

DESCRIPTION

WATER TREATMENT MEMBRANE WASHING APPARATUS AND
WATER TREATMENT MEMBRANE WASHING METHOD

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Technical field

[0001] The present application relates to washing apparatus for water treatment membrane and methods of washing water treatment membrane.

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Background Art

[0002] In a water treatment system such as for drinking water, sewage water, or various waste water, membrane separation using water treatment membrane is employed as a method of removing
15 suspended solids and bacteria. While such a water treatment system separates suspended solids and filtrate by filtering water to be treated through a separation membrane, continuous membrane treatment entails adhesion of the suspended solids inside and on the surface of the water treatment membrane and this may
20 sometimes lead to clogging of pores formed in the water treatment membrane. When the pores of the water treatment membrane are clogged, since separation performance is reduced owing to increase of pressure difference across the membrane or reduction of the amount of filtrate, the inside or the surface of the water treatment
25 membrane needs to be washed to remove the suspended solids.

[0003] The method of washing water treatment membrane is generally backwashing, in which a washing liquid is supplied from the secondary side (filtrate side) of the water treatment
5 membrane to the primary side (raw water side) thereof to washing the inside of and the surface of the water treatment membrane. While there are various washing liquid, water or oxidizing agent solution such as sodium hypochlorite solution is used for backwashing. Furthermore, in order to obtain a higher washing
10 effect, ozone water (ozone-dissolved water) exhibiting a high oxidizability is used in some cases (see, for example, Patent Document 1).

Prior Art Document

15 Patent Document

[0004] Patent Document 1: JP2001-70761 A (FIG. 1)

Summary of the Invention

Problem that the Invention is to Solve

20 [0005] In a traditional washing of water treatment membrane using ozone water, a washing method has been employed in which ozone gas is directly injected into the filtrate filtered through the water treatment membrane and the water treatment membrane is washed after the dissolved ozone concentration reaches a pre-given
25 value. The filtrate filtered through the water treatment

membrane, however, contains a trace quantity of substances, such as low molecular organic substances, that react with ozone. For that reason, although the ozone gas is directly injected into the filtrate, the substances react early with the ozone, thus reducing the ratio of the amount of ozone dissolved in the filtrate to the amount of injected ozone gas. This results in increasing the amount of required ozone gas to be injected in generating the ozone water, thus leading to a problem of increasing the running cost for ozone gas generation.

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[0006] The present application discloses a technology for resolving the above-described problem, and aimed at providing a water treatment membrane washing apparatus that has a high utilization efficiency of ozone gas and further aimed at reducing the capacity of a unit for disposal of exhaust ozone gas and at preventing initial costs from increasing by reusing waste ozone gas generated in generating the ozone water.

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Means for Solving the Problem

[0007] A water treatment membrane washing apparatus disclosed in the present application uses an ozone water generated by dissolving ozone gas in a filtrate generated by filtering a raw water through a water treatment membrane and includes: an ozone gas supply unit configured to generate an ozone gas; a first ozone dissolving tank and a second ozone dissolving tank configured to

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store the filtrate; a first aspirator configured to aspirate an ozone gas using as a driving water a filtrate circulated from the first ozone dissolving tank and to mix the filtrate with the ozone gas supplied from the ozone gas supply unit; a second aspirator
5 configured to aspirate an ozone gas using as a driving water a filtrate circulated from the second ozone dissolving tank and to mix the filtrate with a waste ozone gas generated in the first ozone dissolving tank; and a switching valve configured to switch a supply destination from one of the gas aspirators to the other of the
10 gas aspirators, wherein an ozone gas containing filtrate stored in the second ozone dissolving tank or in the first ozone dissolving tank is passed from the secondary side of the water treatment membrane to the primary side of the water treatment membrane to wash the water treatment membrane.

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Advantage Effect of the Invention

[0008] According to the present application, a water treatment membrane washing apparatus can be provided that has a high utilization efficiency of ozone gas. Moreover, by reusing waste
20 ozone gas to generate ozone water, a unit for disposal of exhaust ozone gas can be reduced in capacity and initial costs can be prevented from increasing.

Brief Description of the Drawings

25 [0009]

FIG. 1 is a schematic diagram showing a whole configuration of a water treatment system according to Embodiment 1;

FIG. 2 is a process flowchart showing a water treatment membrane washing method according to Embodiment 1;

5 **FIG. 3** is a schematic diagram showing a whole configuration of a water treatment system according to Embodiment 2;

FIG. 4 is a schematic diagram showing a whole configuration in a state during backwashing, of the water treatment system according to Embodiment 2;

10 **FIG. 5** is a schematic diagram showing a whole configuration in another state, of the water treatment system according to Embodiment 2 in another state; and

FIG. 6 is a schematic diagram showing a whole configuration of a water treatment system according to Embodiment 3.

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Embodiments for Carrying Out the Invention

Embodiment 1

[0010] Embodiment 1 is described below with reference to **FIG. 1**.

FIG. 1 is a schematic diagram showing the whole configuration of a water treatment system according to Embodiment 1. **FIG. 1** shows a state of the water treatment system in a treatment process of a raw water. The water treatment system **100** includes a membrane separation tank **1** having therein a separation membrane **2**, which is a water treatment membrane for separating suspended solids from a raw water such as drinking water, sewage water, or various

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waste water; a washing apparatus **10** for washing the separation
membrane **2**, i.e., a water treatment membrane washing apparatus
10; and a filtration pump **3** for sucking the raw water to be filtered
through a membrane separation tank **1** through the separation
5 membrane **2**.

[0011] The water treatment membrane washing apparatus **10**
includes an ozone gas supply unit **20**; an ozone dissolving tank **4** for
temporarily storing a filtrate generated by filtering the raw water
10 through the separation membrane; an ozone water generating tank
5 for temporarily storing a pretreated filtrate generated in the
ozone dissolving tank **4**; and an exhaust ozone gas decomposition
column **19** for disposal of an exhaust ozone gas generated in the
ozone dissolving tank **4**. The ozone dissolving tank **4** and the
15 ozone water generating tank **5** are the same in capacity, and are
provided with circulation pumps **8**, **9** and circulation pipes **14**, **15**
for circulating the water in the respective tanks. The circulation
pipes **14**, **15** are provided with gas aspirators **6**, **7** driven by flow
momentum of the circulated flows, respectively.

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[0012] The ozone gas supply unit **20** is made up of a source gas
supply (not shown) and an ozonizer (not shown) for generating an
ozone gas from oxygen supplied from the source gas supply. The
source gas supply uses, for example, a liquid oxygen tank or an
25 oxygen generator utilizing such as vacuum pressure swing

adsorption (APSA), but is not particularly limited to those as long as the source gas supply is able to supply oxygen. The ozonizer may use, for example, a discharge ozonizer.

5 [0013] The ozone gas supply unit **20** is connected via an ozone gas pipe **17** to the gas aspirator **7** provided for the ozone water generating tank **5**. The gas aspirator **7** is provided to the discharge side of the circulation pump **9** and connected to the circulation pipe **15** to aspirate the ozone gas supplied from the
10 ozone gas supply unit **20** using the circulated flow from the circulation pumps **9**, to mix the ozone gas with the circulated water.

[0014] The ozone water generating tank **5** is connected from an upper gas phase space therein via a waste ozone gas aspiration pipe
15 **12** to the gas aspirator **6** provided for the ozone dissolving tank **4**. Similarly, the gas aspirator **6** is also provided to the discharge side of the circulation pump **8** and connected to the circulation pipe **14** to aspirate a waste ozone gas generated in the ozone water generating tank **5** and accumulated in the gas phase space therein using the
20 circulated flow from the circulation pumps **8**, to mix the waste ozone gas with the circulated water.

[0015] The circulation pipe **14** connected to the ozone dissolving tank **4** branches to a pretreated filtrate pipe **13** at a three way valve
25 **34a** provided to the discharge side of the circulation pump **8** and is

connected to the ozone water generating tank **5**. The circulation pipe **15** connected to the ozone water generating tank **5** also branches to a filtrate pipe **21** at a three way valve **34b** provided to the discharge side of the circulation pump **9** and is connected to a backwash water pipe **18**. The filtrate pipe **21** is provided with a differential pressure gauge **23** for measuring the pressure difference across the membrane during the filtration. The circulation pipes **14**, **15** each have an ozone concentration meter (not shown) attached upstream to the gas aspirators **6**, **7** to measure dissolved ozone concentrations in the tanks, respectively.

[0016] The exhaust ozone gas decomposition column **19** is connected with an upper gas phase space in the ozone dissolving tank **4** via a pipe, and the exhaust ozone gas decomposition column **19** is packed with a catalyst, an activated carbon, or the like for reducing the ozone to oxygen. The exhaust ozone gas decomposition column **19** has an atmosphere exhaust pipe **16** connected downstream thereto.

[0017] Next, an operation of the water treatment washing apparatus is described. **FIG. 2** is a process flowchart showing a water treatment membrane washing method according to Embodiment 1. The water treatment membrane washing method according to Embodiment 1 includes four steps: a pretreated filtrate transporting step (Step *ST01*), a filtrate receiving step

(Step *ST02*), an ozone gas supplying step (Step *ST03*), and an ozone water backwashing step (Step *ST04*). Each step is described below.

5 [0018] In Embodiment 1, the waste ozone gas is supplied from the upper gas phase space in the ozone water generating tank 5 into the filtrate in the ozone dissolving tank 4 with the ozone gas being supplied from the ozone gas supply unit 20 into the pretreated filtrate in the ozone water generating tank 5 in the ozone gas
10 supplying step (Step *ST03*).

[0019] Here, assuming a state in which an ozone gas containing filtrate generated in the ozone water generating tank 5 has been supplied to the separation membrane 2 to backwash the membrane
15 and the backwashing is finished, the ozone dissolving tank 4 is filled with the pretreated filtrate dissolving the ozone and the ozone water generating tank 5 is in an evacuated state of the ozone gas containing filtrate.

20 [0020] The pretreated filtrate transporting step (Step *ST01*) is started from this state. To be more specific, in the pretreated filtrate transportation step (Step *ST01*), the pretreated filtrate stored in the ozone dissolving tank 4 reduced in organic substance concentration and pH lower than those of the filtrate from the
25 separation membrane by mixing of the filtrate with the waste ozone

gas in the later-described ozone gas supply step (Step *ST03*), is transported to the ozone water generating tank **5** through the pretreated filtrate pipe **13** by the circulation pump **8**. The flow path on the discharge side of the circulation pump **8** is switched to the pretreated filtrate pipe **13** using the three way valve **34a**.
When the entire pretreated filtrate stored in the ozone dissolving tank **4** is transported to the ozone water generating tank **5**, the pretreated filtrate transportation step is finished.

[0021] Next, the filtrate receiving step (Step *ST02*) is described. While the filtrate filtered through the separation membrane **2** is usually flowing out by the filtrate pump **3** to the outside of the water treatment system **100** through the filtrate pipe **11**, the flow path of the filtrate in filtrate receiving step is switched by three way valve **22**, which is a flow path switching value, from the usual path through the filtrate pipe **11** to a path to the ozone dissolving tank **4** for the filtrate to be transported thereto. When the water level in the ozone dissolving tank **4** reaches nearly its full level (about a level more than 80% of the full level; the same applies below), the flow path is switched by the three way valve **22** to transport the filtrate to the outside of the water treatment system **100**.

[0022] Next, the ozone gas supplying step (Step *ST03*) is described. The flow paths of the circulation pumps **8**, **9** provided for the

respective tanks are switched to the circulation pipes **14, 15** by the three way valves **34a, 34b**, and then the circulation pumps **8, 9** are started to circulate the stored filtrates in the respective tanks through the gas aspirators **6, 7**. Utilizing flow momentum of the circulated flows from the circulation pumps **8, 9**, the gas aspirators **6** reduces pressure of the gas phase space in the ozone water generating tank **5** by aspiration and the gas aspirator **7** reduces pressure by aspirating the ozone gas from the ozone gas supply unit **20**.

[0023] After the flow rates of the circulation pumps **8, 9** stabilizes, the ozone gas is supplied to the gas aspirator **7** from the ozone gas supply unit **20** through the ozone gas pipe **17**. The supplied ozone gas is mixed in the gas aspirators **7** with the pretreated filtrate, which serves as driving water, circulated from the ozone water generating tank **5**. Part of the ozone gas is dissolved in the pretreated filtrate and the rest thereof remains as an undissolved ozone gas, and the pretreated filtrate is returned in a gas-liquid multiphase flow state to the lower liquid phase portion in the ozone water generating tank **5** through the circulation pipe **15**.

[0024] The undissolved ozone gas in the liquid phase portion in the ozone water generating tank **5** moves upward in a bubble state, while being in contact with the pretreated filtrate in the tank, to the upper gas phase space in the ozone water generating tank **5**.

The undissolved ozone gas moved to the upper space in the ozone water generating tank **5** is reduced in pressure by being aspirated by the gas aspirator **6** and mixed in the gas aspirator **6** with the filtrate circulated from the ozone dissolving tank **4** by the circulation pump **8**. Part of the ozone gas is dissolved in the filtrate and reacts with organic substances in the filtrate, to thereby be converted to oxygen.

[0025] Part of the organic substances reacted with the ozone are oxidized to organic acids, to reduce pH of the stored filtrate in the tank. It is known that the decomposition rate of dissolved ozone decreases with reducing pH. Accordingly, pH reduction due to generation of the organic acids contributes to reduction of the ozone gas supply time required for obtaining a desired value, in other words, a pre-given value of dissolved ozone concentration and to increase of the dissolved-ozone concentration.

[0026] The rest of the ozone gas, on the other hand, remains as an dissolved ozone gas in the filtrate and is returned in a gas-liquid multiphase flow state (the gas is the undissolved ozone gas and the liquid is the filtrate) to the liquid phase portion in the ozone dissolving tank **4** through the circulation pipe **14**. The undissolved ozone gas remaining in the liquid phase portion in the ozone dissolving tank **4** moves upward in a bubble state to the upper gas phase space in the ozone dissolving tank **4** while being in contact

with the filtrate in the ozone dissolving tank. The gas phase space in the ozone dissolving tank **4** is reduced in pressure such as by a blower (not shown) provided to the atmosphere exhaust pipe **16**. The ozone gas moving upward to the gas phase space is sucked and
5 decomposed to oxygen by adsorptive reduction such as by the catalyst or the activated carbon in the exhaust ozone gas decomposition column **19**, to be exhausted in the atmosphere through the atmosphere exhaust pipe **16**.

10 [0027] When the dissolved ozone concentration in the stored filtrate in the ozone water generating tank **5** reaches the pre-given value, the ozone gas supplying step is finished. Since the effect of washing the separation membrane **2** becomes larger with increasing dissolved ozone concentration, the pre-given value is
15 preferably set close to the saturation solubility as possible. However, since the saturation solubility of ozone varies depending on temperature and pH of solvent, and atmospheric pressure, the pre-given value may be set at a fixed value of, for example, 30 mg/l or more to keep constant the dissolved ozone concentration for each
20 washing. Otherwise, by calculating beforehand an ozone gas supply time that brings the dissolved ozone concentration to the pre-given value, the ozone gas supply time instead of the pre-given value may be set in an actual ozone gas supplying step.

25 [0028] When the dissolved ozone concentration of the stored

filtrate in the ozone water generating tank **5** reaches the pre-given value and the pressure measured by the differential pressure gauge **23** increases from that at the start of the filtration to a predetermined pressure, the process proceeds to the ozone water backwashing step (Step *ST04*). In the backwashing step, the ozone gas supply from the ozone gas supply unit **20** is stopped and the circulation pump **8** provided to the ozone dissolving tank **4** is stopped, and then the flow path from the discharge side of the circulation pump **9** provided to the ozone water generating tank **5** is switched from the circulation pipe **15** to the backwash water pipe **18** by the three way valve **34b**.

[0029] The ozone gas containing filtrate having the pre-given concentration is supplied by the circulation pump **9** as a backwash water from the secondary side (filtrate side) of the water treatment membrane **2** to the primary side (raw water side) thereof, to wash the inside of the membrane, when passing through the membrane, by dissolving impurities such as organic suspended substances clogging inside the membrane by oxidizing power of the dissolved ozone. The ozone gas containing filtrate after used in the washing is passed to the primary side (raw water side).

[0030] In the backwashing, the pressure of the ozone gas containing filtrate supplied by the circulation pump **9** is preferably no higher than 300 kPa to avoid the breakage of the separation

membrane **2**. In addition, the washing of the separation
membrane **2** usually takes about 30 minutes although depending on
the size of the separation membrane **2** and the degree of clogging.
After the backwashing for a predetermined time, the circulation
5 pump **9** is stopped, and the ozone water backwashing step is
finished.

[0031] As described above, according to Embodiment 1, the
pretreated filtrate generated in the ozone dissolving tank **4** by
10 reacting with the waste ozone gas and transported to the ozone
water generating tank **5** in the last batch process is used to
generate the ozone gas containing filtrate, to be more specific, the
two ozone dissolving tanks are provided, and the ozone gas
containing filtrate is generated from the pretreated filtrate reacted
15 with the waste ozone gas and transported to a first one of the ozone
dissolving tanks in the last batch process, by supplying ozone gas
from the ozone gas supply unit, and at the same time, the
pretreated filtrate for generating the ozone gas containing filtrate
to be used in the next batch process is generated from the filtrate
20 transported to a second one of the ozone dissolving tanks by
reacting with the waste ozone gas from the first ozone dissolving
tank. This enables the ozone gas containing filtrate to be
generated from the pretreated filtrate previously reacted with the
waste ozone gas, thus being able to reduce ozone consumption due
25 to reaction with organic substances in the ozone gas containing

filtrate and being able to provide a water treatment membrane washing apparatus having a high utilization efficiency of ozone gas. Moreover, the waste ozone gas is reused to generate the pretreated filtrate, thus being able to reduce the capacity of the decomposition
5 column for disposal of the exhaust ozone gas and to prevent initial costs from increasing.

Embodiment 2

[0032] While Embodiment 1 described the water treatment system
10 100 that supplies the ozone gas only to one of the ozone dissolving tanks and aspirates the waste ozone gas only from the other ozone dissolving tank, Embodiment 2 describes in detail below a water treatment system 100 that can switch supply destinations of the ozone gas and the waste ozone gas by providing respective
15 switching valves to the ozone gas pipe 17 and the waste ozone gas aspiration pipe 12 to branch and supply the ozone gas and the waste ozone gas to either tanks.

[0033] FIG. 3 shows a specific example of a water treatment
20 system according to Embodiment 2. In the figure, the switching valves indicate by solid marks are in the closed state and the switching valves indicate by open marks are in the open state. Among the three flow paths in the three way valves 34a, 34b, each flow path connecting to the backwash water pipe 18, which is to be
25 used in the ozone water backwashing step, is in the closed state

here. It should be noted that Embodiment **2** described below is an example, but not limited to that.

[0034] **FIG. 3** shows the open/closed state of each switching valve
5 in the ozone gas supplying step (Step *ST03*) shown in **FIG. 2**. The
ozone gas supplied from the ozone gas supply unit **20** is aspirated
by a gas aspirator **6a** after flowing through the ozone gas pipe **17**
and branching through an ozone gas switching valve **33a**. The
ozone gas is mixed in the gas aspirator **6a** with the stored filtrate
10 circulated from an ozone dissolving tank **4a**. Part of the ozone gas
is dissolved in the stored filtrate and the rest thereof remains as an
undissolved ozone gas, and is returned in a gas-liquid multiphase
flow state to the liquid phase portion in the ozone dissolving tank
4a through a circulation pipe **14a**. The remaining undissolved
15 ozone gas moves upward in a bubble state to the gas phase space
therein.

[0035] The undissolved waste ozone gas accumulated in the upper
gas phase space in the ozone dissolving tank **4a** is aspirated by a
20 gas aspirator **6b** through a waste ozone gas aspiration pipe **12a** via
a waste ozone gas switching valve **31a** and a waste-ozone-gas inlet
switching valve **32b**. The stored filtrate circulated from an ozone
dissolving tank **4b** is mixed with the aspirated waste ozone gas in a
gas aspirator **6b** and is returned to the liquid phase portion in the
25 ozone dissolving tank **4b** through a circulation pipe **14b**.

[0036] After mixed, the undissolved ozone gas accumulated in the gas phase space in the ozone dissolving tank **4b** is sucked by a suction device, such as the blower (not shown), provided to the atmosphere exhaust pipe **16** from the upper gas phase space in the ozone dissolving tank **4b** to the exhaust ozone gas decomposition column **19** through a waste ozone gas suction pipe **12b** via an inlet valve **30b** for the exhaust ozone gas decomposition column.

[0037] When the dissolved ozone concentration of the stored filtrate in the ozone dissolving tank **4a** reaches the pre-given value and the pressure measured by the differential pressure gauge **23** increases from that at the start of the filtration to the predetermined pressure, the process proceeds to the ozone water backwashing step (Step *ST04*). In this step, two of the three flow paths in the three way valve **34a** are opened as shown in **FIG. 4** to supply the ozone gas containing filtrate in the ozone dissolving tank **4a** to the secondary side of the separation membrane **2** by the circulation pump **8a**, to wash the membrane. After washing for the predetermined time, the circulation pump **8a** is stopped and the ozone water backwashing step (Step *ST04*) is finished. In addition, the ozone gas switching valve **33a** and an ozone gas switching valve **33b** are closed during this step.

[0038] While Embodiment 1 described that the pretreated filtrate

transporting step (Step *ST01*) is started after the ozone water backwashing step (Step *ST04*), in embodiment 2, since the ozone dissolving tank **4b** is used as the ozone water generating tank **5** of Embodiment 1 and the ozone dissolving tank **4a** is used as the ozone
 5 dissolving tank **4** of Embodiment 1 in the ozone gas supplying step (Step *ST03*) in the next batch process, the pretreated filtrate transporting step (Step *ST01*) can be omitted. In the filtrate receiving step (Step *ST02*), the three way valve **22** is switched to the washing apparatus **10**, and the switching valve **35a** is opened
 10 and a switching valve **35b** is closed to transport the filtrate filtered through the separation membrane **2** to the ozone dissolving tank **4a** by the filtration pump **3**.

[0039] In the ozone gas supplying step (Step *ST03*), the ozone gas
 15 is supplied to the ozone dissolving tank **4b** storing the pretreated filtrate reduced in organic substance concentration and pH by being mixed beforehand with the waste ozone gas in the last batch process by inverting the state of each switching valve shown in **FIG. 3** to the state shown in **FIG. 5** (in this case, a circulation pump **8b**,
 20 the waste ozone gas switching valve **31b**, and the waste-ozone-gas inlet switching valve **32a** are used). This allows for reducing the amount of ozone supply required to obtain the ozone gas containing filtrate having the pre-given ozone concentration. Also during the ozone gas supplying step, the waste ozone gas generated in the
 25 ozone dissolving tank **4b** is aspirated and mixed with the filtrate as

with the last batch by the gas aspirator **6a** provided for the ozone dissolving tank **4a**.

[0040] As described above, according to Embodiment **2**, since the
5 supply destinations of the ozone gas and the waste ozone gas can be
changed, in other words, the ozone gas containing filtrate can be
directly supplied from either tanks to the separation membrane, it
is no need to supply the ozone gas every time when the pretreated
filtrate mixed with the waste ozone gas is transported to the other
10 tank as in the pretreated filtrate transporting step in Embodiment
1. Thus, according to Embodiment **2**, time to complete generation
of the ozone gas containing filtrate can be reduced and the running
cost can be reduced.

15 Embodiment **3**

[0041] While, in Embodiments **1**, **2**, the water treatment system
100 is configured such that the ozone gas is supplied only to one of
the ozone dissolving tanks and the waste ozone gas is aspirated
from the other ozone dissolving tank by the gas aspirators **6**, **7**
20 utilizing such as an ejector, in Embodiment **3**, a water treatment
system is configured such that the ozone gas is dissolved using
diffuser plates without using the gas aspirators **6**, **7**. The water
treatment system **100** with such a water treatment membrane
washing apparatus is described in detail below.

[0042] **FIG. 6** shows a specific example of a water treatment system according to Embodiment 3. In the figure, the switching values indicate by solid marks are in the closed state and the switching values indicate by open marks are in the open state. It should be noted that Embodiment 3 described below is an example, but not limited to that.

[0043] **FIG. 6** shows the open/closed state of the three way valve 22 in the ozone gas supplying step (Step *ST03*) described using **FIG.**

2. The ozone gas from the ozone gas supply unit 20 is supplied to a diffuser plate 50 (also referred to as a first diffuser plate 50; the same applies hereafter) through the ozone gas pipe 17. The ozone gas discharges in a (fine) bubble state from the diffuser plate 50 into the pretreated filtrate in the ozone dissolving tank 4b and is mixed therewith. Part of the ozone gas is dissolved in the pretreated filtrate, and the rest thereof remains in a gas state and is accumulated as the waste ozone gas in the gas phase space in the ozone dissolving tank 4b. The pressure of the accumulated waste ozone gas increases gradually with the amount of ozone gas supplied and exceeds the pressure exerted on a diffuser plate 40 (also referred to as a second diffuser plate 40; the same applies hereafter) by the filtrate stored in the ozone dissolving tank 4a, whereby the accumulated waste ozone gas finally discharges from the diffuser plate 40.

[0044] When the dissolved ozone concentration of the stored filtrate in the ozone dissolving tank **4b** reaches the pre-given value and the pressure measured by the differential pressure gauge **23** increases from that at the start of the filtration to the predetermined pressure, the process proceeds to the ozone water backwashing step (Step *ST04*). In this step, the ozone gas containing filtrate in the ozone dissolving tank **4b** is supplied to the secondary side of the separation membrane **2** by a backwash pump **25**, to backwash the separation membrane. After backwashing for the predetermined time, the backwash pump **25** (a backwash pump **24** too if the water treatment membrane washing apparatus of Embodiment **3** is configured as same as Embodiment **2**) is stopped, and the ozone water backwashing step (Step *ST04*) is finished. The aforementioned circulation pumps are relatively large because they need to generate the driving water for the gas aspirators **6**, **7** to aspirate the ozone gas and the waste ozone gas by utilizing such as ejector and operates for a relatively extended period in aspirating the waste ozone gas. In contrast to this, the backwash pumps **24**, **25** may be smaller pumps and this is different point from the circulation pumps. Even using the smaller pumps, they are sufficiently capable of washing the water treatment membrane and only need to run for a relatively short period of about 30 minutes in the backwashing.

[0045] As described above, according to Embodiment **3**, the ozone

gas can be dissolved using the diffuser plates. This eliminates the need of the circulation flows for driving the gas aspirators **6, 7** used in the water treatment systems of Embodiments **1, 2**, thus being able to omit the circulation pipes **14, 15** and the circulation pump **9**.

5 Thus, if there is a restriction in the installation space for the system or the running cost of the washing apparatus is desired to be prevented from increasing due to use of large circulation pumps, Embodiment **3** has an advantage over Embodiments **2, 3**.

10 [0046] It should be noted that each embodiment may be combined or appropriately modified or omitted.

Reference Numerals

[0047]

15 **1**: membrane separation tank;
2: separation membrane;
3: filtration pump;
4, 4a, 4b: ozone dissolving tank;
5: ozone water generating tank;
20 **6, 6a, 6b**: gas aspirator;
7: gas aspirator;
8, 8a, 8b: circulation pump;
9: circulation pump;
10: washing apparatus;
25 **11**: filtrate pipe;

- 12, 12a, 12b: waste ozone gas aspiration pipe;
- 13: pretreated filtrate pipe;
- 14, 14a, 14b: circulation pipe;
- 15: circulation pipe;
- 5 16: atmosphere exhaust pipe;
- 17: ozone gas pipe;
- 18: backwash water pipe;
- 19: exhaust ozone gas decomposition column;
- 20: ozone gas supply unit;
- 10 21: filtrate pipe;
- 22, 34a, 34b: three way valve;
- 23: differential pressure gauge;
- 24, 25: backwash pump;
- 30a, 30b: inlet valve for exhaust-ozone-gas decomposition column;
- 15 31a, 31b: waste ozone gas switching valve;
- 32a, 32b: waste ozone gas inlet switching valve;
- 33a, 33b: ozone gas switching valve; and
- 100: water treatment system.

CLAIMS

1. A water treatment membrane washing apparatus that uses an
5 ozone water generated by dissolving ozone gas in a filtrate
generated by filtering a raw water through a water treatment
membrane, the water treatment membrane washing apparatus
comprising:

an ozone gas supply unit configured to generate and supply an
10 ozone gas;

a first ozone dissolving tank and a second ozone dissolving tank
configured to store the filtrate;

a first aspirator configured to aspirate an ozone gas using as a
driving water a filtrate circulated from the first ozone dissolving
15 tank and to mix the stored filtrate with the ozone gas supplied from
the ozone gas supply unit;

a second aspirator configured to aspirate an ozone gas using as
a driving water a filtrate circulated from the second ozone
dissolving tank and to mix the stored filtrate with a waste ozone
20 gas generated in the first ozone dissolving tank; and

a switching valve configured to switch a supply destination
from one of the gas aspirators to the other of the gas aspirators,
wherein an ozone gas containing filtrate generated in the second
ozone dissolving tank or in the first ozone dissolving tank is passed
25 from the secondary side of the water treatment membrane to the

primary side of the water treatment membrane to wash the water treatment membrane.

2. The water treatment membrane washing apparatus of claim 1,
5 wherein the ozone gas containing filtrate stored in the first ozone dissolving tank includes the ozone gas containing filtrate transported from the second ozone dissolving tank.

3. The water treatment membrane washing apparatus of claim 1
10 or claim 2, wherein the ozone gas containing filtrate for washing the water treatment membrane has a pre-given dissolved ozone concentration.

4. The water treatment membrane washing apparatus of any one
15 of claims 1 to 3, wherein the ozone gas containing filtrate for washing the water treatment membrane is reduced in organic substances and pH compared with the filtrate from the raw water.

5. A water treatment membrane washing apparatus that uses an
20 ozone water generated by dissolving ozone gas in a filtrate generated by filtering a raw water through a water treatment membrane, the water treatment membrane washing apparatus comprising:

an ozone gas supply unit configured to generate and supply an
25 ozone gas;

a first ozone dissolving tank and a second ozone dissolving tank configured to store the filtrate;

a first diffuser plate configured to discharge in a bubble state the ozone gas supplied from the ozone gas supply unit into a stored
5 filtrate in the first ozone dissolving tank, to dissolve the ozone gas in the stored water in the first ozone dissolving tank;

a second diffuser plate configured to discharge in a bubble state a waste ozone gas accumulated in a gas phase space in the first ozone dissolving tank into a stored filtrate in the second
10 dissolving tank, to dissolve the waste ozone gas in the stored water in the second dissolving tank;

a differential pressure gauge configured to measure a pressure difference across the water treatment membrane during a filtration; and

15 a backwash pump configured to pass the filtrate through the water treatment membrane,

wherein when a dissolved ozone concentration of the stored filtrate in the first ozone dissolving tank reaches a pre-given value and a pressure measured by the differential pressure gauge increases
20 from a pressure at a start of the filtration to a predetermined pressure, an ozone gas containing filtrate generated in the first ozone dissolving tank is passed by the backwash pump from the secondary side of the water treatment membrane to the primary side of the water treatment membrane to wash the water treatment
25 membrane.

6. A water treatment membrane washing method that uses an ozone water generated by dissolving ozone gas in a filtrate generated by filtering a raw water through a water treatment
5 membrane and uses a water treatment membrane washing apparatus including an ozone gas supply unit configured to generate and supply an ozone gas; a first ozone dissolving tank and a second ozone dissolving tank configured to store the filtrate; a first aspirator configured to aspirate an ozone gas using as a
10 driving water a stored filtrate circulated from the first ozone dissolving tank to mix the stored filtrate with the ozone gas supplied from the ozone gas supply unit, and to return an ozone gas containing filtrate to the first ozone dissolving tank; a second aspirator configured to mix a stored filtrate circulated from the
15 second ozone dissolving tank with a waste ozone gas generated in the first ozone dissolving tank and to return a generated ozone gas containing filtrate to the second ozone dissolving tank; and a switching valve configured to switch a supply destination from one of the gas aspirators the other of the gas aspirators, the water
20 treatment membrane washing method comprising steps of:

 sending the waste ozone gas generated in one of the two ozone dissolving tanks to other of the ozone dissolving tanks;

 storing as an ozone gas containing filtrate in the other dissolving tank after mixing the filtrate from the raw water with
25 the waste ozone gas;

passing the stored ozone gas containing filtrate from the secondary side of the water treatment membrane to a primary side of the water treatment membrane to wash the water treatment membrane.

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7. The water treatment membrane washing method of claim 6, wherein the water treatment membrane is washed using the stored ozone gas containing filtrate having a pre-given dissolved ozone concentration.

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8. The water treatment membrane washing method of claim 6, wherein the washing of the water treatment membrane uses the stored ozone gas containing filtrate reduced in organic substances and pH compared with the filtrate from the raw water.

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9. The water treatment membrane washing method of any one of claims 6 to 8, wherein the washing of the water treatment membrane uses the ozone gas containing filtrate stored in either one of the first ozone dissolving tank or the second ozone dissolving tank.

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10. A water treatment membrane washing method that uses an ozone water generated by dissolving ozone gas in filtrate generated by filtering a raw water through a water treatment membrane and uses a water treatment membrane washing apparatus including an

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ozone gas supply unit configured to generate an ozone gas; a first ozone dissolving tank and a second ozone dissolving tank configured to store the filtrate; a first diffuser plate configured to discharge in a bubble state the ozone gas supplied from the ozone gas supply unit into a stored filtrate in the first ozone dissolving tank, to dissolve the ozone gas in the stored water in the first ozone dissolving tank; a second diffuser plate configured to discharge in a bubble state a waste ozone gas accumulated in a gas phase space in the first ozone dissolving tank into a stored filtrate in the second dissolving tank, to dissolve the waste ozone gas in the stored water in the second dissolving tank; a differential pressure gauge configured to measure a pressure difference across the water treatment membrane during the filtration; and a backwash pump configured to pass the filtrate through the water treatment membrane, the water treatment membrane washing method comprising steps of:

driving the backwash pump based on the pressure measured by the differential pressure gauge; and

passing an ozone gas containing filtrate generated in the first ozone dissolving tank from the secondary side of the water treatment membrane to a primary side of the water treatment membrane to wash the water treatment membrane.