gases tested were flammable (i.e. HFC-32, HFC-143a, and HFC-152a), the IGA003 was mounted

inside a custom stainless steel cabinet purged with nitrogen that minimize the possibility of a flame.

Thermogravimetric measurements were corrected for a number of gravitational balance forces introduced at high pressure as described by Pinkerton, E. P., *et al.*, High-pressure gravimetric measurement of hydrogen capacity in vapor-grown carbon nanofibers and related materials [Proceedings of the 11th Canadian Hydrogen Conference, Victoria, BC, 2001, 633-642]). These included:

- (1) Changes in the buoyant forces due to changes in pressure and temperature.
- (2) Aerodynamic drag forces created by the flow of gases.
- (3) Changes in the balance sensitivity due to changes in temperature and pressure.
- (4) Volumetric changes in the samples due to expansivit.

The gravitational balance forces previously described are often of the same order of magnitude (0.1 to 5 mg) as the overall weight change in the sample and can lead to inaccurate results if not accounted for precisely. Distinguishing mass changes with an accuracy of 0.01 wt.% on small and sometimes limited sample quantities requires knowledge of the sample weight to within about 5 to 10 µg.

20

The buoyancy correction follows from Archimedes' principal: there is an upward force exerted on an object equivalent to the mass of fluid displaced. The upward force (C_b) due to buoyancy is calculated using eq 27 where the mass of the gas displaced is equivalent to the volume of the submersed object (V_i) times the density (ρ_g) of the gas at a given (T, P) and the gravitational acceleration (g). If the volume of the object remains constant, V_i can be calculated by knowing the mass (m_i) and density (ρ_i) of the object.

$$C_b = \text{Buoyancy} = gV_i\rho_g(T, P) = g\frac{m_i}{\rho_i}\rho_g(T, P)$$

(27)

Instead of using the gas densities provided in the Hiden Isochema IGA software, the gas density for each gas was calculated using a computer program (REFPROP

v.7) developed by the National Institute of Standards and Technology (NIST) (Lemmon EW, *et al.* [NIST reference fluid thermodynamic and transport properties – REFPROP, version 7.0 user's guide, U.S. Department of Commerce, Technology Administration, National Institute of Standards and Technology, Standard Reference Data Program, Gaithersburg, Maryland, 2002]).

The buoyancy correction using the IGA003 system involves many additional objects for weighing the sample. Table 20 provides a list of each critical component along with the weight, material, density, and temperature. The component arrangement in Figure 13 leads to a mass balance as shown by eq 28. This expression accounts for the summation of all components as well as the contribution of the absorbed gas mass (m_a) and a correction factor (C_f) which accounts for the balance sensitivity to T , P . The density of air (ρ_{air}) at ambient temperature and pressure was subtracted from ρ_i and ρ_j because the components were initially weighed in air.

$$\begin{aligned} & \sum_{i=1} m_i - \sum_{j=1} m_j - \sum_{i=1} \frac{m_i}{\rho_i} \rho_g(T_i, P) + \sum_{j=1} \frac{m_j}{\rho_j} \rho_g(T_j, P) + m_{IL} + m_a \\ & - \frac{m_{IL}}{\rho_s(T_s)} \rho_g(T_s, P) - \frac{m_a}{\rho_a(T_s)} \rho_g(T_s, P) - C_f(T_s, P) = reading \end{aligned}$$

(28)

The largest contributions in eq 28 are typically those of the sample container, sample, and counter weight; the other referenced objects in Table 20 contribute less because of their larger densities (denominators in eq 28). Physical densities of ionic liquids were measured using a Micromeritics Accupyc 1330 helium pycnometer with an accuracy of $\pm 0.001 \text{ g cm}^{-3}$ (Micromeritics Instrument Corp., Norcross, GA). Initially, the volume (V_{IL}) of each sample was calculated from its pycnometric density (ρ_s) and dry mass sample weight (ρ_s), but volumetric expansion ($\Delta\tilde{V}/\tilde{V}_0$) due to the gas absorption was later taken into account as described below to more accurately determine the buoyancy effect.

The system was operated in static mode that essentially eliminates any aerodynamic drag forces due to flowing gases. Electrobalances are sensitive to

temperature and pressure fluctuations on the beam arm and internal electronics.

To minimize this effect, the balance electronics are heated externally with a band heater to a temperature of 45 ± 0.1 °C. In addition, the component temperatures provided in Table 20 are measured for the sample (T_s) and all others are

5 estimated. Therefore, a correction factor (C_f) was determined as a function of T , P by measuring the buoyancy effect without a sample and calculating a least-squares fit to tare the balance. The correction factor was on the order of 0.1 to 0.3 mg and increased as expected with decreasing temperature and increasing pressure.

10

Initially the ionic liquid sample volume was considered to be constant and the mole fraction solubility calculated without taking into account buoyancy effects due to sample expansivity. In order to make a proper buoyancy correction due to the liquid volume change, a simple mole fraction average for the molar

15 volume, $\tilde{V}_m$, was used.

$$\tilde{V}_m(T, P) = \tilde{V}_{IL}(1 - x) + \tilde{V}_g x,$$

(29)

where $\tilde{V}_i = MW_i / \rho_i$ and x represents the molar fraction of gas in the solution.

$$20 \quad V_m(T, P) = \tilde{V}_m(T, P) \left[\left(\frac{m_{IL}}{MW_{IL}} \right) + \left(\frac{m_g}{MW_g} \right) \right]$$

(30)

$$\frac{m_s}{\rho_s(T_s)} \rho_g(T_s, P) + \frac{m_a}{\rho_a(T_s)} \rho_g(T_s, P) = V_m(T, P) \rho_g(T, P)$$

(31)

As a first approximation, eqs 29 and 30 were used to estimate the change in the liquid sample volume, V_m , at the measured T , P conditions. Eq 31 can be substituted into eq 28 to account for the buoyancy change with respect to sample expansivity.

25

Besides the equilibrium solubility, time-dependent absorption data were also obtained using the Hiden gravimetric microbalance for each T , P set-point. In order to understand the time-dependent behavior of gas dissolving in liquid, we applied a mathematical model based on a simplified mass diffusion process.

5 Imagine a flat-bottom sample container filled with ionic liquid at a certain liquid level height (L). The height is determined by knowing the cylindrical geometry of the sample container, dry sample weight after evacuation and heating, and the ionic liquid density at the proper temperature. After evacuation, the gas is introduced into the Pyrex[®] sample container with a constant pressure at a given

10 temperature. A small amount of gas will start dissolving into the ionic liquid, and after a sufficient time it will reach a thermodynamic equilibrium, that is the solubility limit of the gas in the ionic liquid at the given T and P . This transient behavior with time is modeled as described by Shiflett MB, and Yokozeki A, *supra*; and Yokozeki A, (*Int. J. Refrigeration*, 2002, 22, 695-704).

15

Processes of gas dissolving in liquid may be highly complex phenomena because of a possible evolution of heat of mixing, the subsequent liquid convection due to the local temperature difference, as well as the free convection due to the density difference, and the possible change in thermophysical

20 properties of the liquid. The following assumptions were made for the dissolving gas (Shiflett, MB, and Yokozeki, A, *supra*; and Yokozeki A, Time-dependent behavior of gas absorption in lubricant oil [*Int. J. Refrigeration* 2002, 22, 695-704]):

- (1) Gas dissolves through a one-dimensional (vertical) diffusion process, in
- 25 which there is no convective flow in the liquid.
- (2) A thin boundary layer between the gas and liquid phases exists, where the thermodynamic equilibrium is instantly established with the saturation concentration (C_s), and where the concentration is constant all the time at a given temperature and pressure.
- 30 (3) Temperature and pressure are kept constant.
- (4) The gas-dissolved liquid is a highly dilute solution, and so the relevant thermophysical properties of the solution do not change.

The process is then described by one-dimensional mass diffusion due to the local concentration difference. The governing differential equations are:

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial z^2}$$

(32)

5 Initial Condition: $C = C_0$ when $t = 0$ and $0 < z < L$

(33)

Boundary Conditions: $C = C_s$ when $t > 0$ and $z = 0$

(34)

$$\frac{\partial C}{\partial z} = 0 \text{ at } z = L$$

10 (35)

where C is the concentration of a dissolving substance in ionic liquid as a function of time, t and vertical location, z , where L is the depth of ionic liquid in the container, and $z = 0$ corresponds to the vapor-liquid boundary. C_0 is an initial homogenous concentration of the dissolving gas, and is zero (initially) or a small finite amount at $t > 0$. D is the diffusion coefficient that is assumed to be constant.

Eq 32 can be solved analytically for the initial and boundary conditions eqs 33 - 35 by a standard method such as separation variables or Laplace transform and yields:

$$C = C_s \left[1 - 2 \left(1 - \frac{C_0}{C_s} \right) \sum_{n=0}^{\infty} \frac{\exp(-\lambda_n^2 D t) \sin \lambda_n z}{L \lambda_n} \right],$$

(36)

$$\text{where } \lambda_n = \left(n + \frac{1}{2} \right) \frac{\pi}{L}.$$

An experimentally observed quantity at a specified time is the total concentration (or mass) of dissolved gas in ionic liquid, and not the concentration profile in z . This space-averaged concentration at a given time, $\langle C \rangle$, can be calculated from eq 37.

$$\langle C \rangle = \int_0^L C dz / L$$

(37)

$$\langle C \rangle = C_s \left[1 - 2 \left(1 - \frac{C_0}{C_s} \right) \sum_{n=0}^{\infty} \frac{\exp\left(-\lambda_n^2 D t\right)}{L^2 \lambda_n^2} \right]$$

(38)

5

Although eq 38 contains an infinite summation, only the first few terms, except for initial small time periods, are sufficient in practical applications. In this work, the summation was terminated after ten terms when the numerical contribution to the summation in $\langle C \rangle$ became less than 10^{-12} . By analyzing
 10 experimental data with this equation, we obtained the saturation concentration (C_s) and diffusion constant (D) at given T and P , when C_0 was known.

Examples 3 – 7 and Figures 5 – 9 show solubility and diffusivity results for several hydrofluorocarbons (HFC-32, HFC-125, HFC-134a, HFC-143a, and
 15 HFC-152a) in one ionic liquid, [bmim][PF₆], at 10, 25, 50, and 75 °C. Compositions were prepared that consisted of HFC-32 and [bmim][PF₆] from about 0.3 to about 81.2 mole percent of HFC-32 over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to 10 bar. Compositions
 20 were prepared that consisted of HFC-125 and [bmim][PF₆] from about 0.1 to about 65.1 mole percent of HFC-125 over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-134a and [bmim][PF₆] from about 0.1 to about 72.1 mole
 25 percent of HFC-134a over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to 3.5 bar. Compositions were prepared that consisted of HFC-143a and [bmim][PF₆] from about 0.1 to about 23.5 mole percent of HFC-143a over a temperature range from about 10 to about 75 °C at a pressure from
 30 4.5 bar. Compositions were prepared that consisted of HFC-152a and [bmim][PF₆] from about 0.5 to about 79.7 mole percent of HFC-152a over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to

Examples 8 – 14 and Figures 10 and 11 show solubility and diffusivity results for HFC-32 in several additional ionic liquids ([bmim][PF₆], [bmim][BF₄], [dmpim][tTFMSmethide], [omim][I], [doim][I], [emim][bPFESimide], [dmpim][bTFMSimide], and [pmpy][bTFMSimide]). Compositions were prepared that consisted of HFC-32 and [bmim][BF₄] from about 0.1 to about 76.5 mole percent of HFC-32 over a temperature range from about 10 to about 75 °C at a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-32 and [dmpim][tTFMSmethide] from about 0.4 to about 80.2 mole percent of HFC-32 over a temperature range from about 10 to about 75 °C and a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-32 and [omim][I] from about 0.4 to about 41.6 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-32 and [doim][I] from about 0.7 to about 46.8 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-32 and [emim][bPFESimide] from about 1.0 to about 66.6 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-32 and [dmpim][bTFMSimide] from about 0.8 to about 64.5 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to 10 bar. Compositions were prepared that consisted of HFC-32 and [pmpy][bTFMSimide] from about 1.0 to about 63.9 mole percent of HFC-32 at a temperature of about 25 °C and a pressure from about 0.1 to 10 bar.

25

Figure 12 shows measured isothermal solubility data (in mole fraction) at 10 °C of the systems HFC-32, HFC-152a, HFC-134a, HFC-125, and HFC-143a + [bmim][PF₆] in terms of absolute pressure divided by the gas saturation pressure (P_0) at 10 °C shown by ratio (P/P_0). The saturation pressures for HFC-32, HFC-125, HFC-134a, HFC-143a, and HFC-152a at 10 °C are $P_0 = 11.069$ bar, $P_0 = 3.7277$ bar, $P_0 = 4.1461$ bar, $P_0 = 9.0875$, and $P_0 = 8.3628$ bar, respectively. Negative deviations from Raoult's law (i.e. curvature below the dashed line) are unusual and indicate strong interaction between the refrigerant and the ionic

30

liquid. This in turn translates into high solubility that is ideal for an absorption cycle working fluid. In particular HFC-32 has negative deviation from Raoult's law as shown in Figure 12. A composition was prepared comprising HFC-32 and [bmim][PF₆] from about 0.1 to 63 mole percent of HFC-32 at about 10 °C and P/P₀ from about 0.1 to about 0.63. Strong positive deviations from Raoult's law (i.e. curvature above the dashed line) are more typical and indicate refrigerant and ionic liquids are less soluble and eventually may form a liquid-liquid phase separation. A composition was prepared comprising HFC-152a and [bmim][PF₆] from about 0.1 to about 80 mole percent of HFC-152a at about 10 °C and P/P₀ from about 0.1 to about 0.86. A composition was prepared comprising HFC-134a and [bmim][PF₆] from about 0.1 to about 72 mole percent of HFC-134a at about 10 °C and P/P₀ from about 0.1 to about 0.84. A composition was prepared comprising HFC-125 and [bmim][PF₆] from about 0.1 mole to about 65 mole percent of HFC-125 at about 10 °C and P/P₀ from about 0.1 to about 0.88. A composition was prepared comprising HFC-143a and [bmim][PF₆] from about 0.1 to about 25 mole percent at about 10 °C and P/P₀ from about 0.1 to about 0.90.

EXAMPLE 1

Absorption Cooling Process

Table 2. EOS Constants of Pure Refrigerants and Absorbents.

Compound	Molar Mass	T_c (K)	P_c (kPa)	β_0	β_1	β_2	β_3
R-32	52.02	351.26	5782	1.0019	0.48333	-0.07538	0.00673
R-125	120.22	339.19	3637	1.0001	0.47736	-0.01977	-0.0177
R-134a	102.03	374.21	4059	1.0025	0.50532	-0.04983	0
R-134	102.03	391.97	4580	1.0012	0.48291	-0.05071	0
R-143a	84.04	346.20	3759	1.0006	0.45874	-0.04846	-0.0143
R-152a	66.05	386.44	4520	1.0012	0.48495	-0.08508	0.0146
NH ₃	17.03	405.40	11333	1.0018	0.46017	-0.06158	0.00168
H ₂ O	18.02	647.10	22064	1.0024	0.54254	-0.08667	0.00525
[bmim][PF ₆]	284.18	950	2027	1	0.6571	0	0
[bmim][BF ₄]	226.02	950	2533	1	0.8362	0	0

Table 3. Coefficients for Ideal Gas Heat Capacity [$\text{J}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$] in eq 14.

Compound	C_0	C_1	C_2	C_3
R-32	20.34	0.07534	1.872×10^{-5}	-3.116×10^{-8}
R-125	16.58	0.33983	-2.873×10^{-4}	8.870×10^{-8}
R-134a	12.89	0.30500	-2.342×10^{-4}	6.852×10^{-8}
R-134	15.58	0.28475	-2.028×10^{-4}	5.395×10^{-8}
R-143a	5.740	0.31388	-2.595×10^{-4}	8.410×10^{-8}
R-152a	8.670	0.2394	-1.456×10^{-4}	3.392×10^{-8}
NH_3	27.31	0.02383	1.707×10^{-5}	-1.185×10^{-8}
H_2O	32.24	1.924×10^{-3}	1.055×10^{-5}	-3.596×10^{-9}
[bmim][PF ₆]	-2.214	0.57685	-3.854×10^{-4}	9.785×10^{-8}
[bmim][BF ₄]	8.946	0.43986	-1.881×10^{-4}	1.177×10^{-8}

5 **Table 4.** Binary Interaction Parameters of Refrigerant-Absorbent Pairs
Determined from Experimental PTx data shown in Examples 2 – 7.

Binary Systems (1)/(2)	l_{12}	l_{21}	$m_{12, 21}$	$\tau_{12, 21}$	β_1 (absorbent)
R-32/[bmim][PF ₆]	-0.142	-0.0123	0	0	0.6571
R-32/[bmim][BF ₄]	-0.0474	-0.0474	0	0	0.8362
R-134a/[bmim][PF ₆]	0.0730	0.0187	0	0	0.6571
R-134/[bmim][PF ₆]	-0.0957	-0.1037	0	0	0.6571
R-152a/[bmim][PF ₆]	0.0483	0.0212	0	0	0.6571
R-125/[bmim][PF ₆]	0.1575	0.0218	0	0	0.6571
$\text{NH}_3/\text{H}_2\text{O}$	-0.316	-0.316	-0.0130	0	0.54254

Table 5. Comparisons of Theoretical Absorption Cycle Performances.^(a)

Mode 1 Configuration	P_{con}, P_g kPa	P_{eva}, P_a kPa	f	x_g mass%	x_a mass%	Q_e kW	COP
R-32/[bmim][PF ₆]	2486	1106	7.35	90.40	78.10	250.4	0.385
R-32/[bmim][BF ₄]	2486	1106	6.41	90.17	76.11	250.4	0.330
R-134a/[bmim][PF ₆]	1015	414	10.66	92.36	83.70	150.8	0.254
R-134/[bmim][PF ₆]	810	322	4.38	88.75	68.48	165.5	0.348
R-152a/[bmim][PF ₆]	907	373	13.27	94.07	86.98	247.7	0.300
R-125/[bmim][PF ₆]	2011	909	16.49	92.15	86.56	82.4	0.128
NH ₃ /H ₂ O	1548	615	2.54	59.5	36.1	1112	0.646
H ₂ O/LiBr	7.38	1.23	4.08	66.3	50.0	2502	0.833

^(a) Absorption Cycle conditions: $T_g / T_{con} / T_a / T_{eva} = 100 / 40 / 30 / 10$ °C, and $m_r = 1$ kg·s⁻¹.

EXAMPLE 2

Table 6. Comparisons of Theoretical Vapor Compression and Hybrid Vapor Compression - Absorption Cycle Performances.^(a,b)

Mode 2 Parallel and Series Configuration	P_{con}, P_g kPa	P_{eva}, P_a kPa	f	x_g mass%	x_a mass%	Q_e kW	COP
R-32 ^(b)	2486	1106	-	-	-	250.4	7.48
R-134a ^(b)	1015	414	-	-	-	150.8	7.95
R-152a ^(b)	907	373	-	-	-	247.7	8.21
R-125 ^(b)	2011	909	-	-	-	82.4	6.66
R-32/R-125 ^(b) (50/50 wt%)	2393	1077	-	-	-	161.7	7.27
Mode 3 Parallel Configuration	P_{con}, P_g kPa	P_{eva}, P_a kPa	f	x_g mass%	x_a mass%	Q_e kW	COP
R-32/[bmim][PF ₆] ^(a+b)	2486	1106	7.35	90.40	78.10	500.8	0.732
R-32/[bmim][BF ₄] ^(a+b)	2486	1106	6.41	90.17	76.11	500.8	0.632
R-134a/[bmim][PF ₆] ^(a+b)	1015	414	10.66	92.36	83.70	301.6	0.492
R-152a/[bmim][PF ₆] ^(a+b)	907	373	13.27	94.07	86.98	495.4	0.579
R-125/[bmim][PF ₆] ^(a+b)	2011	909	16.49	92.15	86.56	164.8	0.251
Mode 3 Series Configuration	P_{con}, P_g kPa	P_{eva}, P_a kPa	f	x_g mass%	x_a mass%	Q_e kW	COP
R-32/[bmim][PF ₆] ^(b+c)	2486	1106	18.78	82.50	78.10	250.4	0.478
R-32/[bmim][BF ₄] ^(b+c)	2486	1106	15.00	81.56	76.12	250.4	0.418
R-134a/[bmim][PF ₆] ^(b+c)	1015	414	35.87	86.11	83.7	150.8	0.339
R-152a/[bmim][PF ₆] ^(b+c)	907	373	44.21	89.0	86.98	247.8	0.356
R-125/[bmim][PF ₆] ^(b+c)	2011	909	79.51	87.7	86.6	82.5	0.166

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(a) Absorption cycle conditions: $T_g / T_{con} / T_a / T_{eva} = 100 / 40 / 30 / 10$ °C, and $m_r = 1$ kg·s⁻¹.

(b) Vapor compression cycle conditions: $T_{con} / T_{eva} = 40 / 10$ °C, and $m_r = 1$ kg·s⁻¹.

(c) Absorption cycle conditions: $T_g / T_{con} / T_a / T_{eva} = 60 / 40 / 30 / 10$ °C, and $m_r = 1$ kg·s⁻¹.

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EXAMPLE 3

Solubility of difluoromethane (HFC-32) in 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆])

A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 10 bar where the solubilities ($X_{\text{meas.}}$) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_0), final saturation concentration (C_s), and calculated solubility ($X_{\text{calc.}}$) are also provided in the table.

Tables 7a, 7b, 7c and 7d provide data for C_0 , C_s , D , $X_{\text{calc.}}$, and $X_{\text{meas.}}$ at temperatures of 10, 25, 50 and 75 °C, respectively.

Table 7a

T (°C)	P (bar)	C_0 (mass%)	C_s (mass%)	D (m ² /sec)	$X_{\text{calc.}}$ (mol. fraction)	$X_{\text{meas.}}$ (mol. fraction)
10.0	0.0979	--	--	--	--	0.026
10.0	0.9957	0.82	2.53	1.94E-11	0.124	0.106
10.0	2.4967	3.32	7.56	1.71E-11	0.309	0.270
10.0	3.9964	8.18	12.38	3.65E-11	0.436	0.426
10.0	5.4975	14.44	18.71	6.34E-11	0.557	0.555
10.0	6.9965	22.12	27.85	7.42E-11	0.678	0.676
10.0	8.4954	--	--	--	--	0.812

Table 7b

T (°C)	P (bar)	C_0 (mass%)	C_s (mass%)	D (m ² /sec)	$X_{\text{calc.}}$ (mol. fraction)	$X_{\text{meas.}}$ (mol. fraction)
24.9	0.0965	--	--	--	--	0.018
25.0	0.9952	0.49	1.69	2.45E-11	0.086	0.076
25.0	2.4965	2.22	4.53	2.44E-11	0.206	0.189
25.0	3.9979	5.05	7.37	3.51E-11	0.303	0.295
24.9	5.4969	8.23	10.47	5.41E-11	0.390	0.387
24.9	6.9950	11.82	14.09	6.75E-11	0.473	0.471
25.0	8.5012	15.75	18.26	8.33E-11	0.550	0.548
24.9	9.9994	20.38	23.31	8.84E-11	0.624	0.622

Table 7c

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
49.6	0.0992	0.00	0.12	4.76E-11	0.007	0.006
49.9	0.9954	0.33	0.92	5.28E-11	0.048	0.047
49.9	2.4963	1.43	2.31	5.29E-11	0.115	0.113
49.9	3.9949	2.84	3.72	5.98E-11	0.174	0.173
49.9	5.4966	4.41	5.22	5.99E-11	0.231	0.229
49.9	6.9965	5.81	6.72	7.69E-11	0.282	0.282
50.0	8.4959	7.37	8.32	8.54E-11	0.331	0.331
50.0	9.9959	9.78	10.05	4.04E-11	0.379	0.377

Table 7d

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T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
75.0	0.0988	0.00	0.06	7.12E-11	0.003	0.003
75.0	0.9968	0.30	0.56	8.19E-11	0.030	0.029
75.0	2.4950	0.96	1.38	8.14E-11	0.071	0.069
75.0	3.9944	1.74	2.19	9.82E-11	0.109	0.108
74.9	5.4983	2.60	3.03	9.70E-11	0.146	0.145
74.9	6.9966	3.42	3.89	9.58E-11	0.181	0.180
75.0	8.4958	4.28	4.77	9.56E-11	0.215	0.212
75.0	9.9989	5.12	5.62	1.18E-10	0.245	0.244

EXAMPLE 4**Solubility of pentafluoroethane (HFC-125) in 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆])**

5 A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 10 bar where the solubilities ($X_{\text{meas.}}$) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_0), final saturation concentration (C_s), and calculated solubility ($X_{\text{calc.}}$) are also provided in the table.

10 Tables 8a, 8b, 8c and 8d provide data for C_0 , C_s , D , $X_{\text{calc.}}$, and $X_{\text{meas.}}$ at temperatures of 10, 25, 50 and 75 °C, respectively.

Table 8a

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T (°C)	P (bar)	C_0 (mass%)	C_s (mass%)	D (m ² /sec)	$X_{\text{calc.}}$ (mol. fraction)	$X_{\text{meas.}}$ (mol. fraction)
9.9	0.0992	0.0	0.12	2.52E-12	0.003	0.013
10.0	0.9964	0.73	1.50	1.83E-11	0.035	0.034
10.1	1.9959	1.72	3.96	6.36E-12	0.089	0.074
10.0	2.9960	3.55	6.25	9.31E-12	0.136	0.125
10.1	3.9964	6.03	8.88	1.56E-11	0.187	0.182
9.9	4.9965	9.10	12.52	2.44E-11	0.253	0.250
10.0	5.9965	13.18	17.56	4.05E-11	0.335	0.336
9.9	6.9962	19.19	26.04	6.12E-11	0.455	0.454
10.0	7.9979	--	--	--	--	0.651

Table 8b

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
25.0	0.0977	--	--	--	--	0.003
25.0	0.9963	0.23	0.09	1.81E-11	0.002	0.023
25.0	1.9982	1.05	2.12	1.50E-11	0.049	0.050
24.9	2.9949	2.13	3.11	2.15E-11	0.071	0.079
25.0	3.9982	3.50	4.71	2.03E-11	0.105	0.109
25.0	4.9947	4.84	6.18	2.39E-11	0.135	0.140
25.0	5.9951	6.38	7.91	2.65E-11	0.169	0.176
25.0	7.9955	8.96	12.10	4.81E-11	0.246	0.254
24.9	9.9977	14.20	18.16	7.82E-11	0.344	0.352

Table 8c

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T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
49.9	0.1003	--	--	--	--	0.000
49.9	0.9963	0.18	0.55	4.29E-11	0.013	0.013
49.9	1.9983	0.73	1.17	4.59E-11	0.027	0.027
50.0	2.9996	1.34	1.78	5.19E-11	0.041	0.041
49.9	3.9969	1.96	2.44	4.75E-11	0.056	0.056
50.0	4.9993	2.60	3.10	5.38E-11	0.070	0.070
49.9	5.9961	3.29	3.80	5.14E-11	0.086	0.085
49.9	7.9970	4.38	5.25	5.55E-11	0.116	0.116
49.9	9.9958	5.85	6.82	5.87E-11	0.148	0.148

Table 8d

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
75.0	0.1021	--	--	--	--	0.001
74.9	0.9965	0.07	0.28	7.49E-11	0.007	0.007
75.0	1.9961	0.36	0.60	9.46E-11	0.014	0.016
75.1	2.9967	0.70	0.93	7.04E-11	0.022	0.025
75.0	3.9971	1.04	1.27	7.96E-11	0.030	0.033
75.0	4.9983	1.36	1.61	9.86E-11	0.037	0.042
75.0	5.9980	1.75	1.97	7.12E-11	0.045	0.052
75.1	7.9997	2.26	2.65	1.14E-10	0.061	0.068
75.0	9.9959	3.00	3.33	8.89E-11	0.075	0.085

EXAMPLE 5

5 **Solubility of 1,1,1-2-tetrafluoroethane (HFC-134a) in 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆])**

A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 3.5 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were
 10 calculated using a one-dimensional diffusion model analysis. The initial concentration (C₀), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Tables 9a, 9b, 9c and 9d provide data for C₀, C_s, D, X_{calc.}, and X_{meas.} at
 15 temperatures of 10, 25, 50 and 75 °C, respectively.

Table 9a

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D _{eff.} (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
9.8	0.0999	0.0	0.23	4.21E-12	0.006	0.003
10.0	0.4981	0.35	2.20	6.46E-12	0.059	0.050
9.9	0.9986	2.25	5.73	5.78E-12	0.145	0.126
9.9	1.4981	5.40	9.15	1.01E-11	0.219	0.212
9.9	2.0024	9.50	13.64	1.48E-11	0.306	0.303
9.9	2.4907	14.39	19.36	2.67E-11	0.401	0.402
9.9	2.9974	20.96	27.51	5.33E-11	0.514	0.516
9.9	3.4900	--	--	--	--	0.721

Table 9b

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T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D _{eff.} (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
25.0	0.1002	--	--	--	--	0.011
24.9	0.4981	0.57	1.52	1.89E-11	0.041	0.042
25.0	0.9972	1.82	3.26	1.71E-11	0.086	0.085
25.0	1.4987	3.60	5.09	2.00E-11	0.130	0.130
25.0	1.9930	5.43	7.09	2.27E-11	0.175	0.175
24.9	2.4996	7.53	9.31	2.59E-11	0.222	0.222
25.0	2.9952	9.78	11.82	2.82E-11	0.272	0.273
24.9	3.5000	12.51	14.62	3.99E-11	0.323	0.323

Table 9c

T (°C)	P (bar)	C₀ (mass%)	C_s (mass%)	D (m²/sec)	X_{calc.} (mol. fraction)	X_{meas.} (mol. fraction)
49.9	0.0992	0.07	0.13	2.44E-11	0.004	0.004
50.0	0.4984	0.25	0.75	4.39E-11	0.021	0.021
49.9	0.9971	1.00	1.57	3.94E-11	0.043	0.043
49.9	1.4989	1.79	2.42	4.48E-11	0.064	0.065
50.0	1.9895	2.65	3.28	4.38E-11	0.086	0.086
50.0	2.4900	3.75	4.23	2.33E-11	0.110	0.108
50.0	2.9897	4.43	5.10	4.90E-11	0.130	0.130
50.0	3.4933	5.39	6.06	5.00E-11	0.152	0.152

Table 9d

T (°C)	P (bar)	C₀ (mass%)	C_s (mass%)	D (m²/sec)	X_{calc.} (mol. fraction)	X_{meas.} (mol. fraction)
75.0	0.0970	0.00	0.03	6.45E-11	0.001	0.001
74.9	0.4984	0.09	0.32	7.49E-11	0.009	0.009
74.9	0.9934	0.51	0.79	7.93E-11	0.022	0.022
74.9	1.5010	0.98	1.27	7.78E-11	0.035	0.035
75.0	1.9983	1.44	1.73	8.37E-11	0.047	0.046
75.0	2.5014	1.89	2.21	8.37E-11	0.059	0.059
75.0	3.0022	2.39	2.71	8.26E-11	0.072	0.072
75.0	3.4897	2.95	3.21	5.53E-11	0.085	0.084

EXAMPLE 6

10 Solubility of 1,1,1-trifluoroethane (HFC-143a) in 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆])

A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 7.5 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial

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concentration (C_o), final saturation concentration (C_s), and calculated solubility ($X_{calc.}$) are also provided in the table.

Tables 10a, 10b, 10c and 10d provide data for C_o , C_s , D , $X_{calc.}$, and $X_{meas.}$ at temperatures of 10, 25, 50 and 75 °C, respectively.

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Table 10a

T (°C)	P (bar)	C_o (mass%)	C_s (mass%)	D (m ² /sec)	$X_{calc.}$ (mol. fraction)	$X_{meas.}$ (mol. fraction)
11.7	0.0956	0.03	0.10	8.10E-12	0.003	0.003
12.0	0.9970	0.22	0.92	8.51E-12	0.031	0.029
11.9	1.9830	0.99	1.93	8.11E-12	0.064	0.060
12.0	2.9740	1.95	2.39	3.21E-12	0.078	0.093
12.3	3.9808	3.06	4.03	1.04E-11	0.127	0.124
12.0	4.9975	4.16	5.23	1.10E-11	0.161	0.156
12.0	5.9821	5.30	6.42	1.44E-11	0.192	0.188
12.2	6.9975	6.54	7.63	1.94E-11	0.223	0.219
12.2	7.4832	7.80	8.31	2.03E-11	0.239	0.235

Table 10b

10

T (°C)	P (bar)	C_o (mass%)	C_s (mass%)	D (m ² /sec)	$X_{calc.}$ (mol. fraction)	$X_{meas.}$ (mol. fraction)
25.0	0.0951	0.00	0.01	1.53E-11	0.001	0.004
24.9	0.9970	0.24	0.69	2.05E-11	0.023	0.023
24.9	2.0054	0.84	1.33	2.56E-11	0.045	0.042
24.9	2.9895	1.40	2.10	1.83E-11	0.069	0.068
24.9	4.0147	2.26	2.89	1.77E-11	0.093	0.090
24.9	4.9886	2.95	3.60	2.24E-11	0.114	0.112
24.9	5.9855	3.71	4.33	2.73E-11	0.136	0.134
24.9	7.0019	4.47	5.12	2.83E-11	0.157	0.155
24.9	7.5011	5.14	5.53	3.61E-11	0.169	0.165

Table 10c

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
49.9	0.1050	--	--	--	--	0.001
49.9	1.0023	0.16	0.40	4.47E-11	0.014	0.013
50.1	2.0045	0.61	0.84	3.41E-11	0.028	0.027
50.0	3.0002	1.03	1.26	2.90E-11	0.042	0.040
50.0	4.0021	1.39	1.65	5.08E-11	0.055	0.054
50.0	5.0046	1.81	2.08	4.10E-11	0.069	0.067
50.0	6.0039	2.29	2.50	3.75E-11	0.082	0.079
50.0	7.0029	2.63	2.90	5.57E-11	0.094	0.092
50.0	10.0030	3.56	4.16	5.51E-11	0.131	0.127

Table 10d

5

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
75.0	0.0995	--	--	--	--	0.001
74.9	1.0005	0.18	0.26	7.38E-11	0.009	0.009
74.8	1.9960	0.38	0.54	1.04E-10	0.018	0.018
74.9	3.0001	0.67	0.81	1.07E-10	0.028	0.027
74.9	4.0015	0.91	1.08	1.32E-10	0.037	0.036
74.9	5.0027	1.18	1.36	1.20E-10	0.045	0.044
75.0	5.9979	1.44	1.63	1.40E-10	0.054	0.053
75.0	7.0026	1.92	1.94	3.79E-09	0.064	0.061
74.9	10.0035	2.65	2.76	1.90E-09	0.089	0.083

EXAMPLE 7**Solubility of 1,1-difluoroethane (HFC-152a) in 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆])**

5 A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 4.5 bar where the solubilities ($X_{\text{meas.}}$) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_o), final saturation concentration (C_s), and calculated solubility

10 ($X_{\text{calc.}}$) are also provided in the table.

Tables 9a, 9b, 9c and 9d provide data for C_o , C_s , D , $X_{\text{calc.}}$, and $X_{\text{meas.}}$ at temperatures of 10, 25, 50 and 75 °C, respectively.

Table 11a

15

T (°C)	P (bar)	C_o (mass%)	C_s (mass%)	D (m ² /sec)	$X_{\text{calc.}}$ (mol. fraction)	$X_{\text{meas.}}$ (mol. fraction)
10.0	0.0973	--	--	--	--	0.021
10.0	0.4994	1.23	2.90	1.14E-11	0.114	0.103
10.0	0.9933	3.58	6.11	1.56E-11	0.219	0.210
10.0	1.4985	6.91	9.60	3.09E-11	0.314	0.301
9.9	2.0011	10.40	14.00	3.60E-11	0.412	0.407
9.9	2.4952	15.52	20.42	6.44E-11	0.525	0.521
9.9	3.1963	--	--	--	--	0.797

Table 11b

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
25.0	0.1002	0.16	0.66	2.00E-11	0.028	0.030
25.0	0.5006	1.02	1.92	2.01E-11	0.078	0.077
24.9	0.9982	2.34	3.55	2.64E-11	0.137	0.136
25.0	1.4924	4.20	5.35	2.89E-11	0.196	0.194
25.0	2.4969	6.74	9.52	4.96E-11	0.312	0.311
25.0	3.4818	11.59	15.05	7.73E-11	0.433	0.432
25.0	4.5051	18.83	23.81	1.04E-10	0.573	0.574

5 **Table 11c**

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
50.1	0.9921	0.03	0.15	5.73E-11	0.007	0.007
50.0	1.0017	0.88	1.46	5.52E-11	0.060	0.060
50.0	1.5020	1.63	2.22	5.94E-11	0.089	0.089
50.0	2.4969	2.72	3.81	6.43E-11	0.145	0.145
50.0	4.5051	6.31	7.33	7.88E-11	0.254	0.254

Table 11d

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
74.9	0.1032	0.04	0.11	1.38E-10	0.005	0.005
74.9	0.5019	0.19	0.42	1.25E-10	0.018	0.018
74.9	1.0023	0.57	0.84	1.21E-10	0.035	0.035
74.9	1.5014	0.99	1.27	1.25E-10	0.052	0.052
75.0	2.4964	1.63	2.12	1.42E-10	0.085	0.085
75.0	3.4970	2.57	2.98	1.48E-10	0.117	0.117
74.8	4.5003	3.51	3.89	1.21E-10	0.148	0.149

EXAMPLE 8**Solubility of difluoromethane (HFC-32) in 1-butyl-3-methylimidazolium tetrafluoroborate ([bmim][BF₄])**

5 A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 10 bar where the solubilities ($X_{\text{meas.}}$) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_0), final saturation concentration (C_s), and calculated solubility

10 ($X_{\text{calc.}}$) are also provided in the table.

Tables 12a, 12b, 12c and 12d provide data for C_0 , C_s , D , $X_{\text{calc.}}$, and $X_{\text{meas.}}$ at temperatures of 10, 25, 50 and 75 °C, respectively.

Table 12a

15

T (°C)	P (bar)	C₀ (mass%)	C_s (mass%)	D (m²/sec)	X_{calc.} (mol. fraction)	X_{meas.} (mol. fraction)
9.9	0.1002	8.35	9.20	1.76E-11	0.008	0.009
9.9	0.9985	10.08	13.74	1.72E-11	0.100	0.108
10.0	2.4995	15.10	18.94	3.29E-11	0.239	0.254
10.0	3.9954	21.28	25.08	4.53E-11	0.376	0.396
9.8	5.4992	28.16	33.17	8.48E-11	0.499	0.519
9.9	6.9988	37.79	46.86	1.08E-10	0.625	0.636
9.9	8.4966	52.61	52.61	1.01E-10	0.766	0.765

Table 12b

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
25.0	0.0969	0.01	0.15	3.37E-11	0.007	0.006
25.0	0.9968	0.59	1.81	3.36E-11	0.074	0.070
25.0	2.4955	2.75	4.79	3.70E-11	0.180	0.174
25.0	3.9989	5.87	7.95	4.62E-11	0.273	0.270
25.0	5.4977	9.23	11.36	5.98E-11	0.358	0.356
25.0	6.9955	12.90	15.12	7.44E-11	0.436	0.434
25.0	8.4945	17.08	19.33	9.10E-11	0.510	0.510
25.0	9.9985	21.83	24.46	9.94E-11	0.585	0.583

5 Table 12c

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
50.0	0.0977	0.01	0.07	8.71E-11	0.003	0.003
49.9	0.9961	0.37	0.95	7.56E-11	0.040	0.039
50.0	2.4967	1.67	2.47	7.40E-11	0.099	0.099
50.0	3.9964	3.16	4.01	8.23E-11	0.154	0.153
49.9	5.4956	4.75	5.59	8.95E-11	0.205	0.204
49.9	6.9953	6.38	7.22	9.88E-11	0.253	0.253
49.8	8.4986	8.05	8.91	1.06E-10	0.298	0.298
50.0	9.9963	9.75	10.64	1.11E-10	0.341	0.341

Table 12d

T (°C)	P (bar)	C₀ (mass%)	C_s (mass%)	D (m²/sec)	X_{calc.} (mol. fraction)	X_{meas.} (mol. fraction)
75.0	0.0971	0.0	0.03	1.26E-10	0.001	0.001
74.9	0.9956	0.26	0.54	1.28E-10	0.023	0.023
74.9	2.4948	1.03	1.40	1.25E-10	0.058	0.058
75.0	3.9950	1.92	2.27	1.22E-10	0.092	0.091
74.9	5.4951	2.75	3.14	1.45E-10	0.124	0.123
75.0	6.9955	3.64	4.03	1.59E-10	0.154	0.154
74.9	8.4964	4.54	4.94	1.42E-10	0.184	0.183
74.9	9.9994	5.44	5.82	1.89E-10	0.212	0.212

5 EXAMPLE 9

Solubility of difluoromethane (HFC-32) in 1,2-dimethyl-3-propylimidazolium tris(trifluoromethylsulfonyl)methide ([dmpim][tTFMSmethide])

A solubility and diffusivity study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 10 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C₀), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Tables 13a, 13b, 13c and 13d provide data for C₀, C_s, D, X_{calc.}, and X_{meas} at temperatures of 10, 25, 50 and 75 °C, respectively.

Table 13a

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
10.0	0.1010	0.03	0.11	1.71E-11	0.012	0.012
10.0	0.9964	0.43	1.44	1.39E-11	0.134	0.136
10.0	2.4970	2.39	4.13	2.52E-11	0.313	0.311
10.0	3.9969	5.57	7.39	5.04E-11	0.458	0.457
10.0	5.4947	9.70	11.67	8.93E-11	0.583	0.583
10.0	6.9966	15.43	17.70	1.37E-10	0.695	0.696
10.0	8.4959	24.33	28.09	1.56E-10	0.805	0.802

Table 13b

5

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
24.9	0.0998	0.01	0.09	2.71E-11	0.010	0.010
24.9	0.9997	0.42	1.01	2.52E-11	0.098	0.096
24.9	2.4956	--	--	--	--	0.225
24.9	3.9958	3.61	4.55	5.46E-11	0.336	0.335
24.9	5.4927	5.76	6.69	7.98E-11	0.432	0.431
24.9	6.9955	8.15	9.13	1.10E-10	0.516	0.515
24.9	8.4948	11.02	12.07	1.34E-10	0.593	0.593
24.9	10.0000	14.52	15.59	1.83E-10	0.662	0.662

Table 13c

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
50.0	0.0991	0.21	0.04	6.45E-11	0.004	0.004
50.0	0.9995	0.29	0.57	6.75E-11	0.058	0.057
50.0	2.4945	1.11	1.52	7.87E-11	0.141	0.141
50.0	3.9947	2.10	2.50	9.56E-11	0.213	0.213
50.0	5.4954	--	--	--	--	0.278
50.0	6.9968	--	--	--	--	0.338
50.0	8.4944	5.37	5.73	1.51E-10	0.392	0.392
50.0	9.9952	6.61	6.96	1.68E-10	0.442	0.442

Table 13d

T (°C)	P (bar)	C_o (mass%)	C_s (mass%)	D (m ² /sec)	X_{calc.} (mol. fraction)	X_{meas.} (mol. fraction)
75.0	0.0940	--	--	--	--	0.000
74.9	1.0018	0.06	0.31	6.06E-11	0.032	0.031
75.0	2.5040	0.71	0.89	1.23E-10	0.087	0.087
74.9	3.9958	1.32	1.49	1.26E-10	0.138	0.138
74.9	5.4938	1.92	2.09	1.59E-10	0.184	0.184
74.9	7.0051	2.58	2.72	1.35E-10	0.229	0.229
74.9	8.4954	3.24	3.37	1.19E-10	0.270	0.268
74.9	10.0046	3.89	4.05	2.10E-10	0.309	0.308

5 EXAMPLE 10**Solubility of difluoromethane (HFC-32) in 1-octyl-3-methylimidazolium iodide ([omim][I])**

A solubility and diffusivity study was made at a temperature of 25 °C over a pressure range from 0 to 10 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_o), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Table 14 provides data for C_o, C_s, D, X_{calc.}, and X_{meas.} at a temperature of 25 °C.

Table 14

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
25.0	0.1007	0.01	0.06	1.75E-11	0.004	0.004
25.2	1.0021	0.23	0.80	1.77E-11	0.048	0.048
25.0	2.4971	1.20	2.13	1.86E-11	0.119	0.118
25.0	3.9999	2.58	3.55	2.27E-11	0.186	0.185
25.0	5.5008	4.07	5.04	3.13E-11	0.247	0.246
25.0	6.9964	5.64	6.64	3.81E-11	0.306	0.306
25.0	8.5027	7.52	8.33	2.86E-11	0.360	0.362
25.0	10.0022	9.27	10.35	6.37E-11	0.417	0.416

5 **EXAMPLE 11**
Solubility of difluoromethane (HFC-32) in 1,3-dioctylimidazolium iodide ([doim][I])

A solubility and diffusivity study was made at a temperature of 25 °C over a pressure range from 0 to 10 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_o), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Table 15 provides data for C_o, C_s, D, X_{calc.}, and X_{meas.} at a temperature of 25 °C.

Table 15

T (°C)	P (bar)	C₀ (mass%)	C_s (mass%)	D (m ² /sec)	X_{calc.} (mol.fraction)	X_{meas.} (mol. fraction)
25.0	0.1002	0.03	0.11	1.78E-11	0.009	0.007
25.0	1.0010	0.29	0.87	2.11E-11	0.066	0.064
25.0	2.5003	1.29	2.17	2.35E-11	0.152	0.150
25.0	4.0024	2.62	3.51	2.91E-11	0.227	0.225
25.0	5.5024	4.03	4.93	3.54E-11	0.295	0.293
25.0	7.0010	5.51	6.43	4.25E-11	0.357	0.355
24.9	8.4988	7.12	8.07	5.00E-11	0.415	0.413
25.0	10.0024	8.83	9.85	5.77E-11	0.469	0.468

EXAMPLE 12

5 Solubility of difluoromethane (HFC-32) in 1-ethyl-3-methylimidazolium bis(pentafluoroethylsulfonyl)imide ([emim][bPFESimide])

A solubility and diffusivity study was made at a temperature of 25 °C over a pressure range from 0 to 10 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C₀), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Table 16 provides data for C₀, C_s, D, X_{calc.}, and X_{meas.} at a temperature of 25 °C.

Table 16

T (°C)	P (bar)	C ₀ (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
25.0	0.0956	0.03	0.11	7.46E-11	0.010	0.010
25.0	0.9970	0.71	1.22	7.95E-11	0.104	0.104
25.0	2.4959	2.49	3.19	1.09E-10	0.237	0.237
25.0	3.9961	4.61	5.33	1.31E-10	0.347	0.347
25.0	5.4925	7.03	7.75	1.57E-10	0.443	0.442
25.0	6.9931	9.70	10.49	1.83E-10	0.525	0.525
25.0	8.5025	12.87	13.71	2.07E-10	0.600	0.598
25.0	10.0050	16.49	17.56	1.66E-10	0.668	0.666

EXAMPLE 13

5 **Solubility of difluoromethane (HFC-32) in 1,2-dimethyl-3-propylimidazolium bis(trifluoromethylsulfonyl)imide ([dmpim][bTFMSimide])**

A solubility and diffusivity study was made at a temperature of 25 °C over a pressure range from 0 to 10 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C₀), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Table 17 provides data for C₀, C_s, D, X_{calc.}, and X_{meas.} at a temperature of 25 °C.

Table 17

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
24.9	0.0989	0.02	0.11	6.31E-11	0.008	0.008
25.0	0.9951	0.65	1.22	6.60E-11	0.091	0.090
25.0	2.4949	2.44	3.25	8.94E-11	0.213	0.212
25.0	3.9762	4.62	5.46	1.21E-10	0.317	0.317
25.0	5.5013	7.08	8.00	1.46E-10	0.412	0.412
25.0	7.0174	10.02	10.92	1.75E-10	0.497	0.496
25.0	8.5131	13.56	14.29	2.23E-10	0.573	0.573
25.0	10.0108	17.55	18.41	2.33E-10	0.645	0.645

EXAMPLE 14

5 **Solubility of difluoromethane (HFC-32) in 1-propyl-3-methylpyridinium
bis(trifluoromethylsulfonyl)imide ([pmpy][bTFMSimide])**

A solubility and diffusivity study was made at a temperature of 25 °C over a pressure range from 0 to 10 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance and the diffusivities (D) were calculated using a one-dimensional diffusion model analysis. The initial concentration (C_o), final saturation concentration (C_s), and calculated solubility (X_{calc.}) are also provided in the table.

Table 18 provides data for C_o, C_s, D, X_{calc.}, and X_{meas.} at a temperature of 25 °C.

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Table 18

T (°C)	P (bar)	C _o (mass%)	C _s (mass%)	D (m ² /sec)	X _{calc.} (mol. fraction)	X _{meas.} (mol. fraction)
24.9	0.0951	0.02	0.12	9.96E-11	0.010	0.010
24.9	1.0020	0.74	1.32	1.00E-10	0.097	0.096
24.9	2.5034	--	--	--	--	0.221
24.9	3.9959	4.93	5.73	1.52E-10	0.327	0.328
24.9	5.4973	7.52	8.30	1.92E-10	0.420	0.419
24.9	6.9923	10.35	11.16	2.20E-10	0.501	0.502
24.9	8.4965	13.61	14.48	2.41E-10	0.575	0.575
24.9	10.0044	17.35	18.06	6.21E-10	0.638	0.639

5 **EXAMPLE 15**
Solubility of 1,1,2,2-tetrafluoroethane (HFC-134) in 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim][PF₆])

10 A solubility study was made at temperatures of 10, 25, 50, and 75 °C over a pressure range from 0 to 3.5 bar where the solubilities (X_{meas.}) were measured using a gravimetric microbalance.

Tables 20a, 20b, 20c and 20d provide data for X_{meas} at temperatures of 10, 25, 50 and 75 °C, respectively.

Table 19a

T (°C)	P (bar)	X_{meas.} (mol. fraction)
10.0	0.010	0.031
10.0	0.500	0.189
10.0	1.000	0.377
10.0	1.500	0.541
10.0	2.000	0.683
10.0	2.500	0.788

Table 19b

5

T (°C)	P (bar)	X_{meas.} (mol. fraction)
25.0	0.100	0.024
25.0	0.500	0.116
24.9	1.000	0.225
24.9	1.500	0.330
24.9	2.000	0.428
25.0	2.500	0.522
24.9	3.000	0.611
24.9	3.500	0.689

Table 19c

T (°C)	P (bar)	X_{meas.} (mol. fraction)
50.0	0.100	0.006
50.0	0.500	0.049
50.0	1.000	0.103
50.0	1.500	0.154
50.0	2.000	0.204
50.0	2.500	0.253
50.0	3.000	0.300
50.0	3.500	0.344

Table 19d

5

T (°C)	P (bar)	X_{meas.} (mol. fraction)
74.9	0.100	0.006
75.0	0.500	0.029
75.0	1.000	0.058
75.0	1.500	0.086
75.0	2.000	0.113
75.0	2.500	0.140
75.0	3.000	0.166
75.0	3.500	0.194

10

Claims

5 What is claimed is:

1. An apparatus for temperature adjustment comprising

(a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent;

10 (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor;

(c) a condenser that receives the vapor from the generator and condenses the vapor under pressure to a liquid;

15 (d) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant;

(e) an evaporator that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form first and second portions of refrigerant vapor;

20 (f) a compressor that receives the first portion of the refrigerant vapor, increases the pressure thereof, and passes the first portion of the refrigerant vapor to the condenser; and

(g) a conduit that passes the second portion of the refrigerant vapor leaving
25 the evaporator to the absorber.

2. An apparatus for temperature adjustment comprising

(a) an absorber that forms a mixture of a mixture of a refrigerant and an absorbent;

30 (b) a generator that receives the mixture from the absorber and heats the mixture to separate refrigerant, in vapor form, from the absorbent, and increases the pressure of the refrigerant vapor;

(c) a compressor that receives the vapor from the generator and further increases its pressure;

- (d) a condenser that receives the vapor from the compressor and condenses the vapor under pressure to a liquid;
- (e) a pressure reduction device through which the liquid refrigerant leaving the condenser passes to reduce the pressure of the liquid to form a mixture of liquid and vapor refrigerant;
- (f) an evaporator that receives the mixture of liquid and vapor refrigerant that passes through the pressure reduction device to evaporate the remaining liquid to form refrigerant vapor; and
- (g) a conduit that passes the refrigerant vapor leaving the evaporator to the absorber.

3. An apparatus according to Claim 1 wherein the condenser is located in proximity to an object, medium or space to be heated.

4. An apparatus according to Claim 2 wherein the condenser is located in proximity to an object, medium or space to be heated.

5. An apparatus according to Claim 1 wherein the evaporator is located in proximity to an object, medium or space to be cooled.

6. An apparatus according to Claim 2 wherein the evaporator is located in proximity to an object, medium or space to be cooled.

7. An apparatus according to Claim 1 or 2 wherein the refrigerant is selected from one or more members of the group consisting of a hydrofluorocarbon, a hydrochlorofluorocarbon, a chlorofluorocarbon, a fluorocarbon, N₂, O₂, CO₂, NH₃, Ar, H₂, H₂O, and a non-fluorinated hydrocarbon, wherein the non-fluorinated hydrocarbon is selected from the group consisting of C₁ to C₄ straight-chain, branched or cyclic alkanes and C₁ to C₄ straight-chain, branched or cyclic alkenes.

8. An apparatus according to Claim 7 wherein a hydrofluorocarbon is selected from the group consisting of: difluoromethane (HFC-32), pentafluoroethane (HFC-125), 1,1,2,2-tetrafluoroethane (HFC-134), 1,1,1,2-

tetrafluoroethane (HFC-134a), 1,1,1-trifluoroethane (HFC-143a), 1,1-difluoroethane (HFC-152a), and fluoroethane (HFC-161).

9. An apparatus according to Claim 7 wherein a hydrochlorofluorocarbon
5 is chlorodifluoromethane (HCFC-22).

10. An apparatus according to Claim 7 wherein a chlorofluorocarbon is
dichlorodifluoromethane (CFC-12).

11. An apparatus according to Claim 7 wherein a fluorocarbon is selected
10 from the group consisting of perfluoromethane (FC-14) and perfluoroethane (FC-116).

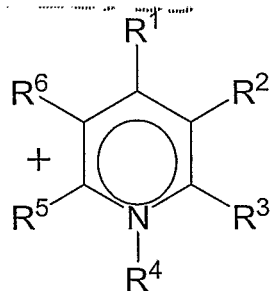
12. An apparatus according to Claim 7 wherein a non-fluorinated
15 hydrocarbon is selected from the group consisting of methane, ethane, ethylene, propane, cyclopropane, propene, propylene, butane, butene, and isobutane.

13. An apparatus according to Claim 7 wherein a refrigerant is selected
from the group consisting of HFC-32, HFC-125, HFC-134, HFC-134a, HFC-
20 143a, HFC-152a, HFC-161, HCFC-22, FC-14, FC-116, CFC-12.

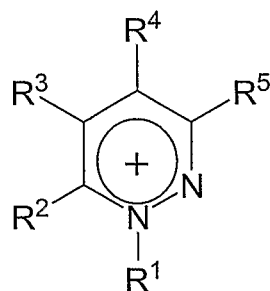
14. An apparatus according to Claim 1 or 2 wherein the absorbent
comprises one or more ionic liquids.

15. An apparatus according to Claim 7 wherein the absorbent comprises
25 one or more ionic liquids.

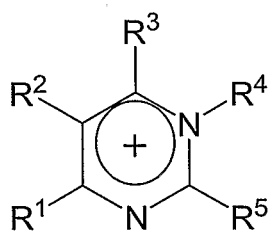
16. An apparatus according to Claim 14 wherein an ionic liquid comprises
a cation selected from the group consisting of:



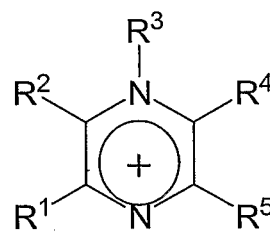
Pyridinium



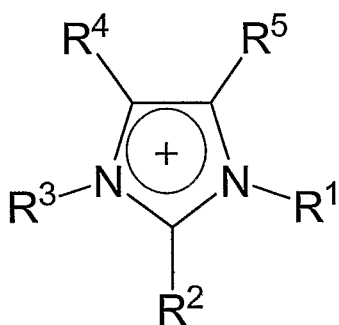
Pyridazinium



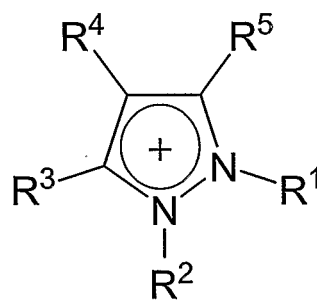
Pyrimidinium



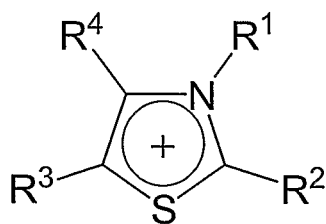
Pyrazinium



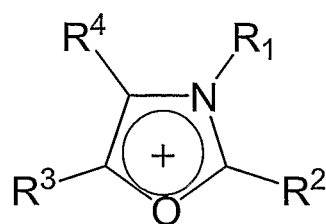
Imidazolium



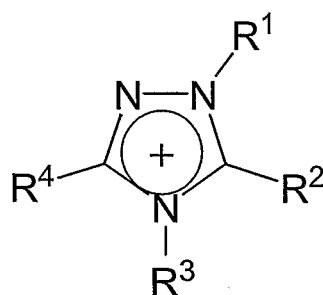
Pyrazolium



Thiazolium

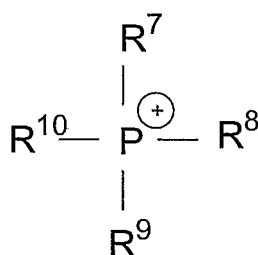


Oxazolium



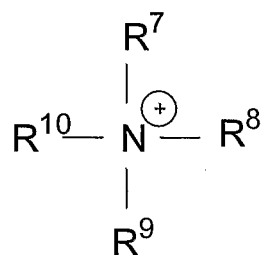
5

Triazolium



Phosphonium

and



Ammonium

10 wherein R^1 , R^2 , R^3 , R^4 , R^5 and R^6 are each independently selected from the group consisting of:

- (i) H;
- (ii) halogen;
- (iii) $-CH_3$, $-C_2H_5$, or C_3 to C_{25} straight-chain, branched or cyclic
15 alkane or alkene, optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH_2 and SH;
- (iv) $-CH_3$, $-C_2H_5$, or C_3 to C_{25} straight-chain, branched or cyclic
20 alkane or alkene comprising one to three heteroatoms selected from the group consisting of O, N, Si and S, and

optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH;

(v) C₆ to C₂₀ unsubstituted aryl, or C₃ to C₂₅ unsubstituted heteroaryl having one to three heteroatoms independently selected from the group consisting of O, N, Si and S; and

(vi) C₆ to C₂₅ substituted aryl, or C₃ to C₂₅ substituted heteroaryl having one to three heteroatoms independently selected from the group consisting of O, N, Si and S; wherein said substituted aryl or substituted heteroaryl has one to three substituents independently selected from the group consisting of:

1. -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or cyclic alkane or alkene, optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH,
2. OH,
3. NH₂, and
4. SH; and

wherein R⁷, R⁸, R⁹, and R¹⁰ are each independently selected from the group consisting of:

(vii) -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or cyclic alkane or alkene, optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH;

(viii) -CH₃, -C₂H₅, or C₃ to C₂₅ straight-chain, branched or cyclic alkane or alkene comprising one to three heteroatoms selected from the group consisting of O, N, Si and S, and optionally substituted with at least one member selected from the group consisting of Cl, Br, F, I, OH, NH₂ and SH;

(ix) C₆ to C₂₅ unsubstituted aryl, or C₃ to C₂₅ unsubstituted heteroaryl having one to three heteroatoms independently selected from the group consisting of O, N, Si and S; and

(x) C₆ to C₂₅ substituted aryl, or C₃ to C₂₅ substituted heteroaryl having one to three heteroatoms independently selected

from the group consisting of O, N, Si and S;
wherein said substituted aryl or substituted heteroaryl has
one to three substituents independently selected from the
group consisting of:

- 5 (1) $-\text{CH}_3$, $-\text{C}_2\text{H}_5$, or C_3 to C_{25} straight-chain, branched
or cyclic alkane or alkene, optionally substituted
with at least one member selected from the group
consisting of Cl, Br, F, I, OH, NH_2 and SH,
- (2) OH,
- 10 (3) NH_2 , and
- (4) SH; and

wherein optionally at least two of R^1 , R^2 , R^3 , R^4 , R^5 , R^6 , R^7 , R^8 , R^9 , and R^{10} can
together form a cyclic or bicyclic alkanyl or alkenyl group.

- 15 17. An apparatus according to Claim 16 wherein any one of, or any group
of more than one of, R^1 , R^2 , R^3 , R^4 , R^5 , R^6 , R^7 , R^8 , R^9 and R^{10} comprises F-

18. An apparatus according to Claim 14 wherein an ionic liquid comprises
an anion selected from the group consisting of $[\text{CH}_3\text{CO}_2]^-$, $[\text{HSO}_4]^-$, $[\text{CH}_3\text{OSO}_3]^-$,
20 $[\text{C}_2\text{H}_5\text{OSO}_3]^-$, $[\text{AlCl}_4]^-$, $[\text{CO}_3]^{2-}$, $[\text{HCO}_3]^-$, $[\text{NO}_2]^-$, $[\text{NO}_3]^-$, $[\text{SO}_4]^{2-}$, $[\text{PO}_4]^{3-}$,
 $[\text{HPO}_4]^{2-}$, $[\text{H}_2\text{PO}_4]^-$, $[\text{HSO}_3]^-$, $[\text{CuCl}_2]^-$, Cl^- , Br^- , I^- , SCN^- and any fluorinated anion.

19. An apparatus according to Claim 18 wherein a fluorinated anion is
selected from the group consisting of $[\text{BF}_4]^-$, $[\text{PF}_6]^-$, $[\text{SbF}_6]^-$, $[\text{CF}_3\text{SO}_3]^-$,
25 $[\text{HCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{HFCCF}_2\text{SO}_3]^-$, $[\text{HCClFCF}_2\text{SO}_3]^-$, $[(\text{CF}_3\text{SO}_2)_2\text{N}]^-$,
 $[(\text{CF}_3\text{CF}_2\text{SO}_2)_2\text{N}]^-$, $[(\text{CF}_3\text{SO}_2)_3\text{C}]^-$, $[\text{CF}_3\text{CO}_2]^-$, $[\text{CF}_3\text{OCFHCF}_2\text{SO}_3]^-$,
 $[\text{CF}_3\text{CF}_2\text{OCFHCF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{CFHOCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_2\text{HCF}_2\text{OCF}_2\text{CF}_2\text{SO}_3]^-$,
 $[\text{CF}_2\text{ICF}_2\text{OCF}_2\text{CF}_2\text{SO}_3]^-$, $[\text{CF}_3\text{CF}_2\text{OCF}_2\text{CF}_2\text{SO}_3]^-$, $[(\text{CF}_2\text{HCF}_2\text{SO}_2)_2\text{N}]^-$,
 $[(\text{CF}_3\text{CFHCF}_2\text{SO}_2)_2\text{N}]^-$, and F^- .

- 30 20. An apparatus according to Claim 7 wherein the absorbent comprises
one or more ionic liquids, and a refrigerant comprises from about 0.05 to about
99.95 mole percent of the mixture of refrigerant and absorbent over a temperature

range from the evaporator temperature to the generator temperature at a pressure from vacuum to the critical pressure.

21. An apparatus according to Claim 1 or 2 wherein the mixture of
5 refrigerant and absorbent comprises an additive selected from the group consisting of lubricants, corrosion inhibitors, stabilizers and dyes.

22. An apparatus according to Claim 1 or 2 that is fabricated as a
refrigerator, a freezer, an ice machine, an air conditioner, an industrial cooling
10 system, heater or heat pump.

23. A process for adjusting the temperature of an object, medium or a
space comprising

- (a) absorbing refrigerant vapor with an absorbent to form a mixture;
- 15 (b) heating the mixture to separate refrigerant, in vapor form, from the absorbent and increase the pressure of the refrigerant vapor;
- (c) condensing the refrigerant vapor under pressure to a liquid;
- (d) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form first and second portions of refrigerant vapor;
- 20 (e-1) mechanically increasing the pressure of the first portion of refrigerant vapor, and then repeating step (c) to subject the first portion of refrigerant vapor to condensation to liquid; and
- (e-2) repeating step (a) to re-absorb, with the absorbent, the second portion of refrigerant vapor.

25

24. A process according to Claim 23 wherein, in step (c), the refrigerant vapor is condensed to a liquid in proximity to the object, medium or space to heat the object, medium or space.

30 25. A process according to Claim 23 wherein, in step (d), liquid refrigerant is evaporated to form refrigerant vapor in proximity to the object, medium or space to cool the object, medium or space.

26. A process for adjusting the temperature of an object, medium or a space comprising
- (a) absorbing refrigerant vapor with an absorbent to form a mixture;
 - (b) heating the mixture to separate refrigerant, in vapor form, from the
 - 5 absorbent and increase the pressure of the refrigerant vapor;
 - (c) further increasing the pressure of the refrigerant vapor mechanically;
 - (d) condensing the refrigerant vapor under pressure to a liquid;
 - (e) reducing the pressure of the liquid refrigerant, and evaporating the refrigerant to form refrigerant vapor; and
 - 10 (f) repeating step (a) to re-absorb the refrigerant vapor with the absorbent.
27. A process according to Claim 26 wherein, in step (d), the refrigerant vapor is condensed to a liquid in proximity to the object, medium or space to heat the object, medium or space.
- 15 28. A process according to Claim 26 wherein, in step (e), liquid refrigerant is evaporated to form refrigerant vapor in proximity to the object, medium or space to cool the object, medium or space.
- 20 29. A process according to Claim 23 or 26 wherein the absorbent separated from refrigerant in step (b) is recirculated for use in a later step.
- 25 30. A process according to Claim 23 or 26 wherein the refrigerant comprises one or more members of the group consisting of a hydrofluorocarbon, a hydrochlorofluorocarbon, a chlorofluorocarbon, a fluorocarbon, N₂, O₂, CO₂, NH₃, Ar, H₂, H₂O, and a non-fluorinated hydrocarbon, wherein the non-fluorinated hydrocarbon is selected from the group consisting of C₁ to C₄ straight-chain, branched or cyclic alkanes and C₁ to C₄ straight-chain, branched or cyclic alkenes.
- 30 31. A process according to Claim 23 or 26 wherein the absorbent comprises one or more ionic liquids.

32. A process according to Claim 30 wherein the absorbent comprises one or more ionic liquids.