

2000 07040-5
1805/1



PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau

INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

<p>(51) International Patent Classification ⁶ : F01N 3/08, B01J 19/08</p>	<p>A1</p>	<p>(11) International Publication Number: WO 99/67510</p> <p>(43) International Publication Date: 29 December 1999 (29.12.99)</p>		
<table style="width: 100%; border: none;"> <tr> <td style="width: 50%; vertical-align: top; padding: 5px;"> <p>(21) International Application Number: PCT/GB99/01912</p> <p>(22) International Filing Date: 16 June 1999 (16.06.99)</p> <p>(30) Priority Data: 9813482.8 24 June 1998 (24.06.98) GB</p> <p>(71) Applicant (for all designated States except US): AEA TECHNOLOGY PLC (GB/GB); 329 Harwell, Didcot, Oxfordshire OX11 0RA (GB).</p> <p>(72) Inventors; and (75) Inventors/Applicants (for US only): NG, Ka, Lok (GB/GB); 8 Harwich Close, Lower Barley, Reading, Berkshire RG6 3UD (GB). WEEKS, David, Michael (GB/GB); 60 Blandy Avenue, Southmoor, Abingdon, Oxfordshire OX13 5DB (GB).</p> <p>(74) Agents: WOOD, Paul, Austin et al.; AEA Technology plc, Patents Dept., 329 Harwell, Didcot, Oxfordshire OX11 0RA (GB).</p> </td> <td style="width: 50%; vertical-align: top; padding: 5px;"> <p>(81) Designated States: AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).</p> <p>Published <i>With international search report.</i></p> </td> </tr> </table>			<p>(21) International Application Number: PCT/GB99/01912</p> <p>(22) International Filing Date: 16 June 1999 (16.06.99)</p> <p>(30) Priority Data: 9813482.8 24 June 1998 (24.06.98) GB</p> <p>(71) Applicant (for all designated States except US): AEA TECHNOLOGY PLC (GB/GB); 329 Harwell, Didcot, Oxfordshire OX11 0RA (GB).</p> <p>(72) Inventors; and (75) Inventors/Applicants (for US only): NG, Ka, Lok (GB/GB); 8 Harwich Close, Lower Barley, Reading, Berkshire RG6 3UD (GB). WEEKS, David, Michael (GB/GB); 60 Blandy Avenue, Southmoor, Abingdon, Oxfordshire OX13 5DB (GB).</p> <p>(74) Agents: WOOD, Paul, Austin et al.; AEA Technology plc, Patents Dept., 329 Harwell, Didcot, Oxfordshire OX11 0RA (GB).</p>	<p>(81) Designated States: AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).</p> <p>Published <i>With international search report.</i></p>
<p>(21) International Application Number: PCT/GB99/01912</p> <p>(22) International Filing Date: 16 June 1999 (16.06.99)</p> <p>(30) Priority Data: 9813482.8 24 June 1998 (24.06.98) GB</p> <p>(71) Applicant (for all designated States except US): AEA TECHNOLOGY PLC (GB/GB); 329 Harwell, Didcot, Oxfordshire OX11 0RA (GB).</p> <p>(72) Inventors; and (75) Inventors/Applicants (for US only): NG, Ka, Lok (GB/GB); 8 Harwich Close, Lower Barley, Reading, Berkshire RG6 3UD (GB). WEEKS, David, Michael (GB/GB); 60 Blandy Avenue, Southmoor, Abingdon, Oxfordshire OX13 5DB (GB).</p> <p>(74) Agents: WOOD, Paul, Austin et al.; AEA Technology plc, Patents Dept., 329 Harwell, Didcot, Oxfordshire OX11 0RA (GB).</p>	<p>(81) Designated States: AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).</p> <p>Published <i>With international search report.</i></p>			
<p>(54) Title: THE OPTIMISATION OF GAS FLOW IN REACTORS FOR THE TREATMENT OF GASEOUS MEDIA</p> <div style="text-align: center; margin: 20px 0;"> </div> <p>(57) Abstract</p> <p>A reactor for the processing of a gaseous medium including a cylindrical reactor chamber (300) within which there is a hollow cylindrical bed of active material (303), and the annular space (311) between the outside (305) of the bed of active material and the reactor chamber (300) is arranged to provide an impedance to axial gas flow which increases in the direction of gas flow along the said annular spaces.</p>				

The Optimisation of Gas Flow in Reactors for the
Treatment of Gaseous Media

The present invention relates to reactors for the
5 treatment of gaseous media and, more specifically to
reactors for the removal of noxious substances from the
exhaust gases from internal combustion engines.

One type of reactor for the treatment of gaseous
10 media consists of a cylindrical reactor chamber which has
inlet and outlet ports by means of which it can be
connected into a gas flow system. Inside the reactor
chamber, and co-axial within it, is a hollow cylindrical
gas permeable bed of active material. The bed of active
15 material is held in place by two supporting disks made of
an impermeable material. One support disk has a ring of
axially directed holes around its periphery and the other
disk has a central hole the diameter of which is
approximately equal to the inside diameter of the
20 cylindrical bed of active material. In use a gaseous
medium to be processed is admitted to the reactor chamber
via the port closer to the first support disk. The
gaseous medium is then directed into the annular space
between the outside of the cylindrical bed of active
25 material and the wall of the reactor chamber. The
closure of this space by the other support disk
constrains the gaseous medium to pass radially through
the bed of activate material prior to leaving the reactor
via the central electrode. The support disks are made of
30 a temperature resistant insulating material and there is
provided an electrical connection to the inner electrode
by means of which a potential of some kilovolts can be
applied to the inner electrode so as to establish a
plasma discharge in the gaseous medium in the interstices
35 in the gas permeable bed of active material.



In practice, it has been found that the gas flow distribution through the bed of active material of such a reactor is uneven, being greater at the downstream end of the bed of active material. Thus the reactor may not
5 operate at its maximum efficiency because the upstream end of the bed of active material may be underused while the downstream end of the bed of active material may be subjected to a higher rate of gas flow than it can usefully process.

10

It is an object of the present invention to provide an improved reactor of the type described above for the processing of a gaseous medium.

15 According to the present invention there is provided a reactor for the treatment of a gaseous medium, including a cylindrical reactor chamber having an inlet port and an outlet port for a gaseous medium to be processed, a hollow cylindrical gas permeable bed of an
20 active material contained within the reactor chamber and substantially co-axial therewith, an annular space between the outside of the bed of active material and the inside of the reactor chamber and means for constraining the gaseous medium to enter the said annular space at one
25 end in an axial direction, the other end of said annular space being closed to axial flow of gaseous medium therefrom, the gaseous medium passing radially through the bed of active material, wherein the said annular space is configured to provide an impedance to the flow
30 of the gaseous medium which increases along the length of the said annular space in the direction from the said one end towards the said other end.

The increasing impedance to the axial flow of the
35 gaseous medium through the said annular space preferably is provided by progressively reducing the cross-sectional



area of the said annular space. The reduction in the cross-sectional area of the said annular space may be continuous, but preferably is discontinuous. A preferred arrangement has two step reductions in the cross-
5 sectional area of the said annular space, the first being greater than the second.

According to the present invention in a particular aspect the reactor is for the plasma-assisted treatment
10 of gaseous media, the bed of active material is contained between two gas permeable co-axial disks and two support disks made of an impermeable temperature-resistant insulating material, the support disk nearer the inlet end of the reactor has a plurality of axially directed
15 gas passages around its periphery, and the support disk nearer the outlet end of the reactor has a central hole the diameter of which is substantially equal to the internal diameter of the inner electrode so that a gaseous medium to be processed enters the annular space
20 between the outer electrode and the wall of the reactor chamber axially but is constrained to pass radially through the bed of active material.

Preferably the active material is adapted to remove
25 nitrogenous oxides and carbonaceous combustion products from the exhaust emissions from internal combustion engines.

The invention will now be described, by way of example,
30 with reference to the accompanying drawings, in which:

Figure 1 is a schematic longitudinal section of an existing type of reactor for the plasma-assisted processing of a gaseous medium;

- 4 -

Figure 2 illustrates how the radial component of gas flow through a bed of active material included in the reactor of Figure 1 varies with distance along the reactor bed from the entrance to the active region of the reactor;

Figure 3 is a schematic longitudinal half-section of a first reactor embodying the invention for the processing of a gaseous medium;

Figure 4 is a schematic longitudinal half-section of a second reactor embodying the invention for the processing of a gaseous medium;

Figure 5 is a schematic longitudinal half-section of a third reactor embodying the invention for the processing of a gaseous medium;

Figure 6 is a flow diagram showing the radial components of gas flow for the embodiment of Figure 3;

Figure 7 is a flow diagram showing the radial component of gas flow for the embodiment of Figure 4;

Figure 8 is a flow diagram showing the radial component of gas flow for the embodiment of Figure 5; and

Figure 9 is a schematic longitudinal half-section of a fourth embodiment of the invention.

Referring to Figure 1, a reactor 1 for the plasma-assisted processing of a gaseous medium consists of a stainless chamber 2 which has an inlet stub 3 and an outlet stub 4. The chamber 2 is arranged, in use, to be connected to an earthing point 5. Perforated cylindrical stainless steel electrodes 6 and 7 and positioned co-

- 5 -

axially within the chamber 2 by means of two impervious electrically-insulating supports 8 and 9. The space 10 bounded by the electrodes 6 and 7 and the insulating supports is filled with a bed 11 of pellets 12 of an active material which has a dielectric constant sufficient to enable a plasma to be established and maintained in the gaseous medium in the interstices between the pellets 12 of the bed 11 of active material. The upstream end 13 of the inner electrode 6 is closed off and arranged to be connected via an insulating feedthrough 14 to a source 15 of an electrical potential sufficient to excite the above-mentioned plasma in the gaseous medium.

15 The upstream electrode support 8 has a ring of axially-oriented gas passages 16 around its periphery, whereas the downstream electrode support 9 has a central hole 17 in it of approximately the same diameter as the internal diameter of the inner electrode 6. Thus, in use, a gaseous medium to be processed is directed axially into the annular space 18 between the outer electrode 7 and the wall of the chamber 2. As the gas cannot escape from the downstream end of the space 18, it is constrained to enter the bed 11 of active material and pass radially through it.

Figure 2 is a flow diagram showing how the radial component of gas flow for such a reactor varies along the length of the bed of active material. It can be seen that there is very little radial flow through the bed 11 for almost half its length and the radial gas flow increases progressively along the remainder of the bed 11 of active material. Thus, the overall efficiency of the bed 11 of active material is much below that which would be achieved if the radial flow of gas through the bed 11 of the reactor was regular. At present the active

material at the downstream end of the reactor may be saturated while that at the upstream end of the reactor largely is unused.

5 The present invention seeks to overcome this problem by progressively increasing the resistance to axial flow along the annular space 18 between the wall 2 of the reactor 1 and the outer electrode. Figures 3, 4 and 5 illustrate three ways in which this increase in the
10 resistance to axial flow of the gaseous medium can be achieved.

Unlike Figure 1, these figures are half-sections and extraneous detail has been omitted. However, those parts
15 which are common to all three figures have the same reference numerals.

Referring to Figure 3, a reactor for the processing of a gaseous medium consists of a reactor chamber 300
20 which has inlet and outlet fixing stubs 301 and 302, respectively. Within the reactor chamber 300 is a hollow cylindrical gas permeable bed 303 made of an active material adapted to carry out a desired process on the gaseous medium. For example, the active material may be
25 adapted to catalyse a reaction between one or more components of the gaseous medium. The bed 303 of active materials is contained between two co-axial cylindrical support members 304 and 305, which are gas permeable and two disk transverse supports 306 and 307, made of an
30 unpermeable material, as in the reactor described with reference to Figure 1. If the bed 303 is made of a material which is self supporting, the support members 304 and 305 can be omitted. As before, the support 306 nearer the inlet to the reactor chamber 300 has a number
35 of axially directed gas passages 308 around its periphery and the support 307 nearer the outlet from the reactor

- 7 -

chamber 300 has a central hole 309 of approximately the same diameter as the inner active bed support member 304. The inner active bed support 304 has a closed, domed end 310 which projects through the support 306 and
5 facilitates the deflection of the incoming gaseous medium towards the periphery of the reactor chamber 300. As with the reactor previously described, a gaseous medium entering the reactor chamber 300 is directed into the annular space 311 between the outer active bed support
10 305 and the wall of the reactor chamber 300 initially in an axial direction but is then constrained to pass radially through the bed 303 of active material.

However, in the present case, the reactor chamber
15 300 is not a true cylinder, but tapers in the direction of gas flow along the space 311 between the outer active bed support 305 and the wall of the reactor 300. As a result, the impedance to axial gas flow increases along the annular space 311 between the outer active bed
20 support 305 and the wall of the reactor chamber 300, so increasing the amount of gaseous medium which flows radially through the upstream part of the bed 303 of active material. A suitable taper angle is in the region of two degrees.

25

Figure 4 shows a second embodiment of the invention in which the diameter of the reactor chamber 300 is reduced half way along the bed 303 of active material. In a particular example, the width of the annular space
30 311 between the outer active bed support 305 and the wall of the reactor chamber is 10 mm initially and 5 mm for the second part of the reactor chamber 300. All other components are as for the reactor described with reference to Figure 3.

35

Figure 5 shows another embodiment of the invention in which there is a second step-wise reduction in the width of the annular space 311 between the outer active bed support 305 and the wall of the reactor chamber 300 half way along the second part of the bed 303 of active material. In another specific case, the widths of the regions of the annular space 311 between the outer active bed support 305 and the wall of the reactor chamber 300 are 10, 5 and 3 mm.

10

Figure 6 is a diagram showing the variation in radial gas flow along the bed 303 of active material for the embodiment of Figure 3. Compared with Figure 2 it can be seen that much more gas passes radially through first half of the bed 303 of active material. In fact the distribution of radial gas flow along the length of the bed 303 of active material is now approximately, symmetrical, but the middle two fifths, approximately of the bed 303 of active material still are underused.

20

Figure 7 is a diagram showing the variation in radial gas flow along the bed 303 of active material for the embodiment of Figure 4. More gas now passes radially through the first half of the bed 303 of active material than through the second half, with an intermediate peak at the position of the step where the width of the annular space 311 between the outer active bed support 305 and the wall of the reactor chamber 300 is halved. Immediately downstream of this position the radial gas flow rate is less than half that before it. This region of low gas flow extends about one fifth of the length of the bed 303 of active material.

Figure 8 is another gas flow diagram, similar to those of Figures 6 and 7, for the embodiment of Figure 5. It can be seen that this embodiment of the invention

gives the most even distribution of radial gas flow through the bed 303 of active material.

Figure 9 shows another embodiment of the invention in which the opposite approach to the problem is adopted. In this embodiment of the invention, instead of reducing the width of the gap 311 between the outer active bed support 305 and the wall of the reactor chamber 300 along the length of the bed 303 of active material so as to cause more gas to be diverted radially in the upstream regions of the bed 303 of active material, a number of axial expansion chambers 901 are provided along the first part of the reactor chamber 300. In this arrangement, not only is the impedance to axial gas flow higher in the second region of the reactor 300 than in the first region, but the expansion chambers 901 reduce the pressure of the gaseous medium as it enters the second region of the reactor chamber 300.

The invention has been described above in connection with gas reactors in general. As before, if the reactor is for use in the plasma-assisted processing of gaseous media, specifically, the treatment of the exhaust emissions from internal combustion engines to remove noxious combustion products therefrom, then the inner and outer active bed supports 304 and 305 are made of a metal such as stainless steel and used as electrodes, the outer one being earthed, as is the reactor chamber 300. Also, the transverse supports 306 and 307 have to be made of a temperature resistant insulating material. The material of the active bed 303 has to have a dielectric constant sufficient to enable a plasma to be established and maintained in the interstices within the bed of active material.

Claims

THIS SHEET HAS BEEN REPLACED

1. A reactor for the treatment of a gaseous medium,
including a cylindrical reactor chamber (300) having an
5 inlet port (301) and an outlet port (302) for a gaseous
medium to be processed, a hollow cylindrical gas
permeable bed (300) of an active material contained
within the reactor chamber (300) and substantially co-
axial therewith, an annular space (311) between the
10 outside of the bed of active material (303) and the
inside of the reactor chamber (300) and means (306) for
constraining the gaseous medium to enter the said annular
space (311) at one end in an axial direction, the other
end of said annular space (311) being closed to axial
15 flow of gaseous medium therefrom, the gaseous medium
passing radially through the bed (303) of active
material, characterised in that the said annular space
(311) is configured to provide an impedance to the flow
of the gaseous medium which increases along the length of
20 the said annular space (311) in the direction from the
said one end towards the said other end.

2. A reactor according to claim 1, further
characterised in that the width of the said annular space
25 (311) decreases continuously along the length of the said
annular space (311).

3. A reactor according to claim 1, further
characterised in that there is at least one discontinuous
30 decrease in the width of the said annular space (311)
along the length of the said annular space (311).

4. A reactor according to claim 3, further
characterised in that there is a single discontinuous
35 decrease in the width of the said annular space (311)



This Sheet Has Been Replaced



approximately at the middle of the said annular space (311)..

5. A reactor according to claim 3, further
5 characterised in that there are two discontinuous decreases in the width of the said annular space (311).

6. A reactor according to claim 5, further
characterised in that the first discontinuous decrease in
10 the width of the said annular space (311) occurs approximately at the middle of the said annular space (311) and the second discontinuous decrease in the width of the annular space (311) occurs approximately three
quarters along the length of the said annular space
15 (311).

7. A reactor according to claim 5, further
characterised in that the second discontinuous decrease
in the width of the said annular space (311) is less than
20 the first discontinuous decrease in the width of the said annular space (311).

8. A reactor according to claim 1, further
characterised in that a first portion of the reactor
25 chamber (300) is provided with at least one axially extending expansion chamber (901).

9. A reactor according to any preceding claim, further
characterised in that the bed (303) of active material is
30 contained between two co-axial gas permeable electrodes (304, 305) and two unpermeable transverse insulating supports (306, 307), the transverse support (306) nearer the inlet port (301) to the reactor has a plurality of axially directed gas flow passages (308) disposed around
35 its periphery, the transverse support (307) nearer the outlet port (302) of the reactor has a central hole (309)

This Sheet Has Been Replaced



* C L M S *

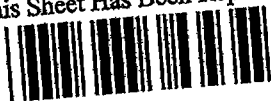
- 12 -

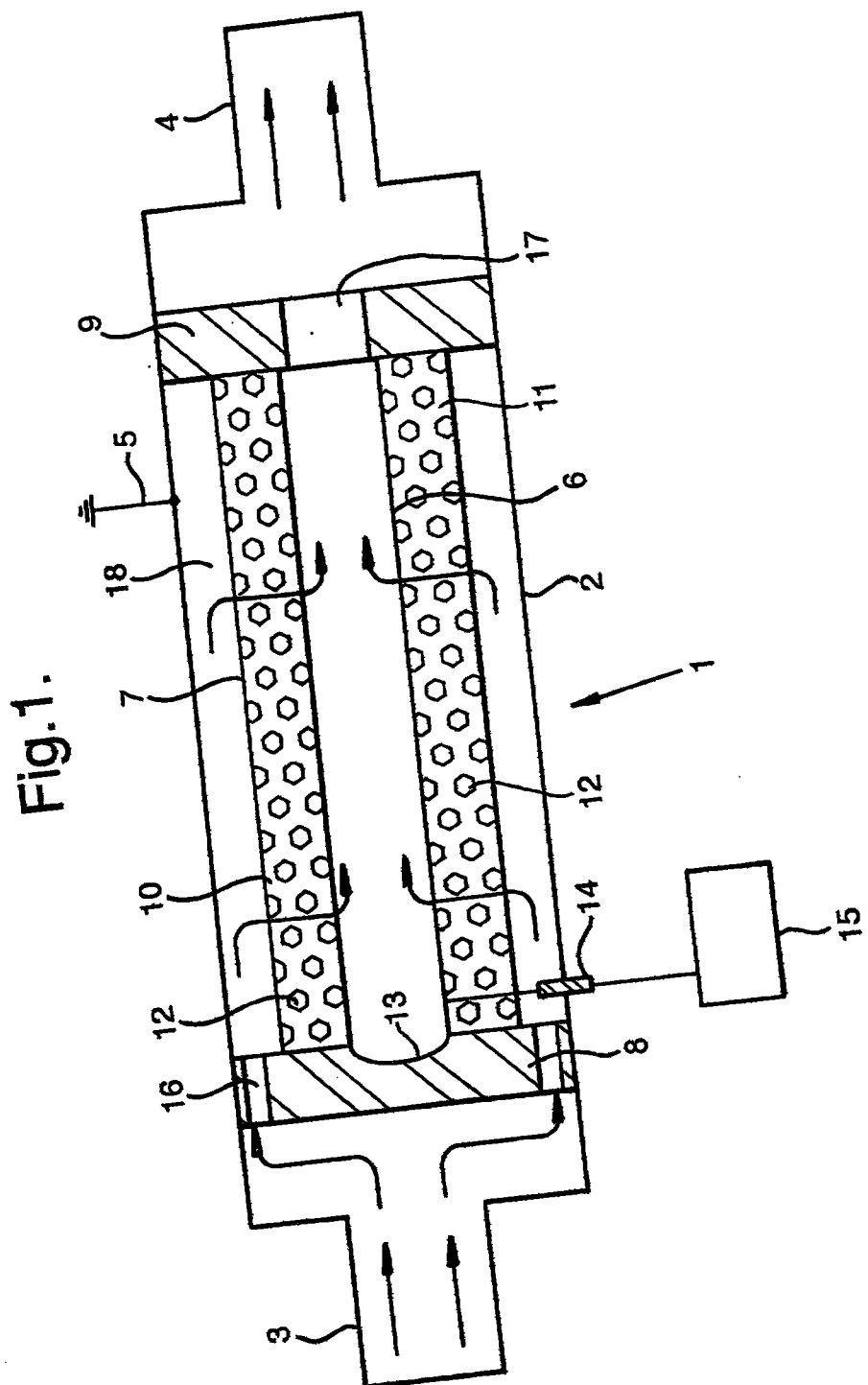
the diameter of which is approximately equal to the diameter of the inner co-axial electrode (304) and there is provided means for applying to the inner electrode (304) a potential sufficient to excite and maintain a
5 plasma in a gaseous medium passing through the bed (303) of active material.

THIS SHEET HAS BEEN
REPLACED



This Sheet Has Been Replaced

A standard 1D barcode with vertical black bars of varying widths on a white background.



2/4

Fig.2.

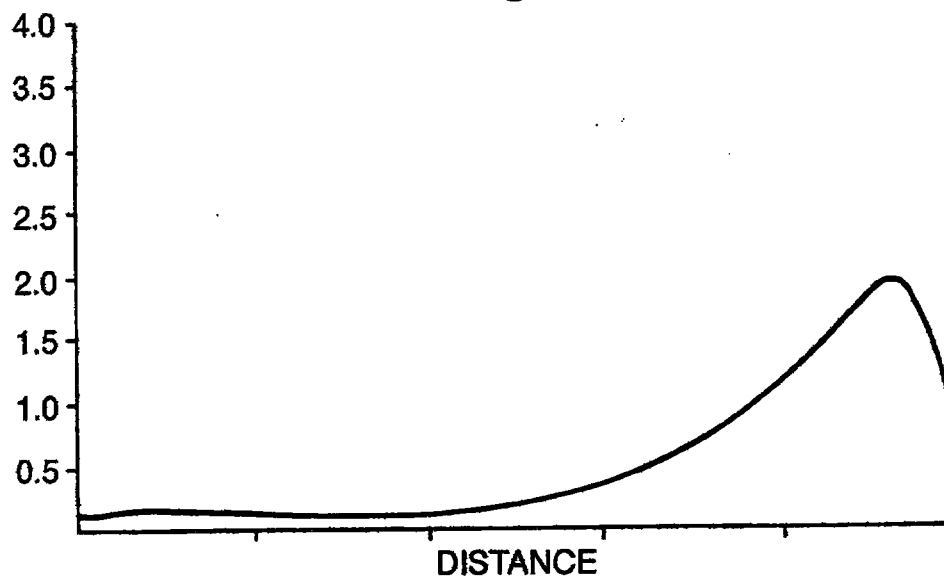
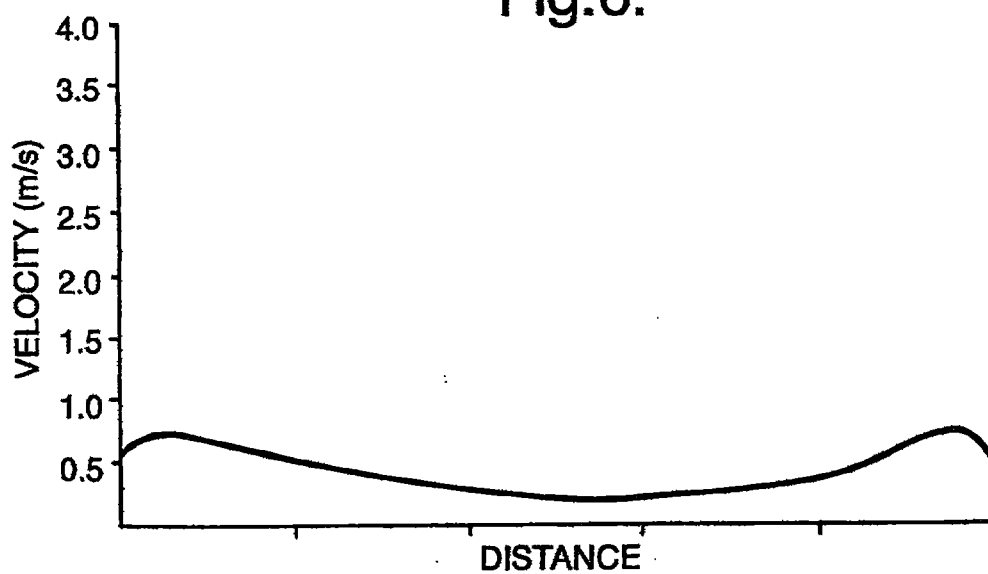


Fig.6.



3/4

Fig.3.

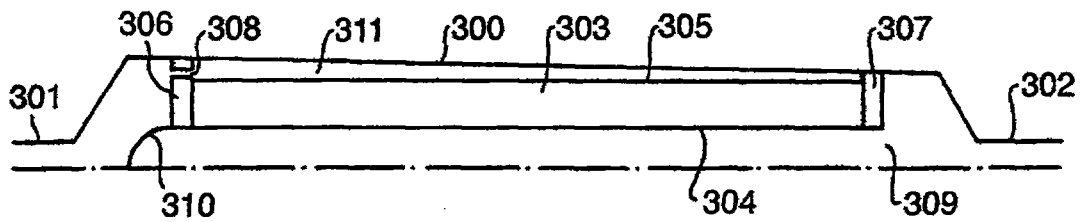


Fig.4.

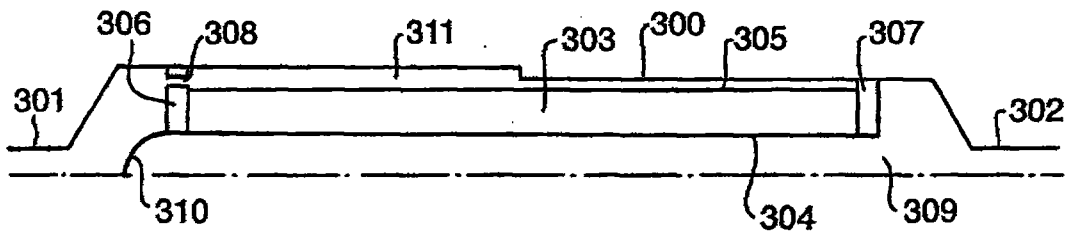


Fig.5.

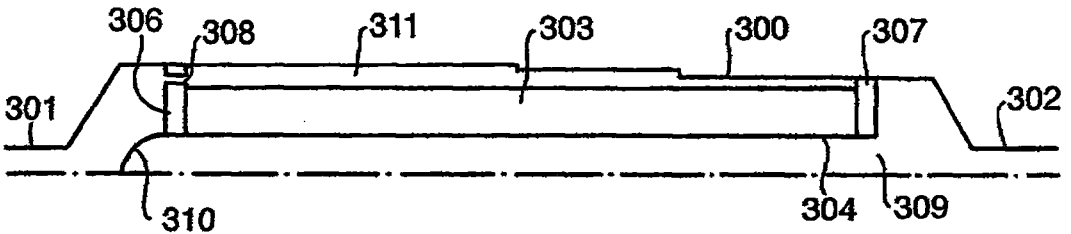


Fig.9.

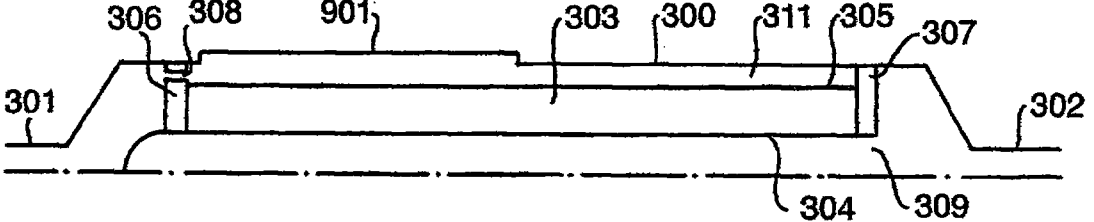


Fig.7.

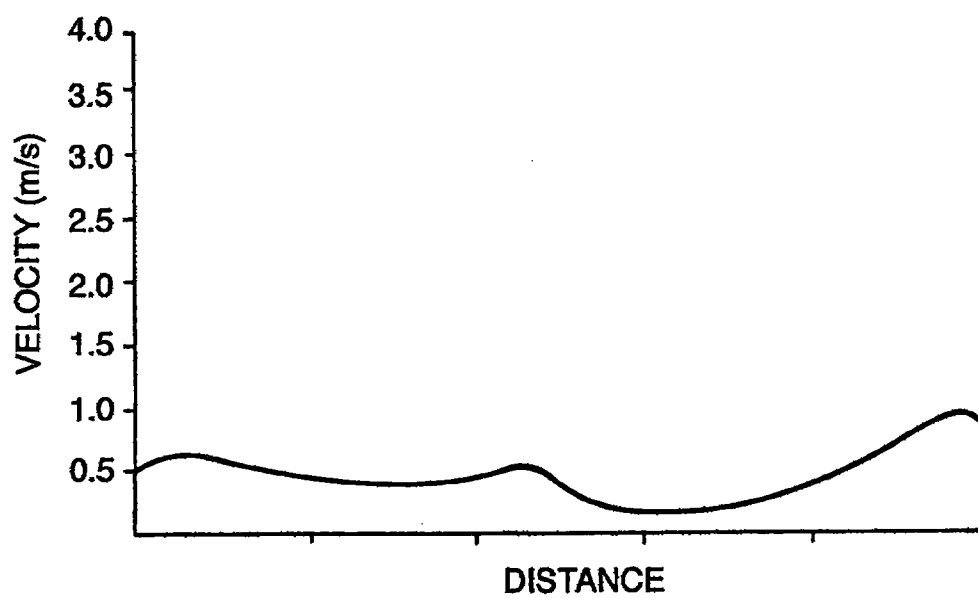
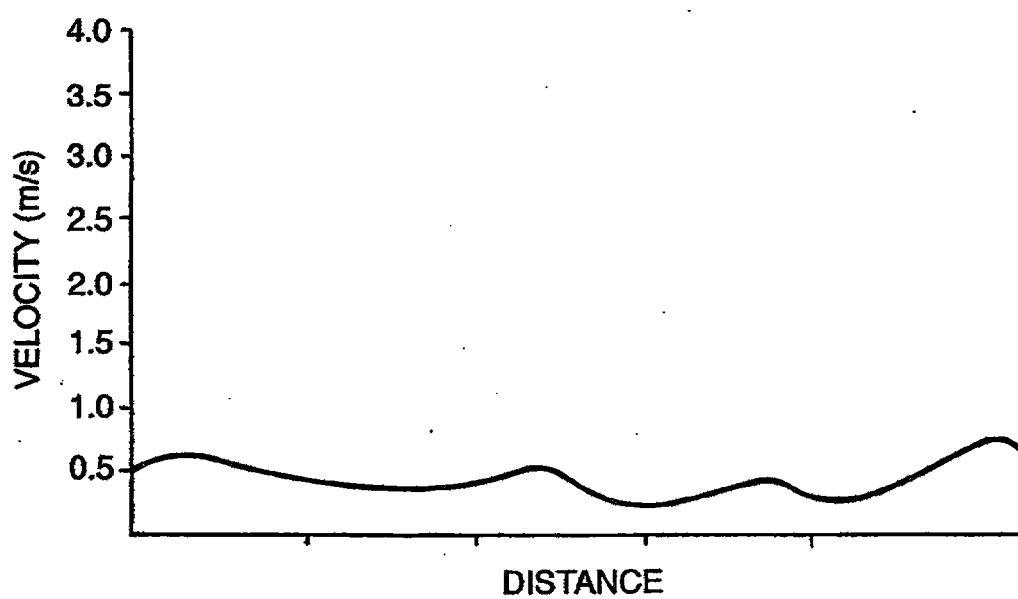


Fig.8.



- 1 -

The Optimisation of Gas Flow in Reactors for the
Treatment of Gaseous Media

The present invention relates to reactors for the
5 treatment of gaseous media and, more specifically to
reactors for the removal of noxious substances from the
exhaust gases from internal combustion engines.

One type of reactor for the treatment of gaseous
10 media consists of a cylindrical reactor chamber which has
inlet and outlet ports by means of which it can be
connected into a gas flow system. Inside the reactor
chamber, and co-axial within it, is a hollow cylindrical
gas permeable bed of active material. By the term "active
15 material", as used herein, is meant a material which
interacts with a gaseous medium to promote reaction
therein as the gaseous medium passes through the reactor.

A reactor of this type is shown in EP 0608619 (see
20 Figure 2). In a different configuration of reactor for
through flow of gaseous media, entering at one end and
exiting at the other, the bed of active material is held
in place by two supporting disks made of an impermeable
material. One support disk has a ring of axially
25 directed holes around its periphery and the other disk
has a central hole the diameter of which is approximately
equal to the inside diameter of the cylindrical bed of
active material. In use a gaseous medium to be processed
is admitted to the reactor chamber via the port closer to
30 the first support disk. The gaseous medium is then
directed into the annular space between the outside of
the cylindrical bed of active material and the wall of
the reactor chamber. The closure of this space by the
other support disk constrains the gaseous medium to pass
35 radially through the bed of active material prior to
leaving the reactor via the central electrode. The

- 2 -

support disks are made of a temperature resistant insulating material and there is provided an electrical connection to the inner electrode by means of which a potential of some kilovolts can be applied to the inner
5 electrode so as to establish a plasma discharge in the gaseous medium in the interstices in the gas permeable bed of active material.

In practice, it has been found that the gas flow
10 distribution through the bed of active material of such a reactor is uneven, being greater at the downstream end of the bed of active material. Thus the reactor may not operate at its maximum efficiency because the upstream end of the bed of active material may be underused while
15 the downstream end of the bed of active material may be subjected to a higher rate of gas flow than it can usefully process.

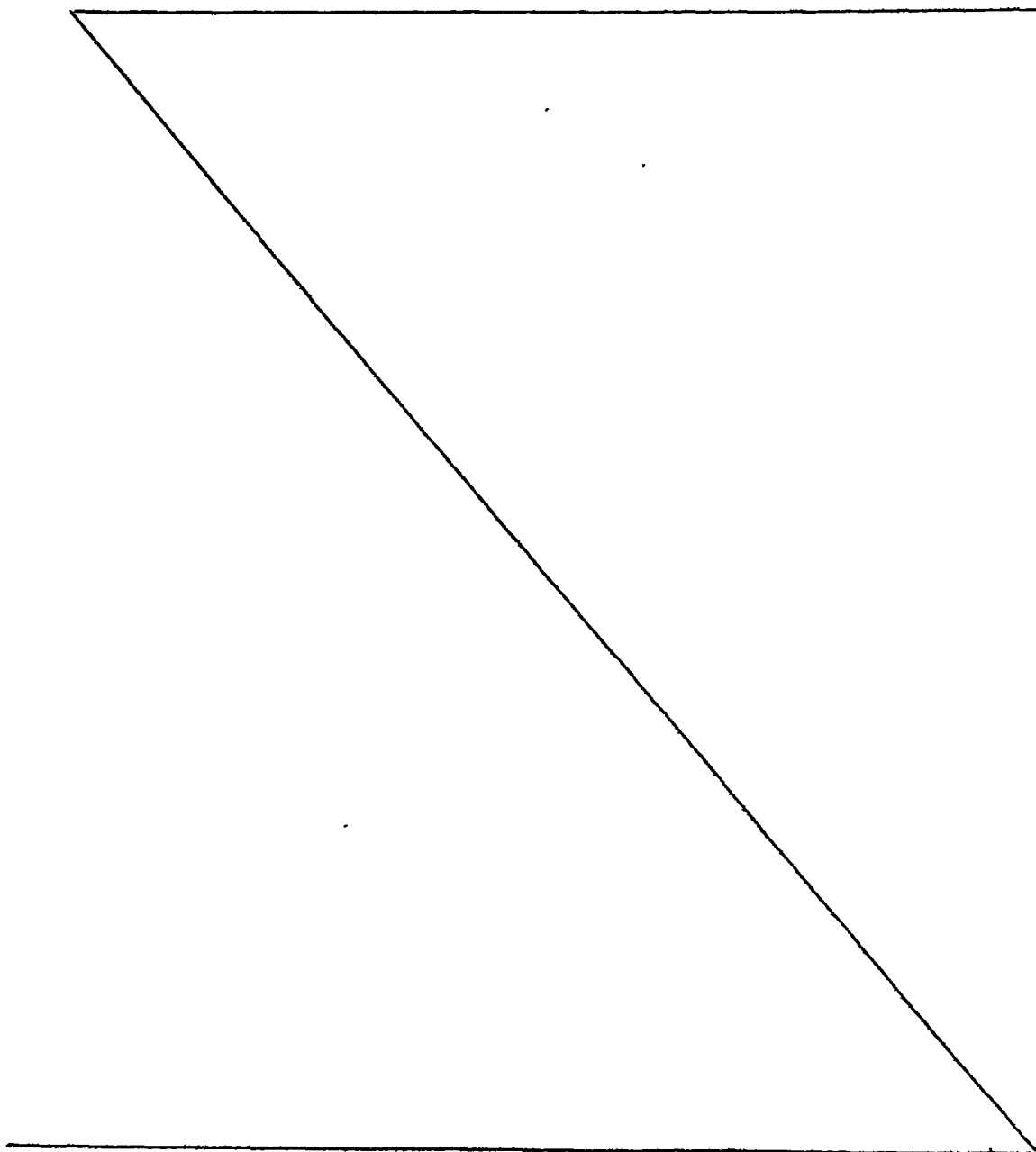
It is an object of the present invention to provide
20 an improved reactor of the type described above for the processing of a gaseous medium.

According to the present invention there is provided a reactor for the treatment of a gaseous medium,
25 including a cylindrical reactor chamber having an inlet port and an outlet port for a gaseous medium to be processed, a hollow cylindrical gas permeable bed contained within the reactor chamber and substantially co-axial therewith, the gas permeable bed comprising
30 catalytically active material for interacting with the gaseous medium to promote chemical reaction therein, an annular space between the outside of the bed of active material and the inside of the reactor chamber and means for constraining the gaseous medium to enter the said
35 annular space at one end in an axial direction, the other end of said annular space being closed to axial flow of

- 2a -

gaseous medium therefrom, the gaseous medium passing radially through the bed of active material, wherein the said annular space is configured to provide an impedance to the flow of the gaseous medium which increases along
5 the length of the said annular space in the direction from the said one end towards the said other end.

The increasing impedance to the axial flow of the gaseous medium through the said annular space preferably
10 is provided by progressively reducing the cross-sectional

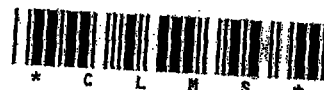


AMENDED SHEET

- 10 -

Claims

1. A reactor for the treatment of a gaseous medium, including a cylindrical reactor chamber (300) having an inlet port (301) and an outlet port (302) for a gaseous medium to be processed, a hollow cylindrical gas permeable bed (300) contained within the reactor chamber (300) and substantially co-axial therewith, the gas permeable bed comprising a catalytically active material for interacting with the gaseous medium to promote chemical reaction therein, an annular space (311) between the outside of the bed of active material (303) and the inside of the reactor chamber (300) and means (306) for constraining the gaseous medium to enter the said annular space (311) at one end in an axial direction, the other end of said annular space (311) being closed to axial flow of gaseous medium therefrom, the gaseous medium passing radially through the bed (303) of active material, characterised in that the said annular space (311) is configured to provide an impedance to the flow of the gaseous medium which increases along the length of the said annular space (311) in the direction from the said one end towards the said other end.
2. A reactor according to claim 1, further characterised in that the width of the said annular space (311) decreases continuously along the length of the said annular space (311).
3. A reactor according to claim 1, further characterised in that there is at least one discontinuous decrease in the width of the said annular space (311) along the length of the said annular space (311).
4. A reactor according to claim 3, further characterised in that there is a single discontinuous



- 11 -

decrease in the width of the said annular space (311) approximately at the middle of the said annular space (311).

5. A reactor according to claim 3, further characterised in that there are two discontinuous decreases in the width of the said annular space (311).

6. A reactor according to claim 5, further characterised in that the first discontinuous decrease in the width of the said annular space (311) occurs approximately at the middle of the said annular space (311) and the second discontinuous decrease in the width of the annular space (311) occurs approximately three quarters along the length of the said annular space (311).

7. A reactor according to claim 5, further characterised in that the second discontinuous decrease in the width of the said annular space (311) is less than the first discontinuous decrease in the width of the said annular space (311).

8. A reactor according to claim 1, further characterised in that a first portion of the reactor chamber (300) is provided with at least one axially extending expansion chamber (901).

9. A reactor according to any preceding claim, further characterised in that the bed (303) of active material is contained between two co-axial gas permeable electrodes (304, 305) and two unpermeable transverse insulating supports (306, 307), the transverse support (306) nearer the inlet port (301) to the reactor has a plurality of axially directed gas flow passages (308) disposed around its periphery, the transverse support (307) nearer the



- 12 -

outlet port (302) of the reactor has a central hole (309) the diameter of which is approximately equal to the diameter of the inner co-axial electrode (304) and there is provided means for applying to the inner electrode

5 (304) a potential sufficient to excite and maintain a plasma in a gaseous medium passing through the bed (303) of active material.

