

PROCESS FOR THE PREPARATION OF ODOUR-LEAN POLYETHER
POLYOLS

5 The present invention relates to a process for the preparation of substantially odour-lean polyether polyols from a polyether polyol starting product, which has been obtained by polymerizing at least one alkylene oxide in the presence of a suitable polymerization catalyst.

Methods for preparing polyether polyols, also sometimes referred to as poly(alkylene oxide) polyols, are well known in the art. Typically, such methods involve reacting a starting compound having a plurality of active hydrogen atoms with one or more alkylene
10 oxides, such as ethylene oxide, propylene oxide, butylene oxide or mixtures of two or more of these. Suitable starting compounds include polyfunctional alcohols, generally containing 2 to 6 hydroxyl groups. Examples of
15 such alcohols are glycol, such as diethylene glycol, dipropylene glycol, glycerol, di- and polyglycerols, pentaerythritol, trimethylolpropane, triethanolamine, sorbitol, mannitol, etc. Usually a strong base like potassium hydroxide is used as a catalyst in this type of
20 reaction.

The polyether polyols obtained from the type of process described above as well as polyurethane foams manufactured from these polyether polyols usually suffer from a rather unpleasant odour. Although this odour does
25 not adversely affect the chemical properties of the polyether polyol in any way, it would be desirable when polyether polyols could be provided not having such unpleasant odour. Since consumers have become more and more critical over the years, there is an increasing need
30 for providing odour-lean products. Particularly in those



applications where people come in close contact with polyurethane foams (e.g. in mattresses and pillows), the odour of the foam could be a problem. Since relatively large amounts of polyols are used in the manufacture of flexible polyurethane foams, it could be expected that at least some of the unpleasant odour of the polyurethanes stems from the polyols.

The present invention therefore aims to provide a method for reducing the odour of polyether polyols manufactured as alkylene adducts of polyfunctional alcohols, substantially as described above.

Accordingly, the present invention relates to a process for the preparation of an odour-lean polyether polyol from a polyether polyol starting product which is obtained by reacting a starting compound having a plurality of active hydrogen atoms with one or more alkylene oxides, which process comprises the steps of:

- (a) contacting the neutralised or unneutralised polyether polyol product with an excess of an acid having a pKa of less than 5, preferably of less than 3, under hydrolysis conditions,
- (b) contacting the reaction mixture with water under hydrolysis conditions, and
- (c) recovering the odour-lean polyether polyol.

Without wishing to be bound by any particular theory it is believed that components which are for a large part responsible for the short term chemical odour of polyether polyols are aldehydes, present as such or in a latent form as alkenyl ether endgroups of the polyether polyol, while the long term musty odour of polyurethane foams is due to ether-like compounds -presumably cyclic ethers- formed during the polyol manufacturing, i.e. during the alkoxylation (so normally under basic conditions). Examples of such cyclic ethers could be 2-ethyl-4,7-dimethyl-1,3,6-trioxacyclo-octane and

2,5,8-trimethyl-1,4,7-trioxacyclononane. In the case of propylene oxide, for instance, the short term chemical odour is considered to be caused by propionaldehyde and propenylether end groups of the polyether polyol. For the sake of convenience, the odour causing compounds in case propylene oxide is used as the alkylene oxide will be further referred to in this patent application. It will, however, be understood that if other alkylene oxides are used, the odour-causing compounds will vary accordingly.

In step (a) of this process the propenylether end groups are removed from the neutralised (i.e. the polyol end product after working-up) or unneutralised (i.e. the polyol end product as it leaves the reactor prior to working-up) polyether polyol by hydrolysis, thus resulting in propionaldehyde and a hydroxyl end group in the polyether polyol. In subsequent or simultaneous step (b) water is added in order to hydrolyse the cyclic ethers present, e.g. into propionaldehyde and dipropylene glycol. In step (c), finally, the odour-lean polyol is recovered. This recovery suitably involves several treatments, including dewatering and steam or nitrogen stripping to remove the propionaldehyde formed as one of the hydrolysis products in steps (a) and (b), as will be discussed hereinafter.

It is preferred within the context of the present invention that the polyether polyol starting product is obtained by polymerizing propylene oxide and optionally ethylene oxide. Nevertheless, other alkylene oxides may be used as well.

The acid to be used in step (a) of the present process in principle may be any water-soluble acid having a pKa less than 5, preferably of less than 3. The acid may be an organic or mineral acid. Examples of suitable organic acids are para-toluene sulphonic acid and acetic acid. Examples of suitable mineral acids include

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sulphuric acid, hydrochloric acid, nitric acid and phosphoric acid. It has been found particularly useful to use para-toluene sulphonic acid or phosphoric acid (H_3PO_4). A combination of both acids may also be suitably used. Para-toluene sulphonic acid was found to be particularly suitable when steps (a) and (b) are carried out simultaneously, whereas phosphoric acid is advantageously used when carrying out steps (a) and (b) successively.

If step (a) is carried out before step (b), the acid is suitably added in the form of a concentrated solution in water, for instance in a concentration of 50-90%. In addition, further water may also be added. The acid should be used in such amount so as to impart sufficient acidity to the reaction medium to allow the hydrolysis reactions in steps (a) and (b) to proceed. In practice the term "excess" in relation to the acid added in step (a) refers to such amount of acid that the amount of free acid will be between 0.001 and 0.5 mole acid per kg polyether polyol, preferably between 0.005 and 0.2 mole acid per kg polyether polyol. The expression "free acid" as used herein refers to the acid which has not reacted with any component present in the reaction medium. For instance, if unneutralised polyether polyol is used as the starting material in step (a) of the present process, potassium ions from the KOH initiator will be present in the polyol. The anion of the acid added will then first react with the potassium ions. Only after the potassium ions have been "neutralised", any acid added will be present as free acid.

The conditions under which the hydrolysis in step (a) is carried out may vary within wide limits. In general, the hydrolysis conditions can be varied within limits known by the person skilled in the art. It has been found particularly advantageous to carry out step (a) at a

temperature of 80 to 130 °C, preferably 100 to 120 °C, at any arbitrary pressure ranging from essentially 0 bar up to 15 bar, preferably from 0.1 to 5 bar. If step (a) is carried out in vacuo, then the vacuum should be broken
5 once step (a) is finished. The time necessary to carry out the reaction in step (a) may also vary within wide limits. Depending on the amount of excess acid used and the temperatures applied, the length of step (a) if carried out before step (b) will normally vary from
10 several minutes to several hours, suitably from 10 minutes to 5 hours. It is preferred that while step (a) is carried out continuous mixing of the components takes place to ensure optimum contact between the reactants.

15 In step (b) of the present process water is added to the reaction mixture. The water is necessary to hydrolyse the cyclic ethers. Water can be added either in excess or in an equivalent or even lower amount. The term "excess" as used in this connection refers to such amount that a
20 two-phase system can be formed, i.e. an amount of water that exceeds the solubility of water in the particular polyol to be treated under the process conditions applied. When equivalent or lower amounts of water are added, no separate water-phase is formed, i.e. the amount
25 of water added does not exceed the solubility of water in the polyol under the conditions applied.

If an excess of water is added this eventually results in a two-phase system: an organic phase containing the polyol and part of the free acid and a
30 water/acid phase. It is believed that in such a system the cyclic ethers, which initially are present in the organic phase, are extracted into the water/acid phase, where they are hydrolysed. If no excess of water is used, but only an equivalent or even lower amount, no separate
35 water/acid phase will be formed. Step (b) can be carried

out after step (a) or simultaneous with step (a). In the first case step (b) involves contacting the reaction product of step (a) with water (suitably an excess of water), whilst in the latter case excess acid and water (suitably in such amount that a one-phase system is formed) are simultaneously added to the neutralised or unneutralised polyether polyol starting product. As indicated herein before, the water is believed to hydrolyse the cyclic ethers present in the polyol. The amount of water added should be sufficient to hydrolyse the cyclic ethers present. The conditions under which step (b) are carried out may vary within broad limits. For an optimum result, however, it has been found advantageous to let the hydrolysis reaction take place at a temperature of 80 to 130 °C, preferably 100 to 120 °C, at any arbitrary pressure. Again, the reaction time is not particularly critical, but should be long enough to allow the hydrolysis reaction to be as complete as possible. Normally, the reaction time will vary from about 10 minutes to 10 hours, suitably from 15 minutes to 4 hours. It is preferred that while step (b) is carried out continuous mixing of the components takes place to ensure optimum contact between the reactants. If steps (a) and (b) are carried out simultaneously, the conditions under which both steps are carried out will be the same.

Step (c) of the present process, recovery of the odour-lean polyether polyol, can be carried out in different ways. Generally, the recovery will include treatments to ensure that the reaction products of steps (a) and (b) and the excess of water and acid still present in the reaction mixture are removed. In a preferred embodiment step (c) comprises the following subsequent stages:

- (i) neutralisation,
- (ii) optionally dewatering,
- (iii) steam stripping, and
- (iv) drying and filtration.

5 The neutralisation involves adding a base to the
reaction mixture to increase the pH. Useful bases are
water-soluble, strong bases, such as potassium hydroxide,
sodium hydroxide and the like. The use of potassium
hydroxide is preferred. The base may be added in one or
10 more stages. Suitably, a first batch of base is added
under continuous mixing and after some time (e.g.
10 minutes to 1 hour) the remainder of base is added to
get the pH at the desired level. Neutralisation is
suitably carried out at approximately the same
15 temperature as applied in step (b) to avoid unnecessary
loss of energy and to ensure a good neutralisation.

 Dewatering, i.e. the removal of water from the
reaction system can be carried out in ways known in the
art, for example, by carrying out the dewatering at
20 atmospheric conditions, possibly in combination with a
vacuum dewatering treatment.

 Steam stripping and/or nitrogen stripping takes place
to remove substantially all the hydrolysis products
formed in steps (a) and (b) from the polyether polyol.
25 Hot steam and/or nitrogen is introduced into the
optionally dewatered polyether polyol to strip off these
hydrolysis products. In case the polyether polyol is
based on propylene oxide, the main hydrolysis product is
propionaldehyde. The pressure applied may vary over a
30 broad range and normally will be between 0.01 and 10 bar,
although higher pressures may be applied as well. In
general, any steam stripping technique and/or nitrogen
stripping technique can be applied, but for the purpose
of the present invention it is preferred to work at

subatmospheric conditions, more particularly at a pressure of 0.05 to 0.5 bar.

5 The polyether polyol product remaining after the removal of the hydrolysis products (i.e. mainly propionaldehyde) is finally dried and filtered to obtain the odour-lean polyether polyol.

The invention is further illustrated by the following examples.

Example 1

10 A 5 litre reactor equipped with a stirrer was charged with 3000 g unneutralised polyether polyol (MW 3500, containing 0.24% wt potassium). While stirring under a slight nitrogen flow, the charge was heated to 110 °C and 31.4 g 75 %wt H₃PO₄ (a 30% excess relative to potassium)
15 was added. The reaction mixture was maintained at 110 °C during 60 minutes. Then 352 g water was added and stirring was continued for 60 minutes at 110 °C. The reaction mixture was neutralised with 6.2 g 50% wt KOH during 30 minutes at 110 °C. The temperature was raised
20 to 120 °C and the reaction mixture was dried and volatiles were stripped off at 120 °C at a final pressure of 100 mbara using nitrogen as stripping gas. Crystals were filtered off.

25 The final product contained 0.2 mmol propenylether end groups per kg, which is a reduction of 98%. The musty odour initially observed for the unneutralised polyether polyol could no longer be detected. This was illustrated by comparative GC/MS analysis showing a 99% reduction of cyclic ether (2-ethyl-4,7-dimethyl-1,3,6-trioxacyclo-
30 octane and 2,5,8-trimethyl-1,4,7-trioxacyclononane) compared with the polyol intake. The propionaldehyde content was less than 1 ppm. The product was considered odour lean.

Example 2

A 1 litre reactor equipped with a stirrer was charged with 491 g unneutralised polyether polyol (MW 3500, containing 0.24% wt K). While stirring under a slight nitrogen flow, the charge was heated to 90 °C and 7.5 g para-toluene sulphonic acid monohydrate (a 30% excess relative to K) dissolved in 59.1 g water was added. The reaction mixture, which consists of a dispersion of the water phase in polyol, was maintained at 90 °C during 2 hours.

The reaction mixture was neutralised with 1.05 g 50 %wt KOH during 30 minutes at 90 °C. The temperature was raised to 120 °C and the final mixture was dried and volatiles were stripped off at 120 °C at a final pressure of 100 mbara using nitrogen as stripping gas. Crystals were filtered off.

The final product contained 0.1 mmol propenylether end groups per kg, which is a reduction of 99%. The musty odour initially observed for the unneutralised polyether polyol could no longer be detected. This was illustrated by comparative GC/MS analysis showing a 99% reduction of cyclic ether (2-ethyl-4,7-dimethyl-1,3,6-trioxacyclo-octane and 2,5,8-trimethyl-1,4,7-trioxacyclononane) compared with the polyol intake. The propionaldehyde was less than 1 ppm. The product was considered odour lean.

Example 3

A 1 litre reactor equipped with a stirrer was charged with 473 g unneutralised polyether polyol (MW 3500, containing 0.24 %wt K). While stirring under a slight nitrogen flow, the charge was heated to 90 °C and 7.2 g para-toluene sulphonic acid monohydrate (a 30% excess relative to K) dissolved in 3.7 g water was added. The reaction mixture, which is a homogeneous liquid mixture of excess para toluene sulphonic acid dissolved in polyol

and a solid phase of K-salt of said acid, was maintained at 90 °C during 2 hours.

5 The reaction mixture was neutralised with 1.01 g 50 %wt KOH during 30 minutes at 90 °C. The temperature was raised to 120 °C and the final mixture was dried and volatiles were stripped off at 120 °C at a final pressure of 100 mbara using nitrogen as stripping gas. Crystals were filtered off.

10 The final product contained 0.1 mmol propenylether end groups per kg, which is a reduction of 99%. The musty odour initially observed for the unneutralised polyether polyol could no longer be detected. This was illustrated by comparative GC/MS analysis showing a 96% reduction of cyclic ether (2-ethyl-4,7-dimethyl-1,3,6-trioxacyclo-
15 octane and 2,5,8-trimethyl-1,4,7-trioxacyclononane) compared with the polyol intake. The propionaldehyde was less than 1 ppm. The product was considered odour lean.
Comparative example 1

20 The procedure of Example 1 was repeated except that the addition of 352 g water was omitted.

The final product contained 0.2 mmol propenylether end groups per kg, which is a reduction of 98%. The level of cyclic ether (2-ethyl-4,7-dimethyl-1,3,6-trioxacyclo-
25 octane and 2,5,8-trimethyl-1,4,7-trioxacyclononane), however, was reduced by only 50% compared with the polyol intake, established by comparative GC/MS analysis. The propionaldehyde was less than 1 ppm. The product smelled musty, which is considered to be attributable to the presence of cyclic ethers.

C L A I M S

1. Process for the preparation of an odour-lean polyether polyol from a polyether polyol starting product which is obtained by reacting a starting compound having a plurality of active hydrogen atoms with one or more alkylene oxides, which process comprises the steps of:
- 5 (a) contacting the neutralised or unneutralised polyether polyol product with an excess of an acid having a pKa of less than 5, preferably of less than 3, under hydrolysis conditions,
- 10 (b) contacting the reaction mixture with water under hydrolysis conditions, and
- (c) recovering the odour-lean polyether polyol.
2. Process according to claim 1, wherein steps (a) and (b) are carried out simultaneously.
- 15 3. Process according to claim 1, wherein steps (a) and (b) are carried out consecutively.
4. Process according to any one of claims 1 to 3, wherein the acid used in step (a) is phosphoric acid and/or para-toluene sulphonic acid.
- 20 5. Process according to any one of claims 1 to 4, wherein in step (b) an excess of water is added.
6. Process according to any one of claims 1 to 4, wherein in step (b) such amount of water is added that a one-phase system is formed.
- 25 7. Process according to any of the claims 1 to 6, wherein in step (a) the amount of acid added is between 0.001 and 0.5 mole acid per kg polyether polyol.