**[0025c]** In a further aspect of the present disclosure, there is provided a use of an adsorbent as described herein, in processes for:

- separation of cuts of C8-aromatic isomers and notably of xylenes,
- separation of isomers of substituted toluene,
- separation of cresols,
- separation of polyhydric alcohols.

**[0025d]** In yet another aspect of the present disclosure, there is provided a method for separating *para*-xylene from cuts of aromatic isomers with 8 carbon atoms, using, as agent for adsorption of *para*-xylene, a zeolitic adsorbent comprising barium and/or potassium having a large external surface area characterized by nitrogen adsorption greater than 20 $m^2.g^{-1}$, employed in liquid-phase processes, but also in gas-phase processes.

**[0025e]** In a further aspect of the present disclosure, there is provided a method for separating polyhydric alcohols, using an adsorbent as described herein.

**[0025f]** In another aspect of the present disclosure, there is provided a method for separating isomers of substituted toluene, using an adsorbent as described herein.

**[0025g]** In yet another aspect of the present disclosure, there is provided a method for separating cresols using an adsorbent as described herein.

d) additional optional cationic exchange of the agglomerates from step c) by bringing into contact with a solution of potassium ions;

e) washing and drying the agglomerates obtained in steps c) or d), at a temperature between 50°C and 150°C; and

f) obtaining the zeolitic adsorbent according to the invention by activation of the agglomerates obtained in step e) while flushing with oxidizing and/or inert gas, at a temperature between 100°C and 400°C, for a time determined as a function of the desired water content and loss on ignition.

**12.** Method according to Claim 11, wherein said at least one FAU type zeolite has an Si/Al atomic ratio between 1.00 and 1.50, inclusive.

**13.** Use of an adsorbent according to any one of Claims 1 to 10 in processes for:

- separation of cuts of C8-aromatic isomers and notably of xylenes,
- separation of isomers of substituted toluene,
- separation of cresols,
- separation of polyhydric alcohols.

**14.** Use according to Claim 13, for separating *para*-xylene from cuts of aromatic isomers with 8 carbon atoms.

**15.** Method for separating *para*-xylene from cuts of aromatic isomers with 8 carbon atoms, using, as agent for adsorption of *para*-xylene, a zeolitic adsorbent comprising barium and/or potassium having a large external surface area characterized by nitrogen adsorption greater than 20 $m^2.g^{-1}$, employed in liquid-phase processes, but also in gas-phase processes.

**16.** Method according to Claim 15, using a zeolitic adsorbent according to any one of Claims 1 to 10 as the agent for adsorption of *para*-xylene.

**17.** Method according to Claim 15 or Claim 16, for separating *para*-xylene from cuts of isomers of aromatic hydrocarbons containing 8 carbon atoms, in the liquid phase, by adsorption of *para*-xylene by means of an adsorbent according to any one of Claims 1 to 10 in the presence of a desorbent.

**18.** Method according to any one of Claims 15 to 17, of the simulated moving-bed type.

**19.** Method for separating polyhydric alcohols, using an adsorbent according to any one of Claims 1 to 10.

**20.** Method for separating isomers of substituted toluene, using an adsorbent according to any one of Claims 1 to 10.

**21.** Method for separating cresols using an adsorbent according to any one of Claims 1 to 10.